Techno-economic optimization model for polygeneration hybrid energy storage systems using biogas and batteries

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1. Introduction

The need for a transition towards more sustainable energies has been recognized globally with various technologies competing while also complementing each other to provide more sustainable and secure energy-related services [1,2]. Amongst these technologies, small-scale biogas has gained increasing interest as a low-emission and locally available energy carrier with ecological and socio-economic benefits for developing regions in Africa, South-East Asia and Latin America [3]. With rising living standards, the usage of biogas as a cooking fuel may no longer be sufficient and advanced energy-related services like electricity will be in higher demand. However, despite of high scientific interest in small-scale biogas electricity generation [4], a broad-scale penetration of rural areas has not been observed [5]. This may be due to the drawbacks of higher complexity and increased capital costs outweighing the benefits. The concept of polygeneration offers the possibility of dramatically increasing the benefits by providing several energy-related services rendered with a relatively modest addition of complexity [6,7]. By increasing the total energy efficiency of the biogas systems and hence reducing losses, polygeneration also maximizes the utilization of the limited biogas resources. Such polygeneration systems serve apart from electricity also other energy-related services like hot water, cooling, or potable water by further using the heat inevitably produced in the biogas combustion process. In consequence, biomass-based polygeneration systems can decrease oil dependency and lower Greenhouse Gas (GHG) emissions [8]. Solar technologies like Photovoltaics (PV) can be added to decrease the amount of biogas usage and batteries can be used to extend the services of the solar energy beyond sunshine hours [9]. Despite the lower electric efficiencies, small-scale biogas-
based systems may prove to be the most efficient method to use biomass due to smaller transport paths compared to large systems [10].

Several authors have proposed specific small-scale polygeneration systems using biogas, water purification, solar and/or storage technologies: Kyriakarakos et al. [11] proposed a polygeneration system consisting of 4.8 kWp PV panels, a 3 kW wind turbine and a 1 kW fuel cell to generate electricity and to desalinate water with reverse osmosis technology. The system uses a Proton Exchange Membrane electrolyser to produce hydrogen as a transport fuel as well as batteries to cover electric loads for 3 days. Based on particle swarm optimization the results show that the optimal port fuel as well as batteries to cover electric loads for 3 days. Based on particle swarm optimization the results show that the optimal system is economically feasible for an off-grid island system with a probability of 90%, depending on fuel price fluctuations. Gazda et al. [12] developed an algorithm for biogas-based CCHP systems with various RES (Renewable Energy Sources) to evaluate the energetic and ecological efficiencies of facilities in the agri-food sector like distilleries, waste digesters, juice storage facilities etc. Using a 750 kW e biogas engine and ca. 228 kW PV panels, the system could lower GHG emissions by up to 67.4% and Primary Energy Savings kWe biogas engine and ca. 228 kW PV panels, hence allowing for electricity service during maintenance downtime of gas system components as well as for surpassing the energetic limitation of the biomass resources. The aim of this paper is to facilitate the design of polygeneration with a hybrid energy storage system (HESS) using biogas by developing a versatile model. Additionally, the benefits and drawbacks are to be analysed based on a case study. Hence, the scientific contribution of this paper is twofold:

1. Firstly, a novel model for economic optimization for a HESS using biogas storage coupled to a biogas ICE and batteries, is presented. The model applies a dispatch control algorithm, which can take into account photovoltaic energy as an additional energy source, so that even with insufficient biomass resources a given demand load can be satisfied. In order to allow for a highly efficient system design, the model calculates the thermal energy recovered from the engine.

2. Secondly, an innovative polygeneration system has been designed to identify the benefits of a HESS employing biogas and batteries controlled by the algorithm. By adding a MD subsystem, the energy efficiency of the total system is further increased and a second service is provided for an off-grid locality in Bolivia. Further considering the fertilizer in form of bio-slurry, the polygeneration system can provide up to three energy-related services: electricity, potable water, and fertilizer. The system is scrutinized with a techno-economic analysis in comparison with a diesel-based reference system in a case study.

After this introduction, the model approach is explained and one of many possible polygeneration layouts is presented in section 2. In section 3, the parameters and variables for the case study are described. The economic, energetic, as well as ecologic results are shown in section 4. The results and the model are discussed in section 5. Finally, conclusions on the algorithm and on the proposed polygeneration system are drawn in section 6.

1 Model and strategy description

The model aims to minimise the costs of the project over its lifetime. For this the Net Present Costs (NPC) are used, which are defined as follows in equation (1):

\[
\text{NPC} = \sum_{t=1}^{n} \frac{C_t}{(1+r)^t} + I
\]

where:

- \(C_t\): Costs in time period \(t\)
- \(r\): Discount rate
- \(I\): Initial investment

This equation takes into account the time value of money and allows for a comparison of alternatives with different lifetimes. The model considers both the economic and environmental benefits of polygeneration systems, providing insights into the most sustainable and cost-effective options for rural energy supply.
A graphic visualization of the algorithm is given for an optimization model of a polygeneration system. Unlimited biogas supply is assumed and the PV panel capacity remains 10% below its technical upper limit, the algorithm will signal to release biogas to the engine.

1. Check the state of storage of the biogas system. If the biomass storage is 10% below its technical upper limit, the algorithm will signal to release biogas to the engine.

2. Check the state of charge of the battery system.

3. Compare the electric load (after PV panels if included) with the capacities of battery discharge, converter discharge, and generator output.

4. Finally, the algorithm sets the generator output and the battery charging or discharging power. In case some load demand cannot be met the algorithm calculates the unmet load. Similarly, in case unused surplus power is generated, which can neither be used directly nor stored in the batteries, the model calculates the excess power.

A block diagram with a generic polygeneration system layout is shown in Fig. 1 and the optimization and analysis procedure of the model is shown in Fig. 2. The model is based on MATLAB (Version R2019a) and the Hybrid Optimization Model for Multiple Energy Resources HOMER (Version Pro 3.12.4). HOMER allows for a brute-force optimization approach running hundreds of simulations for all selected component sizes of the proposed polygeneration system. The connection to MATLAB allows for a more specific control of the energy storage and generation devices as well as for more precise calculations for the heat recovery. To validate the model behaviour under varying conditions firstly a white box testing approach with boundary value testing has been chosen with the results presented in the supplementary material [23]. Secondly, the model has been tested using results from a previous case study of a polygeneration system. The new dispatch (ND) control strategy has been used in a CCHP model and compared to the two most common strategies: load following (LF) and cycle charging (CC) [24]. The CCHP model has been presented in a previous study by Wegener et al. [25]. For the simulation, all input parameters have been kept equal while only the sizing of the biomass combustion system, the batteries, and the converter are being determined by the optimization model. Unlimited biogas supply is assumed and the PV panel capacity remains fixed.

The optimal component sizes for each strategy are shown in Table 1 and key results are shown in Fig. 3. Without biogas limitation, the ND strategy performs economically between the LF and the CC. However, the ND strategy requires less fuel and less engine operation time as the engine operates at higher efficiencies compared to the other two strategies. The results underline the universal applicability of the model and show that it optimizes biomass exploitation as aimed for.

2. Case description

2.1. Current electricity and water demand

For the case study, the locality of El Sena in Pando, Bolivia, has been chosen. In the reference case, the electricity demand of the inhabitants is covered by diesel-fuelled generators. These generators imply high GHG emissions and instability due to long fuel transport chains using unsecured roads. According to data from the national electricity agency (Autoridad de Fiscalización y Control Social de Electricidad) of Bolivia the total electricity demand of the village in 2016 was 1342.4 MWh with peaking values during the major harvest season in October [26]. For the daily demand profile, a typical demand profile of a rural community has been used with random variabilities of ±10% from day-to-day and ±10% from hour-to-hour.

\[ \text{NPC} = \sum_{t=0}^{n} \frac{R_{i}}{(1+i)\text{i}} = \sum_{t=0}^{n} \frac{CC_{j} + RC_{j} + OM_{j} + FC_{j} + SR_{j}}{(1+i)\text{i}} \] (1)

where \( R_{i} \) are the cashflows for year \( t \), \( i \) is the real discount rate and \( n \) represents the project lifetime. For each component \( j \), \( R_{i} \) is composed of all capital costs \( CC_{j} \), replacement costs \( RC_{j} \), costs and revenues for operation & maintenance \( OM_{j} \), fuel costs \( FC_{j} \), and salvage revenues \( SR_{j} \). The optimization problem can be expressed as shown in equation Eqn 2:

\[ \text{min NPC subject to } E_{cs} \leq E_{cs,\text{max}} \] (2)

where \( E_{cs} \) is the annual capacity shortage, where the energy system cannot satisfy the total electricity demand of the client, and \( E_{cs,\text{max}} \) is the maximum annual capacity shortage permitted to the system. As the NPC is determined by component size and component utilization, the model simulates in an iterative process the system performance for each component size as predetermined in a given search space. For a more general comparison of the economic performance in relationship to the energetic output the Levelized Cost Of Energy (LCOE) is used and calculated as follows in equation (3):

\[ \text{LCOE} = \frac{C_{\text{ann,tot}}}{E_{\text{served}}} \] (3)

where \( C_{\text{ann,tot}} \) are the annualized cost of the system [in $/yr] and \( E_{\text{served}} \) is the total electrical load served for one year [in kWh/yr]. To calculate \( C_{\text{ann,tot}} \) equation (4) is used:

\[ C_{\text{ann,tot}} = \frac{i \times (1 + i)^{n}}{(1+i)^{n} - 1} \times \text{NPC} \] (4)

where \( i \), \( n \), and \( \text{NPC} \) are defined the same as for equation (1). For the ecologic performance of the optimal system, the total mass of CO2-emissions \( m_{\text{CO2,\text{tot}}} \) is considered using equation (5):

\[ m_{\text{CO2,\text{tot}}} = m_{\text{CO2,\text{transp}}} + m_{\text{CO2,\text{comb}}} \] (5)

where \( m_{\text{CO2,\text{transp}}} \) and \( m_{\text{CO2,\text{comb}}} \) are the masses of emissions due to transport and combustion of fuel, respectively. The fuel used \( m_{\text{biog}} \) in relation to the electric output by the engine is calculated as shown in equation (6):

\[ m_{\text{biog}} = (IC \times P_{\text{gen,max}} \times \text{Slope} \times P_{\text{load}}) \times t \] (6)

where \( IC \) is the interception coefficient [in kg/(h·kW)]. \( \text{Slope} \) is the fuel slope [in kg/(kWh)], \( P_{\text{load}} \) is the electric load supplied by the engine [in kW], \( P_{\text{gen,max}} \) is the peak load capacity of the engine [in kW], and \( t \) is the duration of one time step [in h]. With the electrical output of the engine depending on its partial load behaviour also its thermal output is varying according to electricity generated.

The model employs a unique dispatch strategy based on IF-THEN statements, which allows for optimal utilization of local biomass resources. Although there are similar control algorithms for HESS [21,22], none have been developed for the combination of two independent energy storage modes (chemical/biogas and electrochemical/batteries) for an optimization model of a polygeneration system. A graphic visualization of the algorithm is given in the supplementary material. The objective of the algorithm is to operate the biomass engine as often as possible at maximum load and hence at maximum electric efficiency. The control algorithm operates according to the following order:

1. Check the state of storage of the biogas system. If the biomass storage is 10% below its technical upper limit, the algorithm will signal to release biogas to the engine.

2. Check the state of charge of the battery system.

3. Compare the electric load (after PV panels if included) with the capacities of battery discharge, converter discharge, and generator output.

4. Finally, the algorithm sets the generator output and the battery charging or discharging power. In case some load demand cannot be met the algorithm calculates the unmet load. Similarly, in case unused surplus power is generated, which can neither be used directly nor stored in the batteries, the model calculates the excess power.
to-hour [27]. The yearly electricity demand is shown in Fig. 4 and an exemplary weekly electricity demand for the first week in January is shown Fig. 5.

Additionally, the locality suffers from insufficient potable water provision as does the entire region of Pando [28]. This can cause higher infant mortality rates, more frequent malaria infections, and more cases of pneumonia. However, the production of potable water within the concept of polygeneration systems is especially attractive for remote areas with insufficient water access [29]. Therefore, the polygeneration system has been enhanced with a water purification subsystem based on thermally driven MD technology. For the potable water demand, a daily minimum of 3 l per person as proposed by the World Health Organisation’s guidelines for drinking water has been assumed [30]. With a population of 8,258, this means a potable water demand of 24,774 l/day for the entire locality.

2.2. RES potential and costs

As shown in Table 2, the biogas potential has been calculated based on the amount of animals and humans in the locality registered by the national statistics institute of Bolivia [31,32]. A collection factor has been added to account for any losses during the collection and transportation processes. The biogas price has been calculated based on the local average cow dung price with a value of 10 USD/ton [14]. An average transport distance of 50 km has been assumed due to the proximity of nearby localities and conservative average transport costs of 6.5 USD/t for manure and liquid slurry have been used in the calculations [33]. Considering further a price of 10 USD/t for cow dung [14], an average dry matter ratio of 20% and average biogas yield of 0.3 m³/kg DM (s. Table 3), a biogas price of 0.28 USD/Nm³ has been calculated.

The monthly average values for solar global horizontal irradiance (GHI) and the clearness are provided by the NASA Surface meteorology and Solar Energy database and are shown in Fig. 6 [34]. The clearness index indicates how much of the extraterrestrial horizontal radiation arrives on a horizontal surface on the earth. With an annual average radiation of 4.84 kWh/m²/day and an annual average clearness index of 0.50, the potential for solar energy can be considered as rather high.

2.3. Polygeneration system design

The polygeneration system designed for the case study is shown in Fig. 7. The biomass is transformed into biogas in the AD, where also bio-slurry is produced as a side-product, which can be used later as fertilizer. The biogas leaving the AD is cleaned using various technologies (filter, cyclones, scrubber etc.) and then pumped to the biogas storage dome. Whenever the engine is started, biogas is drawn by the gas engine and combusted to generate electricity and heat. In the first heat exchanger (HEx), the heat of the exhaust gases is transferred to the cooling liquid and the gases are then emitted into the environment. In the second HEx, the heat between the engine cooling circuit and the feed water circuit for water purification is exchanged. The heated feed water is pumped into various MD units. The cold side of the MD unit is connected to the AD in order to keep the AD at optimal temperatures above 35°C. A schematic diagram of the MD separation process is shown in Fig. 8 and another explanatory figure can be found in the supplementary material. A very informative and more detailed description of the purification process used in air gap MD systems has been provided by Noor et al. [38]. In case the cooling liquid is too hot, the temperature of the engine cooling liquid is further lowered for optimal engine cooling conditions in the third HEx and then returned to the engine. The kinetic energy of the engine shaft is transformed into electricity within the generator. The electric control system based on the dispatch control decides when to use the engine and/or the batteries to satisfy the electricity demand. The DC of the batteries and the PV panels is converted to AC using the converter and vice versa when excess energy from the engine is stored in the batteries [39].
Fig. 2. Optimization and analysis procedure of the best ranked system.
Table 1
Optimal component sizes of different dispatch strategies.

| Strategy/Comp. Size | Bio-Eng. (kW) | Batteries (kWh) | Converter (kW) | PV cap. (kW) |
|---------------------|---------------|-----------------|----------------|--------------|
| LF                  | 56            | 317             | 56             | 85           |
| CC                  | 40            | 365             | 45             | 85           |
| ND                  | 46            | 272             | 40             | 85           |

Fig. 3. System and component performance for various operating strategies.

Fig. 4. Hourly electricity demand for one year.
2.4. Technical inputs

Key technical variables for the model are shown in Table 3. The size of the AD has been calculated to 150 Nm³ based on the biomass availability shown in Table 2 and values provided by Teymoori Hamzehkolaei et al. [40]. The biogas production has been randomized within an hourly fluctuation of ±5% to account for inevitable process disturbances [41]. Furthermore, to account for downtimes, either scheduled (e.g. regular maintenance) or unscheduled (e.g. unexpected breakdowns), the biogas production has been set to zero for four days during three different occasions within the year (on the 1st of April, 1st of August and 1st of December) [42]. It has been assumed that the produced biogas has always the same chemical composition and hence the same LHV of 6.9 kWh/m³. For the additional electric load due to the AD system and gas storage, a value of 0.7 kWh per Nm³ of biogas stored has been assumed [43,44]. The dimensions of a biogas storage dome are based on a technical data sheet by Sattler Ceno TOP-TEX GmbH [45].

The engine performance based on the Patraus 370 BG CHP model by 2G Energy AG [46,47] is shown in Fig. 9. Exemplary values for HEx mass flows, temperatures, and heat transfers for a 370 kWe engine at full load are shown in the supplementary materials. Thermal efficiencies have been assumed to be 90% for the HEx and 90% for the MD unit [48]. Other losses (e.g. due to distribution) have been neglected. The minimum value of ΔT employed in the system is 3.16 K for the heat transfer between the jacket fluid and the heating circuit. In the simulations, all values have been adjusted proportionally depending on the optimal engine size calculated by the model.

2.5. Economic inputs

For the different parameters, values from scientific and commercial references have been used as shown in Table 4. Due to the rural environment with complicated access, additional transport and installation obstacles may arise during initial construction as well as for replacement. To account for these uncertain parameters, additional reserve costs of 500 kUSD have been assumed based on the authors’ experience with previous systems. For transport, the costs for renting trucks with drivers have been considered [33]. As the farmers can bring their biomass to sell it profitably, it has been assumed that they cover the transport costs of biomass and bio-slurry. For the bio-slurry, it has therefore been assumed that the bio-slurry will be distributed to the farmers in exchange for the transport costs. For the diesel price, the diesel opportunity price (1 UDS/l) has been chosen, which approximately represents the price for diesel on the international market [57].

### Table 2

| Biomass sources and production parameters | Bovine Animals | Poultry | Pigs | Human excrement | Organic food waste | Totals |
|------------------------------------------|---------------|---------|------|-----------------|-------------------|-------|
| Number                                   | 730 [32]      | 7287 [32] | 646 [32] | 8258 [31]      | 8258 [31]        |       |
| Daily production (kg/source/day) [35]    | 8             | 0.08    | 2    | 0.5             | 0.1               |       |
| Dry matter (DM) [35]                     | 16%           | 17%     | 25%  | 20%             | 34%               |       |
| Biogas yield per DM (m³/kg DM) [35]      | 0.2–0.3       | 0.25–0.5 | 0.35–0.8 | 0.35–0.5   | 0.5               |       |
| Biogas yield per prod. (m³/producer/day) | 0.320 [35]    | 0.010 [35] | 0.128 [35] | 0.040 [35]   | 0.019 [36]       |       |
| Collection factor                        | 0.9           | 0.9     | 0.9  | 0.5             | 0.5               |       |
| Total biogas yield (m³/day)              | 210.2         | 65.6    | 74.4 | 165.2           | 77.2              | 592.6 |
| Total biogas yield (kWh/day)             | 1460.0        | 455.4   | 516.8 | 1146.9          | 536.2             | 4115.4 |

1. With daily production – waste per human (0.2 kg/day)/organic waste ratio (50%) [36].
2. With an average energy value of 25 MJ/m³ or 6.9 kWh/m³ [37].

3. Results

3.1. Economic

The optimal component sizes for the polygeneration and the reference system are shown in Table 5. Although peak demand reaches up to 450 kW, demand values above 330 kW occur less than 1% of the time, which is the maximum permitted by the capacity shortage constraint. Hence in the reference case a 330 kW contribution is sufficient. Notably, the peak power output of the PV system exceeds the maximum conversion capacity of the converters so that nearly 500 MWh/year of excessive PV power are generated, which neither can be stored nor used directly. A larger converter or more batteries could prevent this albeit with an increase in costs. The required size of the PV panels would be equivalent to the size of one large football field [53]. The parasitic load due to biogas processing and water purification is equivalent to approx. 10% of the client load of the locality.

The NPC for each component and for each category is shown in Fig. 10. The total costs over the lifetime of 20 years for the polygeneration system are nearly 2 MUSD smaller than for the reference system equivalent to savings of more than 22%. This can be attributed mostly to the revenue from the water sales as well as diminutive costs for biomass compared to diesel. However, the capital investment costs as well as the replacement costs exceed those of the reference system by several million USD. At the end of the project lifetime, the salvage value of the battery system is approx. 1 MUSD, indicating that this set of batteries could still operate for several years after project termination. In direct comparison the LCOE of the polygeneration system is 27.4% lower with 0.297 $/kWh compared to 0.409 $/kWh for the reference system. The relatively larger difference in LCOE compared to NPC can be attributed mostly to the larger amount of electricity served by the polygeneration system, which is not accounted for by the NPC.
3.2. Energetic

An exemplary electricity generation curve for one week in October is shown in Fig. 11. For most days, the PV panels generate enough power during the day to simultaneously charge the batteries as well as to serve the electricity demand. After sunny days, the batteries can serve most of the demand with the engine operating only in the morning hours. However, after days with less PV output the engine has to start more often to serve the load while most often charging the batteries as well.

A summary of the yearly system inputs and outputs is given in Table 6. The extra demand for biogas storage and water purification raises the electricity demand slightly. As the biogas production only stops during maintenance days, bio-slurry is constantly produced at around 334 kg/h, while potable water production occurs only sporadically when enough heat from the engine can be utilized. The

### Table 3
Summary of the technical component input data.

| Component | Further characteristics |
|-----------|--------------------------|
| Anaerobic Digester (AD) system | Biogas composition: 60% CH₄ : 40% CO₂ [15]  
Biogas LHV: 6.9 kWh/m³ [37]  
Digest Volume: 150 Nm³ [40]  
Average hourly biogas production: 24.7 Nm³/h [40]  
Hourly fluctuation in production: ±5% [41]  
Yearly Downtime: 3 × 96 h [42]  
Mass transformation: 8% Biogas: 92% Slurry (s. Table 2)  
Electric load for pumps, clean-up, separation etc.: 0.7 kWh/Nm³ₙₐ₃,μₜₜ [43,44]  
Lifetime: 20 years [46] |
| Biogas storage system | Type: SATTLER double membrane gas storage dome tank - B9 127/250 [45]  
Dome volume: 3840 m³ (diameter: 21.1 m, height: 15.9 m) [45]  
Max. pressure: 20 mbar (low pressure zone) [45] |
| Biogas Engine CHP system | Based on Patruus 370 BG CHP system [46]  
Max. electric efficiency: 38% [13,46]  
Recovered thermal heat: 70% (Approx. thermal efficiency of 47%) [46]  
Total efficiency: 84% [46]  
Heating water outlet circuit temperature: 90 °C [46]  
Lifetime: 15,000 h [49] |
| Water Purification system | Air gap membrane lifetime: approx. 5 years [48]  
Remaining Air gap membrane distillation (MD) equipment: 20 years [48]  
Specific thermal consumption: 800 kWh/m³ [48]  
Specific electricity consumption: 0.35 kWh/m³ [48]  
Heat transfer to cooling circuit: 90% [48] |
| Battery system | Based on Generic 1 kWh Li-Ion battery model  
Depth of Discharge: 80% (equivalent to minimum SOC of 20%) [50]  
Approx. life cycles: 10,000 [51] |
| Converter | Hybrid converters  
Lifetime: 15 years [52] |
| PV system | Generic flat plate model  
Derating factor: 83% (equivalent to an electric efficiency of 17%) [53]  
Peak capacity per area: 170 W/m² [53]  
Lifetime: 25 years [53] |
| Diesel Engine reference system | Max. electric efficiency: 35% [54]  
Min. partial load: 40% [55]  
Lifetime: 15,000 h [56] |
| System constraints | Maximum capacity shortage $E_{c,max}$: 1%  
Operating reserve: 10% |

Fig. 6. Global horizontal irradiance (GHI) and clearness index for El Sena.
3.3. Ecologic

More than 3000 t/year of bio-slurry would be produced. With a max. load of 30 t [33], every three to four days one truck would have to collect biomass and redistribute the bio-slurry. The diesel consumption of the reference system would imply that a 30 t transport truck would have to arrive approximately every 12 days. As most petroleum in Bolivia is refined in the South, an average transport distance of 1350 km (distance from El Sena to Gualberto Villarroel Refinery) has been assumed. As shown in Table 7, the CO₂-emissions for the biomass system would lead to a reduction of more than 98% when compared to the reference system. The difference in CO₂-emissions between the two systems is visualized in Fig. 12.

3.4. Sensitivity analysis

The results of the sensitivity analysis for the economic performance of the polygeneration system and of the reference system are shown in Fig. 13. The polygeneration system performs better or close the reference case system for all scenarios with capital costs at 75% and 100%. Only with capital costs of 125% and low fuel prices of 75%, the polygeneration system can be outperformed by the fossil fuel based system. However, while the capital costs will be known beforehand and the biomass costs are dependent on only regional factors, the costs for diesel are very dynamic and dependent on many national as well as international factors out of the

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**Fig. 7.** System sketch of a particular bio-solar polygeneration system with hybrid storage.
municipality’s control. This leads to significant uncertainty for long-term financial planning.

4. Discussion

4.1. Polygeneration system

The biomass resources of the locality could not satisfy the electricity demand entirely, so that enhancing the system with solar technology is necessary when aiming for a 100% renewable energy system. In consequence, the algorithm calculated that large capacities of PV panels and batteries would be necessary. On the one hand, this leads to a flexible energy system, which relies on two different energy sources and hence is more resilient. On the other hand, this increases capital investment costs immensely, which could complicate the financing process when looking for public and private investors. Despite of the high capital investment costs, the polygeneration system has considerably lower project lifetime costs than the reference system. This is especially due to much lower fuel costs stemming from locally available biomass as well as due to the potable water sales, which would lower operation costs substantially. The sensitivity analysis showed that, when compared with the reference system, the polygeneration systems is much more robust towards changes in fuel prices but much more susceptible to changes in the capital investment costs. This indicates that once the polygeneration system is constructed the municipality will have a financially more secure and stable energy system. This is also why the sizing of the components and their consecutive costs are crucial for a cost-effective design of the entire system underlining the importance of the optimization algorithm.

Although the produced water could only satisfy 8% of the assumed minimum potable water demand of the locality, the provision of potable water at low costs is another incentive for the local administration to support the polygeneration system financially. The MD system can therefore be considered as a supplemental water supply system providing high quality water to clinics and other critical areas. A compromise between a bio-solar and a fossil-fuel based system could be contemplated, where the CO2-reduction potential may not be as high but the necessary investment costs could be lowered. A substitution of electricity from PV panels with more electricity from diesel combustion would also further increase the MD-subsystem operation time. This could also be a convenient solution in case the population and hence the
electricity demand rises beyond the expected scope of this study. Introducing the bio-slurry redistribution system would close the nutrition cycle, but also require a well-adjusted system for mass and nutrition flows [66]. Depending on the business strategy, more sophisticated post-treatment of the digestate can be contemplated in order to produce high quality fertilizer. A selling price for the fertilizer could further improve the system economics. The advanced technologies of the system would require several educational courses for local technicians and highly qualified personal as well as proper communication structures with the component manufactures for maintenance and reparation issues in order to operate the system safely. Considering further the complexity of the system, the planning and installation process should be carefully executed.

Table 4
Summary of the economic component input data.

| Component                                          | Characteristics                                                                                                                                 |
|----------------------------------------------------|-----------------------------------------------------------------------------------------------------------------------------------------------|
| Anaerobic Digester (AD) and biogas storage system  | Capital costs (for digester, clean-up, pumps etc.): 200 USD/m³ [40] Capital & Replacement costs: 200 USD/kW [40] O&M costs: 0.2 USD/kWh (Including AD and biogas storage system at 3000 working hours per year) [58] Biogas price: 0.28 USD/Nm³ (s. chapter 2.1.2) |
| Biogas Engine CHP system                           | Capital & Replacement costs: 200 USD/kW [40] O&M costs: 0.145 USD/l [59] MD unit capital & replacement costs: 390 USD/kWe (coupled to engine output) [16] MD unit attachments capital costs: 365 USD/kWe (coupled to engine output) [16] |
| Water Purification system                          | Capital & Replacement costs: 1000 USD/kWh [51] O&M costs: Negligible [56]                                                                         |
| Battery system                                      | Capital & Replacement costs: 1,800 USD/kW [62] O&M costs: 10 USD/kWe/year [62]                                                                    |
| Converter system                                    | Capital & Replacement costs: 700 USD/kW [60, 61] O&M costs negligible [60]                                                                       |
| PV system                                           | Capital & Replacement costs: 1,800 USD/kW [62] O&M costs: 10 USD/kWe/year [62]                                                                    |
| Diesel Engine reference system                      | Diesel opportunity cost: 1 USD/l [57] Capital/Replacement costs: 200 USD [52] O&M: 0.03 USD/op. hour [52]                                           |
| System economics                                    | Inflation rate: 4% [63] Nominal discount rate: 6% [63] Fin. reserves for uncertainties & engineering: 500 kUSD (s. chapter 2.1.5) Project lifetime: 20 years |

Table 5
Optimal system component parameters.

| Component              | Size                          | Yearly Production                  | Additional electricity expenses |
|------------------------|-------------------------------|-----------------------------------|---------------------------------|
| PV system              | 1075 kW (~6320 m² [53])      | 1602 MWh/yr (74%)                 | 486 MWh/yr (excess)             |
| Battery system         | 2250 kWh                      | 556 MWh/yr (annual throughput)    | 49 MWh/yr (losses)              |
| Converter system       | 450 kW                        | 1876 MWh/yr (Inverter output)     | 138 MWh/yr (losses)             |
| Biogas engine system   | 260 kW                        | 554 MWh/yr (26%)                  | 145 MWh/yr (parasitic demand)   |
| MD unit system         | Membrane area 16.7 m² (18 modules) | 800 m³/yr (~ 2190 l/day)          |                                 |
| Reference Diesel system | 330 kW                        | 1337 MWh/yr                       |                                 |

Fig. 10. Summary of the NPC values for the polygeneration system and the reference system.
4.2. Dispatch control

The results of the validation and of the case study show that the algorithm successfully optimized the system for project lifetime costs given the limitations of biomass and solar resources as well as the need to serve the electricity demand. However, optimizing the economic performance of the system is just one of many possible optimization objectives with another option being minimizing CO2-emissions. Even within the selection of economic parameters, a reduction of capital investments costs or operational costs may be favoured over project lifetime costs depending on the business strategy. Nonetheless, the algorithm can easily be adopted to optimize similar energy systems employing the strength of long- and short-term storage technologies (e.g. hydro-pump storage with super-capacitors). Using MD for potable water generation is only one of several possible extensions for the system to reach high energy efficiency by transforming the waste heat of the engine. Other possible extensions like hot water generation, room heating, refrigeration etc. can be considered depending on the system location and demand characteristics.

A considerable trade off of the control mechanism lies in the high flexibility it demands from the gas ICE, because sporadically turning the engine on and off leads to lower engine lifetime than continuous operation. When designing a polygeneration system with the help of the algorithm, it should be aimed for an engine that can withstand such exigencies. Nonetheless, modern gas engines used in the land transport sector should be able to comply easily with these requirements. Future investigations could also take into account a more dynamic biogas generation profile, where the biogas composition and hence the LHV value fluctuate. Alternatively, other less cost-oriented component size configurations could be studied, where a smaller biogas engine works more continuously and hence produces potable water more continuously, while the PV panels and batteries cover the major part of the electricity demand.

5. Conclusion

A model introducing a novel dispatch control strategy for the optimization of polygeneration HESS using biogas and batteries has been developed. The control algorithm regulates the two storage...
technologies with the aim to maximize capitalization on the biomass resources. The control strategy within the model allows for economic optimization of project lifetime costs under the constraints of biomass resource availability and electricity demand. If the amount of available biomass is insufficient to fulfil the electricity demand, PV panels and batteries are added as additional energy resource and storage options. The model calculates the residual thermal energy of the combustion process within the ICE in order to allow for a further increase in energy efficiency of the system via additional heat-driven energy-related services (e.g. water purification, heating, cooling, etc).

The model has been applied in a case study for a rural off-grid locality in Bolivia, where in the reference case a diesel-based system serves the electricity demand. The biogas potential has been calculated and a polygeneration system has been designed, which produces electricity, purified water, and fertilizer in form of bio-slurry. The polygeneration system performs economically much better than the reference system with 22% lower project lifetime costs and shows much more robustness towards fuel price changes according to the results of the sensitivity analysis. Nonetheless, high capital investment costs may be an obstacle for the realization of the project. As an additional advantage, CO2-emissions could be reduced by more than 98% and the locality could achieve a much more sustainable and autonomous energy and water supply system. The developed model can help scientists, engineers, and investors in the design process of renewable energy systems. Furthermore, it underlines that in rural areas smartly designed biomass-based polygeneration systems represent a viable economic alternative.

**Author contributions**

M.W. is the principal investigator of this work and wrote the manuscript. M.W. conceived and designed the control algorithm and system layout. J.V–S. has contributed greatly to the literature research. J. V–S., A.I., A.M. (Anders Malmquist), A.M. (Andrew Martin) and V.M contributed to data analysis work and manuscript structuring. All authors revised and approved the manuscript for publication.

**Declaration of competing interest**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.
Acknowledgements

This research has been conducted in collaboration between UPC (Universitat Politècnica de Catalunya) and KTH Royal Institute of Technology, funded through Erasmus Mundus Joint Doctoral Programme SELECT+, the support of which is gratefully acknowledged. The project STandUP for Energy provided resources for supervision of this study. AI acknowledges support from Spanish project MOET_BIA2016-77675-R.

Appendix A. Supplementary data

Supplementary data to this article can be found online at https://doi.org/10.1016/j.energy.2020.119544.

Appendix

Nomenclature

m_bio,AD biomass to AD
m_bog, unclean clean uncleaned biogas mass from AD
m_fert,AD fertilizer mass from the AD
m_bog, clean cleaned biogas mass from biogas clean-up
m_bog, fromstorage biogas mass from biogas storage
m_air, engine air mass to engine
mWP,cold,ln mass of cold water into water purifier
mWP,cold,Out mass of cold water out of water purifier
m_cooling, afterengine mass of cooling water after engine
m_exhgas, hot mass of exhaust gas after engine
m_exhgas, cold mass of exhaust gas after HEX1
m_cooling, afterHEX1 mass of cooling water after HEX1
m_cooling, afterHEX2 mass of cooling water after HEX2
m_cooling, afterHEX3 mass of cooling water after HEX3
m_CT,in mass of water into cooling tower
m_CT,Out mass of water out of cooling tower
m_feed,hot mass of hot feed water into water purifier
m_feed, cold mass of cold feed water into HEX2
m_feed,return mass of cold feed water from water purifier
m_cleanwater mass of cleaned water
m_make-upwater mass of make-up water
E_kinetic, engine electric energy of the engine
Eelectric, energy into or out of the batteries
E_MPV, cv energy from the MPV panels to the converter
E_MPV, bat energy from the MPV panels directly to the batteries
E_conv energy into or out of the converter
E_epd, client electric energy provided to the client

Abbreviations

AC/DC Alternating Current/DC Current
AD Anaerobic Digestor
CAES Compressed Air Energy Storage
CC Cycle Charging
CHP Combined Heat and Power
CCHP Combined Cooling, Heating and Power
LCOE Levelized Cost Of Energy
ICE Internal Combustion Engine
HHG Greenhouse Gases
ghi Global Horizontal Irradiation
PV Photovoltaic
HES Hybrid Energy Storage
HESS Hybrid Energy Storage System
HEX Heat Exchanger
MD Membrane Distillation
ND New Dispatch
RES Renewable Energy Sources
PES Primary Energy Savings

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