Article

Polyvinylnorbornene Gas Separation Membranes

Wouter Dujardin 1,2, Cédric Van Goethem 2, Julian A. Steele 2, Maarten Roëffaers 2, Ivo F. J. Vankelecom 2,* and Guy Koeckelberghs 1,*

1 Laboratory for Polymer Synthesis, Department of Chemistry, KU Leuven, Celestijnenlaan 200F, B-3001 Heverlee, Belgium; wouter.dujardin@kuleuven.be
2 Centre for Surface Chemistry and Catalysis, Department of Microbial and Molecular Systems, KU Leuven, Celestijnenlaan 200F, B-3001 Heverlee, Belgium; cedric.vangoethem@kuleuven.be (C.V.G.); julian.steele@kuleuven.be (J.A.S.); maarten.roe@kuleuven.be (M.R.); ivo.vankelecom@kuleuven.be (I.F.J.V.)
* Correspondence: guy.koeckelberghs@kuleuven.be

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Abstract: Polynorbornenes are already used in a wide range of applications. They are also considered materials for polymer gas separation membranes because of their favorable thermal and chemical resistance, rigid backbone and varied chemistry. In this study, the use of 5-vinyl-2-norbornene (VNB), a new monomer in the field of gas separations, is investigated by synthesizing two series of polymers via a vinyl-addition polymerization. The first series investigates the influence of the VNB content on gas separation in a series of homo and copolymers with norbornene. The second series explores the influence of the crosslinking of polyvinylnorbornene (pVNB) on gas separation. The results indicate that while crosslinking had little effect, the gas separation performance could be fine-tuned by controlling the VNB content. As such, this work demonstrates an interesting way to significantly extend the fine-tuning possibilities of polynorbornenes for gas separations.

Keywords: polynorbornene; addition polymerization; crosslinking; photoinitiator; TPO; gas separation; membrane; copolymerization; 5-vinyl-2-norbornene; free-standing membrane

1. Introduction

Norbornene (NB, bicyclo[2.2.1]-2-heptene) and its many derivatives are used in a wide range of applications such as photoresists, adhesives and rubbers [1–4]. They can be polymerized in various ways depending on the desired properties of the end material [5–7]. If ring-opening metathesis polymerization (ROMP) is used, rubbery polynorbornenes with an unsaturated backbone are formed. A second possibility is a vinyl-addition polymerization which typically produces polynorbornenes with rigid saturated backbones with high glass transition temperature ($T_g$) [8]. This variety of monomers and polymerization methods produces a wealth of different polynorbornenes which can be used for gas separation membranes [6,8–11]. Specifically, vinyl-addition polynorbornenes show a lot of promise as they have higher thermal stability, plasticization resistance and a rigid and sterically demanding bicyclic backbone [6,11]. This last property mimics the principles of polymers of intrinsic microporosity (PIMs) which have proven that high permeabilities could be obtained with soluble glassy polymers by having a rigid and contorted backbone [12–14].

The gas separation properties of many vinyl-addition polynorbornenes have been intensively studied [6]. Polynorbornene with trimethylsilyl groups showed an extremely high CO$_2$ permeability of 4350 Barrer but a low CO$_2$/CH$_4$ selectivity of 5.5 [15]. Recently, high CO$_2$ permeabilities were achieved (1350 Barrer) with a CO$_2$/N$_2$ selectivity of 17 by using a triethylsiloxane pendant side group [9] and impressive BET surface areas (420–970 m$^2$/g) were achieved with derivatized polynorbornenes [16]. From the wide variety of functionalized norbornene monomers that were used for gas separation
membranes, 5-vinyl-2-norbornene (VNB) was still missing. This is surprising as this monomer presents possibilities of copolymerization with other norbornenes, post-polymerization functionalizations and crosslinking, significantly increasing application and fine-tuning options (Figure 1). In this manuscript, a first step is taken by studying the influence of the copolymerization with NB and the crosslinking with a photoinitiator on the gas separation performance.

First, a series of copolymers of NB and VNB was synthesized to study the influence of the exocyclic vinyl group on gas separation. Previous results have shown that the gas permeability is extremely dependent on the size of the side chain: Replacing hydrogen with a mere methyl group can result in a permeability increase from 34–49 to 81–396 Barrer [6,7,15,17]. Therefore, the VNB feed content in a series of polynorbornenes using NB and VNB was varied using 0% (only NB), 25%, 50%, 75% and 100% (only VNB). A Pd catalyst was used, capable of specifically targeting the cyclic double bond and leaving the exocyclic double bond intact. The resulting copolymer membranes were then tested for their gas separation performance.

Crosslinking is often used to improve gas separation performances by fine-tuning retention and permeance or by increasing plasticization resistance [18–20]. Therefore, a second series was developed involving the crosslinking of polyvinyl norbornene (pVNB) using its exocyclic vinyl group with a photoinitiator. It is known that polymers with unsaturated carbon bonds in their backbone, such as with ROMP polynorbornenes, are degraded by UV irradiation [21,22]. In contrast, vinyl-addition polynorbornenes with an unsaturated side group, such as 5-ethylidene-2-norbornene, are suitable for this type of crosslinking [21,22]. A well-known photoinitiator, diphenyl(2,4,6-trimethylbenzoyl)phosphine oxide (TPO), was chosen as photoinitiator as it offers a beneficial balance between photostability and photoreactivity [23]. This balance is important to control the degree of crosslinking. Various TPO loadings in the membrane were used to introduce varying degrees of crosslinking and their influence on the gas separation performance was assessed.

2. Materials and Methods

2.1. Materials

All solvents were purchased from Chem-Labs (Zedelgem, Belgium), VWR (Oud-Heverlee, Belgium) or Fisher Scientific (Merelbeke, Belgium). All reagents were purchased from Acros Organics (Geel, Belgium), AK Scientific (Union city, CA, USA), Sigma-Aldrich (Overijse, Belgium), Fischer Scientific (Merelbeke, Belgium) or J&K Scientific (Overpelt, Belgium). Toluene was dried by a solvent purification system MBRAUN SPS 800. Other solvents and reagents were used as received unless...
specified otherwise. NB was sublimed under reduced pressure. All reactions were done in oven-dried or flame-dried apparatus under nitrogen or argon atmosphere.

2.2. Characterization Methods

Proton nuclear magnetic resonance (\(^{1}H\) NMR) spectra were recorded on a Bruker Ascend 400 MHz or a Bruker Avance II 600 MHz spectrometer. Infrared spectra were recorded on a Bruker Alpha FT-IR-spectrometer equipped with a Platinum ATR single reflection ATR module. A 2 cm\(^{-1}\) resolution was used with 24 scans. Gel permeation chromatography (GPC) measurements were carried out on a Shimadzu 10A GPC system. The column was a PLgel 5 µm mixed-D type column which is kept at 35 °C. High-performance liquid chromatography (HPLC) grade tetrahydrofuran (THF) or chloroform were used as solvent with a flow rate of 1.0 mL/min. The detection system consisted of a differential refractometer. The GPC system was calibrated toward polystyrene standards purchased from Polymer Laboratories. The polymer samples were dissolved in the same solvent mixture as used for the GPC with a concentration of about 1 mg/ml. Once dissolved, the samples were filtered over a polytetrafluoroethylene (PTFE) filter with a pore size of 0.2 µm. The X-ray diffraction patterns were collected in transmission mode on a STOE Stadi P high-throughput powder diffraction apparatus equipped with a CuKα X-ray tube (\(\lambda = 1.5418 \text{ Å}\)) and an image plate detector. The \(T_g\) of the polymers was recorded using differential scanning calorimetry (DSC). The measurements were performed with a TA Instruments Q2000-DSC. DSC samples were prepared by weighing 4–7 mg pieces of membrane in Tzero Aluminium Hermetic pans and calibration was done towards an empty pan. A heating rate of 10°/min was employed up to 340 °C under nitrogen flow, after which the sample was cooled to 25 °C at the same rate. The thermal degradation temperature and dryness of the membranes were tested by TGA under nitrogen atmosphere. A TA Instruments TGA-Q500 was used with 5 mg polymer membrane samples on a platinum pan. The samples were kept isothermal for 5 min at 50 °C after which they were heated at 20 °C/min up to 700 °C. The membrane cross-section microstructure was visualized by using a Jeol JSM-6010LV scanning electron microscope operated at 10 kV. The cross-sections were obtained by freeze-fracturing the samples in liquid nitrogen. All samples were sputter coated with Au/Pd for two times 30 s by a Jeol JFC-1300 autfine sputter coater in order to minimize sample charging during imaging. The membrane thickness was measured by a Mitutoyo Disk micrometer (369-511-30, ±4 µm). For UV induced crosslinking, a UV chamber with 3 LEDs (365 nm, output power 200 mW) was used. Raman scattering spectra were recorded using a home-built optical microscope (Ti-U, Nikon) in confocal mode. An air objective of 0.92 NA and 60× magnification was used to focus the 632.8 nm line of a He-Ne laser for Raman excitations. The optical power density was regulated using neutral density filters and a 650 nm long-pass filter was employed to filter Rayleigh scattering. Dispersion was achieved using a 600 g/mm, resulting in a spectral resolution of 0.5 cm\(^{-1}\).

2.3. Polymerization

2.3.1. Polynorbornene (pNB)

Dichloromethane (DCM) was dried by refluxing with CaH\(_2\) and subsequent distillation. The solvent was then stored on molecular sieves. NB (940 mg, 10.0 mmol) was weighed in a flask and put under dry atmosphere. Next, DCM (4 mL) was added. After dissolution, Ni(C\(_6\)F\(_5\))\(_2\)(SbPh\(_3\))\(_2\) (10.8 mg, 10.0 µmol) was added. After 10 s, white precipitate formed. The mixture was then poured in 200 mL acetone and stirred for 1 h. Afterwards, the mixture was filtrated and the resulting white polymer was dried under reduced pressure at 60 °C.

Yield: 0.556 g of white fibers (58%).

2.3.2. pNB-VNB-50 Using Ni(C\(_6\)F\(_5\))\(_2\)(SbPh\(_3\))\(_2\)

NB (942 mg, 10.0 mmol) and 5-vinyl-2-norbornene (1.43 mL, 10.0 mmol) were dissolved in 3 mL dichloromethane. While stirring, Ni(C\(_6\)F\(_5\))\(_2\)(SbPh\(_3\))\(_2\) (21.6 mg, 20.0 µmol) was added and the flask
was brought under dry atmosphere. Another 3 mL dichloromethane was added and the reaction was continued at 30 °C for overnight. Afterwards, the reaction mixture was poured in stirring methanol, forming white fibers. The fibers were collected by filtration over a filter and analyzed by GPC.

2.3.3. pVNB Using Ni(C₆F₅)₂(SbPh₃)$_2$

The same methodology was used as with pNB-VNB-50 using the same catalyst. 5-vinyl-2-norbornene (600 mg, 5.00 mmol) was polymerized with Ni(C₆F₅)₂(SbPh₃)$_2$ (5.40 mg, 5.00 µmol).

2.3.4. pNB-VNB-50 Using Pd$_2$dba$_3$/AgSbF$_6$/PPh$_3$

NB (1.84 g, 20.0 mmol) and 5-vinyl-2-norbornene (2.40 g, 20.0 mmol) were mixed, purged with N$_2$ and sonicated. Toluene was purged with N$_2$ and sonicated as well. Meanwhile, Pd$_2$dba$_3$ (9.20 mg, 10.0 µmol, 20.0 µmol of Pd), AgSbF$_6$ (10.3 mg, 30.0 µmol) and PPh$_3$ (5.30 mg, 20.0 µmol) were added to a flask and put under dry atmosphere. Toluene (4 mL) was added to the solids and the mixture was heated to 70 °C. The norbornene mixture was added to the catalyst solution using a transfer needle. After 15 h, a brown gel-like solid had formed and no free solvent was visible. The solid was transferred to a beaker and toluene (70 mL) was added, dissolving the solid. The polymer was then measured on GPC.

2.3.5. pVNB Using Pd$_2$dba$_3$/AgSbF$_6$/PPh$_3$

The same methodology was used as with pNB-VNB-50 using the same catalyst. The 5-vinyl-2-norbornene (36.0 g, 300 mmol) was polymerized with Pd$_2$dba$_3$ (27.5 mg, 30.0 µmol, 60.0 µmol of Pd), AgSbF$_6$ (24.8 mg, 72.0 µmol) and PPh$_3$ (15.7 mg, 60.0 µmol) using 30 mL toluene.

2.3.6. pVNB Using Pd$_2$dba$_3$/TTPB/PCy$_3$

In a 25 mL flask, Pd$_2$dba$_3$ (9.10 mg, 10.0 µmol), triphenylcarbenium tetrakis(pentafluoro)borate (TTPB, 18.4 mg, 20.0 µmol), PCy$_3$ (5.60 mg, 20.0 µmol) and toluene (20 mL) were added. This solution was brought under inert atmosphere and stirred for 5 min. In a 50 mL flask under inert atmosphere, 5-vinyl-2-norbornene (1.20 g, 10.0 mmol) was added and stirred. 10 mL of the catalyst solution and 20 mL of toluene was added to the monomer. The reaction temperature was set at 40 °C and the polymerization was continued for 5 h. Afterwards, the solution was poured in methanol, yielding white fibers. The fibers were collected by vacuum filtration over a filter and dried under vacuum at room temperature overnight.

Yield: 1.12 g of white fibers (93%).

2.3.7. pNB-VNB Copolymers Using Pd$_2$dba$_3$/TTPB/PCy$_3$

The copolymers were made using the same modus as pVNB. The specific monomer amounts and resulting yields are summed up in Table 1.

| NB VNB Yield | Yield | Yield |
|--------------|-------|-------|
| pNB-VNB-25   | 706 mg| 7.50 mmol | 300 mg | 2.50 mmol | 754 mg | 75% |
| pNB-VNB-50   | 471 mg| 5.00 mmol | 601 mg | 5.00 mmol | 836 mg | 78% |
| pNB-VNB-75   | 235 mg| 2.50 mmol | 901 mg | 7.50 mmol | 935 mg | 82% |

2.4. Membrane Preparation

The membranes of pNB, pNB-VNB-25, pNB-VNB-50, pNB-VNB-75 and pVNB were prepared by dissolving 400 mg of polymer in 20 mL of chloroform. After 5 days of stirring, the solutions were filtrated and the resulting clear solutions were poured in Teflon Petri dishes (4.7 cm diameter).
These Petri dishes were covered with a blocked funnel and put in a nitrogen glove bag. After at least 40 days of drying, they were used for gas separation and membrane characterization tests.

The crosslinked membranes (pVNB-0%, pVNB-0.13%, pVNB-1.3%, pVNB-33%, pVNB-65%) were prepared by adding 6.75 mL of the polymer solution containing 193 mg pVNB to a flask. Then, the respective amounts of TPO were added and the total volume was diluted to 14 mL. These solutions were filtered and subsequently poured in Teflon Petri dishes (4.7 cm diameter), which were covered with a blocked funnel, shielded from light and put in a nitrogen glove bag. After 5 days of drying, they were put in a UV chamber at 365 nm for 1 h to crosslink the membranes. The inner temperature of the UV chamber did not exceed 50 °C, making thermal crosslinking unlikely. After crosslinking, the membranes were soaked in methanol for 5 h to remove excess TPO and its degradation products. The membranes were collected from methanol and dipped dry with a towel. Next, they were dried under vacuum at 70 °C for 12 h. The gas separation tests were done within 24 h after drying.

2.5. Gas Separation Measurements

The gas separation properties were assessed using high-throughput gas separation equipment [24]. The experiments were performed at 35 °C, feed pressure was set at 2.5 bar and the permeate side was kept under vacuum. For the mixed-gas tests, a 50/50 mixture was used at 5 bar. The permeate gas composition was determined by a compact gas chromatograph (Interscience).

The mixed-gas selectivity was calculated by Equation (1) with \( x_i \) and \( y_i \) the mole fractions of gas \( i \) in, respectively, the up and downstream:

\[
\alpha_{ij} = \frac{y_i / y_j}{x_i / x_j}
\]  

The mixed and single-gas permeability of the membrane was determined by recording the increase in gas pressure in a fixed volume cylinder using Equation (2):

\[
P_i = \frac{273 \times 10^6}{760} \frac{y_i V}{A T (\frac{273}{T_1})} \frac{dP}{dt} x_i / P_2
\]  

With \( V \) the downstream volume in cm\(^3\) and \( dP / dt \) is the pressure rate. \( A \) refers to the membrane area in cm\(^2\), \( T \) is the cell temperature in Kelvin, and \( P_2 \) is the feed pressure in Psi.

3. Results

3.1. Polynorbornenes with Increasing VNB Content

3.1.1. Polymerization and Characterization

Polynorbornene (pNB) was easily synthesized using the catalyst Ni(C\(_6\)F\(_5\))\(_2\)(SbPh\(_3\))\(_2\) [10] (Table S1, entry 1). However, synthesizing polymers made with 5-vinyl-2-norbornene proved to be more difficult. Neither Ni(C\(_6\)F\(_5\))\(_2\)(SbPh\(_3\))\(_2\) or Pd\(_2\)dba\(_3\)/AgSbF\(_6\)/PPh\(_3\) [25] were capable of obtaining large molecular weights with a monomer mixture of NB and VNB (ratio 50:50) or with only VNB (Table S1, respectively entries 2-3 and 5-6). VNB is known to be challenging to polymerize as the exocyclic vinyl group can act as a reactive site for chain transfer [26] or it can slow the catalyst down by sterical hindrance or coordination [26,27]. Since large molecular masses are required to obtain mechanically stable membranes, another catalyst system was employed using Pd\(_2\)dba\(_3\)/TTPB/PCy\(_3\) [26] (Table S1, entries 4 and 7), resulting in number average molecular weights above 167 kg/mol. This proved to be sufficient for producing mechanically stable free-standing membranes. Therefore, with this catalyst system, a series of polynorbornenes with varying VNB content were synthesized. During workup, aliquots were taken for GPC analysis in THF (Table 2, Figure S1). The aliquots did not precipitate in THF, but had difficulty passing through a 0.2 \( \mu \)m filter. Possibly, the higher molar mass chains were retained,
resulting in an underestimation of the real molar masses. Still, high molar masses were obtained for all polymers.

Table 2. Reaction and GPC data for polynorbornene series with increasing exocyclic vinyl group presence. Calibrated using polystyrene standards.

| Polymer     | Catalyst                | Monomer Catalyst | Yield | \(\overline{M}_w\) (kg/mol) | \(\overline{M}_n\) (kg/mol) | D  |
|-------------|-------------------------|------------------|-------|-----------------------------|-----------------------------|----|
| pNB         | Ni(C₆F₅)₂(SbPh₃)₂      | 1000             | 58%   | 84                          | 277                         | 3.3|
| pNB-VNB-25  | Pd₂dba₃/TTPB/PCy₃      | 1000             | 75%   | 121                         | 263                         | 2.2|
| pNB-VNB-50  | Pd₂dba₃/TTPB/PCy₃      | 1000             | 78%   | 167                         | 440                         | 2.6|
| pNB-VNB-75  | Pd₂dba₃/TTPB/PCy₃      | 1000             | 82%   | 104                         | 198                         | 1.9|
| pVNB        | Pd₂dba₃/TTPB/PCy₃      | 1000             | 93%   | 349                         | 471                         | 1.4|

\(\text{data obtained in THF, }^{b}\text{ data obtained in chloroform.}\)

The solubility of the polymers after drying proved to be challenging. pNB, pNB-VNB-25 and pNB-VNB-50 were soluble in chloroform. pNB-VNB-75 and pVNB were stored in solution as they would become insoluble after drying. As a consequence, not all solvent could be removed, resulting in large residual solvent signals in the NMR spectra (Figure 2). The \(^{1}\text{H NMR spectra showed that the polymers were monomer free as no sharp correlating monomer signals are present in the polymer spectra. Also, by equalizing the vinyl proton signal intensity (4.5–6.5 ppm), a gradual decrease in aliphatic signals (0.5–2.5) is visible. This indicates that an increasing amount of VNB to NB is built in, which is in accordance with the monomer composition. The integration of the signals indicate that for pNB-VNB-25 and for pNB-VNB-50 respectively about 31% and 55% VNB was built in (Figures S10 and S11). These values may be slightly overestimated due to the presence of solvent signals in the aliphatic region (e.g., water).}

![Figure 2](image_url)

**Figure 2.** \(^{1}\text{H NMR spectra, from top to bottom, of pNB, pNB-VNB-25, pNB-VNB-50, pNB-VNB-75, pVNB and the monomer VNB. Residual solvent signals from work up are marked in spectra of less soluble pNB-VNB-75 and pVNB.}\)**

The free-standing membranes were analyzed by Fourier-transform infrared spectroscopy (FT-IR) (Figure 3). Analyzing the spectra with increase in VNB content, it is clear that the purple regions, related to the unsaturated C=C and C–H bonds, increase in intensity while the orange regions, related to the saturated C–H bonds, decrease in intensity. This confirms the conclusion from the NMR spectra: NB-VNB copolymers can be synthesized by controlling the VNB content in the polymerization feed.
Figure 3. FT-IR of polynorbornene membranes with various amounts of VNB built in. Purple regions are unique for alkenes, while orange regions are related to saturated C–H bonds.

Raman, which is highly sensitive to the C=C stretching vibration, allow for a deeper analysis of the VNB content in the polymer membranes, by analyzing the relative changes in the C=C signal at 1637 cm\(^{-1}\). For this, the Raman spectra were recorded across different VNB feed concentrations using their common and invariant CH\(_x\) signatures just below 3000 cm\(^{-1}\) and were subsequently normalized. As such, the relative intensity of the C=C signal in the material can be quantified and compared directly. This analysis is presented in Figure 4, which exhibits a near perfect correlation between VNB content in the monomer feed and the C=C signal strength at 1637 cm\(^{-1}\). This correlation is in accordance with the VNB content analysis by NMR signal integration for pNB-VNB-25 and pNB-VNB-50. Such an approach may facilitate a direct means of analyzing the VNB content when such details are not known.

Figure 4. Raman analysis of the membranes. Left: A comparison of the Raman signals recorded over the C=C vibrational band. To facilitate the comparison and analysis leading these data, the C=C band intensity has been normalized relative to their common CH\(_x\) band at 2950 cm\(^{-1}\) (Figure S7). Right: The C=C signal intensity at 1637 cm\(^{-1}\) is plotted against the VNB content in the monomer feed.

Scanning Electron Microscopy (SEM) was used to view the cross-sections of the membranes (Figure 5). All membrane cross-sections show homogeneous dense films.
Three interesting trends are visible with an increase in VNB content (Figure S3). The degradation temperature of pVNB at 5% mass loss was 350 °C, indicating high thermal stability. No \( T_g \) was detected under 340 °C, confirming the rigidity of the polynorbornenes (Figure S5).

Figure 5. SEM pictures of the cross-sections of the polynorbornene membranes. All membranes were imaged using the same magnification (×500). Larger images and images with higher magnification can be found in the supporting information.

Thermogravimetric analysis (TGA) showed no discernable pattern with increasing VNB content (Figure S3). The degradation temperature of pVNB at 5% mass loss was 350 °C, indicating high thermal stability. No \( T_g \) was detected under 340 °C, confirming the rigidity of the polynorbornenes (Figure S5).

The wide-angle X-ray scattering (WAXS) pattern of the polynorbornenes included two broad peaks, indicating that the polymers are completely amorphous (Figure 6). It is generally accepted that the peak at higher \( 2\theta \) correlates with intrasegmental interactions while the peak at lower \( 2\theta \) correlates with intersegmental interactions [15,28,29]. Three interesting trends are visible with an increase in exocyclic vinyl group presence in the polymers. First, the intrasegmental peak broadens at higher VNB content. This can be explained by the increasing presence of the exocyclic vinyl groups which may be capable of increasing the amorphous character of the intrasegmental packing. Second, the intersegmental peak shifts from 10° to 8.4°. This corresponds, using Bragg’s law, with a \( d \)-spacing shift from 8.8 to 10.5 Å, indicating that the increase in exocyclic vinyl group presence considerably increases intersegmental \( d \)-spacing. Third, relatively increasing scattering intensities of the low \( 2\theta \) peak with increase in VNB content indicates that more numerous intersegmental scattering events took place compared to the intrasegmental scattering. Therefore, based on these observations, an increase in exocyclic vinyl group content seems to benefit larger intersegmental spacing. Comparing this data with other addition type polynorbornenes with different side groups, it is clear that the X-ray scattering data for pNB is similar to previously published pNB X-ray data (Table 3) [17]. Also, the intersegmental \( d \)-spacing of pVNB is situated between the intersegmental \( d \)-spacings of polynorbornene with a methyl group and with a butyl group, further confirming the trend that intersegmental \( d \)-spacing increases with increasing side-group bulkiness [28,30].

Figure 6. Normalized WAXS spectra of polynorbornenes with increasing VNB content.
Table 3. WAXS data for addition type polynorbornenes with different side groups (R).

| Polynorbornene       | 2θ [''] | d-Spacing [Å] | Ref            |
|----------------------|---------|---------------|----------------|
|                      | Low Angle | High Angle | Low Angle | High Angle |               |
| pNB                  | 10       | 18.5         | 8.8       | 4.7       | [17]          |
| pNB (R: –CH₃)        | 9.5      | 18.2         | 9.3       | 4.9       | this work     |
| pVNB                 | 8.4      | 18.6         | 10.5      | 4.8       | this work     |
| pNB (R: n–C₄H₉)      | 7.2      | 18.8         | 12.2      | 4.7       | [30]          |
| pNB (R: –Si(CH₃)₃)   | 6.5      | 15.5         | 13.6      | 5.7       | [15]          |
| pNB (R: –n–C₆H₁₃)    | 6.6      | 19.2         | 13.5      | 4.6       | [30]          |

3.1.2. Gas Separations

First, the membranes were tested for CO₂/CH₄ and CO₂/N₂ separations using a mixed-gas feed (Figure 7) to investigate the influence of the exocyclic vinyl group. The permeability quadrupled for both gas pairs with increasing VNB content, while α_{CO₂/CH₄} declined slightly and α_{CO₂/N₂} remained largely constant, even though trends hardly exceed the experimental error. Single-gas permeabilities were collected as well to easily compare them with other published data (Table 4). Unfortunately, the membrane pNB-VNB-25 had become defective and was left out of the analysis. For the permeabilities, a trend is visible confirming the previous mixed-gas permeabilities: By increasing the VNB content, the permeability increases. pVNB even achieved a CO₂ permeability of 104 Barrer. This is also in line with the WAXS trend which shows that a larger VNB content resulted in larger d-spacings. The permeabilities obtained in this work for pNB are close to those previously published [15]. The permeabilities of pVNB are close to the one of the polynorbornenes with a methyl side group [28]. The ratio of two single-gas permeabilities gives the ideal selectivity of that gas pair. The ideal selectivity differs from mixed-gas selectivity in the sense that it allows for a more direct comparison with other single gas measurements and the resulting ideal selectivities, but it does not take into account any interactions between the mixture components as is the case with mixed-gas selectivity. These ideal selectivities show a slight decrease with increase in VNB content (Table 5). In the case of H₂/CO₂, this even results in a reverse selectivity for pVNB.

Figure 7. (Left) Mixed-gas selectivity and (right) mixed-gas permeability for CO₂/CH₄ and CO₂/N₂ for the series of polynorbornenes with increasing VNB content.
These loadings were chosen as they cover a broad range, enabling the detection of interesting effects both in the lower and higher loading region. The crosslinking mechanism is explained in Figure 8.

3.2. Crosslinking of pVNB

3.2.1. Polymerization, Crosslinking and Characterization

The exocyclic vinyl group offers possibilities such as post-polymerization functionalization and crosslinking. In this section, the influence of crosslinking on the gas separation properties such as mixed-gas selectivity and permeability and CO\(_2\) plasticization is investigated. Therefore, five crosslinked polymer membranes were prepared from pVNB with the following TPO loadings: 0 mol % (pVNB-0%), 0.13 mol % (pVNB-0.13%), 1.3 mol % (pVNB-1.3%), 33% (pVNB-33%) and 65% (pVNB-65%). These loadings were chosen as they cover a broad range, enabling the detection of interesting effects both in the lower and higher loading region. The crosslinking mechanism is explained in Figure 8.

Table 4. Single-gas permeability data of polynorbornenes with increasing VNB content after 100 days of aging and other polynorbornenes with different side groups (R) performances.

| Polynorbornenes | Catalyst | Single-Gas Permeability [Barrer] | Ref. |
|-----------------|----------|----------------------------------|------|
| pNB             | Ni \(^a\) | CH\(_4\) (2.0 ± 0.7) CO\(_2\) (28.2 ± 5.3) N\(_2\) (1.9 ± 0.5) | This work |
| pNB-VNB-50      | Pd \(^b\) | CH\(_4\) (5.7) CO\(_2\) (85.3) N\(_2\) (3.6) | This work |
| pNB-VNB-75      | Pd \(^b\) | CH\(_4\) (3.9 ± 0.1) CO\(_2\) (60.8 ± 2.1) N\(_2\) (2.5 ± 0.1) | This work |
| pVNB            | Pd \(^b\) | CH\(_4\) (8.3 ± 1.4) CO\(_2\) (104.3 ± 3.2) N\(_2\) (4.8 ± 1.0) | This work |
| pNB             | Ni \(^c\) | CH\(_4\) (2.6) CO\(_2\) (33.6) N\(_2\) (1.5) | 15 |
| pNB (R=CH\(_3\))| Ni \(^d\) | CH\(_4\) (5.6) CO\(_2\) (81.1) N\(_2\) (4.3) | 28 |
| pNB (R=Si(CH\(_3\))\(_3\)) | Pd \(^d\) | CH\(_4\) (16.9) CO\(_2\) (202.1) N\(_2\) (12.6) | 28 |
| pNB (R=Si(CH\(_3\))\(_3\)) | Ni \(^d\) | CH\(_4\) (790) CO\(_2\) (4350) N\(_2\) (297) | 15 |

\(^a\) Ni(C\(_6\)F\(_5\))\(_2\)(SbPh\(_3\))\(_2\), \(^b\) Pd\(_2\)dba\(_3\)/TTPB/PCy\(_3\), \(^c\) Ni \([(\text{Nph})\text{Ni}]\)-methylaluminoxane, \(^d\) no further information on the catalyst was given.

Table 5. Ideal selectivity of polynorbornenes with increasing VNB content.

| Polynorbornenes | Single-Gas Selectivity |
|-----------------|------------------------|
|                 | CO\(_2\)/CH\(_4\) | CO\(_2\)/N\(_2\) | \(\text{H}_2\)/CO\(_2\) | \(\text{H}_2\)/CH\(_4\) | \(\text{H}_2\)/N\(_2\) |
| pNB             | 15.0 ± 2.9 | 15.5 ± 1.3 | 2.1 ± 0.0 | 31.7 ± 6.5 | 32.7 ± 3.1 |
| pNB-VNB-50      | 14.9 | 23.4 | 1.1 | 15.7 | 24.6 |
| pNB-VNB-75      | 15.6 ± 0.1 | 24.2 ± 0.1 | 1.1 ± 0.0 | 16.6 ± 0.1 | 25.8 ± 0.1 |
| pVNB            | 12.9 ± 1.6 | 22.4 ± 3.5 | 0.9 ± 0.0 | 10.9 ± 1.1 | 18.9 ± 2.5 |

3.2. Crosslinking of pVNB

Figure 8. (1) TPO produces two initiator (In) radicals by exposure to UV light. (2) The initiator radicals start a radical polymerization with the exocyclic vinyl groups, thereby crosslinking pVNB.

The extent of crosslinking was first assessed by FT-IR (Figure S2) where no measurable difference in C=C stretching or bending signals were found. In contrast, Raman clearly showed a decrease in
C=C signal at 1637 cm$^{-1}$ with an increase in TPO loading (Figure 9). This confirms that the extent of crosslinking can be controlled by varying the TPO loading. However, no full conversion could be obtained as even with 65 mol % TPO, only about 55% of vinyl groups were converted.

Crosslinking surprisingly had a slightly detrimental effect on the thermal stability (Figure S4). As double carbon bonds are converted into single carbon bonds, a higher thermal stability, close to that of pNB would be expected. This is probably caused by the lower thermal resistance of TPO, possibly still present in the membrane [31]. Yet, no clear trend is visible within the membranes with higher TPO loading. Normally, as crosslinking increases chain rigidity, a higher $T_g$ is expected for crosslinked polymers. No $T_g$ was measured up to 250 °C using DSC (Figure S6). Higher temperatures were not feasible due to the decreased thermal resistance of the membranes with higher TPO loading.

SEM was used to view the cross-sections of the polymer membranes, showing homogeneous dense films (Figure 10).

3.2.2. Gas Separations

Defect-free membranes were obtained from pVNB-0%, pVNB-1.3%, pVNB-33% and pVNB-65%. Mixed-gas CO$_2$/CH$_4$ selectivity and permeability were measured to assess the influence of the crosslinking on the gas separation (Table 6). Overall, low to modest selectivities were obtained with no particular trend. The permeability declines with increasing TPO loading. This can be due to the presence of crosslinks, tightening the polymer network and, therefore, decreasing the size of the free volumes, resulting in lower permeability. Additionally, the presence of excess TPO and its degradation products can fill up the free volume, which also results in lower permeability. Overall, these results demonstrate that crosslinking pVNB has little benefit to its gas separation performance. Nevertheless, in combination with high-permeability polynorbornenes, such as those with a trialkylsilyl side chain, copolymerization with VNB and subsequent crosslinking might improve stability, possibly leading to high-performance gas separation membranes.
Table 6. Mixed-gas properties of pVNB crosslinked with different TPO loadings.

| pVNB with TPO Loading | \( P_{CO2/CH4} \) [Barrer] | \( \alpha_{CO2/CH4} \) |
|-----------------------|-----------------------------|----------------------|
| pVNB-0%               | 26.8 ± 3.3                  | 18.9 ± 1.2           |
| pVNB-1.3%             | 20.0                        | 22.0                 |
| pVNB-33%              | 9.8 ± 0.4                   | 21.9 ± 0.2           |
| pVNB-65%              | 14.3 ± 1.7                  | 19.4 ± 3.5           |

3.3. Robeson Plot

Robeson plots are used to put the gas separation performance of pVNB and its derivatives in perspective to other polynorbornenes and state-of-the-art polymers for the gas pairs \( CO_2/CH_4 \) and \( CO_2/N_2 \). Robeson plots are ubiquitous to compare gas separation performances of polymer membranes to each other and to the ‘upper bound’, a line visualizing the trade-off between permeability and selectivity [32,33]. Typically, only single-gas permeability and ideal selectivity are used for a Robeson plot. However, both single and mixed-gas data were collected in this research. While single-gas data collection has the advantage to quickly scan through multiple gas pairs, it lacks the capability to assess the interaction between the different gas molecules. To calculate the permeability of 1 species from a mixed-gas experiment, Equation (3) was used, while the interaction between the different gas molecules was assumed negligible.

\[
P_i = \frac{P_{mixed}}{(1 + \frac{1}{\alpha_{mixed}}) \times x_i}
\]

\( P_{mixed} \) is the mixed-gas permeability, \( \alpha_{mixed} \) mixed-gas selectivity and \( x_i \) the mole fraction of gas \( i \) in the upstream. The Robeson plots (Figure 11) show that selectivity of the crosslinked polynorbornenes is a little higher and their permeability somewhat lower than the polynorbornenes with increasing VNB content. This latter series’ performance is close to the performance of one of the two polynorbornenes with a methyl side chain. Compared to the other polynorbornene derivatives, overall better selectivities are obtained with largely comparable permeabilities. In comparison with state-of-the-art polymers (black), relatively modest performances are obtained by using polynorbornenes.

![Figure 11](image-url) (Left) \( CO_2/CH_4 \) and (Right) \( CO_2/N_2 \) Robeson plots with polynorbornenes with increasing VNB content (blue), pVNB with increasing TPO loading (purple), other polynorbornenes (pink) and polyimides, PIMs and thermally rearranged polymers (black). * Single-gas \( P_{CO2} \) data [Barrer] obtained using Equation (3). Data obtained from [7,9,15,28,34–44]. Upper bound data was taken from [33].
4. Conclusions

The use of VNB was introduced as a new building block for polynorbornenes gas separation membranes. Two series of membranes were prepared: A series varying the VNB content from pure pNB to pure pVNB and a series with varying extent of pVNB crosslinking. With increasing VNB content, higher permeabilities and lower selectivities were obtained, which was in agreement with increasing d-spacings, as measured by WAXS. With an increasing degree of crosslinking, the selectivity did not change significantly, while the permeability decreased. Overall, compared to other polynorbornenes, similar permeabilities with higher selectivities were obtained. Compared to state-of-the-art polymers (e.g., PIMs), the gas separation performance is still modest. As this polymer class has the potential to provide chemically and thermally robust polymers which can be easily synthesized, further research into new building blocks and methods of fine-tuning the polymer properties should be used in order to improve their basic gas separation performance.

Supplementary Materials: The following are available online at http://www.mdpi.com/2073-4360/11/4/704/s1, Table S1: GPC data of homopolymers pNB and pVNB and copolymers pNB-VNB-50, prepared by different catalyst systems. Figure S1: GPC spectra of polynorbornenes with increasing vinyl content. Figure S2: FT-IR of pVNB with increasing TPO loading. ‘TPO’ and ‘TPO - UV’ are, respectively, unexposed and exposed TPO to UV light. Figure S3: TGA thermogram of polynorbornenes membranes with increasing VNB content. Figure S4: TGA thermogram of crosslinked polynorbornenes membranes. Figure S5: DSC of polynorbornenes with increasing VNB content. Figure S6: DSC of polynorbornenes with increasing TPO loading. Figure S7: Comparison of Raman spectra recorded over the CH2 stretching region, for rising VNB in monomer feed. These spectra have been normalized relative to their common band at 2950 cm−1, which does not evolve with changing VNB concentration, allowing for the C=C band analysis shown in Figure 4 of the main article. Figure S8: Comparison of Raman spectra recorded over the CH2 stretching region, for increasing TPO content in the pVNB membranes. These spectra have been normalized relative to their common band at 2950 cm−1, which does not evolve with changing VNB concentration, allowing for the C=C band analysis shown in Figure 9 of the main article. Figure S9: SEM images of polynorbornene copolymers with increasing VNB content. Figure S10: 1H NMR spectrum of pNB-VNB-25. (400 MHz, CDCl3). Figure S11. 1H NMR spectrum of pNB-VNB-50. (400 MHz, CDCl3).

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