Simulation study on dynamic characteristics of gas diffusion in coal under nitrogen injection

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To reveal the mechanism of desorption of methane in coal seams by inert gas N2, the desorption behavior of CH₄ after N₂ injection was studied by using Giant Canonical ensemble Monte Carlo (GCMC) and Molecular Dynamics (MD) methods with wiser bituminous coal as the research object. The results show that the adsorption isotherms of CH₄ and N₂ in the molecular structure model of bituminous coal are in good agreement with the Langmuir adsorption isotherm model. The adsorption capacity of the two gases in the bituminous coal structure model is CH₄ > N₂. The higher the N₂ injection pressure, the higher the temperature, and the more methane desorption. N₂ can replace some adsorbed CH₄ through competitive adsorption with CH₄. Compared with injecting high-temperature nitrogen to desorb methane in coal seams, in high-pressure nitrogen, the diffusion effect of CH₄ flowing in coal is more significant. The higher the nitrogen injection pressure, the better the effect of N₂ promoting CH₄ desorption. The relative concentration of CH₄ in the vacuum layer gradually increases with the increase of water content. This indicates that the water in coal promotes the desorption of CH₄. The mechanism of N₂ injection and CH₄ desorption in coal seams mainly includes gas displacement and gas dilution and diffusion. This study provides theoretical support for methane extraction technology in goaf.

Gas injection mining is an important stimulation technology for CBM development. For coal seams with poor gas permeability, low permeability, and rapid borehole gas flow decay, traditional negative pressure drainage takes a long time and achieves slow results, which can no longer meet the needs of mining replacement and underground safety production. Coal seam gas injection not only increases the internal pressure of the coal body and increases the gas seepage velocity, but also reduces the effective partial pressure of gas and promotes the desorption of adsorbed gas. Therefore, it is of great significance to study CBM gas injection stimulation technology and improve the permeability of CBM wells.

Many scholars have carried out relevant studies on nitrogen injection to promote emission/gas extraction. Clarkson et al. believed that injecting non-gas gas into coal seam can reduce the partial pressure of the gas, promote the desorption of adsorbed gas, and increase the gas recovery rate. Yang conducted a field test of low-pressure nitrogen injection in coal seam to promote gas extraction/drainage in the underground coal mine of Yangquan Mining area, and found that injecting nitrogen into coal seam could significantly promote gas extraction/drainage. Katayama believed that the mechanism of CO₂ replacing CH₄ was due to the stronger adsorption capacity of CO₂, while N₂ replacing CH₄ was due to the reduction of the partial pressure of CH₄ by N₂ injection. Wu et al. carried out an experimental study on the effect of nitrogen injection based on the theory of diffusion seepage and multi-component adsorption equilibrium and discussed the stimulation mechanism of gas displaced by nitrogen injection. Most of the above studies are carried out through laboratory experiments and field tests. However, coal is composed of inorganic and organic matter, and its inner surface has complex structural characteristics, so the gas injection displacement mechanism should be explained from the molecular level. Molecular simulation method can be used to study the microscopic mechanism of interaction between adsorbent and adsorbent at the molecular level.

Scholars at home and abroad have done a lot of research on molecular simulation of the adsorption characteristics of CO₂, N₂, and other mixed gases of coalbed methane. Wu et al. used the grand canonical integrated Monte Carlo method to analyze the ability and competitive difference of coal to adsorb CO₂, O₂, and N₂ according to the fire prevention and storage practice of flue gas injected into the goaf of power plant. Lou et al. established a physical adsorption model for different gas molecules such as O₂, CO₂, and N₂ on the surface of coal macromolecules to explore the gas competition difference of mixed gas molecules on the surface of coal macromolecules. Cui et al. studied the adsorption of CH₄, N₂, and CO₂ gases by coal, and the results showed...
that the adsorption capacity of coal for the three gases was \( \text{CO}_2 > \text{CH}_4 > \text{N}_2 \). Song et al.\(^20\) used GCMC and DFT methods to study the influence of oxygen-containing functional groups and electrostatic interaction on the competitive adsorption of \( \text{CO}_2 \), \( \text{CH}_4 \), and \( \text{N}_2 \) in the low-rank coal molecular model, and found that the strong quadrupole moment and polarization ability of \( \text{CO}_2 \) led to the stronger selective adsorption of oxygen-containing functional groups than \( \text{CH}_4 \) and \( \text{N}_2 \).

In terms of nitrogen injection to promote methane extraction, the adsorption/desorption mechanism of different gases in coal is studied mainly through laboratory experiments, field tests, and numerical simulation. In fact, coal itself contains adsorbed methane, and different temperatures, types of injected gas, and injection pressure of coal seam have a great influence on the desorption of coal seam methane. Therefore, the interaction mechanism between injected gas molecules and methane-containing coal in the process of gas injection is not clear at present. Coal contains methane, and the molecular dynamics mechanism of gas injection under different conditions to promote methane desorption in coal needs to be further studied. Although some scholars have studied the mechanism of methane adsorption by coal from a microscopic point of view, there is still a lack of systematic simulation of the influence of water on methane desorption by coal. Therefore, the mechanism of nitrogen injection promoting gas desorption by water in coal has not been fully grasped. Taking Wiser bituminous coal as an example, the molecular simulation was used to study the desorption behavior of \( \text{CH}_4 \) in methane-containing coal structure after \( \text{N}_2 \) injection at different temperatures, pressures, and moisture content, to clarify the mechanism of promoting \( \text{CH}_4 \) desorption in coal by \( \text{N}_2 \) injection. It provides theoretical support for methane extraction technology in goaf.

**Calculation methods**

**Coal molecular structure model.** Theoretical coal models are generally composed of coal molecules consisting of a large number of atoms, and these idealized coal models are applied to solve practical problems\(^21,22\). In this study, a typical bituminous coal Wiser molecular substrate \((\text{C}_{192}\text{H}_{165}\text{O}_{20}\text{N}_{5}\text{S}_{8})\) was selected, as shown in Fig. 1. The lignite substrate model is composed of an aromatic skeleton amorphous molecular structure composed of 390 atoms, including carbon, hydrogen, oxygen, nitrogen, and sulfur elements. This molecular model has been successfully applied in the study of gas competitive adsorption on bituminous coal surface\(^23\). Table 1 shows the structural parameters of Wiser bituminous coal macromolecular model.

| Molecular formula | Molecular weight | C | H | O | N | S |
|-------------------|------------------|---|---|---|---|---|
| \( \text{C}_{192}\text{H}_{165}\text{O}_{20}\text{N}_{5}\text{S}_{8}\) | 3115  | 73.96 | 10.27 | 5.30 | 2.25 | 8.22 |

**Molecular dynamics simulation.** The molecular dynamics simulation was carried out on Materials Studio software, and the COMPASSII force field was used in the calculation process. In this paper, the surface model of bituminous coal was constructed through the Amorphous Cell module, and the initial surface model of bituminous coal was obtained by filling the 16 optimized bituminous coal molecular models into the 3D periodic boundary Cell. Then Anneal is annealed through Anneal task in Forcite module, the precision is set as
Fine, the temperature range is 300–500 K, and the total simulation time is 1 ns. Finally, the structure was further optimized with Fine precision and the Ewald summation method was used for van der Waals interaction with a truncation radius of 15.0 Å to obtain the final bituminous coal surface model (Fig. 2).

The density of the model was 1.20 g/cm$^3$. The cell was expanded to construct a $1 \times 2 \times 2$ supercell, and 50 Å vacuum layer was added, as shown in Fig. 3.

CH$_4$ and N$_2$ molecules were adsorbed in the coal surface model to form the CH$_4$-N$_2$ system, and the structure of the system was optimized by repeating the above structural optimization method. The Dynamics properties are calculated under the Dynamics task in the Forcite module. The NVT canonical ensemble was used to study the dynamics of the system with 40 ps of simulated data. The setting of the calculation method is consistent with that in the structural optimization of the model mentioned above.

Mean Square Displacement (MSD) is the statistical average of particle trajectories, which refers to the measurement of the average distance of other particles around a given particle$^{24}$. MSD calculation formula is as follows:

$$\text{MSD} = \frac{1}{N} \left( \sum_{i=1}^{N} [r_i(t) - r_i(0)]^2 \right)$$  \hspace{1cm} (1)

where $r_i(t)$ and $r_i(0)$ are the instantaneous and initial position vectors of the $i$th particle, respectively. Moreover, $N$ is the total number of particles in the system.

Figure 2. Surface model of bituminous coal.

Figure 3. Bituminous coal supercell model.
The diffusion coefficient of gas can be obtained from the following expression:

\[ D = \frac{1}{6N} \lim_{t \to \infty} \frac{d}{dt} \left( \sum_{i=1}^{N} [r_i(t) - r_i(0)]^2 \right) \]  

(2)

\[ D = \lim_{t \to \infty} \left( \frac{\text{MSD}}{6t} \right) = \frac{1}{6} K_{\text{MSD}} \]  

(3)

where \( D \) is the diffusion coefficient of the gas, \( N \) is the number of particles in the system, and \( K_{\text{MSD}} \) is the slope of the MSD curve.

Monte Carlo simulation. In the Sorption module, the injection pressure is 10–1000 kpa, and the temperature is 293–333 K; The number of simulated loading steps to the equilibrium state is \( 1 \times 10^8 \) steps, and the total number of steps is \( 2 \times 10^8 \) steps. The Metropolis method was chosen for configuration calculation, and the charge balance (QEq) method was used for charge calculation. The Settings of force field, van der Waals force, hydrogen bond force, and Coulomb force calculation methods were consistent with those in the previous model. The simulation calculation of desorption \( \text{CH}_4 \) adopts the Focite module. The task is set as Dynamics and the temperature is set as 293–333 K. The temperature control method, ensemble and force field are consistent with the Dynamics parameters in “Molecular dynamics simulation” section.

| Pressure (MPa) | Adsorption amount/n |
|---------------|---------------------|
| 1             | 177                 |
| 2             | 210                 |
| 3             | 279                 |
| 4             | 361                 |
| 5             | 445                 |

Table 2. The quantity of \( \text{N}_2 \) injected at different pressures.

Figure 4. Initial model of nitrogen injection.

Figure 4 shows the initial model of nitrogen injection. Regions 0–57 Å and 107–164 Å are the molecular layers of coal, and region 57–107 Å is the vacuum layer. The amount of \( \text{N}_2 \) injected under different pressures is consistent with the adsorption amount of \( \text{N}_2 \) in Table 1. The quantity of \( \text{N}_2 \) injected at different temperatures was 256. The simulation calculation of desorption \( \text{CH}_4 \) adopts the Focite module. The task is set as Dynamics and the temperature is set as 293–333 K. The temperature control method, ensemble and force field are consistent with the Dynamics parameters in “Molecular dynamics simulation” section.
Results and analysis

Distribution characteristics of the gas in the model. Figure 5 shows the adsorption isotherms of CH₄ and N₂ in the molecular structure model of bituminous coal when the temperature is 293 K, 303 K, 313 K, 323 K, and 333 K, and the pressure range is 0.01–10 MPa. The nonlinear form of the Langmuir adsorption isotherm model was used to fit the adsorption equilibrium data of CH₄ and N₂, and the fitting curves are shown in Fig. 5. The results show that when the adsorption temperature is 293 K, 303 K, 313 K, 323 K, 333 K, the square R² of the correlation coefficient of CH₄ adsorption isotherm fitting curve is 0.9963, 0.9974, 0.9966, 0.9971, 0.9972, respectively. The R² of N₂ was 0.9979, 0.9992, 0.9974, 0.9994, 0.9991, respectively. It can be seen that the Langmuir adsorption model can well describe the adsorption of the two gases by the molecular structure model of bituminous coal.

As can be seen from Fig. 5, the adsorption capacity of CH₄ is significantly higher than that of N₂ under the pressure of 1 MPa. When the pressure increased from 0.01 mpa to 1 MPa, the adsorption capacity of the two gases increased rapidly, and CH₄ increased the fastest. In the process of pressure increasing from 1 to 8 MPa, the increased rate of adsorption capacity of the two gases showed an obvious downward trend. When the pressure increased to 8 MPa, the adsorption capacity gradually tended to be flat. When the pressure is constant, the adsorption capacity of the two gases decreases gradually with the increase of temperature. The increase in temperature is not conducive to the adsorption of gas, so the adsorption process of gas is exothermic. Under isothermal and isobaric conditions, the adsorption capacity of the two gases in bituminous coal is CH₄ > N₂. This is because the amount of gas adsorbed decreases with the increase of molecular dynamics diameter, and the molecular dynamics diameter of N₂ is larger than that of CH₄, which makes the adsorption of N₂ by coal weaker than that of CH₄.

Effect of temperature on methane desorption. In this paper, the effect of N₂ at different temperatures on the determination of CH₄ in coal is studied from the microscopic point of view. The average relative con-
The average relative concentration distribution of the two types of gases in coal molecules is shown in Fig. 6. Regions 0–57 Å and 107–164 Å are the molecular layers of coal, and region 57–107 Å is the vacuum layer. As can be seen from Fig. 6, both types of gases diffuse into the vacuum layer. The increase of CH$_4$ molecules in the vacuum layer is the most, and the increase of N$_2$ molecules is the least. In the range of 293–333 K, the mean relative concentration of CH$_4$ increased by 59.94% after N$_2$ injection. At the same temperature, the concentration of CH$_4$ in the vacuum layer is 62.15%(293 K), 60.97%(303 K), 53.62%(313 K), 61.08%(323 K), 50.43% (333 K) higher than that of N$_2$.

As shown in Fig. 7, the root mean square (RMS) displacement of gas in the CH$_4$-N$_2$ system increases with the increase of simulation time. At the same time, the RMS of gas in the system increases with the increase of temperature. After N$_2$ is injected into the coal, the CH$_4$ adsorbed on the coal molecules under the influence of pressure gradient is desorbed out. On the contrary, due to a large number of free N$_2$ molecules in the vacuum layer, the concentration of N$_2$ in the vacuum layer increases beyond that in the coal molecular layer, and part of N$_2$ will diffuse to the coal molecular layer and be adsorbed by the coal molecules. Therefore, what actually happens in coal is that N$_2$ resolves CH$_4$ by diffusion. At the same temperature, the overall relationship between the root mean square displacement of the two gases is CH$_4$ > N$_2$.

As shown in Fig. 8, the diffusion coefficients of CH$_4$ increased with the increase of N$_2$ injection temperature, indicating that the molecular activity in the system increased with the increase of temperature. In the range of 293–333 K, the diffusion coefficient of CH$_4$ increases from 0.06 to 0.11 nm$^2$/ps. The diffusion coefficient of N$_2$ increases from 0.03 to 0.08 nm$^2$/ps. At the same temperature, the diffusion coefficient of CH$_4$ is always greater than that of N$_2$. It can be seen that the CH$_4$ molecule is more active in the N$_2$-CH$_4$ system.

Figure 6. Concentration distribution of CH$_4$ and N$_2$ at different temperatures.

Figure 7. MSD curves of CH$_4$ and N$_2$ at different temperatures.
Effect of pressure on methane desorption. The average relative concentration distribution of the two types of gases in coal molecules after \( \text{N}_2 \) injection at different pressures is shown in Fig. 9. As can be seen from Fig. 9, both types of gases diffuse into the vacuum layer. The increase of \( \text{CH}_4 \) molecules in vacuum layer is the most, and the increase of \( \text{N}_2 \) molecules is the least. The concentration in the vacuum layer increases with the increase of pressure. In the range of 1–5 MPa, the mean relative concentration of \( \text{CH}_4 \) increased by 71.82% after \( \text{N}_2 \) injection. Under the same pressure, the concentration of \( \text{CH}_4 \) in the vacuum layer is 62.15% (1 MPa), 48.88% (2 MPa), 49.65% (3 MPa), 50.18% (4 MPa), and 47.23% (5 MPa) higher than that of \( \text{N}_2 \).

Figure 10 shows the root means square displacements of \( \text{CH}_4 \) and \( \text{N}_2 \) at different pressures. In the \( \text{CH}_4-\text{N}_2 \) system, the root means square displacements of gases increased with the increase of the simulated pressure. Under the same pressure, the overall relationship between the root means square displacement of the two gases is \( \text{CH}_4 > \text{N}_2 \).

Figure 11 shows the relationship between the \( \text{CH}_4 \) diffusion coefficient and \( \text{N}_2 \) injection pressure. It can be seen from the figure that the diffusion coefficient of both gases increases with the increase of pressure, indicating that the molecular activity in the system increases with the increase of pressure. In the range of 1–5 MPa, the diffusion coefficient of \( \text{CH}_4 \) increases from 0.06 to 0.16 nm²/ps. The diffusion coefficient of \( \text{N}_2 \) increases from 0.03 to 0.09 nm²/ps. The diffusion coefficient of \( \text{CH}_4 \) is always greater than that of \( \text{N}_2 \) under the same pressure. It can be seen that the \( \text{CH}_4 \) molecule is more active than \( \text{N}_2 \) in the \( \text{N}_2-\text{CH}_4 \) system. Since the diffusion coefficient of \( \text{CH}_4 \) is higher than that of \( \text{N}_2 \), the concentration of \( \text{CH}_4 \) diffusing into the vacuum layer is also higher than that of \( \text{N}_2 \).

Effect of water content on methane desorption. As shown in Fig. 12, the relative concentration of \( \text{CH}_4 \) in the vacuum layer gradually increases with the increase of water content. This indicates that the water in
Figure 10. MSD curves of CH$_4$ and N$_2$ under different pressures.

Figure 11. Diffusion coefficients of CH$_4$ and N$_2$ under different pressures.

Figure 12. Concentration distribution of CH$_4$ and N$_2$ under different water content.
coal promotes the desorption of CH₄. This is because the force between coal and methane molecules is greater than that between water molecules, but water molecules are polar molecules, and there is hydrogen bonding between coal and water molecules, so the estimated force between coal and water molecules is far greater than that between coal and methane molecules. Therefore, from the perspective of intermolecular forces, H₂O is in a dominant competitive position. Because the interaction between coal and water molecules is far greater than that between coal and methane molecules, when the three molecules coexist, water molecules and methane molecules compete for adsorption on the surface of coal, and water molecules will replace some of them to adsorb methane.

**Discussion on the action mechanism of gas molecules.** By comparing the effects of injection pressure and temperature on methane resolution, it can be seen that the average relative concentration of CH₄ increases by 59.94% at 1 MPa and 293–333 K. The diffusion coefficient increased from 0.06 to 0.11 nm²/ps. The average relative concentration of CH₄ at 1–5 MPa and 293 K increased by 71.82% after N₂ injection. The diffusion line increased by 0.10 nm²/ps. It shows that the influence of injection pressure on methane desorption is greater than that of temperature in the simulated range. Compared with the injection of high-temperature nitrogen to desorption seam methane, the diffusion effect of high-pressure nitrogen flowing in the coal body is more significant. The higher the injection pressure of nitrogen, the better the effect of N₂ promoting CH₄ desorption.

According to the above simulation results, the concentration of desorbed CH₄ changes with the pressure and temperature of N₂ injection. With the injection of N₂, the pore pressure in the coal increases, and the diffusion velocity of CH₄ in the coal accelerates accordingly. The adsorbed CH₄ in the coal also begins to desorption and flow out with N₂ airflow. The increase of gas injection pressure accelerates the seepage rate, improves the pore pressure in the coal body, and promotes the increase of adsorbed CH₄ desorption amount. Therefore, the desorbed CH₄ rises with the increase of gas injection pressure. Within the same temperature, the higher the pressure is, the greater the CH₄ analytical amount is, and the more obvious the promoting effect is. After the injected N₂ enters the coal, the pressure in the coal increases, and the partial pressure of N₂ also shows an upward trend. When CH₄ does not desorption, the partial pressure of CH₄ remains unchanged. However, after N₂ injection, there is an additional gas and partial pressure in the system, so the adsorbed CH₄ will desorption and become a free state. In this simulation, CH₄ in the coal body is resolved with the continuous injection of N₂, and the partial pressure of CH₄ decreases, which intensifies the desorption of adsorbed CH₄ in the coal body. When the partial pressure of N₂ promotes the desorption of CH₄, a part of N₂ will also be adsorbed into the coal, which shows that N₂ is adsorbed by the coal while CH₄ is replaced. It can be seen that the higher the N₂ injection pressure and temperature, the more methane desorption, and N₂ can replace some adsorbed CH₄ through competitive adsorption with CH₄. The simulation results are consistent with Zhou's experimental results.

Due to the decrease of partial pressure, CH₄ in coal will desorption from the pores of the matrix. After desorption of CH₄ molecules adsorbed in coal, its main form of movement is diffusion movement under the action of the concentration gradient. In this simulation, after N₂ injection, CH₄ in the vacuum layer was diluted, which resulted in a concentration difference between the coal molecular layer and the vacuum layer, and directional gas diffusion continued. Not only does CH₄ diffuse from the coal molecular layer to the vacuum layer, but also N₂ diffuses into the vacuum layer under the effect of concentration difference. N₂ promotes the desorption of CH₄ by diffusion. This is also one of the mechanisms by which N₂ injection promotes CH₄ desorption.

**Conclusions**

In this paper, the desorption of CH₄ by N₂ injection was studied by using GCMC and MD methods. The results show that:

1. The adsorption isotherms of CH₄ and N₂ in the molecular structure model of bituminous coal are in good agreement with the Langmuir adsorption isotherm model. The adsorption capacity of the two gases in the bituminous coal structure model is CH₄ > N₂. Temperature is negatively correlated with the adsorption amount.
2. In the range of 293–333 K, the average relative concentration of CH₄ in the vacuum layer increased by 59.94% after N₂ injection. In the range of 1–5 MPa, the average relative concentration of CH₄ increased by 71.82% after N₂ injection. The higher the N₂ injection pressure and temperature, the more methane desorption, and N₂ can replace some adsorbed CH₄ through competitive adsorption with CH₄. The activity of the CH₄ molecule is higher in N₂–CH₄ system.
3. The relative concentration of CH₄ in the vacuum layer gradually increases with the increase of water content. This indicates that the water in coal promotes the desorption of CH₄. The results of this article provide theoretical support for methane extraction technology in goaf. Since this study only carried out a molecular simulation on the bituminous coal model, the research scope will be expanded in the future to further improve the research results.

**Data availability**

The datasets used and/or analysed during the current study available from the corresponding author on reasonable request.

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