Photocatalytic CO\textsubscript{2} Reduction and Electrocatalytic H\textsubscript{2} Evolution over Pt(0,II,IV)-Loaded Oxidized Ti Sheets

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Abstract: Energy recycling and production using abundant atmospheric CO\textsubscript{2} and H\textsubscript{2}O have increasingly attracted attention for solving energy and environmental problems. Herein, Pt-loaded Ti sheets were prepared by sputter-deposition and Pt\textsuperscript{4+}-reduction methods, and their catalytic activities on both photocatalytic CO\textsubscript{2} reduction and electrochemical hydrogen evolution were fully demonstrated. The surface chemical states were completely examined by X-ray photoelectron spectroscopy before and after CO\textsubscript{2} reduction. Gas chromatography confirmed that CO, CH\textsubscript{4}, and CH\textsubscript{3}OH were commonly produced as CO\textsubscript{2} reduction products with total yields up to 87.3, 26.9, and 88.0 \(\mu\text{mol/mol}\), respectively for 700 °C-annealed Ti under UVC irradiation for 13 h. Pt-loading commonly negated the CO\textsubscript{2} reduction yields, but CH\textsubscript{4} selectivity was increased. Electrochemical hydrogen evolution reaction (HER) activity showed the highest activity for sputter-deposited Pt on 400 °C-annealed Ti with a HER current density of 10.5 mA/cm\textsuperscript{2} at −0.5 V (vs. Ag/AgCl). The activities of CO\textsubscript{2} reduction and HER were found to be significantly dependent on both the nature of Ti support and the oxidation states (0,II,IV) of overlayer Pt. The present result could provide valuable information for designing efficient Pt/Ti-based CO\textsubscript{2} recycle photocatalysts and electrochemical hydrogen production catalysts.

Keywords: energy recycling; photocatalytic CO\textsubscript{2} reduction; electrochemical hydrogen evolution; Ti oxide; Pt oxidation state

1. Introduction

Recycle energy production using abundant CO\textsubscript{2} and H\textsubscript{2}O has been a challenging project for energy and environment solutions. Hydrogen production via water splitting is another useful project for these types of solutions. For CO\textsubscript{2} reduction into fuels, increasing selectivity and production efficiency have been very important issues [1–5]. Many strategies have been employed such as defect controlling [6], crystal facet tailoring [7,8], metal alloys/cocatalysts [9,10], support [11], and hybridization [12]. For hydrogen production, diverse strategies have also been employed [13–16]. Among various metal nanoparticles (NPs) on metal oxide supports such as TiO\textsubscript{2}, Pt NP has been the most studied and known to have very high beneficial catalytic activity to CO\textsubscript{2} reduction as well as hydrogen production [17–25]. Fang et al. prepared Pt-loaded TiO\textsubscript{2} spheres (>500 \(\mu\text{m}\)) by a modified TiO\textsubscript{2} sol-gel method and microwave-assisted Pt reduction method using ethylene glycol as the reducing agent [19]. They reported CO\textsubscript{2} reduction yields of CO and CH\textsubscript{4} with 18 and 3.5 \(\mu\text{mol g}^{-1} \text{ h}^{-1}\), respectively. Liu et al. prepared well-dispersed Pt on ultrathin TiO\textsubscript{2} and showed 47 \(\mu\text{mol}\) of CH\textsubscript{4} formation and 35 \(\mu\text{mol}\) of CO formation after UV light irradiation for 10 h [20]. Zhang et al. reported accumulated CH\textsubscript{4} production yield to be about 2.0 \(\mu\text{mol g}^{-1}\) for Pt (0.12 w/w%-)-loaded TiO\textsubscript{2} catalyst at a reaction...
temperature of 342 K for 13 h [21]. Wang et al. prepared ultrafine Pt (0.5–1 nm)/TiO₂ nanostructures on ITO via aerosol chemical vapor deposition for TiO₂ and gas-phase sputtering deposition for Pt NPs [22]. They reported CO₂ photoreduction efficiency of 1361 μmol g⁻¹ h⁻¹ for CH₄ formation and 200 μmol g⁻¹ h⁻¹ for CO formation. Kometani et al. tested CO₂ reduction over Pt-loaded TiO₂ under supercritical condition of water and CO₂ at 400 °C and 30 MPa [23]. They reported that CO (35.3 ppm), CH₄ (42.7 ppm), and H₂ (65.3 ppm) were major products, and HCOOH (1.7 μM) and HCHO (0.6 μM) were minor. Xiong et al. showed that CO₂ reduction efficiency was highly dependent on the Pt-loading method, which determined the particle size, distribution, and Pt(0)/Pt(II) ratio [26]. They loaded Pt NPs on TiO₂ with co-exposed [101] and [001] facets by photo-reduction and NaBH₄-reduction methods using Pt(NH₃)₄Cl₂ or H₂PtCl₆ as precursors. The highest (4.6 μmol g⁻¹ h⁻¹) and poorest (0.2 μmol g⁻¹ h⁻¹) CH₄ yields were reported for Pt NPs by chemical reduction methods using Pt(NH₃)₄Cl₂ and H₂PtCl₆, respectively. For crystal facet effects, Mao et al. reported that TiO₂ with [010] facets showed a higher CO₂ photoreduction performance (1.6 μmol g⁻¹ h⁻¹ of CH₄) than that (0.8 μmol g⁻¹ h⁻¹) of TiO₂ with [001] facets [27]. However, 1% Pt-loading on TiO₂ with [001] facets showed a higher activity (2.6 μmol g⁻¹ h⁻¹) than that (1.2 μmol g⁻¹ h⁻¹) of Pt-loading on TiO₂ with [010] facets. For catalyst and cocatalyst enhancements, Zhang et al. co-decorated Au and Pt NPs (5–12 nm) on TiO₂ nanofibers (NFs) through an electrospinning method [10]. They reported (0.03 μmol h⁻¹)/(0.06 μmol h⁻¹), (0.31 μmol h⁻¹)/(0.20 μmol h⁻¹), (0.42 μmol h⁻¹)/(0.08 μmol h⁻¹), and (0.57 μmol h⁻¹)/(0.09 μmol h⁻¹) of CH₄ production/CO formation after UV-irradiation for 3 h for pure TiO₂ NFs, Au/TiO₂ NFs, Pt/TiO₂ NFs, and Au₀.25/Pt₀.75/TiO₂ NFs, respectively. The CH₄ production was increased by 14 and 19 times after Pt and Au₀.25/Pt₀.75 loadings, respectively. The Pt-TiO₂ based photocatalysts for CO₂ reduction in the previously reported literatures were further discussed in comparison with the present result below.

Pt NPs on TiO₂ has also been a good model system for photocatalytic and electrochemical hydrogen production [28–33]. Briefly, Lian developed Ptⁿ⁺ (n = 0, 2, or 3)/TiO₂ system and showed that the photocatalytic H₂ evolution efficiency was higher than that of metallic Pt-loaded TiO₂ and commercial P25 [33]. They attributed the higher efficiency to well dispersed Ptⁿ⁺–O species, facilitating a photogenerated charge transfer. Yu et al. prepared Pt-loaded TiO₂ and showed that both H₂ and C₂H₆ products were produced by a photocatalytic reaction in a catalyst-dispersed water system filled with CH₄ gas [29].

Herein, to further investigate the roles of overlayer Pt and Ti supports, we prepared sputter-deposited Pt (Pt-sp) and Pt NPs (using a reducing agent) over oxidized Ti sheets and tested for both photocatalytic CO₂ reduction and electrochemical hydrogen production. Different oxidation states (0,II,IV) of Pt were obtained using two different Pt-loading methods. Different natures of Ti supports were obtained by using different thermal annealing treatments. Two different application tests were employed to examine both positive and negative roles in two different application areas. Thereby, the present results provide very useful information on design of catalysts for energy production via CO₂ reduction and electrochemical hydrogen evolution.

2. Materials and Methods

2.1. Preparation of Sputter-Deposited Pt on Ti Sheets and Pt NP on Ti Sheets

Ti sheets (GR2, 32 mm × 32 mm, 0.1 mm thick) were cleaned by ultrasonication in acetone and isopropyl alcohol repeatedly, and dried under an IR lamp. Afterwards, ozone cleaning (UVC-150 ozone cleaner, Omniscience Co., Yongin, Kyongki, Korea) was performed for 15 min. Ti sheets were then annealed at 400 or 700 °C for 2 h. After the thermal treatment, the sheets were also repeatedly cleaned by the same procedure above. Pt NPs were prepared by a reduction method using NaBH₄ and sodium citrate solution for 24 h at room temperature. After that, the NPs were fully washed and drop-coated on the Ti substrate. The sample was abbreviated as Pt-NP/Ti. Pt deposition on the oxidized Ti sheet was performed by a sputter-coating method with an ionization current of 3 mA for 10 s using a SPT-20 ion sputter coater (COXEM Co., Daejeon, Korea). The calibrated Pt thicknesses
was 0.5 nm, abbreviated as Pt-sp. The samples examined here were bare Ti, Ti (400 °C), Ti (700 °C), Pt-NP/Ti, Pt-NP/Ti (400 °C), Pt-NP/Ti (700 °C), Pt-sp/Ti, Pt-sp/Ti (400 °C), and Pt-sp/Ti (700 °C).

2.2. Characterisation of the Samples

The surface morphology of the sheets before and after CO₂ reduction was examined using a Hitachi S-4800 scanning electron microscope (SEM) (Hitachi Ltd., Tokyo, Japan) at an accelerating voltage of 10 kV and a current of 10 mA. The surface chemical states for oxidized Ti sheet and Pt-loaded Ti sheets before and after CO₂ reduction were examined by taking X-ray photoelectron spectra (survey, Pt 4f, Ti 2p, C 1s, and O 1s) using a using a Thermo-VG Scientific K-alpha⁺ spectrometer (Thermo VG Scientific, Waltham, MA, USA) with a monochromatic Al Kα X-ray source and a hemispherical energy analyzer.

2.3. Photocatalytic CO₂ Reduction and Electrochemical Hydrogen Evolution

The photocatalytic CO₂ reduction was performed in a stainless-steel reactor (volume ~40 mL) with a quartz window (3 mm thick and 45 mm diameter) on top. An oxidized Ti sheet or a Pt-loaded sheet was placed in the reactor with 40 µL (or 5 µL) deionized water beside the sheet. Afterwards, the reactor was fully flushed under a stream of pure (99.999%) CO₂ gas for at least 5 min. After the reactor was filled with CO₂ gas and the inlet and outlet valves were closed. For CO₂ reduction experiment, the reactor was placed under four 15 W UVC (200–280 nm) lamps (a power density of 5.94 mW/cm²) for 13 h. Blank tests under dark condition were also performed to examine the precise role of light. The CO₂ reduction gas products such as CO, CH₄, and CH₃OH were analyzed by a YL 6500 gas chromatograph (Young In Chromass Co., Ltd., Seoul, Korea) equipped with a Ni catalyst methanizer assembly, a flame ionization detector (FID), and a thermal conductivity detector (TCD). For GC analysis, 0.5 mL volume of gas from the reactor was taken using a gastight syringe to be injected into two different columns of 40/60 Carboxen-1000 (Sigma-Aldrich, St. Louis, MO, USA) and HP-PlotQ-PT (Agilent Technologies, Inc., Santa Clara, CA, USA). Electrochemical hydrogen evolution reaction (HER) tests were performed using a three-electrode system (a Pt counter electrode, a Ag/AgCl reference electrode, and a Ti electrode working electrode) using a WPG100 Potentiostat/Galvanostat (WonATech Co., Ltd., Seoul, Korea) electrochemical workstation. Cyclic voltammetry (CV) and linear sweep voltammetry (LSV) were carried in 0.1 M H₂SO₄ electrolyte solution at a potential range from +0.1 to −0.8 V.

3. Results and Discussion

Figure 1 shows the SEM images for bare Ti, oxidized (400 and 700 °C-annealed) Ti, Pt NP/Ti, Pt NP/Ti (400 °C), Pt NP/Ti (700 °C), Pt-sp/Ti, Pt-sp/Ti (400 °C), and Pt-sp/Ti (700 °C) samples. The surface morphology was found to be mainly determined by thermal treatment temperature and the Pt-prepared conditions. The samples (Figure 1(A2,B2,C2)) treated at 700 °C showed a more crystalline structure on the surface. However, the as-received Ti (Figure 1A) showed a blurred image surface. The 400 °C annealed sample (Figure 1(A1)) showed the morphology between the two. Upon Pt NP loading (prepared using a reducing agent) on the three different surfaces (bare Ti, 400 and 700 °C-annealed Ti), the surface morphology shown was quite distinct. The Pt NPs were aggregated on bare Ti (Figure 1B), while the NPs on 400 and 700 °C-annealed Ti (Figure 1(B1,B2)) sheets were relatively well dispersed. For the sputter-deposited Pt, no discernible particles were found. This could be due to that Pt (0.5 nm thick) was evenly embedded to form Pt-O species, which was confirmed by XPS below.
Two general photoreactor systems have been employed, which are (1) catalyst dispersed in a CO$_2$-saturated aqueous liquid: solid-liquid mode, and (2) catalyst dispersed on a support with gaseous CO$_2$ and H$_2$O: solid-gas mode. In the present study, the solid (catalyst)-gas (CO$_2$ + H$_2$O) system was employed. CO$_2$ reduction products were examined and displayed in Figure 2. Carbon monoxide (CO), methane (CH$_4$), and methanol (CH$_3$OH) were commonly been produced with different yields for bare Ti, Ti (400 °C), bare Ti (700 °C), Pt NP/Ti, Pt NP/Ti (400 °C), Pt NP/Ti (700 °C), Pt-sp/Ti, Pt-sp/Ti (400 °C), and Pt-sp/Ti (700 °C) sheets. For bare Ti, it was found that total CO, CH$_3$OH, and CH$_4$ production yields (μmol/mol = ppm) after UVC irradiation for 13 h were observed to be 81.3, 67.1, and 19.5 ppm, respectively. These yields became substantially decreased to 32.3, 0, and 8.7 ppm, respectively for Ti (400 °C) sheet. However, for 700 °C-annealed Ti, CO, CH$_3$OH, and CH$_4$ production yields became again increased to 87.3, 88.0, and 26.9 ppm, respectively. The CO/CH$_4$ production ratios were estimated to be 4.2, 3.7, and 3.2 for bare Ti, Ti (400 °C), and Ti (700 °C), respectively. For bare Pt-free Ti substrates, the activity showed the order of Ti (400 °C) < Ti < bare Ti (700 °C). The Ti (700 °C) sheet showed the highest CO$_2$ reduction activity. This indicates that the nature of Ti surface mainly determines the activity. Upon Pt-loading, the CO$_2$ reduction yields were commonly diminished, but the CH$_4$ production was less impacted. For Pt NP on Ti, the CO and CH$_3$OH productions were decreased by 47% and 68%, respectively. However, CH$_4$ production was increased by 14%. For sputter-deposited Pt on Ti, the CO, CH$_3$OH, and CH$_4$ productions were decreased by 48%, 26%, and 19%, respectively. For Pt NP on Ti (400 °C), CO and CH$_4$ yields were observed to be 2.1 and 12.7 ppm, respectively compared with those of bare Ti (400 °C) sheet. CO yield was substantially decreased by 93%, but the CH$_4$ yield was increased by 45%. For sputter-deposited Pt on Ti (400 °C), no CO was detected, and CH$_3$OH and CH$_4$ production yields were merely observed to be 1.6 and 7.9 ppm. For the Pt-loading on Ti (700 °C) sheet, the CO$_2$ reduction activity was more severely impacted. CO, CH$_3$OH, and CH$_4$...
production yields were decreased by 82%, 50%, and 41%, respectively. For the sputter-deposited Pt on Ti (700 °C), CO, CH$_3$OH and CH$_4$ production yields were more significantly decreased by 98%, 92%, and 38%, respectively. The CO/CH$_4$ production ratios were estimated to be 0.16, 1.0, and 1.9 for Pt NP/Ti, Pt NP/Ti (400 °C), and Pt NP/Ti (700 °C), respectively. For Pt-sp/Ti, Pt-sp/Ti (400 °C), and Pt-sp/Ti (700 °C), the CO/CH$_4$ production ratios were estimated to be 0.0, 0.1, and 2.7, respectively. CH$_4$ selectivity was commonly increased upon Pt-loading.

Figure 2. CO$_2$ reduction (CO, CH$_4$, and CH$_3$OH) yields (μmol/mol) over: (B) bare Ti, Ti (400 °C), and Ti (700 °C); (C) Pt NP/Ti, Pt NP/Ti (400 °C), and Pt NP/Ti (700 °C); (D) Pt-sp/Ti, Pt-sp/Ti (400 °C), and Pt-sp/Ti (700 °C) samples. (A) is the total plot for (B–D).

CO$_2$ reduction mechanism is highly dependent on the production of protons and electrons [1,10]. The general equation is written as $x$CO$_2$ + $y$H$^+$ + $z$e$^-$ → C$_n$ products + $m$H$_2$O, where C$_n$ is an organic compound. Under UV irradiation, electrons (e$^-$) and holes (h$^+$) are created in the conduction and valence bands (CB and VB), respectively. Because CO$_2$ reduction occurs through multielectron processes, the creation of photogenerated electrons is an important factor for the catalytic activity. The photogenerated electrons and holes are separated to participate in several reactions described below:

$$\text{TiO}_2 + h\nu \rightarrow \text{TiO}_2 (\text{VB}, h^+) + \text{TiO}_2 (\text{CB}, e^-)$$

$$\text{H}_2\text{O} + h^+ \rightarrow \cdot \text{OH} + \text{H}^+$$
\[
\cdot\text{OH} + \text{H}_2\text{O} + 3\text{H}^+ \rightarrow \text{O}_2 + 3\text{H}^+
\]
\[
\text{H}^+ + \text{e}^- \rightarrow 1/2\text{H}_2
\]
\[
\text{CO}_2 + 2\text{H}^+ + 2\text{e}^- \rightarrow \text{CO} + \text{H}_2\text{O}
\]
\[
\text{CO} + 6\text{H}^+ + 6\text{e}^- \rightarrow \text{CH}_4 + \text{H}_2\text{O}
\]
\[
\text{CO}_2 + 6\text{H}^+ + 6\text{e}^- \rightarrow \text{CH}_3\text{OH} + \text{H}_2\text{O}
\]
\[
\text{CO}_2 + 8\text{H}^+ + 8\text{e}^- \rightarrow \text{CH}_4 + 2\text{H}_2\text{O}
\]

In the \text{CO}_2 reduction mechanism, several reaction channels are closely spaced and diverse products of \text{CO}, \text{CH}_4, and \text{CH}_3\text{OH} are obtained via multielectron processes described above. Notably, kinetically favored hydrogen production channel is also among the \text{CO}_2 reduction channels. Therefore, \text{H}^+ and \text{e}^- can be consumed for \text{H}_2 production. As discussed above, when Pt species were present, \text{CO}_2 reduction was observed to be negated and photocatalytic hydrogen production was increased.

In Table 1, we have summarized Pt-TiO$_2$ based photocatalysts for \text{CO}_2 reduction in the previously reported literatures [10,17,19–22,24,27,34–37]. \text{CO} and \text{CH}_4 have commonly been observed as \text{CO}_2 reduction products, consistent with the present results. Generally, the yield of \text{CH}_4 was reported to be higher than that of \text{CO}, although the reaction conditions (e.g., light intensity, wavelength, water amount, and reactor type) were all different. In the present result, \text{CH}_4 production over Pt-loaded Ti oxides was also observed to be higher than \text{CO} production, which was consistent with the literature. This indicates that the \text{CH}_4 production channel became superior to the \text{CO} production channel upon Pt-loading, which is discussed further below.

**Table 1.** Photoreactor conditions and reduction yields for reported Pt/Ti-oxide-based catalysts.

| Pt/Ti-Oxide Catalysts [Reference] | Photoreactor Conditions | Major Products and Yields |
|-----------------------------------|-------------------------|---------------------------|
| 1% Pt-loading on TiO$_2$ with [001] facets [27] | 300 W Hg-lamp, 0.1 g on 28 cm$^2$ watch glass in 350 mL reactor | \text{CH}_4: 2.6 \mu\text{mol g}^{-1} \text{h}^{-1}, No CO |
| Pt (0.2 wt.\%)/TiO$_2$: impregnation and thermal treatment [34] | 0.1 g catalyst, 423 K, 400 W Hg lamp, \text{CO}_2 flow (4.5 mL/min) saturated with \text{H}_2\text{O} vapor | \text{CH}_4: 1.46 \mu\text{mol g}^{-1} \text{h}^{-1}, \text{H}_2: 5.28 \mu\text{mol g}^{-1} \text{h}^{-1} |
| Pt (1.82 nm)/TiO$_2$ NPs [24] | 132 mL stainless steel reactor, 500 W Xe lamp, 20 mg catalyst, 5 mL \text{H}_2\text{O} | \text{CH}_4: 60.1 \mu\text{mol g}^{-1} \text{h}^{-1}, \text{C}_2\text{H}_4: 2.8 \mu\text{mol g}^{-1} \text{h}^{-1}, \text{H}_2: 87.5 \mu\text{mol g}^{-1} \text{h}^{-1} |
| 1.5 wt.% Pt/TiO$_2$ photocatalyst [35] | UV 8 W Hg lamp (peak intensity at 254 nm) 0.1 g catalyst, 10 mL \text{H}_2\text{O}, Pressured \text{CO}_2 in the 348 mL reactor | \text{CO}: 7 \mu\text{mol g}^{-1} \text{h}^{-1} \text{for 12 h}, \text{CH}_4: 15 \mu\text{mol g}^{-1} \text{h}^{-1} \text{for 12 h}, \text{H}_2: 270 \mu\text{mol g}^{-1} \text{h}^{-1} \text{for 12 h} |
| Pt (3–4 nm)/TiO$_2$ nanosheet porous film [36] | 300 W Hg lamp (10.4 mW/cm$^2$) 20 mL 0.1 mol/L KHCO$_3$ solution | \text{CH}_4: 20.5 ppm cm$^{-1}$ h$^{-1}$ |
| Pt on ultrathin TiO$_2$ [20] | 10 mg catalyst, 50 cm$^3$ of chamber volume. 300 W Xe lamp | \text{CH}_4: 47 \mu\text{mol for 10 h}, \text{CO}: 35 \mu\text{mol for 10 h} |
| Pt-loaded TiO$_2$ spheres (>500 \mu m) [19] | 200 mg catalyst, 100 \mu L of DI water, pressurized \text{CO}_2 (50 PSI), UV (20 mW/cm$^2$, 254 nm) | \text{CO}: 18 \mu\text{mol g}^{-1} \text{h}^{-1}, \text{CH}_4: 3.5 \mu\text{mol g}^{-1} \text{h}^{-1}, \text{H}_2: 230 \mu\text{mol g}^{-1} \text{h}^{-1} |
| Pt NPs (5–12 nm) on TiO$_2$ nanofibers through electrospinning [10] | 5 mg catalyst on 2 cm \times 2 cm glass, 500 W Xe lamp, 0.1 mL of deionized water, 90 mL gastight reactor | \text{CO}: 0.08 \mu\text{mol h}^{-1}, \text{CH}_4: 0.42 \mu\text{mol g}^{-1} \text{h}^{-1} |
| Pt$^{2+}$–Pt$^{0}$/TiO$_2$ NPs by sol-gel method [37] | 300 W Xe arc lamp, 0.1 g on glass-fiber cloth in 85 mL reactor, a mixture of \text{CO}_2 and water vapor flow | \text{CO}: 20 \mu\text{mol g}^{-1} \text{for 14 h}, \text{CH}_4: 264 \mu\text{mol g}^{-1} \text{for 7 h}, \text{H}_2: 2763 \mu\text{mol g}^{-1} \text{for 7 h} |
Table 1. Cont.

| Pt/Ti-Oxide Catalysts [Reference] | Photoreactor Conditions | Major Products and Yields |
|-----------------------------------|-------------------------|--------------------------|
| Sputter deposited Pt (1 nm) on TiO₂ by aerosol chemical vapor deposition [22] | 400 W Xe lamp (250–388 nm, 19.6 mW/cm²), a mixture of CO₂ and water vapor, flow reactor system | CH₄: 1361 μmol g⁻¹ h⁻¹, CO: 200 μmol g⁻¹ h⁻¹ |
| Platinum-impregnated P25, Pt/TiO₂ [17] | UV-curing 100 W high-pressure Hg lamp (170 mW cm⁻²), 353 and 423 K, gas-phase continuous flow reactor. | CH₄: 1.08 μmol g⁻¹ h⁻¹, H₂: 11.4 μmol g⁻¹ h⁻¹ |
| Pt/TiO₂ nanotube [21] | a 300 W high-pressure Hg lamp (wavelength 365 nm), a fixed-bed photocatalysis reactor, 50 mg on the flat quartz plate | CH₄ yield with 0.0565 μmol h⁻¹ g⁻¹ after 7 h UV irradiation. |

The surface oxidation states were examined by obtaining X-ray photoelectron spectroscopy (XPS) data before and after photocatalytic CO₂ reduction. All the XPS peaks were deconvoluted for the clear identification of several oxidation states. The relative peak ratios are provided in the inset table in each Figures 3–6. Figure 3 shows Ti 2p and O 1s XPS profiles for Pt-free Ti, Ti (400 °C), and Ti (700 °C) samples. The Ti 2p profiles were quite similar before and after CO₂ reduction. For the Ti 2p XPS for bare Ti in Figure 3A, several peaks were observed at binding energies (BEs) of 454.8, 458.8, and 464.6 eV, and between these peaks. The Ti 2p₁/₂ and Ti 2p₃/₂ peaks were observed at BEs of 464.6 and 458.8 eV, respectively. In addition, the broadly distributed Ti 2p peaks were observed around 460.8 and 454.7 eV, respectively. This is attributed to Ti(II,III) oxidation states. For the 400 °C-annealed Ti in Figure 3(A1), substantial change in Ti 2p peak was observed at binding energies (BEs) of 454.8, 458.8, and 464.6 eV, and between these peaks. The Ti 2p₁/₂ and Ti 2p₃/₂ peaks were observed at BEs of 464.6 and 458.8 eV, respectively. In addition, the broadly distributed Ti 2p peaks were observed around 460.8 and 454.8 eV, respectively. This is attributed to Ti(II) oxidation states. For the 700 °C-annealed Ti in Figure 3(A2), the Ti 2p₁/₂ and Ti 2p₃/₂ peaks were observed only at BEs of 464.9 and 459.3 eV, respectively. No Ti 2p signals of Ti(II) and Ti(III) species were observed. This indicates that all Ti(II) and Ti(III) species were oxidized to Ti(IV). For the 700 °C-annealed Ti in Figure 3(A2), the Ti 2p₁/₂ and Ti 2p₃/₂ peaks were observed only at BEs of 464.6 and 459.0 eV, respectively. The BEs were shifted by 0.3 eV to a lower BE position, compared with those for the 400 °C-annealed Ti. This implies that the acidity of Ti⁴⁺ site became lower upon 700 °C annealing.

Figure 3. Ti 2p (left column) and O 1s (right column) XPS of: (A,B) bare Ti; (A1,B1) Ti (400 °C); (A2,B2) Ti (700 °C) before (blue) and after (red) CO₂ reduction. The dot lines are normalized peaks for comparison before and after CO₂ reduction. Inset tables show relative ratios of the deconvoluted peaks.
The Pt NP/Ti sample was found to have a BE position of 78.1 eV, attributed to Pt 4f 5/2 and Pt 4f 7/2 XPS peaks of Pt(IV), respectively. Metallic Pt was weakly seen in the spectrum for the Pt-sp/Ti samples before CO 2 reduction, two major peaks were found at 76.4 and 73.1 eV. The Ti support annealed at a higher temperature showed higher BE position for the Pt 4f 5/2 XPS peaks. The Pt 4f 5/2 and Pt 4f 7/2 XPS peaks were observed to be 74.7 and 71.4 eV for Pt(II) and Pt(IV) species, respectively.

As discussed above, the Ti  (400 °C) samples showed the lowest CO 2 reduction activity, consistent with the data shown in Figure 2C,D. This indicates that sputtered Pt were of Pt(II) and Pt(IV) species co-existing as the intensity of adsorbed surface oxygen species after CO2 reduction, compared with other samples. This shows that the oxygen species were adsorbed on the surface after CO2 reduction.

The Pt NP/Ti and Pt-sp/Ti samples were much higher than those of corresponding Ti (400 °C) and Ti (700 °C) samples, due to a thermal treatment effect. The O 1s XP BE positions for lattice oxygen were found to be similar for the three different samples. A major difference in the O 1s profile after CO 2 reduction was found in the intensity of adsorbed surface oxygen species. The Pt NP/Ti (400 °C) and Pt-sp/Ti (400 °C) samples showed minimal change in the oxygen (Olat) and adsorbed surface oxygen species (Oad), respectively. The Oad/Olat ratios of the deconvoluted peaks for the Pt NP/Ti samples were much higher than those of corresponding Ti (400 °C) and Ti (700 °C) samples.

Figure 4. Ti 2p XPS of: (A) Pt NP/Ti; (A1) Pt NP/Ti (400 °C); (A2) Pt NP/Ti (700 °C); (B) Pt-sp/Ti; (B1) Pt-sp/Ti (400 °C); (B2) Pt-sp/Ti (700 °C) samples before (blue) and after (red) CO 2 reduction. Inset tables show relative ratios of the deconvoluted peaks.

Figure 5. O 1s XPS of: (A) Pt NP/Ti; (A1) Pt NP/Ti (400 °C); (A2) Pt NP/Ti (700 °C); (B) Pt-sp/Ti; (B1) Pt-sp/Ti (400 °C); (B2) Pt-sp/Ti (700 °C) samples before (blue) and after (red) CO 2 reduction. Inset tables show relative ratios of the deconvoluted peaks.
was somewhat decreased after CO

For the Ti 2p XPS for Pt NP

respectively. The BE was shifted by

showed no critical change after CO

and Ti(III) completely disappeared. This indicates that all the species were changed to Ti(IV) upon

Figure 4 shows Ti 2p XPS for Pt NP/Ti, Pt NP/Ti (400 °C), Pt NP/Ti (700 °C), Pt-sp/Ti, Pt-sp/Ti (400 °C), and Pt-sp/Ti (700 °C) samples before and after CO2 reduction. For the Ti 2p XPS for Pt NP/Ti in Figure 4A, several peaks were observed at binding energies (BEs) of 454.7, 458.9, 464.6 eV, and between these peaks, as observed above. The Ti 2p1/2 and Ti 2p3/2 peaks were observed at BEs of 464.6 and 458.9 eV, respectively with a spin-orbit splitting of 5.7 eV. This is attributed to Ti(IV) state of TiO2 [38–40]. Other Ti 2p1/2 and Ti 2p3/2 peaks were observed around 460.8 and 454.7 eV, respectively. This is attributed to Ti(II) of TiC, as mentioned above [38–40]. In addition, the broadly distributed Ti 2p3/2 signals between 454.7 and 459.0 eV could be due to Ti(II,III) oxidation states. The Ti 2p XPS showed no critical change after CO2 reduction. For the Ti 2p XPS for Pt-sp/Ti in Figure 4B, the Ti 2p XPS profiles were quite similar to those for Pt NP/Ti in Figure 4A. For the Ti 2p XPS for Pt NP/Ti (400 °C) before and after CO2 reduction in Figure 4(A1), it was clear that the Ti 2p signals of Ti(0), Ti(II), and Ti(III) completely disappeared. This indicates that all the species were changed to Ti(IV) upon thermal annealing at 400 °C. The Ti 2p1/2 and Ti 2p3/2 peaks were observed at BEs of 465.0 and 459.3 eV, respectively. The BE was shifted by +0.4 eV to a higher BE position. For the Ti 2p XPS for Pt-sp/(400 °C) in Figure 4(B1), the Ti 2p XPS profiles were also quite similar to those for Pt NP/(400 °C) in Figure 4(A1). For the Ti 2p XPS for Pt NP/Ti (700 °C) before and after CO2 reduction in Figure 4(A2), the Ti 2p1/2 and
Two major peaks at 76.6 and 73.3 eV were found for Pt-sp/Ti (400 °C), and Pt-sp/Ti (700 °C) samples before and after CO₂ reduction. Two broad regions were commonly observed as discussed above, and the lower and higher BE peaks were attributed to lattice oxygen (O_{lat}) and adsorbed surface oxygen species (O_{ad}), respectively [29,39–41]. The O_{ad}/O_{lat} ratios of Pt NP/Ti and Pt-sp/Ti samples were much higher than those of corresponding Ti (400 °C) and Ti (700 °C) samples, due to a thermal treatment effect. The O 1s XP BE positions for lattice oxygen were observed to be 530.4, 530.6, and 530.2 eV for Pt NP/Ti, Pt NP/Ti (400 °C) and Pt NP/Ti (700 °C) samples, respectively. For Pt-sp/Ti, Pt-sp/Ti (400 °C), and Pt-sp/Ti (700 °C) samples, the O 1s XP BE positions were observed to be 530.2, 530.3, and 530.0 eV, respectively. However, the O 1s XP BE positions for surface oxygen species were found to be similar for the three different samples. A major difference in the O 1s profile after CO₂ reduction was found in the intensity of adsorbed surface oxygen species. The Pt NP/Ti (400 °C) and Pt-sp/Ti (400 °C) samples showed minimal change in the intensity of adsorbed surface oxygen species after CO₂ reduction, compared with other samples. This reflects that as discussed above, the Ti (400 °C) samples showed the lowest CO₂ reduction activity, consistent with the data shown in Figure 2C,D.

Figure 6 displays Pt 4f XP spectra for Pt NP/Ti, Pt NP/Ti (400 °C), Pt NP/Ti (700 °C), Pt-sp/Ti, Pt-sp/Ti (400 °C), and Pt-sp/Ti (700 °C) samples before and after CO₂ reduction. For the Pt NP-loaded samples before CO₂ reduction, two major peaks were observed at 75.0 and 71.6 eV for Pt NP/Ti (700 °C), attributed to Pt 4f_{5/2} and Pt 4f_{7/2} XPS peaks of metallic Pt, respectively [29,40]. The Pt NP/Ti sample showed at BEs of 74.7 and 71.4 eV for Pt 4f_{5/2} and Pt 4f_{7/2} XPS peaks. The Pt 4f_{5/2} and Pt 4f_{7/2} XPS peaks for the Pt NP/Ti (400 °C) showed BEs of 74.8 and 71.5 eV, respectively. After CO₂ reduction, the major BE position showed no critical change, but the XPS signals above 75 eV were slightly enhanced. This reflects an increase in Pt^{4+} species showing BEs at 78.8 and 75.3 eV for Pt 4f_{5/2} and Pt 4f_{7/2} XPS peaks. For the sputtered-Pt samples before CO₂ reduction, a big difference in BE position was found. Two major peaks at 76.6 and 73.3 eV were found for Pt-sp/Ti (700 °C) sample, attributed to Pt 4f_{5/2} and Pt 4f_{7/2} XPS peaks of Pt(II), respectively [29]. In addition, smaller peaks were observed at 78.7 and 75.4 eV, attributed to Pt 4f_{5/2} and Pt 4f_{7/2} XPS peaks of Pt(IV), respectively. Metallic Pt was weakly seen in the spectra [20,41]. This indicates that sputtered Pt were of Pt(II) and Pt(IV) species co-existed as oxidized Pt species. For the Pt-sp/Ti samples before CO₂ reduction, two major peaks were found at 76.1 and 72.8 eV. For Pt-sp/Ti (400 °C) before CO₂ reduction, two major peaks were found at 76.4 and 73.1 eV. The Ti support annealed at a higher temperature showed higher BE position for the Pt 4f_{5/2} and Pt 4f_{7/2} XPS peaks of Pt(II). For the Pt-sp/Ti samples after CO₂ reduction, Pt(II) oxidation species were decreased while Pt(IV) and Pt(0) species were observed to be increased. The change in Pt 4f became more distinct for the Ti support annealed at a higher temperature. For the Pt-sp/Ti (700 °C) sample, Pt(IV) species became dominant and the corresponding Pt 4f_{5/2} and Pt 4f_{7/2} XPS peaks were found at 78.7 and 75.4 eV. For the Ti (700 °C) support, Pt(IV) species were commonly observed to be higher than other Ti supports.

For hydrogen production in a three-electrode electrochemical system, electrochemical linear sweep voltammetry (LSV) was tested to examine electrocatalytic hydrogen evolution reaction (HER) activities for Pt wire, bare Ti, oxidized (400 and 700 °C-annealed) Ti, Pt NP/Ti, Pt NP/Ti (400 °C), Pt NP/Ti (700 °C), Pt-sp/Ti, Pt-sp/Ti (400 °C), and Pt-sp/Ti (700 °C) samples. Pt has popularly been used for hydrogen production and shown good catalytic activity [13–16,42]. Figure 7 displays the corresponding LSV data (between 0.0 and −0.8 V vs. Ag/AgCl) obtained in 0.1 M H₂SO₄ solution. The corresponding current
density (CD, mA/cm²) taken at −0.5 V was also plotted for direct comparison of the HER activity. It was clearly shown that the CD was found to be considerably dependent on the Pt-loading and thermal treatment temperature of Ti support. The Pt-free bare Ti, Ti (400 °C), and Ti (700 °C) samples showed the poorest activity, showing onset potentials above −0.6 V, compared with Pt-loaded samples. HER CDs were observed to be 0.07, 0.1, and 0.07 mA/cm² at −0.5 V (vs. Ag/AgCl) for Ti, Ti (400 °C), and Ti (700 °C) samples, respectively. For a Pt wire, the onset potential was observed around −0.22 V. For the Pt-loaded Ti and Ti (400 °C) samples (Figure 7A,B, respectively) showed the onset potentials close to that of a Pt wire. However, the Pt-loaded Ti (700 °C) samples (Figure 7C) showed much higher HER onset potential of −0.5 V. This indicates that the HER activity was shown to be much poorer than those of Pt-loaded Ti and Ti (400 °C) samples. The HER activity showed the order of Ti (700 °C) < Ti < Ti (400 °C), whose order was inverse to the CO₂ reduction. The Ti (400 °C) support showed the highest HER activity and increased upon Pt-loading. This is a clear evidence that catalyst support is very important for improving catalytic activity. For Pt-NP loaded samples, HER CDs were observed to be 4.1, 9.6, and 0.09 mA/cm² at −0.5 V (vs. Ag/AgCl) for Pt-NP/Ti, Pt-NP/Ti (400 °C), and Pt-NP/Ti (700 °C), respectively. For sputtered Pt-loaded samples, HER CDs were observed to be 7.6, 10.5, and 1.1 mA/cm² at −0.5 V (vs. Ag/AgCl), Pt-sp/Ti, Pt-sp/Ti (400 °C), and Pt-sp/Ti (700 °C), respectively. It was common that the sputtered Pt-loaded samples showed higher HER activity compared with the corresponding Pt-NP loaded samples, in good agreement with the literature [33]. Lian et al. also observed same for H₂ evolution efficiency tests over Pt<sup>n+</sup> (n = 0, 2, or 3)-Ti³⁺/TiO₂ and metallic Pt-loaded Ti³⁺/TiO₂ [33]. XPS data (Figure 6) and HER activity (Figure 7) clearly confirms that the oxidation state of overlayer Pt plays a significant role in improving HER activity. In addition, when the TiO₂ layer is too thick (in case of the 700 °C-treated samples) the HER activity becomes poor because of poor electrical current flow in an electrochemical reaction.

![HER mechanism diagram](https://example.com/HER_mechanism.png)

**Figure 7.** Linear sweep voltammetry (LSV) data at a scan rate of 10 mV/s for: (A) bare Ti, Ti (400 °C) and Ti (700 °C); (B) Pt NP/Ti, Pt NP/Ti (400 °C) and Pt NP/Ti (700 °C); (C) Pt-sp/Ti, Pt-sp/Ti (400 °C) and Pt-sp/Ti (700 °C) samples, and for Pt wire (blank line); (D) current density (mA/cm²) taken at −0.5 V for the corresponding samples. The HER mechanism is depicted below.
For the HER mechanism in acidic media, hydrogen is adsorbed on the catalyst surface via $\text{H}_3\text{O}^+ + e^- \rightarrow \text{H}_2\text{O} + \text{H}_2$. Then, molecular hydrogen is released from the surface via $\text{H}_2\text{ad} + \text{H}_3\text{O}^+ + e^- \rightarrow \text{H}_2 + \text{H}_2\text{O}$ or $\text{H}_2\text{ad} + \text{H}_2\text{ad} \rightarrow \text{H}_2$.\textsuperscript{[43–45]} The mechanism is depicted in Figure 7, where the adsorption of H occurs on (or periphery of) PtO$_x$ or Pt NPs species. When hydrogen adsorption Gibbs free energy, $\Delta G_{\text{HX}}$ is closer to 0 eV the HER activity become higher. When Pt (or PtO$_x$) is present, the $\Delta G_{\text{HX}}$ appears to be close to 0 and the HER activity becomes enhanced\textsuperscript{[43–45]}. The $\Delta G_{\text{HX}}$ is determined by Pt oxidation states (or the relative ratio). The highest HER activity was observed for the support with higher Pt(II) species. When Pt(IV) species were higher on the Ti support, the activity was observed to be poorer. The Ti support with Pt(0) species showed somewhat less activity, compared with the support with Pt(II) species. On the basis of the results, the oxidation state of Pt determines $\Delta G_{\text{HX}}$ and consequently affects the HER activity. This needs further investigation. In addition to this Pt oxidation state, the thickness of TiO$_2$ overlayer is an important factor as depicted in Figure 7. The thick TiO$_2$ layer for the 700 °C-treated samples exhibited poor electrical current to result in low HER activity.

4. Conclusions

In summary, Pt NPs and sputtered-Pt were loaded on Ti sheets with different oxidation states, and tested for photocatalytic CO$_2$ reduction in a closed reaction chamber and electrochemical hydrogen evolution reaction. Two different demonstration tests were performed to precisely examine the roles of Pt and Ti supports in different application areas. XPS studies confirmed that Pt NP were mainly metallic Pt(0) oxidation state, while sputter-deposited Pt were both Pt(II)-O and Pt(IV)-O species. Ti support before thermal annealing showed oxidation states of Ti(II), Ti(III), and Ti(IV) while the thermal (400 and 700 °C)-annealed Ti showed only the Ti(IV) oxidation state. The CO$_2$ reduction products were commonly observed to be CO, CH$_4$, and CH$_3$OH, and the Pt-free Ti (700 °C) sample showed total yields of up to 87.3, 88.0, 26.9 ppm for the formation of CO, CH$_4$, and CH$_3$OH, respectively under UVC irradiation for 13 h. For bare Pt-free Ti substrates, the activity showed the order of Ti (400 °C) < Ti (700 °C). Pt-loading commonly negated the CO$_2$ reduction yields, but CH$_4$ selectivity was found to be increased. For electrochemical hydrogen evolution reaction (HER), the Ti (700 °C) support showed the poorest activity and the HER CDs commonly showed the order of Ti (700 °C) < Ti (400 °C), whose order was inverse to the CO$_2$ reduction. The Ti (700 °C) support showed poorest HER activity, although Pt was loaded on the support. The Ti (400 °C) support showed the highest HER activity increased upon Pt-loading. HER CDs were observed to be 0.1, 9.6, and 10.5 mA/cm$^2$ at −0.5 V (vs. Ag/AgCl) for bare Ti (400 °C), Pt NP/Ti (400 °C) and Pt-sp/Ti (400 °C), respectively. Sputtered Pt-loaded samples showed a higher activity than the corresponding Pt NP-loaded samples. Conclusively, CO$_2$ reduction and electrochemical HER activities were mainly determined by the nature of Ti support and Pt oxidation (0,II,IV) species. The present demonstration tests provide valuable information on the design of Pt-overlayer metals and Ti-supports for energy and the environment.

**Author Contributions:** J.H.Y. performed the CO$_2$ reduction and HER experiments; S.J.P. performed the XPS experiments; C.K.R. designed the experimental concepts; Y.S. designed the experiments and wrote the paper. All authors have read and agreed to the published version of the manuscript.

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