1. Introduction

Microbe-based systems are important and versatile biotechnological processes for the production of various chemical substrates because of the limited space required for their cultivation, their rapid growth, and diverse physiological and biochemical properties [1]. Citric acid is one of the most common microbial fermentation-based commercial products for which there is a never ending demand. In 2008, global production of citric acid exceeded 1.6 million tons, and is only expected to increase in the future [2,3]. Because of its low toxicity and high solubility and palatability, citric acid plays an essential role in the beverage, food, pharmaceutical, cosmetic, and household cleaning product industries, amongst others [4,5]. Citric acid is generally produced on a commercial scale either by fermentation or chemical synthesis, although the vast majority (>90%) is produced via fermentation [6]. A large number of microorganisms, including both bacteria and fungi, are used to produce citric acid [7,8]. Although fungal species Aspergillus niger is traditionally used for commercial citric acid production, systems using various yeast species have recently attracted some attention [9,10]. Bioprocesses for citric acid production using yeasts have several advantages compared with Aspergillus processes, including a larger spectrum of substrates, decreased sensitivity to low dissolved oxygen concentrations and heavy metals, genetic and mechanical stability, and fewer health hazards [11].

Three fermentation methods, including surface fermentation, submerged fermentation, and solid-state fermentation, can be used for the industrial production of citric acid. However, these conventional fermentation mechanisms suffer from various drawbacks such as nutritional limitations, low cell density, and batch-mode operations with significant down times [12]. In addition to environmental conditions, strain isolation and selection are important.
factors for the regulation of product formation during fermentation [13]. There is significant interest in improving the production of citric acid using immobilized cell techniques [9,14].

The aims of this study were: (i) to obtain new yeast isolates that could produce high yields of citric acid; (ii) to identify citric acid-producing yeasts at the species level using polymerase chain reaction (PCR)-based amplification and sequence analysis of the D1/D2 region of the 26S rRNA gene; (iii) to optimize the nutritional and environmental factors affecting citric acid production; and (iv) to improve citric acid production using an immobilization technique and repeated-batch culture.

2. Materials and methods

2.1. Samples collection

Yeast strains were isolated from fruits, juices, dates, tomatoes, bread wastes, and soil samples collected from different locations in the Asir region of Saudi Arabia. The samples were maintained in a clean plastic container at room temperature and stored until rot to be ready to use.

2.2. Isolation and purification of yeast isolates

The yeast strains were isolated and purified according to the method described by Kurtzman and Fell [15].

Dilution plate method and direct touch method were used for yeast isolation. For dilution plate method, one gram of each sample was placed in a conical flask containing 50 mL sterile distilled water. The suspension was shaken on mechanical shaker for 30 min. A 0.1 mL of the suspension was added to the yeast extract peptone dextrose (YEPD) agar medium and incubated at 27°C for 48–72 h. The YEPD agar plates contained (g/L): glucose 100, NH₄Cl 0.6, KH₂PO₄ 1, MgSO₄·7H₂O 1.0, yeast extract 1.0, CaCO₃ 4.0, bromocresol green 0.2, Triton X-10 1.5 mL (pH 5.5). A loopful of yeast colony was inoculated on agar plates and incubated at 27°C for 48 h. Formation of a yellow halo around the colonies indicated the ability of isolates to produce organic acid. The AU values of the colonies were determined by dividing the diameter (mm) of the yellow zone by the diameter (mm) of the colonies [16]. The promising colonies having notable AU values were selected for further study and kept as stock cultures at 4°C on YEPD agar medium. The isolates showing the highest levels of acid production were secondary screened for citric acid production using submerged cultures by free and immobilized cell techniques [17]. The inoculum was prepared by incubation of the isolates at 27°C, 150 rpm for 48 h in a YEPD agar medium. The production of citric acid was carried out in 250 mL flasks containing 50 mL of fermentation medium (without bromocresol green) in an incubator shaker at 27°C and 150 rpm for five days. After incubation, the medium was centrifugation at 6000 rpm for 20 min and the supernatant was used for the determination of citric acid production.

2.3. Screening of acid producing yeasts

All yeast isolates were primarily screened for organic acid production by determining the acid unitage (AU) values using the fermentation medium containing (g/L): glucose 100, NH₄Cl 0.6, KH₂PO₄ 1, MgSO₄·7H₂O 1.0, yeast extract 1.0, CaCO₃ 4.0, bromocresol green 0.2, Triton X-10 1.5 mL (pH 5.5). A loopful of yeast colony was inoculated on agar plates and incubated at 27°C for 48 h. Formation of a yellow halo around the colonies indicated the ability of isolates to produce organic acid. The AU values of the colonies were determined by dividing the diameter (mm) of the yellow zone by the diameter (mm) of the colonies [16]. The promising colonies having notable AU values were selected for further study and kept as stock cultures at 4°C on YEPD agar medium. The isolates showing the highest levels of acid production were secondary screened for citric acid production using submerged cultures by free and immobilized cell techniques [17]. The inoculum was prepared by incubation of the isolates at 27°C, 150 rpm for 48 h in a YEPD agar medium. The production of citric acid was carried out in 250 mL flasks containing 50 mL of fermentation medium (without bromocresol green) in an incubator shaker at 27°C and 150 rpm for five days. After incubation, the medium was centrifugation at 6000 rpm for 20 min and the supernatant was used for the determination of citric acid production.

2.4. Molecular identification of the selected yeasts

Genomic DNA was extracted from the isolated yeast strains according to our previously described method [18]. The D1/D2 domain of the 26S rRNA gene was amplified using universal primers NL1 (5′-GCATATCAATAAGCGGAGGAAAAG-3′) and NL4 (5′-GGTCCGTGTTTCAAGACGG-3′) and the PCR conditions and parameters described by Kurtzman and Robnett [19]. PCR was performed in 50 μL as a final volume containing GoTaq (Promega, Madison, WI, USA) green master mix, 1 μL DNA sample and each primer 1 μL (at a concentration of 0.5 mM). PCR was under the following conditions: initial denaturation at 95°C for 5 min, followed by 36 cycles at 94°C for 2.0 min, 52°C for 1.0 min, 72°C for 2.0 min; final extension at 72°C for 7 min, holding at 4°C. Briefly, 5 μL of PCR products was then analyzed using 1.5% 0.59 TBE agarose gel electrophoresis. The gel was stained with ethidium bromide, visualized under UV light, and photographed. Product of the correct size was purified with a TaKaRa Agarose Gel DNA Purification Kit version 2.0 and sequenced in both directions using an ABI 3730 automated sequencer (Macrogen,
2.5. Optimization of culture conditions for citric acid production

Citric acid production by the selected strains was evaluated using fermentation medium [17,20]. The inoculum was prepared by growing the yeast culture in the YEPD medium at 27 °C, 150 rpm for 48 h. After immobilization technique, the calcium alginate pellets (4 g) were washed with distilled sterile water and suspended in a 250-mL Erlenmeyer flask containing 50 mL of fermentation medium and incubated at 27 °C in an incubator shaker at 150 rpm for 8 days. At regular (1 day) intervals, the triplicate samples were harvested. The pellets were removed by centrifugation (6000 rpm for 20 min) and used for growth determination and the supernatant was used for glucose and citric acid assay. Factors affecting citric acid production, including pH (3–7), temperature (18–42 °C), carbon source (sucrose, mannitol, glucose, fructose, maltose, starch, ethanal, glycerol), and nitrogen source (urea and ammonium salts; ammonium sulfate monobasic, ammonium sulfate, ammonium ferrous sulfate, diammonium hydrogen-phosphate, ammonium dihydrogen phosphate, ammonium chloride), were then investigated. All experiments were conducted in triplicate.

2.6. Immobilization of yeast cells

Sodium alginate was used to prepare the immobilized cells as described previously [21]. It was autoclaved for 5 min at 121 °C and stored overnight at 4 °C to facilitate de-aeration. To form an alginate–cell mixture, 5 mL of cell suspension was added to 50 mL of 3% (wt/vol) alginate solution and then dropped into 1.5% (wt/vol) CaCl₂ by using 2 mL pipettes to prepare the immobilized cells of approximately 3 mm in diameter. Pellets were hardening in the same solution with stirring for 1 h at 20 °C, washed three times with 0.9% (wt/vol) NaCl solution and stored in CaCl₂ solution at 4 °C.

2.7. Repeated-batch fermentation

Repeated-batch cultures were conducted by running the citric acid fermentation for the optimum period, at the end of each cycle the immobilized cells were washed (2% (wt/vol) CaCl₂ for 30 min) for curing the gel capsules by maintaining their mechanical structure and increasing their productive life, fresh production medium was added and the fermentation was continued. Curing the gel capsules with 2% CaCl₂ after each fermentation batch not only prevented the disruption of the capsules and maintained their mechanical structure but it also increased significantly the productive life of the biocatalysts as described by Konsoula and Liakopoulou-Kyriakides [22].

2.8. Analytical methods

Microbial growth: After fermentation process, the culture was centrifuged and both cell growth in freely suspended cultures and immobilized cells in alginate matrix were determined as cell dry weight (drying in an oven at 70 °C). Biomass were determined from the difference between the total weight of the alginate gel capsules containing cells and that of alginate capsules without cells (blank) prepared under the same conditions. Glucose assay: The culture supernatant was used for the calorimetric determination of consumed glucose (%) by Sigma-Aldrich kit according to the manufacturer’s recommendations using a double beam UV/vis scanning spectrophotometer at 500 nm. Citric acid assay: Anhydrous citric acid was estimated by pyridine-acetic anhydride method [23] using a double beam UV/vis scanning spectrophotometer (Model 1601PC: Shimadzu, Kyoto, Japan). The citric acid content in supernatant was determined by adding 1 mL of sample (containing from 25 to 200 mg of citric acid), 1.3 mL of pyridine, and 5.7 mL of acetic anhydride to a test tube. After incubation for 30 min at 32 °C, the color intensity was estimated at 420 nm. Citric acid standard was prepared from anhydrous citric acid at 0.1–0.3 g/L. It was also performed using KCITR enzymatic test kit (Megazyme, Wicklow, Ireland).

2.9. Statistical analysis

The results were analyzed by comparing the means of the obtained data with the values for individual controls. Results are expressed as mean ± standard deviation. Significant differences among values were
analyzed using analysis of variance (one-way ANOVA). Results were considered significant at \( p < 0.05 \). Statistical analysis was performed using SPSS version 15.0 software [24].

3. Results and discussion

3.1. Isolation and screening of citric acid-producing yeast isolates

In this study, 260 yeast isolates were successfully isolated from various samples collected from the southern region of Saudi Arabia. The isolates were screened for their ability to produce organic acids using bromocresol green agar plates test, with 251 isolates showing a positive result (yellow halo formation around the colonies). The halo zone diameters gradually increased from 2 mm at 24-h post-inoculation to about 16 mm at 48-h post-inoculation, which was similar to observations made using the same screening method for organic acid-producing yeasts [16,25]. The highest organic acids producing ability was detected by two yeast isolates: KKU-L42 isolated from banana wastes (16.2 mm), and KKU-L53 isolated from apple wastes (15.4 mm). Twenty promising yeast isolates were subjected to further screening for their ability to produce citric acid using free and immobilized cell technique. Results showed that citric acid production by immobilized cells (30–40 g/L) was significantly greater than that of the freely suspended cells (8–19 g/L) within the same period (Figure 1). The use of immobilized cells as a novel fermentation technology has been investigated for many microbial products, and several advantages of this method over free cells have been identified [14,26]. Of the 20 isolates examined, isolates KKU-L42 and KKU-L53 showed the highest levels of citric acid production (36.9 g/L and 27.5 g/L, respectively). Using the immobilized cell technique, isolate KKU-L42 showed a 62.5% increase in production compared with free cells, while immobilized KKU-L53 cells showed a 52.2% increase in citric acid production. These isolates were therefore selected for further studies. The increased citric acid production by the immobilized cells than by the free cells may be due to the formation of strong gel capsules possessing high substrate mass transfer rates, higher cell density, the low viscosity of the broth substantially, facilitating oxygen transfer with less agitation [27]. Despite several carriers such as k-carrageenan, polyurethane gel, nylon web, and polyurethane foam used for immobilization of the yeast cells, entrapped cells in alginate exhibited highest citric acid productivity [28]. The highest citric acid productivity by Candida guilliermondii was recorded with alginate-bead-immobilized cells because of its large surface area for cell attachment [26].

![Figure 1. Screening of citric acid producing yeasts. (A) Using free cells (F value = 3.518); (B) Using immobilized cells technique (F value = 3.518). Mean ± standard error (n = 3) were presented. Vertical bars indicate the standard errors of the means.](image-url)
3.2. 26S rRNA gene D1/D2 domain sequence-based identification and phylogenetic analysis

Genomic DNA was obtained from isolates KKU-L42 and KKU-L53 and used as a template for amplification and sequencing of the D1/D2 region of the 26S rRNA gene which has gained recognition in yeast taxonomy as important identification tool [19,29–31]. Alignment of the resulting sequences against published 26S rRNA gene sequences in the GenBank database confirmed that the KKU-L42 and KKU-L53 sequences showed 99% nucleotide identity to the corresponding regions in Candida tropicalis and Pichia kluyveri, respectively. To confirm the identification of each strain, a number of representative Candida and Pichia 26S rRNA gene sequences were selected from the GenBank database for construction of phylogenetic trees. The trees showed that the strain KKU-L42 sequence clustered with the C. tropicalis sequences (Figure 2(A)), while the sequence from strain KKU-L53 clustered with the P. kluyveri sequences (Figure 2(B)), confirming the original identification of the two strains. The citric acid-producing yeast isolates were obtained from pineapple, plantain, and sugar cane waste and molecular identified as Saccharomyces cerevisiae, Schizosaccharomyces pombe, C. tropicalis, Pichia guilliermondii, Debaryomyces sp., Candida parapsilosis, Candida rugosa, and Candida krusei [1].

3.3. Effects of time course on citric acid production

Yeast growth and citric acid production were influenced by the fermentation time. As shown in Figure 3, citric acid was secreted early on in the active growth phase, reaching a maximum near the end of the logarithmic phase. Maximum production was obtained after 5 days of cultivation for both C. tropicalis (36.3 g/L) and P. kluyveri (27.4 g/L). At the end of the optimum fermentation period, biomass and glucose consumed were 8.66 g/L and 82.2% for C. tropicalis and 10.76 g/L and 71.46% for P. kluyveri. The citric acid production was observed to be dependent on microbial growth suggesting that these organisms may be sensitive to metabolite repression [32,33]. The decrease in productivity at the later phase of growth probably resulted from the following factors: (i) the age of the microbes used, (ii) the inhibitory effects of high concentrations of citric acid, (iii) decay in the enzyme system responsible for biosynthesis of citric acid, and (iv) depletion of sugar in the culture broth [32]. As has been shown previously, the optimum incubation time for maximum citric acid production varies with the microbes and fermentation conditions. The optimum citric acid production by S. cerevisiae and C. guilliermondii was attained after 3–5 days of incubation [34], 40 h for Candida lipolytica [35], 12 days

Figure 2. Phylogenetic analyses of the isolates using 26S rRNA gene sequences. (A) KKU-L42; (B) KKU-L53. The scale bar corresponds to a 0.02 nucleotide substitution per sequence position. The number in parentheses represents the accession number in GenBank.
Vertical bars indicate the standard errors of the means. For Yarrowia lipolytica [8,10], while using of P. kluveyi to enhance the flavor of fish sauce, it produced citric acid, malic acid, and succinic acid within the first 3 days of fermentation [36].

### 3.4. Effect of initial pH on citric acid production

The pH of the fermentation medium is known to be a critical parameter for citric acid production by yeasts. In the current study, the influence of initial pH on citric acid production was examined over a pH range of 3.0–7.0. The results presented in Figure 4 showed that a pH of 5.0 was the most favorable for citric acid production and growth of the two strains. Our results were in agreement with those of Papanikolaou et al. [37] and Ferreira et al. [38] and Y. lipolytica, using glucose as carbon source and finding that the highest citric acid concentration and biomass productivity were obtained at pH 5. Above optimum pH, citric acid production was markedly decreased, at pH 5.5, C. tropicalis showed a 5.9% decrease in citric acid production compared with that at pH 5.0, with only 75.6% of glucose being consumed, while P. kluveyi showed a 25.1% reduction in citric acid production and only 64.5% of the available glucose was consumed. Furthermore, below pH 5.0, the citric acid concentration decreases due to the accumulation of some polyalcohols like erythritol and arabitol instead of citric acid [39] and inhibition of transport of citrate from cell membrane [40]. The initial pH of the fermentation medium must be very well defined and optimized depending on the microorganism, substrate, and production technique [41]. Several studies mentioned that the optimum pH for citric acid production was varied even for the same strain at a broad value between pH 3.5 and pH 7.0. The maximum citric acid production by Y. lipolytica was achieved at pH 5.5–6.0 [8,10,25,42], Y. lipolytica 57 and Y. lipolytica NBRC 1658 at pH ranges of 5.2–7.0 [17], S. cerevisiae at pH 4.5 [6], whereas for S. cerevisiae and C. guilliermondii at pH 3.5 [34], while for S. cerevisiae and C. tropicalis citric acid was produced at pH 6 and pH 4.0 for P. guilliermon-dii [1].

### 3.5. Effect of incubation temperature on citric acid production

Incubation temperature plays an important role in citric acid production by affecting all the physiological activities of microbes [8,10]. To determine the optimal temperature for citric acid production, fermentations were carried out at temperatures ranging from 22 to 42°C (Figure 5). The results revealed a significant relationship between citric acid production and incubation temperature up to
The ability of the two novel yeast strains to utilize different carbon sources (ethanol, glycerol, starch, glucose, sucrose, fructose, maltose, and mannitol) for the production of citric acid was conducted. The results revealed that citric acid production is strongly affected by the carbon source, with glucose being the preferred carbon source for both strains (Table 1). Other than fructose, sucrose, and maltose, all of the carbon sources examined supported growth and citric acid production by the two yeast strains. Glycerol was the second most favorable carbon source, resulting in citric acid production levels of about 80.89% and 82.88% than those obtained using glucose for C. tropicalis and P. kluyveri, respectively. When fructose and sucrose were used as carbon sources, the citric acid yield of C. tropicalis decreased to only 13.69% and 34.56%, respectively, of the yield obtained using glucose. Similarly, citric acid production by P. kluyveri decreased to 8.24% and 33.6% of levels obtained using glucose when fructose and maltose were used as the carbon source, respectively. The presence of easily metabolized carbohydrates is essential for optimum production of citric acid [45]. Candida strains can produce citric acid from various carbohydrates, although glucose has generated increasing interest [39]. The basic principle of utilizing glucose as a carbon source for citric acid production extensively investigated where the high activity of citrate synthase is pronounced for yeast strains [46]. The highest citric acid production was achieved at optimum sugar concentration, because such high concentration of the carbon source lead to suppression of α-ketoglutarate dehydrogenase while, at low glucose levels, the yeast size and its shape is affected [47]. The highest amounts of citric acid produced by Y. lipolytica were observed in the production medium containing sunflower oil (50–66.2 g/L) as a carbon source [25], sucrose (127–140 g/L) [41], and crude glycerol (8–10 g/L) [38].

3.7. Effects of nitrogen source on citric acid production

The effects of seven different nitrogen sources (diammonium hydrogen phosphate, ammonium dihydrogen phosphate, ammonium chloride, ammonium ferrous sulfate, urea, ammonium phosphate monobasic, and ammonium sulfate) on citric acid production was also investigated. As illustrated in Table 2, the results revealed that the ammonium salts were the best sources of nitrogen for the synthesis of citric acid by both strains. Citric acid production and sugar consumption by C. tropicalis were highest when ammonium chloride was used as the nitrogen source, reaching 50.53 g/L and 94.53%, respectively. Furthermore, while ammonium sulfate and diammonium hydrogen phosphate did not result in any significant change in the production of citric acid, urea and ammonium ferrous sulfate
significantly decreased the production of citric acid. In comparison, optimum citric acid production (35.4 g/L) and glucose consumption (81.56%) by *P. kluyveri* were achieved using ammonium sulfate as the nitrogen source, corresponding to 33.28% and 10.06% increases, respectively, over the control medium. Diammonium hydrogen phosphate and ammonium dihydrogen phosphate did not result in any significant change in the production of citric acid, while urea and ammonium ferrous sulfate significantly reduced citric acid production. Interestingly, Çelik et al. [25] reported that optimum citric acid production (66.2 g/L) by *Y. lipolytica* was achieved using ammonium sulfate as the nitrogen source, while Yalcin [48] showed that ammonium chloride was the optimum nitrogen source for citric acid production by *Y. lipolytica* (50 g/L). On the other hand, *C. tropicalis* produced 132.2 mg/L using sodium nitrate as an optimum nitrogen source [1].

### 3.8. Repeated-batch fermentation

One of the most important benefits of immobilized cells is their ability to stably produce citric acid under repeated-batch cultivation. Separately, immobilized *C. tropicalis* and *P. kluyveri* cells were collected from the fermentation medium after 5 days and transferred into fresh sterile fermentation medium. This process was repeated six times. The citric acid and glucose concentrations over this period are shown in Table 3. The results indicated that immobilized cells of both strains showed high citric acid productivity upon re-use. The culture activity of *C. tropicalis* remained stable up until the

### Table 1. Effect of carbon sources on citric acid production by *Candida tropicalis* (F value = 279.651) and *Pichia kluyveri* (F value = 85.656).

| Yeast isolates          | *Candida tropicalis* | *Pichia kluyveri* |
|-------------------------|----------------------|-------------------|
| Carbon sources          | Citric acid (g/L)    | Biomass (g/L)     | Citric acid (g/L) | Biomass (g/L) |
| Ethanol                 | 26.36 ± 0.40         | 6.53 ± 0.29       | 17.13 ± 0.31      | 7.30 ± 0.52   |
| Glycerol                | 21.96 ± 0.88         | 10.76 ± 0.23      | 22.43 ± 0.65      | 9.80 ± 0.20   |
| Starch                  | 21.96 ± 0.94         | 7.10 ± 0.41       | 11.43 ± 0.29      | 4.20 ± 0.34   |
| Glucose                 | 49.36 ± 0.75         | 11.53 ± 0.44      | 27.06 ± 0.40      | 7.96 ± 0.23   |
| Sucrose                 | 17.06 ± 0.63         | 4.86 ± 0.31       | 21.33 ± 0.57      | 9.03 ± 0.29   |
| Fructose                | 6.76 ± 0.80          | 1.08 ± 0.22       | 2.23 ± 0.59       | 3.30 ± 0.37   |
| Maltose                 | 35.33 ± 0.74         | 8.73 ± 0.52       | 9.13 ± 0.58       | 6.20 ± 0.47   |
| Mannitol                | 28.66 ± 0.83         | 6.40 ± 0.32       | 14.66 ± 0.73      | 8.56 ± 0.31   |

Mean ± standard error (*n* = 3) were presented.

### Table 2. Effect of nitrogen sources on citric acid production by *Candida tropicalis* (F value = 107.536) and *Pichia kluyveri* (F value = 44.401).

| Yeast isolates          | *Candida tropicalis* | *Pichia kluyveri* |
|-------------------------|----------------------|-------------------|
| Nitrogen sources        | Citric acid (g/L)    | Biomass (g/L)     | Glucose consumed (%) | Citric acid (g/L) | Biomass (g/L) | Glucose consumed (%) |
| Diammonium hydrogen phosphate | 40.90 ± 0.73         | 8.90 ± 0.79       | 82.96 ± 0.90       | 23.10 ± 0.92      | 9.36 ± 0.48   | 66.03 ± 0.58   |
| Ammonium dihydrogen phosphate | 30.60 ± 0.78         | 5.40 ± 0.51       | 65.60 ± 0.45       | 11.33 ± 0.98      | 8.36 ± 0.35   | 60.83 ± 0.99   |
| Ammonium chloride       | 50.53 ± 0.83         | 11.40 ± 0.62      | 94.54 ± 0.92       | 26.56 ± 0.43      | 10.90 ± 0.37  | 71.50 ± 0.56   |
| Ammonium ferrous sulfate | 24.40 ± 0.72         | 6.43 ± 0.56       | 45.46 ± 0.64       | 14.66 ± 0.49      | 7.30 ± 0.52   | 30.43 ± 0.75   |
| Urea                   | 21.83 ± 0.58         | 3.43 ± 0.35       | 36.23 ± 0.84       | 8.43 ± 0.43       | 4.26 ± 0.17   | 22.10 ± 0.80   |
| Ammonium phosphate monobasic | 37.13 ± 0.72         | 9.16 ± 0.43       | 62.33 ± 0.99       | 17.36 ± 0.35      | 6.30 ± 0.47   | 37.16 ± 0.89   |
| Ammonium sulfate        | 41.52 ± 0.46         | 10.53 ± 0.76      | 88.90 ± 0.46       | 35.40 ± 0.46      | 11.46 ± 0.40  | 81.56 ± 0.10   |

Mean ± standard error (*n* = 3) were presented.

### Table 3. Repeat batch culture for citric acid production by *Candida tropicalis* (F value = 279.651) and *Pichia kluyveri* (F value = 374.689).

| Yeast isolates | *Candida tropicalis* | *Pichia kluyveri* |
|----------------|----------------------|-------------------|
| Batches no.    | Citric acid (g/L)    | Glucose consumed (%) | Citric acid (g/L) | Glucose consumed (%) |
| 1.0            | 49.73 ± 0.753        | 94.53 ± 0.920      | 35.40 ± 0.461     | 81.56 ± 1.043      |
| 2.0            | 50.33 ± 0.491        | 94.56 ± 0.384      | 35.16 ± 0.648     | 81.96 ± 1.074      |
| 3.0            | 50.60 ± 1.121        | 95.10 ± 0.519      | 34.76 ± 0.437     | 81.93 ± 0.883      |
| 4.0            | 47.53 ± 0.779        | 86.03 ± 0.480      | 35.56 ± 0.825     | 80.46 ± 0.943      |
| 5.0            | 28.66 ± 1.065        | 45.26 ± 0.560      | 21.50 ± 0.680     | 45.46 ± 0.643      |
| 6.0            | 14.66 ± 0.731        | 7.30 ± 0.529       | 6.43 ± 0.643      | 14.66 ± 0.731      |

Mean ± standard error (*n* = 3) were presented.
third cycle, and cells retained about 93.93% of their initial efficiency during the fourth batch. However, citric acid production and glucose consumption decreased from the fourth batch and a dramatic reduction was observed during the fifth batch. In comparison, culture activity of _P. kluyveri_ remained stable up until the fourth cycle before reducing to about 60.73% of the initial activity during the fifth batch. Therefore, repeated-batch fermentation with calcium alginate beads was successfully run for four batches for both strains. The repeated-batch culture technique is superior to batch cultivation for reducing the costs of fermentation by eliminating the need for multiple sterilization and inoculum preparation steps [49]. The activity of the repeat batch culture of _Y. lipolytica_ remained stable after cultivation for more than 58 days which reduces the costs of fermented sterilization and inoculum preparation compared to batch fermentation [32]. Also, repeated batch production of citric acid by _C. oleophila_ ATCC 20177 [46] and _C. guilliermondii_ [26] seems to have many advantages compared with the traditional industrial processes. The decline of the cultural activity after the fourth cycle may be occurring because of clogging of pores of the alginate immobilized cells. Thus, citric acid was accumulated inside the gel and could not penetrate the outside of the gel which causes the inhibition of the citrate synthase [2].

In conclusion, 260 yeast isolates were successfully isolated from Saudi Arabia. A total of 251 yeast isolates were able to produce organic acids. The productivity of citric acid by immobilized cells was significantly greater than that of the freely suspended cells. The sequences of domains D1 and D2 of the 26S rRNA gene and phylogenetic analysis confirmed the identification of the two promising citric acid-producing isolates as _C. tropicalis_ and _P. kluyveri_. Maximum citric acid production was achieved after 5 days of fermentation with optimum pH 5.0 and glucose as a carbon source for the two isolates. Optimum incubation temperature for citric acid production by _C. tropicalis_ was 32°C with ammonium chloride as the best nitrogen source, while it was 27°C with the ammonium sulfate as a good nitrogen source for _P. kluyveri_. The activity of the cultures remained stable after a repeat batch culture for four cycles of 20 days. The results demonstrated that the two yeast strains _C. tropicalis_ and _P. kluyveri_ could be recommended for citric acid production using a repeat batch culture technique by immobilized cells.

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**ORCID**

Abd El-Latif Hesham [http://orcid.org/0000-0002-0614-7658](http://orcid.org/0000-0002-0614-7658)

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