Effect of Operating Parameters on Extraction of Oil from Bitter Gourd Seeds: A Kinetic and Thermodynamic Study

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Abstract: Bitter gourd (Momordica charantia) is a very nutritious vegetable having high therapeutic value due to the presence of α-Eleostearic acid and exhibits anti carcinogenic properties. Present study involves extraction of oil from bitter gourd seeds using soxhlet apparatus with n-hexane as a solvent. The effect of extraction time, volume of solvent and particle size of bitter guard on oil yield was estimated and observed that, the oil yield has increased with increase in time and volume of solvent but decreased with increase in particle size. It was also observed that, a maximum oil yield of 51% was obtained at 100°C for an extraction time of 150 minutes using 15g of dried Bitter Gourd seed and 50 ml of n-hexane. Apart from these, the kinetics and thermodynamics of oil extraction from bitter gourd seeds was also studied. The kinetic studies have shown that the extraction process has fourth order kinetics and the thermodynamic studies reveal that the process is endothermic and requires energy.

Keywords: Kinetics, Thermodynamics, Solvent Extraction, Bitter gourd, n-Hexane

1. Introduction

Momordica charantia L., commonly referred as bitter gourd, Karela, bitter melon, or balsam pear belongs to the Cucurbitaceae family [1]. It is a tropical plant that is widely cultivated in Asia, East Africa and South America [2,3]. The immature fruits of bitter gourd are a good source of Vitamin C, Vitamin A, phosphorus and iron and are rich in minerals including K, Ca, Zn and Mg [4,5]. Biologically, it has a good source of dietary fiber. It is used in folk medicine for treatment of various ulcers, diabetes, infections [6,7,8], gout [9], wounds, infections, parasites (e.g., worms), hepatitis and fevers. Also, it is extensively used in paints, coatings and inks.

There are various techniques such as mechanical, solvent, traditional and super critical fluid extraction methods to obtain the oil from the seeds. Among these methods solvent extraction has become popular for easy and high percentage of oil recovery from seeds. Further, mechanical extraction produces oil with high turbidity and water content and supercritical fluid extraction is very expensive to build and maintain. The solvent, n-Hexane is often used for oil extraction because of its lower boiling point, non-polar nature for easy separation after extraction and it has low toxicity. The yield % of oil obtained by using n-hexane is high compared with ethanol from neem [10]. Several parameters such as particle size, volume of solvent, operating temperature and extraction time has been found to affect the percentage yield of oil from seeds. Hence, the determination of the effects of these parameters on oil yields from seeds is important to minimize the loss of oil, amount of energy expanded over time and finally the cost of extraction. The present study involved extraction of oil from bitter gourd seeds using n-Hexane, determining the effect of time, volume of solvent and particle size on the percentage yield of oil and in detail the kinetic and thermodynamic properties of oil.

2. Materials and Methods

2.1. Seed Collection and Preparation

Commercially available bitter melon seeds were bought from local market and washed thoroughly with distilled water to remove dirt, dust and the pesticide residue. The seeds were then dehulled and subsequently dried in a tray drier at 60°C until a constant weight of seeds is obtained [11]. The dried seeds were cooled and ground using a grinding machine and sieved through different Tyler screens to obtain average particle sizes of 1.303mm, 0.9545mm, 0.564mm, 0.358mm and 0.253mm. The samples were stored in separate air tight containers and labeled adequately.

2.2. Solvent Extraction

A determined quantity of n-Hexane was taken in a Soxhlet extractor. The weight of 12.0024 g of bitter gourd seed on Whatman No.1 filter paper was placed in the thimble of the Soxhlet extractor. The condenser ensures that the solvent vapor cools and drips back down into the chamber housing the solid material. The heating mantle was set at a specified temperature for the experiment and the extraction was carried out for a given time. After the extraction of oil with n-hexane, the set up was dismantled and the miscella (mixture of n-hexane and Bitter gourd oil) obtained was poured into the distillation flask placed on the heating mantle. The heating mantle was set at 68°C which is the boiling point of pure hexane. After distillation, the weight of the oil was determined. The effect of various parameters like time, amount of solvent and particle size on oil yield was estimated during the extraction process.

\[% \text{Yield}(Y) = \frac{\text{weight of pureoil extracted (g)}}{\text{weight of the initial sample (g)}} \times 100 \] (1)
2.3. Kinetics Studies

The kinetic parameters are calculated by studying the effect of time on the extraction process which are related by the equation, 
\[ (dY/dt) = kY^n \]  
- (2)

Where Y is percentage oil yield; t is time of extraction (min); k is extraction constant; and n is the reaction order. The plot of ln (dY/dt) and ln Y gives a straight line, the slope of which gives the order of the reaction n and the intercept gives the ln(k) value [12].

2.4. Thermodynamics

Thermodynamic parameters for Bitter gourd oil extraction were determined using the following equation.
\[ \frac{-\Delta G}{RT} = \frac{-\Delta H}{R} \frac{1}{T} + \frac{\Delta S}{R} \]  
- (3)

\[ k = \left( \frac{Y_f}{Y_u} \right) \]  
- (4)

Where K is the equilibrium constant; Y_f is the percent oil yield at temperature T; Y_u is the percent un-extracted oil; ∆H is the enthalpy change (kJ/mol); ∆S is the entropy change (kJ/mol.K); ∆G is the free energy or Gibb's energy (kJ/mol), R is Universal gas constant (8.314 kJ/K.mol) and T is Temperature (K). From eq 4, the plot between lnk versus 1/T gives straight line and the slope of the line gives -∆H/R and intercept gives ∆S/R. These values are used in calculating the value of ∆H, ∆S and ∆G.

3. Results and Discussion

The current work is mainly focused on study on various factors affecting the % yield of oil extraction using n-hexane as solvent.

3.1 Effect of Volume of Solvent

The effect of solvent volume was studied by keeping other variables like particle size, time of extraction and temperature as constant. The % yield of oil at different volumes of solvent was estimated and found that as the volume of solvent increased from 10 ml to 50 ml, the % yield is also increased from 15% to 27%. The maximum yield of 27% was obtained at a solvent volume of 50 ml.

3.2. Effect of Particle Size

The yield percentage of oil has increased with decreasing particle size. The experimental results shown that as the size of the particle decreased from 1.303 mm to 0.253 mm, the yield % of oil increased from 13 to 31%. Therefore, lower particle size influenced and increased the extraction % yield of Bitter gourd oil.

3.3. Effect of Temperature

The % yield of oil extracted from Bitter gourd seeds at different Temperature conditions are shown in the Fig 3.

When the temperature was increased from 343 K to 368 K, the % yield also increases accordingly from 26.5% to 52.1%. The % yield of bitter gourd oil increased up to 358 K, after that there is no remarkable increase and the % yield of bitter gourd oil remains nearly constant. In this study, a maximum value of 52.1% of oil yield was obtained at a temperature of 368 K.

3.4. Effect of Extraction Time

The yield of oil increased with time as the extraction process was carried out at a constant temperature of 308K (ambient temperature) and with 50 ml of solvent. The processing time is varied between 30 to 150 min with an interval of 30 min. The plot between % yield and time showed that the % oil yield increases with time. The amount of extracted oil by n-hexane did not change significantly after 90 min.
maximum of 29.42% oil yield is achieved after 150 minutes of extraction.

Figure 4: Effect of time on % of yield for Bitter gourd oil extraction

3.5. Kinetic Study

The plot between ln (dY/dt) and lnY resulted in a straight line. The process of extraction of oil from Bitter gourd has displayed a fourth order kinetics as observed from the slope of the line and its intercept was used to determine the reaction rate constant as 9.433 min⁻¹.

Figure 5: A plot between ln(dY/dt) vs lnY for oil extraction

3.6. Thermodynamic Study

A plot of lnK and 1/T is as shown in Fig.6. From the slope of the plot enthalpy change (ΔH) of the process was calculated as 11.70 KJ/mol. This indicates that the process is endothermic and required energy during the extraction process. An intercept of 3.228 was obtained from which the entropy change of 0.26 KJ/mol K was calculated. The Gibbs free energy calculated at various temperatures is shown in Table 1. The negative values of Gibbs energy indicate that the process is spontaneous in nature and it is feasible.

Table 1: Equilibrium constant (K) and Gibbs free energy (ΔG) at various Temperatures

| T (K) | K (min⁻¹) | ΔG (KJ/mol.K) |
|------|-----------|---------------|
| 343  | 0.418     | -2.487        |
| 348  | 0.443     | -2.356        |
| 353  | 0.46    | -2.279        |
| 358  | 0.496     | -2.087        |
| 363  | 0.524     | -1.95         |

Figure 6: Plot between ln K vs 1/T for oil extraction

4. Conclusion

In this study n-Hexane was used for oil extraction from bitter gourd seeds. The obtained results show that there is a remarkable effect of parameters like volume of solvent, particle size, extraction time and temperature on extraction of oil. It was also observed that, a maximum oil yield of 51% was obtained at 100°C for an extraction time of 150 minutes using 15g of dried Bitter Gourd seed and 50 ml of n-hexane. The estimation of kinetic studies concluded that the bitter gourd seed oil extraction process has fourth order kinetics. The thermodynamic studies reveal that the process is endothermic and required energy, as a positive value of enthalpy change (ΔH= 11.70 kJ/mol) was obtained. The positive value of entropy change (ΔS= 0.26 kJ/ mol K) indicates that the process is irreversible and it can be inferred that the process is feasible and spontaneous in nature as Gibbs energy at various temperatures was negative.

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