APPLICATION OF RESPONSE SURFACE METHODOLOGY TO ENHANCEMENT OF BIOMASS PRODUCTION BY LACTOBACILLUS RHAMNOSUS E/N

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ABSTRACT

Response surface methodology (RSM) was employed to study the effects of various medium components on biomass production by Lactobacillus rhamnosus E/N. This strain is commonly used in the pharmaceutical and food industries due to its beneficial effect on the human gut and general health. The best medium composition derived from RSM regression was (in g/l) glucose 15.44, sodium pyruvate 3.92, meat extract 8.0, potassium phosphate 1.88, sodium acetate 4.7, and ammonium citrate 1.88. With this medium composition biomass production was 23 g/l of dry cell weight after 18 h of cultivation in bioreactor conditions, whereas on MRS the yield of biomass was 21 g/l of dry cell weight. The cost of 1 g of biomass obtained on MRS broth was calculated at the level of 0.44 € whereas on the new optimal medium it was 25% lower. It may be concluded then, that the new medium, being cheaper than the control MRS allows large scale commercial cultivation of the L. rhamnosus strain. This study is of relevance to food industry because the possibility to obtain high yield of bacterial biomass is necessary step in manufacturing of probiotic food.

Key words: response surface methodology, Lactobacillus rhamnosus, medium selection, biomass production.

INTRODUCTION

Lactobacilli are members of the heterogeneous group of lactic acid bacteria (LAB) and many of them are used as probiotics. The main reason for the choice of these bacteria are their documented health benefits (11, 10). By competing for adhesion sites and nutrients and producing antimicrobial substances, lactobacilli can decrease the levels of potentially pathogenic bacteria. Establishment of pathogens in the gastrointestinal tract is connected with the mechanism of biosynthesis of inhibitory substances. Another benefit from diet supplementation with probiotics is immunomodulation (9). Probiotics play a regulatory role in allergic diseases (20). Lactic acid bacteria contribute to relief of lactose intolerance symptoms. It has also been reported that probiotic LAB reduce LDL-cholesterol and are successfully used in the treatment and prevention of colorectal cancer (14).

Strains of Lactobacillus rhamnosus due to their probiotic benefits, are widely used in the pharmaceutical and food industries.
activity, have been increasingly applied in food supplements and novel pharmaceutical products. *L. rhamnosus* has been for many years added to new generation fermented food such as bioyoghurts (15). This strain was also used as a probiotic culture in ice cream and cheese manufacture (4, 6, 25), and was applied to fresh-cut apple wedges or to fruit juices for their fortification as an alternative probiotic food choice for consumers intolerant to dairy products (23, 26). These strains are resistant to commonly used antibiotics, which is a good reason for their use simultaneously with antibiotic therapy (24). For those reasons, the possibility of cheap and fast cultivation of lactobacilli is gaining in importance. The growth activity of this genus is strictly connected with medium formulation because lactic acid bacteria are fastidious in their nutrient requirements (1).

Response surface methodology (RSM) can be used to evaluate the relative significance of several factors in the presence of complex interactions. It is a powerful technique for testing multiple-process variables because fewer experimental trials are needed as compared with the study of one variable at a time. RSM answers the question of how to select the levels for the applied factors to obtain the desirable, smallest or largest, value of the response function in a reduced number of experiments (12). This technique includes primary screening of variables by the application of “one variable at a time” method or Plackett-Burman design (27, 21) as well as using a design for fitting the chosen model (19). The most popular approach is based on full factorial central composite design (CCD), which enables one to estimate the coefficients of a second-order model.

In the present work, we used RSM to examine the effect of various carbon and complex nitrogen sources as well as growth factors in media on the yield of biomass of the probiotic strain *L. rhamnosus* E/N. The aim of our study was to choose the best carbon and nitrogen sources and to compose a cheap medium for effective biomass concentration of *L. rhamnosus* E/N.

### MATERIALS AND METHODS

**Strain and culture condition**

*Lactobacillus rhamnosus* strain E/N obtained from Biomed Serum and Vaccine Production Plant Ltd. in Lublin (Poland) was used in all experiments. The bacteria were stored at -80°C in MRS medium with an addition of 20% (v/v) glycerol. The strain was revitalized in MRS broth (BTL, Poland) at 37°C for 24h before use.

Different sources of carbon were tested for their influence on the growth of *Lactobacillus*. They included glucose (POCH, Poland), glucose with sodium pyruvate (Sigma) or with sodium lactate (Sigma) or with ammonium citrate (POCH, Poland), galactose (POCH, Poland), fructose (POCH, Poland), lactose (POCH, Poland), sucrose (POCH, Poland), maltose (POCH, Poland), lactulose (ICN), fructooligosaccharides (Arnaut), and maltodextrins DP 4-7 and 13-17 (Sigma). The MRS medium containing each carbon source separately at a concentration of 20 g/l and pH 6.2 was distributed into tubes and sterilized at 121°C for 15 min. The media were complemented with multiple carbon sources according to Bajpai-Dikshit et al. (3).

The effect of the optimal concentration of a complex source of nitrogen was examined in modified MRS broth, in which yeast extract, meat extract and pepton K were used at different concentrations (Table 1). The media prepared in tubes were pasteurized in a Koch apparatus (100°C) for 20 min.

| Dilutions of nitrogen sources in relation to MRS broth | Yeast extract | Meat extract | Pepton K |
|--------------------------------------------------------|---------------|--------------|----------|
| 10x                                                    | 0.40          | 0.80         | 1.0      |
| 25x                                                    | 0.16          | 0.32         | 0.4      |
| 50x                                                    | 0.08          | 0.16         | 0.2      |
| 75x                                                    | 0.05          | 0.11         | 0.13     |
| 100x                                                   | 0.04          | 0.08         | 0.10     |
| 500x                                                   | 0.01          | 0.02         | 0.02     |
The effect of amino acids and vitamins from B group on bacterial growth was also investigated. The modified MRS medium containing 100 times lower concentrations of complex nitrogen sources was supplemented with the L form of amino acids (Pro, Ser, Val, Leu, Ile, His, Trp, Tyr, Thr, Met, Glu, and Phe) at a concentration of 0.1 mg/ml or with vitamins (biotin, folic acid, nicotinic acid, pantothenic acid, pyridoxal, riboflavin, thiamine, and cyanocobalamine) at a concentration of 0.001 mg/ml. The vitamin solutions were filter-sterilized and added to the pasteurized cultivation medium in tubes prior to inoculation.

A revitalized culture of \textit{L. rhamnosus} E/N was used to prepare 24 h inocula in MRS medium, pH 6.3 ± 0.1. Each kind of medium in tubes was inoculated with bacteria at a concentration of 2.5% (v/v), and the cultures were incubated at 37°C for 24-48 h in relatively anaerobic conditions. Every 2 h, samples were collected from the stationary cultures, and an analysis of optical density (OD) was carried out. OD was measured at 600 nm using a Biorad spectrophotometer. Biomass concentration was determined using a standard curve of OD$_{600}$ against dry cell weight.

**RSM experimental design**

Plackett-Burman design was used in order to limit the number of the studied variables by choosing the media which influenced the biomass value to the largest extent. The results of the analysis of this design are presented in the form of a Pareto chart.

Central composite design was chosen to estimate the response calculated according to the following form of a second degree polynomial equation (7):

\[
Y = \beta_0 + \sum \beta_i X_i + \sum \beta_{ii} X_i^2 + \sum \beta_{ij} X_i X_j
\]  

where $Y$ is the predicted response variable, $\beta_0$ is the interception, $\beta_i$ are linear coefficients, $\beta_{ii}$ are quadratic coefficients, and $\beta_{ij}$ are coefficients of the interaction. $X_i$ and $X_j$ represent the chosen independent variables.

Each variable was set at a low and a high level. The low level was fixed far from the high one in order to differentiate the influence of the media on the biomass production. As a consequence, the minimum value obtained as a star point was set at zero (21).

The results of the analysis of this design were expressed in terms of polynomial coefficients, and the significance of the model was verified by applying the ANOVA analysis. Additionally $R$ and $R^2$ values were calculated to measure the goodness of fit of this regression model. The relationships between response value and the chosen media were represented in the form of 3D response surface plots.

Statistica version 7 (StatSoft, USA) was used to generate design matrices and plots as well as to calculate the results of the analyses.

**Verification of the statistical model in stationary and bioreactor conditions**

On the basis of the results obtained from statistical analysis, the optimal medium was composed. After pasteurization at 100°C for 20 min, tubes were inoculated with the \textit{Lactobacillus} strain at a concentration of 2.5% (v/v). Incubation continued at 37°C for 24 h. Then, samples were collected to determine biomass concentration. The experiments were done in triplicate. The culture of \textit{Lactobacillus rhamnosus} E/N was also run in the same medium in a bioreactor (Biostat, Sartorius, Germany). Four pH values were tested: 6.3 (as a control), 4.5, 5.0, and 5.5. The working volume was 500 ml in a 1 l vessel with stirring (100 rpm). Rods were incubated at 37°C for 24 h in relatively anaerobic conditions. Samples of the culture were examined for biomass concentration using OD$_{600}$ analysis.

**RESULTS**

**Preliminary tests**

First, screening experiments were performed to evaluate the efficacy of the different kinds of carbon sources on the
yields of biomass of \textit{L. rhamnosus} E/N. Among the examined monosaccharides, glucose and galactose gave promising results at biomass production levels of 15.1 and 18.2 g/l dry cell weight (d.c.w), respectively. Lactose was the only disaccharide suitable for high biomass production (20.0 g/l d.c.w). The best results were obtained when glucose was used simultaneously with pyruvate or lactate, or citrate, giving biomass concentrations of 25.6 g/l, 24.8 g/l, and 21.0 g/l, respectively (Fig. 1). Glucose + pyruvate were chosen as a carbon source for further experiments.

The optimal concentration of complex nitrogen sources, mineral and organic salts for the growth of \textit{L. rhamnosus} E/N was estimated at the level of 0.22 g/l, which corresponds to the 100x dilution of nitrogen sources in relation to MRS broth. Any positive effect on bacterial growth was not observed after amino acids supplementation at the level of 0.1 mg/ml. The analyzed vitamins did not sufficiently influence the growth of the examined bacteria when they were added to the medium at a concentration of 0.001 mg/ml. The data obtained were used in the design of a response surface methodology.

\begin{figure}[h]
\centering
\includegraphics[width=\textwidth]{figure1.png}
\caption{Effect of various carbon sources on the growth of \textit{L. rhamnosus} E/N after 24 h of incubation.}
\end{figure}

\textbf{Central composite design}

Variables such as glucose + pyruvate ($X_1$), meat extract ($X_2$) as well as organic and inorganic salts ($X_3$) were chosen for further studies on the basis of the results of the analysis of Plackett-Burman design (Table 2), which are presented in the Pareto chart (Figure 2) as the absolute values of effect estimates. The increase in the values for these media influenced biomass production the most, compared to the other media. $X_1$, $X_2$ and $X_3$ were used as independent variables in the $2^3$ full factorial central composite design containing low and high levels of variables, six star points with $\alpha=\pm 1.68$ and the same number of replicates at centre points (Table 3).

The following regression function describing the relationships between the chosen media and biomass
production was obtained as a result of CCD analysis:

\[ Y = -1.24379 + 0.96775 X_1 - 0.03680 X_1^2 + 1.62525 X_2 - 0.11784 X_2^2 + 0.39791 X_3 - 0.03009 X_3^2 + 0.06152 X_1X_2 - 0.00465 X_1X_3 + 0.02464 X_2X_3 \]

(2)

The results of ANOVA for the current model indicated its high statistical significance (Tab. 4). The goodness of fit of the model was checked by the correlation coefficient \( R^2 = 0.955008 \) and the determination coefficient \( R^2 = 0.91204 \), the high values of which confirmed the high agreement between the experimental and the predicted values as well as the high percentage of total variations explained by this model.

The relationship between the independent variables and the response is presented in a graphical form in Figures 3-5. The three-dimensional response surface plots illustrate the interactive effects of the media on biomass production. The optimum medium composition for the growth of \( L. \ rhamnosus \) E/N is as follows: glucose 15.44 g/l, sodium pyruvate (3.92 g/l), meat extract (8.0 g/l), potassium phosphate (1.88 g/l), sodium acetate (4.7 g/l), and ammonium citrate (1.88 g/l).

Table 2. Plackett-Burman design for seven variables

| Run | Glucose + pyruvate | Pepton K | Meat extract | Yeast extract | Organic and inorganic salts | Microelements | NaCl | Biomass (g/l) |
|-----|-------------------|---------|--------------|----------------|-----------------------------|---------------|------|--------------|
| 1   | -1\(^{a}\)        | -1      | -1           | 1              | 1                           | 1             | -1   | 4.2139       |
| 2   | 1                 | -1      | -1           | -1             | -1                          | 1             | 1    | 6.1327       |
| 3   | -1                | 1       | -1           | -1             | -1                          | 1             | -1   | 1.1805       |
| 4   | 1                 | 1       | -1           | 1              | -1                          | -1            | -1   | 12.099       |
| 5   | -1                | -1      | 1            | 1              | -1                          | -1            | 1    | 2.5366       |
| 6   | 1                 | -1      | 1            | -1             | 1                           | -1            | -1   | 22.085       |
| 7   | -1                | 1       | 1            | -1             | 1                           | -1            | 1    | 3.1762       |
| 8   | 1                 | 1       | 1            | 1              | 1                           | 1             | 1    | 25.413       |

\(^{a}\) Code levels (g/l)

| Independent variables | -1 | +1 |
|-----------------------|----|----|
| Glucose + pyruvate    | 0.8| 20 |
| Pepton K              | 0.2| 10 |
| Meat extract          | 0.16| 8  |
| Yeast extract         | 0.08| 4  |
| Organic and inorganic salts | 0.9| 9  |
| Microelements         | 0.02| 0.24|
| NaCl                  | 0| 30 |

Figure 2. Pareto chart - a ranking of variables investigated in the Plackett-Burman design.
Table 3. Central composite design matrix with values of biomass

| Glucose + pyruvate (X₁) (g/l) | Meat extract (X₂) (g/l) | Organic and inorganic salts (X₃) (g/l) | Biomass (g/l) |
|-------------------------------|------------------------|----------------------------------------|--------------|
| 0.8                           | 0.16                   | 0.9                                    | 1.7988       |
| 0.8                           | 0.16                   | 9                                      | 2.1465       |
| 0.8                           | 8                      | 0.9                                    | 5.6417       |
| 0.8                           | 8                      | 9                                      | 6.9501       |
| 20                            | 0.16                   | 0.9                                    | 4.2113       |
| 20                            | 0.16                   | 9                                      | 3.2319       |
| 20                            | 8                      | 0.9                                    | 16.711       |
| 20                            | 8                      | 9                                      | 17.900       |
| 0                             | 4.08                   | 4.95                                   | 2.5101       |
| 26.528                        | 4.08                   | 4.95                                   | 13.749       |
| 10.4                          | 0                      | 4.95                                   | 2.2288       |
| 10.4                          | 10.665                 | 4.95                                   | 20.9442      |
| 10.4                          | 4.08                   | 0                                      | 12.0005      |
| 10.4                          | 4.08                   | 11.754                                 | 14.9889      |
| 10.4                          | 4.08                   | 4.95                                   | 14.4713      |
| 10.4                          | 4.08                   | 4.95                                   | 14.3758      |
| 10.4                          | 4.08                   | 4.95                                   | 13.8185      |
| 10.4                          | 4.08                   | 4.95                                   | 14.5509      |
| 10.4                          | 4.08                   | 4.95                                   | 13.8822      |
| 10.4                          | 4.08                   | 4.95                                   | 14.0892      |

Table 4. Analysis of variance for the current regression model

| Source of variation | Sum of square | Degree of freedom | Mean Square | F-Value | p-Value  |
|---------------------|---------------|-------------------|-------------|---------|----------|
| Model               | 660.5372      | 9                 | 73.39302    | 11.52083| 0.000345 |
| Error               | 63.70465      | 10                | 6.370465    |         |          |

Figure 3. Influence of the interaction between glucose + pyruvate (X₁) and meat extract (X₂) on the biomass production (Y), with organic and inorganic salts (X₃) at their center point level.
Verification of the model in a bioreactor

The yield of biomass obtained under bioreactor conditions was in agreement with the results from the stationary culture. Our results show that the maintenance of pH at a constant level is important for biomass production by \textit{L. rhamnosus} E/N. When pH value was maintained at the level of 5.0, the highest yield of \textit{Lactobacillus} biomass was obtained on the optimal medium. After 24 h of cultivation dry cell weight was 24 g/l (Fig. 6).

\textbf{Figure 4.} Influence of the interaction between glucose + pyruvate ($X_1$) and organic and inorganic salts ($X_3$) on the biomass production ($Y$), with meat extract ($X_2$) at its center point level.

\textbf{Figure 5.} Influence of the meat extract ($X_2$) and organic and inorganic salts ($X_3$) on biomass production ($Y$), with glucose + pyruvate ($X_1$) at its center point level.
DISCUSSION

The yields of biomass of *L. rhamnosus* E/N after 24-h culture in MRS containing different carbon sources are shown in Figure 1. The results demonstrate that mixtures of glucose with salts of organic acids were optimal complex carbon sources for the growth of the examined strain. However, the best growth was observed when sodium pyruvate was added. In this case bacteria achieved stationary phase after six hours of incubation whereas in media containing other carbon sources this state was achieved after 16 – 18 h. Our observation is in agreement with the findings of other researchers. As regards the effect of carbohydrates, Mataragas et al. (18) reported that glucose concentration did not improve the total biomass produced by *Leuconostoc mesenteroides* and *Lactobacillus curvatus*, whereas Liew et al. (16) showed a slight effect of glucose on the cell number of *Lactobacillus rhamnosus*. Bajpaj-Dikshit et al. (3) reported that *L. rhamnosus* increased the maximum growth rate nearly 1.4-fold when it co-metabolized sodium pyruvate with glucose. It appears that among the various carbon sources studied, the yield of biomass was mostly influenced by the increase in the concentration of glucose + sodium pyruvate which is the preferred substrate for the growth of *L. rhamnosus*.

Meat extract had a great positive effect on the growth of the examined bacteria, whereas the effect of yeast extract, and pepton K was slight and similar. We took into consideration the fact that meat extract contains a larger amount of total nitrogen (12% w/v) than YE (10% w/v) (8) and the fact that some authors recommended adding ammonium salts (13, 29) and citrate (2) into the medium as they increased the yield of biomass production, so meat extract and organic and inorganic salts (potassium phosphate, sodium acetate, and ammonium citrate) were selected for further analysis.

An increase in NaCl and, to a lesser extend, microelements had a negative effect on biomass production.

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**Figure 6.** Growth of *L. rhamnosus* E/N in the optimal medium (pH 4.5, pH 5.0, pH 5.5) in comparison with the MRS medium (pH 6.3) in bioreactor conditions.
The shapes of the response surface plots presented in Figures 3-5 provide some information about the interactions among the studied media (7). The nearly circular nature of the shape in Figure 3 points to no interaction between glucose + pyruvate and meat extract, while the rest of the shapes (Figures 4-5) presenting ellipses indicate a strong interaction among organic and inorganic salts and the other studied medium components. It can also be noticed that the changes in glucose + pyruvate and meat extract concentrations affected biomass production much more than changes in the concentrations of organic and inorganic salts.

The search for the optimum (maximum) value of the response was limited to the low-high interval of the studied media. For such assumptions the following values were calculated: \( X_1 = 19.36 \), \( X_2 = 8 \), \( X_3 = 8.46 \) with the corresponding \( Y = 20.805 \).

Our experiments indicate that increasing the scale of the biomass production of \( L. \) rhamnosus E/N requires maintaining a constant pH of the medium at the level 5.0. This result could be explained by differences in lactate concentration in the culture medium and in pH gradient value. The elevated content of the ionic lactate form at high pH values damaged membrane integrity which lead to decrease in viability. In contrast, the high pH gradient observed throughout pH 5 cultures was associated with an enhanced energetic level, which helped the cells maintain their physiological state (22). Our results are consistent with those reported by Rault et al. (22). Such results may be of benefit to industrial starter producers and fermented-product manufacturers by allowing them to better control the quality of their starters.

With the optimal medium composition biomass concentration was 23 g/l of dry cell weight after 18 h of incubation in bioreactor culture. The yield presented here is not very impressive compared with the control MRS medium (22.5 g/l), but in the control, after 18 h of incubation, bacterial growth decreased whereas in the optimal medium the growth curve was sloping upward. Many reports on the production of \( L. \) rhamnosus biomass (5, 17, 28) describe yields which are generally lower than 15 g/l. The biomass yield in our experiment was significantly higher because of the application of a mixed carbon source (glucose + pyruvate) and a constant pH level of 5.0.

The analysis of costs indicates that the price of 1 l of the optimal medium is 7.54 € and the price of 1 g of biomass produced using this medium is at the level of 0.33 €. Considering the cost of the control MRS medium (9.92 €), it may be concluded that the new medium can not only be successfully used for effective biomass production by \( L. \) rhamnosus E/N, but can also significantly lower the costs of this production. The final yield and costs were compared with results of other authors (5, 28). They reported a growth yield of 4.0 g/l dry cell weight for \( L. \) rhamnosus grown for 26 hours on a defined medium costing 33.34 €/l (28) or 10.50 g/l costing 56.76 €/l (5).

In view of the above, the lower costs of the new, optimal medium developed in this study and the high biomass concentration of the examined Lactobacillus strain grown on this medium could be of potential practical value to industry.

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