Study of the Tableting Properties of MCR, a Newly Coprocessed Cellulose-based Direct Compression Excipient

Yeni Koproses Selüloz Bazlı Doğrudan Basım Yardımcı Maddesi Olan MCR’nin Tabletleme Özelliklerinin İncelenmesi

ÖZ

Amaç: Bu çalışmada, lokal olarak ekstrakte edilmiş mikrokristal selülozdan ve rejenerasyonu ile elde edilmiş yeni selüloz bazlı doğrudan basım tabletleme yardımcı maddesini (MCR) koprosesini ve değerlendirilmesi amaçlandı.

Gereç ve Yöntemler: Serbest akmayan ve dolaylı olarak sıkıştırılabilir bir aktif farmasötik bileşen modeli olarak metronidazolın (MZ) model tablet formülasyonları, MCR’nin tabletleme özellikleri için kullanılmaktadır.

Bulgular: Kabul edilen ağız özellikleri ve yüksek sıkıştırma özellikleri ile yardımcı maddesi (CRC) konsantrasyonunun, %20 (a/a) olduğu gözlem görmüştü. MCR, bileşenlerin tek başına veya basit bir ikili karışım içerisinde olduğunda iyi performans göstermiş, MCR ile geliştirilmiş mekanik özellikleri ve hızlı dağılama ve çözünme hızı, sahip olan MZ tabletleri basılcısa.

Sonuç: Kırma dayanımı (H) ve dağılma hız sabitleri (k_d), %50 a/a MCR ile yapılan tabletler için sırasıyla 3.76 dan 11.08 kg’a ve 0.92ден 13.1×10^{-3}s^{-1}e yükselmiştir. Belirli bir MZ tablet partisinin hem H hem de k_d’sinin, verilen partideki yardımcı maddenin içinde mevcut olan toplam bağlanma bölgesi sayısının (α) fonksiyonu olduğu bulunmuştur. MCR ne yazık ki magnezyum stearate karşı duyarlıdı. Elde edilen sonuç, MCR’in başarılı bir tamamlayıcı doğrudan basım yardımcı maddesi olduğunu ortaya koymuştur.

Anahtar kelimeler: Mikrokristal selüloz, rejenerasyon selüloz, MCR koproses, MCR tabletleme özelliği

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INTRODUCTION

The coprocessing technique has been utilized to develop excipients of improved and/or desired functionalities. The technique is defined as the concept of two or more excipients interacting physically at the subparticle level to provide a synergy of functionality and improvements as well as masking the undesirable properties of individual excipients. It provides a broad platform for the manipulation of excipient functionality or particle engineering of two or more existing excipients. Silicified microcrystalline cellulose (MCC) (Prosolve), Cellactose, and Avicel CE-15 are commercially available coprocessed excipients that have improved flow and consolidation properties. Controlling particle size and particle-size distribution as coprocessing means were used to produce excipients of improved flow with no need to add glidants. However, cases of some coprocessed powders with enhanced mechanical properties but having similar particle-size distribution of the parent powders were reported.

One of the major limitations challenging the coprocessing technique is the fixed ratio of the excipients in a coprocessed mixture, which may not be an optimum choice for the active ingredient(s) and the dose for a formulation under development. MCC tableting properties are close to optimal. The excipient has high degrees of compressibility and compactibility, and high dilution potential. However, the bad flow properties and the sensitivity to magnesium stearate (MS) are the main drawbacks of this excipient. Cellulose regenerated (RC) from microfibril showed high physicochemical and tableting properties. Ahmad reported that RC has glidant activity. Rojas et al. found that RC has strong disintegration activity. Due to its large specific surface area, RC was successfully employed with olive oil to produce Dis-Lub-Tout, a newly coprocessed tablet excipient of bifunctional activity.

Metronidazole (MZ) is an antimicrobial agent effective against anaerobic bacteria and protozoa. It is primarily used to treat bacterial vaginosis, pelvic inflammatory disease, wounds, intraabdominal infections, trichomoniasis, and infections caused by susceptible anaerobic organisms. Tablets are commonly used dosage form of this drug. Trials were conducted to coprocess excipients to manufacture direct compression MZ tablets.

Our objective in this work was to coprocess and evaluate the tableting properties of cellulose-based direct compression tableting excipient (MCR), a new cellulose-based tableted excipient produced from the granules of colloidal microcrystalline cellulose (CMCC)/regenerated cellulose (CRC) slugs. MCR was locally extracted from the dried leaves and hollow stems of the common reed plant (Phragmites australis (Grassinae)) and was used to prepare CRC. Metronidazole, a model of nonfreely flowing incompressible active pharmaceutical ingredient (API) powder, was employed to evaluate the tableting properties of MCR.

MATERIALS AND METHODS

Materials

Dried leaves and hollow stems of the common reed plant were collected from different areas near water resources and sewages in the town of Assiut (upper Egypt) at harvest time (March-June). Analytical-grade chemicals, namely absolute ethanol and sodium hydroxide pellets given by Krishna Chemicals, Mumbai-40078, Maharashtra, and 98% sulfuric acid obtained from Scharalab, S.L., Gato Prez, Spain, were used in this investigation. Metronidazole (Provizer Pharma, India), a model of nonfreely flowing incompressible API, and MS, the commonly used tablet lubricant (Scharalab, S.L., Gato Prez, Spain), were employed in this investigation.

Methods

CMCC and CRC processing

The collected plant material was thoroughly examined and the decayed parts were discarded. The selected parts were thoroughly washed, dried, and ground using a suitable grinder. A 500-g sample of the powdered plant material was boiled in 2% sulfuric acid for 2 h to destroy the lignin content in order to separate the cellulose fibers. The acid and the acid soluble materials were filtered out and the collected solid material was washed to remove the acid, neutralized, and boiled in 12% sodium hydroxide solution for 4 h to completely get rid of the lignin. The solid material was thoroughly washed to remove the alkali, neutralized, and subjected to acid hydrolysis by boiling in 3 L of 10% sulfuric acid solution for 3 h to produce CMCC. The yield was thoroughly washed to remove the acid, neutralized, and bleached by boiling in 3 L of 6% sodium hypochlorite for 2 h. The CMCC was thoroughly washed with distilled water, neutralized, dried, pulverized, and stored in a screw-capped brown powder bottle until use. A 100-g sample of CMCC was suspended in 300 mL of 20% sodium hydroxide solution. The suspension was frozen at -28°C for 12 h to dissolve the cellulose. The frozen cellulose solution was kept at room temperature (25±2°C) for 18 h. CRC precipitated with 1 N sulfuric acid solution was thoroughly washed with distilled water, neutralized, dried, pulverized, and stored at room temperature (25±2°C) in screw-capped brown powder bottles until use.

Infrared characterization of cellulose powders

The infrared (IR) spectra of authentic MCC sample and samples of CMCC and CRC powders were run using the technique described by Rojas et al. In this technique, 1 mg of a given sample was mixed with 100 mg of KBr in an agate mortar. Pellets of this mixture were prepared on a portable press (CrushIR Digital Hydraulic Press 161-1900, PIKE, Madison, WI, USA) at a dwell time of 5 min and at a force of 4540 kg. The infrared spectra were run between 650 and 4000 cm⁻¹ using a PerkinElmer IR spectrometer (Spectrum BX, PerkinElmer, San Jose, CA, USA) equipped with the software Omnic (Nicolet Corp., Madison, WI, USA). The resolution and interval length were 16 and 2 cm⁻¹, respectively, and the number of scans employed was 16 cm⁻¹.
Physical properties of cellulose and MZ powders

Particle shape and effective mean particle diameter
The shapes of CMCC and CRC particles were characterized by scanning electron microscopy (SEM) (BM-180, Bo-eco, GmbH, Frankfurt, Germany) attached to a digital camera (S8000fd, Fujifilm Corp., Japan). A suitable volume of the given powder sample was mounted in the specimen stub of the SEM for microphotographing (no sputtering was noticed). The effective mean diameters of CMCC and MZ particles were determined by the sieving technique using a set of stainless steel sieves (Fritsch, GmbH, FRG) arranged in descending order as described earlier. The effective mean diameter of CRC particles was determined using a size analyzer (Brookhaven Instruments Corp., Holtsville, NY, USA) equipped with default particle sizing software (ver. 3.74). A sample of dilute CRC/water suspension was used for the test. The refractive index of the sample was 1.33, while the beam angle and the wavelength were 90° and 678 nm, respectively.

Flow properties, density, and moisture content determinations of powders
The funnel technique was employed to determine the volumetric flow rates and repose angles of the powders under investigation. The apparent density, \( \rho_a \), of a given powder was determined using the liquid displacement technique. The bulk, \( \rho_b \), and tap, \( \rho_t \), densities and packing fraction, \( \varphi_f \), were determined using earlier reported techniques. The mean of five determinations of each experiment was calculated and taken as the determined value. The moisture content (dry weight basis) was determined by drying technique as described earlier.

Moisture sorption isotherm study
The moisture sorption isotherm exhibited by MCR was studied and compared with that of the parent components. For the test, accurately weighed 1-g samples of MCR CRC, and CMCC were stored on a shelf in ambient conditions (25±2°C - relative humidity (RH) 45±2%) and at 40°C - RH 75%. The RH% conditions were achieved using a saturated solution of sodium chloride. A Gallenkamp humidity oven (Gallenkamp, London, United Kingdom) was employed for the test. At a predetermined time interval, a sample of a stored powder was evaluated for the amount of adsorbed moisture (dry weight basis).

Swelling index and hydration capacity determinations
The swelling index (SI) of a given cellulose powder was determined as follows: an accurately weighed 1-g sample of the given cellulose powder was suspended in 25 mL of distilled water and vigorously shaken at 10-min time intervals for 1 h. The suspension was equilibrated for 24 h and the volume occupied by the powder under the test was precisely determined. SI was calculated from: SI= \( \frac{v-v_0}{v_0} \times 100 \), where \( v \) and \( v_0 \) stand for the volumes of the test powder sample before and after the test, respectively. The mean of such 5 determinations was taken as the SI of the given powder. The hydration capacity (HC) of a given cellulose powder was measured as follows: a 2-g sample of a given powder was suspended in 10 mL of distilled water in a centrifuge tube and shaken intermittently for 2 h. The tube was left to stand for 30 min and centrifuged at 3000 rpm for 10 min. HC was calculated from the weight (w) of the powder before the test as HC= \( w-2/2\times100 \) as reported earlier. The mean of 5 such determinations was taken as the HC of the given powder.

MCR coprocessing
Binary mixtures of CMCC/CRC containing varying portions of CRC were prepared using a laboratory assembled 0.75-kg capacity drum mixer. The preliminary tests carried out showed that the optimum concentration of CRC needed to produce a mixture of improved flow properties (flow rate and repose angle) was 20% w/w (1 part CRC to 4 parts CMCC). A batch of 500 g of this physical mixture was prepared and employed to coprocess MCR as follows. The mixture was placed into a porcelain mortar of suitable capacity and kneaded with a sufficient volume (400 mL) of absolute ethanol. The damp mass was forced through a 350-\( \mu \)-mesh sieve and the resulting granules were dried at 50°C for 6 h using a Binder oven (FRG). The granules were placed on a tray and put into the oven. The obtained dried granules were equilibrated at room conditions for 24 h. Although the fourier-transform infrared spectroscopy technique to test for the residual alcohol in pharmaceutical solids is limited by the high detection limit (above 100 ppm), it was decided to employ it using the above-mentioned method and equipment to test for residual alcohol in the prepared granules since the allowed limit for residual ethanol in pharmaceutical solids is high (5000 ppm). The IR spectrum run showed that the produced granules were alcohol-free. The produced granules were compressed into large slugs using a single punch tableting machine (F3, Manesty Machines Ltd., Liverpool, UK). The machine settings were adjusted to produce slugs of 5-g mean weight and of the highest tensile strength that could be achieved. The machine was manually run and the surfaces of the punches were frequently cleaned of sticky powder. The produced slugs were crushed using a laboratory oscillating granulator and sifted through a 90-\( \mu \)-mesh sieve. The obtained MCR powder was stored at room temperature (25±2°C) in a screw-capped wide mouth brown powder bottle until use.

Characterization of MCR
The flow rate, repose angle, packing fraction, \( \varphi_f \), and density (apparent, bulk and tap) of MCR were determined using the above-mentioned techniques. The moisture content, swelling index, and hydration capacity determinations were also carried out employing the above-mentioned methods. The mean of 5 determinations of each experiment was calculated and taken as the determined value.

Formulation, compression, and evaluation of MZ tablets
A simple mixing technique was adopted to prepare MZ tablets. Tablets batches formulated with 20%, 30%, 50%, and 75% w/w of a given excipient were prepared. Lubrication was carried out just before compression. Tablets were compressed using a Manesty single punch tableting machine fitted to flat faced punches adopting the modified compression technique. The machine was adjusted to compress tablets of 250±0.05 mg
mean weight, 9.0±0.02 mm mean diameter, and of the highest crushing strength, H, and lowest friability, F, levels that could be achieved from the batch formulated with 75% w/w (the highest concentration) of a given excipient. The machine settings were kept constant throughout compressing the rest of the batches formulated with the lower concentration of the given excipient. Altogether 1000 tablets were compressed from each batch. The machine settings were readjusted whenever formulations of a new excipient were compressed. The produced tablets were evaluated for uniformity of weight and thickness, mechanical properties, (H, F, and porosity, $\varepsilon$), and disintegration times ($D_t$).

**Determination of $H$, $F$, and $D_t$ of MZ tablets**

A digital recording hardness tester, Erweka TBH-28 (Erweka, Darmstadt, Germany), was used to determine the mean crushing strength of a given MZ tablet batch. For the test, a sample of 10 tablets was randomly collected from a given batch. The tablets were individually tested for crushing strength and the mean was calculated and taken as the crushing strength of the given batch. $F$ of a given tablet batch was calculated from the relation $F = (v_i - v_o)/v_o$ where $v_i$ and $v_o$ equal the tablet volume and the true volume(s) of the powder(s) in the given tablet batch. The mean of five calculations was considered the porosity of the given tablet batch. $D_t$ of a MZ tablet batch was determined using a Roche friabilator (Erweka, Darmstadt, Germany). A sample of 20 tablets randomly collected from the given batch was brushed free of adhering dust and precisely weighed and placed into the friabilator drum. The apparatus was adjusted to revolve at 25 rpm for 4 min. At the end of the test, the tablets were rebrushed and precisely reweighed. The percent loss in weight was calculated as $F$ of the tablets. The mean of such five determinations was used as $F$ of the tested MZ tablet batch.

**Determination of $D_t$ and $k_d$ of tablets**

Neutral buffer solution of pH 7.2 was employed to carry out the disintegration and dissolution rate determination tests. This was to exclude the effect of pH of the medium on the disintegration and dissolution rates.

**Determination of $D_t$ of tablets**

A USP disintegration test apparatus (ZT 220, Erweka, Darmstadt, Germany) was employed to determine the disintegration times of the compressed tablets. A sample of 6 tablets randomly selected from a given MZ batch was used in this investigation. Each tablet was accurately weighed and placed into a disintegration tube of the apparatus. The time when the fragments of the tested tablet completely passed through the screen mesh at the base of the disintegration tube was recorded as the $D_t$. The mean of such 10 determinations was calculated as the $D_t$ of a given MZ batch.

**Study of dissolution behavior of MZ tablets**

A rotating basket USP dissolution rate test apparatus (model DT-D, Erweka, Germany) was employed to determine the dissolution rate of MZ tablets in 900 mL of 7.2 buffer solution. All the USP requirements for dissolution rate test were kept constant. The test was carried out at 37±0.5°C. A sample of 6 tablets randomly collected from a given batch was employed to carry out the test. For the test, one tablet was precisely weighed and placed into the basket of the apparatus. The revolution of the basket was adjusted to 100 rpm. At a predetermined time interval accommodated with the disintegration time of the batch under the test, a 5-mL aliquot sample was withdrawn from the dissolution chamber and was immediately substituted by an equal volume of freshly prepared dissolution medium maintained at 37±0.5°C. The amount of MZ in the withdrawn sample was determined spectrophotometrically at 340 nm with reference to a calibration curve constructed using a pure MZ sample as used in the formulation. The mean of such 6 determinations was taken as a point on the dissolution curve.

**Study of MCR sensitivity against MS**

The effects of lubrication with 1.0%, 1.5%, and 3% w/w of MS on the $H$, $F$, and $D_t$ values of the MZ tablet batch formulated with 75% w/w of MCR were studied.

**RESULTS**

**IR characterization of CMCC and CRC**

The IR spectra of MCC and CRC powders given in Figure 1 show the following characteristic vibration peaks of cellulose: 3445/cm corresponding to intramolecular OH stretching, including hydrogen bonds; 2898/cm due to CH and CH$_2$ stretching; 1650/cm corresponding to OH from absorbed water; 1430/cm due to CH$_2$ symmetric bending; 1375/cm due to CH bending; 1330/cm due to OH in-plane bending; 1161/cm due to C-O-C asymmetric stretching ($\beta$-glucosidic linkage); 1061/cm due to C-O-C asymmetric stretching (C-O-C-C stretching); and 898/cm corresponding to the asymmetric (rocking) C-O-C ($\beta$-glycosidic linkage) out-of-plane stretching vibrations. No new peaks were seen in the spectra, suggesting that CMCC and CRC are chemically similar to microcrystalline cellulose.

**Physical properties of cellulose and MZ powders**

Figure 2 shows that CMCC and CRC particles were morphologically similar. They were elongated and amorphous particles. Table 1
shows that their effective mean particle diameters were 90 and 3 μm, respectively. Such elongated particles have a tendency to intermesh and create internal resistance against the flow of the powder.

Table 1 also shows that the moisture contents and SI and HC values of the studied powders were high. Figure 3 shows that the investigated excipients exhibited more or less equal moisture sorption isotherm patterns.

**Physical properties of MZ tablets**

**Uniformity of MZ tablets**

The data in Table 2 show that more uniform MZ tablets were compressed with CRC followed by MCR and CMCC, in that order. The uniformity generally increased (estimated by the decrease in % CV) as the concentration of the excipient in an examined tablet batch increased. Powder metallurgy (PM) produced nonuniform tablets due to the segregation observed during compression.

**Mechanical properties of MZ tablets**

**Compressibility and compactibility of excipients**

The yield value obtained from the Heckel plot and the energy consumption during compression determined from the force-displacement plot are usually parameters used to measure powders’ compressibility. In this investigation since a given tablet formulation was compressed under confined machine settings, it follows that the number of sites available for bonding in a given concentration of an excipient in a formulation is the sole working parameter. In other words, the mechanical properties of the excipient in the given formulation are excipient concentration dependent factors. An excipient concentration-displacement plot was constructed (see Figure 4a) and the area under the curve (AUC) was taken as a parameter indicative of the compressibility of a studied excipient. The compressibility index, $k_r$, of an excipient in a given formulation was calculated from the relation:

$$
\varepsilon = \varepsilon^o \exp. - k_r C
$$

where $\varepsilon$ and $\varepsilon^o$ stand for the porosity fractions for compacts made from a given excipient and the lubricated drug only (control tablets batch) (see Figure 4b), respectively. On the other hand, Figure 4c was constructed to calculate the compactibility index, $k_p$, of the given excipient. It was calculated from the relation:

$$
H = H^o \exp. k_p C
$$

| Drug and excipient used | Mean part diam μm | Flow rate g s⁻¹ SD | Repose angle degree ± SD | Density (g/cm⁻³) App ± SD | Bulk ± SD | Tap ± SD | Moist contact %w/w ± SD | Packing fraction % calculated | Compressibility index % | Haussner ratio (h) | Surface area m²g⁻¹ x10⁻² calculated | Hydration capacity g/g ± SD | Swell index g/g ± SD |
|-------------------------|-------------------|---------------------|-------------------------|-------------------------|-----------|-----------|------------------------|-----------------------------|------------------------|----------------|--------------------------------------|-------------------------|------------------|
| MZ                      | 90                | 0.11 (0.03)         | 40 (2.11)               | 1.5 (0.34)              | 0.90 (0.11) | 1.30 (0.31) | 3.50 (0.34)             | 59                         | 31                     | 1.44          | 6.5                             | -                       | -                |
| CMCC                    | 90                | 0.21 (0.10)         | 42 (4.30)               | 1.50 (0.76)             | 0.91 (0.18) | 1.32 (0.52) | 4.76 (0.19)             | 61                         | 31                     | 1.45          | 8.2                             | 2.31 (0.41)             | 1.50 (0.33)      |
| CRC                     | 3                 | 1.20 (0.05)         | 38 (6.70)               | 1.52 (0.32)             | 0.28 (0.27) | 0.41 (0.13) | 6.4 (0.08)              | 18                         | 32                     | 1.46          | 132.0                           | 2.87 (0.65)             | 1.75 (0.53)     |
| MCR                     | -                 | 0.94 (0.09)         | 38 (3.92)               | 1.62 (0.18)             | 0.78 (0.20) | 1.25 (0.16) | 5.38 (0.54)             | 48                         | 38                     | 1.60          | -                              | 2.67 (0.34)             | 1.73 (0.22)     |
| PM                      | -                 | 0.52 (0.06)         | 40 (2.43)               | 1.65 (0.25)             | 0.71 (0.31) | 1.28 (0.11) | 5.11 (110)              | 43                         | 45                     | 1.64          | -                              | 2.61 (0.24)             | 1.66 (0.19)     |

SD: Standard deviation, MZ: Metronidazole, CMCC: Colloidal microcrystalline cellulose, CRC: Regenerated cellulose, MCR: Cellulose-based direct compression tableting excipient, PM: Powder metallurgy

Figure 2. Microphotographs for a) CMCC, and b) CRC

CMCC: Colloidal microcrystalline cellulose, CRC: Regenerated cellulose

Figure 3. Moisture sorption isotherm exhibited by MCR stored at O, ambient condition and at □, 40°C-75% RH

MCR: Cellulose-based direct compression tableting excipient, RH: Relative humidity
where \( H \) and \( H^0 \) represent the crushing strengths of the batches made with the given excipient and the control tablets batch, respectively. The data given in Table 3 show that more compressed formulation was produced by MCR, followed by CRC, CMCC, and PM, in that order.

Disintegration and dissolution behaviors of MZ tablets

Figure 5 shows that the disintegration rate constant, \( k_d \), generally decreased as the excipient concentration, \( C \), increased in a given tablet batch and the relation:

\[
k_d = k_d^0 \exp(xC)
\]

where \( x \) is the disintegration activity of the excipient in a given formulation, worked. The constants \( k_d^0 \) and \( k_d^0 \) stand for the disintegration rate constants of the batches made with a given excipient and the control tablets batch, respectively. The data

### Table 2. Physical properties of metronidazole tablets compressed directly with increasing concentrations of the named cellulose excipients

| Excipient used | Concentration % w/w | Weight (g) | CV % | Thickness (cm) | CV % | Friability, (Loss % w/w) | CV % |
|---------------|----------------------|------------|------|---------------|------|--------------------------|------|
|               |                      | Mean       | CV % | Mean          | CV % | Mean                     | CV % |
| CMCC          | 20                   | 0.2502     | 9.1  | 0.360         | 2.4  | 0.23                     | 11.5 |
|               | 30                   | 0.2533     | 12.2 | 0.351         | 5.5  | 0.37                     | 14.2 |
|               | 50                   | 0.2603     | 16.4 | 0.343         | 3.2  | 0.41                     | 3.1  |
|               | 75                   | 0.2696     | 8.2  | 0.336         | 2.1  | 0.49                     | 1.1  |
| MCR           | 20                   | 0.2521     | 2.2  | 0.356         | 1.6  | 0.18                     | 8.1  |
|               | 30                   | 0.2576     | 6.1  | 0.341         | 12.4 | 0.25                     | 3.8  |
|               | 50                   | 0.2651     | 4.9  | 0.332         | 12.4 | 0.31                     | 1.1  |
|               | 75                   | 0.2708     | 1.5  | 0.326         | 12.4 | 0.38                     | 6.1  |
| CRC           | 20                   | 0.2517     | 4.7  | 0.362         | 6.4  | 0.18                     | 6.3  |
|               | 30                   | 0.2571     | 3.2  | 0.357         | 9.2  | 0.31                     | 3.4  |
|               | 50                   | 0.2599     | 1.3  | 0.352         | 12.6 | 0.39                     | 7.2  |
|               | 75                   | 0.2601     | 0.8  | 0.330         | 14.8 | 0.48                     | 1.9  |
| PM            | 20                   | 0.2500     | 49.2 | 0.359         | 11.6 | 0.43                     | 9.8  |
|               | 30                   | 0.2276     | 36.1 | 0.211         | 12.4 | 0.95                     | 3.8  |
|               | 50                   | 0.2151     | 14.9 | 0.212         | 12.4 | 1.91                     | 1.1  |
|               | 75                   | 0.2208     | 35.5 | 0.216         | 12.4 | 4.38                     | 6.1  |

CMCC: Colloidal microcrystalline cellulose, MCR: Cellulose-based direct compression tableting excipient, CRC: Regenerated cellulose, PM: Powder metallurgy

where \( x \) is the disintegration activity of the excipient in a given formulation, worked. The constants \( k_d^0 \) and \( k_d^0 \) stand for the disintegration rate constants of the batches made with a given excipient and the control tablets batch, respectively. The data
Table 3. Some parameters determined for the tested cellulose excipients using the mathematical expressions in the text

| Excipients used | AUC cm²×10⁻² | k_p | k_ε | x   |
|-----------------|--------------|-----|-----|-----|
| CMCC            | 1.1          | 0.61| -0.24| -0.43|
| MCR             | 2.3          | 0.69| -0.20| -0.35|
| CRC             | 1.9          | 0.59| -0.49| -0.38|
| PM              | 1.0          | 0.38| -0.46| -0.48|

CMCC: Colloidal microcrystalline cellulose, MCR: Cellulose-based direct compression tableting excipient, CRC: Regenerated cellulose, PM: Powder metallurgy, AUC: Area under the curve

Table 4. % Change in some physicochemical properties of tablets compressed with the named excipients and lubricated with different concentrations of MS

| Excipient used | % Change in H for tablets lubricated with % MS w/w | % Change in F | % Change in Dt |
|----------------|-----------------------------------------------|--------------|---------------|
|                | 1    | 2   | 3       | 1   | 2   | 3       | 1   | 2   | 3       |
| CMCC           | 11   | 14  | 23    | -18 | 20  | 43     | -30 | 27  | 53     |
| MCR            | -9   | 16  | 27    | -14 | 19  | 33     | -33 | 29  | 47     |
| CRC            | -22  | 18  | 43    | -33 | 22  | 51     | -42 | 34  | 62     |

CMCC: Colloidal microcrystalline cellulose, MCR: Cellulose-based direct compression tableting excipient, CRC: Regenerated cellulose, MS: Magnesium stearate

Figure 7. Dissolution profiles of MZ tablets compressed from ◊, CRC; □, MCR; and Δ, CMCC

MZ: Metronidazole, CRC: Regenerated cellulose, MCR: Cellulose-based direct compression tableting excipient, CMCC: Colloidal microcrystalline cellulose

in Figure 6 disclose that k_ε and x of a given excipient were functions of k_p of the given excipient. In other words, the compressibility and the disintegration activity of an excipient are excipient compatibility dependent parameters. Figure 7 shows that tablets made from CR and MCR dissolved in more or less equal rates faster than those of the tablets made from CMCC.

**MCR sensitivity against MS**

Lubrication with MS generally produced less hard and more friable and slower disintegrating tablets. These adverse effects increased as the concentration of MS in a tested tablet batch increased. The changes in H, F, and Dt of tablets lubricated with 3% w/w MS are given in Table 4.

**DISCUSSION AND CONCLUSIONS**

The IR spectra in Figure 1 indicate that the tested powders are chemically similar. No new peaks suggesting the development of new materials were seen. The differences in the shape and intensity of the peaks were due to the different crystal lattices of the tested powders.

CMCC and CRC particles were elongated and amorphous. Such particles have a tendency to intermesh and create resistance (due to interparticle friction) to the flow of the bulk powder. This explains why CMCC is not a freely flowing powder (0.21 g s⁻¹). Although the Hausner ratio (h) and the % compressibility determined for MCR were 1.6 and 38, MCR showed an improved flow rate. This is supported by the concept that the Hausner ratio and Carr’s index, which are empirically derived parameters, failed in many cases to give a reliable base to judge powder flowability. The improved flow properties of MCR may be due to the glidant effect of CRC. It seems that CRC reduced the interparticle friction of the powder and improved its flow. Since CRC had a large specific surface area wherein a large α is available, it is expected that MCR has improved compression and compaction properties and generates larger AUC, k_ε, and k_p values. α of a given excipient may be calculated as;

\[
\alpha = \frac{L . k_p \cdot \text{wt.} \cdot \Sigma (r_i / MW_i)}{6.022 \times 10^{23}}
\]

where L, wt., r_i, and MW_i stand for Avogadro’s number (6.022×10²³), the weight of the excipient in a batch, the fraction of a parent excipient used in coprocessing, and its molecular weight, respectively. CRC and MCR showed almost the same level of disintegration activity and they generated smaller x values as shown in Table 3. CRC followed by MCR produced fast dissolving tablets. This is due to the powerful disintegration effect of CRC. Incorporating a powerful disintegrant in formulating tablets would contribute to the bioresponse of the tablets. MCR was unfortunately sensitive to MS.

In response to the increasing demand for inexpensive and multifunctional excipients with minimum risk to the products, MCR was engineered from MCC and regenerated cellulose. MCR has high functionality in terms of flow and compression, good binding properties, and strong disintegrating activity. However, it is sensitive to MS and exhibits high moisture uptake and therefore it is recommend as a complementary direct compression excipient.

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