**Comparative Study between Membrane Bioreactor MBR and Rotating Biological Contactors RBC for Greywater Treatment**

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**Abstract**—Greywater is the major part of water consumption in houses. Greywater should be treated to comply with the specifications for several purposes such as toilet flush, landscaping irrigation, and agriculture. The treatment efficiency of both MBR and RBC systems was investigated by using a verified mathematical model. The simulation program GPS-X (version 6.0) was used to simulate both MBR and RBC systems. The simulation model for biological treatment for both MBR and RBC systems is based on Activated Sludge Model 1 (ASM1). The experimental data for model calibration and verification for the MBR system were taken from experimental work done at Tubitak, Marmara Research Center, Turkey ATASOY. As well as the RBC proposed model was verified also by using RBC experimental results for a pilot plant according to BABAN. The RBC pilot plant consists of three units. The first is the RBC unit, the second unit is the settling tank and the last unit is the disinfection tank. The results of the MBR plant showed that the removal efficiencies of the greywater were: 95% for COD; 95% for BODs; 96% for TKN; 92% for NH4+ and 99% for TSS. Whereas, the results of the RBC show that, The BOD efficiency removal was ranged between about 93.0 to 96.0 %, and for the total SS removal was ranged between 84.0 to 95.0 %. The MBR system provides complete nitrification and suspended solid removal. The RBC system provides less nitrification process and suspended solid removal. The effluent of the rotating biological contactors units for the greywater could be reused after filtration and disinfection with minimal cost of operation. The effluent of the membrane bioreactor unit needs only disinfection before reuse.

**Index Terms**—Membrane bioreactor, rotating biological contactors, greywater treatment, mathematical models, wastewater reuse.

I. INTRODUCTION

The polluted wastewater collecting from washing basins, showers, bathtubs, and washing machines is defined as greywater. The economical treatment choices are required to reuse the treated effluent on site. The greywater might be used for many purposes like cleaning water, toilet flushing, and landscape irrigation [1]. Many different greywater treatment plants are in operation, but a comparative review of experiences and results is still lacking [2], [3]. The strong regional and seasonal fluctuations in the quality of the produced greywater at its source make it difficult to create a binding universal treatment pattern as the best available technique [4], [5].

Many treatment options could be used including, Filtration, sedimentation as physical treatment, whereas Rotating Biological Contactors and Sequencing Batch Reactor as a biological treatment process [6], [7]. The membrane bioreactors (MBR) have been utilized as an onsite compact treatment unit. The main advantages of MBRs are to get a good quality of the treated effluent with very less bacteriologic organisms. Also, the membrane system has a high resistance to organic shock loads. The following table can be summarized the advantages and disadvantages of both MBR and RBC systems [8], [9].

| Technology | Advantages | Disadvantages |
|------------|------------|---------------|
| **RBC** | - Low operational cost | - The requirement for covering RBC units. |
|            | - Short hydraulic retention time | - Shaft bearings and mechanical drive units require frequent maintenance |
|            | - Capable of handling a variation inflows | |
|            | - Good process control | |
| **MBR** | - Good effluent quality with high hygienic standards | - Complex and costly pre-treatment of the incoming wastewater |
|            | - Reduced reactor volume and footprint | - Membrane integrity (failure detection, lifetime) |
|            | - Reduced net sludge production | |

The evaluation of both MBR and RBC systems for greywater treatment was done by using a simulation model developed for both systems based on the IWA Activated Sludge Model 1. The modular program used in this study is GPS-X which is a modular, multi-purpose modeling environment for the simulation of municipal and industrial wastewater treatment plants. GPS-X uses an advanced graphical user interface to facilitate dynamic modeling and simulation. GPS-X is also using the most recent advances in process modeling, simulation technology, graphics, and a host of productivity tools that simplify model construction, simulation, and interpretation of results.

The GPS-X program was used in the simulation process. Model verification was done by using the experimental results of two pilot plants. Once the model was validating, the model was used in different scenarios to evaluate the performance of the two treatment processes.

II. MATERIALS AND METHODS

A. Experimental Pilot Plant

1) MBR pilot plant system
The model calibration and verification for the MBR system were done based on taken experimental work done at Marmara Research Center [10]. Fig. 1 shows the schematic for the MBR experimental pilot plant. The summary of the operational parameters is shown in Table II.

![Membrane bioreactor pilot plant](image)

**Fig. 1. Membrane bioreactor pilot plant.**

| Parameter                | Greywater  |
|--------------------------|------------|
| Volume                   | 600 L      |
| Time of operation        | 50 d       |
| Influent discharge        | 800 L d⁻¹  |
| Pore size                | 0.4 μm     |
| Membrane area            | 5 m²       |
| Flux                     | 26-36 L m⁻² h⁻¹ |
| HRT                      | 18 h       |
| Cycle number             | 8 d⁻¹      |
| Time of aeration per cycle| 33 min   |
| MLSS                     | 1500 mg L⁻³ |
| Organic loading          | 0.3 kg COD m⁻³ d⁻¹ |

| TABLE II: MBR PLANT OPERATION CONDITIONS |

2) RBC pilot plant

After segregation of grey and black water from residential Buildings, Greywater was fed for the rotating biological contactors pilot plant. The greywater has collected the kitchen of the residential buildings. Fig. 2 shows the RBC pilot plant. The treated greywater from the RBC system has been disinfected by using the UV treatment process [11].

The operational conditions for the RBC system will be as follows:

- Coarse screen pore opening = 10 mm.
- Fine screen pore opening = 3 mm.
- The number of RBC discs =36, the total surface area of the discs = 16.2 m².
- Period of RBC plant operation=10 months.
- Influent discharge = 400 l/d.

![Rotating Biological Contactor pilot plant](image)

**Fig. 2. Rotating Biological Contactor pilot plant.**

The activated sludge was used to the rotating biological contactors unit to accelerate the growth of the microorganisms on the discs in the startup period. The sludge was taken from the membrane bioreactor unit which operated with greywater as influent wastewater. The related parameters to the biofilm growth (BOD₃, TKN, TSS, Turbidity, and Total coliform) were measured to confirm that the characteristics of treated effluent satisfy the international reuse regulations. Also, NH₄⁺, NO₃⁻ and Total Phosphorus were measured to control the treatment process.

According to guidelines for wastewater reuse in the EPA standards (especially for landscape irrigation, urban reuses, and toilet flushing), the BOD₃ concentration and TSS should be less than 10, 5 ppm respectively. Also, the fecal coliform should not be detected in the sample 100 cubic cm, and pH should be within the range of 6-9. Whereas, for WHO guidelines the treated greywater reuses have higher allowable values for the same parameters. Hence, the guidelines for the EPA were mainly taken in this study to assist the compliance of the treated effluent for the greywater. The influent greywater concentrations for the rotating biological contactors unit was ranged from a high, medium, and low concentrations to assist the performance of the RBC system.

B. Operation Conditions and Model Configuration

1) MBR model configuration

The MBR plant model consisted of two units, the first one is the aeration basin and the other one is the membrane unit for the physical separation of the treated effluent from the aeration tank. The layout of the MBR plant model is shown in Fig. 3. The MBR model was known as the submerged MBR system.

**Simulation model and kinetic parameters**

The MBR model includes two main parts: a kinetic module that simulates the biological reactions in the system, and a transport module throw the membrane which represents the physical system modeled to separate the treated effluent from the activated sludge. The MBR kinetic module is based on the ASM1 model. The model has 19 stoichiometric and kinetic parameters. Fractionation of raw grey water and black water to its components, as required by the kinetic module, was performed based on the findings of Dixon et al. [12]: soluble biodegradable COD 45%, particulate biodegradable COD 31%, soluble non-biodegradable COD 15% and particulate non-biodegradable COD 9%. Default values for calibration of the MBR model as kinetic parameters were used as initial values for dynamic calibration. The GPS-X program (ver. 6.0) was used as simulation software for the MBR model. Fig. 3 shows the layout for the mathematical model for the MBR system.

![MBR plant model](image)

**Fig. 3. MBR plant model.**

2) RBC model configuration and operation conditions

The RBC model was used to investigate the greywater treatment capability and performance for the RBC. The GPS-X program was used to simulate the RBC system. Fig. 4 shows the layout for the mathematical model for the RBC system. The RBC proposed treatment plant was composed of three units, the first one was the rotating biological contactors unit, the second was the settling tank and the last one was a...
disinfection unit. The model was optimized for the biological kinetic parameters for the proposed unit. Three concentrations were used as influent greywater to run the proposed rotating biological contactor system. High, medium, and low greywater concentrations were used in different scenarios to run the RBC model.

Greywater concentrations with wide ranges were used within the experimental work. High, medium, and low greywater concentrations to run the rotating biological contactors model. The experimental results were used to calibrate and validate the model.

**Rotating biological contactors pilot plant operation conditions:**
- Influent greywater discharge = 400 l/d.
- RBC unit volume = 0.2 m³.
- Area of the RBC disks = 16.2 m².
- MLSS = 2800 mg/l.
- The submerged ratio of the discs = 40%.
- The volume of the Disinfection unit = 30 l.
- Chlorination dose = 1.0 mg/l.

**C. Influent Wastewater**

The influent characteristics for the greywater for both MBR and RBC plant models were shown in Table III. The influent BOD₅ and COD are 90±5.5 mg/l and 245±12.4 mg/l respectively. The results of the raw greywater characterization show that the BOD₅/COD ratio was 0.36, which is slightly lower than the domestic wastewater. The difference can be explained by the higher concentration of soaps and detergents in greywater, which are known to be slowly biodegradable. The average ratio of COD/TKN/T-P for greywater was estimated as 100/3.7/3, which is lower for nitrogen but higher for phosphorus compared to the domestic wastewater. So the greywater contains limited nitrogen concentration and a higher phosphorus concentration.

| Parameters | Greywater (mg L⁻¹) |
|------------|--------------------|
| Ph         | 7.1±0.5            |
| T          | 22±4               |
| BOD₅       | 90±5.5             |
| COD        | 245±12.4           |
| Sol. COD   | 177±9.5            |
| TKN        | 9±1.3              |
| NH₄⁺       | 1.3±0.2            |
| T-P        | 7.3±1.3            |
| TSS        | 48±8               |
| VSS        | 39±4               |
| Grease     | <2                 |
| TDS        | 301±26             |

**III. RESULTS AND DISCUSSION**

**A. MBR Model Operation**

After the MBR model calibration, the normal operational period was 50 days of operation. A comparative study between the results of the model and experimental pilot plant was done to validate the model results. Table IV shows the summary of the results of the greywater treated effluent was shown in Table III for both the MBR model and MBR pilot plant. Fig. 5-7 show the relation between effluent BOD₅, COD, TKN with timerespectively, for both MBR model and MBR pilot plant. The BOD₅ and COD removal efficiency for the MBR model was 96% and 96% respectively. Whereas, the removal efficiency of total nitrogen TKN and ammonia nitrogen NH₄⁺ for the MBR model were 96% and 92% respectively. Also, the total suspended solid TSS removal efficiency was more than 99%.

The results of the model showed that the treated effluent of greywater has complied with international reuse criteria for different purposes. Fig. 5 and 6 showed an increase of effluent organic matter in the first 3 days of operation due to the start-up period of the MBR plant. After that, due to steady-state operation, the effluent organic matter was decreased again up to a certain limit. Fig. 7 shows the effluent total nitrogen TKN was increased during the start-up period. Although, the results showed that complete nitrification and denitrification were not achieved by the MBR plant but the effluent quality of greywater was found to be satisfactory with the all household usages purposes and toilet flushing that not need potable water quality. Table IV shows a comparison between the effluent characteristics for both the MBR model and experimental data.

**TABLE IV: EFFLUENT CHARACTERISTICS FOR MBR SYSTEMS**

| Parameters        | Raw Greywater (mg L⁻¹) | Effluent (mg L⁻¹) | Removal eff. % |
|-------------------|------------------------|-------------------|---------------|
|                   | MBR Model              | MBR Pilot Plant   | MBR Model     | MBR Pilot Plant |
| BOD₅              | 90±5.5                 | 3.8±0.2           | 4.5±0.3       | 95.8±0.2       | 95.0±0.3       |
| Total COD         | 245±12.4               | 10.5±9.0          | 13.1±1.2      | 95.7±0.4       | 94.7±0.5       |
| TKN               | 9±1.3                  | 0.4±0.1           | 0.5±0.14      | 95.6±1.1       | 93.9±1.6       |
| NH₄⁺              | 1.3±0.2                | 0.1±0.03          | 0.2±0.04      | 93.3±2.3       | 82.3±3.1       |
| TSS               | 48±8                   | 0.2±0.03          | 2.0±0.5       | 99.6±0.1       | 95.8±1.0       |

**Fig. 4. RBC Model General layout.**

**Fig. 5. Relation between effluent BOD5 with time for the MBR system.**

**Fig. 6. Relation between effluent COD with time for the MBR system.**
B. RBC Model Operation

Table V shows the results of the RBC model and RBC pilot plant. The BOD$_3$ and COD removal efficiency for the rotating biological contactors model was 95.5±0.3% and 92.6±0.4% respectively. Whereas, the BOD$_3$ and COD removal efficiency for the RBC pilot plant were 94.7±0.4% and 92.3±1.1% respectively. Also, the removal efficiency of total nitrogen TKN and ammonia nitrogen NH$_4^+$ for the RBC model were 71.1±5.6% and 78.5±5.4% respectively. Whereas, the TKN and NH$_4^+$ removal efficiency for the RBC pilot plant were 71.1±5.6% and 78.5±5.4% respectively. Also, the removal efficiency for the total suspended solid TSS for the RBC model and RBC pilot plant was 92.8±0.6% and 86.1±0.8% respectively. Fig. 8 shows the relation between effluent BOD$_3$ with time, Fig. 9 shows the relation between effluent COD with time, Fig. 10 shows the relation between effluent TKN with time, for both RBC model and RBC pilot plant.

### TABLE V: EFFLUENT CHARACTERISTICS FOR RBC SYSTEM

| Parameters | Raw Greywater | Effluent | Removal eff. % |
|------------|---------------|----------|----------------|
|            | RBC Model | RBC Pilot plant | RBC Model | RBC Pilot plant |
| COD        | 92±5.5       | 4.05±0.3    | 3.46±0.3 | 94.7±0.4 |
| Total COD  | 245±12.4     | 18.1±1.1    | 18.6±1.0 | 92.3±1.1 |
| TKN        | 9±1.3        | 3.3±0.6     | 2.6±0.5  | 71.1±5.6 |
| NH$_4^+$   | 1.3±0.2      | 0.38±0.0    | 0.28±0.0 | 70.8±3.8 |
| TSS        | 48±8         | 3.46±0.3    | 2.6±0.5  | 86.1±0.8 |

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