Experimental Investigation on Combustion Characteristics of Hybrid Rocket Fuels with Multi-Angle Diverging Injector

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Abstract: Injection pattern of the oxidizer injected into the combustion chamber is a significant factor in evaluating the performance of a hybrid rocket. In the hybrid rocket combustion process, oxidizer flows over the solid fuel grain surface, leading to a turbulent diffusion boundary layer formation and the flame is established inside the boundary layer. The heat transfer from flame to the fuel surface leads to pyrolysis of the fuel. The heat fluxes, due to pyrolysis, block the heat transfer further to the fuel surface, thus reducing the fuel regression rate. An attempt has been made in this paper to design and study the effect of the multi-angle diverging injector on the enhancement of the fuel regression rate and combustion efficiency of the hybrid rocket. The designed injector was compared with a shower head injector i.e., axial injector. The fuels used were paraffin wax and polyvinyl chloride (PVC) with gaseous oxygen as oxidizer. The effect of formation of the re-circulation zone and flow velocity were studied numerically by a cold flow simulation using ANSYS-Fluent software. It has been observed that direct impingement of the multi-angle diverging injector produces velocity in three directions, leading to distortion of the boundary layer. An increase of 8% in the average fuel regression rate for PVC fuel grain and 36.14% for paraffin wax fuel grain was observed, as compared to the shower head injector for the same oxidizer mass flow rate. A combustion efficiency increase of 38% and 14% was also observed using multi-angle diverging injector for PVC and paraffin wax fuel grains, respectively. A reduction in sliver and uniform fuel consumption was also observed using the novel multi-angle diverging injector.

Keywords: hybrid rocket; injection pattern; regression rate; paraffin wax; polyvinyl chloride

1. Introduction

Hybrid rocket engines are those engines which use oxidizer and fuel of different physical states i.e., liquid or gaseous oxidizer and a solid fuel. Generally, fuel is present in the combustion chamber in solid phase and the liquid or gaseous oxidizer is injected into the combustion chamber through an injector. The two propellants are ignited with the help of an external heat source. The solid fuel grain surface undergoes pyrolysis (as in case of polymeric fuels) or melting (as in case of paraffin wax) and, hence, it leads to chemical changes like de-polymerization and vaporisation, respectively. This vaporized fuel further mixes with the oxidizer to undergo combustion, which further expands the combustion products through the nozzle to develop thrust [1]. The hybrid rockets provide several advantages over the solid and liquid propellant rockets, such as simplicity, safety, lower cost and thrust tailoring. The fuel regression rate is the key parameter for the characterization of the hybrid rocket’s performance [2].
It was widely demonstrated, both theoretically and experimentally, that the regression rate of the solid fuel grain depends upon the convective heat transfer from the flame to the fuel surface, where negligible radiation was considered. Marxman and Gilbert [3] proposed a turbulent boundary layer regression rate model yielding that the rate of fuel consumption is fundamentally governed by mass flux ($r \propto G^{0.8}$). Generally, at lower or higher mass fluxes, another influencing factor on the regression rate for certain solid fuels was found to be pressure. Several investigators credited this effect to either wall heterogeneous reactions with the oxidizer [4], or finite rate gas phase chemical kinetics [5].

In spite of its various advantages, hybrid rocket engines face some difficulties [6] which need to be overcome to enhance its level of performance, such as low regression rate, reduced combustion efficiency, combustion instability and shift in O/F (oxidizer-to-fuel ratio). There have been several techniques proposed to enhance the regression rate of solid fuel in hybrid rockets, such as use of protrusion [7], use of multi-port grain [8], use of cryogenic fuels [9], high mixture ratio, swirl flow of oxidizer inside the chamber, particle additives in solid fuel [10], energetic compounds like plasticizers and binders with solid fuel [11] and manufacturing of grains with helical port shape [12]. However, all of these approaches suffer from some drawbacks.

The oxidizer injection characteristics have a significant part in improving the regression rate of the hybrid rocket because the whole process of combustion is severely affected by the pattern of the incoming oxidizer flow. In the hybrid rocket combustion process, oxidizer flows over the solid fuel grain leading to a boundary layer formation. The flame is formed inside the boundary layer. The heat from the flame travels toward the fuel surface, leading to pyrolysis. The heat flux of the pyrolyzed fuel acts as a hindrance and reduces the heat feedback to the fuel surface. Therefore, an injector is designed to create re-circulation zones inside the chamber such that convective heat transfer to the fuel surface is enhanced, thus increasing both regression rate and combustion efficiency [13]. There have been several researches over injection pattern and the three main types were axial, radial and swirl injectors. Pucci [14] studied the flame holding combustion instability for swirl injectors of 30° and 60° tangential angles and compared them with axial and radial injectors. The conducted experiments showed that a 60° swirl injector produces more stable combustion than radial and 30° swirl injectors as a result of the presence of a high central toroidal re-circulation zone in the combustion port, which in turn created preheating zones at the head end of the combustion chamber. In addition, a rise of 182% in the regression rate was recorded using a 60° swirl injector as compared to an axial injector. Sliver losses with both axial and swirl injectors, on the other hand, were very high.

Carmicino and Sorge [15] conducted a series of tests to examine the regression rate performance of a hybrid rocket system study using conical axial and radial injectors. They concluded that axial injection of the oxidizer produced a higher regression rate and stable combustion as compared to radial injection, but the radial injector produced a uniform combustion along the fuel grain length and thus reduced sliver loss. Further, Martino et al. [16,17] proposed an optimized injector design which included both the axial and radial orifices to combine their characteristics. They observed a raise of 8% in the regression rate in comparison to the axial injector and smooth fuel consumption along the grain length. In this paper, an attempt was made to fabricate a multi-angle diverging injector to study the effects of the re-circulation zone over the regression rate and combustion efficiency of the hybrid rocket for both non-liquefying and liquefying fuels at various port diameters. Moreover, mass flux dependence on the fuel regression rate was observed.

2. Experimental Setup

The experimental set-up utilized in the present study is shown in Figure 1. It consists of a commercial oxygen cylinder having a maximum pressure of 2200 Psi, which was used to supply the oxygen utilizing the feed line made of brass and stainless steel [18,19]. It had various valves to control the output pressure and flow from feed line to the combustion chamber. For all the experiments, the pressure was regulated in the feed line to keep oxygen pressure at 300 Psi, in order to keep the oxidizer mass flow rate at 30 g/s for all of the experiments. To calculate the oxidizer mass flow rate, the oxygen
cylinder was placed on a weighing machine with a minimum count of 1g and a reduction in cylinder weight was continuously recorded for the purpose.

![Figure 1. Complete layout of the experimental set-up.](image)

A solenoid valve was provided at the end of the feed line or near the injection point of oxygen into the combustion chamber, to start and stop the supply of oxidizer into the chamber. For ignition, a bead of solid composite propellant was used. The composition of solid composite propellant bead was 70% ammonium perchlorate and 30% PVC with plasticizer di-octyl phthalate (DOP). For igniting the propellant, the ignition system used was powered by a 12-Volt DC power supply through an AC/DC converter. The Selec 8-channel sequential timer was used to control the ignition system and solenoid valve.

The sequential timer was powered by 220 V AC supply and, through outlet channels, it is connected to solenoid valves and an AC/DC converter, to provide AC supply. The sequential timer regulates the timings to power the solenoid valve and igniter i.e., solid propellant bead. At first, the sequential timer provides DC supply to the igniter through the AC/DC converter for about 3.70 s and ignites the solid propellant; after that it cuts off the supply to the igniter and switches on the supply to the solenoid valve. The solenoid valve is opened to allow oxidizer to flow into the combustion chamber for the desired time interval of operation. The combustion chamber pressure data was taken during firing using a pressure transducer. Data from the pressure transducer was received through a NI DAQ card and NI Signal Express software.

A lab scale hybrid motor was used for this study, as shown in Figure 2. The hybrid rocket motor was made of mild steel with a combustion chamber of length 188 mm and inner diameter of 50 mm. The motor used an aluminium nozzle with graphite insert at the aft end. The hybrid motor at its aft end utilized a convergent-divergent nozzle of 10 mm throat diameter and area ratio of 6.25. The head end of the hybrid motor comprised of the injector plate from where the oxidizer was injected at the desired injection pressure. There was no pre or post chamber in the motor.

In this study, the two injectors used were shower head and multi-angle diverging injectors with an outer diameter of 110 mm, the same as that of the combustion chamber, so that no air gap is left between the leading edges to avoid leakage of gaseous oxidizer. The 3-D CATIA model for the shower head and multi angle diverging injectors are shown in Figures 3 and 4a,b, respectively. Figure 3 shows the geometrical positions of 21 holes of 1 mm diameter, each in the shower head injector. One hole is
drawn at the center and 8 and 12 holes are drilled at equal angular positions on two concentric circles of diameter 8 mm and 12 mm, respectively.

![Figure 2. Schematic of lab-scale model of hybrid rocket motor.](image1)

**Figure 2.** Schematic of lab-scale model of hybrid rocket motor.

![Figure 3. Catia V5 model of (a) shower head injector, (b) Exploded sectional view of shower head injector.](image2)

**Figure 3.** Catia V5 model of (a) shower head injector, (b) Exploded sectional view of shower head injector.

![Figure 4. Catia V5 model of (a) Schematic diagram, (b) Sectional view of multi-angle diverging injector.](image3)

**Figure 4.** Catia V5 model of (a) Schematic diagram, (b) Sectional view of multi-angle diverging injector.

Figure 4a shows the front and back view of the novel (multi-angle diverging) injector with 21 holes of 1 mm diameter, with one hole at the center and 4, 6 and 10 holes are drilled at three concentric circles of PCD of 7, 12 and 16 mm, respectively. The central hole is axial and the other holes drilled at three concentric circles of PCD of 7, 12 and 16 mm, making an angle of 15°, 10° and 5° with the axis, respectively. For further incite, the sectional view of diverging angles was developed by CATIA V5,
as shown in Figure 4b. The cross-sectional area of each hole and the number of holes in both injectors are the same, so that total discharge area of oxidizer to chamber should be the same for justifiable comparisons of performance of the injectors under study. The PCD of the outer concentric circles of both of the injectors is less than the port diameter of fuel grain.

The non-liquefying fuel utilized in the present work was polyvinyl chloride (PVC) with dehumidified plasticizer di-octyl phthalate (DOP) in a mixture ratio of 50:50 by weight. The homogenous slurry of powdered PVC and liquid DOP was casted in an aluminium mould of 200 mm length and 50 mm inner diameter with a mandrel of diameter 21mm, to prepare a tubular grain. The casted slurry was then kept inside the hot air oven for 4 h at 125 °C for curing. The casted slurry is popularly known as fuel grain, with an outside diameter 50 mm and 188 mm length, whereas the inner hollow tubular portion is called port, with a diameter of 21 mm across its length, as shown in Figure 2. The liquefying fuel used in the present work was a combination of 30% microcrystalline wax and 70% paraffin wax. The melted wax was casted in the mould and cured at atmospheric conditions for 4 h. The wax fuel was casted inside a PVC pipe for easy handling.

3. Results and Discussion

The section includes the regression rate and combustion efficiency studies using the multi-angle diverging injector and comparison with the conventional shower head injector. The fuel types utilized in the present study were PVC and paraffin wax fuels with gaseous oxygen as oxidizer.

3.1. Effect of Injector Type

In the present study, two injector types have been evaluated. One is the shower head injector i.e., axial type and other is the fabricated multi-angle diverging injector. Table A1 (Appendix A) summarizes the test conditions and regression rate obtained using both of the injector types, with PVC as fuel.

An increase of the average regression rate, using multi-angle diverging injector of around 8%, was obtained as compared to the conventional shower head injector. The increase in average regression rate using the multi angle diverging injector is obtained because the oxidizer enters into the chamber through injector and impinges at three different locations on the fuel grain surface, creating more recirculation as compared to the shower head injector. This recirculation zone enhances the internal energy of the oxidizer flow, which is then converted into the kinetic energy of the oxidizer molecules, leading to a rise in heat flux at the head end. The average mass flux is enhanced due to a higher fuel mass flow rate at the head end before the formation of the boundary layer. This in turn diminishes the blocking effect due to fuel mass flux, as the core flow is strongly influenced by the directional flow structures that arise due to the unique injection method. Hence, a rise in the average regression rate was observed using multi-angle diverging injector. Figure 5 shows the average regression rate vs the average mass flux for both of the injector types. The power value of average mass flux of 0.35 is observed during experimentation utilizing multi-angle diverging injector, 0.68 using shower head injector. This clearly suggests that the injection pattern using multi-angle diverging injector affects the average regression rate due to jet impingement zone dynamics. The flow field in the port is dominated by the reattachment or impingement region, which results in an increase in the average regression rate, and a diminishing of the dependence of the average mass flux on the regression rate. Carmicino and Sorge [15] also reported similar dependence of mass flux with a power raised to 0.35, which further supports the effect of impingement as obtained in the present case.

A 2-dimensional cold flow analysis of oxygen inside the combustion chamber was also carried out using Ansys fluent software in order to study the variation of oxidizer flow velocity (axial component) along the length of the combustion chamber, as shown in Figure 6a,b, using the two injector types. The combustion chamber is represented by uniform cross-sectional area, and, on the right end of the chamber, the converging-diverging area represents the nozzle. The analysis is based on the impact
of axial components of oxidizer flow velocity along the length of chamber, to show the disturbance created by the radial entrance of the oxidizer inside the chamber using the novel injector.

![Graph showing the relation between average regression rate and average mass flux.](image)

**Figure 5.** Average regression rate vs. average mass flux using the two injector designs for PVC fuel.

![Axial velocity contour.](image)

(a)

![Axial velocity contour.](image)

(b)

**Figure 6.** Axial velocity contour using (a) shower head injector and (b) multi-angle diverging injector.

The velocity inside the nozzle is beyond the scope of discussion as it does not affect the combustion process inside the chamber. Figure 6a depicts that, for the shower head injector, the axial velocity component gradually increases from 122 m/s to 400 m/s along the length of the combustion chamber. In the case of the multi-angle diverging injector, Figure 6b, the axial velocity of the oxidizer is quite low, of the order of around 2.9 m/s, and is even negative. These values suggest the formation of a recirculation zone near the head end of the chamber due to radial entry of the oxidizer, considerably reduces the axial component of velocity. Contrary to this, the recirculation of the oxidizer flow at the head end increases the residence time of the gases inside the chamber. Thus, cold flow analysis suggested more turbulence in oxidizer flow near the head end of the port using multi-angle diverging injector, which led to an increase in the residence time for an actual combustion process in a real scenario. On the other hand, a linear increase in velocity was observed using the shower head injector with higher values approaching downstream of the combustion chamber, which results in shorter residence time and hence incomplete combustion occurs.
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A study of the local regression rate along the chamber length of 188mm was also carried out and Figure 7 shows the trend of local regression rate versus the ratio of axial length to grain length (x/L) of the grain using the two injector designs. The web thickness uniformity was obtained downstream of the flow in the case of the multi-angle diverging injector, as shown in Figure 7. The graph shows that the regression rate at the head end is higher in the case of the multi-angle diverging injector by 83.1%, as compared to the shower head injector. In the case of the multi-angle diverging injector, the combustion starts at the head end itself as the heat flux is high due to increased residence time of the oxidizer and, as the flow goes downstream, the particles flow uniformly and reduce sliver loss. This uniformity occurs presumably due to the stagnation point heat transfer near the edge of the impinging oxidizer jet. Analogous observations were reported by Caravella et al. [20].

![Figure 7. Local regression rate vs. x/L using the two injector designs using PVC fuel.](image)

The photographic view of burnt PVC grain used in the shower head injector and multi angle diverging injector are shown in Figure 8a,b, respectively. The depressions at the head end of the fuel grain using the multi-angle diverging injector clearly indicate that, due to the larger residence time for oxidizer in the beginning, using multi angle diverging injector helps to burn the larger portion of grain, initially in comparison to fuel grain burnt using the shower head injector.
3.2. Effect of Port Diameter

In the present study, three port diameters of 21, 24 and 28 mm were taken to study the effect of the port diameter on the regression rate using multi-angle diverging injector for PVC fuel grain. Table 1 shows the average regression rate studies for the varying port diameter.

Table 1. Average regression rate for the varying port diameter using multi-angle diverging injector.

| Port Diameter (mm) | Average Regression Rate (mm/s) | Burn Time (s) |
|--------------------|-------------------------------|---------------|
| 21                 | 0.74                          | 6             |
| 24                 | 0.73                          | 6             |
| 28                 | 0.67                          | 6             |

Figure 9 shows the variation of local regression rate for various port diameters versus the ratio of axial length to grain length (x/L). The figure depicts that near the head end, up to 5 cm distance, the local regression rate increases sharply and then decreases; this behavior was observed for all three of the port diameters. However, the maximum rise in local regression rate was observed with a port diameter of 21 mm. Further, across the length of the chamber until the aft end, the curves for all port diameter become flat and comparatively a higher local regression rate was observed for 24 mm port diameter. However, after 5 cm distance from the head end, the decrease in average regression rate is because the average mass flux reduces due to a higher increase in the port area. This could be explained by the local regression rate along the grain length depicting a decrease in the heat flux at the head end, which is observed with the increase in the port diameter as the oxidizer mass flux reduces, and the same can be observed in Figure 9. Carmicino et al. [21] also reported a decrease in regression rate with increasing port diameter for a converging nozzle.
3.3. Effect of Fuel Type

The liquefying fuel utilized in the present study is paraffin wax with gaseous oxygen as oxidizer. As stated in the literature, paraffin wax burns 2–3 times faster than the polymeric-based fuels [22,23]. Interrupted test firing of 1 s each for three times was conducted to calculate the regression rate using the weight loss method. Table A2 summarizes the test conditions and regression rate obtained using both of the injector types with paraffin wax as fuel. The results suggested an increase in the average regression rate using a multi-angle diverging injector as compared to a shower head injector by 36.14%.

The graphical representation of the values of regression rate with respect to average mass flux of Table A2 is shown in Figure 10. Figure 10 depicts that the average regression rate increases with an increase in the average mass flux for both of the injector designs. However, the rise in average regression rate with the increase of average mass flux is steeper for the multi-angle diverging injector in comparison to the shower head injector; it is due to the combined effect of injector design as well as the effect of melt-layer formation by paraffin wax fuel. The multi-angle diverging injector creates higher recirculation at the head end as compared to the shower head and, therefore, the mixing of oxidizer with fuel droplets is enhanced. This results in an increase of the average regression rate.

![Graph showing local regression rate vs. x/L using multi-angle diverging injector by varying port diameter.](image)

**Figure 9.** Local regression rate vs. x/L using multi-angle diverging injector by varying port diameter.

3.4. Effect on Combustion Efficiency

In the present study, combustion efficiency performance was also compared for the two injector designs with both liquefying and non-liquefying fuel types. The c* efficiency was calculated using the following formulas:

\[ c^* = \frac{\text{I}}{\text{m}} \]

The graphical representation of the values of regression rate with respect to average mass flux using the two different injector designs for paraffin wax fuel is shown in Figure 10. Figure 10 depicts that the average regression rate increases with an increase in the average mass flux for both of the injector designs. However, the rise in average regression rate with the increase of average mass flux is steeper for the multi-angle diverging injector in comparison to the shower head injector; it is due to the combined effect of injector design as well as the effect of melt-layer formation by paraffin wax fuel. The multi-angle diverging injector creates higher recirculation at the head end as compared to the shower head and, therefore, the mixing of oxidizer with fuel droplets is enhanced. This results in an increase of the average regression rate.

![Graph showing average regression rate vs. average mass flux using the two different injector designs for paraffin wax fuel.](image)

**Figure 10.** Average regression rate vs. average mass flux using the two different injector designs for paraffin wax fuel.
3.4. Effect on Combustion Efficiency

In the present study, combustion efficiency performance was also compared for the two injector designs with both liquefying and non-liquefying fuel types. The c* efficiency was calculated using the following formulas:

\[ C_{\exp} = \frac{P_c A_l}{m_{ox} + m_f} \]  

(1)

\[ \eta_c = \frac{C_{\exp}}{C_{\text{theo}}} \]  

(2)

The average chamber pressure was measured using the pressure transducer at the aft end of the chamber with obtained pressure curves shown in Figures 11 and 12, and theoretical characteristic velocity was obtained using NASA CEA software.

**Figure 11.** Pressure-time data using (a) shower head injector and (b) multi-angle diverging injector for PVC fuel.
Figure 12. Pressure-time data using (a) shower head injector and (b) multi-angle diverging injector for paraffin wax.

Table 2 summarizes the combustion efficiency results. The multi-angle diverging injector induces higher mixing of oxidizer and pyrolyzed fuel and hence a rise in combustion efficiency was observed in comparison to the shower head injector. In comparison to PVC fuel, combustion efficiency has decreased in the case of paraffin wax using shower head and multi-angle diverging injectors, by around 3% and 24.4%, respectively. This decrement has been observed due to dual phase flow dynamics during the combustion of paraffin wax, as liquid droplets of wax and gaseous oxidizer mix and undergo chemical reaction. In comparison to wax, polymeric fuel i.e., PVC undergoes a single-phase flow as both oxidizer and pyrolyzed fuel are in the gaseous phase.
Table 2. Combustion efficiency data for two injector designs.

| Injector Type          | Fuel Type      | Average Chamber Pressure (Psi) | O/F Ratio | Theoretical Characteristic Velocity (m/s) | Combustion Efficiency (%) |
|------------------------|----------------|-------------------------------|-----------|------------------------------------------|----------------------------|
| Shower head injector   | PVC            | 74.26                         | 2.55      | 1558.5                                   | 61.9                       |
| Multi-angle diverging  | PVC            | 101.33                        | 0.76      | 1505.5                                   | 85.7                       |
| injector               | Paraffin wax   | 93.83                         | 0.96      | 1382.3                                   | 60.23                      |
| Multi-angle diverging  | Paraffin wax   | 115.79                        | 0.73      | 1298.3                                   | 68.90                      |

4. Conclusions

In the present study, the effects of changing oxidizer patterns were studied on the liquefying and non-liquefying fuels by designing a new injector type i.e., the multi-angle diverging injector. The following were the conclusions drawn from the experiments conducted:

1. The multi-angle diverging injector showed a better performance by increasing the average regression rate and combustion efficiency by around 8% and 38.45%, respectively, for non-liquefying fuel, i.e., PVC+DOP, in comparison to the shower head injector.
2. The multi-angle diverging injector showed the better performance by increasing the average regression rate and combustion efficiency by around 36.14% and 14.4%, respectively, for liquefying fuel, i.e., paraffin wax, in comparison to the shower head injector.
3. Uniform burning downstream of the combustion chamber and sliver loss reduction was observed using the multi-angle diverging injector for PVC+DOP fuel, in comparison to non-uniform burning observed using the shower head injector.
4. The power exponent value of around 0.35 was obtained for multi-angle diverging injectors and 0.68 for the shower head injector, depicting the effect of jet zone dynamics on the regression rate for the PVC+DOP fuel type.

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Nomenclature

- $A_t$: Throat area, m$^2$
- $A_p$: Port area, m$^2$
- $a$: Oxidizer mass flux constant
- $n$: Power exponent of mass flux
- $\rho_f$: Density of fuel, kg/m$^3$
- $C_{*exp}$: Experimental characteristic velocity, m/s
- $C_{*theo}$: Theoretical characteristic velocity, m/s
- $C_{*ox}$: Characteristic velocity of oxidizer, m/s
- $L/D$: Ratio of total length to initial port diameter of fuel
- $I_{sp}$: Specific impulse, Ns/kg
- $P_c$: Average chamber pressure, Psi
- $G$: Average mass flux, kg/s. m$^2$
- $G_{ox}$: Oxidizer mass flux, kg/s. m$^2$
- $Re$: Reynolds number
- $B$: Blowing number
- $m_f$: Mass of the fuel consumed, g
- $d_i$: Initial port diameter, mm
- $L_g$: Length of the fuel grain, mm
- $b_b$: Burn time, s
- $r$: Regression rate, mm/s
- $m_{ox}$: Oxidizer mass flow rate, g/s
- $\dot{m}_f$: Fuel mass flow rate, g/s
- $\eta$: Combustion efficiency
- $m_{t}$: Total mass flow rate of propellant, g/s
- $T_c$: Combustion chamber temperature, K
- $T_{ox}$: Oxidizer temperature, K
Appendix A

Table A1. Interrupted test firings for PVC fuel.

| Injector Type              | Regression Rate (mm/s) | Oxidizer Mass Flux (kg/s. m²) | Average Mass Flux (kg/s. m²) | Burn Time (s) |
|----------------------------|------------------------|-------------------------------|------------------------------|---------------|
| Shower head injector       |                        |                               |                              |               |
| (axial injection)          | 1. 0.698               | 76.19                         | 102.86                       | 2             |
|                            | 2. 0.710               | 60.13                         | 84.18                        | 2             |
|                            | 3. 0.665               | 48.88                         | 69.25                        | 2             |
|                            | 4. 0.562               | 41.31                         | 57.15                        | 2             |
| Multi-angle diverging      |                        |                               |                              |               |
| injector                   | 1. 0.793               | 74.92                         | 104.88                       | 2             |
| (axial injection)          | 2. 0.700               | 58.44                         | 81.82                        | 2             |
|                            | 3. 0.709               | 47.41                         | 68.75                        | 2             |
|                            | 4. 0.625               | 39.62                         | 56.78                        | 2             |

Table A2. Interrupted test firings for Paraffin wax fuel.

| Injector Type              | Regression Rate (mm/s) | Oxidizer Mass Flux (kg/s. m²) | Average Mass Flux (kg/s. m²) | Burn Time (s) |
|----------------------------|------------------------|-------------------------------|------------------------------|---------------|
| Shower head injector       |                        |                               |                              |               |
| (axial injection)          | 1. 2.17                | 71.22                         | 138.39                       | 1             |
|                            | 2. 1.98                | 51.26                         | 99.61                        | 1             |
|                            | 3. 1.91                | 39.27                         | 76.32                        | 1             |
| Multi-angle diverging      |                        |                               |                              |               |
| injector                   | 1. 3.12                | 65.68                         | 151.08                       | 1             |
| (axial injection)          | 2. 2.71                | 42.61                         | 99.42                        | 1             |
|                            | 3. 2.42                | 31.05                         | 76.61                        | 1             |

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