Synthesis of oil palm frond (OPF) based silica nanomaterial via sol-gel method with enhanced phenol removal

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ABSTRACT – This research investigates the potential of the oil palm frond (OPF), a well-known biomass from the oil palm industry, as a feasible silica precursor that can be utilised in the removal of phenol from an aqueous solution. Dried OPF was combusted to obtain OPF ash that was treated with citric acid before being synthesised as silica nanomaterial via the sol-gel method. The FTIR results of synthesised silica exhibit a similar peak with commercially available silica. Silica material was then used for phenol removal under different parameters including pH, contact time, dosage, concentration, and temperature, then analysed using UV-Vis Spectrophotometer. The optimum condition was obtained at pH 7 within 45 mins of contact time using 0.2 g/L silica dosage under 10 ppm of phenol concentration at 303 K that aid in enhancing phenol removal by the OPF-based silica. At this condition, silica nanomaterial successfully removed up to 68% of phenol in an aqueous solution with adsorption capacity of the adsorbent is within the range of 34 mg/g. These results demonstrate the potential application of silica nanomaterial from OPF as an adsorbent in phenol removal from wastewater.

INTRODUCTION

Several approaches have been studied extensively for the removal of toxic substances from water and can be divided into biological, chemical, and physical treatment. Since the rapid expansion of industrialization, water pollution is arguably the most concerning issue that has affected human life. Water pollutants mainly come from human and industrial waste and consist of heavy metal material, biological contaminants, pharmaceutical contaminants that are dangerous to the ecosystem and living things due to their indestructible nature and acute behaviour [1]. Phenol (benzenol) or also known as hydroxybenzene with molecular formula C₆H₅OH, is an aromatic hydrocarbon group bound to the hydroxyl group (OH). It has various industrial uses and has been utilized widely in dyes production, pesticides, and drugs as intermediate chemicals [2,3]. In ambient temperature, phenol physical attributes are identified as white/colourless crystalline powder that is hydrosopic in water and slightly in an organic solvent such as alcohol, glycerol and petroleum that make it easier to leak into groundwater sources or water surface [3].

In Malaysia, massive industrialization has caused population growth and rapid urbanization. It has led to the increase of hazardous substance discharge and effluent from a wastewater treatment plant. As a result, a higher level of pollutants including phenol and phenolic compounds were traced as they are easily dissolved in water at room temperature [3-5]. According to National Water Quality Standards for Malaysia, phenol concentration shall not exceed 10 ug/L in water. Higher phenol concentrations (100–1000 ug/L) produce unpleasant odor and taste that can react with chlorine to form chlorophenol, a carcinogenic and toxic to humans [6].

The introduction of nanomaterials caused literal explosive growth in the evolution of water treatment technology. Its smaller size and larger surface area are beneficial to many interfaces related applications. The chemical, physical, electro and mechanical characteristics can be tuned to control their surface morphology, crystal orientation, shape, size and others [7]. Silica was studied extensively over the years in the development of nanomaterials owing to the marked improvement of their preparation through a sol-gel method and the stable free energy that almost resemblance to crystalline quartz. Furthermore, the Si-O bond is strong that the reaction that takes place during the sol-gel process is highly irreversible. The synthesis of amorphous silica also has high thermal stability and the interactions between surfactants can be tuned due to silica ability to be in anionic, cationic, or neutral form depending on the pH [8,9].

Phenol removal using silica as an adsorbent has been investigated by Roostaei and Tezel [10]. In this study, HiSiV 1000, an adsorbent that contains crystalline, inorganic silica-alumina structure, displays the best result whereby in the powder form, it has the highest adsorption capacity [10]. The application of commercial porous silica gel was used in a study that investigates the efficiency of polyamine coated silica gel in removing phenol [11]. Silica aerogel synthesised from the commercial sodium silicate also has been investigated. The results showed that the synthesis silica gel via sol-gel method could remove phenol in an aqueous solution at pH 8.5 with efficiency up to 90% when phenol concentration was below 50 ppm, and the maximum adsorption capacity was 75.25 mg/g [12]. Other work has studied the performance...
of amino-modified silica nanoparticles synthesised from TEOS (tetraethyl orthosilicate) via the sol-gel method [11]. In this study, the synthesised silica is categorized based on TEOS concentration used during synthesis and the best adsorbent is AMS-10 with removal capacity calculated to be 35.2 mg/g [13].

Prior to this, phenol removal using agricultural biomass adsorbent has been investigated which includes the biomass such as coconut, rice husk, and sugarcane bagasse which all manifested in ash form and render as adsorbent after activation with various forms of treatment and success in removing phenol [14]. Silica nanomaterial was synthesised from commercially available silica precursors such as TMOS and TEOS, however, a recent trend has seen the emergence of agricultural biomass as silica sources such as rice husk, bamboo culm and corn cob [15-18].

Roslan et al. (2016) suggested an OPF containing siliceous material based on the analysis of its ash contain [19]. Approximately 10 tonnes dry weight of OPF were produced per hectare during the pruning session and this can increase up to 14 tonnes dry weight per hectare during replanting [20]. The abundance of this biomass made it a viable alternative as a silica precursor for the synthesis of silica nanomaterial from agricultural waste.

For this research, an oil palm frond (OPF), biomass from the oil palm industry (plantation) has been utilised as silica precursor in the synthesis of silica nanomaterial via a modified sol-gel method which was later applied as adsorbent material for phenol removal from aqueous solution. Based on previous silica extraction from agricultural waste, silica is usually extracted and produced into powder form before being used as a precursor in silica nanoparticle synthesis. This project aims to utilise sodium silicate solution produced from OPF ash that is treated with nitric acid as silica precursor and directly used in sol-gel synthesis to produce the silica nanoparticle. The method of producing sodium silicate from treated OPF ash has been established based on a study performed previously by this research group [21]. The modification aspect of this study is by directly applying treated OPF ash-based sodium silicate solution into the sol-gel process instead of extracting it as powder silica which is usually performed in a previous study setting.

**MATERIALS AND METHODS**

**Chemicals**

Oil palm frond (OPF) was collected from a private palm oil plantation at Alor Gajah, Melaka. The OPF ash was treated using citric acid from HmBG. Reagents used in sol-gel including NaOH pellet from VChem, hydrochloric acid from Sigma-Aldrich (37%), and hexadecyltrimethylammonium bromide (CTAB) from Sigma Aldrich (98% purity) while phenol powder was purchased from Merck Millipore (>98% purity). SiO$_2$ reagent grade purchase from Merck Millipore (~98% purity).

**Preparation of raw material (OPF) and acid leaching treatment**

The collected OPF was cleaned, sorted, and cut before being dried in the oven at 313 K for 24 hours. The OPF was then combusted in an electric muffle furnace at 873 K for 3 hours to obtain oil palm frond ash (OPFA). Citric acid with a concentration of 3% was first prepared. 20 g of OPFA was measured on an analytical balance and poured into the citric acid solution. The mixture was placed in the hot place at 343 K with a reaction time of 1 hour. The treated ash was rinsed using distilled water at room temperature to remove citric acid from the ash then followed with drying at 353 K for 8 h in the drying oven. Dried treated ash was finally calcined at 1073 K for 30 minutes in the electric muffle furnace [21].

**Silica nanomaterial synthesis**

Silica was prepared at ambient temperature by mixing acid-leached OPFA in 2M NaOH for 1 hour with continuous stirring. The direct application of treated OPF-based sodium silicate solution as silica precursor is the modification in this sol-gel process. Previous study agricultural waste silica was extracted into powder form before being applied in silica synthesis using the sol-gel method. CTAB was dissolved in distilled water and stirred on a hot plate at 500 rpm for 30 mins at room temperature. Sodium silicate solution was then added gradually and where it turned into a murky whitish solution. HCl acid was used to obtain pH between 1-10 with removal capacity calculated to be 35.2 mg/g [13]. The solution was aging at 333 K overnight. The solution was filtered after 1 hour at 353 K. Sodium silicate solution was then added gradually and where it turned into a murky whitish solution. The solution was continuously stirred at 800 rpm for another 1 hour at 353 K. The solution was aging at 333 K overnight. The solution was filtered, and the silica nanomaterial was repeatedly rinsed with water-methanol solution (1:1) and dried at 373 K. The white powder silica was then calcined at 773 K for 5 hours at 278 K/min rate. Silica nanomaterial obtained was characterized using FTIR (Thermo Scientific Nicolet iS10).

The following equations were used to calculate the corresponding parameters.

\[
\frac{OPF_a}{OPF_t} \times 100 = \text{% of OPF ash obtained} \quad (1)
\]

where OPF$_a$ represent the initial amount of dry OPF before combustion and OPF$_t$ represent the OPF ash obtain after combustion,

\[
\frac{OPF_{a \text{acid leached}}}{OPF_{a}} \times 100 = \text{% of acid leached OPF ash obtained} \quad (2)
\]

where OPF$_{a \text{acid leached}}$ represent the initial amount of OPF ash before acid leaching and OPF$_a$ represent the amount of OPF ash after acid leaching,

\[
\frac{OPF - \text{based silica}}{OPF_t} \times 100 = \text{% of silica nanoparticle obtained} \quad (3)
\]
where OPF$_t$ represents the amount of OPF ash after acid leaching and OPF-based silica is the amount of silica nanoparticle obtained from the synthesis.

**Phenol removal from aqueous solution**

Phenol nanomaterial obtained was used as an adsorbent in phenol removal. Performance analyses were performed at different pH (3, 5, 7, 9, 11), contact time (5, 10, 15, 30, 45, 60 min), silica dosage (0.2, 0.4, 0.5, 0.8, 1.0 g/L), phenol concentration (10, 20, 30, 50, 70, 100 ppm), and temperature (303 K, 323 K, 343 K); with continuous stirring on hot plate (400 rpm). The results were analysed using UV-Vis (Perkin-Elmer Lambda 35 UV-Vis) at $\lambda$ max 267 nm. A standard calibration curve was initially produced to obtain a linear equation to calculate the concentration of phenol in an aqueous solution after removal.

The percentage removal of phenol using silica nanomaterial absorbent is measured and its efficiency is calculated as follows:

$$\frac{C_i - C_f}{C_i} \times 100 = \% \text{ of phenol removal}$$

(4)

where $C_i$ is the initial concentration and $C_f$ is the final concentration. The adsorption capacity were then calculated such that

$$\frac{(C_i - C_f)V}{W} = Adsorption \ capacity \ (q)$$

(5)

where $V$ is the volume of the phenol used during adsorption process (cm$^3$), $W$ is the mass of adsorbent used during the adsorption process (mg) and $q$ is the amount adsorbed in unit mass of the adsorbent (mg/g).

**EXPERIMENTAL RESULTS**

**Silica nanomaterial synthesis from OPF and characterization**

In the synthesis of silica nanomaterial from OPF as silica precursor, modified sol-gel methods were applied and CTAB was chosen as the surfactant that renders the sodium silicate obtained from treated OPF ash to be a white colour powder. Figure 1 provides the overall process of synthesising the silica nanomaterials. Table 1 shows the yield percentage of silica nanomaterial obtained per 1000 gm of dry weight OPF.

| Dry OPF (g) | OPF Ash (g) | OPF Ash (%) | Acid Leached OPF Ash (g) | Acid Leached OPF Ash (%) | Silica (g) | Silica (%) |
|------------|-------------|-------------|--------------------------|--------------------------|------------|-----------|
| 1,000      | 45          | 4.5         | 21.6                     | 48%                      | 14.04      | 65        |

The results show approximately 65% silica nanomaterial yield and are relatively comparable to the yield of silica from other agricultural biomass such as sugarcane bagasse ash (50%-80%), bamboo leaf (60%-80%), wheat straw (50%-55%) and OPA (40%-80%) [15,16]. It is also slightly higher when compared to the yield of silica from sources such as corn cob, bamboo culm and cassava peel [15].

![Figure 1. Silica nanomaterial synthesis from OPF.](image-url)
Silica nanomaterial from OPF was analysed using FTIR and the result was shown in Figure 2. The spectra of the silica obtained from OPF display similar peaks to commercial silica when examined within the range of 4000-400 cm\(^{-1}\). For both silicas, the presence of a strong and broad band around 3420-3440 cm\(^{-1}\) is due to the -OH stretching vibration of the silanol or the adsorbed water molecules on the silica surface. The next peak within the range of 1620-1640 cm\(^{-1}\) represents the bending vibration band of the trapped H\(_2\)O molecule within the silica matrix. The strong band around 1060-1110 cm\(^{-1}\) corresponds to the asymmetric vibration of the Si-O-Si siloxane bond, the bond that forms the silica matrix backbone.

The peak at 941 cm\(^{-1}\) and 451 cm\(^{-1}\) represents the valent and deformation vibrations of the Si-O-Si siloxane bond that were absent in OPF-based silica however this bond is present by the strong peak at 640 [18]. The absence of both peaks in OPF-based silica might be due to the water content in OPF-based silica that is smaller compared to the commercial silica [18]. FTIR spectra obtain from the OPF-based indicate the presence of the essential functional group that was also present in FTIR spectra for the synthesise of silica nanomaterials from agricultural waste [16,17].

![FTIR spectra of silica nanomaterial.](image)

**Figure 2.** FTIR spectra of silica nanomaterial.

### Effect of different parameters in phenol removal using OPF-based silica

The removal of phenol using silica nanomaterial from OPF was performed and analysed using UV-Vis by measuring maximum absorption at 267 nm. The efficiency was investigated through various parameters including pH, contact time, silica dosage, phenol concentration, and temperature as shown in Figure 3.

The pH\(_{zpc}\) of silica were analysed using pH titrations at different strengths that provide the value of 6.45. The result shows that the best pH is 7 where the equilibrium was reached within 30-45 mins. There is no significant reduction after 45 mins contact time. At this condition, phenol was removed up to 63% with adsorption capacity (\(q\)) at 31.3 mg/g. However, at acidic and basic conditions, phenol removal was significantly lower with only 25-26% with adsorption capacity (\(q\)) of 11-13 mg/g. These findings supported the results obtained by Rahmani et al. [12] and Saleh et al. [13] where the highest removal of phenol was recorded at pH 8.5 and pH 6-7, respectively.

Phenol has a pKa value of approximately 10, indicating an anionic form while OPF-based silica has a pH\(_{zpc}\) value of 6.45 indicating negative sides on its surface. This could be the reason for the low removal of phenol at a higher pH value. Thus, at higher pH, electrostatic repulsive force occurs between the negative surface of OPF-based silica and the phenoxide ion and prevents the adsorption of phenol onto the silica nanoparticle. Meanwhile, for phenol solution on pH lower than 11, phenol maintains its dissociative form and is relatively attracted to the negative side of OPF based silica (6.45 < pH < 11) and positive surface (3 < pH < 6.45) due to dispersion interaction. Lower phenol removal at low pH might be due to the competition occurring on the OPF-based silica surface between proton ions and phenol molecules [12]. This also could explain the adsorption capacity of OPF-based silica which increases as pH increases but decreases when pH is more than 10.

The effect of silica dosage was investigated between 0.2 g/L and 1.0 g and the results are shown in Figure 3(c). It demonstrates a higher phenol removal when the dosage is increased. Nonetheless, the increment of phenol removal at a higher dosage does not give a significant difference which might be due to the saturation of silica at a higher dosage and the phenol removal reaching equilibrium at a faster rate. This result indicates that this silica material working mechanism in removing phenol may not be driven based on its dosage in the aqueous solution.

The effect of phenol concentration was investigated from between 10 and 100 ppm. From the result, phenol removal shows a significant decrease as the phenol concentration increases. It is highly improbable that the phenol adsorption by silica is driven based on phenol concentration, as though the removal percentage decrease; however, the adsorption...
capacity \(q\) by the silica is retained almost at a similar rate even at a higher phenol concentration. The effect of temperature shows that phenol removal is significantly higher at room temperature (303 K) with the highest adsorption capacity \(q\) of silica is within the range of 33-36 mg/g. Silica nanomaterial adsorption capacity \(q\) calculated from this study is comparable to other studies performed utilising amino-modified silica [15].

Figure 3. Removal of phenol as a function of several parameters: (a,b) pH and contact time (c) silica dosage (d) phenol concentration (e) temperature.
Silica nanomaterial performance in phenol removal

The efficiency of phenol removal by the OPF-based silica nanomaterial was performed in batches at optimum pH 7, contact time (45 min), silica dosage (0.2 g/mL), phenol concentration (10 ppm), and temperature (303 K). The data tabulated in Table 2 shows the removal efficiency at 68% and the adsorption capacity (q) is significantly constant at 34 mg/g at the optimum parameters. These results indicate that the silica synthesise from OPF has a feasible application in phenol removal from an aqueous solution as it efficiently lowered phenol concentration. The maximum adsorption capacity obtained by this study is almost comparable to Saleh et al. that utilised amino-modified silica synthesised from TEOS [13]. Nonetheless, the result from this work is slightly lower when compared to the results obtained by Rahmani et al. [12].

Table 2. Adsorption of phenol by OPF-based silica nanomaterial at optimum condition [pH 7, 45 mins of contact time, 0.2 g/L silica dosage, 10 ppm concentration of phenol, and 303 K]

| Batch | Before (ppm) | After (ppm) | Removal (%) | Adsorption Capacity (mg/g) |
|-------|-------------|-------------|-------------|---------------------------|
| 1     | 10          | 3.183       | 68.170      | 34.085                    |
| 2     | 10          | 3.283       | 67.170      | 33.585                    |
| 3     | 10          | 3.198       | 68.020      | 34.010                    |

The adsorption capacity (q) ability by OPF-based silica display a higher feasible adsorption interaction as its viable mechanism in removing phenol from the investigated solution. The synthesised silica tested in different batches exhibit similar results with the literature when the optimum parameter was utilised. This provides a probable indication that the parameter investigation has an effect in optimizing the working mechanism that allows OPF-based silica to remove phenol from an aqueous solution.

CONCLUSION

The utilisation of OPF as a silica precursor in this research project has shown a positive result when applied as feasible adsorbent material in removing phenol from the aqueous solution. The FTIR spectra from the OPF-based silica display significant similarity with the FTIR spectra of commercially available reagent grade silica. Sodium silicate solution obtained from treated OPF ash was successfully synthesised into silica nanomaterial where CTAB was applied as surfactant via modified sol-gel method. Subsequently, synthesised material was analysed for its feasibility as adsorbent material in removing phenol, a widely used intermediate chemical in various industries. OPF-based silica was analysed at different parameters including pH, contact time, dosage, phenol concentration, and temperature. At optimum parameters, (pH 7, 45 mins of contact time, 0.2 g/L silica dosage, 10 ppm of phenol concentration, and 303 K temperature), synthesised silica significantly removed up to 68% phenol from aqueous solution, and retain constant adsorption capacity at 34 mg/g. Therefore, this research resulted in an open plethora viability of the utilisation of OPF as silica precursor in nanomaterial synthesis as well as possible application in toxic pollutant removal in wastewater.

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