Aerobic Denitrification Microbial Community and Function in Zero-Discharge Recirculating Aquaculture System Using a Single Biofloc-Based Suspended Growth Reactor: Influence of the Carbon-to-Nitrogen Ratio

Min Deng¹, Zhili Dai², Yeerken Senbati¹,², Lu Li¹, Kang Song¹,³* and Xugang He⁴

¹ State Key Laboratory of Freshwater Ecology and Biotechnology, Institute of Hydrobiology, Chinese Academy of Sciences, Wuhan, China, ² School of Materials Science and Chemical Engineering, Anhui Jianzhu University, Hefei, China, ³ University of Chinese Academy of Sciences, Beijing, China, ⁴ College of Fisheries, Huazhong Agricultural University, Wuhan, China

In this study, the effect of aerobic denitrification on nitrogen removal was investigated using two zero-discharge biofloc-based recirculating aquaculture systems with representative carbon-to-nitrogen (C/N) ratios of 15 (CN15) and 20 (CN20). Aquaculture wastewater, residual feed, and fish feces were treated in an aerated suspended growth reactor (SGR, dissolved oxygen > 5.0 mg L⁻¹). Low toxic NH₃ (<0.1 mg L⁻¹) and NO₂⁻-N (<0.5 mg L⁻¹) concentrations and high NO₃⁻-N (83.3%) and NO₂⁻-N (100%) removal efficiencies were achieved in the fish tank and SGR of CN20, respectively. The nitrogen mass balances indicated that the gaseous nitrogen loss accounted for 72–75% of the nitrogen input. Illumina sequencing and quantitative polymerase chain reaction revealed that increasing the C/N ratio significantly increased the amount of aerobic denitrifying bacteria (Dechloromonas, Rhodobacter, Flavobacterium, and Zoogloea) and aerobic denitrifying functional genes (napA, nirK, and nosZ). Autotrophic Nitrosomonas was the dominant nitrifying bacteria in the CN15 system, and autotrophic (Nitrosomonas) and heterotrophic nitrifiers coexisted in the CN20 system. Moreover, the functional prediction analysis showed that the carbohydrate, energy, and amino acid metabolisms in the SGR of the latter increased. In conclusion, aerobic denitrification should widely exist in biofloc systems.

Keywords: aerobic denitrification, C/N ratio, nitrogen removal, qPCR, microbial community, function prediction

INTRODUCTION

Aquaculture provided 80 million metric tons of fish for consumption in 2016 (FAO, 2018). Although cage and freshwater pond aquaculture produce the main aquatic products, industrial recirculating aquaculture systems (RAS) are expected to play a more important role in the future because of environmental and health concerns (Yogevis and Gross, 2019). In aquaculture systems,
1–2 kg of feed is consumed to produce 1 kg of fish products. Approximately 75% of the nitrogen in the feed is released to the culturing environment as total ammonia nitrogen (TAN, 56.2%), feces (13.8%), and non-consumed feed (5%) (Jackson et al., 2003; Hari et al., 2006; Hu et al., 2012). However, TAN at low concentration can be toxic to fishes and therefore must be continuously removed (Yoge and Gross, 2019).

Traditional RASs consist of particulate solid waste removal and TAN treatment (nitrification) plants (Liu et al., 2019). Some RASs (almost 23.4% of aquaculture production companies) also contain denitrification plants to achieve zero water discharge (Badiola et al., 2012; Liu et al., 2019). However, waste treatment plants complicate RAS and demand long payback time (average of 8 years) for establishment and maintenance (Badiola et al., 2012). Moreover, because of the opposing demands for dissolved oxygen (DO) and organic matter, implementing waste treatment in RAS through conventional autotrophic nitrification and anaerobic denitrification in actual ecosystems is difficult. Biofloc-based suspended growth reactor (SGR) has been recently developed as substitute for the complicated treatment plants (Azim and Little, 2008; Liu et al., 2019; Yogev and Gross, 2019). Through organic carbon addition and continuous aeration, bioflocs are generated in the SGR and nitrogen is removed from the effluent of fish tanks (De Schryver and Verstraete, 2009; Liu et al., 2016, 2019; Yogev and Gross, 2019). Moreover, biofloc biomass can be consumed by fishes and thus recovers nitrogen (Azim and Little, 2008).

The performance measures of biofloc-based SGRs under different conditions, such as carbon sources, carbon-to-nitrogen (C/N) ratio, and aeriation condition, were extensively studied (Liang et al., 2014; Luo et al., 2017b; Yogev and Gross, 2019). Biofloc systems usually require a C/N ratio of 15–20 (Avnimelech, 1999; Luo et al., 2017a). Microbial nitrogen assimilation was the most investigated process in biofloc systems because of the conversion of nitrogen waste into microbial protein, which can be used as fresh food for fishes (Gao et al., 2019). However, the nitrogen balance indicated that gaseous nitrogen loss, which is mainly caused by denitrification (\(\text{NO}_3^- \rightarrow \text{NO}_2^- \rightarrow \text{NO} \rightarrow \text{N}_2\)) (Hu et al., 2013), accounted for more than 60% of nitrogen input to the biofloc aquaculture system (Hu et al., 2014; Yogev and Gross, 2019); such loss can reduce the efficiency in nitrogen recovery. Given that high oxygen concentration (>5.0 mg L\(^{-1}\)) in aquaculture systems significantly inhibits the activity of traditional anaerobic denitrification enzymes, denitrification was assumed to occur only in the inner anoxic region of the bioflocs (Nootong et al., 2011; Hu et al., 2013). However, a novel group of aerobic denitrifying bacteria, which can perform denitrification under aerobic condition, has been recently discovered in tidal flow constructed wetlands (Tan et al., 2020), sequencing batch biofilm reactor (Wang et al., 2017; Pan et al., 2020), airlift reactor (Ruan et al., 2016), and sequencing batch reactor (Alzate Marin et al., 2016) for wastewater treatment. Many aerobic denitrifiers are also capable of heterotrophic nitrification (Wang et al., 2017; Tan et al., 2020). However, the complex microbial process of nitrogen removal in biofloc systems was still unclear.

In this study, biofloc-based RASs (BRASs) containing different C/N ratios were established to treat real aquaculture wastes and achieve zero water discharge. First, the water quality in the fish tanks and the nitrogen removal efficiency of the SGRs were evaluated. Second, the relative abundance of nar\(G\), nap\(A\), nir\(K\), nir\(S\), and nos\(Z\) genes were measured using quantitative polymerase chain reaction (qPCR) to evaluate the denitrifying function. Subsequently, the bacterial communities were investigated through Illumina high-throughput sequencing to identify the main functional microbes. In addition, PICRUSt analysis was performed to obtain a comprehensive insight into the metabolism pathway.

**MATERIALS AND METHODS**

**System Setup**

Two bench-scale BRASs were designed to achieve zero water discharge through a single SGR (Figure 1). Each system consists of a 40-L glass fish tank (30 L working volume) attached to a biofloc-based SGR. The SGR is composed of a 12-L continuously aerated reactor and a 5-L settler. Water, residual feeds, and feces from the fish tank were continuously pumped into the SGR at a rate of 0.5 L h\(^{-1}\) by a 5-W peristaltic pump (Kamoer Fluid Tech Co., Ltd., Shanghai, China). The generated biofloc in the settler returned to the aerated reactor because of gravity, and no biofloc biomass was removed during the entire experimental period. The treated water was recycled back to the fish tank. A 55-W air pump was used to perform aeration. The airflow rate was controlled using air flow meters (LZB-10, Senlod Co., Ltd., Nanjing, China) to maintain the high aerobic condition (approximately 5.0 mg L\(^{-1}\)). The fish tanks and SGRs were sealed to minimize water evaporation.

**Experimental Design**

Three weeks before the onset of the experiment, water containing bioflocs from a biofloc aquaculture system in Wuhan, China (30°32′48′′ N, 114°21′00″ E), was added to the SGRs of two BRASs for microbe seeding. The water quality of the inoculated water (IW) is shown in [**Table 1**](#). The initial total suspended solid (TSS) for the two BRASs was 380 mg L\(^{-1}\). The microstructure of the bioflocs was loose, with a diameter of approximately 600 μm (Supplementary Figure S1). Crucians (*Carassius auratus* gibelio) were stocked at 20 kg m\(^{-3}\). The two systems were conducted under natural light. High aeration (DO > 5.0 mg L\(^{-1}\)) and C/N ratio were set for the development of the biofloc during the 3-week start-up period (Table 1). The
Deng et al. Aerobic Denitrifiers in Biofloc System

FIGURE 1 | Schematic diagram of the zero-water discharge recirculating aquaculture system using a biofloc-based suspended growth reactor.

Fishes were fed daily with 15 g of commercial feed (Xiamen Fwuso Industry Co., Ltd., Xiamen, China) containing 35% protein and 4% fat. Commercial tapioca starch (Hengshuifu Bridge Starch Co., Ltd., Hebei, China) was also introduced into the SGRs of the two BRASs to reach a basic C/N (w/w) ratio of 16 (Avnimelech, 1999). During the 3-week start-up period, the inorganic nitrogen concentrations in both BRASs stabilized (1.1 and 1.8 mg L$^{-1}$ for TAN and NO$_3^-$-N, respectively, and daily change < 5%) for 1 week (Supplementary Figure S2). Then, the C/N ratio of the two systems was adjusted to 15 (CN15) and 20 (CN20). The details of the adjustment were provided in Supplementary Material. The systems were continuously run for another 35 days, and water samples from the different units (fish tank and SGR outlet) were collected every 2 days before feeding.

Water Quality Analysis
The TAN, NO$_2^-$-N, and NO$_3^-$-N concentrations were analyzed through spectrophotometry (Deng et al., 2018).

| Period (days) | Commercial feed (g) | Tapioca starch (g) | C/N |
|---------------|---------------------|--------------------|-----|
| Start-up*     | 21                  | 15.1 ± 0.0         | 17.4 ± 0.6 | 16  |
| CN15          | 35                  | 15.2 ± 0.2         | 14.3 ± 0.4 | 15  |
| CN20          | 35                  | 15.4 ± 0.5         | 25.3 ± 0.6 | 20  |

*A 3-week start-up period has been conducted in the CN15 and CN20 systems for the development of biofloc and stable of inorganic nitrogen concentration in both systems.

The total nitrogen concentration of the fish, commercial feed, and biofloc were detected using multi N/C 3100 TOC analyzer (Analytik Jena AG, Jena, Germany). The nitrogen mass balance of the two systems was calculated using the method proposed by Hu et al. (2014). The temperature, DO, pH, and electrical conductivity were measured on-site daily using an HQ30d YSI meter (YSI Inc., Yellow Spring, OH, United States). The toxic NH$_3$-N concentration in water was calculated in accordance with the approach of Emerson et al. (1975). The details are presented in Supplementary Material.

Microbial Community Analysis
Three IW samples were collected at the beginning of the start-up period. Water samples from the fish tanks and SGRs of the two systems (CN15 and CN20) were collected in triplicate at the end of the experiment and mixed and marked as IW, T15, T20, R15, and R20 for the subsequent analysis. The DNeasy<sup>®</sup> PowerSoil Kit (Qiagen, Hilden, Germany) was used to extract DNA. The primers 515F (5′-GTG CCA GCM GCC GCG GTA A-3′) and 806R (5′-GGA CTA CHV GGT WTC TAA T-3′) were used for bacterial 16S rRNA gene amplification. The library was constructed (Supplementary Material) and sequenced on an Illumina platform of Guangdong Magigene Biotechnology Co., Ltd. (Guangzhou, China) following the standard protocols. Phylogenetic classification and biodiversity analysis were conducted using the proposed technique of Deng et al. (2018). All raw sequencing data were stored in the Sequence Read Archive database (SRP267197).
Functional Gene qPCR and Functional Profile Prediction

The abundance of the key denitrifying genes for nitrate reduction (narG and napA) (Bru et al., 2007), nitrite reduction (nirS and nirK) (Chen et al., 2017), and NO₂ reduction (nosZ) (Henry et al., 2006), along with the bacterial 16S rRNA genes (He et al., 2017) in two BRAS, were assessed by qPCR. The primers, reaction system, and annealing temperatures are presented in Supplementary Table S2. The functional potential of the microbial community was predicted on the basis of the 16S rRNA sequences using PICRUSt (Langille et al., 2013), and the functional predictions were assigned according to the standard method¹. The Nearest Sequenced Taxon Index range (0.18–0.33) indicated relatively accurate predictions.

Statistical Analysis

IBM SPSS Statistics 21 was used for the statistical analysis. The water quality and functional genes were measured in triplicate and expressed as mean ± SD. ANOVA was used to determine the significant differences at p < 0.05.

RESULTS AND DISCUSSION

Water Quality in the Fish Tank

The experimental results show that the DO, temperature, and pH in the fish tanks were suitable for fish growth (Table 2). The TAN, NO₂⁻⁻N, and NO₃⁻⁻N concentrations in the fish tanks of CN15 and CN20 are shown in Figure 2. TAN, which comes from fish metabolism and uneaten feed and feces decomposition, is a major pollutant in the aquaculture system (Hu et al., 2012). Based on the daily feeding amount, the average TAN production in the fish tank was approximately 480 mg day⁻¹ (Hu et al., 2012; Supplementary Material). TAN can be oxidized into NO₂⁻⁻N and eventually NO₃⁻⁻N in aquaculture systems because of nitrification (Liu et al., 2019). Without water discharge, total inorganic nitrogen (TIN) concentrations accumulate in BRAS. However, the final TIN in the CN20 and CN15 systems was less than 9.8 and 32.5 mg L⁻¹, respectively, which indicated the high inorganic nitrogen removal potential in BRAS. Denitrification, which transforms NO₃⁻⁻N and NO₂⁻⁻N to N₂O and N₂ that are released to the air, is the main process that causes nitrogen loss in the BRAS (Hu et al., 2014). Given the high DO concentration (>5.0 mg L⁻¹) in the fish tank and SGR, the denitrification in this study was processed under aerobic conditions. In addition, increasing the C/N ratio from 15 to 20 significantly decreased the TAN, NO₂⁻⁻N, and NO₃⁻⁻N concentrations in the fish tank by 67.3, 79.8, and 77.3%, respectively. This finding indicated that increasing the C/N ratio can improve the denitrification potential in BRAS.

The NH₃⁻⁻N and NO₂⁻⁻N in the fish tank should be strictly controlled because both are toxic to fishes even at low concentrations (Sun et al., 2012; Yogev and Gross, 2019).

| Parameter | Mean | Standard error | Minimum | Maximum |
|-----------|------|----------------|---------|---------|
| Dissolved oxygen (mg L⁻¹) | 5.2  | 0.5            | 4.4     | 6.0     |
| EC (mS cm⁻¹)             | 0.9  | 0.4            | 0.4     | 1.9     |
| pH                     | 7.6  | 0.2            | 7.2     | 8.0     |
| Temperature (°C)        | 30.0 | 0.2            | 29.5    | 30.6    |

Therefore, the pollutants from the fish tanks were continuously treated in the SGR to avoid the accumulation of NH₃⁻⁻N and NO₂⁻⁻N in the fish tanks in long or short term. The calculated NH₃⁻⁻N concentrations in the fish tanks of CN15 and CN20 were 0.30 and 0.10 mg L⁻¹, respectively, which were significantly lower than the average acute toxicity concentration for 32 freshwater fish species (2.79 mg NH₃ L⁻¹) (Randall and Tsui, 2002). Although the CN15 system was NH₃ toxicity-free, the high TAN concentration (average of 12 mg L⁻¹) may still exert a negative effect on the immunity of the fishes during the long-term culturing period (Luo et al., 2014). The NO₂⁻⁻N concentration in the CN20 system was below 1.0 mg L⁻¹, whereas that in the CN15 system (2.3 mg L⁻¹) exceeded the prescribed concentration for aquaculture systems (<1.5 mg L⁻¹) (Yogev and Gross, 2019). The high NO₂⁻⁻N concentration in the fish tank of the CN15 system was caused by the imbalance of the nitrifying bacteria in the system, which will be discussed in section “Microbial Community Analysis.”

Nitrogen Removal Performance of SGR

The inorganic nitrogen removal efficiency of the SGRs with different C/N ratios is presented in Table 3. The TAN removal efficiency of the SGRs in both systems was lower than 25%, which slightly increased when the C/N ratio was increased from 15 to 20. A previous study reported the low TAN removal efficiency of a real SGR that treated aquaculture wastes (Liu et al., 2019). This unsatisfactory result can be attributed to the degradation of residual feeds and fish feces, which produced additional TAN in the SGR effluent (the details will be discussed in section “Microbial Functions”). Moreover, the high concentration of organic carbon in the SGR can inhibit the autotrophic nitrification activity (Ruan et al., 2016) and therefore reduce the TAN removal efficiency. In the CN20 system, the NO₂⁻⁻N concentration in the fish tank ranged from 0.2 to 0.8 mg L⁻¹, which was undetectable in the SGR effluent. The NO₂⁻⁻N concentration in the SGR effluent of the CN15 system was higher than that in the influent; such high concentration was mainly due to the incomplete nitrification and denitrification because NO₂⁻⁻N is the intermediate metabolite of both processes. The NO₃⁻⁻N and NO₂⁻⁻N removal efficiencies significantly increased when the C/N ratio was increased from 15 to 20 (p < 0.05), thereby indicating that a high amount of available carbon was beneficial to the aerobic denitrification in the SGR.

The nitrogen mass balances of the CN15 and CN20 systems during the entire experimental period (day 0 to day 56) were

¹http://picrust.github.io/picrust/
FIGURE 2 | The concentrations of total ammonia nitrogen (TAN), nitrite, and nitrate in the fish tank of the CN15 and CN20 systems. **p < 0.01; ***p < 0.001.

TABLE 3 | Nitrogen removal efficiency of SGR in the CN15 and CN20 systems.

|                | SGR influent (mg L⁻¹) |                      | SGR effluent (mg L⁻¹) |                      | Removal efficiency (%) |
|----------------|------------------------|-----------------------|-----------------------|-----------------------|------------------------|
|                | CN15                   | CN20                  | CN15                  | CN20                  | CN15                   | CN20                  |
| TAN            | 11.9 ± 2.6             | 3.9 ± 0.8             | 9.9 ± 4.8             | 3.0 ± 0.4             | 16.8%                  | 23.1%                 |
| NO₂⁻-N         | 2.3 ± 1.2              | 0.5 ± 0.3             | 2.7 ± 1.6             | 0.0 ± 0.0             | -17.4%*                | 100.0%                |
| NO₃⁻-N         | 17.7 ± 2.8             | 3.6 ± 1.4             | 14.8 ± 1.8            | 0.6 ± 0.8             | 16.4%                  | 83.3%                 |
| TIN            | 31.9 ± 0.5             | 8.0 ± 1.7             | 24.1 ± 5.2            | 3.7 ± 1.1             | 11.4%                  | 59.8%                 |

*Negative value means NO₂⁻-N concentration in effluent was higher than influent. TAN, total ammonia nitrogen; TIN, total inorganic nitrogen (TAN + NO₂⁻-N + NO₃⁻-N).

evaluated (Table 4). Fish feed was the main nitrogen input to both systems. The CN15 system had a higher amount of inorganic nitrogen retained in water than the CN20 system because of the high TAN, NO₂⁻-N, and NO₃⁻-N concentrations in the water (Figure 2 and Table 3). Increasing the C/N ratio increased the increments in the fish and biofloc biomasses. The gaseous nitrogen loss accounted for 72–75% of the nitrogen input, which was similar to the findings of Hu et al. (2014) at a C/N ratio of 16 (76% gaseous nitrogen loss). The gaseous nitrogen loss in the CN20 system was slightly lower than that in the CN15 one, because the denitrifiers in the former were hungrier than those in the latter during the experimental period (the influent NO₂⁻-N and NO₃⁻-N were less than 0.5 and 5.0 mg L⁻¹, respectively). These results indicated a high denitrification potential in the biofloc system because of the sufficient amount of organic carbon.

Microbial Community Analysis

The microbial community structures were further analyzed through high-throughput sequencing to investigate the difference in the inorganic nitrogen concentration and nitrogen removal efficiency in the BRASs with two different C/N ratios. A total of 97,884–338,198 high-quality sequencing tags were obtained, which corresponded to 1629–2136 operational taxonomic units (OTUs) (Table 5). The sequencing tags of IW were lower than those in the CN15 and CN20 systems. However, the obtained OTU and observed species were within the same range. The sequencing number for each sample was significantly higher than that in a previous research (Luo et al., 2017a), and the Chao1, Shannon, and Simpson indices of all samples reached stable values (Supplementary Figure S3), which indicated that the sequencing depth of the present study is sufficient to reflect the microbial community abundance and diversity. As shown in Table 5, the α-diversity (Chao1 richness and Shannon and Simpson diversity indices) of the samples in the CN20 system (T20 and R20) was higher than that in the CN15 system (T15 and R15). This result suggested that increasing...
the C/N ratio can enhance the microbial diversity of BRAS. The rich bacterial diversity in a system can result in a highly efficient nitrogen removal process (Ebeling et al., 2006). This inference is consistent with the lower TAN, NO$_2^-$-N, and NO$_3^-$-N concentrations of the CN20 system than the CN15 one (Figure 2).

The high-quality OTUs were annotated at phylum and genus levels, and those with a relative abundance higher than 1% are shown in Figure 3. **Proteobacteria** (58.9%) and Bacteroidetes (16.7%) were the predominant phyla in the IW and Proteobacteria (35.8 ± 2.0%), Deinococcus–Thermus (22.5 ± 3.9%), Bacteroidetes (17.6 ± 0.8%), and Planctomycetes (14.3 ± 2.8%) were the dominant ones in the fish tank and SGR in the CN15 system. The predominant phyla in the fish tank in the CN20 system included Proteobacteria (31.1%), Bacteroidetes (23.1%), Firmicutes (13.16%), and Planctomycetes (12.2%), whereas those in the SGR were Proteobacteria (68.0%) and Bacteroidetes (11.8%). The Proteobacteria in R20 was 2.0, 1.8, and 2.2 times higher than in T15, R15, and T20, respectively, which implied the high aerobic denitrification potential in the SGR of the CN20 system because aerobic denitrifying bacteria mainly belonged to this phylum (Chen et al., 2018).

Twenty-eight predominant genera (>1%) were retrieved at the genus level (Figure 3B). Different nitrifiers and denitrifiers, which play key roles in the biological nitrogen removal process, are displayed in Figure 4. For the nitrifiers, **Nitrosomonas** (0.7–21%) was the only detected ammonia-oxidizing bacteria (AOB), and its abundance in R20 was 3.1 times higher than in R15 (Figure 4A). The relative abundance of phyla **Nitrospinae** and **Nitrosira**, which are nitrite-oxidizing bacteria (NOB), was extremely low (<0.1%). The AOB/NOB ratio in R15 and R20 was 14 and 24, respectively (Figure 4A). The relative abundance of NOB (autotrophic) in the CN15 and CN20 systems was lower than that in IW, which might because of the growth of heterotrophic bacteria in the two systems.

Azim and Little (2008) reported that *Nitrosomonas* is the dominant AOB species in aquaculture systems, and the addition of organic matter can enhance its abundance of *Nitrosomonas*. The high AOB/NOB ratio was consistent with the increase in NO$_2^-$-N concentration in the SGR effluent of the CN15 system (Table 3), suggesting that partial nitrification is the main process for the TAN removal in this system. Although the AOB/NOB ratio in R20 was 1.7-fold higher than that in R15, no NO$_2^-$-N accumulation was observed in the SGR of the CN20 system. To some extent, this may be the result of the significant increase in the aerobic denitrifiers in the SGR.

For the denitrifiers, *Rubrivivax* (phylum *Proteobacteria*) was the predominant genus (7.0–8.5%) in the CN15 system, and *Flavobacterium* (phylum *Bacteroidetes*), *Dechloromonas* (phylum *Proteobacteria*), and *Rhodobacter* (phylum *Proteobacteria*) were enhanced in the CN20 system (Figure 4B). *Zoogloea* (phylum *Proteobacteria*) dominated in IW and R20. The total abundance of abovementioned denitrifiers in the CN15 (8.1 and 9.5% for T15 and R15, respectively) and CN20 systems (11.1 and 10.1% for T20 and R20, respectively) was higher than that in IW (4.5%). The high AOB/NOB ratio and the increase in the NO$_3^-$-N concentration in the SGR effluent indicated the partial nitrification process in the CN15 system. *Rubrivivax* sp. (facultative–anaerobic denitrifying bacteria) was the main denitrifying bacteria in the CN15 system (87.6 ± 1.2% of the denitrifiers); such bacteria can transform NO$_2^-$-N to N$_2$ without using NO$_3^-$-N as an electron acceptor (Zhang et al., 2016) because of the deficiency in nitrate reductase (Nagashima et al., 2012). These results implied that the partial nitrification and denitrification (PND, NH$_4^+$-N → NO$_2^-$-N → NO → N$_2$O → N$_2$) may be the main nitrogen removal process in the CN15 system.

The denitrification process in the CN20 system was mainly performed by aerobic denitrifying bacteria (Dechloromonas, *Rhodobacter, Flavobacterium*, and Zoogloea). *Dechloromonas* exhibited an excellent aerobic denitrification ability in tidal flow constructed wetland and was the dominant denitrifying and phosphorus-removing bacteria in the single-sludge sequencing batch reactor (Xu et al., 2018; Tan et al., 2020). *Rhodobacter* demonstrated enhancement in the single reactor for nitrogen removal under aerobic conditions (Chen et al., 2018). *Flavobacterium* (phylum *Bacteroidetes*) served as a complete aerobic denitrifier in the granular reactor (Pishgar et al., 2019). The amount of *Zoogloea*, which is correlated with biofloc formation (Weissbrodt et al., 2013) and facilitates aerobic denitrification (Huang et al., 2015; Pishgar et al., 2019), was increased in R20. In addition, *Dechloromonas, Flavobacterium*, and *Zoogloea* also displayed heterotrophic nitrification ability; therefore, it can conduct heterotrophic nitrification and aerobic denitrification (Huang et al., 2015; Pishgar et al., 2019; Tan et al., 2020). These results indicated the coexistence of autotrophic nitrification and heterotrophic nitrification in the CN20 system. Aerobic denitrifying bacteria (9.6–10.6% of the total bacteria) accounted for more than 95% of the denitrifying bacteria, thereby indicating that aerobic denitrification was the main process of denitrification in the CN20 system.

**Key Functional Genes of Denitrification**

The key enzymes secreted by denitrifying bacteria, such as nitrate reductase (including NAR and NAP), nitrite reductase, and nitrous oxide reductase, are encoded using the corresponding functional genes. For nitrate reduction, the NAR encoded by narG is seriously inhibited by oxygen, whereas the NAP encoded by napA can be expressed under aerobic and anaerobic conditions (Sparacino-Watkins et al., 2014; Pan et al., 2020). The expression of the napA gene was often applied as an evidence...
of aerobic denitrification (Chen et al., 2018). The enzymes that catalyze the reduction of \( \text{NO}_2^- \) to NO are encoded by \( \text{nirK} \) and \( \text{nirS} \) genes. Some \( \text{nirK} \) gene clusters in the denitrifying bacteria are similar to their homologs in the aerobic nitrifying bacteria in terms of sequence and organization and thus could be functional under aerated conditions (Cantera and Stein, 2007). The final step of denitrification is the catalysis by \( \text{N}_2\text{O} \) reductase, which is encoded by the \( \text{nosZ} \) gene, such catalysis is uniform in the aerobic and anaerobic denitrifiers (Deng et al., 2019).

To obtain a deep insight into the aerobic and anaerobic denitrification in BRAS, the relative abundance of the representative functional genes that encode the key denitrification enzymes was quantified through qPCR (Figure 5). For the nitrate reductase genes, the relative abundance of \( \text{napA} \) in T20 and R20 was 3.0 and 4.6 times higher than that in T15 and T20, respectively. A 1.5-fold increase was observed in the \( \text{narG} \) level in R20 (\( p < 0.05 \)). For the nitrite reductase genes, the relative abundances of the \( \text{nirK} \) gene in T20 and R20 showed a 2.6-fold increase compared with those in T15 and R15. In addition, the relative abundance of the \( \text{nirS} \) gene was 3.1-fold higher in R20 than in R15. For the \( \text{N}_2\text{O} \) reduction, increasing the C/N ratio from 15 to 20 significantly elevated the relative abundance of \( \text{nosZ} \) in the fish tank and SGR. Deng et al. (2019) reported that \( \text{napA} \), \( \text{nirK} \), and \( \text{nosZ} \) genes exhibited high oxygen tolerance and maintained aerobic denitrification. Hence, increasing the C/N ratio can provide additional electron donors for denitrification and increase the aerobic denitrification-related functional genes (\( \text{napA} \), \( \text{nirK} \), and \( \text{nosZ} \)) in the fish tank and SGR. The high amount of available organic carbon in the SGR of the CN20 system increased the heterotrophic biofloc biomass in SGR and provided the anaerobic environment for the expression of anaerobic denitrification-related functional genes (\( \text{narG} \) and \( \text{nirS} \)). These findings can explain the high nitrogen loss (\( \text{N}_2 \) emission) in the biofloc-based aquaculture system (Hu et al., 2014; Yogev and Gross, 2019). Furthermore, these results indicated that increasing the C/N ratio of the biofloc-based SGR can significantly increase aerobic and anaerobic denitrification.

**Microbial Functions**

The predicted functional potential of the microbial community in the CN15 and CN20 systems is illustrated in Figure 6. The functional potential of the microbial community in IW was not presented because of the relative low sequencing tags compared with those of the CN15 and CN20 systems. The PICRUSt results at the Kyoto Encyclopedia of Genes and Genomes Ortholog (KO) hierarchy level 1 demonstrated that metabolism (49.3–50.2%), genetic information processing (16.6–18.7%), and environmental information processing (12.7–13.5%) were the major microbial processes in both BRASs. At the KO hierarchy level 2, the most abundant functions included carbohydrate, energy, and amino acid metabolisms; membrane transport; and replication and repair, all of which were strengthened in R20.

The high C/N ratio in the SGR of the CN20 system was conducted through the addition of organic carbon source,
which increased the carbohydrate metabolism (e.g., starch and sucrose metabolism and tricarboxylic acid cycle) in R20. This metabolism played an important role in degrading complex organic molecules (e.g., residual feeds, fish feces, and tapioca starch) into easily degradable substances to provide organic carbon sources for denitrifiers (Wei et al., 2018), which was consistent with the high energy metabolism (e.g., methane and nitrogen metabolisms) in R20 that provides energy for other
The increase in the membrane transport, replication, and repair indicated a high substance exchange (including nitrogen nutrient) in the bacterial cell, as well as a high bacterial activity in the SGR of the CN20 system. The increase in the amino acid metabolism increased the ammonia assimilation (Wu et al., 2017) and consequently improved the nitrogen removal efficiency in the CN20 system. Furthermore, the amino acid metabolism enabled bacteria to degrade residual feeds and feces and produce TAN, which may be the reason for the low TAN removal efficiency (<25%) in the SGR of the CN20 system (Table 3). These results indicated that increasing the C/N ratio can improve the nitrogen removal efficiency in SGR by increasing the carbohydrate, energy, and amino acid metabolisms.

**CONCLUSION**

In this study, an RAS that uses a biofloc-based SGR for aquaculture waste treatment was constructed. Results showed that increasing the C/N ratio from 15 to 20 can significantly improve the water quality in the fish tank and enhance the nitrogen removal efficiency in the SGR by adjusting the microbial community structure and nitrogen removal pathway. PND was the main nitrogen removal pathway in the CN15 system. Autotrophic and heterotrophic nitrification coexisted in the CN20 system, and aerobic denitrification was the main denitrification process. The carbohydrate, energy, and amino acid metabolisms, along with membrane transport and replication...
and repair, were the key microbial processes that improved the nitrogen removal efficiency in the SGR of the CN20 system.

DATA AVAILABILITY STATEMENT

The datasets generated for this study can be found in the online repositories. The names of the repository/repositories and accession number(s) can be found at: https://www.ncbi.nlm.nih.gov/, SRP267197.

AUTHOR CONTRIBUTIONS

MD: conceptualization, software, data curation, and writing – original draft. ZD and YS: formal analysis. LL: writing – review and editing. KS: conceptualization and project administration. XH: conceptualization. All authors contributed to the article and approved the submitted version.

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SUPPLEMENTARY MATERIAL

The Supplementary Material for this article can be found online at: https://www.frontiersin.org/articles/10.3389/fmicb.2020.01760/full#supplementary-material
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**Conflict of Interest:** The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.