Nonlinear Dynamic Process Monitoring Based on Ensemble Kernel Canonical Variate Analysis and Bayesian Inference
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ABSTRACT: By considering autocorrelation among process data, canonical variate analysis (CVA) can noticeably enhance fault detection performance. To monitor nonlinear dynamic processes, a kernel CVA (KCVA) model was developed by performing CVA in the kernel space generated by kernel principal component analysis (KPCA). The Gaussian kernel is widely adopted in KPCA for nonlinear process monitoring. In Gaussian kernel-based process monitoring, a single learner is represented by a certain selected kernel bandwidth. However, the selection of kernel bandwidth plays a pivotal role in the performance of process monitoring. Usually, the kernel bandwidth is determined manually. In this paper, a novel ensemble kernel canonical variate analysis (EKCVA) method is developed by integrating ensemble learning and kernel canonical variate analysis. Compared to a single learner, the ensemble learning method usually achieves greatly superior generalization performance through the combination of multiple base learners. Inspired by the ensemble learning method, KCVA models are established by using different kernel bandwidths. Further, two widely used $T^2$ and $Q$ monitoring statistics are constructed for each model. To improve process monitoring performance, these statistics are combined through Bayesian inference. A numerical example and two industrial benchmarks, the continuous stirred-tank reactor process and the Tennessee Eastman process, are carried out to demonstrate the superiority of the proposed method.

1. INTRODUCTION
Recent developments in the field of process monitoring have led to a renewed interest in ensuring operation safety in the process industry. Model-based and data-driven methods are the two sorts of process monitoring strategies in general. Accurate process models, which are typically difficult to generate for complicated industrial processes, are required for model-based techniques. Data-driven methods, unlike model-based methods, rely solely on process data. A massive amount of process data can be captured, stored, and analyzed because of the rapid advancement of information, communication, and computing technology. As a result, data-driven process monitoring has triggered an amount of innovative inquiry.

The multivariate analysis (MVA) approach has been widely used and explored among data-driven process monitoring methods for its simplicity and adaptability. Representative MVA methods include principal component analysis (PCA), partial least-squares (PLS), and canonical variate analysis (CVA). In PCA, features are extracted from process data by maximizing the variance in the projection space. To address the shortcomings of the standard PCA, Rohoma et al. suggested two methods for evaluating sparse principal components. These two approaches surpass PCA in threshold determination because they use resampling and measurement error covariance matrices to obtain the distribution of the loading components. Furthermore, Yu et al. suggested a nonlinear, robust, and sparse PCA by using Spearman’s and Kendall’s correlation matrices. PLS is usually employed in quality-related process monitoring. PLS concentrates on maximizing the covariance between input and output variables. However, many theoretical researchers have found that these two methods do not satisfy these conditions of temporal correlation and autocorrelation of most industrial data. To settle this issue, PCA and PLS have been extended to dynamic versions by using time-lagged process variables. In addition, the construction of a graphical framework based on the PCA algorithm using a Bayesian network can also realize the dynamic connection between data.

Different from PCA and PLS, as a variant of canonical correlation analysis (CCA), canonical variate analysis (CVA)
attempts to extract the state-space from process variables. Hence, CVA is more suitable for monitoring dynamic processes. More recently, CVA-based process monitoring methods have attracted much attention in process monitoring.\textsuperscript{16,17} Juricek et al. used a local approach to detect changes in the canonical variable coefficients which are extracted from the built CVA model.\textsuperscript{18} Odiowei and Cao\textsuperscript{9} constructed a minimum state-space model using CVA to derive the state variable and residual canonical variates, and employed kernel density estimations (KDE) to establish the upper control limits to deal with the nonlinearity and non-Gaussian issues for process monitoring. Jiang and Braatz\textsuperscript{20} improved the interpretability of fault detection by using correlation features that provide a more efficient representation of process features and reduce redundancy to space compared to raw data. Lu et al.\textsuperscript{2} employed a sparse CVA (SCVA) to generate sparse canonical variates to explore the major structures among process variables for process monitoring. A new metric to quantify the dissimilarity of past and future data was proposed by Pilario and Cao.\textsuperscript{21} The new index is more reliable than the CVA $T^2$ and $Q$ index for detecting incipient faults. Li et al.\textsuperscript{22} pointed out that taking into account the residuals of the canonical variant produces a more reliable and interpretable contribution plot than contribution maps based on $T^2$ and $Q$ statistics from the CVA for detecting faults that evolve slowly. Zhong and Zhao\textsuperscript{23} combined CVA and slow feature analysis (SFA) to achieve the separation of process static and dynamic information, which better explains the process dynamics of the system.

However, the above CVA-based process monitoring methods would fail to detect faults efficiently for nonlinear processes owing to the assumption that the process variables are linear related. To address this issue, kernel methods have been widely adopted to extend linear MVA methods to nonlinear MVA methods.\textsuperscript{24} Ciabattoni et al. combined kernel canonical variate analysis (KCVA) and kernel density estimation (KDE) to develop a nonlinear monitoring method for detecting faults and occupant bad behaviors for a residential microgrid application.\textsuperscript{25} Xiao et al. integrated locality preserving projections into KCVA to retain local manifold structure in kernel space for fault detection.\textsuperscript{26} In the research of Shang et al.,\textsuperscript{27} the exponential weighted moving average approach is used to update the covariance in the feature space after changing the operating conditions. The first-order perturbation theory is used to decrease the calculation of Hankel matrix singular value decomposition in high-dimensional eigenspace. To reduce the storage and computational expense, Yu et al. presented accelerated KCVA for fault isolation by applying full rank factorization incorporated in kernel matrix approximation.\textsuperscript{28} A limitation of applying the KCVA to nonlinear dynamic systems is that a singular kernel matrix may be involved, particularly for industrial processes, since the process variables are often colinear. To solve this issue, Samuel and Cao\textsuperscript{30} performed CVA in the kernel space created by KCRA. The singularity problem can be avoided owing to the compression of KCRA.

Only a single Gaussian kernel function is used in kernel-based process monitoring approaches such as KPCA and KCVA. The width parameters, on the other hand, are calculated empirically. Thus, the detection performance may be significantly degraded if an unfit Gaussian kernel function is selected while fault information is unavailable.\textsuperscript{31} As a class of combinatorial optimization learning methods, the ensemble learning (EL) method can derive better performance by combing multiple simple models.\textsuperscript{31} To enhance the process monitoring performance, Li and Yang, through the analysis of a nonlinear numerical example, pointed out that a single KPCA model can hardly meet the needs of the overall monitoring. Therefore, a new approach is proposed where multiple KPCA models are combined with a Bayesian inference strategy to obtain a new metric.\textsuperscript{32} Cui et al.\textsuperscript{33} further considered both global and local structure information on the original data and preserved the local information in the based KPCA models before performing ensemble learning.

Several nonlinear dynamic process monitoring approaches, such as DKPCA and KCVA, have recently been presented. The correlation relationship between process variables is investigated by KCVA. DKPCA, on the other hand, solely considers the variance information on process variables. The relationship between process variables is not taken into account. Yet, the kernel parameter is hard to determine. Moreover, only a single model is derived for one kernel parameter. Inspired by EDKPCA which combined ensemble learning and DKPCA, in this work, the KCVA is extended to ensemble KCVA by integrating the ensemble learning strategy into KCVA. Due to the merits of ensemble learning and KCVA, the dynamics and nonlinearity of complex industrial processes can be better presented for process monitoring. First, the KPCA models with different kernel parameters are established to extract the kernel principal components. Then, CVA is performed in each kernel principal component space, and $T^2$ and $Q$ statistics are constructed. The corresponding thresholds are determined by KDE. For nonlinear dynamic process monitoring, a Bayesian combination strategy is employed to integrate these monitoring statistics to take advantage of these CVA models. Two widely employed case studies are presented to demonstrate the performance of the proposed EKCVA compared to other related methods.

The main contribution and novelty of this article lie in the following aspects:

- Ensemble learning approach is introduced to KCVA to improve the process monitoring performance. Through several base KPCA learners, the nonlinear characteristics of nonlinear dynamic processes are better described.
- Meanwhile, by taking the autocorrelation and cross-correlation into consideration, the proposed EKCVA method can present superior fault detection performance for nonlinear dynamic processes.
- A Bayesian inference strategy is adopted to define a single fault detection index to facilitate the fault detection logic.

The remainder of this work is organized as follows. Section 2 briefly recalls the KPCA and CVA methods. Section 3 describes in detail the proposed methodology and how the ensemble idea is applied. Section 4 tests the effectiveness of the proposed approach using a numerical example, the CSTR process, and the widely accepted industry benchmark TEP and analyzes the results. In the final section, we summarize the approach of this paper and provide an outlook on future work in the context of the experimental results.

2. BRIEF REVIEW OF KPCA AND CVA

2.1. KPCA. The general idea of KPCA is to perform PCA in a reproducing kernel Hilbert space. First, all original data samples are mapped to a high-dimensional space (called feature space) using a nonlinear mapping. Then, linear PCA is performed as a dimension reduction technique to extract features in this high-dimensional space.\textsuperscript{34,35} Given an input data matrix $X = [x_1, x_2, \ldots, x_n] \in \mathbb{R}^{n \times m}$ collected at $n$ time points for $m$ variables. A nonlinear function
\( \Phi(\bullet) \) is employed to map the original data \( X \) into a high-dimensional feature space \( \mathbf{H} \),

\[
\mathbb{R}^n \xrightarrow{\Phi(\bullet)} \mathbf{H}
\]

Assuming that \( X \) has been centralized, the covariance matrix of the high-dimensional feature space is constructed as

\[
C = \frac{1}{n} \sum_{i=1}^{n} [\Phi(x_i)][\Phi(x_i)]^T
\]

Then, in the feature space \( \mathbf{H} \), PCA is conducted by solving the eigenvalue problem,

\[
\lambda \omega = C \omega
\]

Here, \( \lambda \) and \( \omega \) are the eigenvalue and eigenvector of the matrix \( C \), respectively. The eigenvector \( \omega \) can be represented through a linear combination of mapped data points with a series of coefficients \( \beta_j (j = 1, \ldots, n) \),

\[
\omega = \sum_{j=1}^{n} \beta_j \Phi(x_j)
\]

By multiplying both sides of eq 3 by \( \Phi(x_k)^T (k = 1, \ldots, n) \), it yields,

\[
\lambda \beta_k < \Phi(x_k), \Phi(x_k) > = \frac{1}{n} \sum_{i=1}^{n} \alpha_j < \Phi(x_i), \Phi(x_i) > < \Phi(x_k), \Phi(x_k)>
\]

where \( < \bullet, \bullet > \) represents the inner product operator. Generally, although the mapping \( \Phi(\bullet) \) exists, it may not always be computationally accessible. To avoid such explicit mappings, the use of kernel functions has become popular. Thus, an \( n \times n \) kernel matrix \( K_n \) is defined. Further, the centering operation on kernel matrices is performed,

\[
K_n = K_n - \frac{1}{n} \sum_{i=1}^{n} \phi(x_i) (i = 1, \ldots, n)
\]

The eigenvalue decomposition problem eq 5 is rewritten as,

\[
n \lambda \beta = K \beta
\]

where \( \beta = [\beta_1, \ldots, \beta_n]^T \) is the eigenvector of the kernel matrix \( K_n \) with corresponding eigenvalues \( \lambda_1, \ldots, \lambda_n \).

2.2. CVA. CVA is a technique for reducing dimensions that has been extensively researched in the field of process monitoring.\(^{36,37}\) For the purpose of taking the autocorrelation into consideration, the past and future vectors \( x_{p,k} \) and \( x_{f,k} \) are constructed. With a time-lag number \( l \), \( x_{p,k} \) and \( x_{f,k} \) are constructed as

\[
x_{p,k} = [x_{p,k-l}, x_{p,k-l+1}, \ldots, x_{p,k}] \in \mathbb{R}^{ml}
\]

Then, the past and future Hankel matrices \( X_p \) and \( X_f \) are obtained,

\[
X_p = [x_{p,l+1}, x_{p,l+2}, \ldots, x_{p,l+N}] \in \mathbb{R}^{ml \times N}
\]

\[
X_f = [x_{f,l+1}, x_{f,l+2}, \ldots, x_{f,l+N}] \in \mathbb{R}^{ml \times N}
\]

where \( N = n - 2l + 1 \). The overall estimates of the sample-based covariance and cross-covariance matrices of the past and future vectors are calculated,

\[
\Sigma_{pp} = \frac{1}{N-1} [X_p X_p^T]
\]

\[
\Sigma_{pf} = \frac{1}{N-1} [X_f X_p^T]
\]

To gain the best correlated linear combination of past and future observations, a singular value decomposition (SVD) is computed on the following Hankel matrix \( H \).\(^{38}\)

\[
H = \Sigma_{pp}^{-1/2} \Sigma_{pp}^{-1/2} = U \Lambda V^T
\]

Here, \( U \) and \( V \) are the left and right singular matrices of \( H \), respectively. \( \Lambda = \text{diag} [\sigma_1, \sigma_2, \ldots, \sigma_q] \) is a diagonal matrix containing all singular values, and \( q \) is the rank of \( H \).

For dimensionality reduction, \( U_w \in \mathbb{R}^{m \times l} \) and \( V_w \in \mathbb{R}^{m \times l} \) contain the first \( w \) columns of \( U \) and \( V \), respectively. Thus, the weight matrices \( J \) and \( L \) are derived,

\[
J = V_w^T \Sigma_{pp}^{-1/2} \in \mathbb{R}^{m \times ml}
\]

\[
L = (I - V_w V_w^T) \Sigma_{pp}^{-1/2} \in \mathbb{R}^{ml \times ml}
\]

Finally, the state variables and the residuals are derived from the past vector matrix, respectively,

\[
Z = JX_p \in \mathbb{R}^{w \times n}
\]

\[
E = LX_f \in \mathbb{R}^{ml \times n}
\]

3. PROPOSED EKPCA-BASED PROCESS MONITORING

3.1.EKPCA Model. To overcome the limitation that a singular kernel matrix may be involved, KPCA is performed before exploring the correlation relation in process variables. In KPCA, the Gaussian kernel function is widely employed for process monitoring which is established,

\[
k(x, y) = \exp(-||x - y||^2/h)
\]

where \( h \) is the kernel width. A specific \( h \) will only generate a single model. Although different methods for selecting an optimal \( h \) for process monitoring have been devised, the problem remains unsolved.\(^{35}\) For the improvement of process monitoring performance, Li et al.\(^{37}\) applied ensemble learning to the KPCA method. Inspired by this idea, we also adopt ensemble learning in the proposed EKPCA.

To do so, multiple Gaussian kernel functions are defined,

\[
k^{(i)}(x, y) = \exp(-||x - y||^2/h_i)
\]

where \( h_i = 2^{-i} \sigma \), and \( i = 1, \ldots, n\), represents the \( i \)th submodel, and \( n \) stands for the ensemble size.

The training data set is denoted by \( X = [x_1, x_2, \ldots, x_n] \in \mathbb{R}^{w \times m} \). For each submodel, the kernel matrix \( K^{(i)} \) is computed by \( K^{(i)} = k(X, X) \). \( K^{(i)} \) denotes the centered kernel matrix of the \( i \)th submodel which is computed as eq 6. Now, performing KPCA in high-dimensional space is equivalent to solving the eigenproblem of eq 16.
Based on the constructed Hankel matrices \( \tilde{Y}_i^{(0)} \) and \( \tilde{Y}_{i}^{(1)} \), the transformation matrices \( \mathbf{J}^{(0)} \) and \( \mathbf{L}^{(0)} \) are estimated by performing SVD on the scaled Hankel matrix,

\[
\mathbf{H}^{(0)} = \mathbf{K}^{(0)}_n \mathbf{K}^{(0)}_n = \mathbf{S}^{(0)} \mathbf{S}^{(0)} = \mathbf{U}^{(0)} \Lambda^{(0)} \mathbf{V}^{(0)\top}
\]

(19)

where \( \Sigma^{(i)}_{f_f} \) and \( \Sigma^{(i)}_{y} \) can be calculated in a similar way to eq 10. The transformation matrices \( \mathbf{J}^{(0)} \) and \( \mathbf{L}^{(0)} \) are calculated by retaining the first \( w \) singular vectors with dominant singular values,

\[
\mathbf{J}^{(i)} = \mathbf{V}^{(i)} \Sigma^{(i)}_{y} \mathbf{V}^{(i)} \mathbf{T}^{(i)} \mathbf{T}^{(i)} = \mathbf{R}^{w \times d}
\]

(20)

\[
\mathbf{L}^{(i)} = (\mathbf{I} - \mathbf{V}^{(i)} \Sigma^{(i)}_{y} \mathbf{V}^{(i)} \mathbf{T}^{(i)} \mathbf{T}^{(i)}) \in \mathbf{R}^{d \times d}
\]

Thus, the state variables and residual variables \( \tilde{Z}^{(i)} \) and \( \tilde{E}^{(i)} \) of the \( i \)th submodel are estimated,

\[
\tilde{Z}^{(i)} = \mathbf{J}^{(i)} \mathbf{Y}^{(0)} \in \mathbf{R}^{N \times d}
\]

(21)

\[
\tilde{E}^{(i)} = \mathbf{L}^{(i)} \mathbf{Y}^{(0)} \in \mathbf{R}^{N \times d}
\]

3.2. EKCVA-Based Process Monitoring. Offline modeling and online monitoring are two stages of the data-driven process monitoring strategy. The EKCVA model is developed utilizing the acquired samples under normal operating conditions in the offline modeling stage. With a chosen confidence level, the relevant upper control limits are determined. For online monitoring, the statistics of the newly collected samples are constructed and compared to the upper control limits. While the online monitoring statistic is over the corresponding upper control limit, an alarm is triggered to indicate the occurrence of a fault.

Two commonly used statistical metrics for fault detection are the \( T^2 \) statistic and \( Q \) statistic.\(^3\) For the \( i \)th submodel as expressed in eq 20, the monitoring \( T^2 \) and \( Q \) statistics are established from \( \tilde{Z}^{(i)} \) and \( \tilde{E}^{(i)} \),

\[
\mathbf{T}_{k}^{(i)} = \sum_{j=1}^{w} z_{j,k}^{(i)2}
\]

(22)

\[
\mathbf{Q}_{k}^{(i)} = \sum_{j=1}^{d} e_{j,k}^{(i)2}
\]

where \( z_{j,k}^{(i)} \) and \( e_{j,k}^{(i)} \) are the elements of the \( j \)th row and \( k \)th column of the \( \tilde{Z}^{(i)} \) and \( \tilde{E}^{(i)} \) matrices.

Usually, the Gaussian distribution assumption would be violated in practice. Thus, it is inappropriate to calculate the upper control limits from \( F \)-distribution and \( \chi^2 \) square distribution for the established \( T^2 \) and \( Q \) statistics. To determine the upper control limits, the widely used kernel density estimation (KDE) is employed in this study. In KDE, a smoothed peak function (kernel) is used to estimate the probability density functions (PDF) from the observed data points curve.\(^34,39,40\) Thus, the Gaussian distribution assumption of process data is not necessary. Taking the \( T^2 \) as an example, the PDF of the calculated \( N \) \( T^2(k) \), \( k = 1, ..., N \) statistics is estimated as

\[
p(T^2) = \frac{1}{N h} \sum_{j=1}^{N} K \left( \frac{T^2 - T^2(j)}{d} \right)
\]

(23)
where $d$ is the kernel bandwidth, and $\mathcal{K}(\cdot)$ is the kernel function. A rough estimate of the optimal bandwidth is based on an approximation of the minimized mean squared error of integration. Usually, the kernel function $\mathcal{K}(\cdot)$ is defined,

$$
\mathcal{K}(g) = \frac{1}{\sqrt{2\pi}} \exp\left(-\frac{g^2}{2}\right)
$$  (24)

Then, for a given confidence level $\alpha$, the upper control limits of $T^{2(i)}$ and $Q^{0(i)}$ can be computed for the $i$th submodel by solving the following equations,

$$
P(T^{2(i)} < T^{2}_{\text{limit}}) = \int_{-\infty}^{T^{2}_{\text{limit}}} p(T^{2(i)}) \, dT^{2(i)} = \alpha
$$  (25)

$$
P(Q^{0(i)} < Q^{0}_{\text{limit}}) = \int_{-\infty}^{Q^{0}_{\text{limit}}} p(Q^{0(i)}) \, dQ^{0(i)} = \alpha
$$  (26)

While a new sample $x_i \in \mathbb{R}^n$ is collected, the centralized Gaussian matrix is calculated through a nonlinear mapping: $x_i \rightarrow \phi(x_i)$,

$$
\begin{align*}
\kappa_i &= \phi(x_i)\Phi(\mathbf{X})^T \\
\tilde{\kappa}_i &= \kappa_i - 1_n, \kappa = \kappa_1 + 1_n, \kappa_n
\end{align*}
$$  (27)

where $1_n = 1/\mu[1, \ldots, 1] \in \mathbb{R}^1$. For the $i$th submodel, the projection of the test sample after performing KPCA is

$$
y^{(i)}_t = \mathbf{S}^{(i)} \tilde{\kappa}_i
$$  (28)

Then, two statistics $T^{2(i)}(i = 1, \ldots, n)$ and $Q^{0(i)}(i = 1, \ldots, n)$ can be constructed for the $i$th KPCA submodel.

To take the monitoring results of all submodels into consideration and enhance the interpretation of the final monitoring results, the Bayesian inference strategy is used to convert the monitoring results into fault probabilities of each submodel. For this purpose, the fault probabilities of the two monitoring statistics are calculated,

$$
P_t^{(i)}(F|x) = \frac{p_t^{(i)}(F|x) p_t^{(i)}(F)}{p_t^{(i)}(x)}
$$  (29)

$$
P_{Q_t}^{(i)}(F|x) = \frac{p_{Q_t}^{(i)}(F|x) p_{Q_t}^{(i)}(F)}{p_{Q_t}^{(i)}(x)}
$$  (30)

where $N$ denotes the normal state and $F$ denotes the fault state. The prior probability terms $p_t^{(i)}(N), p_{Q_t}^{(i)}(N), p_t^{(i)}(F),$ and $p_{Q_t}^{(i)}(F)$ are determined as $1 - \alpha$. Meanwhile, $p_{t}^{(i)}(N)$ and $p_{Q_t}^{(i)}(N)$ are equal to $\alpha$. The likelihood terms $P_t^{(i)}(x|N), P_{Q_t}^{(i)}(x|N), P_t^{(i)}(x|F),$ and $P_{Q_t}^{(i)}(x|F)$ are determined as,

$$
P_t^{(i)}(x|N) = \exp(-T^{2(i)}_{\text{limit}}/T^{2(i)}_{\text{limit}})
$$  (31)

$$
P_t^{(i)}(x|F) = \exp(-T^{2(i)}_{\text{limit}}/T^{2(i)}_{\text{limit}})
$$  (32)

$$
P_{Q_t}^{(i)}(x|N) = \exp(-Q^{0}_{\text{limit}}/Q^{0}_{\text{limit}})
$$  (33)

$$
P_{Q_t}^{(i)}(x|F) = \exp(-Q^{0}_{\text{limit}}/Q^{0}_{\text{limit}})
$$  (34)

Then the fault probabilities of each submodel for each of the $i$th submodels, determine state $\tilde{\phi}_i$ and residuals $\tilde{E}_i^{(i)}$, and compute the monitoring indices and their upper control limits using eq 22 and eq 25.

The weighted combination approach is used to fuse the calculated fault probabilities. First, as demonstrated in eq 34, the weights of the monitoring results for each submodel are determined. It can be found that the submodel with higher fault probability will make a bigger impact on the final monitoring result.

$$
C_t^{(i)} = \frac{p_t^{(i)}(F|x)}{\sum_{j=1}^{n} p_t^{(j)}(F|x)}
$$  (35)

Second, two new unified monitoring indicators are defined to fuse the monitoring results of the submodels:

$$
E T^2 = \sum_{i=1}^{n} C_t^{(i)} p_{t}^{(i)}(x)
$$

$$
E Q = \sum_{i=1}^{n} C_{Q_t}^{(i)} p_{Q_t}^{(i)}(x)
$$

With the unified monitoring indicators, the fault detection logic is as follows,

$$
\begin{cases}
ET^2 < 1 - \alpha \text{ and } EQ < 1 - \alpha \Rightarrow \text{fault – free} \\
\text{otherwise } \Rightarrow \text{faulty}
\end{cases}
$$  (36)

The details of each step of the process monitoring procedure are summarized as follows:

- **Offline training**
  - Collect and normalize the training samples $X$ under normal condition.
  - Select $n_i$ appropriate kernel width parameters $h_i = 2^{-i-1}c_{m\sigma}$, $i = 1, \ldots, n_i$ and perform KPCA algorithm to obtain the reduced kernel matrix $\tilde{Y}^{(i)}$, $i = 1, \ldots, n_i$.
  - Construct past and future vectors from the reduced kernel component space using eq 18 for each submodel, and compute the cross-covariance and covariance matrices.
  - For the $i = 1, \ldots, n_i$ submodels, perform SVD on $\tilde{H}^{(i)}$ to derive the projection matrices $\tilde{J}^{(i)}$ and $\tilde{L}^{(i)}$.
  - For the $i = 1, \ldots, n_i$ submodels, determine state variables $\tilde{Z}^{(i)}$ and residuals $\tilde{E}^{(i)}$, and compute the monitoring indices and their upper control limits using eq 22 and eq 25.

- **Online monitoring**
  - Collect and normalize the new sample $x_i$.
  - Use eq 26 to construct the kernel matrix $k_i$, $i = 1, \ldots, n_i$ with normalized $x_i$ for each submodel.
  - Calculate the score matrix $y^{(i)}_t$ using eq 27, and construct the past data matrix at the point $k$. 


For the $i$th submodel, calculate state and residual of $x_t$ by multiplying the transformation matrices $J^{(i)}$ and $L^{(i)}$ to obtain the monitoring statistics ($T_t^{(i)}$ and $Q_t^{(i)}$).

Compute the fault probabilities for $i = 1, \ldots, n_l$ submodels by eq 28–eq 33.

Obtain the monitoring indices $ET^2$ and $EQ$ using eq 34 and eq 35.

Determine the process status based on the fault detection logic eq 36.

The scheme of the proposed EKCVA-based process monitoring method is depicted in Figure 1.

3.3. Parameters Selection. The parameters selection is critical in the proposed EKCVA-based process monitoring algorithm. The number of time lag $l$, the number of kernel principal elements (KPCs) $r$, the number of canonical variables (CVs) $w$, the kernel width parameter $h$ in KPCA, and the ensemble size $n_l$ should be appropriately selected. The determination of these parameters is discussed as follows:

- number of time lag $l$: $l$ is determined from the autocorrelation function of the measured values. Since the autocorrelation of each variable is different, we used the autocorrelation of the sum of all variables in this work. This allows for a better description of the dynamic characteristics of the process.

- number of KPCs $r$: To determine how many KPCs should be retained, the cumulative percent variance (CPV) is...
often calculated. The number of KPCs is selected while the CPV is over a predefined value.

- number of CVs: Similar to that in ref, the number of CVs is determined by finding the point where the “knee” appears in the singular value curve.

- kernel width parameter $h$: According to literature studies, the kernel width parameter is usually determined empirically such as $h = cm\sigma^2$, where $c$ is a constant, $m$ and $\sigma^2$ are the dimension and variance of the process data.

Figure 3. Monitoring diagrams of the nonlinear fault (a) KPCA, (b) EKPCA, (c) DKPCA, (d) EDKPCA, (e) KCVA, and (f) EKCVA.

| Table 1. Numerical Example: Monitoring Performance by Five Methods for Each Fault |
| --- |
| | KPCA | EKPCA | DKPCA | EDKPCA | KCVA | EKCVA |
| fault | $T^2$ | Q | $T^2$ | Q | $T^2$ | Q | $T^2$ | Q | $T^2$ | Q |
| 1 | 9.75$^b$ | 6.25 | 10.75 | 11.25 | 25.75 | 41.5 | 56.25 | 71.50 | 70.75 | 91.50 |
| 1.00$^b$ | 1.00 | 1.00 | 1.50 | 0.51 | 1.02 | 0.51 | 0.51 | 0.51 | 0.51 |
| 2 | 93.75 | 69.25 | 92.25 | 93.25 | 54.25 | 99.50 | 55.00 | 99.75 | 96.25 | 72.75 |
| 1.50 | 1.00 | 1.50 | 1.00 | 0.51 | 1.53 | 0.51 | 0.51 | 0.51 | 1.53 |

$^a$First row: FDRs. $^b$Second row: FARs.
respectively. If the data are normalized to $\sigma^2 = 1$, then $h = \text{CHL}$.\(^{32,44}\)

- ensemble size $n_z$. Obviously, the selection of $n_z$ is crucial for ensemble learning based process monitoring. If $n_z$ is set to a small value, the process characteristics can not be fully explored. The performance of process monitoring will be degraded. On the other hand, a larger value of $n_z$ implies higher computational complexity, which is not recommended, particularly for kernel-based methods. By considering the trade-off between fault detection performance and computational complexity, the number of ensemble size is determined by cross-validation in a similar way as in ref \(^33\).

4. CASE STUDIES

In this section, the proposed EKCVA-based process monitoring method is evaluated through a numerical example, a closed-loop CSTR process, and an industry benchmark of the Tennessee Eastman process. For comparison study, KPCA, EKPCA,\(^{32}\) dynamic KPCA (DKPCA),\(^{45}\) ensemble DKPCA, and KCVA are employed.

4.1. Numerical Example. The nonlinear state space model of the numerical example is described as follows,\(^{46}\)

$$
\begin{align*}
\mathbf{z}_k &= A \mathbf{z}_{k-1} + \mathbf{c} + \mathbf{e}_k \\
\mathbf{x}_k &= \mathbf{P} \mathbf{z}_k + f(\mathbf{u}_k) + \mathbf{e}_k
\end{align*}
$$

(37)

Table 3. Fault Description in CSTR Model

| fault no. | description | value | units | type |
|-----------|-------------|-------|-------|------|
| 1         | $f = f_0 e^{-\omega}$ | $5 \times 10^{-4}$ |    | multiplicative |
| 2         | $g = g_0 e^{-\omega}$ | $1 \times 10^{-4}$ |    | multiplicative |
| 3         | Faults 1 and 2 occur simultaneously | | | multiplicative |
| 4         | $C = C_0 + \xi t$ | $1 \times 10^{-3}$ |    | additive |
| 5         | $T = T_0 + \xi t$ | 0.05 |    | additive |
| 6         | $T = T_0 + \xi t$ | 0.05 |    | additive |
| 7         | $C = C_0 + \xi t$ | $1 \times 10^{-3}$ |    | additive |
| 8         | $T = T_0 + \xi t$ | 0.05 |    | additive |
| 9         | $T = T_0 + \xi t$ | 0.05 |    | additive |
| 10        | $Q = Q_0 + \xi t$ | $-0.1$ |    | additive |

The state space vector $\mathbf{z}_k \in \mathbb{R}^3$ used to describe the dynamic relationship between multivariate time series is which is generated from a vector autoregressive VAR(1) process. $f(\mathbf{u}) = 0.05 [u_1, u_2, u_1^2 - 2u_2, u_3^2 - 3u_3, -u_1^3 + 3u_2^2]^T$ is a nonlinear mapping function. The input $\mathbf{u} = [u_1, u_2]$ is a vector uniformly distributed over the interval [0, 2]. $\xi_k \in \mathbb{R}^3 \sim \mathcal{N}(0, I^3)$ and $\mathbf{e}_k \in \mathbb{R}^3 \sim \mathcal{N}(0, 0.1^3)$ denote the noises.

Two types of faults are considered including the change of dynamics and nonlinearity. All faults are injected from the 201st sampling point. The faults are described as follows:

- Fault 1: $\mathbf{z}_k := \mathbf{z}_k + [0, 2, 0]^T$ for $k > 200$
- Fault 2: $\mathbf{u}_k := \mathbf{u}_k + [3, 0]^T$ for $k > 200$

500 samples were generated under normal conditions for the training model. Two faulty test data sets were generated, which all consist of 600 samples.

For fair comparison, the number of time lag $l$ is set as 4 for all methods; $h = 200, r = 5$ are selected for the KPCA, DKPCA, and KCVA models, and $w = 6$ for the KCVA method. For EKPCA, EDKPCA, and EKCVA, the ensemble size is selected as $n_z = 8$, and the kernel parameters $h_i = 5 \cdot 5 \cdot 2^{(i-1)} (i = 1, \ldots, n_z)$. Other parameters of submodels are selected as KPCA, DKPCA, and KCVA. The confidence level $\alpha$ is 0.99.

The results obtained from process monitoring of Fault 1 are set out in Figure 2. As can be seen from Figure 2a,b, the KPCA and EKPCA fail to detect the abnormality from both $T$ and $Q$ statistics. The reason is that the variation of the state space vector is covered due to the process dynamics as shown in eq 37. On the contrary, DKPCA, EDKPCA, and KCVA methods can model the dynamic characteristics of the process by augmenting the process data. Thus, the monitoring performance is significantly improved as displayed in Figure 2c–f. Besides, the good generalization capability inherited from ensemble learning can further improve the model efficiency. Thus, EDKPCA and EKCVA can provide better monitoring performance than DKPCA and KCVA, respectively. Since the nonlinear dynamic behavior can be modeled more accurately by the

Figure 4. Schematic of the closed-loop CSTR.

Table 2. Constant Values in the CSTR Model

| parameter | description | value | units |
|-----------|-------------|-------|-------|
| $Q$       | inlet flow rate | 100.0 | L/min |
| $V$       | tank volume   | 150.0 | L     |
| $V_r$     | jacket volume | 10.0  | L     |
| $\Delta H_r$ | heat of reaction | $-2.0 \times 10^3$ | cal/mol |
| $UA$      | heat transfer coefficient | $7.0 \times 10^3$ | cal/min/K |
| $k_0$     | pre-exponential factor to $k$ | $7.2 \times 10^{10}$ | min$^{-1}$ |
| $R$       | activation energy | $1.0 \times 10^4$ | K     |
| $\rho_f$, $\rho_c$ | fluid density | 1000 | g/L   |
| $C_{p_f}$, $C_{p_c}$ | fluid heat capacity | 1.0 | cal/g/K |

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18911
Table 4. Comparison Results of FDRs for CSTR Process

| fault no. | KPCA (%) | EKPCA (%) | DKPCA (%) | EDKPCA (%) | KCVA (%) | EKCVA (%) |
|-----------|-----------|-----------|-----------|------------|----------|-----------|
|           | $T^2$     | $Q$       | $ET^2$    | $EQ$       | $T^2$    | $ET^2$    | $EQ$     |
| 1         | 75.50     | 44.40     | 75.80     | 54.40      | 59.54    | 83.33     | 60.04    | 84.14    | 84.26    | 87.69    | 84.36    | 87.89    |
| 2         | 83.10     | 87.90     | 83.10     | 94.10      | 68.27    | 87.75     | 68.88    | 89.16    | 85.17    | 88.70    | 85.37    | 88.90    |
| 3         | 78.50     | 88.30     | 78.60     | 94.70      | 69.78    | 85.54     | 69.98    | 86.75    | 82.14    | 85.37    | 82.34    | 85.57    |
| 4         | 94.80     | 70.30     | 94.80     | 74.70      | 92.57    | 72.79     | 92.57    | 72.49    | 91.32    | 90.21    | 91.32    | 90.31    |
| 5         | 87.30     | 72.10     | 87.30     | 73.10      | 78.11    | 80.02     | 78.71    | 79.91    | 79.52    | 75.68    | 79.72    | 75.78    |
| 6         | 85.80     | 81.20     | 85.80     | 91.90      | 75.30    | 80.62     | 78.31    | 80.52    | 78.30    | 79.41    | 78.61    | 79.72    |
| 7         | 99.10     | 94.90     | 99.10     | 97.40      | 95.78    | 99.40     | 95.78    | 99.50    | 95.06    | 96.67    | 95.26    | 96.87    |
| 8         | 91.00     | 96.70     | 91.00     | 98.50      | 83.63    | 96.39     | 83.73    | 96.89    | 95.76    | 98.67    | 95.76    | 98.67    |
| 9         | 93.20     | 96.90     | 93.20     | 98.50      | 86.33    | 96.39     | 87.33    | 98.69    | 95.76    | 96.87    | 95.76    | 98.67    |
| 10        | 79.70     | 81.00     | 79.70     | 92.60      | 68.88    | 87.75     | 69.28    | 80.62    | 77.60    | 81.84    | 78.00    | 81.84    |
| Average   | 86.82     | 73.27     | 86.84     | 86.99      | 76.98    | 86.12     | 77.26    | 86.48    | 86.85    | 88.20    | 87.02    | 88.32    |

Table 5. Comparison Results of the Average FARs for CSTR Process

| KPCA (%) | EKPCA (%) | DKPCA (%) | EDKPCA (%) | KCVA (%) | EKCVA (%) |
|----------|-----------|-----------|------------|----------|-----------|
| $T^2$    | $Q$       | $ET^2$    | $EQ$       | $T^2$    | $ET^2$    | $EQ$     |
| 1.00     | 0         | 1.15      | 0.15       | 0.30     | 0.20      | 0.40     |
| 0.40     | 0.85      | 0.40      | 0.90       |

Table 6. Comparison Results of DDs (hours) for CSTR Process

| KPCA (%) | EKPCA (%) | DKPCA (%) | EDKPCA (%) | KCVA (%) | EKCVA (%) |
|----------|-----------|-----------|------------|----------|-----------|
| $T^2$    | $Q$       | $ET^2$    | $EQ$       | $T^2$    | $ET^2$    | $EQ$     |
| 3.50     | 11.62     | 3.50      | 5.02       | 4.92     | 2.72      | 4.92     |
| 3.13     | 2.25      | 3.13      | 2.12       | 3.52     | 1.97      | 3.52     |
| 2.67     | 1.87      | 2.67      | 0.97       | 4.60     | 2.43      | 4.60     |
| 0.95     | 5.23      | 0.95      | 4.67       | 1.32     | 4.60      | 1.32     |
| 2.42     | 4.67      | 2.42      | 4.58       | 3.70     | 3.33      | 3.70     |
| 2.33     | 3.07      | 2.33      | 1.55       | 3.72     | 3.35      | 3.72     |
| 0.18     | 0.92      | 0.18      | 0.50       | 0.72     | 0.12      | 0.72     |
| 1.80     | 0.73      | 1.80      | 0.35       | 4.32     | 0.62      | 4.32     |
| 1.40     | 0.60      | 1.40      | 0.28       | 2.87     | 0.57      | 2.87     |
| 0.67     | 3.38      | 0.67      | 1.18       | 5.42     | 0.60      | 4.73     |
| 1.91     | 3.43      | 1.91      | 2.03       | 3.51     | 2.03      | 3.42     |
| Average  | 1.91      | 3.43      | 1.91       | 2.03     | 3.51      | 2.03     |

EKCVA model, it can also be observed that the proposed EKCVA method can acquire more excellent performance over DKPCA, EDKPCA, and KCVA.

Fault 2 represents the change of nonlinearity. The monitoring result of Fault 2 is plotted in Figure 3. It can be seen that Fault 2 can be detected by most methods. Compared to the KPCA based method, the KCVA based method can provide a better performance, since the autocorrelation is taken into consideration. Through ensemble learning, the nonlinear feature is more efficiently extracted than single model approaches. Thus, EKCVA-based process monitoring has the best performance among the comparative methods.

To further carry out the comparison of monitoring performance, two indexes are used. One is the fault false alarm rate (FAR), and the other one is the fault detection rate (FDR). The definitions of FAR and FDR are as follows:

\[
\text{FDR} = \frac{\text{no. of samples (} f > I_{th} \text{) }}{\text{total sample (} f \neq 0 \text{) }} \times 100
\]

\[
\text{FAR} = \frac{\text{no. of samples (} f > I_{th} \text{) }}{\text{total sample (} f = 0 \text{) }} \times 100
\]

where $f$ and $I_{th}$ denote the test statistic and corresponding threshold. $f \neq 0$ and $f = 0$ denote fault and fault-free, respectively.

For Fault 2, the FAR of EKCVA is 0.51% and FDR is 75.72%. The EKCVA based model can acquire more excellent performance over DKPCA, EKPCA, and KCVA. EKCVA method can acquire more excellent performance over EKCVA model, it can also be observed that the proposed EKCVA method can acquire more excellent performance over DKPCA, EDKPCA, and KCVA.

Table 1 lists the FDRs and FARs of the comparative methods. It is noticed that the EDKPCA $Q$ statistic can provide better performance than KPCA, EKPCA, and DKPCA for Fault 1 and Fault 2. Thus, it will be helpful for process monitoring by using ensemble learning and considering the process dynamics. On the other hand, it can be found that the EKCVA $T^2$ statistic can offer the best performance in terms of FAR and FDR. For Fault 1, the FAR of EKCVA $T^2$ statistic is 0.51% and FDR is 75.72%. For Fault 2, the FAR of EKCVA $T^2$ statistic is 0.51% and FDR is 99.75%.

4.2. CSTR Process. A CSTR, also known as a completely mixed flow reactor, is a tank reactor with stirring paddles. The physical and chemical changes in the substance in the system are part of the reaction process. Temperature, pressure, and flow rate are some of the parameters that characterize its system attributes. Researchers have used various forms of CSTRs for process monitoring in a variety of studies. A simplified diagram of the three-state closed-loop CSTR process is depicted in Figure 4. The following equations primarily describe the mechanism of the CSTR process:

\[
\frac{dT}{dt} = \frac{Q}{V} (T_i - T) - \int f(\Delta H_i)kC_p \rho_{C_p} \left( T - T_i \right) + v_i
\]
There are some constant values in the model, and these parameters are listed in Table 2. The process variables of the model $X = [T_o, C_o, T_{in}, T, C, T_c, Q_c]^T$. Furthermore, $v_i, i = 1, 2, 3$ are Gaussian white noise. For all variables, the sampling interval is 1 min. $k = k_0 \exp^{-RT}$ is an Arrhenius-type rate.

In this example, we simulate 10 types of faults in the CSTR process. For Faults 1–3, $f$ and $g$ are equal to 1.00 in normal operation. By attenuating their values to zero, the decay of catalyst and heat transfer pollution can be simulated, respectively. Faults 4–10 are sensor drifts. The details of these faults are described in Table 3. The training data set contains 1200 data points generated under normal operating conditions; 1200 samples are collected for each fault. The time point for fault

\[
\frac{dC}{dt} = \frac{Q}{V}(C_i - C) - fK + v_2
\]

\[
\frac{dT}{dt} = \frac{Q}{V_c}(T_{ci} - T) + g \frac{UA}{\rho C_p V_c}(T - T_c) + v_3
\]
import is the 200th minute. The data acquisition for this experiment can be downloaded from https://www.mathworks.com/matlabcentral/fileexchange/66189-feedback-controlled-cstr-process-for-fault-simulation. As it can be seen from the model expression, the CSTR is a typical nonlinear dynamic process.

According to the parameter selection procedure, \( h = 7 \cdot 20 \cdot 2^{(i-1)} \) \((i = 1, \ldots, n_l)\), \( l = 5 \), \( r = 6 \), \( w = 5 \), \( n_l = 10 \) are set for the EKCVA model. For the EDKPCA model, \( l = 5 \), \( r = 6 \), \( n_l = 10 \), \( h = 7 \cdot 20 \cdot 2^{(i-1)} \) \((i = 1, \ldots, n_l)\). For PKPCA model, \( r = 6 \), \( n_l = 10 \), \( h = 7 \cdot 20 \cdot 2^{(i-1)} \) \((i = 1, \ldots, n_l)\). The confidence level \( \alpha \) is 0.99 for determining the control limits. To evaluate the monitoring performance, three indexes including DD, FAR, and FDR are employed. Moreover, the detection time is determined as the first time after five consecutive alarms have been triggered to make the comparison more fair. DDs computed in the experiment are in units of hours.

The monitoring results are listed in Tables 4, 5, and 6. The EKCVA has the highest average FDRs (i.e., 87.02% and 88.32% for the \( T^2 \) and Q statistics, respectively). It is also noticed that the average FDRs of the ensemble models are both higher than those of the individual models. EKCVA \( T^2 \) and Q statistics are considered to be the most sensitive to all faults, where the DDs are 1.52 and 1.79 h, respectively. Compared to EDKPCA and KCVA, the FARs of EKCVA \( T^2 \) and Q statistics are slightly higher. However, the FAR values are at the same level as EKPCA. Nevertheless, the EKCVA \( T^2 \) and Q statistics provide the best monitoring performance among these comparative methods.
The results obtained from the preliminary analysis of Fault 1 and Fault 7 can be compared in Figure 5 and Figure 6, respectively. For Fault 1, it is a catalyst degradation fault. Variations in process variables are not immediately apparent at first. The difference between normal and abnormal conditions will progressively become significant after a few hours. As shown in Figure 5, the DDs of all methods are relatively large, but the EKCVA model has the smallest DDs. Additionally, EKCVA achieves the best monitoring results with the highest FDR. Fault 7 is the sensor drifts in the concentration of product reactants with a small magnitude of failure. Since KPCA and EKPCA models ignore the dynamics of process data, it can be found that there are larger DDs as displayed in Figure 6. Nevertheless, the proposed EKCVA method has superior monitoring performance than other methods in terms of FDR, FAR, and DD.

4.3. TEP. The industrial benchmark of the Tennessee Eastman process (TEP) was developed by Eastman Chemical Company based on a practical chemical process.\(^{48}\) The flow diagram of TEP is exhibited in Figure 7. In TEP, the process data have time-varying, strongly coupled, and nonlinear characteristics, thus it is widely used in the comparison study of process monitoring and fault detection.\(^{46,49−51}\)

In the TEP benchmark, 21 faults were predefined. The specific description of 21 faults is listed in Table 7. For process monitoring, 22 continuous variables and 11 manipulated variables were selected. The TEP data set can be found on the Web site (http://web.mit.edu/braatzgroup/links.html). A total of 500 observations under normal operating conditions were collected as training data. The testing data were acquired under a 48 h run of the simulation, with faults introduced at the eighth hour. And a total of 960 observations were collected. In this case study, the kernel width of KPCA model is empirically determined as

\[ h = 10m = 330, \quad r = 30, \quad h_i = 5m \cdot 2^{-i} \quad \text{(i = 1, ..., 11)} \]

for EKPCA model proposed Li and Yang. For EDKPCA model, \( l = 5, \quad r = 30 \), and \( h_i = 5m \cdot 2^{-i} \). For DKPCA model, \( l = 5, \quad r = 30, \quad \text{and} \quad w = 26 \). For KCVA model, \( h = 10m, \quad r = 30, \quad l = 5, \quad \text{and} \quad w = 26 \). For EKCVA model, \( r = 37, \quad w = 24, \quad l = 5, \quad h_i = 50m \cdot 2^{-i} \). The confidence level \( \alpha \) is 0.99.

Table 8 and Table 9 summarize the monitoring results for all 21 faults. The proposed EKCVA model can provide superior performance over other models for most faults such as faults 4, 8, 10, and 11 as shown in Table 8. The average FDRs of \( ET^2 \) and EQ are 83.74% and 81.26%, respectively, whereas the average FDRs of other methods are below 80%. Although the FAR of EQ (i.e., 4.946%) is higher than other Q statistics, the FAR of \( ET^2 \) (i.e., 5.554%) is at the same level as other \( T^2 \) statistics. The numbers of detection delays (DD) are provided in Table 10. From this table, we can see that the average DD of the EKCVA EQ statistic is the smallest among the monitoring statistics, and
the average DD of EKCVA $E T^2$ statistic is 21, which is smaller than KPCA $T^2$, DKPCA $T^2$, EDKPCA $E T^2$, and KCVA $T^2$. Nevertheless, the proposed EKCVA has superior monitoring performance than the other methods in terms of FDR, FAR, and DD.
Faults 5, 10, and 19 are employed for comparison. Fault 5 involves a step change in condenser cooling water inlet temperature. This fault does not cause a continuous change in the variable as the controller will compensate for the effects of the fault. However, this type of fault can also disrupt the normal operating process. The monitoring results are plotted in Figure 8. It can be found that the monitoring statistics of KPCA, DKPCA, and KCVA have a similar trend where the monitoring statistics will degrade after 10 h, although the step change still was imposed. On the other hand, through ensemble learning, more models are established by EKPCA, EDKPCA, and EKCVA methods. Thus, they can capture this change accurately. The monitoring statistics of EKPCA, EDKPCA, and EKCVA can detect fault 5 more sensitively as shown in Figure 8.

Fault 10 is a randomly varying fault, and the controller cannot fully compensate for the variation of this fault, and the dynamics of the process change under this fault condition. The monitoring results for this fault are shown in Figure 9. The monitoring charts for KPCA, DKPCA, and KCVA do not indicate the occurrence of all faults. Similar to fault 5, EKCVA still achieves the best monitoring results compared with both methods, EKPCA and EDKPCA, where almost all fault samples are detected. EKCVA ET and EQ statistics reach 93.71% and 91.57% of the FDRs, respectively.

The fault information of fault 19 is unknown. From Figure 10, it is obvious that the Q statistic of the EKCVA model has improved significantly over the Q statistic of the other five compared methods, reaching a fault detection rate of 99.55%.

Figure 8. Monitoring results in TEP of Fault 5: (a) KPCA, (b) EKPCA, (c) DKPCA, (b) EDKPCA, (e) KCVA, (f) EKCVA.
This indicates that the system deviates from the set operational level. In addition, EDKPCA outperforms EKPCA due to the capture of process dynamics. However, the EKCVA method still has the best performance.

5. CONCLUSION

The findings reported here shed new light on a data-driven dynamic nonlinear process monitoring approach. In the proposed EKCVA method, an ensemble learning strategy is introduced into KCVA. With the aid of ensemble learning, the capability of extracting nonlinearity features of KCVA is enhanced. Additionally, to give a final comprehensive statistic, Bayesian inference is applied to reorganize the monitoring results derived by KCVA which achieves comprehensive and accurate monitoring of process changes. To evaluate the proposed EKCVA method, a numerical example, the industrial TEP benchmark, and the CSTR process are carried out. Experimental results show that the EKCVA method outperforms other methods in terms of detection rate and detection time.

Although the superiority of the presented method has been verified, there are three issues that deserve further investigation. First, only the Gaussian kernel function is adopted in the model establishment. As a local kernel function, the Gaussian kernel function has good interpolation ability. The linear kernel is often used as the global kernel. Therefore, to further improve the feature extraction performance, mixed kernels that contain local and global kernel functions would be studied. Second, this study

Figure 9. Monitoring results in TEP of fault 10: (a) KPCA, (b) EKPCA, (c) DKPCA, (b) EDKPCA, (e) KCVA, (f) EKCVA.
mainly focuses on the fault detection issue for nonlinear dynamic processes. Fault identification is crucial to determine the root cause of faults. Reconstruction based fault identification has been widely studied in kernel-based process monitoring methods. However, since there is more than one model used in the EKCVA method, the decision making strategy should be another topic to investigate in future work for fault identification.

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**Notes**

The authors declare no competing financial interest.

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**Figure 10.** Monitoring results in TEP of fault 19: (a) KPCA, (b) EKPCA, (c) DKPCA, (d) EDKPCA, (e) KCVA, (f) EKCVA.
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