OPTIMIZATION OF NATURAL DYE EXTRACTION FROM COCONUT HUSK

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Received – November 15, 2019; Revision – December 30, 2019; Accepted – February 05, 2020

Available Online – February 25, 2020

DOI: http://dx.doi.org/10.18006/2020.8(1).54.62

KEYWORDS
Dye yield
RSM
Box-Behnken approach
Fibrous husk

ABSTRACT

Coconut is used throughout worldwide in various rituals, festivals and in food. A huge amount of unused parts of coconut such as fibrous husk and shells are thrashed every day. The present study illustrates the sustainable use of fibrous husk as a source of natural dye. Hence, in order to improve the dye yield, various dye extracting factors were optimized with the help of statistical software. The RSM based Box Behnken approach for optimization was found effective which increases dye yield up to 37%. The analysis of the model implies that the model fits well for all the four factors and found to be significant. All the factors M: L ratio, temperature, Time and pH were found influential in the dye extracting process. The system also helps to improve the yield for desired pH to obtain multiple hues. The optimized parameters to improve dye yield were M:L ratio of 1:130, temperature 80°C, time 250 minutes, pH 9.3.

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Peer review under responsibility of Journal of Experimental Biology and Agricultural Sciences.
1 Introduction

Natural colors are dyes or pigments acquired from plants, animals or mineral resources without any chemical preparations. They are produced from sources such as fruits, leaves, flowers, roots, barks, insects, etc. Indeed, they are not easily accessible and require an appropriate extraction method. Modern day synthetic dyes marked by Perkin’s invention of mauve in 1856, leads to the decline of natural dyes (Zollinger, 2003). Most synthetic dyes are carcinogenic and can cause allergic reactions. While natural dyes impart several benefits over synthetic colors as they are ecofriendly, non-toxic, biodegradable, aesthetically pleasing and having multiple medicinal properties (Gupta et al., 2004).

Cocos nucifera L (Family Arecaceae), often referred to as ‘coconut’ is regarded as a major plant in tropical and subtropical areas (Imo et al., 2018). Fruits of coconut is consumed as a nutritional diet while non-consumable Coir fiber and husk (mesocarp) are considered as agricultural and domestic waste (Khalid Thebo et al., 2016). These natural wastes are cheaper, in toxic, extremely efficient and easily available. Thus, applying waste products as natural dyes can reduce the cost of natural dyeing and also helps in maintaining the environment.

The heavy, fibrous, and dry-tanned mesocarp has many industrial uses. Industry uses pith husk fiber as raw material for carpets, stuffing seats for cushioning, and as fertilizers in agriculture (Verma et al., 2019). The plant is commonly being used in the food industry and the use of thrown away parts of the plant will help lower waste and pollution. The fiber exhibited antibacterial, anti-inflammatory and anti-parasitic activity (Lima et al., 2015). Tea prepared from C.nucifera husk fiber is used in Brazil to treat diarrhea (Esquenazi et al., 2002). Likewise, the husk fiber extract in Guatemala is used as an antipyretic to decrease renal inflammation and as an ointment for dermatitis, abscesses, and injuries (Cáceres et al., 1987). Aqueous extract of husk fiber is used as an asthma treatment (Hope et al., 1993). Diabetes is treated by husk extract in Jamaica (Mitchell & Ahmad, 2006). Peruvians orally use the aqueous extract of fresh coconut fiber for asthma, diuretics, and gonorrea (Lima et al., 2015). Presence of polyphenols such as catechins, flavonoids and tannins were reported in high quantity in ethyl acetate extract (Matos, 1997; Freitas et al., 2011; Pal et al., 2011; Renjith et al., 2013). South Indian people utilize fibrous husks for brushing the teeth is a common dental care practice of many rural individuals.

Optimization of the process is an important task to improve the extraction efficiency of dye from the material. The response surface methodology (RSM) a statistical approach to the optimization method is better as it requires a lesser number of experiments compared to the full-factorial or (OFAT) one factor at a time (Sundari, 2015; Ali et al., 2016; Jabeen et al., 2019). Box-Behnken design is a very effective method optimization model fitting (RSM) tool (Tayeb et al., 2018). It also checks the adequacy of the model by finding interactions between inputs and outputs for recognizing optimum conditions. One of the benefits of this model is that this doesn’t include all the variables at its extreme limit, so we can prevent experiments that may not give anticipated outcomes (Sundari, 2015). However, to the utmost of our understanding, there is almost no information on optimizing the conditions of natural dye extraction from C. nucifera. So, in this research, the effect of multiple process factors such as extraction time, pH, temperature, material to liquor ratio (M:L) on percent production output was evaluated using Box-Behnken design.

2 Materials and Methods

Based on previous research findings and subsequent trials, current study identified that pre-soaking and ultrasonification of material prior to conventional simple boiling method improves production yield.

2.1 Preparation and extraction of colorant

Coconut husk along with its coir fiber was collected as a waste material from temples and household use. The collected material was ground in a commercial pulverizer to produce in powder form. Further, the powder was sieved to get 0.25 mm fine powder which was used for extraction purposes. The extraction process was carried out by taking 1gm of 0.25 mm fine powder in 500 ml conical flask containing 100 ml distilled water in 1:100 ratio at pH 7 was kept for soaking for 24 hours, after soaking it was subjected for 10 min ultrasonification and placed in the water bath at 90° C for 120 min. The flask was covered and stirred manually by frequent shaking to prevent the wasting of solvent by evaporating. The sample was filtered and stored under cool temperature 0°- 4° C. The same method is implied for all the 29 combinations with four different factors and their three levels which are generated by the system as given in table 1. The extracted crude dye specimens are then transferred to a pre-weighted evaporating dish and subjected to drying at 50° C on a water bath until all solvent is evaporated and dried powder is formed. This powder is then cooled and weighed to determine the extracted dye weight and used to calculate the percentage of the color yield as follows (Sundari, 2015).

\[
\% \text{yield} = \frac{W_f - W_i}{W_p} \times 100
\]

Were, \(W_p\) – Weight of raw plant material; \(W_i\) – Initial weight of the empty evaporating dish; \(W_f\) – Final weight of dried natural dye with the evaporating dish.

2.2 Optimization of the process:

Response surface methodology (RSM) identifies optimum process configurations to attain maximum efficiency and also reduces the number of trails. Therefore, by using Design-Expert software (version 11.1.2 Stat-Ease Inc., Minneapolis, USA), a Box-Behnken approach for four variables was selected as the design of the experiment. The percentage yield of dye was chosen as a system response whereas the
four process parameters such as time, pH, temperature and material to liquor ratio (M:L) were taken as input variables (Sundari, 2015). On the basis of previous trails, the lower and upper limits of each factor (time varying from 120 minutes to 300 minutes, pH 4 to 10, temperature 50° C to 90° C and M:L ratio ranging from 1:100 to 1:200) were inputted in the model as shown in table 2. The combinations and the number of runs are depended upon the number of factors and their center points per block. Here, 29 runs of different combinations were generated and the optimized results were calculated. Regression analysis and Analysis of variance (ANOVA) were performed with the quadratic model by design expert software to satisfy the system generated mathematical model. Notable conditions were discovered in the model for response by analysis of variance and the importance was assessed by the F-value calculated from the data.

3 Result and discussion:

The 2nd-order quadratic model was equipped to correlate the connection between independent and dependent (yield) factors to predict the optimum values. The four-factor equation is indicated as follows:

\[
\% \text{ dye Yield} = 31.47 + 0.236667 A + 3.735 B + 4.40583 C + 6.9925 D + (-0.02 AB) + (-0.3425 AC) + (-0.7325 AD) + 0.135 \ BC + 1.895 BD + 2.565 CD + (-2.81167 A^2) + (-4.42792 C^2) + (-2.69542D^2)
\]

The F-value of 26.33 stated that the model Box-Behnken design depicts significant extracted dye yield as shown in Table 3. The terms B, C, D, CD A², B², C² and D² are significant, since the resulted P-value which is below 0.05 states that the model and terms are of statistical significance. The model's adequacy and fitness are calculated using the correlation coefficient (R²) and by the adjusted R² values. The R² value of 0.9634 ensures that the experimental data is compatible with the regression model. The Predicted R² of 0.8306 is in reasonable agreement with the Adjusted R² of 0.9268; i.e. the difference is less than 0.2, this indicates a decent correlation between predicted and actual value. The adequate precision of 18.6432 shows that the signal-to-noise ratio is adequate as the values above 4 are considered normal. Furthermore, the F-value for the lack of fit is 1.09 which is non-significant relative to the pure error value as shown Table 3. The 8.16% as the observed (CV) correlation of coefficient illustrates that the deviation is below 10 % indicates a decent response model (Segurola et al., 1999).

3.1 Model adequacy check:

The diagnostics plots obtained by the system for dye extraction optimization were used for the validation of the Box-Behnken model to prevent incorrect and misleading outcomes. The adequacy of Box-Behnken regression model for prediction is assessed in diagnostic plots shown in figure 1 (A, B and C). The figure 1A, denotes a plot of
Table 1 Four factorial and Three-level experimental design and Response % Dye yield

| Std | Run | M:L ratio (g:ml) | Temperature (°C) | Time (min) | pH | Response Dye Yield % |
|-----|-----|-----------------|-----------------|-----------|----|----------------------|
| 14  | 1   | 150             | 90              | 120       | 7  | 18.11                |
| 26  | 2   | 150             | 70              | 210       | 7  | 33.91                |
| 9   | 3   | 100             | 70              | 210       | 4  | 17.44                |
| 25  | 4   | 150             | 70              | 210       | 7  | 29.49                |
| 5   | 5   | 150             | 70              | 120       | 4  | 14.96                |
| 15  | 6   | 150             | 50              | 300       | 7  | 21.45                |
| 24  | 7   | 150             | 90              | 210       | 10 | 34.46                |
| 7   | 8   | 150             | 70              | 120       | 10 | 23.68                |
| 22  | 9   | 150             | 90              | 210       | 4  | 19.61                |
| 3   | 10  | 100             | 90              | 210       | 7  | 22.79                |
| 19  | 11  | 100             | 70              | 300       | 7  | 28.87                |
| 23  | 12  | 150             | 50              | 210       | 10 | 20.51                |
| 16  | 13  | 150             | 90              | 300       | 7  | 27.91                |
| 28  | 14  | 150             | 70              | 210       | 7  | 31.36                |
| 10  | 15  | 200             | 70              | 210       | 4  | 17.87                |
| 21  | 16  | 150             | 50              | 210       | 4  | 13.24                |
| 27  | 17  | 150             | 70              | 210       | 7  | 32.86                |
| 4   | 18  | 200             | 90              | 210       | 7  | 24.43                |
| 6   | 19  | 150             | 70              | 300       | 4  | 18.41                |
| 20  | 20  | 200             | 70              | 300       | 7  | 28.96                |
| 17  | 21  | 100             | 70              | 120       | 7  | 19.86                |
| 8   | 22  | 150             | 70              | 300       | 10 | 37.39                |
| 2   | 23  | 200             | 50              | 210       | 7  | 18.41                |
| 1   | 24  | 100             | 50              | 210       | 7  | 16.69                |
| 18  | 25  | 200             | 70              | 120       | 7  | 21.32                |
| 29  | 26  | 150             | 70              | 210       | 7  | 29.73                |
| 12  | 27  | 200             | 70              | 210       | 10 | 33.45                |
| 11  | 28  | 100             | 70              | 210       | 10 | 35.95                |
| 13  | 29  | 150             | 50              | 120       | 7  | 12.19                |

Table 2 Experimental factors and Levels used in current study

| Factors                      | -1   | 0   | 1   |
|------------------------------|------|-----|-----|
| M:L ratio, g:ml (A)          | 1:100| 1:150| 1:200|
| Temperature, °C (B)          | 50°C | 70°C | 90°C |
| Time, min (C)                | 120  | 210 | 300 |
| pH (D)                       | 4    | 7   | 10  |
normal probability versus studentized residuals which was used to check normality of results, all the resultant points of experiments are arranged on the continuous diagonal line this is due to the lack of obvious design normality problems. Studentized residuals and predicted dye yield values of coconut husk are plotted in figure 1B, shows randomly scattered variance with good dispersion within the accepted range indicates that all response values have constant significant variability. The model adequacy is estimated by comparing experimental and predicted values on the diagonal line in a plot of actual vs. predicted values as shown in Figure 1C. As all the points are close to the straight diagonal line, it could be said that there is a significant agreement between the actual experimental values and the predicted values.

3.2 3D Surface plots depicting the interaction between experimental variables and response Dye yield

3D graph shows the correlation between temperature and M:L ratio i.e. solvent ratio on dye yield as shown in Figure 2A. The dye yield increases as the temperature increased from 50 to 80 °C and slightly decreased when the temperature increase from 80 to 90 °C as shown in figure 2D. This is due to the increase in temperature the density of the solvent is changed which decreases the solubility of coloring compound, therefore, reduces dye yield (Sundari, 2015). The desired dye yield should contain polyphenols which are abundant coloring compounds in the material. As the material is fibrous coconut husk which is thick and made up of cellulose and polyphenols such as lignin the temperature as experimental variable was kept from 50 to 90 °C. The high temperature degrades and unstabilize the desired polyphenol compounds. Opposite to this the low temperature slows downs the color extraction (Berhanu & Ratnapandian, 2017; Khoo et al., 2017). This material also occupies the space and hold high amount of water so, the solvent ratio is kept from 1:100 to 1:200. Roughly the observation shows the percentage yield remains constant throughout the range for differential M:L ratio. The mere observation of graphs in Figure 2A shows that the temperature at 75°C along with the solvent quantity of 1:150 results high percent dye yield.

Figure 2C describes the interaction between the time and the M:L ratio. The percent dye yield increase as the time increases from 120 to 300 min. As the contact time with the material along with the increasing temperature, the extraction rate of coloring compounds in the solvent system gets increased (Zhang et al., 2018).

### Table 3 ANOVA for Quadratic model

| Source            | Sum of Squares | df | Mean Square | F-value | p-value |  
|-------------------|----------------|----|-------------|---------|---------|
| Model             | 1452.35        | 14 | 103.74      | 26.33   | < 0.0001|  
| A-M:L ratio       | 0.6721         | 1  | 0.6721      | 0.1706  | 0.6859  |  
| B-Temperature     | 167.40         | 1  | 167.40      | 42.48   | < 0.0001|  
| C-Time            | 232.94         | 1  | 232.94      | 59.12   | < 0.0001|  
| D-pH              | 586.74         | 1  | 586.74      | 148.91  | < 0.0001|  
| AB                | 0.0016         | 1  | 0.0016      | 0.0004  | 0.9842  |  
| AC                | 0.4692         | 1  | 0.4692      | 0.1191  | 0.7352  |  
| AD                | 2.15           | 1  | 2.15        | 0.0185  | 0.8937  |  
| BC                | 0.0729         | 1  | 0.0729      | 0.0004  | 0.9842  |  
| BD                | 14.36          | 1  | 14.36       | 3.65    | 0.0769  |  
| CD                | 26.32          | 1  | 26.32       | 6.68    | 0.0216  |  
| A²                | 51.28          | 1  | 51.28       | 13.01   | 0.0029  |  
| B²                | 349.62         | 1  | 349.62      | 88.73   | < 0.0001|  
| C²                | 127.18         | 1  | 127.18      | 32.28   | < 0.0001|  
| D²                | 47.13          | 1  | 47.13       | 11.96   | 0.0038  |  
| Residual          | 55.16          | 14 | 3.94        |         |         |  
| Lack of Fit       | 40.32          | 10 | 4.03        | 1.09    | 0.5108  |  
| Pure Error        | 14.85          | 4  | 3.71        |         |         |  
| Cor Total         | 1507.52        | 28 |             |         |         |  

Std. Dev =1.99, Mean = 24.32, R² = 0.9634, Adjusted R² =0.9268, Predicted R² = 0.8306, Adeq Precision = 18.6432, C.V. % =8.16.
Figure 2. 3D Surface plots depicting Effect of (A) Temperature and M:L ratio, (B) pH and M:L ratio (C) Time and M:L ratio (D) Time and Temperature (E) pH and Temperature (F) pH and Time on response % dye yield.
The graph in the figure 2 (B, E and F) shows that the dye yield increase as the pH is increased from 4 to 10. Therefore pH is an important factor for the increase in dye yield. This indicates that the material is rich in phenolic compounds (Saxena & Raja, 2014). Although in previous study, it has been observed that the original pH in distilled water was found to be 6.4 (Israel et al., 2011). Thus, the different hues were obtained in different pH solutions from 4 to 10. The solutions of different pH were used to determine the percent dye yield from material. Here, darkness of brown color shade was improved as the pH is increased from 4 to 10.

3.3 Optimization:

The optimization function in the system searches different combinations of factor levels that simultaneously fulfill the requirements imposed for each factor and response. Here, for the optimization of factors, a numerical optimization method was used. In which goal for all the factors was kept in range, and for the response it was kept at maximizing level. The weight assigned for the response was 1 which forms a linear ramp function between lower value and the goal, and the importance was set to 5 pluses as the study was done to increase percent dye yield. From the resultant solutions top best solution was used as the optimum values for extraction as depicted in figures 3 (Al-Alwani et al., 2016).

For acidic to neutral pH, rich brown shade was obtained so the optimized values for this were also calculated by keeping pH range from 4 to 7 as shown in Figures 4. Further the experiments were conducted under the optimal predicted conditions with a percentage dye yield of 37.39, M:L ratio of 130.64, with extracting temperature of 80.02 for time 251.61 and at pH 9.30 as shown in figure 3. The experiments were also conducted for optimal predicted conditions given for acidic neutral pH with a percentage dye yield of 33.05, M: L ratio of 150.54, with extracting temperature of 75.17 for time 255.15 and at pH 7 as shown in figure 4.

Conclusion

In present research, four factors M:L ratio, temperature, time and pH were optimized effectively using RSM based Box-Behnken method and the dye yield was improved up to 37%. The ANOVA showing an F-value of 26.33 implies the model is significant and a high correlation coefficient value $R^2$ of 0.9604 confirms that decent fit of model. The optimized values obtained by the model approximately were M:L ratio of 1:130, temperature 80°C, time 250 minutes, pH 9.3 and the optimized values acidic neutral pH were M:L ratio of 1:150, the temperature of 75°C, time 255 minutes and pH 7. The yield obtained for acidic-neutral pH extraction of 33% was also found to be convincing to extract.
Optimization of natural dye extraction from coconut husk
different brown color shade. Thus, different hues can be obtained from coconut husk depending upon different pH. Overall the high percent yield shows that the coconut husk is the valuable source of natural dye, it is easily available and shows a good quality use of waste material and thus this dye might be used in wide applications from food to textile industries.

Acknowledgment
The authors are thankful to the Department of botany Shivaji University, Kolhapur for providing necessary research facilities and Council of scientific and industrial research (CSIR) for Junior Research Fellowship (JRF).

Compliance with Ethical Standards
Conflict of interest: The authors declare no conflict of interest.

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