Optimization of Operational Method to Improve Sustainable Energy Efficiency of Auxiliaries in a CFBC Coal Fired Boiler- Problem Statement and Probable Solution.

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Abstract: The thermal power station uses some amount of their generated power to be consumed by its auxiliary power requirements. The auxiliary power consumption in the country is around 8-9%. The auxiliary power consumption can be minimize by increasing the load factor, by operational optimization, applying advanced control techniques and energy efficient measures. By decreasing the auxiliary extra power will be available at grid. Thus, the aim of the audit is to determine the potential areas for minimizing auxiliary power consumption by operational optimization and energy management policy to improve energy efficiency of auxiliaries. This study will give the basic understanding of energy management approach, energy efficiency and energy saving areas so as to achieve maximum plant efficiency resulting fuel saving. Boiler feed pump is one of the equipment in a power plant with the highest auxiliary consumption. The research is specifically targeted at the feed water system and its potential for obtaining considerable energy and cost savings.

Keywords: energy audit, boiler feed pump, boiler auxiliary, differential pressure, drum level control, cfbc boiler.

I. INTRODUCTION

The audit deals with the Energy efficiency achieved through operation of boiler feed pump by means of scoop control in auto mode (DP method) during daily operation of the plant at varying load conditions. The scope of the audit covers the boiler feed pumps and the feed water system in each unit of the AMNEPL power plant. Boiler feed pump is one of the equipments in a power plant with the highest auxiliary consumption. Thus after the study on this audit the results showed that with automated operation of scoop by means of DP method provided considerable savings in auxiliary consumption. The drum with 1.8m inner diameter and 2.09m outer diameter is hung on front roof by two U-shape hooks, valve hole seats and thermal detection parts and sealing iron parts, preventing wear and tear. Also, diameter of economizer’s mid-header economizer coiler hangs on economizer mid-header. Water feeding heated by economizer runs into steam drum first, and then runs into four pieces concentrated sewer pipes after mixing with boiler water, finally led to front, rear and two sides' water wall lower header by launch connection tube. Steam-water mixture through water wall and water wall upper header is run into drum by drum-water wall connection tube, which is separated by steam-water separator to fulfill water circulation.

Steel structure erection and covering position should be finished. All high-tension bolts should be tightened and qualified. Boiler proper equipment should be checked as per drawings and regulations, and the exposed defects should be eliminated. All heating surface, pressure parts and accessories of boiler proper (such as buckstays, guiding devices etc.) should be installed as per drawing requirements (including header’s inner checking and cleaning, pipes through ball, component alignment and connection working etc.). The pipelines and supports participating in Hydraulic test should be installed. Boiler proper pipelines for emptying, water draining, sampling, nitrogen filling, acid washing, meter controlling, chemical dosing, pollution discharge and de-superheated water have been connected to secondary valve. Pay more attention to heat expansion offset during pipeline erection. All weld craters included in Hydraulic test should be welded, visual inspected, heat treated, NDE ( as stated sampling inspection rate) and qualified. All components welded on heating surface pipes or pressure part should be finished, such as fins, pins, sealing iron parts, preventing wear enclosures, insulation hook nails, valve hole seats and thermal detection parts and expansion joints etc.

II. EQUIPMENTS OF FEEDWATER SYSTEM

Table 2.1: Technical Specification of Boiler

| Equipment Detail | Technical Specification | Parameters |
|------------------|------------------------|------------|
| Boiler           | Year of installation   | 2009       |
| Type of boiler   |                        | CFBC       |

PSH and PRH are hanged by hanger tube of economizer’s mid-header; economizer coiler hangs on economizer mid-header. Water-feeding heated by economizer runs into steam drum first, and then runs into four pieces concentrated sewer pipes after mixing with boiler water, finally leaded to front, rear and two sides’ water wall lower header by launch connection tube. Steam-water mixture through water wall and water wall upper header is run into drum by drum-water wall connection tube, which is separated by steam-water separator to fulfill water circulation.

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### Table 2.2: Technical Specification of Turbine

| Equipment Detail | Technical Specification | Parameters |
|------------------|-------------------------|------------|
| Type of furnace  | Membrane wall           |            |
| Capacity         | 250 TPH                 |            |
| Peak capacity    | 270 TPH                 |            |
| Temperature      | 540 °C                  |            |
| Design steam pressure | 11.781 Mpa             |            |
| Boiler drum pressure | 11.22 Mpa               |            |
| Type of cyclone  | Steam cooled            |            |
| Type of fuel feeding | Belt conveyor and pocket feeder | |

| Type            | High temp. and high press. non control extraction condensing |
| Maximum output  | 61.5 MW            |
| Main steam pressure | 8.83 Mpa          |
| Main steam temp. | 537 °C            |
| Main steam flow  | 238 TPH            |
| Rated speed     | 3000 RPM           |
| Flow path series | 21 (1 governing stage + 20 pressures stage) |
| Turbine         | Turbine heat rate |
|                 | 9287 kJ / kwhr(T-MCR), 2218 Kcal / kwhr, 9285 kJ / kwhr (VWO), 2217 Kcal / Kwhr |

| Regeneration series | 6 (2 HPH + 3 LPH + 1 deaerator) |
| Points for non-controlling extraction | Behind stages no. 5, 8, 11, 15, 17, 19 |

### Table 2.3: Technical Specification of Feed Pump Motor

| Equipment Detail | Technical Specification | Parameters |
|------------------|-------------------------|------------|
| Boiler Feed Pump Motor | Type | Squirrel cage motor |
| Rated voltage    | 6600v              |
| Frequency        | 50 hz.             |
| Connection       | Star               |
| Phase            | 3                  |
| Speed            | 2985 rpm           |
| Power factor     | 0.88               |
| Current          | 166 amps           |
| Efficiency       | 96.10%             |
| Rated power output | 1600 kw         |

![Fig 2.1: Pump Characteristic Curves of Feed Water System](image)
1. Boiler Drum

Water wall lower header, enclosure wall lower header and displacement indicator of steam drum should be prepared completely. The erection position should be correct. Indication hand should be firm and adjusted it at zero. Pre-welding parts have been installed on other headers, with which expansion indicators should be equipped. The equipment, pressure weld seams of pipelines and other parts in the range of hydraulic test shouldn’t be heat insulated and painted. All measuring gauge that will be used in hydraulic test should be prepared completely and have qualification certificate in the period of validity. Accuracy and measuring range should accord with regulation. The pathway, stair, platform, handrail, temporary scaffold, communication equipment and lighting used in hydraulic test should be installed.
Ground and road should be cleaned, unblocked and have no sundries and seep. Safety valve has been installed and the specific valve core for hydrotest should be installed as per manual. The conduits of PRH inlet, FRH outlet and FSH outlet should be installed. Blocking valves’ pressure grade should meet the requirement of hydraulic test.

The water source should use qualified desalted water from chemical water workshop, in which chloride content can’t be more than 25ppm. For some proper ammonia liquor and hydrazine have been added into desalted water for hydraulic test and avoiding polluting environment when draining. Temporary draining pipelines should be separately met on inlet header water draining pipe of PRH, inlet header water draining pipe of FSH, lower header water draining pipe of enclosure wall, inlet header draining pipe of economizer and inlet general valve of nearby furnace heating location header, and then the temporary draining pipelines should be concentrated on the main draining pipeline of φ168*5, finally the desalted water should be drained to acid and alkali neutralization pond.

2. Drum Internal Equipments

When emptying pipes can drain water uniformly for a long time without air bubble, the system has been filled with water. Shut off Emptying pipes valves in the order of effluent water. When the boiler is about to be filled with water, recycle valve of desalted water pump should be opened up slightly. When outlet pressure of condensation water transfer pump should be in the range of 1.1~1.3Mpa. Shut off outlet valve of condensation water transfer pump after the boiler is filled with water. Then open up #8 temporary valve and the draining valves of water cooling system, super-heater system and re-heater system. And open up all emptying valves in the reversed order of shutting off emptying valves to drain all of water in furnace for meeting the purpose of flushing heating surface equipment.

Before filling water, the test on site should be conducted as per test table, and the water can be filled after correlated conditions are met positive and signed by every representative. Before filling water, enough desalted water should have been prepared first. Shut off #1 and #8 temporary valves when filling water. Pump will be started up by formal condensation water transfer pump (the flow is 160m3/h, delivery lift is 125m). Then open up water-feeding operation valve, draining valve of PRH inlet header, #4 temporary valve, draining valve of FRH outlet header, steam side of double color water gauge, waterside of primary and secondary valves and various emptying valves. Then shut off various left valves. Finally start up condensation water transfer pump and fill water into boiler. During filling water, drum wall temperature difference should be ≤50°C, the temperature difference between filling water temperature and drum wall temperature should be ≤28°C.

Slightly open the outlet valve of condensation water transfer pump and recycle valve. Startup condensation water transfer pump and control its outlet pressure in the range of 1.0~1.3Mpa by adjusting the jaw opening of recycle valve. Open up #8 temporary valve and #2, #3 temporary valves of booster pump outlet. Open up the primary valve and secondary valve of a periodic blowdown pipe connection with booster pipe. Open up draining valves of right side FRH and right side FSH outlet headers (for connection primary steam system with secondary steam system). Open up primary valve and secondary valve of double color water gauge steam side and waterside, and shut off #4 and #9 temporary valves and every system left valves. Finally start up two sets booster pumps for boosting to furnace. The boosting speed should be controlled within 0.294Mpa/min.

3. Problem Identification- Existing System

Fig 5.1 Existing Feed Water System

The feed water system consists of the Boiler feed pump, Feed regulation station, Deaerator, high pressure heaters, Economiser. In all four units for maintaining drum level three element control was used where the feed control station was kept in 3 element mode. In this process BFP discharge pressure was being maintained in manual mode by varying scoop position manually. The differential pressure across FRS is maintained at a very higher side i.e. in the range of 25-30 Kg/cm2. For efficient maintaining of drum level only a DP of 8-10 Kg/cm2 is sufficient, the rest excess is compensated by throttling of control valve and hence as the DP across FRS is increased unnecessary power is consumed at BFP end.

4. Probable Solution- Proposed System

Fig 6.1 Proposed Feed Water System

In the new control philosophy of BFP scoop was put in auto mode which would maintain the Differential pressure across the FRS as per the set point while FRS control valve would maintain the drum level as per 3 element commands to maintain the desired drum level (50%). No additional investment or material is required as all provisions are inherent and provided in the existing system. It is also recommended to lock the control valves of the FRS station to operate between 0% (min) - 75% (max) open condition to ensure that the sensitivity of the Control valves is preserved.
III. RESEARCH METHODOLOGY

1. Review of literature and detail study of related journals
2. Study of water feed system of Boiler in Thermal power plant.
3. Study of various equipments used in Boiler water feed system
4. Data Collection:
   a) System & Equipments specifications.
   b) System & Equipments Layout diagrams.
   c) G.A Drawings of the Equipments.
   d) P&I Drawings of the Systems.
5. To find out scope of Energy conservation & Efficiency improvement areas.
6. Energy Audit of Existing System.
7. Baseline energy use and Cost of Audited system.
8. Energy conservation recommendations.
9. Energy Audit of Proposed System.
10. Analysis and Calculations:
    a) Calculations for Existing system.
    b) Calculations for Proposed system.
    c) Comparison of Existing system and proposed system.
    d) Calculations for Energy savings.
11. Cost benefits and Simple Payback period.
12. Result and Conclusion.

5. Advantages

1. It is very robust control and can be used during fluctuating load conditions without any major variation in drum level.
2. With decreased DP across FRS life of control valve also increases.
3. Life of a bearing increases as compare to the existing system.
4. No extra cost is required to implement the system.

IV. CONCLUSION

The 3 element method consumes more auxiliary power for varying load conditions as the pressure difference is very high. So by adopting new drum control philosophy that require only 8 to 10 kg/cm² differential pressure across feed regulation system (FRS) and scoop in automatic mode provides less human interference. Total auxiliary consumption can be reduced. No extra cost is required to implement the system. Human interference is neglected due to automation.

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