**Speed control of dc motor using artificial bee colony optimization technique**

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**Abstract—** The aim of this work is to design a speed controller of a DC motor by selection of PID parameters using bio-inspired optimization technique of Artificial Bee Colony Optimization (ABC). Here, model of a DC motor is considered as a second order system for speed control. In this work bio-inspired optimization technique in controllers and their advantages over conventional methods is discussed using MATLAB/Simulink. This proposed optimization methods could be applied for higher order system also to provide better system performance with minimum errors. The main aim is to apply ABC technique to design and tune parameters of PID controller to get an output with better dynamic and static performance. The application of ABC to the PID controller imparts it the ability of tuning itself automatically in an on-line process while the application of optimization algorithm to the PID controller makes it to give an optimum output by searching for the best set of solutions for the PID parameters.

**Keywords:** Artificial Bee colony optimization; PID controller; Parameter tuning.

**I. INTRODUCTION**

DC motor drives are widely used in applications requiring adjustable speed, good speed regulations and frequent starting, braking and reversing. Some important applications are rolling mills, paper mills, mine winders, hoists, machine tools, traction, printing presses, textile mills, excavators and cranes. Fractional horsepower DC motors are widely used as servo motors for positioning and tracking. Although, it is being predicted that AC drives will replace DC drives, however, even today the variable speed applications are dominated by DC drives because of lower cost, reliability and simple control. As per the control of DC motor, there are lot of methods to control the speed and position of the motor. The purpose of a motor speed controller is to take a signal representing the demanded speed and to drive a motor at that speed.

PID (proportional-integral-derivative) control is one of the earlier control strategies. It has a simple control structure which was understood by plant operators and which they found relatively easy to tune. Since many control systems using. PID control have proved satisfactory, it still has a wide range of applications in industrial control. PID control is a control strategy that has been successfully used over many years. Simplicity, robustness, a wide range of applicability and near-optimal performance are some of the reasons that have made PID controller so popular in the academic and industry sectors. Recently, it has been noticed that PID controllers are often poorly tuned and some efforts have been made to systematically resolve this matter. PID control has been an active research topic for many years; since many process plants controlled by PID controllers have similar dynamics it has been found possible to set satisfactory controller parameters from less plant information than a complete mathematical model. These techniques came about because of the desire to adjust controller parameters with a minimum of effort, and also because of the possible difficulty and poor cost benefit of obtaining mathematical models.

**The PID controller calculation (algorithm) involves three separate parameters, and is accordingly sometimes called three-term control: the proportional, the integral and derivative values, denoted P, I, and D. The proportional value determines the reaction to the current error, the integral value determines the reaction based on the sum of recent errors, and the derivative value determines the reaction based on the rate at which the error has been changing. The weighted sum of these three actions is used to adjust the process via a control element. By tuning the three constants in the PID controller algorithm, the controller can provide control action designed for specific process requirements. The response of the controller can be described in terms of the responsiveness of the controller to an error, the degree to which the controller overshoots the set point and the degree of system oscillation.**

In Bees Algorithm, the colony of artificial bees consists of three groups of bees: employed bees, onlookers and scouts. First half of the colony consists of the employed artificial bees and the second half includes the onlookers. For every food source, there is only one employed bee. In other words, the number of employed bees is equal to the number of food sources around the hive. The employed bee
whose the food source has been abandoned by the bees becomes a scout. The position of a food source represents a possible solution to the optimization problem and the nectar amount of a food source corresponds to the quality (fitness) of the associated solution. The number of the employed bees or the onlooker bees is equal to the number of solutions in the population. In proposed ABC-PID controller, ABC algorithm is used to optimize the gains and the values are applied into the controller of the plant. The objective of this algorithm is to optimize the gains of the PID controller for the given plant. The proportional gain makes the controller respond to the error while the integral derivative gain help to eliminate steady state error and prevent overshoot respectively.

II. MATHEMATICAL ANALYSIS OF DC MOTOR

In armature control of separately excited DC motors, the voltage applied to the armature of the motor is adjusted without changing the voltage applied to the field. Figure 1 shows a DC motor equivalent model.

![D.C. motor model](image1)

Fig. 1. D.C. motor model

Some useful relations are:

\[ V_a(t) = R_a i_a(t) + L_a \frac{di_a}{dt} + E_b(t) \]  
\[ E_b(t) = K_b \omega(t) \]  
\[ T_m(t) = K_t i_a(t) \]  
\[ T_m(t) - T_L(t) = J_m \frac{d\omega}{dt} + B_m \omega(t) \]

where \( V_a \) = armature voltage (V), \( R_a \) = armature resistance (Ω), \( L_a \) = armature inductance (H), \( I_a \) = armature current (A), \( E_b \) = Back emf (V), \( \omega \) = angular speed (rad/sec), \( T_m \) = motor torque (Nm), \( T_L \) = load torque (Nm), \( \theta \) = angular position of rotor shaft (rad), \( J_m \) = rotor inertia (kgm²), \( B_m \) = viscous friction coefficient (Nms/rad), \( K_t \) = torque constant (Nm/A), \( K_b \) = Back emf constant (Vs/rad).

Substitute (3) in (2) and (4) in (5), we get

\[ V_a(t) = R_a i_a(t) + L_a \frac{di_a}{dt} + K_b \omega(t) \]  
\[ K_t i_a(t) = J_m \frac{d\omega}{dt} + B_m \omega(t) \]  

Taking Laplace transform of equation (6) and (5),

\[ V_a(s) = R_a i_a(s) + s L_a I_a(s) + K_b \omega(s) \]  
\[ K_t I_a(s) = s J_m \omega(s) + B_m \omega(s) \]

There are two possible conditions:

When \( T_L = 0 \)

![Block diagram of D.C. motor model](image2)

Fig. 2. Block diagram of D.C. motor model

Substitute (3) in (2) and (4) in (5), we get

\[ V_a(t) = R_a i_a(t) + L_a \frac{di_a}{dt} + K_b \omega(t) \]  
\[ K_t i_a(t) = j_m d\omega(t)/dt + B_m \omega(t) \]

Taking Laplace transform of equation (6) and (5),

\[ V_a(s) = R_a i_a(s) + s L_a I_a(s) + K_b \omega(s) \]  
\[ K_t I_a(s) = j_m \omega(s) + B_m \omega(s) \]

There are two possible conditions:

When \( T_L = 0 \)

![Block diagram of D.C. motor model when TL = 0](image3)

Fig. 3. Block diagram D.C. motor model when \( T_L = 0 \)

Figure 3 shows that the DC motor is running under no-load condition (ideal) i.e. \( T_L = 0 \). Now find the transfer function of \( \omega(s) \) with respect to \( V_a(s) \).

So, the relation between motor speed and applied voltage is given by the transfer function,

\[ \frac{\omega(s)}{V_a(s)} = \frac{K_t}{L_a J_m s^2 + (R_a J_m + L_a B_m) s + (R_a B_m + K_b K_t)} \]  

and when \( V_a = 0 \).
Figure 4 shows the DC motor model when supply voltage (Va) is 0 and the transfer function of ω(s) is with respect to \( \frac{1}{T_L(s)} \). Here, the relation between motor speed and load torque is given by the transfer function,

\[
\frac{\omega(s)}{T_L(s)} = \frac{-(L_a q + K_e)}{L_a f_m s^2 + (R_a f_m + L_a \theta_m)s + (R_a \theta_m + K_b K_e)}
\]  

(10)

III. SPEED CONTROL USING CLASSICAL PID TUNING METHODS

The PID controller is the most common general purpose controller in today’s industries. It can be used as a single unit or it can be a part of a distributed computer control system.

After implementing the PID controller, now we have to tune the controller; and there are different approaches to tune the PID parameters like P, I and D. The Proportional (P) part is responsible for following the desired set-point while the Integral (I) and Derivative (D) part account for the accumulation of past errors and the rate of change of error in the process or plant, respectively.

PID controller consists of three types of control i.e. Proportional, Integral and Derivative control

The system transfer function in continuous s-domain are given as

For, \( P = K_p \), \( I = \frac{K_i}{s} \) and \( D = K_d s \)

\[
G_c(s) = P + I + D = K_p + \frac{K_i}{s} + K_d s
\]  

(11)

\[
G_c(s) = K_p \left(1 + \frac{1}{T_i s} + T_d s\right)
\]  

(12)

Where \( K_p \) is the proportional gain, \( K_i \) is the integration Coefficient and \( K_d \) is the derivative coefficient.

\( T_i \) is known as the integral action time or reset time and \( T_d \) is the derivative action time or rate time.

There are various tuning strategies based on an open-loop step response. While they all follow the same basic idea, they differ in slightly in how they extract the model parameters from the recorded response, and also differ slightly as to relate appropriate tuning constants to the model parameters. There are different methods, the classic Ziegler-Nichols test, and Cohen- Coon test. Naturally if the response is not sigmoid or ‘S’ shaped and exhibits overshoot, or an integrator, then this tuning method is not applicable.

This method implicitly assumes the plant can be adequately approximated by a first order transfer function with time delay.

\[
G_p = \frac{K e^{-\theta s}}{Ts + 1}
\]  

(13)

Where K is gain, \( \theta \) is the dead time or time delay, and T is the open loop process time constant. Once we have recorded the open loop input/output data, and subsequently measured the times T and \( \theta \), the PID tuning parameters can be obtained directly from the given tables for different classical methods.

Tuning rules based on a measured step response are also called process reaction curve methods. The first (and most well-known) tuning rule of this type was suggested in 1942 [3]; in this method, the process is modeled by a FOPDT process model with the model parameters estimated using a tangent and point method, as indicated in Figure 4.3. Simple formulae are used to define tuning parameters for PI and PID controllers. The PI controller settings are given by of the system response is obtained as shown in the figure:
B: Cohen-Coon Tuning Method

Cohen and Coon based the controller settings on the three parameters \( \theta \), \( T \) and \( K \) of the open loop step response. The main design criterion is rejection of load disturbances. The method attempts to position closed loop poles such that a quarter decay ratio is achieved.

The PID tuning parameters as a function of the open loop model parameters \( K \), \( T \) and \( \theta \) from equation (14) as derived by Cohen-Coon:

**TABLE II : Cohen Coon open loop method**

| Controller | \( K_p \) | \( T_i \) | \( T_d \) |
|------------|----------|----------|----------|
| PI         | \( T/K(0.9+0.1T) \) | 0\((30+30/T)/(9+200/T)) \) | - |
| PI         | \( T/K(4.3+0.4T) \) | 0\((32+60/T)/(13+80/T)) \) | 0\((4)/(11+20/T)) \) |

### IV. ARTIFICIAL BEE COLONY ALGORITHM (ABC) [6-10]

Dervish Karaboga [10] presented the comparison results on the performance of the Artificial Bee Colony (ABC) algorithm for constrained optimization problems. The ABC algorithm has been firstly proposed for unconstrained optimization problems and showed that it has superior performance on these kinds of problems. In this paper, the ABC algorithm has been extended for solving constrained optimization problems and applied to a set of constrained problems [8].

In Bees Algorithm, the colony of artificial bees consists of three groups of bees: employed bees, onlookers and scouts. First half of the colony consists of the employed artificial bees and the second half includes the onlookers. For every food source, there is only one employed bee. In other words, the number of employed bees is equal to the number of food sources around the hive. The employed bee whose the food source has been abandoned by the bees becomes a scout. The position of a food source represents a possible solution to the optimization problem and the nectar amount of a food source corresponds to the quality (fitness) of the associated solution. The number of the employed bees or the onlooker bees is equal to the number of solutions in the population.

A: Implementation of Algorithm

Steps (pseudo-coding) to initialize the artificial BA:

1. Initialize the population of solutions \( X_{i,j} \),
   \( i = 1,2,3 \ldots S \) and \( j = 1,2,3 \ldots D \)

---

**Fig. 7.** System responses for first order time delay transfer function

From the figure we can calculate the time delay (\( \theta \)) and time constant (\( T \)) and maximum response (\( K = Dc \) gain), we can find the parameter of PID controller.

**A: Ziegler-Nichols Tuning Method**

The PID tuning parameters as a function of the open loop model parameters \( K \), \( T \) and \( \theta \) from the Process reaction curve derived by Ziegler-Nichols [2-5].

They often form the basis for tuning procedures used by controller manufacturers and process industry. The methods are based on determination of some features of process dynamics. The controller parameters are then expressed in terms of the features by simple formulas. The method presented by Ziegler and Nichols is based on a registration of the open-loop step response of the system, which is characterized by two parameters. First determined, and the tangent at this point is drawn. The intersections between the tangent and the coordinate axes give the parameters \( T \) and \( \theta \). A model of the process to be controlled was derived from these parameters. This corresponds to modeling a process by an integrator and a time delay. Ziegler and Nichols have given PID parameters directly as functions of \( T \) and \( \theta \). The behavior of the controller is as can be expected. The decay ratio for the step response is close to one quarter. It is smaller for the load disturbance. The overshoot in the set point response is too large.

**TABLE I : Ziegler Nichols open loop method**

| Controller | \( K_p \) | \( T_i \) | \( T_d \) |
|------------|----------|----------|----------|
| Ziegler-Nichols Method (Open Loop) | \( T/K0 \) | - | - |
| PI | \( 0.9T/K0 \) | 0\(/3 \) | - |
| PID | \( 1.2T/K0 \) | 20 | 0.50 |
2. Evaluate the population.
3. Cycle=1
4. Repeat
5. Produce new solutions X_{i,j} for the employed bees by using step (4) and evaluate them.
6. Apply the greedy selection process.
7. Calculate the probability values P_{i,j} for the solutions X_{i,j} by step (4) & (3).
8. Produce the new solutions X_{i,j} for the on looking from the solutions X_{i,j} selected depending on P_{i,j} and evaluate them.
9. Apply the greedy selection process.
10. Determine the abandoned solution for the scout, if exists, and replace it with a new randomly produced solution X_{i,j} by step (4) & (5).
11. Memorize the best solution achieved so far.
12. Cycle = Cycle+1.
13. Until Cycle = MCN.

**B: Objective Function for Particle swarm optimization**

function F= tightness (kd, kp, ki)

\[
T=t(\{[.023\times kd, .023\times kp, .023\times ki] + [.005, .010015, .023\times kd])
\]

\[
S=\text{stepinfo} (T1);
\]

\[
tr=S.\text{RiseTime};
\]

\[
ts=S.\text{SettlingTime};
\]

\[
Mp=S.\text{Overshoot};
\]

\[
Ess=1/(1+\text{degain} (T1));
\]

\[
F= (1-\exp(-0.5)) \times (Mp+Ess) + \exp(-0.5) \times (ts-tr);
\]

**TABLE III : Parameter for ABC**

| Parameter                | Values |
|--------------------------|--------|
| No. of Scout Bees        | 50     |
| No. of Iterations        | 200    |
| No. of Best selected patches | 20  |
| No. of Elite selected patches | 10   |

**C: ABC Flowchart**

The flowchart of the Artificial Bee Colony Optimization based PID control system is shown in figure 8.

**V. SIMULINK MODEL OF DC MOTOR**

The Simulink model of DC motor using is shown in Fig 8.

The Simulink model of various tuning method for speed control of DC motor using PID controller is shown in Fig 9.

**TABLE IV : Parameters of DC Motor**

| Parameter | Values & Unit |
|-----------|---------------|
| R         | Ω             |
| K_t       | 0.023 Kg-m/A  |
| K_r       | 0.023 Vs/rad  |
| L         | 0.5 H         |
| J_m       | 0.01 Kgms²/rad |
| B_m       | 0.03 gms²/rad |

**VI. RESULTS AND DISCUSSION**

The Simulink model in Fig. 8 & 9 was simulated and the plots for various tuning method were observed. Fig. 10 and Fig. 11 show the Speed versus Time plot for conventional and bio inspired optimization method (ABC) respectively.
Performance comparison of different controllers has been reviewed and it is found that Artificial Bee Colony Optimization is best among the all methods which are used for tuning the parameter of PID controller for which settling time and rise is found to be less. The conventional controllers however are not recommended for higher order and complex systems as they can cause the system to become unstable. Hence, a heuristic approach is required for choice of the controller parameters which can be provided with the help of Bio inspired methods such as Artificial Bee Colony Optimization, where we can define variables in a subjective way.

VIII. REFERENCES

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VII. CONCLUSION

It can be seen from the above comparison table that while using the bio-inspired technique (Artificial Bee Colony Optimization) the overshoots obtained is zero as compared to the case when the PID Controller is was tuned via conventional methods. The settling time is also lesser in case of the Artificial Bee Colony Optimization, also the rise time is reduced. The Artificial Bee Colony Optimization PID controller tends to approach the reference speed faster and has, comparatively, a zero overshoot. It can be observed from Fig 11 and 12 that the Conventional PID controller have overshoot from the reference speed and attain a steady state with larger settling time.

TABLE V : Comparative analysis of various tuning methods

| S N | Controller | Kp  | Ki  | Kd  | Ts  | Te  | Mp  |
|-----|------------|-----|-----|-----|-----|-----|-----|
| 1   | Z-N        | 1.385 | 1.67 | 0.282 | 0.5922 | 7.328 | 43.435 |
| 2   | C-C        | 1.545 | 1.55 | 0.228 | 0.444 | 9.17 | 68.7 |
| 3   | ABC        | 71.78 | 6.52 | 76.76 | 0.0063 | 0.012 | 0   |

Fig. 11. Speed versus Time plot with reference speed for PID tuned with Zeigler Nicholas & Cohen Coon

Fig. 12. Speed versus Time plot with reference speed for PID tuned with Artificial Bee Colony optimization (Step response)

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