Kinetic Studies on the Catalytic Degradation of Rhodamine B by Hydrogen Peroxide: Effect of Surfactant Coated and Non-Coated Iron (III) Oxide Nanoparticles

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Received: 3 September 2020; Accepted: 26 September 2020; Published: 29 September 2020

Abstract: Iron (III) oxide (Fe₃O₄) and sodium dodecyl sulfate (SDS) coated iron (III) oxide (SDS@Fe₃O₄) nanoparticles (NPs) were synthesized by the co-precipitation method for application in the catalytic degradation of Rhodamine B (RB) dye. The synthesized NPs were characterized using X-ray diffractometer (XRD), vibrating sample magnetometer (VSM), scanning electron microscopy (SEM), transmission electron microscopy (TEM), and Fourier transform infra-red (FT-IR) spectroscopy techniques and tested in the removal of RB. A kinetic study on RB degradation by hydrogen peroxide (H₂O₂) was carried out and the influence of Fe₃O₄ and SDS@Fe₃O₄ magnetic NPs on the degradation rate was assessed. The activity of magnetic NPs, viz. Fe₃O₄ and SDS@Fe₃O₄, in the degradation of RB was spectrophotometrically studied and found effective in the removal of RB dye from water. The rate of RB degradation was found linearly dependent upon H₂O₂ concentration and within 5.0 × 10⁻² to 4.0 × 10⁻¹ M H₂O₂, the observed pseudo-first-order kinetic rates (kobs, s⁻¹) for the degradation of RB (10 mg L⁻¹) at pH 3 and temperature 25 ± 2 °C were between 0.4 and 1.7 × 10⁴ s⁻¹, while in presence of 0.1% w/v Fe₃O₄ or SDS@Fe₃O₄ NPs, kobs were between 1.3 and 2.8 × 10⁴ s⁻¹ and between 2.6 and 4.8 × 10⁴ s⁻¹, respectively. Furthermore, in presence of Fe₃O₄ or SDS@Fe₃O₄, kobs increased with NPs dosage and showed a peaked pH behavior with a maximum at pH 3. The magnitude of thermodynamic parameters E_a and ΔH for RB degradation in presence of SDS@Fe₃O₄ were 15.63 kJ mol⁻¹ and 13.01 kJ mol⁻¹, respectively, lowest among the used catalysts, confirming its effectiveness during degradation. Furthermore, SDS in the presence of Fe₃O₄ NPs and H₂O₂ remarkably enhanced the rate of RB degradation.

Keywords: magnetite; co-precipitation method; Rhodamine B; sodium dodecyl sulfate; wastewater treatment

1. Introduction

Mushrooming industrialization and urbanization are primarily responsible for deteriorating the surface and sub-surface water quality, causing hazardous effects on both aquatic organisms and human health. Among water contaminants, dyes and pigments, which are widely discharged from textile, pharmaceutical, paint, rubber, cosmetic, and confectionary industries effluents [1,2],
produce unwanted color to water bodies, resulting in intoxication of ecosystems. Rhodamine B (RB) is a synthetic cationic dye, containing a multi-ring aromatic xanthene core planar structure [3]. It is widely used for dyeing and printing applications [4]. The carcinogenic, mutagenic, and toxic effects of RB have been well reported [5–7], evidencing the need of RB contaminated effluents treatment prior to their discharge. Various treatment methodologies, such as reverse osmosis, ion-exchange, precipitation, adsorption, ozone treatment, catalytic reduction, biodegradation, ultrasonic decomposition, coagulation, electrocoagulation, chemical oxidation, and nano-filtration, have been used for the removal of RB and other dyes from water [8–10]. However, high-cost, long process duration, large energy consumption, regeneration difficulties, and pollutants transfer from one phase to another are the major demerits of the aforementioned processes. Thus, advanced oxidation processes (AOPs) are considered comparatively advantageous since they possess favorable decolorizing ability for reactive dyes [11]. Fenton reaction, which is one of the most effective AOPs, has attracted widespread attention. It is operated at acidic pH in the presence of hydrogen peroxide (H\textsubscript{2}O\textsubscript{2}) and ferrous ions while yielding hydroxyl radical with powerful oxidation capacity leading to complete decomposition of organic dyes, thus, converting them into non-toxic lower molecular weight products [12]. In this sense, the Fe\textsuperscript{2+}-H\textsubscript{2}O\textsubscript{2} Fenton system has been widely used for the oxidative removal of RB from water [11–13].

Recently, iron (III) oxide (Fe\textsubscript{3}O\textsubscript{4}) nanoparticles (NPs) have been used for removing various dyes and heavy metals from water [14–16]. These NPs are inert, economical, possess unique magnetic properties, and can be easily separated from reaction medium through an external magnetic field [17–19]. Additionally, Fe\textsubscript{3}O\textsubscript{4} magnetic NPs exhibit a high surface area, depending on the particle size, and show the ability for surface modification. Furthermore, the interaction of Fe\textsubscript{3}O\textsubscript{4} NPs with H\textsubscript{2}O\textsubscript{2} generates hydroxyl and peroxyl radicals, which are able to undergo the oxidative degradation of organic pollutants [20–22]. However, bare Fe\textsubscript{3}O\textsubscript{4} NPs suffer some shortcomings such as agglomeration, limited adsorption ability, and limited working pH range. Coating of Fe\textsubscript{3}O\textsubscript{4} NPs with surfactants, polymers, silica, starch, polyelectrolytes, etc., render an enhancement in their surface properties and chemical stability, making them suitable for industrial wastewater treatment and catalytic applications [23–29]. Among surfactants used for coating, the anionic sodium dodecyl sulfate (SDS) is known to enhance the ability of NPs to remove pollutants from wastewater, which has been related with the binding and chelating efficiency of its functional groups [30]. Although no studies were found on the specific case of RB, Fe\textsubscript{3}O\textsubscript{4} NPs modified with SDS have been successfully used for the adsorptive removal of several dyes from water, including tolonium chloride [31], Basic Blue 41 [32], or Brilliant Green [33].

The present work was undertaken with the aim of developing an efficient, eco-friendly, and economical treatment for the removal of cationic dyes from water. For this purpose, Fe\textsubscript{3}O\textsubscript{4} NPs were synthesized, coated with SDS, and tested as catalyst for the degradation of RB under the presence of H\textsubscript{2}O\textsubscript{2}. The synthesized Fe\textsubscript{3}O\textsubscript{4} and SDS-coated Fe\textsubscript{3}O\textsubscript{4} (SDS@Fe\textsubscript{3}O\textsubscript{4}) NPs were thoroughly characterized through XRD, VSM, SEM, TEM, and FT-IR techniques. The main novelty of this work was the comparative study of the dye degradation by H\textsubscript{2}O\textsubscript{2} under three different situations, namely, in absence of ferrous NPs, in the presence of Fe\textsubscript{3}O\textsubscript{4} NPs, and in the presence of SDS@Fe\textsubscript{3}O\textsubscript{4} NPs. Kinetic experiments were carried out to explore the influence of these catalysts dosages, H\textsubscript{2}O\textsubscript{2}, SDS, and solution pH on the RB degradation rate.

2. Materials and Methods

2.1. Chemicals and Reagents

Rhodamine B (RB: AR grade 80%; CDH, New Delhi, India), hydrochloric acid (HCl: AR grade 36%; Fisher Scientific, Mumbai, India), hydrogen peroxide (H\textsubscript{2}O\textsubscript{2}: 35% v/v, Merck, Mumbai, India), sodium dodecyl sulphate (SDS: 99%; CDH, New Delhi, India), Ammonia solution (NH\textsubscript{4}OH: 25% with purity index 99%, Thermo Fisher Scientific, Mumbai, India), ferrous chloride dihydrate (FeCl\textsubscript{2}·2H\textsubscript{2}O: 99%; CDH, New Delhi), ferric Chloride (FeCl\textsubscript{3}: 97.0%; CDH, New Delhi, India), and sodium hydroxide
pellets (NaOH: 97%, Merck, Mumbai, India) were used as supplied. All the other reagents used during the experimental work were of reagent grade. All the solutions were prepared in deionized (DI) water. The stock solutions of NaOH (1.0 M) and SDS (1.0 \times 10^{-2} \text{ M}) were prepared in DI water. The stock solution (500 mg L^{-1}) of dye was prepared by dissolving 50 mg RB in 100 mL DI water. Likewise, 250 mL stock solution of H\textsubscript{2}O\textsubscript{2} was prepared by dissolving 25 mL of H\textsubscript{2}O\textsubscript{2} in DI water. The stock solution of HCl (0.1 M) was prepared in 100 mL DI water.

2.2. Synthesis and Surfactant Coating of Fe\textsubscript{3}O\textsubscript{4} Magnetic NPs

Magnetic nanoparticles were synthesized by adopting the co-precipitation method as described in the literature [34]. Briefly, Fe\textsubscript{3}O\textsubscript{4} NPs were synthesized by mixing 20.0 g of FeCl\textsubscript{3} (0.4 M) and 10.0 g of FeCl\textsubscript{2}.2H\textsubscript{2}O (0.2 M) into a 1.0 L conical flask. These iron salts were dissolved in 300 mL DI water. The mixture was purged with N\textsubscript{2} gas and stirred for about an hour. Then, liquor ammonia (25%) was added drop-wise in the flask. The pH of the solution in flask was further increased to ~10 by adding 2.0 M of NaOH solution. The temperature of the solution was then raised to 70 °C with stirring and purging of N\textsubscript{2} gas for 5 h. Black precipitate was formed in the flask. It was filtered, washed with acetone, and thereafter with DI water to a neutral pH value. The precipitate was then dried at 70 °C in a vacuum oven. The synthesis of Fe\textsubscript{3}O\textsubscript{4} NPs can be given by the following reaction:

\[
\text{Fe}^{2+} + 2\text{Fe}^{3+} + 8\text{OH}^- \rightarrow \text{Fe}_3\text{O}_4 + 4\text{H}_2\text{O}
\]

To prepare the SDS-coated Fe\textsubscript{3}O\textsubscript{4} NPs, FeCl\textsubscript{3}.6H\textsubscript{2}O (20 g, 0.40 M), FeCl\textsubscript{2}.4H\textsubscript{2}O (10 g, 0.20 M), and SDS (8.64 g, 0.10 M) were taken into the conical flask of 1.0 L capacity containing 300 mL DI water. The overhead stirrer was used to mix the reactants properly. The solution was stirred vigorously for 45 min under the N\textsubscript{2} gas atmosphere. Then, 200 mL of 25% ammonium hydroxide solution was added drop-wise into the above solution until the pH of the resulting solution reached 9–11. The pH of the reaction medium was further raised to 14 by adding 2.0 M NaOH solution drop-wise. The mixture was then stirred vigorously under N\textsubscript{2} gas purging for 5 h. The black precipitate that formed was filtered and washed with acetone and DI water until the pH came to a neutral value.

2.3. Characterization

The crystallinity and phase composition of Fe\textsubscript{3}O\textsubscript{4} and SDS@Fe\textsubscript{3}O\textsubscript{4} NPs were studied by X-ray diffraction (XRD: MiniFlex II, Rigaku, Tokyo, Japan) analysis equipped with a Cu K\textsubscript{\alpha} radiation source (with \(\lambda = 1.5406 \text{ nm}\)). The surface functionalities present over Fe\textsubscript{3}O\textsubscript{4} and SDS@Fe\textsubscript{3}O\textsubscript{4} NPs surface were determined by Fourier infra-red spectrometer (FT-IR: Nicolet iS50, Thermo Fisher Scientific, Madison, WI, USA). The surface morphology and particle size were analyzed by scanning electron microscopy (SEM: JSM-5600LV, JEOL, Tokyo, Japan) and transmission electron microscopy (TEM: CM120, Philips, Amsterdam, The Netherlands). The magnetic properties of Fe\textsubscript{3}O\textsubscript{4} and SDS@Fe\textsubscript{3}O\textsubscript{4} NPs were determined using a vibrating sample magnetometer (VSM: 7307, Lakeshore, Westerville, OH, USA).

2.4. Degradation Kinetic Experiments

A Genesys 10S UV–visible spectrophotometer (Thermo Fisher Scientific, Madison, WI, USA) was used to monitor the change in the absorbance intensity of RB during its degradation under the varying reaction conditions. The spectrophotometer was provided with multiple cell holders in which a 3.0 mL quartz cuvette with a path length of 10 mm was used to measure absorbance. All the kinetic experiments were performed at a constant temperature of 25.0 ± 0.2 °C by using a thermostatic water-bath. A 0.1% \(w/v\) of magnetic Fe\textsubscript{3}O\textsubscript{4} NPs was put together with RB solution with an initial concentration of 10 mg L^{-1} into a three necked round bottom flask of 100 mL capacity. Solution pH was adjusted by adding hydrochloric acid or sodium hydroxide solution and monitored by using a pH meter. The reaction vessel containing RB solution and magnetic Fe\textsubscript{3}O\textsubscript{4} NPs was kept in the
water-bath to equilibrate with the required temperature. The reaction was started with the addition of 
5.0 × 10^{-2} to 4.0 × 10^{-1} M H_{2}O_{2} and zero time was taken when the half of the amount of H_{2}O_{2} was 
added. The concentration of RB was spectrophotometrically analyzed at its maximum absorbance 
wavelength (\lambda_{\text{max}}: 554 nm) at constant time intervals. All the kinetic experiments were carried out 
under pseudo-first-order conditions in which H_{2}O_{2} was kept in excess over RB. The progress of the 
reaction gradually resulted in the decrease of RB concentration and the values of the pseudo-first-order 
rate constants were obtained from the slopes of the plots of ln (absorbance) versus time. Each kinetic 
run was carried out in triplicate to check their repeatability and the rate constant was observed to be 
within the error limits of ~5%.

3. Results and Discussion

3.1. Characterization of Fe_{3}O_{4} and SDS@Fe_{3}O_{4} NPs

3.1.1. X-ray Diffraction (XRD)

Figure 1A shows the XRD patterns obtained for the synthesized Fe_{3}O_{4} NPs and it confirms the 
nanocrystal structure and phase purity of Fe_{3}O_{4} NPs. The diffraction peaks appeared at 2\theta = 30.26^\circ, 
35.5^\circ, 43.12^\circ, 53.74^\circ, 57.10^\circ, and 62.92^\circ corresponding to planes (220), (311), (400), (422), (511), and (440), 
respectively [35], consistent with standard magnetite database (JCPDS-19-0629), indicating a highly 
crystalline nature of Fe_{3}O_{4} NPs. Figure 1B shows the XRD patterns for SDS@Fe_{3}O_{4} NPs with reduced 
peak intensity due to the SDS coating over Fe_{3}O_{4} surface. This confirms crystalline-to-amorphous 
transition of Fe_{3}O_{4} NPs due to SDS coating during SDS@Fe_{3}O_{4} NPs synthesis [36].

![X-ray diffraction patterns](image)

Figure 1. X-ray diffraction patterns for synthesized iron (III) oxide (Fe_{3}O_{4}) (A) and sodium dodecyl 
sulfate (SDS) coated iron (III) oxide (SDS@Fe_{3}O_{4}) (B).

3.1.2. Fourier Transform Infrared Spectroscopy (FTIR)

The FT-IR spectra of Fe_{3}O_{4} and SDS@Fe_{3}O_{4} NPs are shown in Figure 2.
The two peaks at 585 and 435 cm^{-1}, as shown in Figure 2A, correspond to the Fe-O bond vibrations 
of Fe_{3}O_{4} NPs [37]. From these observations, it is confirmed the spinel structure of Fe_{3}O_{4} NPs and also 
inferred the existence of the difference in the bond length in Fe-O. The peak at 3424 cm^{-1} in Figure 2A 
was associated with the O-H stretching vibrations arising from the hydroxyl group due to the presence of 
water molecules associated with Fe_{3}O_{4} [38]. The H-O-H bending of water molecules in Figure 2A is 
observed at 1631 cm^{-1} in Fe_{3}O_{4} NPs [39]. The FTIR spectrum of SDS@Fe_{3}O_{4} NPs is shown in Figure 2B, 
which displayed a new absorption peak at 1252 cm^{-1} due to the stretching vibration of S=O groups of 
SDS and the presence of peaks at 2929 cm^{-1} and 2842 cm^{-1}, which were assigned to the stretching 
mode for aliphatic C-H groups of SDS [40]. The peak at 1635 cm^{-1} in SDS@Fe_{3}O_{4} (Figure 2B) was
attributed to the H-O-H bending of water molecules and that at 3431 cm$^{-1}$ was due to stretching vibration of hydroxyl group on the surface of the NPs. The presence of two peaks at 547 cm$^{-1}$ and at 474 cm$^{-1}$ in Figure 2B is attributed to Fe-O bonds in SDS-modified Fe$_3$O$_4$ [41]. Thus, the FTIR results confirmed successful synthesis of Fe$_3$O$_4$ NPs and their surface modifications through the adsorption of SDS molecules.

3.1.3. Scanning Electron Microscopy (SEM)

The SEM micrograph of the synthesized magnetite (Fe$_3$O$_4$) NPs is shown in Figure 3A. It can be observed that the NPs exhibit spherical surface morphology, having a particle size lower than 100 nm scale with low polydispersity. The SEM image of the SDS@Fe$_3$O$_4$ NPs is shown in Figure 3D on the scale of up to 5 µm. The image depicts successful functionalization of Fe$_3$O$_4$ by SDS and the larger dispersion of SDS@Fe$_3$O$_4$ as compared with Fe$_3$O$_4$ NPs.
3.1.4. Transmission Electron Microscopy (TEM)

The TEM micrograph of pristine Fe₃O₄ NPs (Figure 3B) on the scale of up to 20 µm shows their spherical shape with a narrow range particle size distribution centered at 9 ± 2 nm, as demonstrated by the histogram in Figure 3C. The TEM image of the SDS@Fe₃O₄ NPs is illustrated in Figure 3E. After coating with SDS, the size of SDS@Fe₃O₄ NPs appears to be smaller, as shown by the histogram (Figure 3F). This might be due to the coating of Fe₃O₄ NPs with SDS, which hinders NPs agglomeration.

3.1.5. Vibrating Sample Magnetometer (VSM)

The magnetic behavior of Fe₃O₄ and SDS@Fe₃O₄ NPs was studied by using VSM. As it may be seen in Figure 4, both Fe₃O₄ and SDS@Fe₃O₄ showed superparamagnetic behavior with different magnetic saturations level. The specific magnetic saturation magnitudes for Fe₃O₄ and SDS@Fe₃O₄ NPs were 60.0 and 50.0 emu g⁻¹, respectively, as displayed in Figure 4. Comparatively lower magnetic saturation of SDS@Fe₃O₄ NPs might be due to their coating with SDS [42]. In order to avoid aggregation of Fe₃O₄ NPs, which may severely reduce their catalytic efficiency, coating with SDS was executed in this work. In any case, as for the large magnetic saturation and superparamagnetic property of SDS@Fe₃O₄ NPs (Figure 4), such a coating did not affect the high efficiency in magnetic separation and recovery.

![Magnetization curve for Fe₃O₄ and for SDS@Fe₃O₄ at room temperature.](image)

3.2. Degradation of RB by H₂O₂

The repetitive scans of the reactant mixture containing RB (10 mg L⁻¹) and H₂O₂ (2 × 10⁻¹ M) were recorded at constant time intervals of ten minutes in the visible region (460–600 nm). The temperature and pH were kept constant at 25 ± 0.2 °C and 3, respectively. These spectra, which are shown in Figure 5A, indicated that the absorbance intensities at λₘₐₓ (554 nm) progressively decreased with time. A decrease in the absorbance intensities was due to the degradation of RB by H₂O₂.

The degradation of RB can be represented by the following representative reaction and rate Equation (1):

\[
\text{RB} + \text{H}_2\text{O}_2 \rightarrow \text{Oxidized Products} + \text{H}_2\text{O}, \text{Rate} = -\frac{d[\text{RB}]}{dt} = k_{\text{obs}}[\text{RB}],
\]

where \(k_{\text{obs}}\) is the observed value of the rate constant and was calculated from the slope of the plot of \(\ln \frac{[\text{RB}]}{[\text{RB}]_t}\) versus \(t\). The terms \([\text{RB}]_0\) and \([\text{RB}]_t\) are the concentrations of RB at time zero and at any
time t, respectively. The observed rate constant depends upon the concentration of H$_2$O$_2$ as given by Equation (2). The order of the reaction is assumed to be x with respect to the concentration of H$_2$O$_2$.

$$k_{obs} = k [H_2O_2]^x$$

(2)

where k is the specific rate constant with respect to H$_2$O$_2$ concentration. The values of k and x were respectively obtained from the intercept and slope of the plot of log $k_{obs}$ versus log [H$_2$O$_2$].

Figure 5. UV–visible spectra of Rhodamine B (RB) at various degradation times. In absence of Fe$_3$O$_4$ (A); in presence of Fe$_3$O$_4$ (B); and in presence of SDS@Fe$_3$O$_4$ (C). (Reaction conditions: 10 mg L$^{-1}$ RB, 2.0 x 10$^{-1}$ M H$_2$O$_2$, 0.1% w/v Fe$_3$O$_4$ NPs, 0.1% w/v SDS@Fe$_3$O$_4$, pH 3, and temperature 25 ± 2 °C).

The rate of RB degradation was studied at varied concentrations of H$_2$O$_2$ in the range from 5.0 x 10$^{-2}$ to 4.0 x 10$^{-1}$ M while keeping a RB concentration of 10 mg L$^{-1}$ at pH 3 and temperature 25 ± 0.2 °C. The values of rate constants were calculated and the plot of rate constant versus H$_2$O$_2$ concentration (Figure 6) shows a linear dependence of the rate constant values on H$_2$O$_2$ concentration.

Figure 6. Plots of $k_{obs}$ versus hydrogen peroxide (H$_2$O$_2$) concentration for the degradation of RB. (Reaction conditions: 10 mg L$^{-1}$ RB, 5.0 x 10$^{-2}$ to 4.0 x 10$^{-1}$ M H$_2$O$_2$, pH 3, and temperature 25 ± 2 °C).
3.3. Degradation of RB in the Presence of Fe₃O₄ and SDS@Fe₃O₄ NPs

The addition of 0.1% w/v of Fe₃O₄ NPs to the solution containing RB and H₂O₂ increased the rate of degradation of RB, as is evident from the decrease in the rate of absorbance intensities with time, which is presented in Figure 5). The increase in the degradation rate of RB can be attributed to the catalytic role of Fe₃O₄ NPs. The degradation rate was further increased in the presence of 0.1% w/v SDS@Fe₃O₄ NPs as displayed in Figure 5C.

In order to assess the effect of pH, the degradation rate of RB was studied in the pH range 1–10 by adjusting it with HCl/NaOH solutions. The observed results are presented in Figure 7. The plot of the rate constant versus pH (Figure 7) demonstrates that the values of the rate constant increase with pH until pH 3. Thereafter, on further increasing the pH beyond 3, the values of the rate constant decreased. Thus, a peaked behavior plot was obtained with the maximum degradation rate at pH 3.

![Figure 7](image_url). Effect of pH on the Rhodamine B (RB) degradation process. In presence of Fe₃O₄ (A); and in presence of SDS@Fe₃O₄ (B). (Reaction conditions: 10 mg L⁻¹ RB, 2.0 × 10⁻¹ M H₂O₂, 0.1% w/v Fe₃O₄, 0.1% w/v SDS@Fe₃O₄, and temperature 25 ± 2 °C).

The influence of the magnetic Fe₃O₄ NPs dosage on the RB degradation rate was studied in the range between 0.02% and 0.2% w/v Fe₃O₄. The respective concentrations of H₂O₂ and RB were set at 2.0 × 10⁻¹ M and 10 mg L⁻¹, while the pH and temperature of the solution were 3 and 25 ± 0.2 °C, respectively. The increase in the amount of Fe₃O₄ increased the RB degradation rate, as shown by data graphically presented in Figure 8A. Furthermore, as it may be seen in Figure 8B, the influence of SDS@Fe₃O₄ concentration on the RB degradation rate showed the same pattern observed for Fe₃O₄, but with higher values of the rate constant.

![Figure 8](image_url). Plots of k(obs) versus varying concentration of magnetic nanoparticles (NPs) for the degradation of the RB in presence of Fe₃O₄ (A), and in presence of SDS@Fe₃O₄ (B). (Reaction conditions: 10 mg L⁻¹ RB, 2.0 × 10⁻¹ M H₂O₂, 0.1% w/v Fe₃O₄, 0.1% w/v SDS@Fe₃O₄, pH 3, and temperature 25 ± 2 °C).
The observed enhancement in the rate of the RB degradation in presence of Fe₃O₄ can be described through the production of highly reactive hydroxyl radicals due to the interaction between the NPs and H₂O₂ [43,44], followed by the formation of peroxyl radicals and the subsequent oxidation of RB by these radicals, as described by the following reactions:

(i) \( \text{Fe}^{2+} + \text{H}_2\text{O}_2 \rightarrow \text{Fe}^{3+} + \text{HO}^\cdot + \text{OH}^- \) The possible reactions of free radicals are:

(ii) \( \text{Fe}^{2+} + \text{HO}^\cdot \rightarrow \text{Fe}^{3+} + \text{OH}^- \),

(iii) \( \text{H}_2\text{O}_2 + \text{HO}^\cdot \rightarrow \text{H}_2\text{O}^+ + \text{HO}_2^\cdot \),

(iv) \( \text{HO}_2^- + \text{HO}^\cdot \rightarrow \text{H}_2\text{O} + \text{O}_2 \),

(v) \( \text{HO}^\cdot + \text{HO}^\cdot \rightarrow \text{H}_2\text{O}_2 \),

(vi) \( \text{HO}^\cdot + \text{RB} \rightarrow \text{Products} \),

(vii) \( \text{HO}_2^- + \text{RB} \rightarrow \text{Products} \).

Thus, the oxidation of RB by HO∗and HO₂∗radicals leads to a decrease in its concentration. As for the RB degradation in the presence and absence of Fe₃O₄ and SDS@Fe₃O₄, results shown in Figure 5 to 8 allow to state that RB degradation was enlarged under the presence of Fe₃O₄ and SDS@Fe₃O₄ NPs. As for the degradation rate of RB, it was linearly dependent on the initial concentration of H₂O₂ in the absence of NPs. The RB degradation was comparatively higher in presence of SDS@Fe₃O₄ than Fe₃O₄ and increased with the increase in the dosage of either Fe₃O₄ or SDS@Fe₃O₄ NPs. The variations in pH displayed a similar influence on the RB degradation rate in the presence of Fe₃O₄ and SDS@Fe₃O₄ NPs, the rate showing a peaked behavior. From these observations, it was confirmed that the reaction proceeded through the formation of highly reactive free radicals in the presence of Fe₃O₄ and SDS@Fe₃O₄ NPs due to the interaction between Fe²⁺ and H₂O₂, as described by reactions (i) to (vii). The increase in the amount of the NPs increases the production of HO∗radicals (step (i)) and, therefore, an enhancement in the RB degradation rate was observed with the increase in the NPs dosage, which is coincident with previous observations [45]. As shown in Figure 6, the RB degradation rate increased from 0.4 to 1.7 \( \times 10^4 \) s⁻¹ with increasing H₂O₂ concentration in the absence of NPs. In Figure 9, under the presence of NPs, larger degradation rates are represented, varying between 1.3 and 2.8 \( \times 10^4 \) s⁻¹ in the case of Fe₃O₄ and between 2.6 and 4.8 \( \times 10^4 \) s⁻¹ in the case of SDS@Fe₃O₄, which compare rather well with published rate constants for the catalytic degradation of RB (Table S1 in the Supplementary Materials). However, as it may be seen in Figure 9, in the presence of Fe₃O₄ and SDS@Fe₃O₄ NPs, the rate constant value increased with the concentration of H₂O₂ until it was 2.5 \( \times 10^{-1} \) M H₂O₂, and thereafter decreased with H₂O₂ concentration. After the maximum, this decreasing effect in the rate constant with the increase in the H₂O₂ concentration was due to the other free radical reactions taking place in steps (ii) to (v). Thus, at higher concentrations of H₂O₂, the side reactions scavenged the HO∗radicals and decreased the concentration of free radicals available to oxidize the dye and, therefore, the rate of the reaction decreased [46].

The rate of degradation of RB was highly pH-dependent and, as it is shown in Figure 7, the maximum rate of degradation was observed at pH 3 in the presence and the absence of NPs. At high concentrations of H⁺ ions (pH < 3), peroxide gets solvated to form stable oxonium ions, which enhanced the activity of H₂O₂ and restricted the generation of hydroxyl radicals [47–49]. Moreover, the excess of H⁺ ions acts as hydroxyl radical scavenger and, with the increase in H⁺ ions, the concentration of HO∗radicals decreases, thus, decreasing the rate of reaction [48]. Furthermore, the strong electrostatic interaction between the anionic surfactant head groups and cationic dye molecules at lower pH also decreases the rate of RB degradation. The observed lower rate of reaction at higher pH may be related to the formation of the Fe³⁺-complexes, which decreases the dissolved Fe²⁺ ions that were available to generate free radicals [49].
Figure 9. Effect of H$_2$O$_2$ concentration on RB degradation. In presence of Fe$_3$O$_4$ (A); and in presence of SDS@Fe$_3$O$_4$ (B). (Reaction conditions: 10 mg L$^{-1}$ RB, 5.0 $\times$ 10$^{-2}$ to 4.0 $\times$ 10$^{-1}$ M H$_2$O$_2$, 0.1% w/v Fe$_3$O$_4$, 0.1% w/v SDS@Fe$_3$O$_4$, pH 3, and temperature 25 $\pm$ 2 $^\circ$C).

The higher degradation rate of RB in the presence of SDS@Fe$_3$O$_4$ NPs in comparison with bare Fe$_3$O$_4$ NPs that is observed in Figure 8, might be due to the larger capture of RB by SDS@Fe$_3$O$_4$ than by Fe$_3$O$_4$. Thus, the generated free radicals at the NPs surface can readily attack the attached RB and thus leading to the increase in RB degradation rate. Binding of RB to the SDS@Fe$_3$O$_4$ surface can be explained by the electrostatic interaction between the anionic surfactant and protonated cationic dye at pH 3 [50].

3.4. Effect of SDS Concentration and Fe$_3$O$_4$ NPs Dosage on RB Degradation

The addition of SDS at varied concentrations (5.0 $\times$ 10$^{-4}$ to 5.0 $\times$ 10$^{-2}$ M) to a solution containing RB (10 mgL$^{-1}$), H$_2$O$_2$ (2.0 $\times$ 10$^{-1}$ M), and Fe$_3$O$_4$ (0.1% w/v) NPs at pH 3 resulted in an increase in the rate of the degradation reaction, as shown in Figure 10. On the other hand, an increase in the amount of Fe$_3$O$_4$ NPs from 0.02% to 0.2% w/v at a fixed concentration of SDS (2.0 $\times$ 10$^{-2}$ M) also increased the rate of RB degradation, as shown in Figure 11.

Figure 10. Effect of sodium dodecyl sulfate (SDS) concentration on RB degradation. (Reaction conditions: 10 mg L$^{-1}$ RB, 2.0 $\times$ 10$^{-1}$ M H$_2$O$_2$, 0.1% w/v Fe$_3$O$_4$, pH 3, and temperature 25 $\pm$ 2 $^\circ$C).

The respective degradation rates of RB in presence of SDS and Fe$_3$O$_4$ can be represented by Equations (3) and (4).

\[
\text{RB} + D_n \overset{K_d}{\leftrightarrow} \text{RB}_{\text{mic}} \overset{H_2O_2}{\rightarrow} \text{Products}, \tag{3}
\]

\[
\text{Fe}_3\text{O}_4 + \text{RB}_{\text{mic}} \overset{K_e}{\leftrightarrow} \text{RB}_{\text{mic}} - \text{Fe}_3\text{O}_4 \overset{H_2O_2}{\rightarrow} \text{Products}. \tag{4}
\]
The presence of SDS micelles (Dₙ) partitions RB into micellar (RBmic) and aqueous pseudo-phases resulting into the retardation of RB oxidation with H₂O₂ in the presence of SDS, which may be related to the electrostatic repulsion and, therefore, separation between the species involved in the reaction. However, in the presence of Fe₃O₄, micellised RB (RBmic) is incorporated to the NPs surface to form RBmic−Fe₃O₄ where H₂O₂ interacts to form reactive HO' radicals readily available to oxidize RB at the same site. Therefore, RB degradation is catalyzed and the rate of the reaction increases with increasing SDS concentration in the presence of Fe₃O₄ NPs (Figure 10) and also with increasing the amount of Fe₃O₄ NPs in the presence of SDS (Figure 11). In Figure 10, a two steps increase of the degradation may be observed, which may be related to the formation of premicellar aggregates below the critical micelle concentration (cmc) of SDS and micelles above cmc [8,10,51,52], then increasing micelles formation with SDS concentration. Regarding Figure 11, at a SDS concentration above cmc, an increasing degradation rate occurred under increasing Fe₃O₄ concentration, as previously observed in Figure 8 and explained by reactions (i) to (vii). These results are in agreement with previous studies on RB photocatalytic degradation [53,54].

![Figure 11. Effect of Fe₃O₄ concentration on RB degradation. (Reaction conditions: 10 mg L⁻¹ RB, 0.02% to 0.2% w/v Fe₃O₄, 2.0 × 10⁻² M SDS, pH 3, and temperature 25 ± 2 °C).](image)

3.5. Effect of Temperature on RB Degradation

The effect of temperature on RB degradation (10 mg L⁻¹) in aqueous solutions in the presence of H₂O₂ (2.5 × 10⁻¹ M) and at pH 3 was studied at varied temperatures ranging from 25 to 60 °C (because above 60 °C, due to thermal disintegration of H₂O₂ and free radicals, the rate of RB degradation slowed down) in the absence or in the presence of Fe₃O₄ NPs (0.1% w/v), Fe₃O₄ NPs (0.1% w/v) together with SDS (2.0 × 10⁻² M) or SDS@Fe₃O₄ (0.1% w/v).

The energy of activation was calculated using the Arrhenius equation Equation (5), which gave a straight line plot for log k versus 1/T.

\[
\log k_{\text{obs}} = -\frac{E_a}{2.303 RT} + \log A_0
\]  

where \(E_a\) is the activation energy (kJ mol⁻¹), \(R\) (8.314 J mol⁻¹K⁻¹) is the universal gas constant, \(T\) is the temperature in Kelvin (K), \(A_0\) is the frequency factor, and \(k_{\text{obs}}\) is the measured first-order rate constant. The \(E_a\) was determined from the slope and values are given in Table 1.

The value of \(\Delta H\) (enthalpy of activation) and \(\Delta S\) (entropy of activation) were calculated using the Eyring equation Equation (6).

\[
\ln\left(\frac{k_{\text{obs}}}{T}\right) = -\frac{\Delta H}{R} \times \frac{1}{T} + \ln \frac{k_B}{R} + \frac{\Delta S}{R},
\]  

where \(k_B\) is Boltzmann constant.
where $k_B$ is the Boltzmann’s constant and $h$ is the Plank’s constant. A plot of $\ln (k_{\text{obs}}/T)$ versus $1/T$ produces a straight line and the values of $\Delta H$ and $\Delta S$ may be obtained from the slope and the intercept, respectively. The so determined $\Delta H$ and $\Delta S$ values are given in Table 1.

As it may be seen in Table 1, good fittings ($R^2 > 0.94$) to the Erying equation were obtained within the temperature range here considered. The largest $E_a$ and $\Delta H$ determined for RB degradation were those in the absence of NPs. These values progressively decreased in the presence of Fe$_3$O$_4$ NPs, Fe$_3$O$_4$ NPs together with SDS and SDS@Fe$_3$O$_4$, which provided the lowest $E_a$ and $\Delta H$. Regarding the $\Delta S$, although the effect was not so remarkable as for $E_a$ and $\Delta H$, slightly lower values were also determined under the presence of NPs. These results point to the energetically favorable effect of Fe$_3$O$_4$ and SDS@Fe$_3$O$_4$ NPs, which confirms that these are efficient catalysts.

Table 1. Activation parameters determined for RB degradation by H$_2$O$_2$ in the absence and presence of Fe$_3$O$_4$ and SDS and SDS@Fe$_3$O$_4$.

| Reaction Media | $E_a$ (kJ mol$^{-1}$) | $\Delta H$ (kJ mol$^{-1}$) | $\Delta S$ (J mol$^{-1}$K$^{-1}$) | $R^2$ |
|----------------|----------------------|----------------------------|-------------------------------|-------|
| H$_2$O$_2$     | 69.47                | 66.85                      | $-132.66$                     | 0.949 |
| H$_2$O$_2$ + Fe$_3$O$_4$ | 28.47               | 25.86                      | $-188.18$                     | 0.953 |
| H$_2$O$_2$ + Fe$_3$O$_4$ + SDS | 32.47               | 29.86                      | $-194.42$                     | 0.945 |
| H$_2$O$_2$ + SDS@Fe$_3$O$_4$ | 15.63               | 13.01                      | $-149.00$                     | 0.953 |

Reaction conditions: 10 mg L$^{-1}$ RB, 2.0 $\times$ 10$^{-3}$ M H$_2$O$_2$, 0.1% w/v Fe$_3$O$_4$ (when present), 0.1% w/v SDS@Fe$_3$O$_4$ (when present), 2.0 $\times$ 10$^{-2}$ M SDS, pH 3, and varied temperatures (between 25 and 60 °C).

4. Conclusions

In this work, Fe$_3$O$_4$ NPs were synthesized, coated with SDS to synthesize SDS@Fe$_3$O$_4$ NPs, and both tested as catalysts for the oxidation of RB under H$_2$O$_2$. The main novelty was to compare the dye degradation under three different situations, namely, in presence of just H$_2$O$_2$, of H$_2$O$_2$ and Fe$_3$O$_4$ NPs, and H$_2$O$_2$ and SDS@Fe$_3$O$_4$ NPs. Observed pseudo-first-order kinetic rates ($k_{\text{obs}}$, s$^{-1}$) for the degradation of RB (10 mg L$^{-1}$) at pH 3 and temperature 25 ± 2 °C were between 0.4 and 1.7 $\times$ 10$^4$ s$^{-1}$, linearly dependent upon H$_2$O$_2$ concentrations within 5.0 $\times$ 10$^{-2}$ to 4.0 $\times$ 10$^{-1}$ M. Under identical experimental conditions, except for the presence of 0.1% w/v NPs, the observed rates increased to values between 1.3 and 2.8 $\times$ 10$^4$ s$^{-1}$ in the case of Fe$_3$O$_4$ and between 2.6 and 4.8 $\times$ 10$^4$ s$^{-1}$ in the case of SDS@Fe$_3$O$_4$. Fe$_3$O$_4$ NPs with H$_2$O$_2$ gave readily the highly reactive hydroxyl radicals, which enhanced the rate of RB degradation. Furthermore, an increased catalytic effect was observed for SDS@Fe$_3$O$_4$ because the SDS coating avoided Fe$_3$O$_4$ aggregation and the consequent efficiency depletion. However, under the presence of Fe$_3$O$_4$ and SDS@Fe$_3$O$_4$ NPs, $k_{\text{obs}}$ did not increase linearly with H$_2$O$_2$ concentration but just until 2.5 $\times$ 10$^{-1}$ M H$_2$O$_2$, then decreased with increasing H$_2$O$_2$ concentration, which was associated to free radical competitive reactions. On the other hand, it was verified that the addition of SDS molecules to the dye solution containing Fe$_3$O$_4$ also increased the rate of reaction, which was related to the incorporation of micellized RB ions onto the Fe$_3$O$_4$ NPs surface. Overall, this work demonstrated that the application of Fe$_3$O$_4$ and SDS@Fe$_3$O$_4$ along with H$_2$O$_2$ can be an efficient method for the rapid removal of cationic dyes from wastewater in line with the green chemistry principles.

Supplementary Materials: The following are available online at http://www.mdpi.com/2073-4360/12/10/2246/s1, Table S1: Published results on the rate constant ($k_{\text{obs}}$, s$^{-1}$) for the catalytic degradation of RB using different catalysts.

Author Contributions: Conceptualization, M.Z.A.R. and M.A.K.; methodology, M.Z.A.R. and M.S.A.; software, M.S.A. and K.R.; validation, M.S.A. and K.R.; formal analysis, M.S.A.; investigation, M.S.A. and K.R.; resources, M.Z.A.R.; data curation, M.Z.A.R. and M.S.A.; writing—original draft preparation, M.S.A.; writing—review and editing, M.A.K. and M.O.; visualization, M.O.; supervision, M.Z.A.R.; project administration, M.Z.A.R.; funding acquisition, M.A.K. and M.O.; revision, M.A.K. and M.O. All authors have read and agreed to the published version of the manuscript.

Funding: Marta Otero is thankful to the Portuguese “Fundação para a Ciência e a Tecnologia” (FCT) for the Investigator Program (IF/00314/2015). We would also like to thank FCT/Ministério da Ciência, Tecnologia e
Ensino Superior (MCTES) for the financial support to CESAM (UIDP/50017/2020+UIDB/50017/2020) through national funds.

Conflicts of Interest: The authors declare no conflict of interest. Furthermore, the funders had no role in the design of the study; in the collection, analyses, or interpretation of data; in the writing of the manuscript, or in the decision to publish the results.

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