Electrodeposition of Ni nanoparticles from deep eutectic solvent and aqueous solution promoting high stability electrocatalyst for hydrogen and oxygen evolution reactions

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Abstract
Nanostructured Ni films were synthesized from two distinct baths and were assessed as electrocatalysts for hydrogen evolution reaction (HER) and oxygen evolution reaction (OER) in 1 M KOH. Herein, Ni was electrodeposited from two separate solvents, the aqueous acetate buffer and ethaline solvent as a kind of deep eutectic solvents (DESs), and both the deposited films were investigated as electrocatalysts for HER and OER. The electrodeposition parameters such as pH and deposition potential were studied. The electrodeposition process was performed using chronoamperometry technique and Ni deposits were characterized by scanning electron microscopy (SEM), transmission electron microscopy (TEM), energy-dispersive X-ray spectroscopy (EDX), and X-ray diffraction (XRD). Fabricated Ni@PGE deposit from ethaline only requires an overpotential of −154 mV and 350 mV to achieve a current density of 10 mA cm−2 for HER and OER, respectively. While, Ni@PGE from acetate requires an overpotential of −164 mV and 400 mV to produce the current density of 10 mA cm−2 for HER and OER.

Keywords Ni electrodeposition · Deep eutectic solvents · Hydrogen evolution reaction · Oxygen evolution reaction · Acetate bath

Introduction
Excessive usage of fossil fuel–based energy systems (such as coal, petroleum, and natural gas) pollutes the environment. As a result, the globe invests heavily in the development of renewable and green energy applications [1–8]. Because of its high energy density (140 M J kg−1) and zero emissions, hydrogen is one of the most promising energy sources [9–12]. Thus, electrochemical water splitting in an alkaline medium is a facile and effective approach for producing pure hydrogen and oxygen with no pollution [13–16]. However, both the hydrogen evolution reaction (HER) and the oxygen evolution reaction (OER) have very slow kinetics and require a high overpotential to happen [17–20]. As a result, the development of an intrinsic electrocatalyst with high electrocatalytic activity is critical. To date, the most suited electrocatalysts that have been used for HER are Pt and Ru, or Ir oxides for OER [21–24]. Nevertheless, the insufficiency and high cost of these metals prevent their applications [25, 26]. To overcome these challenges, the design of an electrocatalyst with a high activity towards HER and OER is important and urgent. Thus, there are many strategies employed to design an electrocatalyst and develop its surface electronic structure with more active sites to enhance its catalytic performance. So, the challenge is based on discovering a non-precious catalyst with high catalytic activity and stability to be available for both HER and OER. Among transition metals, Ni was selected as it has good electrocatalytic activity towards HER and OER. Ni has remarkable properties which make it a terrific catalyst used in different related energy applications such as supercapacitors, hydrogen evolution reaction, and oxygen evolution reaction [27–30]. Y et al. have synthesized α(Ni(OH)2) nanoplates supported on Pt by hydrothermal
method with high activity towards HER [31]. $\alpha$(Ni(OH)$_2$)/NF was prepared via electrochemical deposition by Balarm et al. introducing high activity for OER. Rao et al. have designed hexagonal Ni(OH)$_2$ supported on NF via hydrothermal preparation which produces an overpotential of 172 mV for HER to reach a current density of 20 mA cm$^{-2}$ and 330 mV to reach a current density of 50 mA cm$^{-2}$ for OER in 1 M KOH [32]. Taşçi et al. have constructed 3D Ni nanodomes via physical vapor deposition which possesses low overpotential of 85 mV and high stability for HER [33]. Ni(OH)$_2$@Ni/CC electrode introduces 458 mV value of overpotential to give 100 mA cm$^{-2}$ for OER [34]. Most of the catalysts that are used for water splitting are in a powder form and need a binder or adhesive agent to attach to the electrode surface as Nafion and PTFE which blocks the active sites of the catalyst during the time, decreasing its stability and its catalytic activity. The electrodeposition technique is one of the most important and cheap methods that is used for nanomaterial preparation which assists the catalyst preparation with high activity. Therefore, in this work, we improved the properties of the Ni catalyst producing high catalytic activity for both HER and OER depending on a simple and cheap method via the electrodeposition technique. The bath composition and pH affect the deposit morphology, coating properties, and adhesion. First, we prepared two different electrolytes with different properties and made the deposition process of Ni from them. The first electrolyte is acetate buffer and the second is deep eutectic solvent (DES) which has unique physical and chemical properties [35]. DESs have distinct properties as they have wide potential window. Thus, many metals and their alloys which are difficult to be fabricated from the aqueous solvents because of the passivation of the electrode are easily electrodeposited from DESs. Moreover, an increase in the temperature of DESs produces narrower electrochemical windows and in larger capacitance currents [36]. The most popular one is ethaline which consists of choline chloride and ethylene glycol. It is prepared by mixing them with a different new ratio 1:3 until forming a homogeneous colorless solution. The two different electrolytes give us two different properties, and morphologies for Ni deposits. Second, we evaluated the catalytic activity, the kinetics, and the efficiency of the fabricated electrodes from the two solvents for HER and OER.

Experimental

Chemicals

All chemicals are purchased from Sigma and Aldrich without further purification. We made two baths, one in an aqueous solution and the other in ethaline. Table 1 contains all the chemicals that are used and their chemical formula with their purity.

Fabrication of Ni nanostructures from DES bath

DES was developed with a 1:3 molar ratio of choline chloride (ChCl) and ethylene glycol (EG) (this solvent is known as ethaline). It was prepared by mixing the molar ratio at temperature 333 K until a colorless liquid solvent was formed. Afterward, 0.4 M of NiCl$_2$.6H$_2$O was added to ethaline. The electrodeposition process and electrochemical measurements were carried out on an electrochemical work station via a computer-controlled potentiostat/galvanostat model 273 A from Princeton Applied Research, Oak Ridge, TN, the USA, with software of 270/250-PAR 10-mL glass cell containing three electrodes: Pencil graphite electrode (PGE) with 0.0314 cm$^2$ surface area was employed as a working electrode, a silver wire was used as a quasi-reference electrode (QRE), and a platinum wire was used as the counter electrode. The utilization of this type of quasi-reference electrode prevents the possible impurities from the working electrode [37–39]. The working electrode was cleaned and smoothed before each run by adding in conc. HCl for 1 min to remove any attached particles or contaminations to the surface. After that, polishing was done with emery papers having different grades (from 1200 to 2500 P). The electrodeposition process was performed at a constant potential of $-0.98$ V under mild stirring at 318 K for 900 s. Scheme 1 illustrates the deposition process from DES.

Fabrication of Ni nanostructures from acetate bath

In this section, the electrolyte of 0.4 M NiCl$_2$.6H$_2$O was made in a pH 5.8 acetate buffer (0.2 M) calibrated by 0.1 M NaOH. The deposition process was performed at a potential of $-1.1$ V for 900 s at room temperature with slight agitation by the same previous electrodes.

Material characterization

Scanning electron microscopy (SEM) was used to exhibit the morphology of the deposited materials.
Energy-dispersive X-ray spectroscopy (EDX) was used to investigate the composition of the deposits: SEM instrument (JEOL, JSM IT-100) with a maximum magnification of 300,000×, maximum resolution of 3 nm, and maximum acceleration voltage of 30 kV; EDX instrument (silicon drift detector) with an energy resolution about 129 eV or better analysis condition of WD 10 mm and voltage 20 kV. Transmission electron microscopy (TEM) was used to investigate the internal structure of the deposited Ni from DES: TEM instrument (JEOL, JEM-200) with a maximum magnification of 1.5 million×. X-ray diffraction (XRD) was used to show the crystallography structure of the deposited electrocatalysts: XRD instrument (Shimadzu XRD 6000, X-ray diffractometer Cu k alpha radiation (wavelength = 1.5418 Å)). Both films of Ni thickness were very small, so the SEM, XRD, and EDX measurements were accomplished on the deposited films at PGE per se to prevent the distortion of the morphology or the structure, while TEM measurement needs the material in a powder form to make a suspension solution. Therefore, the deposits were scratched carefully.

**Electrochemical studies**

In a conventional three-electrode electrochemical cell, the electrochemical performance of both electrodeposited Ni from acetate and ethaline was investigated. The working electrode was made up of Ni plated films, while the reference and counter electrodes were made up of Ag/AgCl (3 M KCl) and Pt wire, respectively. In the case of HER and OER measurements, linear sweep voltammetry (LSV) was used in a solution containing 1 M KOH at a scan rate of 50 mV s⁻¹ at room temperature. For the fabricated Ni
electrodes, all potential data or overpotential was related to RHE, which can be calculated using the following equation (Eq. 1) [40].

\[
E_{\text{vs RHE}} = E_{\text{vs Ag/AgCl (3 M KCl)}} + E_{0 \text{ vs Ag/AgCl (3 M KCl)}} + 0.059 \times pH (E_{0 \text{ vs Ag/AgCl (3 M KCl)}} = 0.210 \text{ V})
\]

where \(E_{\text{vs Ag/AgCl (3 M KCl)}}\) is the measured potential for HER or OER in the experiment and \(E_{0 \text{ vs Ag/AgCl (3 M KCl)}}\) is the standard electrode potential.

### Results and discussion

**Electrochemical fabrication of Ni nanostructures at pencil graphite electrode**

**Cyclic voltammetry study**

To determine the appropriate electrodeposition potential, a cyclic voltammogram of 0.4 M Ni\(^{2+}\) in the aqueous acetate buffer at pH 5.8 was implemented at a scan rate of 20 mV s\(^{-1}\). The control cyclic voltammetry experiment for PGE in acetate bath and ethaline was accomplished at a scan rate of 20 mV s\(^{-1}\). As presented in Fig. 1a, no peaks appeared for both the acetate solution and ethaline solvent. The cyclic voltammogram of Ni in acetate buffer is shown in Fig. 1b. Two reduction peaks exist in the reduction area, one at \(-0.9 \text{ V}\) with low current density and the other at \(-1.1 \text{ V}\) with a high current density, which are used for the deposition process by the CA technique, and an anodic peak at \(-0.4 \text{ V}\) with tiny current density. The cyclic voltammogram of 0.4 M Ni\(^{2+}\) in ethaline at a scan rate of 20 mV s\(^{-1}\) and a temperature of 318 K is shown in Fig. 1b. It is noticed that there are two redox couples observed: the oxidation peak is at \(-0.55 \text{ V}\), while the reduction peak is located at \(-0.98 \text{ V}\) which is used for the deposition process. It is remarkable that the reduction peak position of Ni\(^{2+}\) in ethaline is shifted to a less negative potential value as the ethaline solvent acted as a complexing agent. In the cathodic direction of the CV, a layer of HBD molecules adheres to the electrode surface, while choline chloride cations are in contact with the electrolyte forming Ni-complex which decreases the reduction potential and the nucleation process, providing smaller particle size compared to the deposited Ni from acetate. [36].
The effect of scan rate on the reduction process of Ni$^{+2}$ ions in acetate buffer solution

More voltammetric experiments were established for calculating the diffusion coefficient of Ni$^{+2}$ species. Figure 2a shows the CV of 0.4 M NiCl$_2$·6H$_2$O in acetate buffer solution with pH 5.8 at different scan rates of 30, 40, 50, 70, and 90 mV s$^{-1}$ at room temperature. The position of the cathodic peak potential is shifted to a more negative value and the peak separation increases by increasing the scan rate. It was observed that both of the anodic peak current density and the reduction peak current density increase which indicates that the process of the reduction of Ni$^{+2}$ ion species may be irreversible [41]. However, the value of the half cathodic peak width ($E_{pc} - E_{pc/2}$) changes with a small value by increasing the scan rate while the separation between the anodic peak potential and the cathodic peak potential ($E_{pa} - E_{pc}$) is 0.82 V at the lowest scan rate of 30 mV s$^{-1}$ and $T = 298$ K. This behavior indicates the sluggishness of the rate of the electron transfer. This value is higher than the calculated theoretical value of the fast reversible exchange process being 2.3 RT/nF (30 mV when $n = 2$, $T = 298$ K), confirming the slow nature of electron exchange between Ni$^{+2}$ and the working electrode. Figure 2b demonstrates the variation between the cathodic peak current density and square root of scan rates which exhibits a good linear relationship, revealing that the electroactive Ni$^{+2}$ ion species undergoes diffusion-controlled process. As discussed, the reduction of Ni$^{+2}$ ions is a slow charge transfer process, so its diffusion coefficient can be calculated by using the Randles–Sevcik equation (Eq. 2) [42].

$$ip = 0.4958nFACD^{1/2}\left(\frac{nαFν}{RT}\right)^{1/2}$$

(2)

where $ip$ is the cathodic peak current in ampere, $n$ is the number of electron transfer, $A$ is the electrode surface area in cm$^2$, $F$ is the Faraday constant in C·mol$^{-1}$, $D$ is the diffusion coefficient in cm$^2$·s$^{-1}$ of Ni$^{+2}$ ion species, $ν$ is the scan rate in V·s$^{-1}$, $C$ is the concentration of Ni$^{+2}$ species in mol·cm$^{-3}$, $α$ is the transfer coefficient, $n_α$ is the number of electrons participating in the rate determining step, $R$ is the gas constant, and $T$ is the thermodynamic temperature. $αn_α$ is determined from Eq. 3.

![Fig. 4 SEM images of a bar electrode and b Ni deposit at PGE electrode from acetate buffer with pH 5.8 at a deposition potential of −1.1 V for 900 s. c Ni deposit at PGE electrode from ethaline at 318 K for 900 s.](image)

![Fig. 5 EDX spectrums of Ni deposits from a acetate and b ethaline.](image)
From this equation, the calculated value for $\alpha_n$ equals 0.72. By substituting in Eq. 2, the calculated value for the diffusion coefficient of Ni$^{2+}$ species is found to be $4.76 \times 10^{-7}$ cm$^2$ s$^{-1}$.

**The effect of scan rate on the reduction of Ni$^{2+}$ ions from DES**

Figure 3a represents CV measurements of 0.4 M NiCl$_2$·6H$_2$O in ethaline DES with different scan rates of 30, 50, 70, 90, and 120 mV s$^{-1}$ at PGE at 318 K. It was found that the reduction peak potential is shifted to a more negative value and the current density for both oxidation and reduction peak increases by increasing the scan rate, providing that the nature of the electron transfer is slow. Figure 3b exhibits the variation of the peak current density with the square root of the scan rate, indicating that the electroactive species of Ni$^{2+}$ ions undergo diffusion-controlled process, while the linear plot of Fig. 3b does not pass through the origin, which may be attributed to the nucleation and growth process that takes place during the diffusion process and/or because of the additional current that results from the resistance of the electrolyte [43–45]. Finally, the rate of charge transfer process of Ni$^{2+}$ species is found to be a sluggish process with one-step two-electron transfer [46]. The diffusion coefficient of Ni$^{2+}$ ions in ethaline is also calculated by using the Randles–Sevcik equation (Eq. 2) giving a value of $1.2 \times 10^{-7}$ cm$^2$ s$^{-1}$ which is slower than the diffusion coefficient of Ni$^{2+}$ ions in acetate buffer solution due to its higher viscosity. The peak separation ($\Delta E_p$) for the reduction reaction of Ni$^{2+}$ ions in the acetate bath is equal to 820 mV while in the case of Ni ions in ethaline solvent is equal to 430 mV which means that the electrode reaction of Ni$^{2+}$ ions in the acetate buffer is slow while fast kinetics electrode reaction of Ni$^{2+}$ ion reduction in ethaline compared with Ni$^{2+}$ ions in the acetate according to its $\Delta E_p$ value as it has lower value.

**Characterization of Ni deposits**

**Morphology and composition**

The surface appearance, content, and crystallographic structure of Ni films produced from acetate buffer and ethaline were investigated and characterized using SEM, TEM, EDX, and XRD. The SEM pictures and EDX for the produced Ni nanostructures from acetate buffer, ethaline, and bare PGE are presented in Fig. 4a–c.

Figure 4a exhibits the SEM image of the PGE surface before Ni electrodeposition, which reveals that the surface is empty, smooth, and featureless due to polishing scratches. The SEM image of the Ni deposit from the acetate solution, shown in Fig. 4b, indicates a homogeneous cauliflower morphology filling the electrode surface, implying that the electrodeposition process takes place in a spherical coordinated way.

In Fig. 4c, the nanostructured Ni deposit from ethaline is efficiently deposited, forming a flower with needles, and a tight, intense surface, and covering the graphite electrode surface zones, as seen in the SEM image.

**Elemental composition analysis**

The EDX spectrum for Ni nanoparticles from ethaline bath can be seen in Fig. 5b, which reflects the characteristic peak of Ni, verifying the appearance of a pure Ni with an atomic percentage and weight percentage of 100, while in Fig. 5a the EDX spectrum for Ni nanoparticles from acetate gives

\[
|E_{pc} - E_{pc/2}| = 1.857RT / \alpha_n F
\]

Table 2 The atomic and weight percentages of the deposited Ni nanoparticles from acetate and ethaline

|                      | Ni peak          | Oxygen peak       |
|----------------------|------------------|-------------------|
|                      | Atomic percentage| Weight percentage | Atomic percentage| Weight percentage |
| Ni@PGE from acetate  | 84.22%           | 95.14%            | 15.78%           | 4.86%             |
| Ni@PGE from ethaline| 100%             | 100%              | -                | -                 |

![Fig. 6 XRD for fabricated Ni/PGE from ethaline and acetate bath. The inset of the graph corresponds to XRD for bare PGE](image-url)
the characteristic peak of Ni with an atomic percentage of 84.22% and weight percentage of 95.14%. Moreover, the appearance of a characteristic peak of oxygen with an atomic percentage of 15.78% and weight percentage of 4.86% may be a result of the oxidation of the Ni nanoparticles. These high mass and atomic percentages of Ni peaks indicate that Ni electrodeposition from ethaline and acetate bath is a successful process. The elemental composition of each characteristic peak of the deposit is tabulated in Table 2.

XRD and TEM analysis

X-ray diffraction had been used to establish the crystalline nature and crystallite size. The XRD of both fabricated Ni from acetate and ethaline solvents can be seen in Fig. 6, which includes three diffraction patterns for the bare graphite electrode at a 2θ value of 26° with high intensity; the XRD of both fabricated Ni from acetate and ethaline solvents is shown in Fig. 6 that contains three diffraction peaks for the electrodeposited Ni from acetate at 2θ values of 44.4°, 52.2°, and 77.2° which correlate to diffraction planes (111), (200), and (220) respectively according to JCPDS card no. 041–0850. It is remarkable that the presence of different phases like (220) plane corresponds to NiO but with a small intensity and this is confirmed by EDX which provides a small characteristic peak of oxygen, while the predominant phase with high intensity relates to diffraction plan (111). Furthermore, the Ni deposit from ethaline exhibits three diffraction peaks at 2θ values of 44.4°, 52.2°, and 77.2° that correlate to diffraction planes (111) with the highest intensity, (200), and (220), suggesting that Ni has an FCC shape [47, 48]. As presented, the diffraction peaks of nanostructured Ni deposit from ethaline perform a lower intensity which suggests and validates the small size of its crystallite particles [47]. According to the Scherrer equation (Eq. 4), the crystallite sizes for the produced Ni deposit from acetate and ethaline were 28 nm and 20 nm, respectively.

\[ D = \frac{K\lambda}{\beta\cos\theta} \]  

where \( D \) represents the crystallite size in nm, \( K \) (0.9) is the Scherrer constant, \( \lambda \) is the wavelength of incident X-ray (0.15406 nm), and \( \beta \) represents the radian value of width at half height of the peak [48].

Transmission electron microscopy (TEM) was used to show the Ni film morphology details and their geometric shape as shown in Fig. 7. TEM image of the fabricated Ni electrode from ethaline shows that a metallic Ni has a cubic shape. Figure 8 shows the internal morphology details of
fabricated Ni nanoparticles from acetate with different magnifications which provides a spherical shape of these particles.

**pH optimization of Ni nanoparticle electrodeposition from acetate buffer**

The pH of the electroplating bath is very important to be controlled to reduce the pitting of the deposit by the hydrogen evolution and also changes the morphology of the deposit and its catalytic activity. Figure 9a–d show the SEM images of the deposited Ni nanoparticles from different pH of acetate buffer with different magnification scales. Figure 9a represents the SEM images of the deposited Ni nanoparticles from acetate bath at pH 3; the images show uneven surface with coarse grain particles because of the agglomeration of the spherical particles. By increasing the pH value to 4.6 (b), the images show porous spherical particles with pitting due to the hydrogen gas evolution because at low pH the overpotential of the hydrogen evolution reaction is decreased providing the hydrogen gas evolution which
adsorbed at the cathode surface, decreasing the active sites of the Ni nucleation [49]. Furthermore, by increasing the pH to a high value of 5.8 (c), the surface becomes more uniform with fine distributed particles forming a cauliflower shape that gives higher catalytic behavior of Ni nanoparticles. At very high pH value 8.5 (d), the particles become very high soft with oval-rod structure with cracking surface.

**Electrodeposition potential optimization of Ni nanoparticles from acetate and ethaline solvents**

The deposition potential varies from two distinct baths, so various morphologies and catalytic efficiency were obtained. It was discovered that shifting the reduction potential to more negative values in two distinct baths with the same amplitude provides various morphologies and characteristics of the deposit resulting in different catalytic properties towards HER. Figure 10a–c exhibit SEM images of Ni deposits from an acetate bath with pH 5.8 at room temperature for 900 s at different deposition potentials (−0.96 V, −1.1 V, and −1.3 V, respectively) and a’–c’ fabricated electrodes by Ni nanoparticles from ethaline at 318 K for 900 s at different deposition potentials (−0.85 V, −0.98 V, and −1.16 V, respectively).

**Fig. 10** SEM images of a–c fabricated electrodes by Ni nanoparticles from acetate with pH 5.8 at room temperature for 900 s at different deposition potentials (−0.96 V, −1.1 V, and −1.3 V, respectively) and a’–c’ fabricated electrodes by Ni nanoparticles from ethaline at 318 K for 900 s at different deposition potentials (−0.85 V, −0.98 V, and −1.16 V, respectively)

The Ni deposit at a potential of −0.96 V (a) has a star shape that changes to a homogeneous cauliflower structure when the potential is increased to −1.1 V (b). The particles agglomerate and their sizes grow as the potential increases, as seen in Fig. 6 at a potential of −1.3 V (c), where the particles become spherical like a ball with a bigger size and are not evenly dispersed. Figure 10a’–c’ depict the various geometries and morphologies of Ni films deposited from...
ethylaline at 318 K for 900 s. The deposition at a potential of −0.85 V appears smooth nodular grains by increasing the cathodic potential to −0.98 V; Ni coatings become well distributed with a uniform needle flower shape filling the surface very well, and then, the particles agglomerate gradually at a high overpotential of −1.16 V forming large particles with random distribution as a fractured layer stuck together. Ni coatings have large particles at a cathodic potential of −1.16 V because of the high overpotential that accelerates the growth rate and this observation agrees with the observation of Wang et al. [50]. The various deposition potentials disclose various morphologies and structures, as can be observed. Additionally, the varied morphologies revealed and confirmed distinct catalytic activity towards HER after deposition from two different baths [52, 53].

| Ni films                  | η (mV) | Tafel slopes (mV dec⁻¹) | j₀ (A cm⁻²) | α  |
|--------------------------|--------|-------------------------|-------------|----|
| Ni@PGE from acetate      | −164   | 147                     | 7.7×10⁻⁴    | 0.20|
| Ni@PGE from ethaline     | −154   | 130                     | 8.3×10⁻⁴    | 0.22|
| Bare PGE                | −490   | 327                     | 3.3×10⁻⁴    | 0.09|

Table 3 Overpotential values for HER, Tafel slopes, and kinetics parameters for different fabricated electrodes in 1 M KOH at room temperature and a scan rate of 50 mV s⁻¹

Comparison between the electrocatalytic activities of fabricated Ni nanoparticles at PGE from acetate and ethaline for HER

Figure 11a shows linear sweep voltammetry (LSV) in 1 M KOH for HER at a scan rate of 50 mV s⁻¹ by fabricated Ni nanoparticles at PGE from acetate, ethaline, and bare electrode. It was found that the bare electrode has the lowest catalytic activity and the highest onset potential among them; at a current density of 10 mA cm⁻², it possesses an overpotential (η) of −490 mV vs RHE. Meanwhile, the fabricated Ni nanoparticles from acetate possess an overpotential of −164 mV at a current density of 10 mA cm⁻² and the fabricated Ni nanoparticles from ethaline only requires an overpotential of −154 mV to reach 10 mA cm⁻², which means the highest catalytic activity of Ni nanoparticle deposit from ethaline compared with the other fabricated Ni electrode from acetate, while the bare electrode is inactive towards HER. Figure 11b shows the Tafel plots of different modified electrodes; the Ni nanoparticle deposit from ethaline has the lowest Tafel slope of 130 mV dec⁻¹, while the Tafel slopes for Ni nanoparticle deposit from acetate and bare PGE are 147 and 327 mV dec⁻¹, respectively, suggesting that the fabricated nanoparticle Ni@PGE from ethaline has the highest catalytic activity and the fastest kinetics for HER compared to the other electrodes. The kinetics parameters were
calculated from the Tafel plots for both Ni deposits from the two different mediums towards HER. The most vital kinetic parameter which is the exchanging current density \( j_0 \) has been calculated and is found to be \( 8.3 \times 10^{-4} \) A cm\(^{-2} \) for the fabricated Ni nanoparticles from ethaline, \( 7.7 \times 10^{-4} \) A cm\(^{-2} \) for the fabricated Ni nanoparticles from acetate, and \( 3.3 \times 10^{-4} \) A cm\(^{-2} \) for the bare PGE. As shown from the previous results, the fabrication of Ni nanoparticles at PGE from ethaline has the highest \( j_0 \) and \( \alpha \) indicating its higher catalytic activity towards HER due to its high surface area according to its needle flower morphology which possesses more active sites and its smaller size.

Table 3 represents the comparison of overpotentials, Tafel slopes, and kinetics parameters between the different modified electrodes.

The ECSA is proportional to the capacitance double layer \( (C_{dl}) \) which is evaluated in the non-faradic region of HER or OER at different scan rates. CV measurements of the two different fabricated Ni nanoparticle electrodes from acetate and ethaline in the non-faradic region of HER were estimated in 1 M KOH at 298 K at different scan rates (20, 30, 50, 70, 90, and 100 mV s\(^{-1} \)) as has been seen in Fig. 12a and b. Figure 12c shows the linear relationship of the difference between charging and discharging current density which is chosen at the constant potential in the middle distance between the initial and final potential (−0.9 V vs. Ag/AgCl) against the different scan rates; half of the slope is the capacitance double layer \( (C_{dl}) \) [54] which is higher four times for the fabricated Ni nanostructure deposit from ethaline compared with the other fabricated Ni nanoparticle electrode from acetate, suggesting its higher catalytic activity towards HER. The comparison between kinetics parameters and Tafel slopes for different Ni-based catalysts and our present work is summarized in Table 4.

As has been shown in Table 4, the deposited Ni@PGE from ethaline has a small negative overpotential value towards HER compared with other bifunctional catalysts like CoNi-30 and NiCo\(_2\)S\(_4\) NW/NF arrays which proves the activity of the deposited Ni nanoparticles from DES and opens a new approach for improving a new bifunctional catalyst from DES towards HER. The overpotential value of the deposited Ni nanoparticles was compared with other researches that used the commercial Pt/C catalysts towards HER. It was found that Pt/C catalyst with high loading of 340 mg cm\(^{-2} \) possesses a lower overpotential value of 53 mV to achieve a current density of 10 mA cm\(^{-2} \), while the deposited Ni nanoparticles from ethaline with lower loading of 0.018 mg cm\(^{-2} \) with higher mass activity of 333.3 mA mg\(^{-1} \) than the Pt/C catalyst of 330 mA mg\(^{-1} \) possess a higher overpotential value of −154 mV to achieve a current density of 10 mA cm\(^{-2} \).

Table 5 contains the comparison between different commercial Pt/C catalyst loading and Ni nanoparticles from ethaline solvent in terms of overpotential values and Tafel slope for HER. Despite the higher overpotential value for Ni nanoflowers than Pt/C, Ni nanoparticle deposit from DES provides a remarkable enhancement in the electrocatalytic activity towards HER with low loading, while the Pt/C possesses a smaller overpotential value in the case of high loading of the catalyst.

Furthermore, the durability and stability of the fabricated Ni deposit from ethaline were studied in 1 M KOH after 1000 cycles and chronoamperometry for 4500 s.

### Table 4

| Catalysts                        | Medium   | \( \eta_{10} \) (mV) | Scan rate (mV s\(^{-1} \)) | Reference |
|----------------------------------|----------|-----------------------|-----------------------------|-----------|
| CoNi-30                          | 1 M KOH  | −210                  | 5                           | [55]      |
| NiCo\(_2\)S\(_4\) NW/NF arrays   | 1 M KOH  | −210                  | 10                          | [56]      |
| Porous Ni                        | 1 M KOH  | 114                   | 50                          | [57]      |
| Pt/Ni-SP                         | 1 M NaOH | 250                   | 50                          | [58]      |
| Ni@PGE nanoparticles from acetate| 1 M KOH  | −164                  | 50                          | This work |
| Ni@PGE nanoflower from ethaline  | 1 M KOH  | −154                  | 50                          | This work |

### Table 5

| Catalysts                        | Mass activity | Catalyst loading (mg cm\(^{-2} \)) | Overpotential \( (\eta) \) (mV) | Tafel slope (mV dec\(^{-1} \)) | Reference |
|----------------------------------|---------------|-------------------------------------|-------------------------------|-------------------------------|-----------|
| Pt/C                             | 330           | 340                                 | 53                            | -                             | [58]      |
| Pt/C/NF                          | -             | 18.6                                | −20                           | 30.6                          | [34]      |
| Pt/C                             | -             | -                                   | −30                           | 63                            | [55]      |
| Ni@PGE nanoflower from ethaline  | 333.3         | 0.018                               | −154                          | 130                           | This work |
Figure 13a shows good stability as the current is retained of 63% of its initial current. While the LSV for HER after 1 cycle and 1000 cycles has been studied to show its durability, as has been shown in Fig. 13b, its catalytic activity drops after 1000 cycles which means that the stability of nano-Ni deposit from ethaline for HER needs to be improved.

The electrocatalytic activity of fabricated Ni nanoparticles at PGE from acetate and ethaline for OER

Further investigations were estimated for both fabricated Ni electrocatalysts from acetate and ethaline for the oxygen evolution reaction (OER). Figure 14a represents LSV polarization curves in 1 M KOH at room temperature at a scan rate of 50 mV s\(^{-1}\) for OER at deposited Ni nanoparticles from acetate bath with pH 5.8 at a potential of −1.1 V and ethaline bath at a potential of −0.98 V and temperature 318 K; it shows that electrodeposited Ni nanoparticle electrocatalyst from ethaline has an overpotential of 350 mV to reach the current density of 10 mA cm\(^{-2}\), while the electrodeposited Ni nanoparticles from acetate and bare PGE have an overpotential of 400 mV and 550 mV to reach the current density of 10 mA cm\(^{-2}\). Remarkably, there is an oxidation peak which refers to the oxidation of Ni nanoparticles to Ni\(^{2+}\) due to the formation of nickel oxyhydroxide (NiOOH) in the alkaline medium which performed as active species to enhance the electrocatalytic activity for OER [34]. From these results, it is clear that the fabricated Ni nanoparticle electrocatalyst from ethaline has the lowest overpotential towards OER and hence the best catalytic activity. Figure 14b shows the Tafel plots of different modified electrodes for OER; the deposited Ni nanoparticles from ethaline own the lowest Tafel slope of 125 mV dec\(^{-1}\) while the Tafel slopes for deposited Ni nanoparticles from acetate and bare PGE are 128 and 167 mV dec\(^{-1}\), respectively, indicating that fabricated PGE with Ni nanoparticles from ethaline has more active sites and the fastest kinetics for OER compared with the other electrodes [55].

The kinetics parameters were calculated for each electrode for OER in Table 6 that shows the fabricated Ni nanoparticle electrode from ethaline has the highest \(j_0\) and \(\alpha\) value and the lowest overpotential means that it has the best kinetics for OER.

Figure 13a

Fig. 13a The chronoamperometry time–current curve for deposited Ni from ethaline at onset pot = 1.1 V vs Ag/AgCl (3 M KCl). b Polarization curves for HER in 1 M KOH after 1 cycle and 1000 cycles for deposited Ni from ethaline

Table 6 Values of overpotential, Tafel slopes, and kinetics parameters for different fabricated electrodes in 1 M KOH at room temperature at a scan rate of 50 mV s\(^{-1}\) in the case of OER

| Ni films           | \(\eta_{10}\) (mV) | Tafel slopes (mV dec\(^{-1}\)) | \(j_0\) (A.cm\(^{-2}\)) | \(\alpha\) |
|-------------------|------------------|-------------------------------|------------------------|-----------|
| Ni@PGE from acetate | 400              | 128                           | \(12.6 \times 10^{-2}\) | 0.230     |
| Ni@PGE from ethaline | 350              | 125                           | \(14.4 \times 10^{-2}\) | 0.236     |
| Bare PGE          | 550              | 167                           | \(2.33 \times 10^{-2}\) | 0.176     |
Figure 15a and b show the CV measurements of deposited Ni nanoparticles from acetate and ethaline, respectively, in 1 M KOH in the non-faradic region of OER at different scan rates to calculate the $C_{dl}$ for both catalysts. Figure 15c represents that fabricated Ni nanoparticles from ethaline own the highest $C_{dl}$ which equals to 18 mF cm$^{-2}$, while the fabricated Ni nanoparticles from acetate possess 14.8 mF cm$^{-2}$, suggesting that Ni nanoparticle deposit from ethaline has higher ECSA and catalytic activity compared with the fabricated Ni nanoparticle deposit from the acetate. The results of $j_0$ of the fabricated Ni from ethaline for HER and OER were compared and show that Ni nanoparticles from ethaline have higher kinetics for OER than for HER.

The overpotential value of the deposited Ni nanoparticles was compared with other researches that used the commercial IrO$_2$ and RuO$_2$ catalysts towards OER in Table 8. The deposited Ni nanoflowers from ethaline with very small loading present a smaller Tafel slope of 125 mV dec$^{-1}$ than the RuO$_2$/NF which exhibits 129.1 mV dec$^{-1}$ with higher loading, suggesting its promoting catalytic activity towards OER.

Figure 16a and b demonstrate the durability and stability of the deposited Ni nanoparticles from ethaline in 1 M KOH. It shows that the catalyst has excellent mechanical properties and stability towards OER as the current is retained at 86% of its initial current, unlike HER. The LSV after 1 cycle and 1000 cycles does not change and is almost the same which demonstrates that it has long-term durability compared with its stability and durability in the case of HER.
Conclusions

The electrodeposition process of Ni from DES is more effective than from the aqueous solvent and produces more fine Ni nanoparticles with a uniform needle flower structure with a small size of 20 nm which has more active sites for HER and OER. Furthermore, it has higher catalytic efficiency and kinetics for both HER and OER compared with the deposited Ni nanoparticles from the acetate bath. The fabricated Ni electrode from ethaline has a higher current density, less overpotential for both HER and OER of $-154$ mV and $350$ mV, respectively, and smaller Tafel slope for both HER and OER of $130$ mV$ \text{dec}^{-1}$ and $125$ mV$ \text{dec}^{-1}$, respectively, compared with the fabricated Ni electrode from acetate bath which has a high overpotential for both HER and OER of $-164$ mV and $400$ mV, respectively, and higher Tafel slope of $147$ mV$ \text{dec}^{-1}$ and $128$ mV$ \text{dec}^{-1}$ for both HER and OER, respectively. The results of $j_0$ for the deposited Ni nanoparticles from ethaline have higher kinetics and higher stability for OER than for HER.

Abbreviations

DESs: Deep eutectic solvents; ECSA: Electrochemical surface area; HER: Hydrogen evolution reaction; ChCl: Choline chloride; EG: Ethylene glycol; SEM: Scanning electron microscopy; XRD: X-ray diffraction; EDX: Energy-dispersive X-ray; PGE: Pencil graphite electrode; QRE: Quasi-reference electrode; CV: Cyclic voltammetry; CA: Chronoamperometry; TEM: Transmission electron microscope; PTFE: Polytetrafluoroethylene; NF: Nickel foam; CC: Carbon cloth

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