Fabrication of New Demulsifiers Employing the Waste Polyethylene Terephthalate and their Demulsification Efficiency for Heavy Crude Oil Emulsions

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Abstract: Two novel amphiphilic polyethylene amine terephthalate have been prepared via the glycolysis of polyethylene terephthalate (PET). The product, bis (2-hydroxyethyl terephthalate) (BHET), was converted to the corresponding dialkyl halide, bis(2-chloroethyl) terephthalate (BCET), using thionyl chloride (TC). This dialkyl compound was used for alkylation of dodecyl amine (DOA) and tetraethylenepentamine (TEPA) or pentaethylenehexamine (PEHA) to form the corresponding polyethylene amine terephthalate, i.e., DOAT and DOAP, respectively. Their chemical structure, surface tension, interfacial tension (IFT), and dynamic light scattering (DLS) were determined using different techniques. The efficiency of the prepared polyethylene amine terephthalate to demulsify water in heavy crude (W/O) emulsions was also determined and found to increase as their concentrations increased. Moreover, DOAT showed faster and higher efficiency, and cleaner separation than DOAP.

Keywords: polyethylene amine terephthalates; polyester waste; demulsification process; heavy crude oil emulsions

1. Introduction

In the last few decades, there is a dynamic escalation of both the production and consumption of polymers. The amount of manufactured polymers has increased globally from 1.3 tons in 1950 to 335 tons in 2017 [1]. This was ascribed to an upsurge of their applications in different fields such as packing, household appliances, construction, electronics, and medicines. However, the increasing of polymer wastes generated from their daily use and their resistance to degradation may lead to the accumulation of solid waste in the environment with a consequent increase of related pollution [2–4]. Polyethylene terephthalate (PET) is one of the most widely manufactured and consumed polymers. Its unique properties such as high mechanical strength as well as excellent moisture and water barrier characteristics make it suitable for different purposes such as beverage bottles, electrical insulation polymers, household materials, and textile manufacturing [5,6]. The huge amounts of waste derived from PET motivate researchers to search for effective methods for its disposal. Several studies were described either the recycling or reuse of PET for producing new applied materials. The resulting materials have been shown promising results as oil spill remediation [7–9], demulsifiers [10,11], corrosion inhibitors [12,13], azo dyestuff [14], textile auxiliaries [15], electrochemical sensors [16], as well as engineering applications [17–20].

The formation of crude oil emulsions is one of the major obstacles faced by the transportation and refining of recovered crude oil [21]. The surfactants added during enhanced oil recovery along with the presence of natural emulsifiers in the crude oil, such as asphaltenates, resins, and solid particles, can promote the formation of very stable emulsions [21–29]. Several techniques have been employed for the demulsification of crude oil emulsions,
including chemical, biological, and physical methods. The demulsification of crude oil emulsions using chemicals is the most applied approach owing to its fast separation and low cost as compared to other techniques [23]. Surfactants are common chemicals used as demulsifiers owing to their efficiency to reduce the interfacial tension (IFT) between the crude oil and water. Several nonionic surfactants are commonly used as demulsifiers including alkyl phenol formaldehyde, ethoxylated polymers, di-epoxides, and ethylene oxide-co-propylene oxide copolymers, alkyl phenols, and polyesters [30]. Usually, commercial demulsifiers contain two or more surfactants based on the composition and type of the petroleum crude oil [31]. In recent years, different natural compounds and waste materials were modified and applied in the petroleum industries [10,11,21,32–38]. Reusing of these materials promotes the principles of green chemistry in the protection of environment. In our previous works, different natural compounds and material wastes were used for synthesizing demulsifiers [10,11,21,32], and oil spill collectors [36–38]. In this work, two new amphiphilic polyethylene amine terephthalate were synthesized based on the conversion of the PET glycolysis product, bis(2-hydroxyethyl) terephthalate (BHET), to the corresponding dialkyl halide, bis(2-chloroethyl) terephthalate (BCET), followed by the alkylation of dodecyl amine and tetraethylenepentamine (TEPA) or pentaethylenehexamine (PEHA) using BCET. The chemical structure, surface activity, and dynamic light scattering of these polyethylene amine terephthalate were investigated, along with their efficiency to demulsify heavy crude oil emulsions.

2. Experimental

2.1. Materials

Tetraethylenepentamine (TEPA), pentaethylenehexamine (PEHA), dodecylamine (DOA), thionyl chloride (TC), zinc acetate anhydrous, ethylene glycol (EG) and, potassium carbonate anhydrous were purchased from Aldrich Co. (St. Louis, MO, USA). All solvents used for the characterization, synthesis, and evaluation of the efficiency of the polyethylene amine terephthalate as demulsifiers, including ethanol, dimethylformamide (DMF), isopropanol absolute, dioxane, and xylene, were purchased from Sigma-Aldrich Co. (St. Louis, MO, USA). Heavy crude oil was supplied by Aramco (Dammam, Saudi Arabia), with API gravity 20.8°, and contents of asphaltenes and water 8.3%, and 0.145% of weight, respectively. Brine (35 g/L) was prepared in our lab using sodium chloride and distilled water. Asphaltenes were precipitated according to ASTM D-2007 using n-heptane as precipitant.

Polyethylene terephthalate (PET) was collected from utilized drinking bottles, converted into small pieces, cleaned with distilled water followed by acetone, and finally kept in an oven at 75 °C for drying till it attained a constant weight. BHET was produced from the glycolysis of PET collected from consumed drinking bottles and converted to BCET, as reported in earlier work [10].

2.2. Preparation of Polyethylene Amine Terephthalate

Solution of BCET (5 g, in 20 mL DMF) was mixed with solution of DOA (3.18 g), and K₂CO₃ (2.37 g), in 15 mL of DMF and stirred for 5 h at room temperature. Next, the product was added to a mixture of TEPA (3.25 g) and K₂CO₃ (2.37 g) or PEHA (3.99 g) and K₂CO₃ (2.37 g). The new mixture was further stirred for 5 h under the same conditions [39]. DMF was evaporated under reduced pressure, and the produced compounds were dissolved in isopropanol absolute and filtered. Solvent was evaporated under reduced pressure and the produced compounds were dried in an oven at 70 °C. The produced polyethylene amine terephthalate originated from either TEPA or PEHA were named as DOAT and DOAP, respectively.

2.3. Characterization

The chemical structures of the newly produced polyethylene amine terephthalate were conducted by Fourier-transform infrared spectroscopy (FT-IR, Nicolet 6700 spectrometer, Waltham, MA, USA) and proton nuclear magnetic resonance spectroscopy (¹H-NMR,
Avance DRX-400 spectrometer, Billerica, MA, United States) using deuterated dimethyl sulfoxide as a solvent. The ability of the polyethylene amine terephthalate to reduce the IFT and surface tension was evaluated by a pendant drop technique using a tensiometer (DSA-100, KRUS, Hamburg, Germany). The relative solubility number (RSN) was measured via the titration of their solutions (1 g of compound in 30 mL of dioxane: toluene 96:4%) using deionized water. The volume of the consumed water (in mL) was considered as the RSN. Different ratios of water in heavy crude oil (W/O) emulsions (50:50%, 60:40%, 70:30%, and 90:10%) were prepared using a mechanical homogenizer at 6000 rpm for 30 min. The demulsification efficiency of the prepared polyethylene amine terephthalates was determined using the bottle test method. The prepared emulsions were transferred to quick-fit measuring cylinders, several concentrations of polyethylene amine terephthalate (in xylene: ethanol 75:25 v/v) were injected. The measuring cylinder was tightly closed, vigorously shaken for 100 times to ensure the dispersion of polyethylene amine terephthalate in the prepared W/O emulsion, and placed in a hot water bath at 60 °C. The injection end point of the polyethylene amine terephthalate doses to emulsion was recorded as zero time for the evaluation of the demulsification time. The demulsification efficiency of the polyethylene amine terephthalate was calculated based on the ratio between separated and emulsified water according to Equation (1) [40].

\[
DE\% = \frac{(Separated\ water)}{(Emulsified\ water)} \times 100
\]  

The size of the formed micelles, zeta potential (ZP) of polyethylene amine terephthalate and their interactions with asphaltenes was determined by dynamic light scattering (DLS, Zetasizer Nano ZS, Malvern, Worcestershire, United Kingdom). The ZP of DOAT and DOAP different concentrations were measured utilizing 0.001 M KCl solution. For measuring ZP of asphaltenes, 3 mL of asphaltenes solution (50 mg of asphaltenes in 15 mL of ethanol absolute) was dispersed in 200 mL of 0.001 M sodium nitrate solution [23]. The optical microscopic images of the prepared emulsions were captured using a polarized-light microscope (Olympus BX51, Shinjuku, Tokyo, Japan).

3. Results and Discussion

3.1. Chemical Structure of the Synthesized Polyethylene Amine Terephthalate

The BHET produced from the glycolysis of PET was converted to BCET and successfully used for the production of novel polyethylene amine terephthalate through alkylation of DOA and TEPA or PEHA using BCET terminal alkyl halide groups, as presented in Scheme 1. The chemical structures of DOAT, and DOAP were confirmed using FT-IR and \(^1\)H-NMR, as represented in (Figure 1a,b) and (Figure 2a,b), respectively. The FT-IR spectrum of DOAT showed the disappearance of the broad bands of the BHET hydroxyl groups at around 3550–3200 cm\(^{-1}\), thus confirming its conversion to BCET. In Figure 1a, the absorption bands of the alkyl chain and methylene groups of TEPA appeared at 2955 cm\(^{-1}\), 2922 cm\(^{-1}\) and 2852 cm\(^{-1}\). Moreover, the terminal NH\(_2\) of TEPA appeared at 3300 cm\(^{-1}\) as two unequal narrow bands. The stretching of the absorption bands of the terephthalate carbonyl groups appeared at 1721 cm\(^{-1}\). Similarly, the stretching bands of alkyl chain and methylene groups in DOAP spectrum (Figure 1b) appeared at 2953 cm\(^{-1}\), 2922 cm\(^{-1}\), and 2851 cm\(^{-1}\). In addition, the terminal NH\(_2\) of PEHA, and carbonyl groups appeared at 1720 cm\(^{-1}\) and 3300 cm\(^{-1}\).
Scheme 1. Preparation route of DOAT and DOAP.

Figure 1. FT-IR spectrum of (a) DOAT, and (b) DOAP.
In the $^1$H-NMR spectrum of DOAT (Figure 2a) the alkyl chain resonated at 0.8, 1, 1.2, and 1.28 ppm. The methylene protons of PEHA appeared between 2.45 and 2.65 ppm. The protons of the aromatic ring appeared at 7.9 ppm. The $^1$H-NMR spectrum of DOAP (Figure 2b) showed the same peaks due to the similarity in their chemical structures. Figure 2b also showed higher intensity for peak of ethylene repeating units attached to amine compared with DOAT due to increase their numbers of protons. The solubility of the prepared polyethylene amine terephthalate in water was determined using the RSN. The RSN values were 13.7 and 14.5 mL for DOAT and DOAP, respectively. These results reflected the increased solubility of DOAP due to its longer hydrophilic moiety compared to DOAT. Moreover, the moderate RSN values for both polyethylene amine terephthalate revealed their ability to dissolve in organic solvents and water to some extent [23].

### 3.2. Surface activity of the Synthesized Polyethylene Amine Terephthalate

The surface tension and IFT of the synthesized polyethylene amine terephthalate were measured to evaluate their surface activity at an air/ water, and crude oil/ water interfaces. The efficiency of the polyethylene amine terephthalate in reducing the surface tension was measured in distilled water, as shown in Figure 3.
Figure 3. Surface tension versus natural logarithm of different DOAT and DOAP concentrations.

The surface tension decreased as the polyethylene amine terephthalate concentrations increased until their critical micelle concentration (CMC). The surface tension parameters were evaluated and are presented in Table 1. The higher CMC value observed for DOAP compared to DOAT reflected its greater solubility in water due to presence of longer hydrophilic chain of ethylamine repeating units, which confirmed the RSN results.

Table 1. Surface Activity Parameters of DOAT and DOAP in Distilled Water at Room Temperature.

| Oligo-Amine | cmc (mM) | γcmc | (∂γ/∂lnc) | Γmax × 10^{10} (mol/cm²) | A_{min} (Å²) | ΔG_{mic} (kJ/mol) | ΔG_{ads} (kJ/mol) | RSN (mL) |
|-------------|---------|------|-----------|-----------------------|------------|-------------------|-------------------|---------|
| DOAT        | 0.026   | 27.6 | 11.0      | 4.4                   | 38         | −36.1             | −46.3             | 13.7    |
| DOAP        | 0.049   | 29.4 | 10.3      | 4.2                   | 40         | −34.6             | −44.9             | 14.5    |

The surface excess concentration (Γ_{max}) and minimum surface area occupied per molecule (A_{min}) determined using the Gibbs adsorption Equations (2) and (3), respectively [21].

\[
Γ_{max} = \frac{1}{RT} (−\partial γ / ∂lnc)T
\]

\[
A_{min} = \frac{10^{16}}{NAΓ_{max}}
\]

where R, T, (−∂γ/∂lnc)_T, and N_A are the gas general constant, measuring temperature, slope of the straight lines in Figure 3, and Avogadro’s number, respectively. The standard free energies of micellization (ΔG_{mic}), and adsorption (ΔG_{ads}) were evaluated using Equations (4) and (5), respectively.

\[
ΔG_{mic} = RT \ln \left( \frac{CMC}{55.5} \right)
\]

\[
ΔG_{ads} = ΔG_{mic} − 6.022(γ_0 − γ_{CMC})A_{min}
\]

where γ_0 and γ_{CMC} are the surface tension of distilled water and polyethylene amine terephthalate solutions at CMC. An increase of Γ_{max} and decrease of A_{min} for DOAT revealed a tighter packing of its molecules on the surface than DOAP. The behavior of polyethylene amine terephthalate at an air/water interface and in bulk solution is represented in Scheme 2. Before CMC (Scheme 2a), the DOAT molecules migrate an aqueous solution to the air/water interface, and easily get adsorbed at there. The dodecyl hydrophobic chains are oriented themselves toward air, whereas the hydrophilic chains (repeating units of ethylamine) are toward water. The adsorption of DOAT molecules at this interface increases as its concentration increases leading to replace water molecules with DOAT molecules.
and hence reducing surface tension up to CMC [41]. An increase the concentration after CMC (Scheme 2b) leads to form micelles. The alkyl hydrophobic chains close together forming micelle cores, whereas the hydrophilic chains interact with water molecules. The $\Delta G_{\text{mic}}$ and $\Delta G_{\text{abs}}$ negative values of polyethylene amine terephthalate (Table 1) indicate their ability to spontaneously form micelles and their adsorption at the water/air interface. The higher negative values of $\Delta G_{\text{abs}}$ than $\Delta G_{\text{mic}}$ suggest the adsorption of polyethylene amine terephthalate molecules at the water/air interface, followed by micelles formation after saturation of adsorption [1]. The surface charges (ZP) of the formed micelles were measured and represented in Figure 4. The surface charge values of DOAT and DOAP were 18.36 mV and 16.01 mV, respectively. The positive values reflect their ability to form positive micelles in a neutral medium.

![Scheme 2](image)

Scheme 2. Behavior of DOAT at (a) before CMC and (b) after CMC.

![Figure 4](image)

Figure 4. Zeta potential of (a) DOAT and (b) DOAP at room temperature.

The IFT of the synthesized amphiphilic polyethylene amine terephthalate was measured between the heavy crude oil and water as shown in Figure 5. The IFT decreased as the polyethylene amine terephthalate concentrations increased. DOAT showed a higher
efficiency than DOAP which may be referred to increase its hydrophobicity due to presence of shorter hydrophilic chain of ethylamine repeating units.

Dynamic light scattering (DLS) measurements were also used to determine the micelle size (MS) and polydispersity index (PDI) of the synthesized polyethylene amine terephthalate (Figure 6a,b). The MS and PDI were found to be 343.2 nm and 0.287 for DOAT, while being 495.3 nm and 0.311 for DOAP. The small size of DOAT micelles reflected its tighter packing compared to DOAP, which was confirmed by surface tension measurements. The low values of PDI for both polyethylene amine terephthalate indicated the formation of uniform micelles. The HLB values of the synthesized amphiphilic polyethylene amine terephthalate were calculated using Griffin equation (Equation (6)) for nonionic surfactants:

\[
HLB = \frac{M_{\text{wt of hydrophilic moieties}}}{M_{\text{wt of molecules}}} \times 20
\]

The calculated HLB values DOAT and DOAP were 11.25, and 11.84, respectively. HLB values seem to be similar for both compounds. The more relative value of DOAP HLB was ascribed to an increase the number of ethylamine units. In addition, the HLB values for both compounds elucidated that the synthesized compounds can be solubilized in both polar and nonpolar solvent.

3.3. Demulsification Performance of the Synthesized Polyethylene Amine Terephthalate

The chemical demulsifiers efficiency depends on the interfacial competition or strong interactions between them and asphaltenes as stabilizing agent. Moreover, the chemical demulsifiers efficiency is also affected by different parameters such as the type and composition of the crude oil, ratio and salinity of water, amphiphilicity of demulsifiers as well as their ability to reduce the surface tension and IFT, and separate clean demulsified water [10]. Usually, commercial demulsifiers contain two or more surfactants having different hydrophilic-lipophilic balance (HLB). In this work, several ratios of heavy crude oil: water (ranging from 50:50% to 90:10%) were utilized to evaluate the demulsification efficiency of the prepared polyethylene amine terephthalate by using the bottle test, as detailed in the experimental section. The type of formed emulsions was determined by conventional drop tests; all prepared emulsions were dispersed in toluene, confirming the formation of W/O emulsions at all ratios. The stability of the prepared emulsions was tested by injecting them
with the same dose of xylene/ethanol and placing them in a hot water bath (at 60 °C) for two weeks. The blank samples did not show any separation. There are different analytical and spectroscopic tools were used to investigate the application of amphiphilic polymeric solutions in the petroleum industry such as scanning electron microscope (SEM) that used to confirm the formation of thin films to protect the steel surfaces from corrosion. The application of amphiphilic polymers as demulsifier for petroleum crude oil emulsion can be investigated by using optical microscope to confirm their adsorption at water/oil interface. An optical microscopy technique was used to confirm the stability of the prepared emulsions. Figure 7a shows a blank sample of a (60/40 vol. %) W/O emulsion after two weeks. The small size of the emulsion droplets with an average diameter of 1.5 µm indicated the formation of a stable emulsion.

Figure 6. Micelle size of (a) DOAT and (b) DOAP at room temperature.
The prepared polyethylene amine terephthalate succeeded to 100% demulsification in the different cases presented in Table 2, depending on the ratio of brine in the synthetic W/O emulsions and polyethylene amine terephthalate concentrations. Figure 8a–d show the demulsification efficiency of DOAT at different concentrations. The demulsification efficiency increased as the DOAT concentration increased. Moreover, the demulsification time decreased with increasing ratios of brine in the synthetic emulsions due to increase the droplet collisions (collision frequency), and thus droplet coalescence rate increase [42].

The prepared W/O emulsions form stable emulsion due to the presence of asphaltenes that act as natural surfactant to form thin rigid film at interfaces. The DAOT and DOAP destabilize the prepared emulsions throughout competitive adsorption with asphaltenes at W/O interfaces. The DAOT reduces both surface tension and interfacial tension more than DOAP as represented in Figures 3 and 5. These data elucidate also that the DAOT was adsorbed either at air/water or water/oil interfaces more than DAOP. It is expected that the presence of heteroatoms (including oxygen, and nitrogen), phenyl ring, and alkyl chain of asphaltenes will enhance their interactions with DOAT or DOAP throughout hydrogen bonding, π-π stacking, and van der Waals forces changing the behavior of interfacial film at crude oil/water interface. Moreover, it is also expected that the great ability of demulsifier to compete with asphaltenes to adsorb more at interfaces. The change in the behavior of this film facilitates the flocculation and coalescence of water droplets. In addition, the electrostatic interactions between positive surface charge of DOAT and DOAP (Table 3) with a negative surface charge of asphaltenes (−43.35 mV) [23] enhanced the replacement of asphaltenes rigid film with a soft film around the water droplets, which facilitated the coalescence of water droplets to from bigger droplets that could be settled at the bottom of the cylinder by gravity (Figure 7b,c) [43]. Furthermore, DOAT showed a higher
efficiency than DOAP, which may be ascribed to its increased hydrophobicity, consequently enhancing its diffusion through heavy crude oil as a continuous phase.

Table 2. Demulsification Efficiency of DOAT and DOAP for Different Compositions of W/O Emulsions at 60 °C.

| Oligo-Amine | Dosage (ppm) | 90/10 Crude Oil/Brine Composition | 70/30 Crude Oil/Brine Composition | 60/40 Crude Oil/Brine Composition | 50/50 Crude Oil/Brine Composition |
|-------------|--------------|----------------------------------|----------------------------------|----------------------------------|----------------------------------|
|             |              | DE (%)  | Time (h) | DE (%)  | Time (h) | DE (%)  | Time (h) | DE (%)  | Time (h) | DE (%)  | Time (h) |
| DOAT        | 250          | 92      | 9        | 83      | 8        | 75      | 7        | 80      | 6        |          |          |
|             | 500          | 95      | 9        | 78      | 9        | 85      | 6        | 100     | 4        |          |          |
|             | 1000         | 100     | 8        | 95      | 7        | 95      | 6        | 100     | 4        |          |          |
|             | 250          | 85      | 11       | 70      | 11       | 77.5    | 10       | 55      | 8        |          |          |
|             | 500          | 85      | 10       | 85      | 10       | 65      | 8        | 85      | 7        |          |          |
|             | 1000         | 100     | 10       | 100     | 8        | 52.5    | 8        | 100     | 7        |          |          |
| DOAP        | 250          | 85      | 11       | 70      | 11       | 77.5    | 10       | 55      | 8        |          |          |
|             | 500          | 85      | 10       | 85      | 10       | 65      | 8        | 85      | 7        |          |          |
|             | 1000         | 100     | 10       | 100     | 8        | 52.5    | 8        | 100     | 7        |          |          |

Figure 8. Demulsification efficiency of DOAT at different concentrations using (a) 50/50 vol%, (b) 60/40 vol%, (c) 70/30 vol%, and (d) 90/10 vol% W/O emulsions.

Table 3. Zeta Potential of DOAT and DOAP for Different concentration.

| Oligo-Amine | Conc. (ppm) | Zeta Potential (mV) |
|-------------|-------------|---------------------|
|             |             | Oligo-Amine | Asphaltenes/Oligo-Amine |
| DOAT        | 250         | 18.36         | 7.4                  |
|             | 500         | 12.8          |                      |
|             | 1000        | 16.2          |                      |
|             | 250         | 5.9           |                      |
| DOAP        | 500         | 16.01         | 13.4                 |
|             | 1000        | 18.1          |                      |

The cleanness of demulsified water is one of the most significant variables for selecting a suitable demulsifier. A suitable demulsifier can separate clean water with very low or
no heavy crude oil residuals. The clarity of demulsified water from W/O emulsions (60/40 vol%) using different concentrations of DOAT and DOAP is shown in Figure 9. A higher clarity of demulsified water was produced by DOAT (Figure 9a), thus confirming its greater efficiency for separating cleaner water than DOAP (Figure 9b).

![Figure 9. Demulsification images of 60/40 vol. % W/O emulsions using different concentration of (a) DOAT and (b) DOAP at 60 °C.](image)

From the previous data, it can propose that the increasing of polyethylene amine chain length in case of DOAP more than DOAT leads to its coiling at interfaces and responsible to increase its minimum surface area occupied per molecule \(A_{\text{min}}\) of DOAP more than DOAT at interface (Table 1). The coiling polyethylene amine of DOAP at interfaces is responsible on its lower interaction with asphaltenes to destabilize the prepared W/O emulsions. This speculation was also proved from lowering of zeta potential of asphaltenes/DOAP than asphaltenes/DOAT at 250 ppm (Table 3). The lowering of zeta potential of asphaltenes/DOAP (5.9 mV) than asphaltenes/DOAT (7.4) at 250 ppm elucidates the lower adsorption of DOAP on asphaltenes at lower concentration and indicates also its lower ability to replace asphaltenes layer and demulsify the emulsions (Table 2 and Figure 8).

4. Conclusions
Two unprecedented polyethylene amine terephthalate were synthesized via on the conversion of the PET glycolysis product BHET to the corresponding dialkyl halide BCET in the presence of TC, followed by the alkylation of DOA and TEPA or PEHA using BCET to form DOAT and DOAP, respectively. The synthesized polyethylene amine terephthalate showed a good ability to reduce the surface tension and IFT. Their surface activities increased as their concentration increased. Moreover, DOAT revealed a higher efficiency than DOAP, which could be attributed to its greater hydrophobicity. An increase of \(\Gamma_{\text{max}}\) and decrease of \(A_{\text{min}}\) for DOAT revealed a good packing of its molecules at the air/water interface. The polyethylene amine terephthalate showed a good demulsification efficiency, which increased as their concentrations increased. The demulsification time decreased with increasing ratios of brine and polyethylene amine terephthalate concentrations, which might be referred to increase the droplet collisions. Moreover, DOAT led to a higher, cleaner, and faster demulsification than DOAT due to its increased hydrophobicity, and hence greater ability to diffuse in heavy crude oil as a continuous phase.

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