3-D Wire Cloth Electrode for Higher Throughput Dielectrophoretic Separation of Bacterial Cell

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Abstract—Dielectrophoresis (DEP) is one of an alternative way for cell separation. It has mainly been limited to processing small volumes due to constraint in fabrication of microelectrode over large surface areas. This work incorporated the wire cloth electrode fabricated using textile technology into a high throughput chamber experiment. The plain-weave wire cloth consists of 71 µm stainless steel wires as the microelectrode arrays hold together by polyester yarn warp. This work determines the cell separation yield with parameters on applied voltage, flow rate and cell concentration as well as its optimized variables on the chamber width of 1.2 cm and 2.5 cm. The optimum voltage achieved was 30 Vpk-pk, with flow rate of 3.5 ml/min and maximum cell concentration of 2.08 x 10^7 cells/ml. In chamber width comparison, 1.2 cm width chamber gives better total percentage yield of 96% than the 2.5 cm width chamber of 85% total percentage yield.

Keywords:—Dielectrophoresis, Large Scale, wire cloth

1. INTRODUCTION

Biochemical and bioprocessing has gained an overwhelming recognition due to constant need for rapid and robust technologies. More and more industries nowadays were moving towards developing process based on biochemical and biotechnology because of their inherent advantages[1]. However, when dealing with bioprocessing, the usual constraint is the downstream processing mainly bioseparation involving the recovery and purification of the desired product from the upstream process whereby the percentage of recovery is low. These kinds of trends and challenges in modern bioseparation have led to various discoveries and novel approaches in the techniques used.

Dielectrophoresis (DEP) is one of an alternative way for cell separation that involved the motion of particles caused by the interaction of cell induced dipole in non-uniform AC electric fields[2]. It has certain advantages over other methods mostly because of its high resolution or selectivity. Additionally, by DEP, cell viability can be maintained and the process can be conducted under sterile condition. Previous works regarding DEP involved separating live and dead cells or monocytes[3,4], manipulating cells using travelling electric fields[5,6], and application in the water[7] and wastewater treatment[8]. In nanotechnology, numerous works have been done regarding viruses[9,10]. Alternatively, research on the use of higher throughput have increased with 3-dimensional insulator[7] or electrode separator[3,11,12], wire cloth electrode separator [13], filter chip separator[14] and integrated microfluidic chip [15]. The process has always been limited to small throughput due to restriction in fabrication of microelectrode for large surface areas which mostly applied the lab-on-a-chip device and printed circuit board. Hence, the fabrication of 3-D microelectrode using textile technology is implemented to address the surface area issue. While previous study[13] proved to be effective for fungi species such as yeast (Saccharomyces cerevisiae), this study targeted smaller microorganism using bacteria Escherichia coli with smaller electrode diameter.

2. MATERIALS AND METHODS

The methodology involves the construction of the chamber, the cell preparation, the DEP experiment and the analytical methods involved.

2.1 Wire Cloth Fabrication and Electric Field Simulation

71 µm stainless steel wire were weaved into plain waeve pattern using textile machine with weft setting of 93 part per inch (PPI) and 16 µm polyester yarn size (83 decitex) to produce 204 µm gap. A study of the electric field strength and pattern generated by electrodes of the wire cloth was performed using FEMLAB 3.0 (COMSOL™) using the Electromagnetic module [13,16]. The drawn system mimicked the actual wire cloth electrode and electric field was simulated.
2.2. Cell preparation.

Escherichia coli (Biotechnology Lab, UPM) was cultured overnight in nutrient broth (Oxoid, UK) at 37°C in a 150 rpm incubator shaker (Stuart, Fisher Scientific, UK). The cell was then harvested, centrifuged at 5000 rpm (Heraeus, Thermo Scientific, USA) and washed four times with distilled water. Early concentration of cells (optical density, OD) suspended in distilled water was measured through 600nm wavelength of a UV spectrophotometer (Thermo Electron Corporation, UK).

2.3 Construction of chamber.

The DEP chamber for higher throughput (Figure 1) consisted of 7 layers of 1.5mm-thick Perspex frames, sandwiched with 6 sheets of wire cloth alternately. 2 solid sheets of the same Perspex used as the top and bottom cover of the chamber. 2 holes were drilled at both the width side as the inlet and outlet point while 2 small holes were bored at the top of the chamber for bubbles control. Flowable silicone glue was applied to the entire outer surface as finishing. 2 chambers with internal width size of 1.2 cm and 2.5 cm is constructed.

2.4 DEP separation experiment.

The chamber as in Figure 2 experimental setup was firstly filled up with distilled water. A frequency generator (model TG120, ThurlbyThandar Instrument, UK) and a self-built amplifier (Basecore (M) SdnBhd, Malaysia) were used to supply voltages of up to 60 Vpk-pk. By using a syringe, 1ml of cell suspension was immediately introduced after the electric field was applied to the system. Then, distilled water was continuously fed through the chamber inlet using a peristaltic pump (Watson-Marlow, UK) to wash out the cells that did not attract to the wire cloth. Few minutes later, the flow was stopped, the applied voltage was taken off, and the chamber was back flushed to collect the suspension for analysis. Experiments were conducted to observe the effects of applied voltage, flow rate and cell concentration towards the DEP separation process.

Variation of flow rate

Flow rates varies from 1 ml min⁻¹ to 5 ml min⁻¹ was used with frequency fixed at 1 MHz while the applied voltage value used was 30 Vpk-pk.

Variation of cell concentration

Cells suspensions with initial optical density absorbance (A) of 0.2, 0.4, 0.8, 0.9, 1.5, 2.0 were prepared. The frequency, applied voltage and flow rate used were 1 MHz, 30Vpk-pk and 3.5ml min⁻¹ respectively.

2.5 Analytical Methods

The experimental data were analysed and expressed in terms of percentage % mechanical yield, percentage % sedimentation loss, percentage % total yield or percentage % electrical yield. The percentage % of mechanical yield and sedimentation loss are essentially the same which denotes the percentage of cells trapped inside the system at 0 V. The percentage % total yield is the total percentage of cells trapped inside the chamber after the application of the electric field. Finally, the percentage % electric yield is the percentage cells collected due only to the application of the electric field. As an approximation, it was assumed that the total yield minus the mechanical loss gave the electrical yield. The basic formulas are summarized as follows:

At 0 V,

\[
\text{percentage % mechanical yield or sedimentation loss} = \left(\frac{\text{no of cell in} - \text{no of cells out}}{\text{no of cells in}}\right) \times 100
\]

After the application of electric field,

\[
\text{percentage % electrical yield} = \left(\frac{\text{no of cell in} - \text{no of cells out} - \text{no of cells trapped by mechanical}}{\text{no of cells in}}\right) \times 100
\]

3. RESULTS AND DISCUSSIONS

3.1 Electric Field Simulation of Wire Cloth Electrode

In the first part of the work, electric field pattern and strength was simulated first to calculate the dielectrophoretic force and also its non-uniformity behaviour. Through simulation by COMSOL, a maximum value of electric field obtained was 1.340x10⁵ Vm⁻¹ as can be seen in Figure 3 and Figure 4. The electric field strength is recorded to be the highest at the edge of electrode. As one move away from the edges, the electric field strength decreases non-linearly. This result is supported by previous works done by other researchers [13]. Electric Field pattern shown in Figure 3 and 4 clearly indicate non-uniformities which is an important essential features for a successful DEP separation system. The maximum electric field strength and DEP force obtained here yield approximately 3.1 x10⁻¹⁵ V² m⁻³ and 3.7 x10⁻¹⁰ N which conformed to previous investigation [16, 17]. This value is sufficient to produce a significant attractive force for DEP separation to occur. By Navier Stokes equation, the drag force was calculated approximately 2.6 x10⁻¹⁰ N when doing a force balance on a single particle, gave a particle velocity of 4x10⁻⁵ m/s moving forwards towards the end of the separation chamber.
3.2. Optimization of Microorganism Separation

This part discussed on the effect of the parameters studied which were the applied voltage, flow rate, cell concentration and the chamber width.

3.2.1 Variation of applied voltage

As depicted in Figure 5, the optimum voltage of 30Vpk-pk was obtained with cell collection yield of 96.13%. and the increment of the applied voltage only resulted to the decrease on the yield due to the interference by DC currents produced by the amplifier when high voltage and currents are used. Factors of electrode overheating also contribute to cell being non-viable towards the dielectrophoretic force available. The results found in this work is slightly higher and comparable to previous work [13,15, 16].

3.2.2. Variation of flow rates

Flow rate is the parameter that influence the drag force needed for the dielectrophoretic separation system. The flow rates were varied from 1 to 5 ml/min with fixed parameters of 1MHz of frequency, 30Vpk-pk of applied voltage and cell concentration of 0.92A. The optimum flow rate was obtained at 3.5ml/min (Figure 6). Higher flow rates distract the cells from the DEP force while lower flow rate caused Brownian motion between the bacteria cells to disturb the formation of the pearl chain [4].

Sedimentation tends to happen in large scale flow system because of gravity inside the chamber in regards to the mass of the particular microorganism [13]. However, the sedimentation percentage obtained was small compared to the total yield, hence the total yield in the end equals to the electrical yield. The usage of E. coli bacteria that is much smaller than yeast defies gravitational force issue entailed during the use of yeast. Yet some loss of cells was recorded at the final analysis during the reducing of the final sample by centrifuging. The results in this work is similar as in previous reported literature [13, 17].

3.2.3. Variation of cell concentration

Figure 7 shows a nearly-zero sedimentation rate and the gradual increase of electrical percentage collection with cell concentration until it reach plateau and no longer change or saturate which is similar to previous findings [13]. The maximum % yield achieved was 89% at 2.08x10^7 cell/ml. Asa can be seen, the cell number increased but not the sedimentation rate confirmed the influence of gravitational force on E.coli was insignificant.

Figure 3: The simulation of 71µm wire cloth system with gap of 204µm and yarn 16µm. Maximum value of electric field obtained was 1.340x10^6 V^2 m^-3.

Figure 4: The electric field plot across the red line as in Figure 3. This plot shows the variation of the electric field along the x-axis for the wire cloth system. It was recorded that the average electric field was 9x10^5 V^2 m^-3.

Figure 6 The effect of flow rate to the percentage yield of cell collected at 30Vpk-pk, 1MHz and 0.92A. The sedimentation yield is very low (<0.01 %) and the highest yield observed was 97.6% at 3.5 ml/min.

Figure 7 The percentage of cells collection by wire cloth in the DEP chamber as a function of voltage. Fixed parameters of 1 MHz frequency with flow of 1ml/min and cell concentration at OD of 0.92A was used.
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4. CONCLUSIONS

The DEP separation of bacteria cell was made possible in higher throughput with the use of wire cloth electrode system. There are much more factors surrounding the principles of DEP but particularly for this study, the optimum variables of 30Vpk-pk, flow rate of 3.5ml/min and cell concentration of 2.08x10^7 cells/ml was recorded with the better performance on the less wide chamber.

5. ACKNOWLEDGEMENTS

The project and student has been funded by MOSTI through EScience Fund (01-03-04-SF0841).

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Figure 7 The variation of cell concentration observed at value as low as 2.89x10^7 cells/ml (OD = 0.2A) until 3.33x10^7 cells/ml (OD = 2.0A). The voltage used was 30Vpk-pk at 1MHz frequency and flow rate of 3.5ml/min.

3.2.4. Width chamber comparison

The width of the chamber and its effect on the % yield was investigated with chamber A (width 1.2 cm x 1.7 cm) and chamber B (width 2.5cm x 1.7 cm). The 2 chambers were built with different cross sectional area and length to travel.

Chamber A which have smaller width but longer in length in turn have a slightly higher percentage of yield instead of chamber B (Figure 8) which was built with larger width but shorter in length. This is due to longer distance travelled by the cells that helps the DEP separation of cells due to longer retention time compared to wide but shorter distance at chamber B. This concept is similar to chromatography principles. Longer length facilitates better separation of different types of microorganisms or analytes and hence results in a greater resolution of the different samples obtain. Furthermore, the particles in chamber B with bigger cross sectional area may experience greater Brownian diffusion motions compared to smaller cross sectional area.

Figure 8 The yield obtained by different width chambers, with total & electrical yield of 96% & 96% for Chamber A and 85% & 84% for Chamber B. % sedimentation yield were nearly zero for both chambers.

Fixed parameters of flow rate (3.5ml/min), applied voltage (30Vpk-pk) and cell concentrations (OD=0.92A) were used.
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