INTRODUCTION
Na-CO$_2$ batteries, which use Na, an element three to five orders of magnitude more abundant on earth than Li, and greenhouse gas CO$_2$, theoretically offer a high energy density of 1.13 kWh kg$^{-1}$ through the reaction of 4Na + 3CO$_2$→2Na$_2$CO$_3$ + C (E$^{\theta}$ = 2.35 V) (1–4). In addition, the released CO$_2$ in car exhaust could generate electricity in Na-CO$_2$ batteries to prolong the driven miles of hybrid electric vehicles. Furthermore, 12% of off-gas emissions of thermal power plants (5) and 96% of the atmosphere of Mars (6) is CO$_2$, suggesting the potential usefulness of Na-CO$_2$ batteries for production of clean electric energy, due to the abundance of necessary materials. However, currently available primary and rechargeable Na-CO$_2$ batteries (2, 4, 7) face safety risks, mainly because of liquid electrolyte and the pure Na anode. Na-CO$_2$ batteries with sodium salt/organic solvent liquid electrolyte are plagued by leakage (because of open battery structure) (8–11), volatilization (especially in working conditions at high temperature), and electrochemical instability (caused by large polarization at high current density) (2). Na-CO$_2$ batteries also encounter dendrite formation or surface cracks in the pure Na anodes during cycling, resulting in the possibility of short circuit (12). Therefore, seeking new alternatives for liquid electrolyte and the pure Na anode is vitally important.

To resolve the liquid electrolyte issue, the quasi-solid state polymer electrolyte (QPE) strategy is effective in inorganic and organic Li-ion batteries and Na-ion batteries (13–16). It has been shown that QPE is capable of absorbing liquid electrolyte without leakage (17); it also has a high ion conductivity (10$^{-6}$ to 10$^{-3}$ S cm$^{-1}$ at room temperature) that is comparable to that of liquid electrolyte (10$^{-3}$ S cm$^{-1}$) (18, 19). In addition, adding nanosized ceramic fillers into QPE to form composite polymer electrolyte (CPE) would further increase Na$^+$ conductivity and improve mechanical strength of the polymer electrolyte (20). However, so far, to the best of our knowledge, CPE has not been used in Na-air or Na-CO$_2$ batteries. A suitable CPE for Na-CO$_2$ batteries must satisfy three conditions: (i) large amorphous region of polymer matrix in QPE to accelerate the Na$^+$ mobility, (ii) nanosized ceramic fillers with hydrophobic property to increase mechanical strength and avoid H$_2$O contamination of QPE, and (iii) elimination of macropores on QPE to avoid potential contamination from anodic CO$_2$ to cathodic Na.

Recently, graphene oxide (GO) or reduced graphene oxide (rGO) has demonstrated electrochemical and electrocatalytic properties (21, 22). In particular, a stable Li/rGO anode for long-term cycling was synthesized by the reduction of a GO sheet and then the absorption of molten Li metal at 250°C (23). However, there are few reports on methods of Na anode protection. Na has similar physical and chemical properties to Li but has stronger reducibility and a lower melting point (98°C) than Li metal. Because rGO-Na has not been reported in Na-ion, Na-air, or Na-CO$_2$ batteries, making a composite of rGO and Na metal to synthesize an rGO-Na anode is worth investigating. Furthermore, the combination of an rGO-Na anode, CPE, and an activated cathode is also important for rechargeable Na-CO$_2$ batteries.

We report here the integration of an rGO-Na anode, CPE, and an activated multiwall carbon nanotubes (a-MCNT) cathode to construct rechargeable quasi-solid state Na-CO$_2$ batteries with highly stable performance at room temperature. The CPE is hemicyrystalline PVDF-HFP [poly(vinylidene fluoride-co-hexafluoropropylene)]−4% SiO$_2$/NaClO$_4$−TEGDME (tetraethylene glycol dimethyl ether), in which hydrophobic fumed SiO$_2$ (10 to 20 nm) used as ceramic fillers enlarges the amorphous region of the CPE matrix, increases the Na$^+$ conductivity to 1.0 mS cm$^{-1}$, and improves the mechanical strength to 0.5 to 0.6 GPa. Only scarce nanopores are spread on the CPE, protecting the anode from CO$_2$. The rGO-Na anodes are achieved through reducing three-dimensional GO foam in molten Na metal (98° to 120°C) and adsorbing this molten metal into pore structures of as-prepared rGO. The addition of rGO results in even plating of Na$^+$ on the rGO-Na anode and is also able to improve the mechanical strength and toughness of the Na-based anode. The porous structure and TEGDME-wettable surface of a-MCNT cathodes benefit CO$_2$ transfer and the occurrence of battery reactions. The assembled quasi-solid state Na-CO$_2$ batteries successfully operate in a series of CO$_2$ partial pressure atmospheres [5 to 100%, simulated car exhaust] and especially to run for 400 cycles at 500 mA g$^{-1}$ with a fixed capacity of 1000 mA·hour g$^{-1}$ in pure CO$_2$. Furthermore, we scaled up the reversible capacity to 1.1 A·hour in pouch-type batteries (20 × 20 cm, 10 g, 232 Wh kg$^{-1}$). This study makes quasi-solid state Na-CO$_2$ batteries an attractive prospect.

QUASI–SOLID STATE RECHARGEABLE Na–CO$_2$ BATTERIES WITH REDUCED GRAPHENE OXIDE Na ANODES

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Na-CO$_2$ batteries using earth-abundant Na and greenhouse gas CO$_2$ are promising tools for mobile and stationary energy storage, but they still pose safety risks from leakage of liquid electrolyte and instability of the Na metal anode. These issues result in extremely harsh operating conditions of Na-CO$_2$ batteries and increase the difficulty of scaling up this technology. We report the development of quasi-solid state Na-CO$_2$ batteries with high safety using composite polymer electrolyte (CPE) and reduced graphene oxide (rGO) Na anodes. The CPE of PVDF-HFP [poly(vinylidene fluoride-co-hexafluoropropylene)]−4% SiO$_2$/NaClO$_4$−TEGDME (tetraethylene glycol dimethyl ether) has high ion conductivity (1.0 mS cm$^{-1}$), robust toughness, a nonflammable matrix, and strong electrolyte-locking ability. In addition, the rGO-Na anode presents fast and nondendritic Na$^+$ plating/stripping (5.7 to 16.5 mA cm$^{-2}$) during cycling, resulting in the possibility of short circuit (12). Only scarce nanopores are spread on the CPE, protecting the anode from CO$_2$. The rGO-Na anodes are achieved through reducing three-dimensional GO foam in molten Na metal (98° to 120°C) and adsorbing this molten metal into pore structures of as-prepared rGO. The addition of rGO results in even plating of Na$^+$ on the rGO-Na anode and is also able to improve the mechanical strength and toughness of the Na-based anode. The porous structure and TEGDME-wettable surface of a-MCNT cathodes benefit CO$_2$ transfer and the occurrence of battery reactions. The assembled quasi-solid state Na-CO$_2$ batteries successfully operate in a series of CO$_2$ partial pressure atmospheres [5 to 100%, simulated car exhaust] and especially to run for 400 cycles at 500 mA g$^{-1}$ with a fixed capacity of 1000 mA·hour g$^{-1}$ in pure CO$_2$. Furthermore, we scaled up the reversible capacity to 1.1 A·hour in pouch-type batteries (20 × 20 cm, 10 g, 232 Wh kg$^{-1}$). This study makes quasi-solid state Na-CO$_2$ batteries an attractive prospect.

Keywords: Na–CO$_2$ batteries; quasi-solid state; CPE; rGO; safety; performance; long-term cycling.

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exhaust (SCE)]. We scaled up the batteries to a reversible capacity of 1.1 A·hour with an energy density of 232 Wh kg\(^{-1}\). By fixing ~20% depth of discharge and charge (200 mA·hour), Na-CO\(_2\) batteries have so far run for 50 cycles with the capacity retention of nearly 100%.

RESULTS

Synthesis and characterization of CPE

A CPE synthesized by integrating polymer matrix of PVDF-HFP, nanosized SiO\(_2\), and a plasticizer of NaClO\(_4\)/TEGDME solution solves the issues of leakage, volatilization, and electrochemical instability of liquid electrolyte in Na-CO\(_2\) batteries (Fig. 1A). The large number of F atoms in the PVDF-HFP and TEGDME agent plays a key role in Na\(^+\) diffusion. The mass percent of fumed SiO\(_2\) with a diameter of 10 to 20 nm (inset of Fig. 1A) as the ceramic filler in CPE is a critical factor for ionic conductivity. The content of fumed SiO\(_2\) with 4 weight % (wt %) reaches the highest ion conductivity of 1.0 mS cm\(^{-1}\) (Fig. 1B and figs. S1 and S2).

The optimized CPE (namely, PVDF-HFP–4% SiO\(_2\)/NaClO\(_4\)–TEGDME) with a thickness of ~160 \(\mu\)m (Fig. 1C) has a high ion conductivity (1.0 mS cm\(^{-1}\)). CPE with pores centered at ~30 nm (fig. S3) could suppress CO\(_2\) diffusion to the anode and thus protect the Na metal (fig. S4). This CPE has a good toughness with a Young modulus of 0.5 to 0.6 GPa and a roughness of ~80 nm (Fig. 1, D and E, figs. S5 and S6). Suitable toughness and roughness of CPE benefit by tight contact to electrodes. Serious leakage occurs in a traditional Na-CO\(_2\) battery containing liquid electrolyte, but the CPE-based Na-CO\(_2\) battery successfully suppresses leakage (fig. S7). Moreover, this polymer matrix of CPE does not easily catch fire. Even if it catches fire after long-time ignition (5 s), the fire is soon quenched automatically (1 s; Fig. 1F). We also find that the addition of SiO\(_2\) increases both flame resistance and the melting point of the polymer matrix of CPE (fig. S8).

As one component of CPE for Na\(^+\) diffusion, TEGDME has a high boiling point (~275°C), but it still volatilizes even at room temperature in the open system of a traditional Na-CO\(_2\) battery. Our synthesized CPE can effectively suppress electrolyte volatilization because of robust intermolecular forces between TEGDME and polymer chains of CPE. This intermolecular force was confirmed by Raman spectroscopy, in which the relative peak intensities of both TEGDME and PVDF-HFP were changed (fig. S9). According to thermal gravity analysis and heat flow curves (Fig. 1G), CPE underwent two mass loss in temperature ranges of 126° to 222°C and 370° to 475°C. Within each temperature range, CPE showed endothermic thermal events twice, corresponding to TEGDME volatilization and PVDF-HFP decomposition, respectively. The residual mass of CPE after TEGDME volatilization at 222°C is 70%, indicating that the absorbed liquid electrolyte amount (ALEA) within CPE is 30%. This low ALEA (<50%) demonstrates that the diffusion of Na\(^+\) in CPE is mainly attributed to the polymer host of CPE (fig. S10A). In the same way, the ALEA within glass fiber (a traditional separator in an open battery system) is 80%, and the corresponding temperature interval of TEGDME volatilization is 82° to 206°C. The elevated volatilization temperature (126° to 222°C versus 82° to 206°C) of TEGDME proves that CPE can suppress electrolyte volatilization. In addition, the wide electrochemical window of CPE, 1.0 to 4.5 V, should provide the battery system with safe and stable conditions (fig. S10B). The CPE also exhibits long-term stability in terms of morphology and chemical structure (fig. S11). The abovementioned properties indicate the practical values of CPE.

Synthesis and characterization of rGO-Na anode

To achieve a highly stable Na-based anode and economize Na resources, we designed and fabricated an advanced rGO-Na anode for quasi–solid state Na-CO\(_2\) batteries. Getting rGO foam with a good Na affinity and infusing molten Na into the abundant nanopores of rGO are vitally important for the fabrication of the rGO-Na anode. When used as a starting material fabricated by the freeze-drying of GO solution, the GO foam displays a porous structure with the mass of GO microsheets (Fig. 2A).
When the GO foam was connected in parallel to the molten Na (120°C), an instantaneous reaction occurred across the whole foam (movie S1). In this step, gray GO foam was reduced to dark black rGO, simultaneously resulting in a more porous and stable construction (Fig. 2B). Next, fast and uniform Na intake was achieved simply by placing the edge of the rGO foam into molten Na, finally resulting in a substantial surface with metal luster (Fig. 2C). It takes about 1 min for Na to diffuse across the whole rGO foam (movie S2). This successful synthesis of the rGO-Na anode is correlated to the capillary force produced by the nanopores of rGO foam and the good Na affinity with rGO foam. The extent of the interior filling of the rGO foam by Na is determined by element mapping (fig. S12A), which shows that the host of the rGO foam is totally filled with Na.

The reduction of GO foam by molten Na is confirmed by Fourier transform infrared spectroscopy (FTIR) and x-ray photoelectron spectroscopy (XPS). Before the reduction reaction, a broad peak beyond 2900 cm\(^{-1}\) corresponding to \(-\text{OH}\) stretching was detected (Fig. 2D), revealing the presence of adsorbed water or surface \(-\text{OH}\). Meanwhile, characteristic peaks of other surface groups, including carbonyl (C=O) (~1725 cm\(^{-1}\)) and epoxy \((\text{C}–\text{O}–\text{C})\) (~1048 cm\(^{-1}\)), were also observed. Obviously, after the reduction reaction, the abovementioned oxygen-containing functional groups became almost undetectable, confirming the high reduction level of rGO. The XPS analysis is consistent with the FTIR result. According to the deconvoluted O1s and C1s spectra (Fig. 2, E and F), the intensity of C–OH dropped from 43.2% (GO foam) to 14.7% (rGO foam), indicating the remarkable removal of \(-\text{OH}\) groups. The Na (0) in the Na1s spectra of the rGO-Na anode (fig. S12B) arises from Na metal absorbed in rGO. A small quantity of Na (I) is probably correlated with the Na\(_2\)O or Na\(_2\)CO\(_3\) that is formed during the thermal reduction of GO in molten Na. The oxygen-containing groups on GO may react with molten Na and produce Na (I) species. The successful Na perfusion into rGO foam is verified by x-ray diffraction (XRD), which also suggests the absence of crystalline Na (I) species (Fig. 2G). The tensile strength test and bending test indicate that the rGO foam improves the mechanical strength and toughness of the rGO-Na anode in comparison with the pure Na anode (fig. S13).

In comparison with the pure Na metal anode, the rGO-Na anode has higher cyclic voltammetry current density (5.7 to 16.5 mA cm\(^{-2}\)), demonstrating a fast kinetics of Na\(^+\) plating/stripping on rGO-Na anodes (Fig. 2H). Fast discharge and charge operation within 1.0 to 4.0 V at 0.3 mA cm\(^{-2}\); voltage range, 1 to 4 V. Inset: SEM images of rGO-Na and pure Na anode surfaces after 450 cycles.
difference between the pure Na anode and the rGO-Na anode indicates that the addition of rGO foam leads to even plating of Na⁺ on the rGO-Na anode. In the fast discharge/charge profiles, the capacitance behavior of rGO-Na in Ar is much more obvious than that of pure Na, a difference that can be attributed mainly to the larger specific area of the rGO-Na anode. Symmetric rGO-Na electrodes also exhibit much lower electrochemical polarization (±0.05 V) in the first 90,000 s at 1 mA cm⁻² during plating/stripping than that of pure Na electrodes (±0.15 V) (fig. S15), further confirming the superiorit of rGO-Na electrodes.

### a-MCNT cathodes

To further improve the reaction activity of carbon nanotubes on cathodes, we boiled the MCNTs in TEGDME at 100°C to be a-MCNTs. The a-MCNTs are characterized by Raman and FTIR, but the TEGDME signals only appear in FTIR (Fig. 3, A and B). This suggests that the TEGDME solvent has infiltrated into the internal walls of a-MCNTs. In detail, bands at around 2850 cm⁻¹ indicate the presence of –CH₃ and –CH₂– in TEGDME, whereas bands at 1100 cm⁻¹ were C=O and C–C stretching signals, which also belong to TEGDME (Fig. 3B). The intensity ratios of D-band and G-band in a-MCNTs and MCNTs are 1.06 and 1.03, respectively (Fig. 3A), indicating a higher disorder degree of carbon atoms in a-MCNTs. In detail, D-band and G-band peaks stand for sp²-type carbon, whereas other peaks at 1317.3 and 1504.8 cm⁻¹ are assigned to the sp³-type carbon (for example, –COOH) in a-MCNTs.

According to the density functional theory (DFT) calculation (Fig. 3, C and D, and fig. S16), the adsorption energy of a-MCNTs (~0.32 eV) is much higher than that of pristine MCNT (~0.17 eV). After activation, the tubular morphology and multwall structure of carbon nanotubes are not destroyed (Fig. 3, E to G), and the wettability of carbon nanotubes toward TEGDME is enhanced (fig. S17). All the abovementioned merits of a-MCNTs lay a solid foundation for following interface reactions of Na-CO₂ batteries. On the basis of the configuration of the Na/NaClO₄-TEGDME/cathode, the initial discharge and charge profiles of Na-CO₂ batteries with a-MCNT cathodes exhibit smaller overpotentials (1.39 V) than those with MCNT cathodes (2.04 V) (fig. S18), preliminarily confirming the effectiveness of a-MCNT cathodes.

### Battery performance

By combining an rGO-Na anode, optimal CPE, and a-MCNT cathodes, quasi–solid state Na-CO₂ batteries are first assembled in CR2032 coin-type cells, which exhibit clear discharge-charge voltage plateaus at various rates (Fig. 4A). When the batteries operate at 100, 200, 300, and 500 mA g⁻¹, the charge-discharge voltage gap is 0.74, 0.88, 0.93, and 1.48 V, respectively. However, the initial charge voltage is still low. For example, even at 500 mA g⁻¹, the initial charge voltage is still <3.49 V, which is much lower than the upper limit of the voltage window of CPE. The reaction of 4Na + 3CO₂ ↔ 2Na₂CO₃ + C in quasi–solid state Na-CO₂ batteries has been demonstrated (figs. S19 and S20), and it is consistent with that in liquid electrolyte–based Na-CO₂ batteries (4). In addition, we find that the current densities could control the morphologies of discharge product in Na-CO₂ batteries (insets of Fig. 4A). The current densities of 100 and 200 mA g⁻¹ lead to discharge products (nanoparticles) with a round shape (100 to 200 nm in diameter). Meanwhile, larger current densities result in larger sizes of discharge products, namely, angular particles (200 to 300 nm) at 300 mA g⁻¹ and nanobelts (30 × 200 × 500 nm) at 500 mA g⁻¹. This variation in discharge products is different from Li-O₂ batteries (24) but similar to Na-O₂ batteries (25). The discharge products at various current densities (for example, 100, 200, and 300 mA g⁻¹)
pile up rather than just grow on a-MCNT surfaces (fig. S21), suggesting large capacity ability.

Charge-discharge operation at current densities of 200 and 500 mA g$^{-1}$ demonstrates an impressive stability of quasi–solid state Na-CO$_2$ batteries (Fig. 4, B and C). Especially at 500 mA g$^{-1}$, the batteries perfectly maintained the specific capacity of 1000 mA·hour g$^{-1}$ for 400 cycles without obvious fading. Highly reversible capacity of 5000 mA·hour g$^{-1}$ at 50 mA g$^{-1}$ is also obtained with controllable capacity, and finally, stable capacity of ~3000 mA·hour g$^{-1}$ is maintained (fig. S22). This advanced battery performance is mainly due to the sufficient ion conductivity of CPE, fast Na$^+$ plating/stripping kinetics of the rGO-Na anode, and the active surface of a-MCNT cathodes. Excitingly, the performance of quasi–solid state Na-CO$_2$ batteries is comparable to that of other liquid electrolyte-based metal-CO$_2$ batteries (table S1). Moreover, we extend the cathode materials to curvy carbon nanosheets that were synthesized by chemical vapor deposition via the reaction of CO$_2$+2Mg→C+2MgO (fig. S23). The MgO was removed from the carbon nanosheets by HCl solution treatment. This carbon material also enables quasi–solid state Na-CO$_2$ batteries to become rechargeable and form nanosized discharge products (fig. S24).

We investigated the battery performance in SCE with different CO$_2$ partial pressure. As is well known, no matter how strict the tailpipe standards [for example, Euro V/VI regulations (26)], all car exhaust must contain a humid mixture of N$_2$ and CO$_2$ (27, 28), which is transformed from initial petrol combustion products by built-in exhaust decontamination equipment. We design a device to fill our coin-type battery vessels with humid (humidity of 100%) or dry SCE (mixture of CO$_2$ and N$_2$; fig. S25), in which the batteries could operate normally even at CO$_2$ partial pressures as low as 0.05 atm (Fig. 4D). The hydrophobic breathable film (PVDF film) provides the battery operation (fig. S26) with relative dry conditions and suppresses side reactions relating to H$_2$O. The batteries in SCE (for example, 50% CO$_2$ and 50% N$_2$) could also run at 50°C for 50 cycles at 200 mA g$^{-1}$ with overpotentials of 0.79 to 0.81 V (fig. S27). The stable discharge and charge profiles indicate the reliability of the battery system in SCE.

Because batteries with high capacity (mA·hour) and high energy density (Wh kg$^{-1}$) are highly desirable for practical applications such as electric cars and electrical grid storage, we expanded the battery scale from CR2032 coin-type batteries (2 cm in diameter) to large batteries (20 × 20 cm). One large piece of semitransparent CPE film was integrated with an rGO-Na/Cu foil anode and a carbon cathode in a plastic bag, finally producing a pouch-type battery (Fig. 4E and fig. S28). With controlled voltage of 1.9 to 3.9 V, initial capacity of 1100 mA·hour at 10 mA is reached, corresponding to 232 Wh kg$^{-1}$ on the basis of the total mass of the pouch-type battery (10.0 g) (fig. S29A). This energy density is higher than that of commercial Li-ion batteries (150 to 180 Wh kg$^{-1}$) (29), suggesting the possibility of large-scale application of quasi–solid state rechargeable Na-CO$_2$ batteries. At the depth of both 20 and 50% discharge/charge, the capacity retention of quasi–solid state rechargeable Na-CO$_2$ batteries is 100%, without obvious voltage fading (Fig. 4F and fig. S29B).

**DISCUSSION**

The investigations described here give us an overall picture of quasi–solid state Na-CO$_2$ batteries with the rGO-Na anode, optimized CPE, and a-MCNT cathodes. During discharge, the CO$_2$ absorbs on the a-MCNT cathode surface and reacts with Na$^+$ to generate products of Na$_2$CO$_3$.
and carbon at the electrode/electrolyte interface. During charge, the products reversibly decompose and release CO2 gas and Na+. The rGO-Na anode promotes dendrite-free plating/stripping (5.7 to 16.5 mA cm−2) and saves Na metal resources. The CPE suppresses electrolyte volatilization and provides high Na+ conductivity (1.0 mS cm−1 at 25°C) for stable operation of batteries. The a-MCNT cathodes offer the adsorption of CO2 on activated carbon surface and the formation of products. Therefore, all components (anode, electrolyte, and cathode) have irreplacable roles and are vitally important to obtain the long life and stability of quasi–solid state Na2CO3 batteries. Moreover, the unflammable PVDF-HFP–4% SiO2 as matrix in CPE, abundant Na metal–based anode, and clean utilization of CO2 for energy conversion further improve the practical value of quasi–solid state Na2O2 batteries for future stationary and mobile storage technologies. On the basis of this rGO-Na/CPE/CO2 system, the ascribed coin-type batteries can operate at various CO2 partial pressures and, in particular, can run for 400 cycles in pure CO2. The pouch-type battery also exhibits a large capacity of 1.1 A·hour with an energy density of 232 Wh kg−1 and a stable cycling life (50 cycles). This demonstrates the feasibility of safe and stable Na2CO3 batteries, which should accelerate the process of practical application with abundant Na resource and CO2 fuels.

MATERIALS AND METHODS
Polymer electrolyte fabrication
The mixture (2.0 g) of PVDF-HFP copolymer and fumed silica with various mass ratio (0, 2, 3, 4, 6, and 8 wt % SiO2) was dissolved in aceton (15 ml). This solution was heated in oil bath at 50°C for 2 hours with vigorous stirring, followed by resting at the same temperature for 1 hour. The resultant viscous solution was spread as a film on aluminium foil using a graduated blade. Then, the polymer film was dried at 100°C under vacuum. After cooling to room temperature, the polymer film was immersed into a pool of 1 M NaClO4/TEGDME for 48 hours. Before use, the moistened film was wiped with filter paper to remove residual liquid electrolyte. We also synthesized large pieces of CPE by film applicator using a composition of PVDF-HFP–4% SiO2.

Cathode fabrication
MCNTs (42 mg) and TEGDME solvent (20 ml) were added to a round-bottom flask (100 ml). When heated in oil bath at 100°C for 2 hours under vigorous stirring. The mixture was then filtered and dried under vacuum at 160°C for 2 hours to obtain TEGDME-activated carbon material (a-MCNTs). The resulting a-MCNTs were mixed with 5 wt % PVDF binder in the solvent of N-methyl pyrrolidone by fully grinding in a mortar. The obtained slurry was pasted onto a piece of Ni mesh (010 mm) and dried under vacuum at 100°C for 10 hours. Finally, a-MCNT cathodes were formed with a loading mass of 0.3 mg cm−2. Cathodes with curly carbon nanosheets were prepared by the same method as a-MCNT cathodes. Ag nanowire cathodes were prepared by the following steps. First, Ag nanowires (1 mg) were added to the TEGDME (2 ml) solvent. After continuous sonication for 2 hours, a homogeneous ink was obtained. Second, 10 μl of the ink was added onto a nickel mesh (400 mesh, Emgrid Australia Pty Ltd.) by a pipette. After drying at 25°C under vacuum for 12 hours, Ag nanowire cathodes were obtained.

rGO-Na anode fabrication
The GO solution (5 g liter−1) was prepared by Hummer’s method (30). Briefly, graphite (10 g), concentrated H2SO4 (230 ml), and NaNO3 (5 g) were mixed and cooled down to 0°C. Then, 30 g of KMnO4 powder was added with vigorous stirring for 2 hours. After reaction at 35°C for 3 hours, distilled water (1000 ml, 18.2 megohm resistance) and H2O2 (400 ml, 30%) were added to remove the unreacted KMnO4 and manganese dioxide. The resulting graphite oxide was separated and washed repeatedly. Afterward, the GO solution was made by the ultrasonication exfoliation of graphite oxides in water (3000 ml) and the centrifugation at a speed of 6000 rpm for 30 min. The centrifuged GO solution was purified by dialysis until its pH value was about 6. Finally, highly stable GO solution was obtained, and the concentration was adjusted to 5 g liter−1. This GO solution was freeze-dried at ~47°C under 19 Pa for 24 hours. Then, freestanding GO films were obtained and transferred to an Ar-filled glove box with O2 level <1 parts per million. To realize the spark reaction, polished Na bulk (99.9%; Alfa Aesar) were melted in a round stainless steel pan on a hot plate at ~120°C. The GO films were slightly pressed and then brought into contact with the molten Na, and the spark reaction occurred instantaneously. This spark reaction partially transformed the GO into rGO. The molten Na was infused through the edges of the pressed rGO foam. Finally, rGO-Na sheets were obtained. Before being used as Na-based anodes in batteries, rGO-Na sheets were pressed slightly and cut into discs (ø10 mm) for coin-cell type or spliced together into square pieces (20 × 20 cm) for pouch-type batteries.

SUPPLEMENTARY MATERIALS
Supplementary material for this article is available at http://advances.sciencemag.org/cgi/content/full/3/2/e1602396/DC1

Chemicals and materials
Fabrication of curly carbon nanosheets
Material characterization
Battery assembly
Electrochemical test
CO2 evolution test
Energy density calculation
Density function theory (DFT) calculation
Explanatory calculation
fig. S1. The raw materials and synthesis procedures of CPE.
fig. S2. The optimization of Na+·CPE.
fig. S3. The pore size distribution of CPE.
fig. S4. The CO2 diffusion test.
fig. S5. SEM images of CPE surface.
fig. S6. Roughness and Young modulus of polymer matrix (PVDF-HFP/4% SiO2) of CPE.
fig. S7. Leakage test of Na-CO2 batteries.
fig. S8. Inflammability test of polymer matrix (PVDF-HFP/SiO2) of CPE.
fig. S9. Raman of CPE, polymer matrix, and liquid electrolyte.
fig. S10. Transporting mechanism of Na+ in polymer chains and work window of CPE.
fig. S11. Long-term stability analysis of CPE.
fig. S12. Element mapping and XPS-Na1s of rGO-Na anode.
fig. S13. Mechanical strength and toughness of pure Na and rGO-Na anodes.
fig. S14. Anode analysis.
fig. S15. Galvanostatic cycling of a symmetric rGO-Na electrodes and pure Na anodes.
fig. S16. The optimized geometries of CO2 adsorbed on MCNT and a-MCNTs.
fig. S17. Soluble inflation of MCNTs and a-MCNTs toward TEGDME solvent.
fig. S18. Initial discharge and charge profiles of Na2CO3 batteries with the configuration of Na/NaClO4/TEGDME/cathode.
fig. S19. Reaction mechanism analysis of Na2CO3 batteries.
fig. S20. Discharge product analysis of quasi–solid state Na2CO3 battery.
fig. S21. SEM image of a-MCNT cathode with discharge capacity of 0.1 mA·hour at 100 mA g−1.
fig. S22. Full discharge and charge of quasi–solid state Na2CO3 batteries.
fig. S23. Characterizations of curly carbon nanosheets.
fig. S24. Discharge/charge curves of quasi–solid state Na2CO3 batteries with new carbon cathodes that contain curly carbon nanosheets.
fig. S25. A device for SCE.
fig. S26. Discharge/charge profiles in SCE with PVDF film protection of quasi–solid state Na2CO3 batteries.
fig. S27. Discharge/charge profiles of quasi–solid state Na2CO3 batteries at 50°C.
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