Weather impact on airborne coronavirus survival

Note: This paper is part of the Special Topic, Flow and the Virus.

Affiliations
University of Nicosia, Nicosia CY-2417, Cyprus

I. INTRODUCTION

Aerosol of respiratory droplet transmission is a primary vehicle for the rapid spread and continued circulation of viruses in humans. There is also evidence that environmental conditions can affect virus transmission.

The virions, i.e., the infectious particle designed for the transmission of the nucleic acid genome among hosts or host cells, are expelled from humans through coughing, sneezing, talking, or normal breathing and are immersed in a respiratory fluid. A critical factor for the transmission of the airborne virions is the saliva liquid carrier-droplet evaporation. If we have a better understanding of the evaporation process and its relation to climate effects, we can more accurately predict the evolution of virus concentration in space and in time and determine its viability rate, i.e., potential of virus survival.

There are many papers dedicated to the investigation of various fluid dynamics and heat transfer aspects of droplet evaporation, e.g., see Refs. 8 and 9 and references therein. Despite the importance of airborne droplet transmission, research regarding heat and mass transfer around and within respiratory droplets containing virions is scarce. Vejerano et al. showed that the chemical microenvironment immediately surrounding virions in droplets and aerosols is likely to be a critical determinant of their stability.

Droplet evaporation, in general, has been studied for various applications, but the evaporation of saliva droplets containing
virus particles is not understood. So far, the theory for heat and mass transfer was based on the Nusselt (Nu) and Sherwood (Sh) number correlations of Ranz and Marshall,\textsuperscript{11,12} which defined Nu and Sh numbers a function of the Reynolds, Prandtl, and Schmidt numbers. However, the Ranz and Marshall\textsuperscript{11,12} formulas concern a steady-state heat and mass transfer of flowing spherical particles made of a single material. Many authors incorrectly adopted them in the literature for different transient cases, neglecting the multi-material (mixture) properties of spherical droplets.

In this study, we develop new correlations for heat and mass transfer for droplet evaporation, which provide Nu and Sh as a function of time, Reynolds, Prandtl, and Schmidt numbers, as well as including fluid and thermodynamic properties of the virus. We have introduced the thermodynamic properties of virions as a liquid. The correlations include the liquid saliva portion inside the droplet through the molecular formula for the phospholipid of a coronavirus (CoV) capsid structure. Furthermore, we introduce transient effects and a thermal history kernel. The new correlations account for the virion concentration in saliva droplets and their effect on the unsteady evaporation process.

The knowledge of climate effects on SARS-CoV-2 and other virus survival and transmission is limited, as recent studies have shown.\textsuperscript{13–18} Virus infections are more common during winter times, and it has been mentioned that the CoV can be transmitted for a period of up to two weeks at low temperatures and low humidity.\textsuperscript{19} However, the mechanisms of climate parameters influencing the virus survival, concentration, and disease transmission remain unknown. There is an urgency to understand the climate parameters on COVID-19, particularly while facing the possibility of continued spread of the virus worldwide. Using the new heat and mass transfer correlations, we present a study of the effects of relative humidity (RH), environmental temperature, and wind speed on the respiratory cloud and virus viability. The results provide new insight into the influence of the above parameters, which contradicts current understanding.

II. SURVIVAL OF AIRBORNE CONTAMINATED SALIVA DROPLETS

The coronavirus (CoV) COVID-19 has been consistently detected in the saliva of infected persons.\textsuperscript{20} Recent studies confirmed that human saliva constitutes high potential for the diagnostic and transmission of COVID-19 among humans.\textsuperscript{21–23}

The mechanism of reduction of virus concentration due to evaporation can be described in three steps (Fig. 1): (a) we assume a contaminated saliva droplet. (b) The process includes the saliva droplet advection and evaporation. An evaporating vapor film of thickness $t_d$ forms around the droplet. (c) The complete droplet evaporation leads to the virus structure decomposition and inactivation. Therefore, evaporation is crucial for limiting airborne virus transmission.

A. Importance of climate conditions

The influence of relative humidity and temperature on the airborne virus survival is a complex topic. The outcomes of past experimental studies are contradictory, and the mechanism of the effect of relative humidity and temperature on virus survival remains mostly unknown. Previous studies from the literature reported that relative humidity is a significant climate determinant in the transmission of influenza.\textsuperscript{24–26} Past research also attempted to optimize and control the humidity level to reduce the virus survival in an indoor environment.\textsuperscript{27}

Yang and Marr\textsuperscript{28} reviewed different conjectures regarding the relationship between relative humidity and the virus in aerosols. Water activity, surface inactivation, and salt toxicity could play an essential role in the virus’s persistence in experimental studies. Sobsey and Meschke\textsuperscript{29} suggested in a WHO report that enveloped viruses containing a lipid membrane have higher survivability at lower RH. In contrast, non-enveloped ones tend to be more stable at higher RH. However, the above hypothesis does not explain several other phenomena, e.g., the Rous sarcoma virus (RSV) and

![FIG. 1. A three-step mechanism of virus destruction due to evaporation. Step 1: A saliva droplet of diameter $d_p$ is initially contaminated by CoV particles of $C_0$ concentration. Step 2: The evaporation process begins with $q$ and $j$ being the surface heat and mass fluxes due to saliva droplet advection in air and evaporation. $t_d$ denotes the thickness of the evaporating vapor film. Step 3: Virus decomposition and inactivation.](image-url)
infectious bovine rhinotracheitis virus (IBRV), which are enveloped and appear more stable at higher RH, or the pigeon pox virus, which is insensitive to RH; see Ref. 28 and references therein. Harper30 studied the RH effects on vaccinia, influenza, Venezuelan equine encephalomyelitis, and poliomyelitis experimentally. At each RH level, he found that viable survival of airborne viruses was better at lower temperature values than at higher ones. He illustrated that poliomyelitis virus has the best durability at high RH, while all the other three viruses have the best survivability at low RH. After 50 years, many researchers still believe and emphasize that the coronavirus is less likely to survive at high RH. They used this message to propose solutions for reducing COVID-19 by increasing the RH in indoor environments. Unfortunately, there exists a vital enigma behind this topic. The findings by Webb et al.31 presented another contradictory theory, which was recently confirmed to be true.28 Yang and Marr showed that the effect of RH on airborne virus survival is profoundly affected by the initial composition of the spraying medium used to create the experimental airborne droplet. When the spraying medium is water, the airborne viruses survive better at high RH. The above is due to the added water through spraying that delays evaporation and not to the environmental humidity that exists in the surrounding air; hence, the conclusions of past research were misleading. By developing a new theory and modeling of heat and mass transfer, we have performed 3D computational fluid dynamics (CFD) simulations showing how the behavior of the virus changes across a range of RH and temperatures. We will show that airborne viruses can survive at high RH, which is in agreement with the experimental findings of Webb et al.31 and the review of Yang and Marr.28

B. Heat and mass transfer of an evaporating virus-contaminated saliva droplet

When a contaminated saliva droplet is expelled from the mouth or nose into the surroundings at speed $U_{cough}$, it exchanges heat and mass with ambient air (evaporation). We consider unsteady free-stream airflow at speed $U_{wind} = U_\infty$ around a spherical saliva droplet at different Reynolds numbers, as illustrated in Fig. 2(a). The saliva droplet contains CoV particles at an initial concentration of $C_0$. We take into account the conjugated heat transfer in the airflow and inside the saliva droplet. Figure 2(b) shows an example at $Re = 200$ [Eq. (1)] for the solution of the temperature distribution at $t = 2.5 \text{ ms}$. The above is due to the added water through spraying that delays evaporation and not to the environmental humidity that exists in the surrounding air; hence, the conclusions of past research were misleading. By developing a new theory and modeling of heat and mass transfer, we have performed 3D computational fluid dynamics (CFD) simulations showing how the behavior of the virus changes across a range of RH and temperatures. We will show that airborne viruses can survive at high RH, which is in agreement with the experimental findings of Webb et al.31 and the review of Yang and Marr.28

FIG. 2. A schematic representation for quantifying the effect of weather on the heat and mass transfer rate of a CoV-contaminated saliva droplet. [(a) and (c)] Schematics of the computational domain showing the weather conditions (wind speed $U_{wind} = U_\infty$, environment temperature $T = T_\infty$, the relative humidity RH, and the initial concentration $C_0$ of CoV in saliva). $d_d$ denotes the thickness of the evaporating vapor film. (b) An example at $Re = 200$ [see Eq. (1)] that shows the temperature distribution at $t = 2.5 \text{ ms}$ around a contaminated saliva droplet from different perspective plane views. (d) An example at $U_{wind} = 4 \text{ km/h}$ showing the transport and evaporation of a contaminated cloud of saliva droplets between 1 and 5 s. The green and red boxes show the parameters used to conduct the different 3D CFD simulations for the freestream of air flowing around a contaminated saliva droplet (green box: single sphere droplet; red box: droplet cloud). The cloud is expelled at a cough speed of $U_{cough} = 8.5 \text{ m/s}$, as explained in the work of Dbouk and Drikakis.32

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t = 2.5 ms around a contaminated saliva droplet. We also consider hundreds of CFD simulations for a contaminated cloud of saliva droplets expelled at a $U_{cough} = 8.5$ m/s [see Fig. 2(c)] to quantify the influence of the weather conditions on the airborne CoV viability, thus virus transmission. Figure 2(d) shows an example at $U_{wind} = 4$ km/h, RH = 10%, and $T_{\infty} = 10^\circ$C for the cloud transport and evaporation between 1 s and 5 s.

The convection inside the saliva droplet was neglected due to the low temperature gradients and high viscosity ratio ($\rho_f/\mu_f \gg 1$). The transient compressible Navier–Stokes and energy equations for the airflow and the heat diffusion equation for the saliva droplet are solved iteratively over a three-dimensional refined computational grid. Mesh sensitivity analysis was conducted and the size of the grid was decided according to a grid convergence index proposed by Ref. 33 applied in our case to the averaged heat flux $q$ (see Fig. 1) computed at the surface of the saliva droplet. Second-order schemes in both space and time in the framework of a finite volume method discretization were applied.

Since the capsid of CoV represents the largest surface area of the virus particle, its thermal and physical properties must be taken into account. The CoV capsid is a phospholipid bilayer that has properties very similar to dipalmitoylphosphatidylcholine (DPPC). DPPC has an effective density close to water. Its heat capacity is 2167 J kg$^{-1}$ K$^{-1}$ and its thermal conductivity is about 0.48 W m$^{-1}$ K$^{-1}$.

We performed several CFD simulations to quantify the heat transfer for an airflow around a CoV-contaminated saliva droplet at different Reynolds and Prandtl numbers,

$$Re_{\infty} = \frac{\rho_{\infty} U_{\infty} dp}{\mu_{\infty}},$$

(1)

$$Pr_{\infty} = \frac{\sigma_{\rho_{\infty} \mu_{\infty}}}{\kappa_{\infty}},$$

(2)

where $\mu_{\infty}$ is the dynamic viscosity, $k_{\infty}$ is the thermal conductivity, $\sigma_{\rho_{\infty}}$ is the heat capacity, and $\rho_{\infty}$ is the density. The subscript $\infty$ symbol denotes airflow properties far away from the spherical droplet (see Fig. 2). The new correlations emerging from the present study are presented in this section together with a historical overview of the evolution of the Nusselt number correlation.

To quantify the heat and mass transfer, we conducted hundreds of different 3D CFD simulations for the freestream of air flowing around a contaminated saliva droplet. Figure 2 The green and red boxes in Fig. 2 show the several parameters used to conduct the numerous CFD simulations.

The averaged local Nusselt number $\overline{Nu}$ describing the ratio of convective to conductive heat transfer is given by

$$\overline{Nu} = \frac{h dp}{k_{\infty}},$$

(3)

where $k_{\infty}$ is the initial thermal conductivity of air at ambient temperature and pressure. $h$ is the averaged convective heat transfer coefficient defined at the droplet surface,

$$\bar{h} = \frac{\bar{q}}{(\bar{T}_S - T_{\infty})},$$

(4)

and

$$\bar{T}_S = \int_{S} T dS,$$

(5)

where $S$ is the spherical surface boundary of the saliva droplet and $\bar{q}$ is the averaged local heat flux per unit area (W/m$^2$) computed at the interface between the saliva droplet and the surrounding airflow. $\bar{T}_S$ is the averaged temperature of the saliva droplet surface, and $T_{\infty}$ is the airflow free-stream temperature ($T_{\infty} = 293$ K).

Experimental studies of heat and mass transfer for a single spherical droplet are scarce because of the difficulties in accomplishing accurate experiments, especially when small microdroplets are involved at varying Reynolds and Prandtl numbers. The classical theory widely used today for estimating the evaporation rate of spherical droplets in many applications originates from Ranz and Marshall, who correlated the Nusselt number to the Reynolds and Prandtl numbers,

$$Nu = 2 + 0.55 Re^{1/2} Pr^{1/3}.$$  

(6)

Ranz’s and Marshall’s studies were complementary to the results by Fuchs, Wells, and Frossling back in the 1930s. Following Ranz and Marshall, several authors researched to improve and extend the Nusselt number correlation as a function of the Reynolds number; see the work of Acivos and Brenner. The Ranz and Marshall correlation was enhanced after several years by Refs. 43 and 44. The result of the above efforts was the following equation:

$$Nu = 2 + (0.4 Re_{\infty}^{1/2} + 0.06 Re_{\infty}^{2/3}) Pr_{\infty}^{0.4}(\mu_{\infty}/\mu_l)^{1/4},$$

(7)

For spheres immersed in infinite media, Whitaker showed that in the laminar boundary layer region, the contribution to the Nusselt number should be of the form $Re_{\infty}^{1/2} Pr_{\infty}^{1/3}$ while in the wake region, Richardson proposed the form $Re_{\infty}^{1/2} Pr_{\infty}^{2/3}$. The above lead to Eq. (7) with the exponents’ values obtained by fitting with the experimental data of Kramers and Vliet and Leppert.

Feng and Michaelides highlighted and quantified the effects of high and low Peclet numbers and the influence of arbitrary shapes and viscous particles on the Nusselt number correlation. Moreover, they shed light on the unsteady effect of heat transfer studying a sphere at small Peclet numbers. They studied the unsteady heat conduction equation from a small sphere considering terms that are analogous to those found in the equation of motion of a sphere ("Basset terms") as it was shown recently by Duan et al. They derived their results from asymptotic analysis and showed that the transient Nusselt number is of the form $Nu = 2 + 1/\sqrt{\pi t^*}$, while $t^* = O(1)$. To our knowledge, there are no experimental measurements for the unsteady evaporation process of liquid droplets immersed in infinite medium that could be used in validating the above term. However, the asymptotic analysis is accurate and derived from first principles. Thus, we have adopted the above term in the present modeling of contaminated liquid saliva droplets.

Yearling and Gould improved the Nusselt vs Reynolds number correlation to account for the influence of the relative turbulence intensity ($\alpha_t$) of an upstream airflow on the evaporation rate of liquid droplets. They introduced a correction term of the form $(1 + \alpha_t^{0.85})$. Lee, Hsu, and Plesnder investigated the role of the heat capacity ratio between the far-field airflow and the zone near the surface of the droplet where evaporation takes place—the above is relevant to the $l_d$ layer in Fig. 1—and they introduced a multiphase term of the form $(\bar{q}_{\infty}/\bar{q}_{l_d})^{0.38}$.
Based upon the above findings, in the present study, we propose a new correlation for the transient Nusselt number that accounts for the transient effects, turbulent airflow intensity, and for the influence of the different properties of the evaporating mixture layer (t_d layer in Fig. 1). This new correlation for the unsteady Nusselt number is under the following form:

$$Nu(t) = 2(1 + 1/\sqrt{\pi t^*}) + (0.4 Re^{1/2}_{\infty} + 0.06 Re^{1/2}_{\infty})$$

$$\times Pr^{0.4} \left( \mu_{\infty}/\mu_{t_d} \right)^{1/4} \left( 1 + \sigma_t \right)^{0.843} \left( c_p_{\infty}/c_p_{t_d} \right)^{0.38}. \quad (8)$$

As explained above, all the terms in Eq. (8) can be found in the correlations addressed by Ref. 44, 47, 52, and 53. Equation (8) will be used later to describe the heat transfer of evaporating airborne contaminated saliva droplets, as well as mass transfer, thanks to the analogy by Chilton and Colburn, accurately. This new transient correlation in Eq. (8) (henceforth labeled as “new theory”) has been validated (see Sec. II C) by comparison to the steady-state correlations of Ranz and Marshall, Richardson, and Whitaker, which have been derived from experimental measurements.

The subscript t_d denotes the property at the vapor film of thickness t_d that depends on the initial concentration of CoV in saliva droplets (see step 2 in Fig. 1). The time t* is made dimensionless by using the diffusion timescale τ_c as

$$t^* = t / \tau_c \quad \text{with} \quad \tau_c = \frac{d_p^2 \rho_d \mu_{t_d}}{4k_{\infty}}. \quad (9)$$

where d_p is the liquid saliva droplet diameter, ρ_d is the droplet initial density, and c_p is the initial heat capacity.

Due to the low temperature values of the surrounding air flow (T < 40°C) and following Prandlt–Blasius–Pohlhausen, one can assume that the mass transfer between the air flow and the contaminated saliva droplet surface occurs within a spherical diffusion film of thickness t_d (Fig. 1),

$$t_d = \frac{d_p}{0.6 Sc^{1/3} Re^{1/2}_{\infty}}. \quad (10)$$

According to Chilton and Colburn, an analogy exists between heat and mass transfer correlations. Therefore, the Nusselt, Nu, and...
Prandtl, Pr, numbers in Eq. (8) can be replaced by the Sherwood and Schmidt numbers, respectively,

\[
Sh(t) = 2(1 + 1/\sqrt{\pi t^*}) + (0.4 \, Re_\infty^{1/2} + 0.06 \, Re_\infty^{2/3}) \\
\times Sc_\infty^{0.4} \left(\mu_\infty/\mu_t\right)^{1/4} \left(1 + 0.843 \left(c_{p_\infty}/c_{p_t}\right)^{0.38}\right) \\
\times \left(0.4 \frac{\mu_\infty}{\mu_t} \left(c_{p_\infty}/c_{p_t}\right)^{1/4} \left(1 + \sigma_{t}^{0.843} t^*\right)^{0.38}\right). \tag{11}
\]

The Sherwood number describes the ratio of convective mass transfer to the diffusive mass transport,

\[
Sh = \frac{h_m}{D/d} \tag{12}
\]

where \(D\) is the mass diffusion coefficient of the evaporating film of thickness \(t_d\) diffused into the airflow and \(h_m\) is the film convective mass transfer coefficient.

The Schmidt number describes the ratio of momentum diffusion to mass diffusion,

\[
Sc_\infty = \frac{\mu_\infty}{\rho_\infty D} \tag{13}
\]

The reduction in the droplet mass \(m_p\), i.e., a reduction in the droplet diameter \(d_p\), is described by the conservation equation

\[
\frac{dm_p}{dt} = -Sh(t) m_p \xi_M, \tag{14}
\]

where \(\tau_p = \rho_p d_p^2/(18 \mu)\) and \(\xi_M\) are the respective saliva droplet relaxation time and the dimensionless potential function driving the evaporation,

\[
\xi_M = \frac{(\rho_S - \rho_\infty)}{\rho_p(C)}, \tag{15}
\]

where \(\rho_\infty\) is the density far away from the droplet and \(\rho_p(C)\) is the effective density of the liquid saliva droplet containing a concentration \(C\) of CoV particles such that \(\rho_p = \rho_{saliva} \cdot (1 - C) + \rho_{CoV} \cdot C\) with \(C = C_0\) at \(t = 0\).

The mass fraction \(Y\) of the vapor film is defined as

\[
Y_S = \frac{\rho_S}{\rho_\infty}; \quad \rho_\infty = \rho_{air}, \tag{16}
\]

where \(\rho_S\) is the density of the vapor at the droplet surface,

\[
\rho_S = \frac{pM}{RT_S}, \tag{17}
\]

where \(M\) is the molar mass of air, \(R\) its universal gas constant, and \(T_S\) is the Eulerian–Lagrangian averaged temperature at the saliva droplet surface,

\[
\tilde{T}_S = \left(\frac{2T_\infty + \tilde{T}_p}{3}\right). \tag{18}
\]
with

$$\bar{T}_p = \frac{\int_{V_p} T_p \, dV_p}{V_p}, \quad (19)$$

where $T_p$ is the local temperature inside the saliva droplet computed at each computational cell and $V_p$ is the volume of the saliva droplet. All of the above are time-dependent. The symbol $\bar{\cdot}$ denotes the averaging operation through a local integration process.

**C. Comparison of old and new theories for the Nusselt number**

The importance of an unsteady correlation [Eq. (8)] compared to the widely used steady-state correlation of Ranz–Marshall\textsuperscript{11,12} [Eq. (6)] is illustrated in Fig. 3. We show that the new theory (labeled NT) has an important effect on the Nusselt number (similarly on the Sherwood number) at larger saliva droplets. For the droplet diameter $d_p$ is about 250 μm and $t < 0.2$ s, the old theory (labeled OT) underestimates the Nusselt number with the relative difference ranging between 10% and 580%. As time passes by, the difference is reduced, e.g., for $d_p = 250$ μm and $t > 0.2$ s, the relative difference is between 1% and 10% [Fig. 3(d)]. For small droplet diameters, e.g., $d_p = 10$ μm [Figs. 3(a) and 3(c)], the NT still has an important effect on the Nusselt number at early times, $t \leq 5 \cdot 10^{-4}$ s. Furthermore, we compare the new transient Nu correlation with the steady-state Nu correlation\textsuperscript{44} [Eq. (7)] for Re = 250 and $d_p = 250$ μm (Fig. 4). The new correlation converges to similar values to Whitaker's

![Fig. 7. Weather impact on virus transmission. Influence of air temperature: [(a)-(e)] RH = 10%; [(f)-(j)] RH = 30%; wind speed: 4 km/h. Wind direction is from left to right.](image-url)
correlation for the steady-state case. As expected, there are important deviations at early time instants. We note two things: (a) any differences between the new and old correlations in the asymptotic limit (steady-state) are not a matter of an error. The old correlations emerged from experimental fitting and are valid only for a range of the Reynolds numbers. For example, the Ranz and Marshall correlation is known to behave well at low Reynolds numbers, while Whitaker’s is known to act better at higher Reynolds numbers. (b) Unsteady heat transfer experiments on evaporation of contaminated saliva droplets do not exist due to the short time and length scales. The results from Figs. 3 and 4 reveal that transient effects must be taken into account in the Nu correlation for accurate prediction of heat and, by analogy, mass transfer by similarity.

III. RESULTS

We have employed the Eulerian–Lagrangian fully-coupled CFD model of Dbouk and Drikakis and implemented the new theoretical transient correlations [Eqs. (8) and (11)] that describe the heat and mass transfer at the microscopic scale of a contaminated saliva droplet. The three-dimensional computational domain comprises a conical injector (30°) of saliva droplets applied at the height

![Weather impact on virus transmission](image)
of 1.7 m mimicking a mouth print. We have chosen a conical injector instead of a detailed mouth print as in the previous studies because the study focuses on the effect of the environmental parameters on saliva droplet cloud dynamics far away from the mouth. The precise form of mouth print plays an essential role only near the mouth.

The boundary conditions are the same as in the work of Dbouk and Drikakis subject to two modifications. Both the wind speed and the droplets injection start at time $t = 0$. The ground temperature is equal to the ambient air. The period of injection is $0.12$ s representing a mild cough. Using the CFD models mentioned above in conjunction with the new theoretical models, we present below the results and analysis of the effects of relative humidity, environmental temperature, and wind on the airborne droplet transmission.

The approach we have followed in investigating the effects of weather conditions follows a similar path as in Dbouk an Drikakis, i.e., we investigate the cloud dynamic and strength of the airborne droplet cloud away from the subject.

Figure 5 shows the quantitative effect of the new theory (correlation) on the evaporation rate. At $t = 3$ s, $RH = 90\%$, $T = 40\,^\circ C$, and $U_{wind} = 4$ km/h, the total number of droplets is overpredicted by the old theory, $T \leq T \leq 20\,^\circ C$, and $U_{wind} = 4$ km/h (Fig. 6). The droplet spectrum is a result of both the new correlation and the contributions from the dynamics of the cloud and droplet/droplet interactions. The crossing of the curves in Fig. 5 is a result of the complex dynamics of the droplet cloud in addition to the evaporation process.

Figures 7 and 8 show the results for a wind speed of 4 km/h and different temperatures and RH. At low RH, $10\%–30\%$, with moderate to low temperatures ($T \leq 30\,^\circ C$), the contaminated droplet cloud travels a distance of 6 m in 5 s. When the temperature increases to $30\,^\circ C$ and $40\,^\circ C$, the droplets evaporate faster and the cloud travels a shorter distance. For example, at $T = 20\,^\circ C$ and $t = 5$ s, comparing Figs. 7(c)–7(h), the increase in RH from $10\%$ to $30\%$ results in an essential reduction of the total number of contaminated saliva droplets. Furthermore, at the same RH $= 30\%$, comparing Figs. 7(g)–7(i), the increase in temperature from $10\,^\circ C$ to $30\,^\circ C$ results at $t = 5$ s in total evaporation of the contaminated saliva droplets.

Figure 8 shows that when the RH increases from lower ($10\%$ and $30\%$) to higher ($50\%$ and $90\%$) values, the droplets become more resistant to evaporation. At high temperature ($30\,^\circ C$) and high RH ($90\%$) [Fig. 8(i)], a significant rise in the total number of contaminated saliva droplets occurs, thus increasing the airborne virus viability. At higher temperatures and RH, the droplet cloud shrinks from an elongated form to a spherical one followed by higher dispersion; see Figs. 8(h) and 8(i) at $t = 5$ s. The above effects could explain the late pandemic acceleration observed in many crowded cities around the middle of July 2020 (e.g., Delhi), where both high temperature and high relative humidity values were recorded one month earlier (during June). The findings should be taken into consideration regarding the possibility of a second pandemic wave in autumn and winter seasons where low temperatures and high wind speeds will increase airborne virus survival and transmission.

We present the strength of the droplet cloud with respect to time in Fig. 9 for RH $= 10\%$. The cloud represents a spanwise view in the eyes of an observer situated 8 m away from the source. At RH $10\%$, the virus viability, which is linked to cloud disappearance, significantly decreases with the increase in temperature, mainly after 1 s of droplet transmission. For low to medium temperature values ($0\,^\circ C$ to $20\,^\circ C$), the cloud disperses as a function of time where vertical elongation occurs, resulting in an elliptic shaped cloud. At high temperature values ($30\,^\circ C$ to $40\,^\circ C$), the cloud disperses more rapidly retaining a spherical-like shape due to a higher evaporation rate that results in the significant cloud evaporation around $t = 3$ s.

To more precisely quantify the weather impact across a range of RH and temperatures, we present the cloud formation at $2$ s (Fig. 10) and $3$ s (Fig. 11). This matrix-like figure sheds light on the combined effect of RH and temperature leading to evaporation. For both simulated times and $U_{wind} = 4$ km/h, the results reveal that the virus viability is reduced at low RH and higher temperatures. Comparing Figs. 10 and 11, we see that at low to medium temperature values ($0\,^\circ C$ to $20\,^\circ C$), the cloud disperses more in the vertical direction. The evaporation is reduced, thus larger droplets remain in the environment and settle more rapidly due to gravity. At higher temperature ($30\,^\circ C$ to $40\,^\circ C$), low to medium RH ($10\%–50\%$) induces a higher evaporation rate, thus a more rapid decrease in the virus viability.

We have also examined the effect of wind speed ($U_{wind} = 10$ km/h, and $U_{wind} = 15$ km/h) in combination with different RH and temperatures (Figs. 12 and 13). We observe an increasing cloud expansion in the spanwise direction with the increase in wind speed. Moreover, at both wind speeds, the cloud retains a spherical-
FIG. 10. Weather effects (temperature and relative humidity) on the transport and evaporation of airborne contaminated respiratory droplets at $U_{\text{wind}} = 4$ km/h. Plane view at $t = 2$ s from an observer located 8 m away from the source in the wind direction.

FIG. 11. Weather effects (temperature and relative humidity) on the transport and evaporation of airborne contaminated respiratory droplets at $U_{\text{wind}} = 4$ km/h. Plane view at $t = 3$ s from an observer located 8 m away from the source in the wind direction.

FIG. 12. Weather effects (temperature and relative humidity) on the transport and evaporation of airborne contaminated respiratory droplets at $U_{\text{wind}} = 10$ km/h. Plane view at $t = 2$ s from an observer located 8 m away from the source in the direction of the wind.

FIG. 13. Weather effects (temperature and relative humidity) on the transport and evaporation of airborne contaminated respiratory droplets at $U_{\text{wind}} = 15$ km/h. Plane view at $t = 2$ s from an observer located 8 m away from the source in the direction of the wind.
like shape at both $t = 2 \text{ s}$ and $t = 3 \text{ s}$ for all temperature and relative humidity values with increasing evaporation rate at low RH and high temperature. The above finding reinforces the recommendations that social distancing becomes important both in the streamwise (wind direction) and spanwise direction. Moreover, the present results could be used to set future prevention measurements in both indoor and outdoor environments to reduce airborne virus transmission by controlling the temperature, RH, and space ventilation rate.

The droplet number, $N$, compared to its initial value of $N_0(t = 0) = 1151$ decreases at different rates due to evaporation (Fig. 14). At RH 90%, the droplet number reduces only when the temperature is at $40^\circ \text{C}$, while it remains intact for temperatures up to almost $40^\circ \text{C}$, with only a small reduction observed after $4.5 \text{ s}$ at $30^\circ \text{C}$. The droplet reduction becomes more significant at lower RH. For RH 50%, the reduction occurs for temperatures higher than $30^\circ \text{C}$. For RH 30%, the temperature starts affecting the droplets after $3.5 \text{ s}$, with the droplet reduction still occurring at $30^\circ \text{C}$ and $40^\circ \text{C}$. At the lowest RH of 10% considered here, we start seeing significant effects of temperature on droplet reduction at $20^\circ \text{C}$ and above.

**IV. CONCLUSIONS**

We have developed new theoretical correlations for the Nusselt and Sherwood number and implemented their mathematical formulas in an Eulerian–Lagrangian multiphase CFD solver. These new correlations take into account the properties of the virus inside the saliva droplet, as well as the transient effects on heat and mass transfer.

We show that the steady-state theory leads to incorrect values of $Nu$ and $Sh$ numbers with the relative difference increasing as a function of the Reynolds number defined at the droplet scale [Eq. (1)]. The above means that the relative difference increases considerably with increasing wind speed or droplet diameter. As an example, we showed that at $Re = 250$, the relative difference could increase up to 600% at the instant of droplet-air impact with its time value being an increasing function of the droplet diameter. Therefore, the predictions of evaporation and virus concentration in saliva droplets are significantly underestimated if applying the widely used Ranz and Marshall correlation that is intended for heat and mass transfer of a single-material sphere at the steady-state. The latter correlation

![Figure 14](image-url)
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DATA AVAILABILITY

The data that support the findings of this study are available on request from the authors.

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