5-Aminolevulinic acid (5-ALA) is generally known as an essential precursor molecule for tetrapyrrole synthesis such as porphyrin, heme, chlorophyll and vitamin B12.\(^1\) It has been widely applied in localizing and photodynamic therapy for various cancers.\(^2\)–\(^4\) It has also been used as a selective biodegradable insecticide, herbicide, salt tolerance agent or plant growth regulator in agricultural fields.\(^5\)

To date, 5-ALA was mainly synthesized by microbial production methods,\(^6\) but the long-time and high-cost course restrict its scaled applications. On the other side, chemical routes using 2-hydroxypropyridine, tetrahydrofurfurylamine and furfurylamine as starting materials involved in numerous bottleneck including toxic intermediates and rigorous reaction conditions.\(^7\)–\(^9\) Thus, to develop a new pathway for 5-ALA production is of great significance, especially one that is a green and sustainable.

Biomass is an appealing starting material in value-added chemicals synthesis because of its advantages of renewability, sustainability and availability.\(^9\) Several biomass-derived platform compounds such as 5-hydroxymethylfurfural (HMF), 5-chloromethylfurfural (CMF), levulinic acid (LA) or its esters have been reported as efficient raw materials in the production of 5-ALA.\(^10\),\(^11\) However, the industrial manufacture of furan-type HMF and CMF cannot currently be achieved easily due to the high production and environment costs.\(^12\),\(^13\) Furthermore, conversion of furan-type chemicals to 5-ALA also suffers the economic problems concerning the use of expensive oxidants in the ring-opening stage. Unlike CMF and HMF, LA and its esters can be easily produced both from hemicellulose and cellulose, and its yearly tonnage is therefore available via the acidic processing of biomass at a competitively low price.\(^14\)–\(^16\) Thus, to synthesize 5-ALA from LA or its esters is exceptionally promising. Typically, 5-ALA can be effectively prepared from levulinate via a three-stage process including bromination, ammoniation and acidolysis.\(^17\) However, the bromination of levulinate with Br\(_2\) in this course has low selectivity to 5-bromo derivatives. Besides, Br\(_2\) is hazardous and environmentally unfriendly. Hence, a crucial step of the production of 5-ALA from levulinate is to explore a safe bromide agent with higher selectivity and activity.

CuBr\(_2\), a green and low toxic brominated reagent, was usually used for the synthesis of \(\alpha\)-bromination of cyclopentenone derivatives and its closest analogues-indanone of carbonyl compounds for its advantages of short reaction times, high selectivity of the products, high yields and easily handle procedures.\(^18\),\(^19\) In this content, various unsymmetrical aliphatic ketones including levulinic acid, methyl levulinate, ethyl levulinate, 5-hydroxy-2-pentanone and 2-butanone was attempted for bromizing with CuBr\(_2\) (Table 1). Interestingly, the yields of bromination products were different, depending on the source of aliphatic ketones.

In this work, we present the synthesis of 5-ALA from biomass derived methyl levulinate (ML) under mild conditions using CuBr\(_2\) as a greener bromine donor, and a high yield of 5-bromolevulinate (MSB) up to 85% was achieved. Furthermore, a detailed discussion of ammoniation and acidolysis was also presented, corresponding a high total 5-ALA yield over 64% (Scheme 1).

The first attempt to screen the reaction conditions for the bromination of ML with CuBr\(_2\) are shown in Table 2. An encouraging yield of the desired product (50%) is indeed obtained using CuBr\(_2\) as bromide agent in CH\(_3\)OH at 40 °C for 3 h (Table 2, entry 1). The investigation of the solvent indicated that CH\(_3\)OH–CHCl\(_3\), mixed solvent was superior to ethyl acetate (EA), CHCl\(_3\), CH\(_3\)OH, CH\(_2\)OH–EA and EA–CHCl\(_3\) (Table 2, entry 2–6). The results may due to the fact that CH\(_3\)OH can improve the selectivity of MSB and haloalkanes are favourable to
Based on the above, changing the volume ratio of CH$_3$OH to CHCl$_3$ (Table 2, entry 6–10), improved the yield of M5B to 80% (Table 2, entry 6). We then proceeded to evaluate various metal bromides, including ZnBr$_2$, MgBr$_2$, and AlBr$_3$ under the identical conditions. However, no conversion was detected even after 24 h (Table 2, entry 11–13). These metal bromides were also found to be inactive in bromination as noted in previous studies.$^{22,23}$ The conventional bromination agent such as Br$_2$, 2C$_4$H$_9$NOHBr·Br$_2$ and NBS can obviously improve the reaction (Table 2, entry 14–17), although they were lower than that achieved with CuBr$_2$ (Table 2, entry 6). Experiments that screened for the bromine donors suggested that CuBr$_2$ was the most effective for the bromination of ML (Table 2, entry 6). Note that a detailed study of the reaction conditions were discussed (Tables S1, S2 and Fig. S1†), and a high M5B yield over 85% was obtained at 40 °C for 5 h (detected by GC-MS, Fig. S3†).

As shown in Fig. 1, XRD patterns indicated that CuBr$_2$ was transformed into CuBr (PDF#06-0292) after the reaction. When TEMPO and 2,6-di-tert-butyl-4-methylphenol (BHT) were introduced to eliminate free radical, no M5B was detected. Based on these results, a mechanism for the current bromination process was proposed, as shown in Scheme 2. Initially, Lewis acidity of CuBr$_2$ promoted the transformation from carbonyl keto to copper-bound enolate at the α-position.$^{24}$ Subsequently, the hemolysis of enolate to get ethenyloxy radical, and the reactive group reacts with CuBr$_2$ to generate an M5B along with an equivalent of CuBr.

Intensive efforts have been devoted to introduce the key amino group on M5B.$^{17,25–27}$ Among them, a typical Gabriel reaction using potassium phthalimide (KPI) as ammonia resource has a promising commercial availability, however, only a moderate M5P yield of 59% was achieved at 110 °C for 12 h.$^{27}$ In this work, optimizing the experimental conditions of Gabriel reaction including reaction time, temperature, the amount of solvent and the molar ratio of KPI to M5B (Tables S3 and S4†) was subsequently conducted, and a maximum M5P yield of 88% was obtained at 40 °C for only 4 h (detected by GC-MS, Fig. S4†). This significant improvement is no doubt accelerate the practical application of 5-ALA. Finally, an acid hydrolysis process was applied with 6 M HCl (Fig. S2†). The obtained products were concentrated in vacuum at 40 °C to avoid the polymerization of 5-ALA at high temperatures,$^{13}$ affording a satisfied 5-ALA yield of 85% (Fig. S11 and 12†) (determined by HPLC, Fig. S5†).

In summary, we have developed a new efficient bromination method for the conversion of biomass derived ML to 5-ALA.

### Table 1: The bromination of aliphatic ketones with CuBr$_2$.$^a$

| Entry | Bromine source | Solvent | M5B yield (%) |
|-------|----------------|---------|---------------|
| 1     | CuBr$_2$      | CH$_3$OH| 50            |
| 2     | CuBr$_2$      | CHCl$_3$| 7             |
| 3     | CuBr$_2$      | EA      | 13            |
| 4     | CuBr$_2$      | CH$_3$OH/EA (1 : 1) | 32         |
| 5     | CuBr$_2$      | CHCl$_3$/EA (1 : 1) | 14         |
| 6     | CuBr$_2$      | CH$_3$OH/CHCl$_3$ (1 : 1) | 80         |
| 7     | CuBr$_2$      | CH$_3$OH/CHCl$_3$ (1 : 4) | 56         |
| 8     | CuBr$_2$      | CH$_3$OH/CHCl$_3$ (1 : 3) | 75         |
| 9     | CuBr$_2$      | CH$_3$OH/CHCl$_3$ (1 : 5) | 74         |
| 10    | CuBr$_2$      | CH$_3$OH/CHCl$_3$ (1 : 4) | 66         |
| 11$^b$| ZnBr$_2$      | CH$_3$OH/CHCl$_3$ (1 : 1) | 0          |
| 12$^b$| MgBr$_2$      | CH$_3$OH/CHCl$_3$ (1 : 1) | 0          |
| 13$^b$| AlBr$_3$      | CH$_3$OH/CHCl$_3$ (1 : 1) | 0          |
| 14    | Br$_2$        | CH$_3$OH/CHCl$_3$ (1 : 1) | 55         |
| 15    | 2C$_4$H$_9$NOHBr·Br$_2$ | CH$_3$OH/CHCl$_3$ (1 : 1) | 40         |
| 16    | NBS + BPO     | CH$_3$OH/CHCl$_3$ (1 : 1) | 28         |
| 17    | NBS + AIBN    | CH$_3$OH/CHCl$_3$ (1 : 1) | 18         |

$^a$ Reaction condition: compounds = 2.5 mmol, CuBr$_2$ = 1.67 g, solvent = 30 mL, temperature = 40 °C, time = 4 h.

### Table 2: The bromination of ML to M5B.$^a$

| Entry | Bromine source | Solvent | M5B yield (%) |
|-------|----------------|---------|---------------|
| 1     | CuBr$_2$      | CH$_3$OH| 50            |
| 2     | CuBr$_2$      | CHCl$_3$| 7             |
| 3     | CuBr$_2$      | EA      | 13            |
| 4     | CuBr$_2$      | CH$_3$OH/EA (1 : 1) | 32         |
| 5     | CuBr$_2$      | CHCl$_3$/EA (1 : 1) | 14         |
| 6     | CuBr$_2$      | CH$_3$OH/CHCl$_3$ (1 : 1) | 80         |
| 7     | CuBr$_2$      | CH$_3$OH/CHCl$_3$ (1 : 4) | 56         |
| 8     | CuBr$_2$      | CH$_3$OH/CHCl$_3$ (1 : 3) | 75         |
| 9     | CuBr$_2$      | CH$_3$OH/CHCl$_3$ (1 : 5) | 74         |
| 10    | CuBr$_2$      | CH$_3$OH/CHCl$_3$ (1 : 4) | 66         |
| 11$^b$| ZnBr$_2$      | CH$_3$OH/CHCl$_3$ (1 : 1) | 0          |
| 12$^b$| MgBr$_2$      | CH$_3$OH/CHCl$_3$ (1 : 1) | 0          |
| 13$^b$| AlBr$_3$      | CH$_3$OH/CHCl$_3$ (1 : 1) | 0          |
| 14    | Br$_2$        | CH$_3$OH/CHCl$_3$ (1 : 1) | 55         |
| 15    | 2C$_4$H$_9$NOHBr·Br$_2$ | CH$_3$OH/CHCl$_3$ (1 : 1) | 40         |
| 16    | NBS + BPO     | CH$_3$OH/CHCl$_3$ (1 : 1) | 28         |
| 17    | NBS + AIBN    | CH$_3$OH/CHCl$_3$ (1 : 1) | 18         |

$^a$ Reaction condition: ML = 0.33 g, bromine source = 3 mole of ML, solvent = 30 mL, temperature = 40 °C, time = 3 h. $^b$ Time = 24 h.
a key chemical that has been widely applied in medical and agricultural areas. CuBr₂ was applied as both catalyst and bromine atom donor and was demonstrated to be of higher selectivity and activity than the conventional hazardous Br₂ in ML bromination. Each stage proceeds in high (~85%) yield and affords 5-ALA in 95% purity, giving a process that could be commercially viable.

Conflicts of interest
There are no conflicts to declare.

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