Laboratory evaluation to assess the effectiveness of inhibitive nano-water-based drilling fluids for Zubair shale formation

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Abstract
While drilling through shale formations, shale hydration, including shale swelling and dispersion, is frequently reported as the main wellbore instability problems, particularly when conventional drilling fluids (water-based) are used. These problems have many adverse effects on the drilling operations resulting in non-productive time. Nanoparticles have been recently introduced as a unique alternative to improve the performance of water-based drilling fluids for shale applications. This paper presents an experimental evaluation to investigate the effectiveness of an inhibitive nano-water-based drilling fluid in reducing the swelling of Zubair shale formation. Well-preserved core samples, which were retrieved from Zubair formation, were characterized using X-ray diffraction, and X-ray fluorescences to quantify the amount of the swelling minerals. Scanning electron microscopy was used to identify the existence of microfractures within the samples. Three different nano-based drilling fluids containing titanium dioxide (TiO2), copper oxide (CuO), and magnesium oxide (MgO) at two different concentrations (0.5% and 1.5% by vol) were evaluated through a set of tests to assess the shale reactivity in the presence of these nano-based fluids. In addition, the effect of these nanoparticles on the rheological and filtration properties was studied. The results showed that the shale samples contain 41.26% silicon dioxide (SiO2) and 22.73% aluminum oxide (Al2O3), indicating the presence of smectite and illite. Based on the reactivity tests, fluids containing CuO at 1.5% by vol outperformed the other fluids in terms of reducing the reactivity, where the expansion rate was reduced by 82.7% compared to the reference sample submerged in fresh water. In addition, the addition of nanoparticles resulted in reducing the plastic viscosity, increasing both the yield point and gel strength, and reducing the fluid loss under low-pressure low-temperature conditions.

Keywords Inhibitive drilling fluid · Nanofluid · Nanoparticles · Shale reactivity · Laboratory investigation

Introduction
Drilling through shale formations is considered as one of the major challenges worldwide due to the wellbore instability related issues. The Zubair formation in Southern Iraq consists of almost 55% shale, which results in approximately 70% of wellbore instabilities while drilling due to the ineffectiveness of the added inhibitors in reducing the shale reactivity (Abbas et al. 2018a). These instabilities, which include shale swelling, wellbore collapse, pipe sticking, etc., could result in unwanted non-productive time (NPT) that increases the overall drilling cost. The chemical interaction between drilling fluids and shale is one of the factors that could lead to these instabilities (Horsrud et al. 1998; Carminati et al. 2001; Balaban et al. 2015); hence, proper selection and evaluation of the shale inhibitors used in drilling fluid play a major role in mitigating this type of instability due to the chemical and physical complexity of the shale (Van Oort 2003). Understanding the characteristics of the shale such as the mineralogy, structure, and reactivity is crucial for the selection of shale inhibitors.

Oil-based drilling fluids (OBM), including synthetic-based drilling fluids (SBM), are often used to drill through shale section due to their effectiveness in inhibition as a result of the lesser amount of water in their formulation.
However, OBM is not considered environmentally friendly fluid; therefore, water-based drilling fluids (WBM) are often preferred. Different types of salts including sodium chloride (NaCl), potassium chloride (KCl), and calcium chloride (CaCl₂) are often used as shale inhibitors. The usage of salts as inhibitors is due to the fact that increasing the concentration of salts in the WBM will result in reducing the ionic exchange process between the shale and water, hence lesser magnitude of shale hydration (Doleuschall et al. 1987).

In a recent investigation, Abbas et al. 2018b conducted an experimental investigation to assess the effectiveness of NaCl, KCl, and a mixture of KCl and glycol in reducing the reactivity of the Zubair shale. Different tests were conducted to characterize the shale samples first including thin-section analysis, X-ray diffraction analysis (XRD), and scanning electron microscopy (SEM), and then the selected fluids were evaluated using cation exchange capacity (CEC), hot rolling dispersion test, capillary suction time test (CST), and linear swell meter test (LSM). The results showed that the mixture of 7% KCl and 3% glycol outperformed both the 7% by wt. KCl brine and the 20% by wt. NaCl brine and resulted in a reduction of the swelling rate by approximately 66%.

Nanofluids, which can be simply defined as fluids containing suspended nano-meter sized particles with sizes ranging between 1 and 100 nm, have recently proven their effectiveness for different applications in the oil and gas industry. These applications include improving the rheological properties of drilling fluids (Barry et al. 2015; Ponmani et al. 2016; Al-Zubaidi et al. 2017; Perween et al. 2018; Parizad et al. 2018; Minakov et al. 2018, Alsaba et al. 2018), wellbore strengthening (Nwaioji et al. 2013; Contreras et al. 2014a, b; Kang et al. 2016), cementing (Ahmed et al. 2018; Alkhamis and Imqam 2018; Vipulanandan et al. 2018), stimulation (Singh et al. 2018; Fakoya and Shah 2018), shale stabilization (Sensoy et al. 2009; Akhtarmanesh et al. 2013; Hoxha et al. 2017; Pourkhail and Nakhae 2019), and enhanced oil recovery (EOR) (Zargartalebi et al. 2014; Abdullahi et al. 2019; Ding et al. 2018; Suresh et al. 2018; Elshawaf 2018; Almohsin et al. 2018).

In this study, different techniques were used to first characterize the retrieved shale samples in order to quantify the amount of swelling minerals and examine the existence of fractures within the samples. In addition, different shale reactivity tests were conducted to evaluate the effectiveness of nanoparticles in reducing the reactivity of the shale samples using nano-water-based drilling fluid (NWBM). The main objective of this study is to determine the best nanoparticle type and concentration in terms of reducing the shale reactivity, which suggests its applicability in being used as an inhibitive for water-based drilling fluids.

### Methodology

#### Shale characterization

Different tests were conducted in this study on well-preserved shale core samples, which were collected from different wells to cover a wide range of the Zubair formation intervals. These tests included X-ray computed tomography (CT), scanning electron microscopy (SEM), X-ray diffraction (XRD), and X-ray fluorescence (XRF). The main objective of running these tests is to characterize the samples in terms of the structure, mineral composition, and the existence of fractures. A detailed description of the above-mentioned tests can be found elsewhere (Abbas et al. 2018b).

#### Fluid used

Three different fluids containing nanoparticles at two different concentrations were prepared and used in this study in addition to fresh water as a reference point to evaluate the effect of adding nanoparticles on the shale reactivity. While a simple 7% bentonite drilling fluid was used as the reference point for evaluating effect of nanoparticles on the rheological properties and filtration characteristics. The nanoparticles evaluated included titanium dioxide (TiO₂), copper oxide (CuO), and magnesium oxide (MgO) at two different concentrations (0.5% and 1.5% by vol), where the 0.5% was considered as low concentration and the 1.5% as a very high concentration of nanoparticles. The composition of the tested fluids is summarized in Table 1.

#### Shale reactivity

To evaluate the effect of nanoparticles on the shale reactivity, different tests were conducted in this study. These tests included the cation exchange capacity (CEC), expansion rate (semiquantitative), and a qualitative hardness test. The

| Fluid type | Bentonite (g) | Water (ml) | CuO (g) | TiO₂ (g) | MgO (g) |
|------------|---------------|------------|---------|----------|---------|
| 7% bentonite | 35 | 465 | – | – | – |
| 0.5% CuO | 35 | 465 | 2.5 | – | – |
| 1.5% CuO | 35 | 465 | 7.5 | – | – |
| 0.5% TiO₂ | 35 | 465 | – | 2.5 | – |
| 1.5% TiO₂ | 35 | 465 | – | 7.5 | – |
| 0.5% MgO | 35 | 465 | – | x | 2.5 |
| 1.5% MgO | 35 | 465 | x | x | 7.5 |
CEC test was conducted according to the API-RP-13I (API 2004).

The expansion rate test was conducted by measuring the weight of the dry sample first and then submerging the shale sample in a container containing the test fluid and leaving it for 24 h. After 24 h, the wet sample weight is then measured and recorded and the percentage of the expansion rate is then calculated as follows:

\[
\% \text{ Expansion rate} = \frac{\text{Wet sample weight} - \text{Dry sample weight}}{\text{Dry weight}} \times 100
\] (1)

This test is semiquantitative since it will give an indication of how much water is being absorbed when comparing the wet to dry sample weight. If the fluid used is inhibitive, then the amount of water absorbed will decrease, resulting in reducing the expansion rate. The results obtained from this test are compared to a reference sample, which contains fresh water only.

The qualitative hardness tests were conducted using an in-house-made simple apparatus (Fig. 1), which was used to measure the required force to break the core sample after being exposed to the different fluids. This test can also give a qualitative indication on the shale reactivity due to the fact that the shale samples will become softer due to swelling. The shale samples were exposed to forces ranging between 5 and 25 Nm using a torque wrench which is connected to a piston that is placed on the top of shale samples to compress them. The force is applied until the sample breaks, and the amount of force required to break the sample is recorded.

**Results and discussion**

**Shale characterization**

The CT scan images for the full core section demonstrated the presence of microfractures as can be seen in Fig. 2, where the green and yellow arrows point to the induced fracture and natural open fractures, respectively.

![CT scan images for full core (1 m). (after Abbas et al. 2018b)](image)
The SEM images (Fig. 3) indicate the presence of microfractures. Overall, the core samples exhibited microfractures ranging between 0.4 and 3 μm (400–3000 nm).

The mineral composition of the shale sample obtained from XRF analysis is tabulated in Table 2, which shows that the sample consists mainly of 41.26% silicon dioxide (SiO$_2$) and 22.73% aluminum oxide (Al$_2$O$_3$), indicating the presence of smectite and illite, where the smectite has higher tendency to swelling when in contact with water (Aghamelu and Okogbue 2015).

Figure 4 shows the obtained results from the XRD analysis along with the list of phases within the sample, which indicates the nature and identification of the individual phases within the shale sample. However, the identification of these phases depends on the crystalline nature of the core and can be distinguished by using the 2Θ values from Brag’s equation. The amorphous material is not expected to be identified with the XRD even if it is partially crystalized. Details about the different shale sample phases are tabulated in Table 3.

**Table 2** XRF analysis results

| Element | Formula | Concentration |
|---------|---------|---------------|
| Na      | Na$_2$O | 0.512%        |
| Mg      | MgO     | 1.485%        |
| Al      | Al$_2$O$_3$ | 22.73%    |
| Si      | SiO$_2$ | 41.256%       |
| S       | SO$_3$  | 1.191%        |
| K       | K$_2$O  | 2.27%         |
| Ca      | CaO     | 3.712%        |
| Ti      | Ti      | 0.859%        |
| Fe      | Fe$_2$O$_3$ | 8.353%   |
| Rb      | Rb      | 92.3 ppm      |
| Sr      | Sr      | 233.2 ppm     |
| Zr      | Zr      | 394.8 ppm     |

The SEM images (Fig. 3) indicate the presence of microfractures. Overall, the core samples exhibited microfractures ranging between 0.4 and 3 μm (400–3000 nm).
Table 3  Tabulated XRD results

| Ref. code   | Compound name  | Chemical formula |
|-------------|----------------|------------------|
| 01-083-2465 | Quartz low     | SiO₂             |
| 00-024-0076 | Pyrite         | Fe₂S₃            |
| 00-006-0221 | Kaolinite      | Al₂Si₂O₅(OH)₄    |
| 01-089-1305 | Calcite, magnesite | (Mg₀.₀₆Ca₀.₉₄) (CO₃) |
| 00-007-0330 | Illite–smectite | K–Al₄(SiAl)₈O₂₀(OH)₄ × H₂O |
| 01-078-2486 | Anatase        | TiO₂             |

Table 4  The result of CEC test

| Fluid type | NP concentration% | Amount of methylene blue used (ml) | CEC | Reactive clay content (lb/bbl) |
|------------|-------------------|-----------------------------------|-----|-------------------------------|
| Water      | –                 | 0.5                               | 0.5 | 2.5                           |
| CuO        | 0.5               | 0.4                               | 0.4 | 2                             |
| CuO        | 1.5               | 0.2                               | 0.2 | 1                             |
| TiO₂       | 0.5               | 0.5                               | 0.5 | 2                             |
| TiO₂       | 1.5               | 0.4                               | 0.4 | 2.5                           |
| MgO        | 0.5               | 0.5                               | 0.5 | 2                             |
| MgO        | 1.5               | 0.4                               | 0.4 | 2.5                           |

Shale reactivity

Cation exchange capacity (CEC)

Table 4 summarizes the results obtained for the cation exchange capacity test (CEC) conducted after exposing the shale samples to the above-mentioned fluids.

Based on the results, it can be seen that the CuO at 1.5% by vol concentration resulted in reducing the amount of reactive clay by 60% compared to the reference point. This is an indication that the CuO has severely reduced the reactivity of the clay content of the shale when compared to the other fluids. On the one hand, CuO, MgO, and TiO₂ at low concentration (0.5% by vol) showed a reduction of approximately 20% compared to the reference point; however, when the concentration was increased using MgO and TiO₂, no effect in reducing the reactivity was observed. It is important to mention that this analysis is qualitative due to the uncertainties with respect to the endpoint of the test. Figure 5 shows graphically the obtained results of the reactive clay content.

Expansion rate

The results of this simple approach showed the expansion rate of the shale sample, as a function of weight increase, using different types of nano-based fluids with two different concentrations (0.5% and 1.5%) in order to assess the effect of the nanoparticles on reducing the absorption of water by the shale sample. Table 5 shows the results of all the tests conducted.

The results clearly demonstrate the effect of nanoparticles on reducing the amount of water absorbed by the shale samples (Fig. 6). Based on the results, it can be clearly observed that the CuO at 1.5% by vol concentration outperformed all the nanoparticles at high and low
concentrations compared to the reference point, which contains fresh water only, with a reduction in the % increase in weight by approximately 83%. The TiO₂ also exhibited a lower % of increase in the sample weight at a concentration of 0.5% by vol suggesting a reduction by 54% compared to the fresh water. However, the MgO at 0.5% by vol showed a negative effect where the % has increased by approximately 6%. The obtained results from this test are in agreement with the finding from the reactive clay content test.

**Qualitative hardness test**

Previous studies have shown that swelling will affect the shale strength (Lal 1999; Shi et al. 2018; Beg et al. 2018). It is believed that the more adsorption of the water by the shale, the weaker the sample it gets. The qualitative hardness test results shown in Table 6 have confirmed the previous tests result. The results clearly show that the sample exposed to fresh water was the weakest sample, where it was partially broken at 9 Nm compared to all other samples, while the sample exposed to 1.5% by vol CuO didn’t break at the maximum applied force, which is in agreement with the previous tests. The sample exposed to 0.5% by vol CuO broke at the minimum force applied, which is believed to be due to an experimental error while conducting the test, and thus this result is not representative.

**SEM/EDX images**

Based on the obtained results from the different tests above, the sample containing CuO at 1.5% by vol showed the best performance in terms of reducing the shale reactivity; therefore, it was decided to take a closer look at the shale sample using the scanning electron microscopy/energy-dispersive X-ray spectroscopy (SEM/EDS) in order to observe the shale sample surface before and after being exposed to the nanofluid.

Figure 7 shows SEM images, which were taken prior to submerging the shale samples into the select fluid. Figure 8 shows the same sample after being exposed to the fluid containing CuO at 1.5% by vol which clearly shows the presence of the nanoparticles (lighter color) on the sample surface.

Figure 9 shows the EDS images of the sample (a) before and (b) after being exposed to the selected nanofluid in order to clearly observe how the CuO nanoparticles were covering

| Sample | Concentration | Force applied |
|--------|---------------|---------------|
|        |               | 5 Nm | 9 Nm | 13 Nm | 21 Nm | 25 Nm |
| Water  | –             | No   | Partially | Broken | –   | –   |
| CuO    | 0.5           | Broken | –   | –   | –   | –   |
| CuO    | 1.5           | No   | No   | No   | No   | No   |
| TiO₂   | 0.5           | No   | No   | No   | Broken | –   |
| TiO₂   | 1.5           | No   | No   | No   | No   | Broken |
| MgO    | 0.5           | No   | No   | Broken | –   | –   |
| MgO    | 1.5           | No   | No   | No   | Broken | –   |

![Fig. 7 SEM image of the shale sample before exposor to fluid](image-url)
the presence of SiO₂. It can be clearly seen in terms of color contrast between the two images that the Cu covered the presence of Si, which can explain the reduction in the shale reactivity. This is believed to be due to plugging the pore spaces as found previously by Hoxha et al. 2017, which resulted in reducing the water invasion into the shale and hence reducing the reactivity of the shale.

**Effect of nanoparticles on the rheological properties and filtration characteristics**

A summary of results for the tests conducted to evaluate the effect of nanoparticles on the rheological and filtration characteristics is summarized in Table 7.

Overall, it can be clearly observed that the added nanoparticles resulted in affecting the rheological properties in a favorable way. On the one hand, the plastic viscosity was reduced for all the blends except for the nanofluids containing TiO₂; on the other hand, both yield point and 10 s gel strength increased for all blends containing nanoparticles. The nanoparticles showed a minor effect on the pH as shown in Table 7. For the filtration characteristics, a reduction in the fluid loss was observed for both blends containing TiO₂ and CuO. However, for blends containing MgO, a negative effect was observed on the filtration characteristics, where the fluid loss increased dramatically compared to the reference point (7% bentonite).
Figure 10 shows a comparison for all nanofluids used along with the % increase/reduction in plastic viscosity, yield point (Fig. 10a), and fluid loss (Fig. 10b), when compared to the reference drilling fluid (7% Bentonite).

It can be clearly observed that the reduction in plastic viscosity ranged between 25 and 50% for blends containing CuO and MgO (Fig. 10a), while the increase was reflected for TiO2. The yield point % increases ranged between 40 and 200%, where the highest increase was observed when adding MgO nanoparticles. The highest reduction in fluid loss was achieved when adding TiO2, which was up to 24%. However, a negative increase in the fluid loss value up to 116% was observed when using MgO. The effect of increasing the concentration of nanoparticles on the magnitude of enhancement was not significant, suggesting that lower concentrations of nanoparticles are preferred.

### Table 7 Summary of the test results

| Blends# | Ø6 RPM | Ø3 RPM | Gel (lb/100ft³) | PV (cP) | YP (lb/100ft³) | pH | Fluid loss (ml/30 ml) | Filter cake thickness (in.) |
|---------|--------|--------|-----------------|--------|----------------|----|---------------------|--------------------------|
| 7% Bentonite | 20     | 20     | 21              | 4      | 19             | 9.26 | 25                  | 0.083                    |
| 0.5% CuO  | 35     | 35     | 33              | 2      | 35             | 9.2  | 22                  | 0.085                    |
| 1.5% CuO  | 37     | 37     | 37              | 2      | 37             | 9.17 | 22.5                | 0.1                      |
| 0.5% TiO2 | 23     | 20     | 32              | 5      | 27             | 8.7  | 19                  | 0.13                     |
| 1.5% TiO2 | 32     | 29     | 35              | 7      | 35             | 8.9  | 19.5                | 0.13                     |
| 0.5% MgO  | 48     | 38     | 35              | 3      | 63             | 10.7 | 45                  | 0.18                     |
| 1.5% MgO  | 51     | 43     | 34              | 2      | 62             | 10.7 | 54                  | 0.18                     |

![Fig. 10](image_url) Effect of nanoparticles on (a) plastic viscosity and yield point, and (b) fluid loss

### Conclusions

The laboratory evaluation presented in this paper demonstrated clearly the effectiveness of different nanoparticles on the shale reactivity as well as the rheological and filtration properties of the drilling fluid. Based on the results and analysis conducted, the following can be concluded:

- The mineral characterization of the shale samples using XRD and XRF showed that this type of shale consists of 41.256% of SiO2 and 22.73% of Al2O3, which indicates the presence of smectite and illite.
- The SEM images showed an average microfracture width of 437.5 nm.
- Based on the different reactivity tests conducted, fluids containing CuO nanoparticles at 1.5% concentration by vol resulted in the best inhibition.
- The addition of CuO at 1.5% by vol resulted in reducing the water absorption by approximately 83% compared...
to the reference point, while the addition of TiO$_2$ at 0.5% by vol resulted in a reduction up to 54%.

- The exposure of the shale samples to the fluid containing CuO at 1.5% by vol resulted in reducing the amount of reactive clay by 60%.

- The SEM/EDS analysis of the shale samples before and after being exposed to the fluid containing CuO at 1.5% by vol showed clearly how the Cu covered the presence of Si, which is in agreement with the reactivity test results.

- Based on the results, both TiO$_2$ and CuO can be considered as good inhibitors that have the capability of minimizing the shale reactivity.

- Based on the effect of nanoparticles on both rheological and filtration properties, both TiO$_2$ and CuO did not negatively affect the drilling fluid, where a reduction in the fluid loss by 12% and 24% was observed for both CuO and TiO$_2$ at low concentration (0.5% by vol), respectively.

- In addition, an acceptable increase in the yield point (up to 95%) was achieved for both CuO and TiO$_2$ at low concentration (0.5% by vol).

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