A Perspective Review on Methodologies for Treating Sugar Industry Effluents

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Abstract
Due to high pollution load, sugar industry is considered as one of the topmost pollutions generating industries affecting our environment. Wastewater from sugar industry bears intricate properties and its treatment is considered as one of the challenging tasks for environmental engineers in terms of its treatment as well as reutilization. The brown color, high temperature, low pH, high COD, high BOD, TDS, odor problems and excessive percentage of dissolved organics and inorganics hallmark the sugar industrial effluent. This effluent if discharged untreated, poses problems for both marine and terrestrial ecosystems. The cost effective and economical treatment of sugar industrial waste is a challenging task. Therefore, implication of appropriate and cost-effective method to meet the discharge standards is the utterly required need of time. This study gives a brief and concise overview of various techniques employed for treating sugar industrial effluents.

Keywords: Sugar industry; Environment pollution; Adsorption; Biological methods; Electro-oxidation, Thermolysis

Abbreviation: AFR: Anaerobic Fixed Bed Reactor; BOD: Biological Oxygen Demand; BSI: British Standard Institutes; BP: British Plastic; COD: Chemical Oxygen Demand

Introduction
Regardless of the entire water accessibility, only 3% of fresh water is accessible on earth [1]. Due to extensive industrialization and urbanization, serious opposing challenges in collection, treatment and disposal of industrial effluents have been observed. Unfortunately, due to deficiency of knowledge, financial support and sometimes reluctance to employ wastewater treatment methods, most of the industries discharge their wastes without adopting requisite treatment strategies. These not only cause health problems but also contaminate freshwater resources [2]. Untreated waste elements from industrial sector, agriculture area and municipalities deteriorate the environment segments causing pollution of air, water, land and soil. Above 700 contaminants, both organic and inorganic have been reported in water followed by microbial and industrial activities [3]. Many pollutants among these are hazardous due to their toxicity and carcinogenic nature [4]. This situation is leading to severe health problems and environmental deprivation. In this regard, water conservation policies are ear mark in preservation of freshwater bodies as well as in maintaining water quality standards [5]. World Bank executed stringent rules and protocols to protect the environment from potential hazards caused by industrial discharge. Various parameters describing the quality of water elucidated given by the World Bank is summarized in Table 1.

| Parameter                  | Max. Value (mg/L) |
|---------------------------|-------------------|
| pH value                  | 6-9               |
| Biological content        | --                |
| Chemical content          | 150-250           |
| Total solid content       | 50                |
| Oil and grease content    | 10                |
| Total nitrogen content    | --                |
| Total phosphorus content  | --                |
| Temperature               | ≤ 3°C increase    |

Sugar industry is an agro-based industry and liquidation of its effluents into nearby land-dwelling and marine systems has become the general practice [6]. Throughout the production of sugar enormous quantity of water is used per day, consequently, the industry generates lot of water effluents on regular basis. This wastewater from sugar industry contains large amount of pollutants [7]. These pollutants include not only a large
number of chemicals being used at different steps during sugar manufacturing process but also includes some quantities of oil and grease generated from the process house [8]. Wastewater from sugar industry when not treated properly also generates nasty odor when discharged into the surroundings. Due to its complex characteristics, treatment of sugar industrial effluent has become an ever-growing challenge [9]. Appropriate treatment methods are needed to meet the rigorous discharge measures for the protection of environment and its surroundings.

Sugar industrial effluents are usually treated by implementing diverse physical, chemical and biological processes [10]. The former includes processes like adsorption, coagulation/ flocculation, electrocoagulation and flotation. Biological methods include aerobic, an-aerobic and membrane assisted methods [11]. Some studies indicate simultaneous use of both aerobic and anaerobic process for the treatment of sugar industrial effluents [12]. The study at hand reveals a contingent approach of various methodologies employed for the removal of pollutants from sugar industries.

### Biological Methods

As the sugar industrial waste comprises a large amount of sugars and volatile fatty acids which can easily be biodegraded by biological methods; therefore, both anaerobic and aerobic treatments have been tremendously employed in treating sugar industrial waste [13].

### Aerobic treatment

Degradation of organic matter in the presence of oxygen is referred to aerobic process. Traditional aerobic methods employed for processing of sugar industrial effluents include usage of activated slime, trickling filters, aerated bayous or combination of these [14]. Effluents from sugar industry can easily be biodegraded excluding the oil and grease contents. The oils and fats cannot be degraded aerobically due to the production of methane during hydrolysis [15,16].

A series of experiments has been conducted by a group of researchers on batch reactor in order to verify the validity of aerobic processes in treating sugar industry wastewater. From the results obtained it was indicated that biodegradation of wastewater in the presence of oxygen offers a promising reduction an agreeable reduction in pollutants [9].

### Anaerobic treatment

Anaerobic process employed for removal of pollutants is the most commonly used method in industries. It has numerous advantages on aerobic processes. One of the most advantageous factors of anaerobic process lies in lesser energy requirement due to methane production resulting in the degradation of organic matters. This consequently causes reduction in sludge production, which in turns effectively lowers down sludge disposal costs [17]. Anaerobic batch reactor, anaerobic fixed-bed reactors (AFR), up-flow anaerobic fixed bed (UAFB) reactor, and up flow anaerobic sludge bed reactor (UASB) reactor are generally engaged for anaerobic treatment of sugar industrial wastewater [18].

Literature studies indicate that most of the biological processes applied for treatment of sugar industrial effluents are not feasible owing to huge land space requirement, high principle and functional cost price [19]. Therefore, physico-chemical methods are considered economical substitute for the treatment of sugar industry wastewater where conventional biological methods fail to diminish the contaminants [20].

### Physico-Chemical Methods

#### Adsorption

Adsorption is considered a primary stage and is ascertained to be useful in the treatment of wastewater by using various adsorbents [21]. Adsorption is defined as accumulation of a specific component at the surface or interface between two phases. Substance or a pollutant that adheres or sticks to the solid surface is known as adsorbate and the solid surface is called adsorbent [22]. Best adsorbents are considered to follow the subsequent characteristics - a substance, with higher surface area, high permeability, inertness and stability to endure thermal, chemical and climatic changes, it should also be cost effective and must have good physicochemical properties [23,24]. Recently advancements in the use of inexpensive adsorbents have led to instant development in this methodology [25].

Presently, adsorption process is being extensively used for the removal of various organic and inorganic pollutants from sugar industry wastewater [26]. In one of the studies M. Sunitha [27] reported that, adsorption is a quick, cost-effective and a promising technique for the elimination of pollutants emerging from different refining and recycling technologies. In this study adsorbents like bentonite, Mgo, activated charcoal, and fly ash were used as adsorbents for sugar industrial effluents [27]. These adsorbents have been reported in 80% removal of TSS, TDS and oils and grease, along with an effective reduction in BOD, COD, smell and color. The major drawback of adsorption lies in the regeneration of the consumed adsorbent and subsequent treatment of backwash water [28].

#### Coagulation and flocculation

Coagulation has been known to be used for effluent treatment since 19th century [29]. Coagulation-flocculation is particularly employed for effective removal of colloidal sized particles. Om Parkash Sahu and his coworkers studied that coagulation is called adsorbent [22]. Best adsorbents are considered to follow the subsequent characteristics - a substance, with higher surface area, high permeability, inertness and stability to endure thermal, chemical and climatic changes, it should also be cost effective and must have good physicochemical properties [23,24]. Recently advancements in the use of inexpensive adsorbents have led to instant development in this methodology [25].

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COD and color reduction [31]. It was reported that Alum shows 80-86% of COD and color reduction as compared to aluminum chloride which showed reductions of 75-85.7% whereas ferrous sulfate gives 76-82% respectively [32] (Figure 1). Coagulation and flocculation are usually followed by sedimentation, filtration and disinfection. The problems with this treatment process include poor % recovery, operational issues, arbitrary guidelines and dependency on various operational parameters [33].

**Electrocoagulation and flotation**

Electrocoagulation is a quicker and an inexpensive methodology. Due to high removal efficiency electrocoagulation and flotation (ECF) are considered to constitute an effective method over other conventional physico-chemical processes [34]. This technology gathers the use of electric current and pollutants that are accumulated without the addition of chemicals or coagulating agents. Application of direct current enables the removal of even minor amounts of pollutants from industrial effluents. Moreover, ECF is a proficient technique to eliminate residues for side products [35]. Different reagents such as aluminium sulfate, ferrous sulfate or ferric chloride have been reported to be employed in electrocoagulation process [36]. However, these chemicals were found to be very expensive and dependent on the volume of water treated.

The advantage of ECF over other physical processes lies in its capability to reduce the need of chemicals which is due to the use of electrodes which themselves act as coagulating agents [37] (Figure 2). This hereby results in decrease of treatment time of the process [38]. A comparative study of electrocoagulation and chemical coagulation in treating sugar industrial effluent was carried out by Erick Butler and his coworkers. In this study iron and aluminium electrodes were used as electro-coagulants whereas FeCl3 and Al2(SO4)3.3H2O were used as chemical coagulants. In accordance with the primary results achieved, the iron electrodes were found to be more promising in pollutants removal as compared to the aluminum electrodes, despite the fact that use of iron electrodes requires an additional filtration step at the final stage [39].

**Thermolysis**

The term “Thermolysis” refers to the thermal treatment of industrial waste. It involves chemical transformation of the
dissolved organics and inorganics into suspended forms with or without the use of metal compounds at moderate temperature and pressure [40]. Parameters like pH, temperature, autogenous pressure, and catalysts have been found crucial to control the rate of thermolysis process. Thermolysis has been reported to be the best methodology exercised for treating moderate to high strength organic wastes. In a study conducted by P.K. Chaudhari [41] investigated the influence of various parameters such as temperature, pH, catalyst mass loading, and nature of catalysts exerted reduction in COD, BOD and color of the wastewater. It was observed that different catalysts give different %age removal under different pH values. Among various catalysts employed in thermolysis process, copper oxide gives maximum efficiency providing 74% COD and 80% reduction in color [41].

A comprehensive comparison of various methodologies described above in treating sugar industrial effluent is given in Table 2.

Table 2: A comparative overview of various methodologies.

| Sr. No. | Coagulants Used | pH Value | Dose [mM] | COD Reduction [%] | Color Reduction [%] | BOD Reduction [%] | Ref. |
|---------|-----------------|----------|-----------|-------------------|--------------------|-------------------|------|
| 1       | Fe$_3$(SO$_4$)$_3$.9H$_2$O | 2-6      | 20-60     | 36-71             | 42-74              | 64                | [36] |
|         |                  | 7        | 20-60     | 64                | 72                 | 70                |      |
|         |                  | 8-10     | 40        | 42-56             | 68-60              | -                 | [36] |
| 2       | FeO$_3$         | 2-6      | 20-60     | 28-62             | 35-74              | 70                | [6]  |
|         |                  | 7        | 20-60     | 69                | 82                 | 80                | [32] |
|         |                  | 8-10     | 40        | 50-58             | 64                 | -                 | [39] |
| 3       | AlCl3.6H$_2$O   | 2-6      | 20-60     | 29-62             | 30-66              | 60                | [15] |
|         |                  | 7        | 20-60     | 69.3              | 76                 | -                 | [15] |
|         |                  | 8-10     | 60        | 55-73             | 71-83              | 74                |      |
| 4       | Alum            | 2-8      | 40-60     | 23-64             | 24                 | 24                | [39] |
|         |                  | 7        | --        | 74.5              | 74                 | -                 | [39] |
|         |                  | 8-10     | --        | 60-67             | 59-66              | -                 |      |

| Sr. No. | Catalyst used | pH Value | Dose [g/dm$^3$] | COD reduction [%] | Color reduction [%] | BOD reduction [%] | Ref. |
|---------|---------------|----------|-----------------|-------------------|--------------------|-------------------|------|
| 1       | Copper oxide  | 2-10     | 4               | 74                | 80                 | 80                | [40] |

| Sr. No. | Adsorbent used | pH value | Dose [mg] | COD reduction [%] | Color reduction [%] | BOD reduction [%] | Ref. |
|---------|----------------|----------|-----------|-------------------|--------------------|-------------------|------|
| 1       | Activated charcoal | -       | 80        | 80                | 80                 | 80                | [21] |
| 2       | Bentonite      | 4        | 50.7      | 80                | 80                 | 80                | [21] |
| 3       | Lignite        | -        | 80        | 80                | 80                 | 80                | [21] |
| 4       | Fly ash        | -        | 80        | 80                | 80                 | 80                | [7]  |
| 5       | Bagasse        | -        | 80        | 80                | 80                 | 80                | [4]  |
| 6       | kaolin         | 500      | 79        | -                 | -                  | -                 | [7]  |
| 7       | Tamarind nut carbon | 600    | 74        | -                 | -                  | -                 | [12] |
| 8       | Dates nut carbon | 600     | 73        | -                 | -                  | -                 | [12] |

| Sr. No. | Electrode Used | pH Value | Time [hrs] | Voltage | COD Reduction [%] | Turbidity Reduction [%] | Ref. |
|---------|----------------|----------|-----------|---------|-------------------|------------------------|------|
| 1       | Iron Electrodes | 5        | 4         | 10-Aug  | 67-82             | 70-84                  | [34] |
|         |                | 6        | 4         | 10-Aug  | 70-84             | 78-93                  | [7]  |
|         |                | 7        | 4         | 10-Aug  | 72-89             | 72-89                  | [34] |
| 2       | Aluminium electrodes | 6.93   | 2         | --      | 60.8-63.5         | 87.5-98                | [26] |
### V. Biological Treatment Process

| Sr. No. | Type of Waste | Type of Reactor | Methane Yield [mL/g] | COD Reduction [%] | Hydraulic Retention Time | Ref. |
|---------|---------------|-----------------|----------------------|-------------------|-------------------------|------|
| 1       | BSI and BP    | Anaerobic batch reactor | 236-322               | 64-87             | -                       | [15] |
| 2       | CSI           | Aerated film reactor | -                     | < 90              | 4 (h)                   | [9]  |
| 3       | SR            | Rotating biological reactor | -                     | 48                | -                       | [15] |
| 4       | CSI           | Aerated fix film biological system | -                     | 74-68             | 2-8 h                   | [9]  |
| 5       | BSI           | UAFB            | -                     | >90               | 20 h                    | [1]  |

### Conclusion

The results of this study have shown the applicability of different strategies to reduce the detrimental effects of various pollutants from sugar industry. To comply with the discharge standards set by the Agencies responsible for environmental compliance, it is important that industries should take appropriate measures for catering these issues that have compelled sugar industry to occupy position as “Red category” industry. Comparative account of various discussed processes/methods actually provides an insight into the best opted alternates to address the challenges imposed by the hazardous wastes. In addition to all possible approaches to minimize the pollutant problems discussed here, more research is required to address existing loopholes and gaps in order to provide a comprehensive and cost-effective solution to revise and establish the status of sugar industries as zero discharge units.

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