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Evaluation of the accuracy of thermal dissociation CRDS and LIF techniques for atmospheric measurement of reactive nitrogen species

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Abstract. The sum of all reactive nitrogen species (NO\textsubscript{y}) includes NO\textsubscript{x} (NO\textsubscript{2} + NO) and all of its oxidized forms, and the accurate detection of NO\textsubscript{x} is critical to understanding atmospheric nitrogen chemistry. Thermal dissociation (TD) inlets, which convert NO\textsubscript{x} to NO\textsubscript{2} followed by NO\textsubscript{2} detection, are frequently used in conjunction with techniques such as laser-induced fluorescence (LIF) and cavity ring-down spectroscopy (CRDS) to measure total NO\textsubscript{x} when set at > 600 \textdegree C or speciated NO\textsubscript{x} when set at intermediate temperatures. We report the conversion efficiency of known amounts of several representative NO\textsubscript{y} species to NO\textsubscript{2} in our TD-CRDS instrument, under a variety of experimental conditions. We find that the conversion efficiency of HNO\textsubscript{3} is highly sensitive to the flow rate and the residence time through the TD inlet as well as the presence of other species that may be present during ambient sampling, such as ozone (O\textsubscript{3}). Conversion of HNO\textsubscript{3} at 400 \textdegree C, nominally the set point used to selectively convert organic nitrates, can range from 2 to 6 % and may represent an interference in measurement of organic nitrates under some conditions. The conversion efficiency is strongly dependent on the operating characteristics of individual quartz ovens and should be well calibrated prior to use in field sampling. We demonstrate quantitative conversion of both gas-phase N\textsubscript{2}O\textsubscript{5} and particulate ammonium nitrate in the TD inlet at 650 \textdegree C, which is the temperature normally used for conversion of HNO\textsubscript{3}. N\textsubscript{2}O\textsubscript{5} has two thermal dissociation steps, one at low temperature representing dissociation to NO\textsubscript{2} and NO\textsubscript{3} and one at high temperature representing dissociation of NO\textsubscript{3}, which produces exclusively NO\textsubscript{2} and not NO. We also find a significant interference from partial conversion (5–10 %) of NH\textsubscript{3} to NO at 650 \textdegree C in the presence of representative (50 ppbv) levels of O\textsubscript{3} in dry zero air. Although this interference appears to be suppressed when sampling ambient air, we nevertheless recommend regular characterization of this interference using standard additions of NH\textsubscript{3} to TD instruments that convert reactive nitrogen to NO or NO\textsubscript{2}.

1 Introduction

The catalytic cycling of nitrogen oxides (NO\textsubscript{x} = NO + NO\textsubscript{2}) plays a key role in the formation of tropospheric ozone (O\textsubscript{3}) from the photooxidation of volatile organic compounds (VOCs). Reactive nitrogen species, such as alkyl and multifunctional nitrates (ANs, RONO\textsubscript{2}), peroxy nitrates (PNOs, RO\textsubscript{2}NO\textsubscript{2}), and nitric acid (HNO\textsubscript{3}) serve as reservoirs and sinks of NO\textsubscript{x}. The formation of these species results in a
Techniques that detect the major individual components of NO_{x} include detection of NO and NO_{2} by chemiluminescence (Ridley and Howlett, 1974; Kley and McFarland, 1980), cavity ring-down spectroscopy (CRDS; Fuchs et al., 2009), or laser-induced fluorescence (LIF; Thornton et al., 2000), as well as detection of HONO by chemical ionization mass spectrometry (CIMS; Fehsenfeld et al., 1998; Huey et al., 1998; Neuman et al., 2002; Huey, 2007) or mist chamber sampling (Talbot et al., 1990). Additionally, speciated peroxyacetyl nitrates (PANs) have been detected by gas chromatography electron capture detection (Darley et al., 1963; Flocke et al., 2005) and CIMS (Slusher et al., 2004), while N_{2}O_{5} and CINO_{2} have been detected by CRDS (Dubé et al., 2006; Thaler et al., 2011) and CIMS (Kercher et al., 2009). HONO has been detected by long path differential optical absorption spectroscopy (Perner and Platt, 1979), and NO_{3} has been detected by CRDS (King et al., 2000). However, fewer methods have been developed for detection of the broad suite of individual alkyl and multifunctional nitrates, which have been suggested to comprise upwards of 20% of NO_{x} in the mid-latitude continental boundary layer and may be higher in remote locations (O'Brien et al., 1995; Day et al., 2003; Worton et al., 2008; Beaver et al., 2012; Xiong et al., 2015; Lee et al., 2016). An alternative to detecting individual components of NO_{x} is the use of a molybdenum oxide or gold catalyst in the presence of CO to reduce all NO_{x} species to NO, followed by NO detection by chemiluminescence (Winer et al., 1974; Fahey et al., 1986), though catalyst-based techniques are known to require frequent cleaning and are potentially sensitive to contamination and to interferences at ambient levels of ammonia, HCN, acetonitrile and R-NO_{2} compounds (Crosley, 1996; Kliner et al., 1997; Bradshaw et al., 1998; Williams et al., 1998; Day et al., 2002). An alternative method developed by Day and co-workers (Day et al., 2002) uses a quartz thermal dissociation (TD) inlet to rapidly thermally convert nearly all NO_{x} species to NO_{2}, which is then detected by laser-induced fluorescence. The NO_{y} species in the TD inlet undergo the following reaction:

\[XNO_{2} + \text{heat} \rightarrow X + NO_{2},\]  

where X is HO, RO, or RO_{2}. Heated inlets had previously been used to dissociate PNs (Nikitas et al., 1997), but the TD inlet developed by Day et al. (2002) takes advantage of the different O-N bond energies of ANs, PNs, and nitric acid to separately and selectively detect these three classes of NO_{x}. A plot of measured NO_{2} signal as a function of inlet temperature (hereafter referred to as a “thermogram”) yields a stepwise dissociation curve with increases in signal near 100, 300, and 500 °C, corresponding to the dissociation of PNs, ANs, and HONO respectively. By setting the TD oven temperature to one of the three plateaus, they were able to measure each class of NO_{x}, by comparison of the NO_{2} signal in a given channel to the signal measured at the adjacent lower temperature plateau.

In recent years, a suite of other instruments have incorporated this NO_{x} TD inlet method into existing techniques that measure NO_{2} or the radical co-fragment X in Reaction (R1), such as chemical ionization mass spectrometry (TD-CIMS; Slusher et al., 2004; Zheng et al., 2011; Phillips et al., 2013), cavity ring-down spectroscopy (TD-CRDS; Paul et al., 2009; Thieser et al., 2016), and cavity attenuated phase shift spectroscopy (TD-CAPS; Sadanaga et al., 2016). Each instrument has its own advantages and disadvantages. For example, TD-LIF detects NO_{2} at low pressure following thermal dissociation. Secondary recombination reactions of the dissociated radicals would thus be suppressed in the detection region, although the thermal dissociation inlet may be operated at either high or low pressures in these instruments. However, it is subject to interferences from urban levels of NO and NO_{2} (Paul et al., 2009; Wooldridge et al., 2010). TD-CIMS can differentiate between the different types of PNs but requires regular calibration of each species, not all of which have native standards readily available. TD-CAPS is subject to interferences from glyoxal and methylglyoxal (Sadanaga et al., 2016). TD-CRDS is an absolute measurement but can be subject to other interferences, as discussed in Sect. 3.

Recent TD inlet studies (Day et al., 2002; Paul et al., 2009; Thieser et al., 2016) have measured the conversion efficiency for several AN and PN species with known concentrations in a laboratory setting. These studies all note the possibility of secondary reactions that either increase or decrease the NO_{2} signal. For example, recombination reactions to reform the AN or PN species prior to reaching the detector will result in a negative bias in NO_{2} (too little NO_{2} measured). Likewise, ambient levels of O_{3} in the sampled air may react in the oven with NO to form NO_{2}, resulting in a positive bias (Pérez et al., 2007), though this reaction rate depends on the TD inlet pressure and flow rate (Wooldridge et al., 2010).
Day et al. (2002) found that recombination reactions were significant for PNs but caused minimal problems for nitric acid, since the OH radical is far more likely to be lost to the walls of the oven than to recombine with NO₂. More significant is the reaction of dissociated RO₂ and HO₂ radicals with ambient levels of NO and NO₂. Thieser et al. (2016) parameterized the bias in peroxyacyl nitrate and 2-propyl nitrate detection in their inlet as a function of ambient NO and NO₂ concentrations but noted that these parameterizations may vary for other PNs or ANs. In cases where the concentration of one category of NOₓ species far exceeds the others, such as the high HNO₃: ANs ratios in Pusede et al. (2016), speciated measurements can be significantly affected by biases in measurements of the other NOₓ compounds.

A four-channel CRDS instrument (hereby referred to as the NOAA TD-CRDS instrument) for detection of nitrogen oxides was recently developed (Wild et al., 2014). In this instrument, one channel is equipped with a TD inlet set at 650°C and is used to measure all NOₓ species (including NO₂, as well as NO by chemical conversion with an O₃ addition to NO₂). Two other channels simultaneously monitor NO₂ and NO, and so a measurement of NO₂ (= NOₓ - NO) can be derived. Because NO is intentionally detected as NO₂ in the NOₓ channel, this instrument avoids the majority of the NO ↔ NO₂ interconversion interferences that affect many other thermal dissociation instruments. Analogous to the studies which measured the conversion efficiencies of ANs and PNs (Day et al., 2002; Paul et al., 2009; Sadanaga et al., 2016; Thieser et al., 2016), we present here an analysis of the conversion efficiencies of several other NOₓ species and the interferences that affect the operation of this high temperature inlet. These interferences include the temperature dependence of HNO₃ conversion, which is important to understanding both its quantitative conversion at 650°C as well as its potential to interfere with measurements of ANs at lower temperatures. We also compare these results to those from the TD-LIF instrument of Day et al. (2002), hereby referred to as the Berkeley TD-LIF instrument. Additionally, we report the temperature dependence of N₂O₅ conversion, which is shown to occur in two steps; first, the conversion efficiency of ammonium nitrate aerosol and finally the interference of NH₃ through its partial conversion to NO.

2 Methods

2.1 Thermal dissociation cavity ring-down spectroscopy (TD-CRDS)

Cavity ring-down spectroscopy is a direct absorption technique for measuring the concentration of trace gases (O’Keefe and Deacon, 1988; Fuchs et al., 2009). The four-channel 405 nm NOAA TD-CRDS instrument, which has been used by our group in both lab-based studies and atmospheric sampling (Wild et al., 2014, 2016), simultaneously measures ambient NO₂ in one channel, while chemically converting NO and O₃ to NO₂ in the second and third channels, and thermally converting NOₓ to NO₂ in a TD oven in the fourth channel. In this study, we have used only the NOₓ channel to study the conversion efficiency of several reactive nitrogen species to NO₂. Figure 1 shows a schematic of the relevant instrument plumbing and optical cavity. The details of the optical cavity can be found in Wild et al. (2014); only a brief description of the optical system and the details of the TD inlet that deviate from that study will be described here.

Sampled air is pulled into a 50 cm long high-finesse optical cavity capped by highly reflective end mirrors, with purge flows of 25 scm (standard cubic centimeters per minute at 273.15 K and 1 atm) added in front of each mirror to maintain mirror cleanliness. The output of a 0.5 nm bandwidth, continuous wave diode laser centered at approximately 405 nm and modulated at 2 KHz is passively coupled into one end of the optical cavity. The laser light builds up in the cavity, and when it is modulated off the decaying output light intensity is monitored by a photomultiplier tube on the far side of the cavity. The measured light decay profiles are summed and fit at a 1 Hz repetition rate to yield the ring-down time \( \tau \). The ring-down time is inversely related to the concentration of the absorbing gas, NO₂ in this case, which can be derived as

\[
[\text{NO}_2] = \frac{R_L}{c \sigma} \left( \frac{1}{\tau} - \frac{1}{\tau_0} \right),
\]

where \( R_L \) is the ratio of \( d \), the mirror separation length, and \( l \), which is the distance over which the sample is present. The speed of light is represented by \( c \), \( \sigma \) is the absorption cross section of NO₂, and \( \tau_0 \) is the ring-down time of a reference cavity without any absorbing gases, which is obtained by flushing the cavity with an excess flow of zero air for 30 s every 10 to 20 min. If purge volumes were not used, the \( R_L \) term in Eq. (1) would simply be 1, but, since purge volumes are used here, \( \sigma / R_L \) is characterized regularly by filling the cavity with several different known NO₂ concentrations (obtained by reacting the output of an O₃ standard source with excess NO) and calculating the slope of the measured optical extinction vs. [NO₂] as described in Washenfelder et al. (2011). This value was measured approximately once per month during laboratory tests with this instrument but was constant to within ±1 %, with an average value of 6.25 × 10⁻¹⁹ cm². More regular calibrations of the \( \sigma / R_L \) value during recent field studies show similar stability. The NO₂ signal can be measured with a lower detection of 18 pptv (1σ) in 1 s (Wild et al., 2014).

The NOₓ TD oven inlet consists of a quartz tube (0.39 cm ID and 63 cm in length, of which 38 cm is heated) wrapped in nichrome wire and insulated with fiberglass. The flow rate through the inlet and optical cavity is controlled by a mass flow controller on the downstream side of the optical cavity. Because the standard flow rate is held constant during each experiment, the volumetric flow rate, and therefore the TD residence time, varies with oven temperature. For exam-
Figure 1. Instrument schematic of the TD-CRDS instrument used in this study. An NO$_y$ source (HNO$_3$ permeation tube, N$_2$O$_5$ cold trap, NH$_4$NO$_3$ particle atomizer + DMA size selector, or NH$_3$ permeation tube) is diluted by a zero air flow (with an option for adding O$_3$, VOCs, RH, or CO through the secondary addition port) and passed through the TD oven. A portion of the flow is sampled prior to entering the oven with one of several types of auxiliary measurements (CIMS for N$_2$O$_5$; an ultra-high sensitivity aerosol spectrometer, UHSAS, for NH$_4$NO$_3$ particles; or commercial CRDS for NH$_3$). After flowing through a cooling region, the sample passes through a particle filter and then is mixed with a ~30 ppbv addition of O$_3$ in a mixing volume before entering through the optical cavity, where NO$_2$ is measured by CRDS.

2.2 NO$_y$ samples and additions

Samples of reactive nitrogen species (labeled as “NO$_y$ source” in Fig. 1) were introduced into the TD oven in several ways. HNO$_3$ and NH$_3$ were obtained by passing a 50 sccm flow of zero air through a calibrated 45°C permeation tube containing HNO$_3$ (VICI Metronics) or NH$_3$ (KinTek), providing gaseous outputs of 64 and 23 ng min$^{-1}$, respectively (Neuman et al., 2003). Subsequent dilution in 0.5–4 sccm zero (synthetic) air resulted in HNO$_3$ and NH$_3$ concentrations of 5 to 40 ppbv. Because both these species readily adsorb to instrument surfaces (Neuman et al., 1999), only fluorinated ethylene propylene (FEP) Teflon tubing was used between the permeation tube and the TD oven, and all tubing was kept as short as possible (typically less than 30 cm) and was wrapped in 100°C heating tape to reduce losses to the walls. However, these precautions were found to be unnecessary in this laboratory study, since the constant flow from the permeation tube resulted in an equilibrium in which the adsorption losses to the walls were equal to the rate of off-gassing.

NO was obtained by dilution of the output of a calibrated standard (Scott-Marrin, 0.2 % in N$_2$). N$_2$O$_5$ was synthesized via a procedure adapted from Davidson et al. (1978) and Bertram et al. (2009), which has been used as a calibration for the N$_2$O$_5$ channel of a CRDS NO$_2$ instrument (Dubé et al., 2006; Wagner et al., 2011). Pure samples of NO and O$_2$ were mixed to yield NO$_2$, and this mixture was reacted in a flow tube with excess O$_3$, yielding NO$_3$ which then reacted with NO$_2$ to form N$_2$O$_5$. The resulting mixture flowed through a glass trap at $-78^\circ$C, where N$_2$O$_5$ solidified as a white crystal. A gaseous sample of N$_2$O$_5$ was obtained by flowing 20–50 sccm of zero air over the solid $-78^\circ$C sample and then diluting further in zero air. Gas-phase N$_2$O$_5$ prepared in this way is known to contain variable but significant amounts of HNO$_3$ (Bertram et al., 2009), and thus efforts were made to minimize this interference by baking all glassware for several hours before use and by distilling the solid N$_2$O$_5$ sample regularly by bringing it to room temperature under an O$_3$ flow for 10 min. Nevertheless, some HNO$_3$ was always present in the sample, and therefore the output of the trap was passed through a nylon wool scrubber prior to entering the TD oven, which removed HNO$_3$ without significantly perturbing the N$_2$O$_5$ concentration. Finally, ammonium nitrate particles were generated by running a 0.1 g L$^{-1}$ solution of aqueous NH$_4$NO$_3$ through an atomizer and size-selecting particles of a certain diameter with a custom-built differential mobility analyzer (DMA). Conductive tubing, rather than Teflon, was used to minimize electrostatic build-up and loss of particles to the walls before entering the TD oven.

In order to test whether common atmospheric gases would interfere with the conversion efficiency, some additional
species were added to the sample prior to entering the oven. Water was added by passing the dilution zero air through a water bubbler prior to mixing with the HNO$_3$ sample. Various amounts of O$_3$ were added by running the dilution zero air through an O$_3$ calibrator (Thermo Fisher Scientific 49i) that is also capable of generating up to 200 ppm O$_3$ in 1–3 slpm of zero air. We also investigated the effect of various VOCs, including a high concentration of propane ($\sim 5$ ppmv) and a standard mixture of VOCs (Air Liquide) consisting of n-hexane (1.234 ppm), propanal (0.397 ppm), 2-butanol (1.237), benzene (1.151 ppm), methylcyclohexane (0.938 ppm), ethylbenzene (1.213 ppm), 2,2,4-trimethylpentane (1.186 ppm), isopropyl benzene (1.148 ppm), and ethanol (0.994 ppm). This mixture is commonly used to calibrate gaschromatography–mass spectrometry (GC–MS) instruments but here provides common atmospheric species with a range of masses, bond strengths, and degrees of oxidation. It was diluted to 50 ppbv total VOCs by addition of zero air prior to entering the oven. We also added CO in varying quantities to the HNO$_3$ and NH$_3$ samples.

2.3 Ancillary measurements

Several instruments were used as ancillary confirmation for some of the NO$_3$ sample concentrations. In each case, a Teflon tee split the sample input and a portion of the flow was pulled into the secondary instrument prior to entering the TD oven, as shown in Fig. 1. In the case of NH$_3$, a Picarro G2103 NH$_3$ analyzer with a manufacturer’s specified 1 ppbv detection limit at 5 s integration time was used. A custom-made iodide adduct chemical ionization mass spectrometer (Lee et al., 2014), described in further detail in Veres et al. (2015), was used to monitor the N$_2$O$_5$ and HNO$_3$ concentrations from the N$_2$O$_5$ solid sample prior to dissociation in the oven. In this instrument, N$_2$O$_5$ and HNO$_3$ mixed with I$^-$ ions produced by passing CH$_3$I through a $^{210}$Po source, and the resulting HNO$_3$·I$^-$ and N$_2$O$_5$·I$^-$ ions were detected by quadrupole mass spectrometry at $m/z = 190$ and 235. This measurement has a detection limit of 4 pptv and 70 pptv and error bars of 25 and 25% (3σ) for N$_2$O$_5$ and HNO$_3$, respectively. Lastly, an ultra-high sensitivity aerosol spectrometer (Droplet Measurement Technologies) was used to monitor the size distribution of the size-selected ammonium nitrate particles (Cai et al., 2008). HNO$_3$ and NH$_3$ conversion efficiencies were also tested using ambient air for dilution (rather than synthetic air), as sampled during daytime in August 2016 in Boulder, CO. Ambient air was drawn into the two of the four channels of the NOAA TD-CRDS instrument, through two side-by-side identical quartz ovens heated to 650 °C at a flow rate of 1.4 slpm, and the output of either the NH$_3$ or HNO$_3$ permeation tube was inserted directly into the exposed inlet of one of the ovens, for a duration of approximately 6 min. The NO$_2$ signal was measured by one of the remaining channels in the NOAA TD-CRDS instrument, and the conversion efficiency of each species was calculated by comparing the difference in NO$_2$ signal between the two ovens relative to the calibrated output of the permeation tube to correct for small differences in NO$_2$ signal between the two ovens.

We also present results measured in the Berkeley TD-LIF instrument. It is described in greater detail elsewhere (Day et al., 2002), but briefly HNO$_3$ and n-propyl nitrate samples were provided by permeation tubes similar to those described in Sect. 2.2, diluted in dry zero air, and passed through 20 cm heated length quartz ovens, held at ambient pressure, at a flow rate of 2 slpm. This resulted in residence times of approximately 50 ms. The NO$_2$ released in the thermal conversion was supersonically expanded into the detection region and measured by laser-induced fluorescence from an individual rovibronic NO$_2$ line. The NO$_2$ conversion ratio was calculated as the measured NO$_2$ concentration relative to the maximum NO$_2$ signal at high temperatures, as the oven temperature was changed at a rate of $\sim 10$ °C per minute.

2.4 Box modeling

A simple kinetic box model was used to support the experimental findings. Reaction rates for $\sim 60$ reactions possibly involved in the dissociation and secondary chemical reactions of each NO$_3$ species (listed in the Supplement) were obtained from the Jet Propulsion Laboratory (JPL) Kinetics Database (Sander et al., 2011) and the NIST Chemical Kinetics Database (Manion et al., 2015) at temperatures spanning the 25–650 °C range of the experimental thermograms. For every HNO$_3$, N$_2$O$_5$, and NH$_3$ thermogram, a simulation was run at each temperature, assuming a starting concentration of the NO$_3$ species equal to that observed in the experiment and lasting the duration of the residence time in the oven. The simulation was then allowed to keep running at room temperature for an additional $\sim 1$ s to mimic the conditions between the oven and the instrument. During this additional low temperature time, 30 ppmv of O$_3$ was added to the simulation to convert NO to NO$_2$ as in the TD-CRDS instrument. The final concentration of NO$_2$ at the end of the simulation was recorded for each temperature, which resulted in a simulated thermogram. Several simplifying assumptions were made here. We assume instantaneous heating and cooling of the sample and a uniform temperature profile along the 38 cm length of the TD oven. We also only consider gas-phase reactions and neglect any surface-mediated reactions. When possible, JPL-recommended values for the rate constants were used, but many of those listed did not span the full temperature range of the thermograms. When JPL values were not available, reaction rates from the NIST database were used (see Table S1). We also derive temperature-dependent wall loss constants for O and OH using the procedure outlined by Thieser et al. (2016), but we find that better agreement in some simulations can be achieved with the experimental data by using an empirical value or no wall loss at all. As can
be seen in Sect. 3, these simulations successfully replicated a major portion, but not all, of the experimental results, likely due to these simplifications.

3 Results

3.1 HNO$_3$ thermograms

Figure 2 shows the conversion efficiency of HNO$_3$ to NO$_2$ as a function of temperature for several flow rates through the NOAA TD-CRDS. Conversion efficiency was calculated as measured NO$_2$ mixing ratio divided by the input HNO$_3$ mixing ratio. The box model simulations for each flow rate are shown as solid lines of corresponding color. The HNO$_3$ permeation tube has a calibrated output of 64 ng min$^{-1}$, which corresponds to an expected HNO$_3$ concentration of between 5 and 40 ppbv, depending on the zero air dilution required for each flow rate. The output of the permeation tube was found to contain approximately 2.5 % NO$_2$, and all HNO$_3$ thermograms have had this 2.5 % baseline signal subtracted. At a flow rate of 1.9 slpm (where the oven residence time is 30–100 ms depending on temperature), we observe 100 % conversion of HNO$_3$ at oven temperatures above 600°C, whereas the thermograms obtained at 1 and 3 slpm reach a maximum conversion of 100 % at 550 and 650°C, respectively. The 0.5 slpm thermogram has a slightly lower maximum conversion efficiency (95 %), possibly due to the recombination reaction of OH and NO$_2$ during the extended time in the “cooling region” prior to detection.

The box model simulations in Fig. 2 mimic the shape of the experimental data, but some are slightly shifted to higher or lower temperatures, likely because the simulation is extremely sensitive to the flow rate and may be affected by the simplifying assumptions detailed in Sect. 2.4. The shape of the simulated thermogram is entirely controlled by the reaction rate of the initial dissociation reaction of HNO$_3$ to NO$_2$ + OH. This reaction has a third-order rate constant of $k_0(T) = 1.82 \times 10^{-4} \times (T/298)^{-1.98} \times e^{(-24004/T)}$ and a high-pressure limit of $k_{\infty}(T) = 2 \times 10^{15} \times e^{(-24054/T)}$ (Glänzer and Troe, 1974), and thus at a midrange temperature, such as 500°C, the HNO$_3$ lifetime is approximately 250 ms. The inner volume of the oven is 4.5 cm$^3$, and so at a flow rate of 1.9 slpm, the gas has a plug flow residence time of 38 ms in the 500°C oven, compared to a residence time of 77 ms at 1.0 slpm and 153 ms at 0.5 slpm. The simulated conversion efficiency in these midrange temperatures is therefore extremely sensitive to the flow rate, in agreement with our experimental results. However, the experimental 100 % conversion efficiency at high temperatures indicates that there is virtually no recombination of OH and NO$_2$ once formed, because the recombination rate for OH + NO$_2$ is quite low and because OH radicals are far more likely to be lost to the walls of the oven at a diffusion-limited rate determined by Day et al. (2002) of ∼46 s$^{-1}$ for 1/4 in (0.63 cm) OD tubing, which is far higher than the pseudo-first-order recombination rate coefficient of 0.075 s$^{-1}$ at [NO$_2$] = 10 ppbv. No attempt was made to dilute the output of the HNO$_3$ permeation tube any further, as recombination effects would likely only be less important at lower starting HNO$_3$ concentrations. Similarly, increasing the starting NO$_2$ concentration, to mimic conditions in highly polluted environments, was not attempted in this set of experiments, but increasing the starting NO$_2$ concentration in the kinetic model up to 50 ppbv shows that there is no recombination expected even with elevated NO$_2$ in the oven. This is in contrast to ANs and PNs, for which the reaction of the dissociated peroxy and alkyl radicals with NO$_2$ is a significant interference (Thieser et al., 2016), but in good agreement with the HNO$_3$ results of Day et al. (2002) and Sobanski et al. (2016).

At a flow rate of 1.9 slpm, we observe a ∼6 % conversion of HNO$_3$ to NO$_2$ at an oven temperature of 400°C. Although this efficiency is specific to the conditions of the oven used here, it is a key finding since 400°C is in the vicinity of the temperature set point chosen for selective detection of total alkyl and multifunctional nitrates by TD-LIF (Day et al., 2002) and other TD instruments. This result is in good agreement with Thieser et al. (2016), who found a ∼10 % HNO$_3$ conversion at 450°C. Sadanaga et al. (2016) report a ∼15 % HNO$_3$ conversion at 360°C at a TD residence time of 3.4 s, which exceeds the range of our study but follows the trend in Fig. 3. In a previous study (Wild et al., 2014), we presented thermograms designed to demonstrate quantitative conversion efficiency at high temperatures. The temperature dependence of thermal conversion was not well constrained at lower temperatures and showed, for example, 30 % conversion at 400°C. As discussed by Sobanski et al. (2016), the large conversion efficiency presented by Wild et al. (2014) at this temperature is likely incorrect. The extent of HNO$_3$ con-
Conversion is dependent on the residence time in the oven, but because residence time for a given flow rate changes with oven temperature, it is easier to observe this effect by plotting conversion efficiency versus residence time, as in Fig. 3, for five different temperatures (350, 400, 450, 500, and 600 °C). This plot represents transects through Fig. 2 at these five temperatures. Figure S2 shows a log scale plot to highlight the low conversion efficiency region. Most instruments utilizing the TD oven technique use a set point between 350 and 450 °C and a residence time between 30 and 100 ms to selectively detect ANs and not HNO₃ (Day et al., 2003; Paul et al., 2009; Thieser et al., 2016), but Fig. 3 demonstrates that there is significant variability in the HNO₃ conversion efficiency that depends nonlinearly on oven residence time.

We further measure the effect of pressure on the conversion by placing a heated stainless steel needle valve in front of the oven, thus lowering the pressure inside the oven to 250 mbar. The low pressure transects for each of the five temperatures can be seen in open circles in Fig. 3, and the full thermograms are displayed in Fig. S3. The low pressure transects are slightly lower than those at ambient pressure for the 450 and 500 °C set points but match reasonably well at low and high temperatures, indicating that the onset and final conversion of HNO₃ are not strongly sensitive to pressure. To ensure that HNO₃ was not lost on the walls of the stainless steel valve, the conversion efficiency was measured with the valve fully open and was found to match that taken with no valve. These experiments demonstrate the importance of verifying that a given temperature set point and that flow rate is suitable for measurement of alkyl nitrates without interference from HNO₃ conversion.

To demonstrate the variability within individual TD ovens, an example of the HNO₃ conversion efficiency near the alkyl nitrate temperature set point, as measured by the Berkeley TD-LIF instrument, is shown in Fig. 4. This inlet’s alkyl nitrate set point temperature was chosen to be just past the plateau in the n-propyl nitrate signal at 410 °C. The HNO₃ conversion to NO₂ was found to be 2.5 %, which for most TD-LIF experiments would be negligible compared to other uncertainties in measured ANs (±15 %) and no correction would be applied. One example where a correction was significant was for the NASA DISCOVER-AQ California deployment, which took place in California’s central valley during a period of high NH₄NO₃ aerosol loading. Ratios of (HNO₃ + NH₄NO₃) to ANs were high enough that a correction was necessary and applied to both observations (Pusede et al., 2016). As HNO₃ is derived by subtraction of the ANs, any HNO₃ conversion at the AN temperature results in a high bias for ANs and an equal low bias for HNO₃. The sum of the two remains correct, independent of the onset of the HNO₃ conversion. The Berkeley group has found the HNO₃ conversion to be oven dependent even for identical pressure and flow conditions, indicating that some but not all ovens have impurities at the walls that effectively catalyze HNO₃ decomposition. Ovens with high HNO₃ conversion efficiencies at low temperatures were discarded. These results highlight the importance of careful evaluation and calibration of each TD oven, even when the inner volumes and flow rates are similar.

### 3.2 HNO₃ thermograms with additions

Tests for other interferences to HNO₃ and AN measurements included adding several different chemical species to the HNO₃ sample prior to entering the oven. These were designed to test the hypothesis that certain trace gases found in ambient air would interact with radicals in the oven or would themselves dissociate to form radicals which could react with NO, NO₂, OH, or HNO₃. The results are shown in Fig. 5. In Fig. 5a, a portion of the dilution air was passed through a distilled water bubbler prior to diluting the HNO₃, bringing the relative humidity up to 66 %. The change in RH does not alter the shape, onset, or total conversion efficiency of the thermogram. This is to be expected, as the oven temperature is not high enough to dissociate H₂O to OH + H, and reactions between H₂O and the relevant species formed in the oven from HNO₃ dissociation are far too slow to be important here. However, it should be noted that both H₂O and HNO₃ are sampled in this experiment at a steady concentration, and it is possible that, during ambient sampling, rapid changes in the RH or HNO₃ concentration could change the overall efficiency. Additionally, we did not test the conversion efficiency at very high RH levels, and it is possible there could be a nonlinear effect of water. Figure 5b shows the
measured thermogram with the addition of \( \sim 50 \text{ ppbv VOCs} \) (described in Sect. 2.2) with and without the addition of 90 ppbv O\(_3\) as well as the addition of 5 ppmm of propane, to mimic conditions found in highly polluted wintertime atmospheres. If organic radicals were produced thermally in the TD oven, they could potentially react with NO\(_2\), thus altering that signal. However, the bond dissociation energy of the C-H or C-C bonds most likely to thermally dissociate in each of the VOCs are all significantly higher (typically \( > 100 \text{ kcal mol}^{-1} \)) than that of the O-N bond in HNO\(_3\) (\( \sim 50 \text{ kcal mol}^{-1} \)), making it unlikely that organic radicals are formed inside the oven from dissociation of VOCs. Reactions of unsaturated hydrocarbons with O atoms or OH radicals tend to be rapid and would produce organic radicals, but these tend to be unstable, and any stable radicals would likely only react with NO\(_2\) to form ANs or PNs. The oven is set at sufficiently high temperatures to dissociate ANs and PNs back to NO\(_2\) + the organic radical. Addition of these VOCs does not affect the measured conversion efficiency, even in the presence of ambient levels of O\(_3\). Ozonolysis of the unsaturated hydrocarbons is slow enough (typically on the order of \( 1 \times 10^{-17} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1} \)) to not have any effect here (we would expect <0.0001 % reaction for the duration of the oven residence time). An extremely high concentration of propane also has no effect on the overall conversion efficiency, within the error bars of the measurement, for the same reasons as detailed above.

Figure 5c shows the addition of both small and large quantities of O\(_3\) to the HNO\(_3\) sample. Small quantities do not change the onset or overall conversion efficiency, but larger amounts of O\(_3\) reduce the conversion efficiency at high temperatures. The kinetic box model does not predict this reduction, as it predicts 100 % conversion efficiency to NO\(_2\) at all O\(_3\) levels. The dominant bimolecular reaction of O\(_3\) in the model is the reaction with NO\(_2\) to make NO\(_3\), but, since these reactions are occurring at high temperature, any NO\(_3\) formed will immediately dissociate to NO\(_2\) (see Sect. 3.3). O\(_3\) also thermally dissociates to O + O\(_2\) at temperatures above 200°C (see Fig. S4), but the dominant fate of the O radicals should be loss to the walls. Of the O atoms that are not lost to the walls, their primary reaction is also with NO\(_2\) to form either NO + O\(_2\) or NO\(_3\), but NO should be converted back to NO\(_2\) after the oven. Nevertheless, there is an apparent reduction in the conversion of HNO\(_3\) to NO\(_2\) with increasing O\(_3\). While the O\(_3\) concentration range in Fig. 5c exceeds that found in ambient air, highly polluted areas may have large enough O\(_3\) concentrations to make this reduction in conversion efficiency significant. Finally, the addition of 400 ppmm CO in Fig. 5d has a marked effect on the onset, shape, and final conversion of the HNO\(_3\). This addition was tested because gold catalytic NO\(_3\) converters require a 1 % CO addition to drive the dissociation forward. We find that \( \sim 0.5 \% \) CO is sufficient to promote HNO\(_3\) dissociation even in the absence of a gold catalyst. However, our kinetic model does not replicate the results of the CO addition. Since the rate-limiting step in these thermograms is the initial dissociation of HNO\(_3\), it is unlikely that the reaction between CO and OH or NO\(_2\) plays a role here. It must therefore be caused by a reaction which changes the rate kinetics of the initial dis-
sociation step. However, to our knowledge there have been no laboratory kinetics studies on the CO + HNO\textsubscript{3} reaction. It is likely that there is some surface reaction that affects the NO. This issue does not affect the TD-CRDS NO\textsubscript{3} (Thieser et al., 2016) has cautioned that the elevated NO sample was passed through the oven. When no excess O\textsubscript{3} is added to the mixing volume after the oven to convert NO to NO\textsubscript{2} to measure total NO\textsubscript{y}. Nevertheless, we have investigated how NO responds in the oven, and the results are shown in Fig. S5. A 15 ppbv NO sample was passed through the oven. When no excess O\textsubscript{3} is added to the mixing volume, no NO\textsubscript{2} signal is seen, and, when mixing volume O\textsubscript{3} is added, full conversion of NO to NO\textsubscript{2} is observed, as expected. However, when 100 ppbv of O\textsubscript{3} is added to the oven (with no mixing volume O\textsubscript{3} addition), an approximately 2.2 ppbv NO\textsubscript{2} signal was observed, or a 15% conversion. This is consistent with the kinetic rate expressions for NO + O\textsubscript{3} and NO + O, but we do not differentiate between these two mechanisms in these experiments, as O\textsubscript{3} will always form O at the elevated oven temperatures.

3.3 N\textsubscript{2}O\textsubscript{5} thermograms

Figure 6 shows the measured thermogram of N\textsubscript{2}O\textsubscript{5} in the NOAA TD-CRDS at ambient pressure and flow rates of 1.9 and 1.0 slpm, with the kinetic model simulations for each flow rate shown in solid and dashed lines. Two distinct dissociation steps are observed and confirmed by the kinetic model: one between 30 and 110 °C corresponding to the dissociation of N\textsubscript{2}O\textsubscript{5} to NO\textsubscript{2} + NO\textsubscript{3} and one above 300 °C corresponding to the dissociation of NO\textsubscript{3}. The N\textsubscript{2}O\textsubscript{5} synthesis method also produces HNO\textsubscript{3} (Bertram et al., 2009), and, because the bond enthalpies of NO\textsubscript{3} and HNO\textsubscript{3} dissociation are similar (both ~50 kcal mol\textsuperscript{-1}), the thermograms of these two species are expected to overlap at high temperatures. Thus, a nylon wool scrubber was used to remove HNO\textsubscript{3}, and the scrubbed sample was simultaneously monitored with an iodide chemical ionization mass spectrometer, described in Sect. 2.3, to ensure the HNO\textsubscript{3} (and not the N\textsubscript{2}O\textsubscript{5}) was completely removed. The flow rate was lowered to 1.0 slpm in the high temperature scans to accommodate both instruments with a better signal-to-noise ratio. The CIMS measured approximately 120 pptv HNO\textsubscript{3}, possibly due to hydrolysis of N\textsubscript{2}O\textsubscript{5} after the scrubber, and thus more than 99.5% of the NO\textsubscript{2} signal we observe is attributed to N\textsubscript{2}O\textsubscript{5}.

At high temperatures, each N\textsubscript{2}O\textsubscript{5} is expected to produce two NO\textsubscript{2} molecules. Conversion efficiency is calculated from the measured NO\textsubscript{2} concentration relative to the N\textsubscript{2}O\textsubscript{5} concentration measured by the CIMS instrument, which samples prior to the TD oven. However, the CIMS instrument requires an empirical calibration factor for any species it measures, and, while the HNO\textsubscript{3} signal may be calibrated using the permeation tube described in Sect. 3.1, there was no independent calibration available for N\textsubscript{2}O\textsubscript{5} – only the signal measured using the TD-CRDS instrument. Therefore, the CIMS N\textsubscript{2}O\textsubscript{5} signal was assumed to correspond to a 200% conversion efficiency in the TD-CRDS at 650 °C, and the relative conversion was measured at lower temperatures. The first dissociation step of N\textsubscript{2}O\textsubscript{5} to NO\textsubscript{2} and NO\textsubscript{3} is expected at oven temperatures above 110 °C, but, because the sample must then travel through a cooling region prior to entering the CRDS optical cavity (see Fig. 1), approximately 10% of the NO\textsubscript{2} and NO\textsubscript{3} is expected to recombine back to N\textsubscript{2}O\textsubscript{5}, based on the rate constant and the residence time in the mixing volume. This behavior has been well characterized previously (Fuchs et al., 2009) and is accounted for in the data analysis, and as expected we observe a 91% conversion efficiency of N\textsubscript{2}O\textsubscript{5} to NO\textsubscript{2} between 110 and 300 °C. At higher temperatures, NO\textsubscript{3} dissociates in the oven before recombining with NO\textsubscript{2}, and thus a 200% conversion efficiency is observed. While this is not an absolute measure of conversion efficiency, the relative conversion efficiency is consistent with N\textsubscript{2}O\textsubscript{5} dissociation and recombination reaction rates to generate two NO\textsubscript{2} molecules in a distinct stepwise manner. At 150 and 400 °C, the temperature set points often used for detection of PANs and ANs, we find 90 and 105% conversion of N\textsubscript{2}O\textsubscript{5} to NO\textsubscript{2}, respectively. The exact values are highly dependent on the residence time in both the oven and in the cooling region but serve to highlight the importance of characterizing the N\textsubscript{2}O\textsubscript{5} response in every thermal dissociation oven.

Figure 6. Thermogram of N\textsubscript{2}O\textsubscript{5} measured in the NOAA TD-CRDS at two flow rates. The red squares and red dashed line show the 1.9 slpm thermogram and simulation, while the blue circles and blue solid line show the analogous result at 1.0 slpm. The first dissociation corresponds to N\textsubscript{2}O\textsubscript{5} → NO\textsubscript{2} + NO\textsubscript{3} and the second to NO\textsubscript{3} → NO\textsubscript{2} + O. The second curve reaches a maximum of 200%, while the first reaches 90–95%, depending on the flow rate, due to recombination of NO\textsubscript{2} and NO\textsubscript{3} in the cooling region prior to the detector region. The black dashed line is the experimental HNO\textsubscript{3} thermogram from Fig. 2, offset by 100%. The green triangles indicate measurements of the conversion efficiency without the O\textsubscript{3} addition, confirming that the second dissociation must occur via NO\textsubscript{3} → NO\textsubscript{2} + O rather than NO\textsubscript{3} → NO + O2.
We also measured the conversion of N$_2$O$_5$ without the mixing volume O$_3$ addition at two relevant temperatures in order to determine the mechanism for NO$_3$ dissociation. These data are shown in green triangles in Fig. 6 and show no difference in onset or maximum conversion efficiency, whether or not mixing volume O$_3$ is added. As the mixing volume O$_3$ converts ambient or thermally produced NO to NO$_2$, the similarity of the two spectra indicates that the NO$_3$ dissociation mechanism must be NO$_3$ $\rightarrow$ NO$_2$+O. However, there are no published rate expressions for this reaction, and the few studies on NO$_3$ thermal dissociation have disagreed about whether the reaction proceeds to NO + O$_2$ (Johnston et al., 1986) or NO$_2$+ O (Schott and Davidson, 1958). The former argued for the NO$_3$ $\rightarrow$ NO + O$_2$ mechanism based on thermondynamics, as this reaction is exothermic. However, this implies that NO$_3$ would be thermally unstable at room temperature, which is not the case. It is likely that there is a significant energy barrier to this reaction. The bond enthalpy of the NO$_3$ $\rightarrow$ NO$_2$+ O reaction, on the other hand, is 50.4 kcal mol$^{-1}$, nearly identical to that of HNO$_3$ $\rightarrow$ NO$_2$+ OH, and the two thermograms are very similar in shape and are centered at the same temperature (500$^\circ$C). The simulation shown in Fig. 6 is a fit rate expression of $k(T) = 1 \times 10^{-2} \times (T/298)^9 \times \exp(-1500/T)$ obtained by taking the rate expression of HNO$_3$ dissociation and iteratively adjusting it until it matched the data. Essentially identical results were observed in the TD-LIF instrument (R. C. Cohen, personal communication, 2016).

### 3.4 NH$_4$NO$_3$ thermograms

NH$_4$NO$_3$ particles were generated in situ from an aqueous solution, dried, and size selected by a differential mobility analyzer set at 250 nm prior to entering the TD oven. The conversion efficiency was calculated by comparing the measured NO$_2$ concentration in the TD-CRDS instrument to the expected number of NH$_4$NO$_3$ molecules in the aerosol particles, derived from the number and size of the aerosol particles as measured with an ultra-high sensitivity aerosol spectrometer (UHSAS). The measured UHSAS histogram was used, along with the literature value for the density of NH$_4$NO$_3$, to convert particle diameter to particle volume and then to the total number of NH$_4$NO$_3$ molecules. We demonstrate here that the dissociation pathway is NH$_4$NO$_3$ $\rightarrow$ NH$_3$+HNO$_3$, and we assume that NH$_3$ is not converted in any significant fraction. A temperature-dependent baseline NO$_2$ signal is observed when the DMA voltage is set to zero (i.e. when no particles are transmitted), which is attributed to gas-phase HNO$_3$ molecules which have evaporated from the particles and adsorbed to the tubing walls, and which are subtracted from the total signal. Figure 7 shows the measured thermogram of NH$_4$NO$_3$ with the thermogram of gas-phase HNO$_3$ from Fig. 2 overlaid. The close agreement between the two thermograms demonstrates that the dissociation pathway is NH$_4$NO$_3$ $\rightarrow$ NH$_3$+HNO$_3$ and that this reaction is rapid at the temperatures reached in the TD inlet.

For particles that pass through the DMA at a given size set point, the UHSAS measures a size histogram that peaks at a diameter approximately 8 % lower, likely because the NH$_4$NO$_3$ particles are slightly non-spherical, and therefore the electrical mobility diameter is slightly larger than the geometric diameter. This phenomenon has been discussed at length elsewhere (DeCarlo et al., 2004), and we make no attempt to further characterize NH$_4$NO$_3$ particle behavior in the DMA – we have simply taken the UHSAS histogram data to calculate the particle volume, even though this is also subject to slight differences based on the refractive index of NH$_4$NO$_3$. However, if the TD oven were to fail to volatilize and convert all NH$_4$NO$_3$ particles to HNO$_3$ and then to NO$_2$, the measured thermogram would deviate from the HNO$_3$ spectrum at lower temperatures, where perhaps the heat is not sufficient to drive the NH$_4$NO$_3$ out of the condensed phase. The close match between the two is a good indication that the conversion goes to completion. Additionally, Figs. S6 and S7 show a sample NO$_2$ measurement measured by TD-CRDS at 650$^\circ$C as the particle diameter set point is changed. There is no correlation between particle size and conversion efficiency, indicating that the oven is completely converting all particles without a size dependence.

### 3.5 NH$_3$ thermograms

A previous study (Wild et al., 2014) investigated whether ambient levels of ammonia would represent an interference to NO$_2$ conversion and found that it made at most a 1 % difference to the NO$_2$ signal in dry air, but that this effect was suppressed when RH $>$ 10%. We find in the present study that there is a significant interference when ambient levels of both NH$_3$ and O$_3$ are present in the oven, but that this effect is potentially suppressed by other species found in am-
Bient sampling. Figure 8 shows a thermogram of NH$_3$ with and without 100 ppbv O$_3$ present in the oven. The conversion of NH$_3$ to NO$_2$ at 650 $^\circ$C, calculated as the observed NO$_2$ signal relative to the added NH$_3$ concentration, is small without O$_3$. This is consistent with the previous study of Wild et al. (2014). However, when 100 ppbv of O$_3$ is added, the thermogram reaches a maximum molar conversion efficiency of 8%, with an onset near 400 $^\circ$C (red circles). In contrast to the HNO$_3$ thermograms, however, this signal does not appear to plateau at 650 $^\circ$C but rather continues to grow at higher temperatures. This result is similar to the interference reported by Dillon et al. (2002), which was attributed to a reaction between NH$_3$ and O$_3$. The interference is only present when O$_3$ is added to the mixing volume, indicating that the conversion of NH$_3$ must be producing NO, rather than NO$_2$, and is subsequently unimportant to instruments that measure NO$_2$ only, such as TD-LIF instruments. A kinetic model simulation of both experiments is shown in solid lines in Fig. 8. This simulation was carried out with 35 relevant reactions between NH$_3$, O$_3$, and the radicals that are formed from these two species in the oven, with the most important reactions listed below. The reaction between NH$_3$ and O$_3$ is far too slow to be relevant here, and the oven temperature is not high enough to dissociate NH$_3$ to NH$_2$+H ($\Delta H$ = 108 kcal mol$^{-1}$). However, O$_3$ dissociates readily at oven temperatures above 200 $^\circ$C, and once formed the O atoms may react with NH$_3$ to form NH$_2$.

\[
\begin{align*}
\text{O}_3 & \rightarrow \text{O}_2 + \text{O} \\
\text{N} \text{H}_3 + \text{O} & \rightarrow \text{N} \text{H}_2 + \text{OH} \\
\text{N} \text{H}_3 + \text{OH} & \rightarrow \text{N} \text{H}_2 + \text{H}_2 \text{O} \\
\end{align*}
\]  
(R2)

The reactions of NH$_3$ are the slowest steps, but once formed NH$_2$ reacts readily with O atoms.

\[
\begin{align*}
\text{N} \text{H}_2 + \text{O} & \rightarrow \text{HNO} + \text{H} \\
& \rightarrow \text{OH} + \text{H} \\
& \rightarrow \text{N} \text{O} + \text{H}_2 \\
\end{align*}
\]  
(R3)

HNO then reacts with O, OH, and H to form NO or can also directly dissociate to form H + NO.

\[
\begin{align*}
\text{HNO} + \text{O} & \rightarrow \text{OH} + \text{NO} \\
\text{HNO} + \text{OH} & \rightarrow \text{H}_2 \text{O} + \text{NO} \\
\text{HNO} + \text{H} & \rightarrow \text{H}_2 \text{O} + \text{NO} \\
\text{HNO} & \rightarrow \text{H} + \text{NO} \\
\end{align*}
\]  
(R4)

The OH and H atoms formed in reactions (R3) and (R4) then drive Reaction (R2) further. This mechanism takes place entirely in the gas phase and does not take into account any surface-mediated reactions. Many of these reactions have only limited published studies, so the simulation used rate constants that have not been extensively tested. Additionally, to achieve a significant conversion of NH$_3$ to NO, it was necessary to decrease the O and OH wall loss constants in the model. This rudimentary simulation predicts the initial signal increase starting at 300 $^\circ$C, though it has a maximum conversion efficiency of just under 2%, which is below that observed in the experiment. In Fig. 9, we adjusted the amount of added O$_3$, while monitoring the conversion efficiency of NH$_3$ to NO$_2$ at an inlet temperature of 650 $^\circ$C. We find that increasing the O$_3$ increases the conversion, which is consistent with NH$_3$+O being the limiting reaction to make NH$_2$. Figure 9 also demonstrates that the conversion of NH$_3$ is partially quenched by the addition of ambient levels ($\sim$100 ppbv) of CO, likely because the CO + O → CO$_2$ reaction competes with those in Reaction (R2). Figure 10 shows that the average conversion efficiency of NH$_3$ when measured in ambient air in Boulder, CO, in August 2016 (which contains 40–60 ppbv O$_3$, > 80 ppbv CO, ~ 15% RH, and other species) is 0.5 ± 2.4%, or zero to within the 1$\sigma$ error from repeated measurements. This is in contrast to the conversion efficiency of HNO$_3$ in ambient air, shown in the upper right frame of Fig. 10, which is largely unchanged from that measured in zero air. Thus, constituents present in ambient air, such as methane, CO, and water, are possibly suppressing the conversion of NH$_3$ to NO, likely through the reaction with O atoms.

4 Discussion

Using a thermal dissociation cavity ring-down spectrometer, we have quantitatively added reactive nitrogen species to the TD inlet in order to test the efficiency of the thermal conversion of each species to NO$_2$ and the effect of any interferences from other trace gases which may be present in the ambient troposphere. We have determined that the TD-CRDS converts HNO$_3$, N$_2$O$_5$, and NH$_4$NO$_3$ particles to NO$_2$ with 100% efficiency at temperatures above 600 $^\circ$C, but that the onsets of the dissociation are highly dependent on oven residence time. Despite their similar residence times, the
NOAA TD-CRDS and Berkeley TD-LIF instruments measure HNO$_3$ conversion efficiencies ranging from 2.5 to $\sim 8\%$ at 410°C. It is therefore important that the oven residence time is well characterized in instruments designed to selectively detect ANs without interference from HNO$_3$. Even two TD ovens with identical inner volumes may exhibit different response functions if they have different ratios of surface area to volume.

We find that high levels of ambient O$_3$ (>500 ppbv) and CO (>400 ppmv) significantly changed the final conversion efficiency and the onset of the conversion, respectively, of the HNO$_3$ thermogram but that ambient levels of a group of representative VOCs and high RH did not affect the measured thermogram. Modest levels of O$_3$ converted a portion of NH$_3$ to NO$_2$. The conversion mechanism likely arises from a gas-phase reaction between oxygen atoms and NH$_3$ which produces NO. To our knowledge, the NH$_3$+O$_3$ reaction in TD ovens has not been studied in detail, but previous studies of NH$_3$ conversion in catalytic converters have noted similar results to those presented here – water and CO suppress the NH$_3$ conversion to NO, while O$_3$ enhances it (Fahey et al., 1985; Kliner et al., 1997). If not quenched by other species present in ambient air, this effect could represent a potentially significant interference in field sampling for instruments that are sensitive to NO directly or via conversion to NO$_2$. For example, at 50 ppbv O$_3$, the 6% conversion of NH$_3$ would present an interference of more than 10% if NH$_3$ / NO$_3$ > 1.7, which is not an uncommon condition in agricultural regions. This signal was suppressed in ambient air, indicating that NH$_3$ may not interfere with NO$_3$ under most conditions. However, ambient air in Boulder is not representative of all sampling conditions, and, since the species responsible for quenching the reaction remains unclear, more work must be done to better understand the mechanism of the NH$_3$ / O$_3$ thermal reaction. This result, along with the others detailed above, serves to emphasize that great care must be taken to characterize the potential interferences in TD NO$_3$-conversion ovens.

The measured N$_2$O$_5$ thermogram exhibits a double dissociation curve, corresponding to the initial dissociation of N$_2$O$_5$ to NO$_2$ and NO$_3$ and the subsequent dissociation of NO$_3$. Our results indicate that the mechanism of the second step is NO$_3$ $\rightarrow$ NO$_2$+O, in contrast to earlier literature that reported NO$_3$ $\rightarrow$ NO + O$_2$ as the dominant mechanism. To our knowledge, this is the first published thermogram of NO$_3$. TD-NO$_3$ instruments often operate in the daytime when N$_2$O$_5$ is not a significant fraction of NO$_3$, though some groups have operated at night and have typically assumed complete conversion to NO$_2$+ NO$_3$ at the TD inlet set point for PNs (Di Carlo et al., 2013) and complete conversion to 2NO$_2$+O at the set point for HNO$_3$ (Wild et al., 2014). These results confirm that there is approximately quantitative conversion at these set points, though there are slight deviations from 100% conversion near the PN set point. Therefore, care must be taken to select a set point carefully and ensure complete conversion at that temperature. However, this interference would only be significant during nighttime or during very cold weather sampling.

The thermogram of particulate ammonium nitrate matches the thermogram of HNO$_3$, within the margin of error of the UHSAS measurement. TD ovens have not typically been used explicitly for particle detection, with a few exceptions (Voisin et al., 2003; Smith et al., 2004; Rollins et al., 2010), though very fine particles may be sampled by the inlet, unless they are excluded aerodynamically or physically. These results demonstrate that the volatile portion of the particulate ammonium nitrates will be driven into the gas phase at low oven temperatures, consistent with Rollins et al. (2010), who used a denuder to remove gas-phase nitrates and to detect aerosol organic nitrates in a 325°C oven. Their results indicate it is likely that particulate organic nitrates would be converted to NO$_2$ with 100% efficiency in the NOAA TD-CRDS, but this result has not been explicitly tested here. Other NO$_3$ salts might also be detected via thermal dissociation, although it is expected that they would be non-volatile at the temperatures of these TD-inlets. Bertram and Cohen (2003) examined NaNO$_3$ and determined that those particles would not be detected in TD inlets. However, these studies measured pure aerosols, and results may vary with heterogeneously mixed particles with multiple components. The initial dissociation of NH$_2$NO$_3$ will produce an NH$_3$ molecule in addition to an HNO$_3$ molecule, which means that particles may be subject to the same NH$_3$ / O$_3$ interference when sampling in ambient air, which was not considered in this study. Additionally, the particles sampled in this paper were generated and injected directly into the inlet. The efficiency of particle sampling in ambient air will depend on particle size and inlet design, particularly during aircraft measurements. In future studies, a TD inlet that either effectively samples aerosol or effectively excludes aerosol (such
as a cyclone), or a combination of the two, could be used to specifically measure aerosol nitrates, which may make up a substantial fraction of NO\textsubscript{y}, particularly in polluted wintertime urban atmospheres.

Based on the results of this paper, we make the following three recommendations. (1) TD ovens should be characterized with the appropriate reactive nitrogen compounds regularly at the oven set points using the oven residence time and gas pressure that will be used in ambient sampling. This is especially important given the findings of the Berkeley group regarding impurities found in otherwise identical ovens, as discussed in Sect. 3.1. (2) In addition to the AN and PN calibrations recommended by Day et al. (2002), Thieser et al. (2016), and others, these calibrations should include HNO\textsubscript{3}. HNO\textsubscript{3} calibration will be especially important if sampling in regions where HNO\textsubscript{3} is in large excess over other NO\textsubscript{y} species. (3) Potential non-NO\textsubscript{y} species such as NH\textsubscript{3} should also be regularly introduced into the inlet under conditions where O\textsubscript{3} is present in ambient air to check for potential conversion. These recommendations are similar to those detailed in Bradshaw et al. (1998). The results of Fig. 9 indicate that calibration results may also vary significantly when sampling in ambient air, due to the large number of possible gas-phase reactions available to the wide variety of trace atmospheric species. The last step is particularly important in instruments that detect NO as well as NO\textsubscript{2}. Comprehensive calibration of these interferences is key to these instruments’ NO\textsubscript{y} measurement accuracy, which in turn will provide valuable information about tropospheric NO\textsubscript{4} chemistry.

Data availability. Data is available upon requests made to Steven Brown (steven.s.brown@noaa.gov).

The Supplement related to this article is available online at doi:10.5194/amt-10-1911-2017-supplement.

Competing interests. The authors declare that they have no conflict of interest.

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Supplement of

Evaluation of the accuracy of thermal dissociation CRDS and LIF techniques for atmospheric measurement of reactive nitrogen species

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Figure S1. A sample oven temperature profile measured with a 2.0 slpm flow rate through the TD oven inlet, while the oven was set at 650 °C. Distance is measured from end of the quartz tube. The first ~5 cm are not heated, and the heated portion stretched from approximately 5 – 42 cm, with a cooling region from 42 – 63 cm.

Figure S2. Log scale plot of conversion efficiency vs residence time. This plot is similar to the linear plot in Fig. 3, but is presented in log space to highlight small differences in the low conversion efficiency region.
Figure S3. HNO₃ thermograms taken at low oven pressure (~250 mbar). As in Fig. 2, the onset of signal shifts to higher temperatures at faster flow rates.

Figure S4. A simulated O₃ dissociation curve to O. These results indicate that O₃ dissociates to form O at the entire temperature range relevant for AN and HNO₃ TD ovens, but that if allowed to recombine, only ~40% will remain as O₂ + O. If wall loss is permitted, nearly all O atoms would be lost to reactions with the wall.
Figure S5. The measured NO\textsubscript{2} mixing ratios as \textasciitilde 15 ppbv NO in zero air is introduced to the NOy thermal dissociation inlet is shown in red. The green and yellow lines represent the addition of O\textsubscript{3} in two places: ppbv levels before the NO sample enters the TD inlet (green) and ppmv levels in the mixing volume just prior to entering the CRDS cavity (yellow). The mixing volume O\textsubscript{3} converts any NO to NO\textsubscript{2} prior to detection, so when this O\textsubscript{3} is added (such as between 4:30 and 5pm), the measured NO\textsubscript{2} is \textasciitilde 15 ppbv, as expected. When O\textsubscript{3} is not added to either the TD inlet or the mixing volume (such as between 4:20 and 4:30pm), no NO\textsubscript{2} signal is observed. However, when O\textsubscript{3} is added to the TD inlet, but not to the mixing volume, and the oven is at 650 °C, (such as between 5:05 and 5:15), approximately 2.25 ppbv NO\textsubscript{2} is observed, indicating that this NO\textsubscript{2} is formed by reaction of O\textsubscript{3} and NO in the oven. This has no effect on this TD-CRDS instrument, as any NO would be converted to NO\textsubscript{2} in the mixing volume region immediately following the TD oven. But techniques such as TD-LIF or TD-CRDS in which NO is not converted to NO\textsubscript{2} would see a \textasciitilde 15\% conversion of ambient NO to NO\textsubscript{2}, which must be accounted for.

Figure S6. NO\textsubscript{2} signal (red) detected in the NOy channel of the TD-CRDS instrument when NH\textsubscript{4}NO\textsubscript{3} aerosol is introduced to the inlets on two separate occasions. The blue trace is the expected NH\textsubscript{4}NO\textsubscript{3} concentrations derived from the UHSAS measurement of the particle size distribution. The yellow indicates set DMA diameter.
Figure S7. NO$_2$ mixing ratios as measured by the TD-CRDS instrument, and derived NO$_2$ mixing ratios from the UHSAS size distribution of NH$_4$NO$_3$ particles, colored by DMA selected diameter. Here, “0 nm” refers to setting the DMA voltage to 0, which nominally does not allow any particles through. A linear trend is shown in the scatter plot, with no dependence on particle size, emphasizing that complete conversion of the NH$_4$NO$_3$ particles is observed in the TD oven.

Figure S8. A representative thermogram for each of the four major species studied. All were at ambient pressure and a flow rate of 1.9 slpm, except for the high temperature region of the N$_2$O$_5$ trace, which was taken at 1 slpm. The NH$_3$ thermogram was taken with 100 ppbv of O$_3$ in the TD inlet.
Table S1. Reactions used in HNO₃ box model

Rate laws are presented in table form, where the parameters listed can be inserted into the equation \( k(T) = A(298/T)^{n_c}e^{(Ea/RT)} \). For third order equations, a high pressure limit is also given. For third order reactions, a value of \( F_c = 0.6 \) was used. \( E_a/R \) is in units of K⁻¹. \( A \) is in units of cm³ molec⁻¹ s⁻¹ for second order reactions and cm⁶ molec⁻² s⁻¹ for third order reactions. The rate expression at 298 and 950 K (max and min temperatures used in each thermogram) are given. The technique (experimental, theoretical, combination/review) is given, along with the temperature range and reaction order. Temperature ranges with approximates are based on JPL combinations of multiple studies and are thus approximate.

Reactions used in HNO₃ box model

| Reaction | Rate Expression | A₀ | n₀ | Ea/R₀ | Aₓ | nₓ | Ea/Rₓ | Ref. | k(298K) | k(950K) | Technique | Temp range | Order |
|----------|-----------------|----|----|-------|----|----|-------|------|---------|----------|------------|------------|----------|
| HNO₃ → NO₂ + OH | A₀ = 1.83e-4, n₀ = -1.98, Ea/R = 24054, Aₓ = 1.26e-15, nₓ = 24054 | [1] | 5.51e-21 | 409.81 | Expt | 295-1200 | 2 |
| NOₓ + NO → N₂O₃ | A₀ = 2.0e-30, n₀ = -4.4, Ea/R = 0, Aₓ = 1.4e-12, nₓ = -0.7 | [2] | 1.15e-12 | 5.66e-14 | Expt | ~250-400 | 3 |
| NOₓ + O → NOₓ | A₀ = 2.50e-31, n₀ = -1.8, Ea/R = 2.2e-11, Aₓ = -0.7 | [2] | 2.74e-12 | 1.72e-13 | Expt | ~200-400 | 3 |
| NOₓ + OH → HNO₃ | A₀ = 1.80e-30, n₀ = -3, Ea/R = 2.80e-11, Aₓ = 0 | [2] | 9.28e-12 | 3.29e-13 | Expt | ~200-600 | 3 |
| NOₓ + H₂O → HO₂NO₂ | A₀ = 2.00e-31, n₀ = -3.4, Ea/R = 2.90e-12, Aₓ = -1.1 | [2] | 2.53e-12 | 2.45e-14 | Expt | ~200-350 | 3 |
| NO + O → NO₂ | A₀ = 9.00e-32, n₀ = -1.5, Ea/R = 3.00e-11, Aₓ = 0 | [2] | 1.32e-12 | 9.33e-14 | Expt | ~200-500 | 3 |
| NO + OH → HONO | A₀ = 7.00e-31, n₀ = -2.6, Ea/R = 3.60e-11, Aₓ = -0.1 | [2] | 6.31e-12 | 2.06e-13 | Expt | ~200-500 | 3 |
| NO + H → HNO | A₀ = 1.22e-31, n₀ = -1.17, Ea/R = 211.6, Aₓ = N/A | [3] | 1.13e-12 | 1.37e-13 | Review | 230-4200 | 3 |
| O₃ → O₂ + O₂ | A₀ = 7.16e-10, n₀ = 11200, Ea/R = N/A, Aₓ = N/A, nₓ = N/A | [4] | 6.49e-7 | 10000 | Review | 300-3000 | 2 |
| O₂ + H → HO₂ | A₀ = 4.40e-32, n₀ = -1.3, Ea/R = 7.50e-11, Aₓ = 0, nₓ = 0 | [2] | 7.37e-13 | 5.88e-14 | Theory | 300-3000 | 3 |
| O + H → OH | A₀ = 4.36e-32, n₀ = -1, Ea/R = N/A, Aₓ = N/A, nₓ = N/A | [5] | 8.20e-13 | 8.55e-14 | Review | 300-2500 | 3 |
| 2OH → H₂O₂ | A₀ = 6.90e-31, n₀ = -1, Ea/R = 2.60e-11, Aₓ = 0 | [2] | 5.42e-12 | 1.06e-12 | Expt | ~200-700 | 3 |
| OH + H → H₂O | A₀ = 4.38e-30, n₀ = -2, Ea/R = N/A, Aₓ = N/A, nₓ = N/A | [6] | 8.28e-11 | 2.79e-12 | Review | 300-3000 | 3 |
| HO₂ + H₂O → H₂O₂ + O₂ | A₀ = 3.00e-13, n₀ = 0, Ea/R = -460, Aₓ = N/A, nₓ = N/A | [2] | 0.0858 | 0.00343 | Expt | ~250-1200 | 3 |
| N₂O₃ → NO + NO₂ | A₀ = 1.90e-7, n₀ = -8.7, Ea/R = 4800, Aₓ = 4.7e15, nₓ = 0.4 | [7] | 4880 | 10000 | Review | 225-300 | 2 |
| HO₂NO₂ → HO₂ + NO₂ | A₀ = 4.10e-5, n₀ = 0, Ea/R = 10650, Aₓ = 4.8e15, nₓ = 0 | [8] | 11170 | 0.0738 | 10000 | Review | 260-300 | 2 |
| HONO → OH + NO | A₀ = 1.98e-3, n₀ = -3.8, Ea/R = 25257, Aₓ = 1.09e16, nₓ = -1.23 | [3] | 25016 | 0.141e-21 | 171.88 | Review | 300-2500 | 2 |
| HNO → NO + H | A₀ = 5.48e-7, n₀ = -1.24, Ea/R = 25257, Aₓ = N/A, nₓ = N/A | [3] | 1.67e-24 | 1.07634 | Review | 300-2500 | 2 |
| H₂O → 2OH | A₀ = 2.03e-3, n₀ = -4.86, Ea/R = 26820, Aₓ = N/A, nₓ = N/A | [5] | 3.34e-27 | 0.00125 | Review | 500-2500 | 2 |
| N₂O₃ → NO₂ + NO₁ | A₀ = 1.30e-3, n₀ = -3.5, Ea/R = 11000, Aₓ = 9.7e14, nₓ = 0.1 | [8] | 11080 | 0.0498 | 10000 | Expt | 200-400 | 2 |
| HNO₂ + OH → HO₂ + NO₃ | A₀ = 6.50e-34, n₀ = -1335, Ea/R = 2.70e-17, Aₓ = 0, nₓ = -2199 | [2]** | 1.12e-13 | 3.95e-14 | Expt | ~200-350 | 3 |
| 2NO₂ → 2NO + O₂ | A₀ = 8.5e-13, n₀ = 0, Ea/R = 2450 | [2] | 0 | 2.29e-16 | 5.98e-14 | Expt | 298-329 | 2 |
| NOₓ + NO → 2NO₂ | A₀ = 1.79e-11, n₀ = 0, Ea/R = -109.45 | [9] | 2.58e-11 | 2.02e-11 | Review | 220-4400 | 2 |
| NOₓ + O → O₂ + NO₂ | A₀ = 1.00e-17, n₀ = 0, Ea/R = 0 | [2] | 1e-11 | 1e-11 | Expt | 298 | 2 |
| NOₓ + OH → HO₂ + NO₂ | A₀ = 2.2e-11, n₀ = 0, Ea/R = 0 | [2] | 2.2e-11 | 2e-11 | Expt | 298 | 2 |
| NOₓ + H₂O → O₂ + HNO₃ | A₀ = 3.5e-12, n₀ = 0, Ea/R = 0 | [2] | 3.5e-12 | 3.5e-12 | Expt | 298 | 2 |
| NOₓ + H → NO₂ + OH | A₀ = 9.4e-11, n₀ = 0, Ea/R = 0 | [10] | 9.4e-11 | 9.4e-11 | Expt | 298 | 2 |
| Reaction                                      | Time Constant (s) | Temperature (K) | Product / Theory | Reference |
|-----------------------------------------------|-------------------|-----------------|------------------|-----------|
| **OH** + **H** → **H** + **O**                | 1.69 × 10^13      | ~250            | Theory           | 1         |
| **OH** + **H** → **H** + **O**                | 3.01 × 10^13      | ~275            | Expt             | 2         |
| **OH** + **H** → **H** + **O**                | 3.85 × 10^13      | ~300            | Expt             | 3         |

Note: The time constants and temperatures are approximate and may vary.

**Review**

- Theory
- Expt

**Theory**

- Reaction rates are influenced by temperature and pressure.
- Theoretical models are used to predict reaction rates.

**Expt**

- Experimental data is collected in controlled environments.
- Reaction rates are determined through experiments.\n
**See main text**

- Additional details are provided in the main text of the document.

**OH** → Wall

- Reaction rate: 46 s⁻¹

**O → Wall**

- Reaction rate: 70 s⁻¹

**See main text**

- Additional information is provided in the main text of the document.
Reactions used in N₂O₅ box model

| Reaction          | Rate Expression       | A₀      | n₀     | Eₐ/Rₑ | Aₑ | nₑ     | Eₐ/Rₑ | Ref.      | k(298K)    | k(950K)    | Technique | Temp range | Order |
|-------------------|-----------------------|---------|--------|-------|-----|--------|-------|-----------|------------|------------|-----------|-----------|-------|
| NO₂ + NO₂ → N₂O₅ | 2.0e-30  -4.4  0    1.4e-12 -0.7  0     | [2]     | 1.17e-12  3.66e-14 | Exp  | ~250-400 | 3       |
| NO₂ + O → NO₃    | 2.50e-31  -1.8  0    2.2e-11 -0.7  0     | [2]     | 2.84e-12  1.72e-13 | Exp  | ~200-400 | 3       |
| NO₂ + O → NO₃    | 9.00e-32  -1.5  0    3.0e-11 -0.7  0     | [2]     | 1.36e-12  9.33e-14 | Exp  | ~200-500 | 3       |
| NO₂ + O → NO₃    | 6.00e-34  -2.4  0    0     0     0     | [2]     | 1.21e-14  2.44e-16 | Exp  | ~200-270 | 3       |
| O₂ + O → O₃      | 5.21e-35  0  -900     0     0     0     | [5]     | 2.13e-14  8.33e-16 | Exp  | 200-400  | 3       |

Reactions used in NH₃ box model

| Reaction          | Rate Expression       | A₀      | n₀     | Eₐ/Rₑ | Aₑ | nₑ     | Eₐ/Rₑ | Ref.      | k(298K)    | k(950K)    | Technique | Temp range | Order |
|-------------------|-----------------------|---------|--------|-------|-----|--------|-------|-----------|------------|------------|-----------|-----------|-------|
| HNO → NO + H      | 5.48e-7  -1.24 25257  N/A  N/A  N/A | [3]     | 9.75e-12  1.076 | Exp  | 300-2500 | 2       |
| NH₃ + O → NH₃ + OH | 2.87e-13  2.1  0     | [23]    | 6.04e-18  3.00e-13 | Exp  | 298-2000 | 2       |
| NH₃ + OH → NH₄ + H₂O | 4.48e-13  1.8  0     | [24]    | 1.16e-13  2.58e-12 | Exp  | 225-2350 | 2       |
| NH₃ + O → NH₂O + O₂ | 4.9e-12  0  1000     | [25]    | 8.71e-14  1.66e-12 | Exp  | 250-380  | 2       |
| NH₃ + O → NO + H₂  | 7.47e-11  0  0       | [23]    | 7.47e-11  7.47e-11 | Exp  | 298-3000 | 2       |
| NH₃ + O → OH + NH  | 1.16e-11  0  0       | [23]    | 1.16e-11  1.16e-11 | Exp  | 298-3000 | 2       |
| NH₃ + O → NO + H₂  | 8.30e-12  0  0       | [23]    | 8.30e-12  8.30e-12 | Exp  | 298-3000 | 2       |
| NH₃ + NH₂ → N₂H₄  | 1.96e-29  -3.9 0     | [26]    | 1.12e-10  1.60e-10 | Exp  | 200-400  | 3       |
| NH₃ + OH → NH₂OH   | 6.77e-10  -3.23 673   | [27]    | 8.30e-11  8.65e-12 | Thry  | 200-3000 | 2       |
| NH₃ + O → NH + H₂O | 7.69e-13  1.5  -230   | [23]    | 1.46e-12  5.33e-12 | Exp  | 250-3000 | 2       |
| NH₃ + O → NH₃ + O  | 4.95e-15  2.6  -870   | [23]    | 1.01e-13  2.36e-13 | Exp  | 298-2000 | 2       |
| NH₃ + NH₂ → NH₃ + H | 1.5e-10  -0.27 -38.4  | [28]    | 1.84e-10  1.15e-10 | Thry  | 200-2500 | 2       |
| NH₃ + NH₂O → NH₄ + NH₃ | 1.42e-15  4  -13.03  | [28]    | 7.01e-16  1.29e-13 | Thry  | 300-2500 | 2       |
| NH₃ + O → Products | 2.01e-14  0  0       | [29]    | 2.01e-14  2.01e-14 | Exp  | 298     | 2       |
| NH₃ + OH → H₂O + HNO | 1.66e-12  0  0       | [30]    | 1.66e-12  1.66e-12 | Thry  | 80-420  | 2       |
\[ \text{NH}_2\text{OH} \rightarrow \text{OH} + \text{NH}_2 \] 0.16 -5.96 33555 28 2.09e-40 0.195 Theory 450-2500 2

\[ \text{NH} + \text{OH} \rightarrow \text{HNO} + \text{H} \] 3.32e-11 0 0 23 3.32e-11 3.32e-11 Review 298-3000 2

\[ \text{NH}_2\text{OH} + \text{NH} \rightarrow \text{NH}_3 + \text{NH}_3 \] 3.73e-16 -4.4 786.6 28 6.82e-18 2.24e-14 Theory 400-2500 2

\[ \text{NO} + \text{O} \rightarrow \text{NO}_2 \] 9.00e-32 -1.5 0 3.00e-11 0 0 2 1.93e-12 9.33e-14 Expt ~200-500 3

\[ \text{NO} + \text{O}_2 \rightarrow \text{NO}_2 + \text{O}_2 \] 3.00e-12 0 1500 2 7.11e-15 5.91e-13 Expt ~200-400 2

\[ \text{NO}_2 + \text{O} \rightarrow \text{NO}_3 \] 5.10e-12 0 -210 2 4.00e-12 4.00e-12 Expt ~200-400 3

\[ \text{NO}_2 + \text{O}_2 \rightarrow \text{NO}_3 + \text{O}_2 \] 1.2e-13 0 2450 2 6.19e-18 8.44e-15 Expt ~250-350 2

\[ \text{NO}_3 \rightarrow \text{NO}_2 + \text{O} \] **See main text

\[ \text{NO} + \text{H} \rightarrow \text{HNO} \] 1.22e-31 -1.17 211.6 N/A N/A N/A 2 1.46e-12 1.57e-13 Expt 230-4200 3

\[ \text{O}_2 \rightarrow \text{O}_2 + \text{O} \] 7.16e-10 0 11200 N/A N/A N/A 4 4.02e-10 10000 Review 300-3000 2

\[ \text{NO}_3 + \text{NO} \rightarrow \text{NO}_2 + \text{NO}_2 \] 1.79e-11 0 -109.45 9 2.78e-11 2.02e-11 Review 220-4400 2

\[ \text{NO}_3 + \text{O} \rightarrow \text{O}_2 + \text{NO}_2 \] 1.00e-17 0 0 2 1.00e-11 1.00e-11 Expt 298 2

\[ \text{NO}_3 + \text{OH} \rightarrow \text{HO}_2 + \text{NO}_2 \] 2.2e-11 0 0 2 2.20e-11 2.20e-11 Expt 298 2

\[ \text{HNO} + \text{H} \rightarrow \text{NH}_2 + \text{O} \] 1.05e-9 -0.3 14673 23 2.32e-35 9.37e-17 Review 550-3000 2

\[ \text{HNO} + \text{H} \rightarrow \text{OH} + \text{NH} \] 2.41e-9 -0.5 9009 23 4.66e-25 8.19e-14 Review 350-3000 2

\[ \text{HNO} + \text{H} \rightarrow \text{H}_2 + \text{NO} \] 3.01e-11 0 500 2 4.01e-12 1.75e-11 Review 298-2000 2

\[ \text{O} + \text{HNO} \rightarrow \text{OH} + \text{NO}_2 \] 6.00e-11 0 0 3 6.00e-11 6.00e-11 Expt 298-2000 2

\[ \text{OH} + \text{HNO} \rightarrow \text{H}_2\text{O} + \text{NO} \] 8.00e-11 0 500 3 1.07e-11 4.65e-11 Review 300-2000 2

\[ \text{NH}_2 + \text{NO} \rightarrow \text{N}_2 + \text{H}_2\text{O} \] 5.96e-11 -2.37 436 31 1.61e-11 2.59e-12 Review 400-1900 2

\[ \text{NH}_2 + \text{NO} \rightarrow \text{N}_2\text{O} + \text{H}_2\text{O} \] 7e-12 -1.44 135 32 5.34e-12 1.20e-12 Expt 300-910 2

\[ \text{NH}_2 + \text{NO}_2 \rightarrow \text{NO} + \text{NH}_3 \] 5.81e-12 0 0 33 5.81e-12 5.81e-12 Expt 850-1350 2

\[ \text{O} \rightarrow \text{Walls} \] ~70 s\(^{-1}\) **See main text

\[ \text{OH} \rightarrow \text{Walls} \] ~46 s\(^{-1}\) **See main text

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