The effect of acid treatment on the active sites and reaction intermediates of the low-cost TS-1 in propylene epoxidation†

Guang Xiong, Qianying Jia, Yuanyuan Cao, Liping Liu and Zhendong Guo

This study investigated the roles of the different titanium species of low-cost TS-1 in propylene epoxidation and the influence of acid treatments. The low-cost TS-1 zeolites with different titanium species were synthesized using the hydrothermal method and characterized by ultraviolet (UV)-Raman, X-Ray Diffraction (XRD), ultraviolet visible diffuse reflectance spectroscopy (UV-Vis), N2 physical absorption and NH3 temperature programmed desorption (NH3-TPD) techniques. The roles of the different titanium species in the low-cost TS-1 samples were investigated by gas chromatography-Raman spectrometry (GC-Raman) during the propylene epoxidation process. The framework titanium species was found to be active for propylene epoxidation, while the extra-framework Ti species were found to be harmful for propylene epoxidation due to their acidity. The extra-framework Ti species can be removed by acid treatments. It was found that the acid treatment of the as-synthesized TS-1 is more effective since the amorphous TiO2 was not transformed into anatase TiO2 upon calcination. Strong acids, such as HCl, HNO3 and H2SO4, are more efficient for the elimination of the extra-framework TiO2, but do not significantly affect the framework titanium species. After treatment with an acid of a suitable concentration, the amount of the active intermediate species Ti\(=\)O\(\equiv\)OH(\(\eta^2\)) can be increased, and a higher conversion of propylene and yield of PO can be achieved.

1. Introduction

The system of titanium silicalite (TS-1) and H\(_2\)O\(_2\) has been an important topic in green catalytic chemistry for decades because of its unique catalytic properties in oxidation reactions under mild conditions.\(^1\text{-}^5\) The classical method was used to produce TS-1 with the crystal size of 100–200 nm, which exhibited good catalytic properties. However, the template tetrapropyl ammonium hydroxide (TPAOH) used in the classical method is expensive, which restrains its applications in industry. Some attempts have been made to reduce the amount of the template TPAOH required. Deng\(^6\) carried out hydrothermal synthesis of TS-1 with a lower ratio of TPAOH/SiO\(_2\) in two-step and multistep hydrolysis processes by fine tuning the nucleation and growth step during crystallization, which showed good activity in the oxidation of alkene and ammonoximation of ketone. To further reduce the cost of the catalyst, tetrapropyl ammonium bromide (TAPBr) was used as a template for the synthesis of TS-1.\(^7\) However, the catalytic performance of the low-cost TS-1 is not as good as that of the classical TS-1. Therefore, post-treatments have been used to further improve the catalytic properties of the low-cost TS-1. Li\(^8\) reported the acid treatment of the low-cost TS-1, and the catalytic activity in the propylene oxidation reaction showed a large improvement because of the elimination of the non-framework titanium species. In addition, the alkali treatment is a common method in improving the catalytic performance of the TS-1 zeolite. Tsai\(^9\) reported the alkali treatment of TS-1 using NaOH, leading to the generation of the mesopore and subsequently an increase in the catalytic activity. Tuel\(^10\text{-}^11\) put forward the dissolution-recrystallization method using the TPAOH to improve the diffusion of TS-1.

In addition, the roles of different titanium species in the classical TS-1 during the propylene epoxidation process have been studied.\(^12\text{-}^13\) It was accepted that the isolated titanium species in the framework of the TS-1 zeolite is the active site for the selective oxidation. The non-framework Ti species is harmful for the epoxidation reactions. It was found that the acidity of the amorphous Ti species is stronger than that of the anatase TiO\(_2\), which leads to undesired side reaction.\(^13\) For the low-cost TS-1 zeolite, the distribution of the titanium species is more complicated. Therefore, to improve its catalytic properties, a systematic study on the distribution and the roles of the different titanium species, before and after the post-treatment, are highly required to be known.

Raman spectroscopy has been proven to be a powerful tool to identify the different Ti species by changing the wavelength of
the excitation source, particularly under reaction conditions.\textsuperscript{13-16} Three resonance enhanced Raman bands at 490, 530, and 1125 cm\textsuperscript{-1} obtained with the use of a 244 nm laser line are the typical peaks of the isolated tetrahedral titanium species in the framework of TS-1. In the spectra excited by the 325 and 532 nm lines, the bands at 149, 390, 515, and 637 cm\textsuperscript{-1} are ascribed to anatase TiO\textsubscript{2}. The band at 700 cm\textsuperscript{-1} was assigned to the amorphous Ti species. Raman spectroscopy has also been used to investigate the reaction intermediates on the TS-1 for propylene epoxidation. The reaction intermediate Ti–OOH(\(\eta^2\)) is found to be crucial for propylene epoxidation, whose typical peak is located at 837 cm\textsuperscript{-1}.\textsuperscript{16}

Our previous studies mainly focused on the classical TS-1 when the expensive TPAOH was used as a template. In this study, the low-cost TS-1 zeolite containing different titanium species was synthesized by changing the Ti/Si ratio and synthesis conditions. Then, the technique of gas chromatography-Raman spectroscopy (GC-Raman)\textsuperscript{13} was used to study the relationship between the amount of active intermediate, the product propylene epoxide (PO) and the conversion of propylene. The roles of different titanium species in low-cost TS-1 for propylene epoxidation are discussed herein. Furthermore, the post treatment with different acids was used to eliminate the extra-framework Ti species of the TS-1. The effects of the acid treatment on the Ti distribution, the reaction intermediates and the catalytic properties were investigated using the GC-Raman technique.

2. Experimental

2.1 Synthesis

2.1.1 Materials. Chemical reagents included colloidal silica (30 wt%, SiO\textsubscript{2}) (CP, Qingdao Chengyu Chemical Co., Ltd.), titanium tetrachloride (TiCl\textsubscript{4}) (AR, Damao Chemical Co., Ltd.), tetrapropylammonium hydroxide (TPAOH, 1.23 M solution in water) (Shanghai Cairui Chemical Co., Ltd.), tetrapropylammonium bromide (TPABr) (CP, Shanghai Cairui Chemical technology Co., Ltd.), isopropyl alcohol (IPA) (AR, Tianjin Fuchun Chemical Co., Ltd.), and ethylamine (65 wt%, EA) (AR, Tianjin Fuchun Chemical Co., Ltd.).

2.1.2 Synthetic procedure. TiCl\textsubscript{4} was hydrolyzed in IPA. The colloidal silica and deionized water were mixed. Hydrolyzed TiCl\textsubscript{4} was added dropwise to the colloidal silica solution. Then, the template TPABr, the base EA, the seed (nanosized, synthesized according to the literature)\textsuperscript{3} and deionized water were added to the mixture. Finally, the gel was crystallized at 170 °C for 3 days in a 100 mL autoclave. The molar compositions of the final synthesis gels were as follows: 1.0SiO\textsubscript{2} : (0–0.3)TiO\textsubscript{2} : (0.1–0.3)TPABr : 30 H\textsubscript{2}O : 1.0 IPA : 0.15 ethylamine. The solid product was filtered, washed with distilled water, dried at 100 °C overnight and calcined at 550 °C for 10 h to remove the template. TS-1 samples with different titanium distributions were synthesized by adjusting the SiO\textsubscript{2}/TiO\textsubscript{2} ratios.

2.2 Acid treatment

The TS-1 sample with a SiO\textsubscript{2}/TiO\textsubscript{2} molar ratio of 30 was treated for 24 h with an acid modifier at a liquid to solid ratio of 50 mL g\textsuperscript{-1}. Following this, the solution was centrifuged, washed with distilled water, dried at 100 °C overnight and calcined at 550 °C for 10 h.

2.3 Characterization

X-ray powder diffraction (XRD) patterns were recorded on a Rigaku D/MAX-2400 using Cu K\textsubscript{z} radiation with a scanning rate of 4° min\textsuperscript{-1}. Ultraviolet-visible diffuse reflectance spectra (UV-Vis) were obtained on a SHIMADZU UV-240 spectrometer using BaSO\textsubscript{4} as a reference.

Nitrogen physisorption measurements were performed on a Quantachrome Autosorb-1-MP adsorption porosimeter at 77 K. All samples were degassed at 623 K for 3 h under vacuum. The specific surface area and the micropore volume were calculated by the BET method and the t-plot method, respectively. The total pore volume was determined at a relative partial pressure P/P\textsubscript{0} of 0.99.

Scanning electron microscopy (SEM) was carried out on a Hitachi S-4800 instrument operating at 3 kV. The NH\textsubscript{3}-TPD was performed on a ChemBET 3000 chemisorption apparatus from Quantachrome. The rate of ammonia desorption was monitored continuously with a thermal conductivity detector (TCD).

Raman spectra were recorded on a DL-2 Raman spectrometer with a collection time of 300 s. A 244 nm line of LEXEL LASER and 325 nm line of a He–Cd laser were used as excitation sources. The laser power at the samples was less than 5 mW. An Acton triple monochromator was used as a spectrometer for Raman scattering. The spectra were collected using a Priston CCD detector. During the in situ experiments, the TS-1 sample (0.05 g) was moved into a stainless steel cell equipped with a quartz window after the addition of H\textsubscript{2}O\textsubscript{2}/H\textsubscript{2}O/CH\textsubscript{3}OH solution. Propylene (3% propylene and 97% helium gas in volume fraction) was introduced into the cell at a flow rate of 25 mL min\textsuperscript{-1}. The spectra during the reaction process were recorded by the UV-Raman spectrometer. Moreover, the component analysis of the output gas was detected on a GC 9790 gas chromatograph, using a flame ionization detector and a capillary column (PEG-20M, 30 m). The concentration of propylene oxide (PO) was presented directly by its peak area in the GC spectra. The peak area was integrated by the OriginPro (8.0) program.

3. Results and discussion

3.1 Catalyst characterization

3.1.1 XRD. In this study, to understand the role of the framework and non-framework Ti species of the low-cost TS-1, the TS-1 with the SiO\textsubscript{2}/TiO\textsubscript{2} ratios of 30 and 120 were synthesized. The TS-1 (SiO\textsubscript{2}/TiO\textsubscript{2} ratio = 120) was expected to contain only framework Ti species, while the TS-1 (SiO\textsubscript{2}/TiO\textsubscript{2} ratio = 30) should contain both framework and non-framework Ti species. Both the samples can be used to study the effect of non-framework Ti species of low-cost TS-1. Furthermore, the TS-1 samples with the SiO\textsubscript{2}/TiO\textsubscript{2} ratios of 100, 110, and 120 were
used to study the role of the framework titanium species, which will be discussed later in the ESI (see part A in the ESI†).

The XRD patterns of the TS-1 samples with different SiO₂/TiO₂ ratios are shown in Fig. 1. Both samples exhibit the characteristic peaks at 2θ = 7.8°, 8.8°, 23.2°, 23.8° and 24.3°, which are typical for MFI topology.

3.1.2 UV-Vis. UV-Vis spectra of the TS-1 samples with different SiO₂/TiO₂ ratios are shown in Fig. 2. The three adsorption peaks located at 210–220, 270 and 320 nm are assigned to the tetrahedrally coordinated framework Ti species, amorphous Ti species, and anatase TiO₂, respectively. It is clear that the TS-1-30 sample consists of the framework Ti species, amorphous Ti species, and anatase TiO₂, while the TS-1-120 sample contains only the framework Ti species. Moreover, the amount of framework titanium species in TS-1-30 is higher than that of the TS-1-120 sample.

3.1.3 Raman. Fig. 3 shows the Raman spectra of the TS-1 samples with different SiO₂/TiO₂ ratios collected with a 244 nm laser line. The peaks at 380, 490, 530, 700, 960 and 1125 cm⁻¹ are observed in the spectra. The peak at 380 cm⁻¹ is characteristic of MFI topology. The band at 960 cm⁻¹ has been assigned to the Ti–O stretching, titanyl group Ti=O, silanol group Si–OH, titanium related defect sites or the Ti–O–Si bridge. The peaks at 490, 530 and 1125 cm⁻¹ are characteristic of the framework Ti species. The TS-1-30 also shows a band at 700 cm⁻¹, which is assigned to the amorphous Ti species. Compared with the spectra of TS-1-120, the intensities of all peaks for the sample TS-1-30 are distinctly weak, which is due to the strong absorption of UV light by the non-framework Ti species.

Fig. 4 shows the Raman spectra of the TS-1 samples with different SiO₂/TiO₂ ratios collected with a 325 nm laser line. The TS-1-30 sample shows the Raman bands at 144, 390, 518 and 635 cm⁻¹, which are typical for the anatase TiO₂. In comparison, the bands of anatase TiO₂ are absent in the spectrum of the TS-1-120 sample. The TS-1-120 sample shows the peaks at 380, 817, 960 and 1125 cm⁻¹, which are assigned to the MFI
structure. The Raman results further confirm that TS-1-120 contains only framework Ti species, while TS-1-30 contains the framework Ti species, amorphous TiO₂ and anatase TiO₂. This is consistent with the UV-Vis result (see Fig. 2).

3.1.4 SEM. Fig. 5 shows the SEM images of the low-cost TS-1 samples with the SiO₂/TiO₂ ratios of 30 and 120. The TS-1 samples show a coalescent-like morphology with a crystal size of about 5 μm × 2.5 μm × 0.5 μm. The surface of the TS-1-30 sample is rough due to the presence of the non-framework TiO₂, while that of the TS-1-120 sample is smooth.

3.1.5 NH₃-TPD. Fig. 6 shows NH₃-TPD profiles of the TS-1 samples with different Ti species. The TS-1-120 sample shows a desorption peak at around 200 °C, indicating that only the weak acid site was observed on the TS-1 species, which contained the framework Ti species. In addition to the low-temperature desorption peak, the TS-1-30 sample also shows the desorption peak at higher temperatures, indicating the presence of strong acid sites. Considering that the titanium-rich samples (TS-1-30) contain non-framework Ti species, a close correlation exists between the non-framework Ti species and the strong acid sites.

3.1.6 N₂-Physical adsorption. Fig. 7 shows the N₂ adsorption isotherms of the TS-1 samples with different SiO₂/TiO₂ ratios. A sharp increase in nitrogen adsorption at P/P₀ = 0.01 indicates the presence of micropores. In addition, compared to the TS-1-120 sample, the TS-1-30 sample also presents an abrupt jump at high relative pressure. This is probably due to the formation of the macropores in between the crystal and TiO₂. The SEM image (see Fig. 5) shows that the surface of the TS-1-120 sample is very smooth. In contrast, the TS-1-30 sample is rough and has numerous small particles adhered onto the surface. This may cause the abrupt jump at high relative pressure.

Table 1 shows the textural properties of the TS-1 samples with different SiO₂/TiO₂ ratios. It can be seen that the BET surface area, the microporous surface area and the microporous volume of the TS-1-30 sample are all lower than that of the sample with high SiO₂/TiO₂ ratio (120). From the previous result, we know that the sample of SiO₂/TiO₂ ratio = 30 contains the non-framework Ti species, which may block the channels to some extent.

3.2 In situ GC-Raman results

3.2.1 The role of the non-framework Ti species of the low-cost TS-1. The role of the isolated Ti species in the framework of the low-cost TS-1 zeolite has been investigated in part A of the ESI.† The TS-1 with SiO₂/TiO₂ ratios of 100, 110 and 120, which contain only the framework Ti species, were used as the model catalysts. A positive correlation among the concentration of the framework Ti species, the amount of reaction intermediate Ti-
OOH(\(\eta^2\)), the propylene conversion and the yield of the PO has been established. Our previous studies\textsuperscript{13,16} indicated that an important active site of TS-1 is TiOOH(\(\eta^2\)), which is formed by the interaction between the framework Ti species and H\(_2\)O\(_2\). The framework Ti species can expand the tetrahedral coordination through the interaction with H\(_2\)O\(_2\) or a solvent to achieve the octahedral coordination. This result indicates that the isolated Ti species in the framework of the low-cost TS-1 zeolite is the active center for the propylene epoxidation. Subsequently, the TS-1 with SiO\(_2\)/TiO\(_2\) ratios of 120 and 30 were investigated using the in situ Raman-GC technique. After dropping 30 \(\mu\)L of H\(_2\)O\(_2\)-H\(_2\)O/CH\(_3\)OH solution (the volume ratio of H\(_2\)O\(_2\) and CH\(_3\)OH in the solvent is 1 : 1) on the TS-1 sample (0.05 g), the Raman spectra of the TS-1/H\(_2\)O\(_2\)-H\(_2\)O/CH\(_3\)OH system, under a continuous flow of propylene, were collected. Methanol was added because it is the best solvent for liquid phase epoxidation of alkenes. The Raman spectra of the TS-1/H\(_2\)O\(_2\)-H\(_2\)O/CH\(_3\)OH system are shown in Fig. 8. It can be seen that the evolution of the Raman spectra of the abovementioned system with different Ti species distributions are similar. In the beginning of the reaction, the bands at 490, 530, and 1125 cm\(^{-1}\) are extremely quenched immediately. The band at 1125 cm\(^{-1}\) shifts to 1134 cm\(^{-1}\), which has been attributed to the expansion of the Ti coordination sphere. Once the Ti coordination sphere expands, the Td-like symmetry of the Ti(IV) species is destroyed, and the symmetry of the vibrational modes is no longer the same as that of the LMCT. A new shoulder at 618 cm\(^{-1}\) is attributed to the symmetric breathing mode of the Ti(O\(_2\))\(_2\) cycle.\textsuperscript{20}

Moreover, the feature at 837 cm\(^{-1}\), which has been assigned to a Ti–OOH(\(\eta^2\)) species, appears quickly. The intensity of the band at 837 cm\(^{-1}\) first increases and then drops gradually as time passes. At the same time, the peak area of PO in the GC spectra shows the same trend, which indicates good correlation. A band at 1644 cm\(^{-1}\), which is related to propylene physisorbed into the zeolite channels, appears and its intensity increases with increasing the reaction time.

Fig. 9 shows the variation trend of the characteristic peak as the reaction time increases. As shown in Fig. 9, the amount of the active intermediate Ti–OOH(\(\eta^2\)) on the TS-1-30 is lower than that on TS-1-120, although the concentration of the framework Ti

**Table 1** Textural properties of the TS-1 samples with different SiO\(_2\)/TiO\(_2\) ratios

| Samples  | \(S_{\text{BET}}\) (m\(^2\) g\(^{-1}\)) | \(S_{\text{micro}}\) (m\(^2\) g\(^{-1}\)) | \(S_{\text{ext}}\) (m\(^2\) g\(^{-1}\)) | \(V_{\text{total}}\) (cm\(^3\) g\(^{-1}\)) | \(V_{\text{micro}}\) (cm\(^3\) g\(^{-1}\)) | \(V_{\text{meso}}\) (cm\(^3\) g\(^{-1}\)) |
|----------|----------------|----------------|----------------|----------------|----------------|----------------|
| TS-1-30  | 389.9          | 355.1          | 34.8           | 0.2382         | 0.1501         | 0.0881         |
| TS-1-120 | 440.8          | 392.5          | 48.3           | 0.2379         | 0.1821         | 0.0558         |

Fig. 8  *In situ* Raman spectra of the TS-1/H\(_2\)O\(_2\)-H\(_2\)O/CH\(_3\)OH system obtained at different times during the methanol-included epoxidation reaction, collected with a 244 nm laser line.

Fig. 9  (a) The UV-Raman intensity of the 837 cm\(^{-1}\) band at different times during the epoxidation reaction. (b) The percent conversion of propene in the TS-1/H\(_2\)O\(_2\)-H\(_2\)O/CH\(_3\)OH system at different times. (c) The peak area of PO in the GC spectra at different times. (d) The total column of the intermediate, conversion and yield with different SiO\(_2\)/TiO\(_2\) ratios.
species of TS-1-30 is higher than that of TS-1-120 (see Fig. 2). The result indicates that the existence of the non-framework Ti species influences the formation of the active intermediate Ti−OOH(η²). The H₂O₂ decomposition is not taken into account in this study due to the low reaction temperature. One possibility is that the non-framework Ti species block the channel, preventing the effective contact between the H₂O₂ solution and active center. The conversion of TS-1-30 is slightly higher than that of the TS-1-120, while the PO yield of the former is much less than the latter. The inverse relationship should be due to the presence of the non-framework Ti species (see Fig. 2). The acidic non-framework Ti species can convert the PO to other by-products and reduce the yield of PO. This result is consistent with that obtained on the classical TS-1 synthesised with TPAOH.¹³ In a vapor-phase epoxidation of propene, the absorbed PO may open the ring to form branched alkanes, which are subsequently converted into polyalkenes, propanal and so on.²⁰–²³ The side reaction of PO lowers the selectivity of the TS-1 catalyst unquestionably. Therefore, the acidic non-framework Ti species in TS-1-30 sample should be eliminated.

3.3 Acid treatment of TS-1 with the SiO₂/TiO₂ = 30

3.3.1 The influence of the sequence of calcination and acid treatment. The non-framework Ti species is harmful for propylene epoxidation according to the above results. The acid treatment procedure was used to eliminate the non-framework Ti species. Fig. 10 shows the UV-Vis spectra of the TS-1 samples treated with hydrochloric acid (C₇HCL = 1.0 mol L⁻¹) in different post-treatment sequences.²⁴ The UV-Vis spectra show that a considerable amount of non-framework Ti species were observed on both the as-synthesized (curve a) and calcined (curve b) samples. The peak shifts to a high-wavelength side, which means that a part of the amorphous TiO₂ was transformed into the anatase TiO₂. It is clear that only a small amount of the amorphous Ti species and the anatase TiO₂ were removed when the samples were treated by HCl after the calcination (curve d). It seems that once the anatase TiO₂ is formed, it is difficult to eliminate it by HCl washing treatment alone. Therefore, it is important that the amorphous TiO₂ is removed before it is transformed into anatase TiO₂ by the calcination step. As expected, most of the non-framework Ti species are eliminated after acid washing treatment, before the calcination step (Fig. 10c). At the same time, the concentration of the framework Ti species (220 nm) has not been obviously affected. These results indicate that the sequence of post treatment is the key to the efficient elimination of the non-framework TiO₂.

Fig. 11 Raman spectra of the TS-1 samples (SiO₂/TiO₂ = 30) modified by different post-treatments (325 nm). (a) Dry; (b) dry-calcine; (c) dry-acid treating-calcine; (d) dry-calcine-acid treating-calcine.

Fig. 12 XRD patterns of TS-1 samples before and after HCl washing.
cannot eliminate the anatase TiO₂. However, if the acid treatment is performed before the calcination step (c), no anatase TiO₂ can be found in the spectrum. The bands at 380, 960 and 1125 cm⁻¹, which are associated with the framework of TS-1, were clearly observed. The results reveal that the anatase TiO₂ cannot be removed once the samples are calcined prior to acid treatment. The above result is in agreement with the UV-Vis spectroscopy result. Therefore, the TS-1 was treated with HCl prior to calcination in the following sections.

Fig. 12 shows the XRD patterns of the TS-1 samples before and after the HCl acid treatment. It is clear that the sample keeps the MFI topology structure perfectly after acid treatment.

3.3.2 The influence of different acid modifiers on acid treatment. To study the effects of different types of acids on the elimination of non-framework TiO₂, HCl, H₂SO₄, HNO₃, H₃PO₄ and H₃BO₃ were used as acid modifiers (C(H⁺) = 1.0 mol L⁻¹). The UV-Vis spectra of the TS-1-30 samples before and after acid treatments are shown in Fig. 13. As a reference, the spectrum of the TS-1-30 sample treated with distilled water is also provided. The treatment with only distilled water shows a slight elimination effect on the non-framework TiO₂ (see the bands at 270 nm and 320 nm). It is clear that the effect of the acid treatment can be divided into two parts. The H₃PO₄ and H₃BO₃-related samples, which belong to relatively weak acids, show the elimination effect similar to that of the distilled water. In contrast, the strong acids such as HCl, H₂SO₄ and HNO₃ show a dramatic effect on eliminating the non-framework Ti species. This indicates that the strong acid is much more effective than the weak acid on the elimination process. This result is confirmed by Raman (see part B, Fig. S1 in the ESI†).

3.3.3 The influence of the acid concentration. The TS-1 samples were washed in HCl solution with different concentrations (0–2.0 mol L⁻¹) to investigate the effect of the acid concentration. As shown in Fig. 14, the intensities of the bands at 270 nm and 310 nm decrease with increasing HCl concentrations (0–0.5 mol L⁻¹). When the HCl concentration reaches 0.5 mol L⁻¹, most of the non-framework Ti species are eliminated, but the framework Ti species is not significantly affected. When the HCl concentration further increases to 2.0 mol L⁻¹, the band at 210 nm, associated with the framework Ti species, shows a slight reduction. This result is also confirmed by the result achieved using Raman (see part B, Fig. S2 in the ESI†).

In conclusion, almost all the non-framework Ti species can be eliminated, while the framework Ti species is barely influenced by choosing the appropriate HCl concentration (0.5–1.0 mol L⁻¹).

3.3.4 Textural properties of TS-1-30 samples before and after acid washing. Depending on the above results, the TS-1-0.7 sample was chosen for the GC-Raman experiment. Fig. 15 shows the nitrogen physisorption isotherms of TS-1 samples before and after HCl washing. All TS-1 samples exhibit the same type of the nitrogen physisorption isotherm. However, the BET surface areas, microporous surface areas and pore volumes of the treated samples increase in comparison to the as-synthesized sample (see Table 2). This change demonstrates that the elimination of non-framework Ti species, by the acid treatment, may improve the diffusion ability of the zeolite.

3.3.5 The results of in situ GC-Raman technique. The in situ GC-Raman experiment was performed on the TS-1-30 before
Table 2  Textural properties of TS-1 samples modified by acid

| Samples    | \( S_{\text{BET}} \) (m\(^2\) g\(^{-1}\)) | \( S_{\text{micro}} \) (m\(^2\) g\(^{-1}\)) | \( S_{\text{ext}} \) (m\(^2\) g\(^{-1}\)) | \( V_{\text{total}} \) (cm\(^3\) g\(^{-1}\)) | \( V_{\text{micro}} \) (cm\(^3\) g\(^{-1}\)) | \( V_{\text{meso}} \) (cm\(^3\) g\(^{-1}\)) |
|------------|-------------------------------------|-------------------------------------|-------------------------------------|-------------------------------------|-------------------------------------|-------------------------------------|
| TS-1-3.0   | 389.9                               | 355.1                               | 34.8                                | 0.2382                              | 0.1501                              | 0.0881                              |
| TS-1-0.7   | 401.9                               | 372.5                               | 29.4                                | 0.2518                              | 0.1575                              | 0.0943                              |

Fig. 16  (a) UV-Raman intensity of the 837 cm\(^{-1}\) band at different times during the epoxidation reaction. (b) The conversion of propene in the TS-1/H\(_2\)O\(_2\)/CH\(_3\)OH system at different times. (c) The peak area of PO in the GC spectra at different times. (d) The total column of the intermediate, conversion and yield with different SiO\(_2\)/TiO\(_2\) ratios.

and after acid washing. The Raman spectra of the TS-1-3.0 and TS-1-0.7 samples are shown in the part B, Fig. S3 in the ESL†.

As shown in Fig. 16d, the amount of the active intermediate Ti-OOH(\(\eta^1\)), conversion and PO yield are increased after the acid washing treatment step. This indicates that the elimination of the non-framework TiO\(_2\) species favors the formation of the active intermediate Ti-OOH(\(\eta^2\)) and PO. This is most likely due to two possible reasons: (1) the acid treatment may improve the diffusion property of the zeolite by removing the non-framework TiO\(_2\), thus facilitating the contact between the framework Ti species and H\(_2\)O\(_2\). (2) The opening reaction of the PO is inhibited by elimination of the acidic non-framework TiO\(_2\). Therefore, the \textit{in situ} GC-Raman results indicate that the conversion and PO yield can be improved by the elimination of the non-framework TiO\(_2\) by a proper acid treatment procedure.

4. Conclusions

The acid treatment on the low-cost TS-1 was systematically investigated using various techniques. The results demonstrate that the framework Ti species is the active center for low-cost TS-1 zeolite. The existence of the non-framework Ti species influences the amount of Ti-OOH(\(\eta^1\)) and reduces the yield of PO. The acid treatment step was used to eliminate the non-framework TiO\(_2\). It was found that the acid treatment of the as-synthesized TS-1 before the calcination is key to efficiently eliminate the non-framework TiO\(_2\). During the calcination process, the amorphous TiO\(_2\) can be transformed into anatase TiO\(_2\), which is difficult to be removed following acid treatment. The strong acids are more efficient for elimination of the non-framework TiO\(_2\) than the relatively weak acids. After treatment with 0.5–1.0 mol L\(^{-1}\) HCl solution, most of the non-framework Ti species were eliminated, while the framework Ti species was maintained. As a result, the amount of active intermediate Ti-OOH(\(\eta^2\)), the conversion of propylene and the yield of PO can be improved through acid treatment with appropriate concentration.

Acknowledgements

This study was financially supported by the National Science Foundation of China(NSFC, Grant 21473016).

References

1. M. Taramasso, G. Perego and B. Notari. Preparation of porous crystalline synthetic material comprised of silicon and titanium oxides, \textit{US Pat.}, 4410501, 1983.
2. A. Thangaraj, M. J. Eapen, S. Sivasanker, \textit{et al.}, Studies on the synthesis of titanium silicalite, TS-1, \textit{Zeolites}, 1992, 12(8), 943–950.
3. G. Li, X. Guo, X. Wang, \textit{et al.}, Synthesis of titanium silicalites in different template systems and their catalytic performance, \textit{Appl. Catal., A}, 1999, 185(1), 11–18.
4. J. Fang, J. Li, B. Zhang, \textit{et al.}, Support Effect on the Size and Catalytic Activity of Thiolated Au\(_{25}\) Nanoclusters as Precatalyst, \textit{Nanoscale}, 2015, 7(14), 6325–6233.
5. B. Zhang, J. Fang, J. G. Li, \textit{et al.}, Soft, Oxidative Stripping of Alkyl Thiolate Ligands from Hydroxyapatite-Supported Gold Nanoclusters for Oxidation Reactions, \textit{Chem.–Asian J.}, 2016, 11(4), 532–539.
6. X. J. Deng, Y. N. Wang, L. Shen, \textit{et al.}, Low-Cost Synthesis of Titanium Silicalite-1 (TS-1) with Highly Catalytic Oxidation Performance through a Controlled Hydrolysis Process, \textit{Ind. Eng. Chem. Res.}, 2013, 52(3), 1190–1196.
7. U. Müller and W. Steck, Ammonium-Based Alkaline-Free Synthesis of MFI-Type Boron- and Titanium Zeolites, \textit{ Stud. Surf. Sci. Catal.}, 1994, 84, 203–210.
8. G. Li, X. Guo, X. Wang, \textit{et al.}, Synthesis of titanium silicalites in different template systems and their catalytic performance, \textit{Appl. Catal., A}, 1999, 185(1), 11–18.
9. S. T. Tsai, P. Y. Chao, T. C. Tsai, \textit{et al.}, Effects of pore structure of post-treated TS-1 on phenol hydroxylation, \textit{ Catal. Today}, 2009, 148(1–2), 174–178.
10. Y. Wang, M. Lin and A. Tuel, Hollow TS-1 crystals formed via a dissolution-recrystallization process, \textit{Microporous Mesoporous Mater.}, 2007, 102(1–3), 80–85.
11 Y. Wang and A. Tuel, Nanoporous zeolite single crystals: ZSM-5 nanoboxes with uniform intracrystalline hollow structures, *Microporous Mesoporous Mater.*, 2008, **113**(1), 286–295.

12 V. Bolis, S. Bordiga, C. Lamberti, *et al.*, A calorimetric, IR, XANES and EXAFS study of the adsorption of NH3 on Ti-silicalite as a function of the sample pre-treatment, *Microporous Mesoporous Mater.*, 1999, **30**(1), 67–76.

13 G. Xiong, Y. Cao, Z. Guo, *et al.*, The roles of different titanium species in TS-1 zeolite in propylene epoxidation studied by *in situ* UV Raman spectroscopy, *Phys. Chem. Chem. Phys.*, 2016, **18**, 190–196.

14 G. Qiang, S. Keju, F. Zhaochi, *et al.*, A thorough investigation of the active titanium species in TS-1 zeolite by *in situ* UV resonance raman spectroscopy, *Chemistry*, 2012, **18**(43), 13854–13860.

15 C. Li, G. Xiong, Q. Xin, *et al.*, UV-Resonanz-Raman-spektroskopische Identifizierung von Titanatomen im Gerüst des Zeoliths TS-1, *Angew. Chem.*, 1999, **111**(15), 2358–2360.

16 L. Wang, G. Xiong, J. Su, *et al.*, *In Situ* UV Raman Spectroscopic Study on the Reaction Intermediates for Propylene Epoxidation on TS-1, *J. Phys. Chem. C*, 2012, **116**(116), 9122–9131.

17 G. Ricchiardi, A. Damin, S. Bordiga, *et al.*, Vibrational Structure of Titanium Silicate Catalysts: A Spectroscopic and Theoretical Study, *J. Am. Chem. Soc.*, 2001, **123**(46), 11409–11419.

18 M. A. Camblor, A. Corma and J. Pérez-Pariente, Synthesis of titanolauminosilicates isomorphous to zeolite Beta, active as oxidation catalysts, *Zeolites*, 1993, **13**(2), 82–87.

19 J. Su, G. Xiong, J. Zhou, *et al.*, Amorphous Ti species in titanium silicalite-1: Structural features, chemical properties, and inactivation with sulfosalt, *J. Catal.*, 2012, **288**(4), 1–7.

20 S. Bordiga, A. Damin, F. Bonino, *et al.*, Resonance Raman effects in TS-1: the structure of Ti(IV) species and reactivity towards H2O, NH3 and H2O2: an *in situ* study, *Phys. Chem. Chem. Phys.*, 2003, **5**(20), 4390–4393.

21 B. S. Uphade, T. Akita, T. Nakamura, *et al.*, Vapor-Phase Epoxidation of Propene Using H2 and O2 over Au/Ti-MCM-48, *J. Catal.*, 2002, **209**, 331–340.

22 X. Feng, N. Sheng, Y. B. Liu, *et al.*, Simultaneously Enhanced Stability and Selectivity for Propene Epoxidation with H2 and O2 on Au Catalysts Supported on Nano-Crystalline Mesoporous TS-1, *ACS Catal.*, 2017, **7**, 2668–2675.

23 X. Feng, Y. B. Liu, Y. C. Li, *et al.*, Au/TS-1 Catalyst for Propene Epoxidation with H2/O2: A Novel Strategy to Enhance Stability by Tuning Charging Sequence, *AIChE J.*, 2016, **62**(11), 3963–3972.

24 L. Kong, G. Li and X. Wang, Kinetics and Mechanism of Liquid-Phase Oxidation of Thiophene over TS-1 Using H2O2 Under Mild Conditions, *Catal. Lett.*, 2004, **92**(3), 163–167.

25 E. Astorino, J. B. Peri, R. J. Villey, *et al.*, Spectroscopic characterization of silicalite-1 and titanium silicalite-1, *J. Catal.*, 1995, **157**(2), 482–500.