BIOGAS POTENTIAL FROM SLAUGHTERHOUSE WASTES AT AMBIENT TEMPERATURES IN LIRA MUNICIPALITY OF NORTHERN UGANDA

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Abstract

The generation of biodegradable solid waste and wastewaters is characteristic of all slaughterhouses including the Lira Municipality slaughterhouse (LMS) in northern Uganda. However, the LMS is not properly designed to handle and manage the ever-increasing biodegradable solid waste and wastewater. The wastes discharged from LMS, contain reasonable amounts of paunch, fat, grease, undigested food, diluted blood, suspended material, urine, loose meat and soluble protein. The lack of a properly designed slaughterhouse in Lira Municipality, needed to manage and handle the waste has resulted in the discharge of the waste into the environment, leading to pollution of water sources, outbreaks of diseases, and production of unfavorable odors. The objective of this study was to investigate the biogas potential of the LMS biodegradable solid waste and wastewaters at ambient temperatures. The waste was quantified based on Measurement at the point of generation method. Representative samples were characterized for biogas potential. Five treatments of the waste replicated three times were anaerobically digested in 1500mL batch digesters with a working volume of 750mL. Treatment A contained only the inoculum and inoculum in the other treatments B, C, D, and E was approximately 20% of the volume of the substrate. Substrate: water ratio of 1:1, maintained pH of 6.0-7.0 and retention time of 30 days were used for the study under ambient conditions. On average, 2,597 L, 40 kg and 502 kg of wastewater, cow dung and punch manure respectively were produced from LMS. The quantity and methane content of the biogas ranged from 1029.6 to 3512.7 ml/gVS and 40.6 to 50.4% respectively. Therefore, slaughterhouse wastes are potential sources of biogas production at ambient temperatures.

Keywords: slaughterhouses, punch, cow dung, wastewater, inoculum, biogas
Introduction

According to [1], there is an increasing demand for meat in the world which has led to increased establishments of slaughterhouses. Within a series of processes, slaughterhouses generate vast amounts of different solid wastes and wastewaters [2]. Approximately, 20 – 50 % of the weight of the animal is not suitable for human consumption [3] thus a lot of by-products are produced such as; paunch, fat and, grease, undigested food, diluted blood, suspended material, urine, loose meat, soluble proteins, excrement among others.

However, many slaughterhouses in the developing countries are not designed to properly manage their wastes such as; the paunch, cow dung, and wastewater. For example, Lira Municipality slaughterhouse, located in Railways division, in Northern Uganda, is the only one in the municipality, operating beyond the designed capacity of 100 cows slaughtered instead of 60 daily. This slaughterhouse produces vast amounts of biodegradable wastes which end up in open places and nearby water bodies as there is no currently organized system for their disposal. These improperly managed wastes from the slaughterhouse pollute the environment, act as breeding places for disease-causing vectors and create bad odour. This makes the living conditions within the community and its outskirts unfavorable. However, these wastes can be converted into useful clean energy (biogas) and fertilizer inform of slurry through anaerobic digestion process since they are organic in nature. According to [4], biogas technology has helped some countries such as India and China in many ways including income generation, life-style improvements and cost saving. Moreover, the conversion of slaughterhouse wastes into clean energy has not been fully tapped in Uganda and it is against this background that this study was conducted. The objective of this study was to investigate the biogas potential from the slaughterhouse wastes at ambient temperatures in Lira district, Northern Uganda.

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2. Methods and materials

2.1 Study area

Figure 1: Map showing Lira slaughter house and Holding pen

The study to investigate the biogas potential from the slaughterhouse wastes at ambient temperatures was carried out from Lira Municipality (LM), Northern Uganda. Lira Municipality has four Divisions, 22 wards and 64 cells (Figure 1). It covers an area of 7,745 hectares and is surrounded by swamps. Lira Municipality has an altitude of 489678.50m and longitude of 249418.12m respectively.

Collection and quantification of biodegradable waste generated from LM slaughterhouse

The biodegradable waste generated from the slaughterhouse was quantified based on Measurement at the point of generation method [5]. Cow dung from the animal holding pen, paunch manure from the slaughter area and wastewater tapped from the outlet of the slaughterhouse were collected and measured using different pre-weighed calibrated buckets of 16 litre capacity and a digital
weighing scale. The wastewater which contained diluted blood, fats, urine and pieces of meat trimming was then quantified for a period of ten (10) days.

Sample preparation and characterization of the biodegradable slaughterhouse waste for biogas production

The waste was cleaned by removing the non-biodegradable wastes such as the bones, plastic bags, metals among others and reduced in size by mashing into paste. Representative samples were then placed in clean plastic bottles and immediately analyzed on the laboratory scale for: total solids (TS), volatile solids (VS), fixed solids (FS), carbon/nitrogen ratio (C/N), and pH using standard methods [6]. The aluminum dishes that were used in the laboratory analyses were first ignited at 550°C for one hour in the furnace to remove any volatiles, cooled in the desiccator and weighed. The samples were heated at 103°C for 6 hours and at 550°C for 30 minutes to determine the total solids and volatile solids respectively. An electronic digital pH meter was used to determine the pH of the representative samples. The determination of waste organic carbon was based on the Walkley-Black chromic acid wet oxidation method, potassium dichromate as the oxidizing agent with other reagents of sulphuric acid and ferrous sulphate. The percentage and quantity of carbon was determined from Equations 1 and 2, adopted:

\[
\% C = \frac{T \times 0.3 \times 1.22 \times N}{W_t} \times 14 \times \frac{100}{W_t} \tag{1}
\]

\[
C (g/L) = \frac{T \times N}{1000} \times \frac{1}{6} \times \frac{3}{4} \times 12 \times \frac{1000}{W_t} \tag{2}
\]

Where:

N = Normality of \( K_2Cr_2O_7 \) solution

T = Volume of \( FeSO_4 \) used in sample titration (mL)

Wt = Oven-dry sample weight (g)

The Kjeldahl method involving the three steps of digestion, distillation and titration was used to determine the nitrogen in the biodegradable waste. The reagents that were used included Potassium sulphate, concentrated sulphuric acid, sodium hydroxide, boric acid and HCl [7]. The percentage and quantity of Nitrogen was determined using Equation 3.

\[
\% N = \frac{\nu \times 0.1 \times 14 \times 100}{W_t} \tag{3}
\]
\[ N(g/L) = \frac{v \times 0.1}{1000} \times 14 \times \frac{1000}{5} \] ........................................4

Where:

V is volume of titrant in ml which is the volume HCL used

\( W_t \) is Oven-dry sample weight (g)

Carbon nitrogen (C/N) ratio was then computed based on the results of the carbon and nitrogen. For reliability of the data and conclusions, three laboratory analyses were involved three replications.

**Biochemical Methane Potential (BMP) Test experimental setup**

Five treatments of the slaughterhouse waste (Table 1), replicated three times were anaerobically digested in 1500mL batch digesters with a working volume of 750mL.

**Table 1: Slaughterhouse waste treatments for the BMP tests**

| S/N | Treatments | Composition by mass (%) |
|-----|------------|-------------------------|
| 1   | A (control)| 100 inoculum            |
| 2   | B          | 10 cow dung and 90 slaughterhouse wastewater |
| 3   | C          | 50 cow dung and 50 punch manure |
| 4   | D          | 75 punch manure and 25 slaughterhouse wastewater |
| 5   | E          | 10 cow dung, 70 punch manure and 20 slaughterhouse wastewater |

The inoculum that was used in the study was obtained from an already existing digester being fed with a mixture of food waste and cow dung as the substrates. Treatment A (control) contained only the inoculum and the inoculum in the other treatments B, C, D, and E was approximately 20% of the volume of the substrate. The substrate-to-water ratio that was used in the study was 1:1[8]. Zero Point eight grams (0.8g) of Sodium Carbonate powder was added to all the batch digesters to maintain pH between 6.0-7.0 which is within the pH range required for biogas production. The retention time used for the study was 30 days under ambient conditions (temperature between 25 and 30°C).

The Biogas that was obtained was then collected by water displacement method. In order to prevent the dissolution of biogas in the water, acidified brine solution was prepared following the
method suggested by [9]. Since the biogas was insoluble in this solution, a pressure was built-up that provided the driving force for displacement of the solution. Thus, the displaced brine solution was measured to represent the amount of biogas produced daily. The biogas produced from the digesters was collected by downward delivery of gas, achieved by filling the burettes with brine solution and inverting them in beakers containing same solution. The reactors were agitated twice a day to make the microorganisms more active during the digestion process for maximum biogas production.

After the 30 days retention time, the gases were left to collect in the digestion bottles where it was delivered to Green Heat for the different gas composition analyses. The percentage of the gases in the biogas were determined by connecting the gas with a cannula to the Geotech portable GA2000 gas analyzer through the inlet port which had an adjuster for connecting the flexible tube. Proportions of CH$_4$, CO$_2$, N$_2$, H$_2$S, CO and O$_2$ were determined and recorded. A one-way analysis of variance (ANOVA) in Genstat software was performed (p≤ 0.05) to verify any significant difference among the treatments.

**Results and discussion**

**Quantification of biodegradable waste generated from LM slaughterhouse**

On average, 2,597 L, 40 kg and 502 kg of wastewater, cow dung and punch manure respectively were produced from Lira Municipality slaughterhouse daily Table 2. Generally, more waste (wastewater, cow dung and punch manure) was produced on Sundays as compared to other days. This could be attributed to the fact that weekends people are on work leave so they travel upcountry homes where LM slaughter house is located to feast with dear ones (generally weekends are reunion days which call for more feasting of beef).

**Table 2. Lira Municipality slaughterhouse waste production**

| Day      | Wastewater (L) | Cow dung (kg) | Punch manure (kg) |
|----------|----------------|---------------|-------------------|
| Saturday | 2,153          | 34            | 302               |
| Sunday   | 4,120          | 46            | 972               |
| Monday   | 2,251          | 38            | 377               |
| Wednesday| 2,340          | 40            | 432               |
| Thursday | 2,470          | 41            | 476               |
Characterization of the biodegradable slaughterhouse waste for biogas production

The total solids, volatile solids and fixed solids ranged from 16 to 19, 71 to 79 and 21 to 30 respectively (Table 3). The findings of this study are in line with the study results of Gebrekidan et al., [10] where the total solids and volatile solids of animal manure were found to vary between 16% to 20% and 80% respectively. The recommended value for slurry is between 8 percent and 12 percent. According to literature reports [10], the %VS of animal waste are usually around 80 percent of the TS. The high proportion of VS in the manure substrate depicts that a large fraction of the substrate was biodegradable and could serve as an important feedstock for biogas production [11].

The C/N ratio for this study ranged from 2.6 to 17.5 (Table 3). This was relatively lower than the recommended range for anaerobic digestion process of 20:1 to 30:1 [12]. Moreover, in a study conducted by [12], C/N ratio of cow manure is about 16 to 25. However, to achieve the objective of this study, the different slaughterhouse wastes were mixed in varying ratios to improve the C/N ratio. The varying ratios may, therefore have been responsible for minimizing the liberation of nitrogen in form of ammonia. The pH of the substrate ranged from 6.8 to 6.9 as shown in (Table 3) which was within ideal range of 6.5 to 8.0 for anaerobic digestion.

| Slaughterhouse waste | Total solids | Volatile solids | Fixed solids | C/N ratio | pH   |
|----------------------|--------------|-----------------|--------------|-----------|------|
|                      | TS (%)       | VS (%)          | FS (%)       |           |      |
| Wastewater           | 19           | 71              | 28           | 2.6       | 6.9  |
| Cow dung             | 19           | 73              | 30           | 17.5      | 6.9  |
| Punch                | 16           | 79              | 21           | 15.8      | 6.8  |

Table 3: Average values from the characterization of the slaughterhouse waste
Biochemical Methane Potential (BMP) Test

Quantity of biogas

All the digesters started gas production on the second day except for the inoculum (A) where gas production commenced on day one (Figure 2). The earlier start of gas production in inoculum (A) may have been attributed to the fact that the inoculum (A) already contained active microorganisms that were adapted to the reaction conditions in the digester thereby lowering the lag phase of the microbial growth curve.

![Figure 2: Average cumulative biogas production from slaughterhouse waste](image)

Generally, biogas production was slow at the beginning due to the fact that biogas production rate in batch anaerobic digestion condition directly relies on growth rate of micro-organism in bio–digester. At the beginning, the microorganisms are in the lag phase trying to get used to the new environment. From the 8–12th day, biogas production rate significantly increased due to exponential growth (doubling in numbers) of micro–organisms. Generally, after 12 days, biogas production decreased due to the stationary growth phase of the microorganisms. At the stationary growth phase, the number of microorganisms being produced is equal to the number of microorganisms dieing. The death of the microorganisms was probably due to the accumulation of microbial metabolic wastes which altered the
environmental conditions necessary for microbial growth and the reduction in food nutrients necessary to support microbial growth.

Treatment E gave the highest biogas production (3512.7 ml / g VS) (Figure 2). This probably was because of the good mix of the slaughterhouse wastes that improved the C/N ratio. Treatment E contained 10 % cow dung, 70% punch manure, and 20% slaughterhouse wastewater. Carbon and Nitrogen serve as good starting structural elements for the bio-synthesis of carbohydrates and proteins that are essential for microbial growth. There was less biogas production (1029.2 ml / g VS) from treatment B probably because of too much slaughter wastewater (10% cow dung and 90% wastewater). The slaughter wastewater created a hypertonic environment (where by the osmotic potential of the wastewater was higher than that of the microbial cell cytoplasm) that negatively impacted on the growth of microorganisms. From the characterization results, wastewater had the least C/N ratio (average of 2.6) hence there was liberation of a lot of nitrogen in form of ammonia in treatment B. During the study period, the temperature fluctuated between 25 and 30°C with an average temperature of 28°C. Methane producing bacteria are temperature sensitive and ideally mesophilic biogas production takes place in a temperature range of 30 to 40°C with an optimum temperature of 37°C. Therefore, the methane production in this study may have been improved if the temperature could have been controlled around 40°C [13].

**Quality of the biogas from the slaughterhouse wastes**

The methane composition of the biogas produced from the slaughterhouse waste at ambient temperatures ranged from 40.6% to 50.4% (Table 4) with treatment A and E giving the highest and the least percentages of methane respectively.

| Treatments | CH4 (%) | CO2 (%) | O2 (%) | N2 (%) | H2S (ppm) | CO (ppm) |
|------------|---------|---------|--------|--------|-----------|----------|
| A          | 50.4    | 28.9    | 0.6    | 0      | 66.5      | 0.8      |
| B          | 44.7    | 25.1    | 0.4    | 0      | 40.0      | 0.3      |
| C          | 44.1    | 25.3    | 0.5    | 0      | 36.8      | 0.2      |
| D          | 47.3    | 26.6    | 0.4    | 0      | 33.6      | 0.6      |
| E          | 40.6    | 26.2    | 0.5    | 0      | 50.6      | 1.0      |
Conclusions
The findings of this study show that there is enough biodegradable waste (2,597 L, 40 kg and 502 kg of wastewater, cow dung and punch manure respectively) generated in Lira Municipality slaughterhouse with high potential for biogas production. The quantity and methane content of the biogas from the wastes ranged from 1029.6 to 3512.7 ml/gVS and 40.6 to 50.4% respectively. It is therefore possible to generate biogas from biodegradable wastes at ambient temperatures.

List of abbreviations
LMS: Lira Municipality slaughterhouse, TS: total solids, VS: volatile solids, FS: fixed solids, carbon/nitrogen ratio (C/N),

Declarations
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References:
[1] M. Vinnari, “The future of meat consumption — Expert views from Finland,” vol. 75, pp. 893–904, 2008.
[2] N. Technologien and B.- Wirtschaftsberatung, “Anaerobic treatment of slaughterhouse waste and wastewater,” vol. 49, no. 0, 2001.
[3] FAO, “Part 3: Feeding the world,” FAO Stat. Yearb. 2013, pp. 123–158, 2013.
[4] H. M. El-Mashad and R. Zhang, “Biogas production from co-digestion of dairy manure and food waste,” *Bioresour. Technol.*, vol. 101, no. 11, pp. 4021–4028, 2010.

[5] United Nations Environment Programme, “Developing Integrated Solid Waste Management Plan - Training Manual,” *UNEP (United Nations Environ. Program.)*, vol. Volume 4, pp. 1–176, 2009.

[6] A. M. Zealand, A. P. Roskilly, and D. W. Graham, “Effect of feeding frequency and organic loading rate on biomethane production in the anaerobic digestion of rice straw,” *Appl. Energy*, vol. 207, pp. 156–165, 2017.

[7] P. Sáez-Plaza, T. Michalowski, M. J. Navas, A. G. Asuero, and S. Wybraniec, “An Overview of the Kjeldahl Method of Nitrogen Determination. Part I. Early History, Chemistry of the Procedure, and Titrimetric Finish,” *Crit. Rev. Anal. Chem.*, vol. 43, no. 4, pp. 178–223, 2013.

[8] L. L. Kasisira and N. D. Muyiiya, “Assessment of the Effect of Mixing Pig and Cow Dung on Biogas Yield,” *CIGR Ejournal*, vol. XI, no. 2003, pp. 1–7, 2009.

[9] R. Misganaw, D. F. Habte, and S. Imru, “Digestion of cattle manure and biodegradable kitchen waste to increase biogas production using rumen fluid as inoculums,” vol. 2, no. 4, pp. 298–304, 2013.

[10] T. Gebrekidan, M. C. Egigu, and M. Muthuswamy, “Efficiency of biogas production from cactus fruit peel co-digestion with cow dung,” *Effic. biogas Prod. from cactus fruit peel co-digestion with cow dung*, vol. 2, no. 7, pp. 916–923, 2014.

[11] A. K. Jha, J. Li, L. Zhang, Q. Ban, and Y. Jin, “Comparison between Wet and Dry Anaerobic Digestions of Cow Dung under Mesophilic and Thermophilic Conditions,” *Adv. Water Resour. Prot.*, vol. 1, no. 2, pp. 28–38, 2013.

[12] S. Riya, K. Suzuki, A. Terada, M. Hosomi, and S. Zhou, “Influence of C/N Ratio on Performance and Microbial Community Structure of Dry-Thermophilic Anaerobic Co-Digestion of Swine Manure and Rice Straw,” *J. Med. Bioeng.*, vol. 5, no. 1, pp. 11–14, 2016.

[13] K. Rajendran, S. Aslazadeh, and M. J. Taherzadeh, *Household biogas digesters-A review*, vol. 5, no. 8. 2012.