Original Research Article

Hydrochar as an Energy Alternative to Coal: Effect of Temperature on Hydrothermal Carbonization of Paper Board Mill Sludge

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Abstract

Hydrothermal Carbonization is a thermochemical conversion process in which a biomass is processed under hot compressed air to form carbon rich products called as hydrochar. Hydrochar is a hydrophobic, condensed and friable solid product with a fuel property similar to conventional non-renewable energy sources like coal and lignite. Hydrothermal Carbonization performed with Effluent Treatment Plant (ETP) sludge at a temperature range of 180-240°C for a time period of 4 hours in a hydrothermal autoclave reactor resulted in the production of hydrochar with good energy values thereby ensuring its utilization as an alternative to coal. The energy properties like higher heating value (15.25 MJ Kg⁻¹), energetic recovery efficiency (69.8%) and energy densification (1.24) were found to increase after hydrothermal carbonization at 220°C for 4 hours.

Keywords
Hydrothermal Carbonization, Paper board mill sludge, Proximate analysis, Higher heating value, H/C and O/C ratio

Introduction

The sludge generation from treatment plants of pulp and paper mill varies from 0.3 to 1 m³ per ton of paper produced Priadi, Wulandari, Rahmatika, and Moersidik (2014). The sludge generated from ETP (Effluent Treatment Plant) of paper board mill possess enormous amount of organic matter that are generally managed by land filling, incineration, land reclamation and energy recovery through combustion Pervaiz and Sain (2015). This results in the creation serious environmental issues in the form of secondary pollution Karthikeyan and Balasubramanian (2010). These sludge materials are mainly composed of organic fractions in the form of cellulose and inorganic fractions due to the addition of salts during the paper manufacturing process Abdullah, Ishak, Kadir, and Bakar (2015). This organic composition serves as a promising precursor material for the
hydrothermal carbonization process because of their hydrophilic nature. Additionally, these compounds are readily available with lower cost and lower energy requirements (Ho et al., 2014).

Hydrothermal Carbonization is a thermochemical conversion method of biomass wherein the wet biomass compounds are converted into a carbon-rich solid product under sub-critical water conditions called as Hydrochar. Hydrothermal treatments are performed under auto-generated pressure conditions where the water in the biomass acts as a precursor, reactant or catalyst thereby assuring completion of the process Jin et al., (2014). This process is carried out between the temperature range of 180°C and 280°C within the time period of 1 minute to several hours under an inert atmosphere Reza et al., (2014). This method ensures the upgrading of biomass into energetic solid fuels wherein relatively higher yield can be recovered from a range of biomass precursors under comparatively lower temperature and pressure Libra et al., (2011). A series of reaction mechanisms takes place during the hydrothermal carbonization process that includes hydrolysis, dehydration, decarboxylation, polymerization and aromatization. This results in the dissolution of part of feedstock materials into liquid phase and also into minor quantity of gaseous compounds Falco et al., (2013). This process is advantageous in the sterilization of sludge materials within shorter period of time wherein the hydrophilic sludge particles are converted to hydrophobic carbonaceous products with variety of environmental applications thus enhancing the drying properties of sludge materials Phasee and Areeprasert (2017). The fuel property in terms of higher heating value, H/C and O/C ratios have been evaluated which lead to the utilization of the hydrothermally formed carbon product as brown coal. This energy rich carbon material have already been produced with various precursor materials like cellulose, microalgae, anaerobically digested silage, municipal solid waste, distiller’s grains and black liquor Kim, Lee, and Park (2014). Also, the fuel characteristics and process energetics of hydrothermally carbonized paper and pulp mill sludge at different temperature have also been studied wherein 240°C for 30 minutes showed an increased higher heating value by 6.8% as compared to raw biomass Areeprasert, Zhao, Ma, Shen, and Yoshikawa (2014). So, it becomes evident that the temperature plays an important role in the fuel characteristics of hydrochar. With an objective of sustainable management of paper board mill sludge and energy production, this work concentrates on the effect of temperature on hydrothermal carbonization of the paper board mill sludge so as to attain a ecofriendly solid fuel production technology

Materials and Methods

Sampling and processing of Sludge

Sludge samples were collected from ITC Ltd., Paper Board and Speciality Papers Division Unit, Coimbatore, Tamil Nadu, India. The collected sludge materials were stored in sample containers under 4°C. The Initial characterization of sludge samples were carried after drying and pulverizing as mentioned under analytical procedures.

Wet torre faction or hydrothermal carbonization

The sludge samples were mixed before taking it in the reactor after which 60g of sludge samples were taken in 100 ml hydrothermal autoclave reactor followed by purging with nitrogen gas for attaining inert atmosphere. Then, the reactor was placed inside the hot air oven and the desired temperature was set up
with the retention time of 4 hours as exhibited in the Figure 1. At the end of the process, the wet product was dried to form hydrochar which was stored in an air tight container for further characterization Nakason et al., (2018). The selected temperature levels include 180°C, 200°C, 220°C and 240°C with a residence time of 4 hours which were designated as 180-4, 200-4, 220-4 and 240-4 respectively.

**Analytical procedures**

The moisture content, volatile matter, ash content and fixed carbon content of the samples have been determined by following the analytical procedures of ASTM (American Society of Testing and Materials).

The elemental composition (C, H, N, S and O) of the samples were determined using Elementar Vario EL III at CHNS operating mode with digestion temperature of 950-1200°C. The Higher Heating Value (HHV) of the samples were calculated from the elemental composition according to the correlation of Channiwala and Parikh Wilk (2016).

\[
\text{HHV (MJ Kg}^{-1}\text{)} = 0.349C + 1.1783H + 0.10055S - 0.1034O - 0.0015N - 0.0211A
\]

Where, C – Carbon, H – Hydrogen, S – Sulphur, O – Oxygen, N – Nitrogen, A – Ash content

The Solid yield, Energy Densification, fuel ratio and energetic recovery efficiency of the samples were also calculated Lin et al., (2015).

\[
\text{Fuel Ratio} = \frac{\text{Fixed Carbon (\%)}}{\text{Volatile matter (\%)}}
\]

\[
\text{Hydrochar yield} = \frac{\text{Mass of Hydrochar}}{\text{Mass of feedstock}}
\]

\[
\text{Energy Densification} = \frac{\text{HHV of Hydrochar}}{\text{HHV of feedstock}}
\]

**Results and Discussion**

The visual interpretation of sludge and different was carried out with the help of Figure 2 with special attention to color and texture. The dynamics in volatile matter, ash content and fixed carbon content has been shown in Figure 3. It can be seen that the volatile matter content of 240-4 have significantly decreased from 62.5% to 48.77% as compared to raw paper sludge that sums up to a reduction of 21%. This reduction resulted due to dehydration and decarboxylation reactions Kim et al., (2014). On the other hand, the fixed carbon percentage increased from 7.5% for sludge to a maximum value of 13.92% for 240-4. Nevertheless, the increment in fixed carbon was lower than the loss in volatile matter thereby indicating conversion of volatile compounds into liquid and gaseous products respectively Lin et al., (2015). The main reason behind the loss of volatile matter is that the organic composition of paper sludge like carbohydrates, proteins, cellulose and hemicellulose compounds gets decomposed and dissolved into liquid and gaseous portions of hydrothermal carbonization as glucose, fructose, amino acids and phenolic compounds Román, Nabais, González, González- García, and Ortiz (2012). Also, the loss of volatile matter and retainment of mineral matter attributed towards the increase of ash content from 30% to 37.3% for 240-4.

The fuel ratio and the Higher Heating Value (HHV) of the sludge and hydrochar samples were tabulated in table 1. The significance of fuel ratio is to evaluate the alternative of a solid fuel. As a result of increased fixed carbon at higher temperatures, the fuel ratio tends to increase from 0.12 for sludge to 0.285 for 240-4. The Higher Heating value increased gradually over the temperature rise,
however, higher ash content generation at higher process temperatures decreased the heating value Lin et al., (2015). It can be seen that the HHV increased gradually and attained a maximum value of 15.25 MJ Kg\(^{-1}\) for 220-4 and decreased for 240-4 (12.76 MJ Kg\(^{-1}\)) due to higher ash generation.

The coalification degree of the hydrochar can be assessed by Van Krevelen diagram (Fig. 4). Van Krevelen diagram encompasses the plotting of H/C and O/C atomic ratios in order to assess the fuel properties of the samples. The H/C and O/C ratios of the sludge were 1.74 and 0.8 which reduced to a lowest value of 1.4 and 0.4 for 220-4 respectively. The extent of decarboxylation and dehydration can be assessed by this diagram wherein the H/C and O/C ratios of conventional energy products like coal and lignin was compared. Generally, a compound with low H/C and O/C ratio can be considered as a fuel Kambo and Dutta (2014). It can be seen that the H/C and O/C ratios of the hydrochar samples were close to H/C and O/C ratio of lignite Liu and Balasubramanian (2012).

Table 1: Elemental composition and energy properties of sludge and hydrochar

| Sample | Carbon (%) | Hydrogen (%) | Nitrogen (%) | Sulphur (%) | Oxygen (%) | Higher heating value (MJ Kg\(^{-1}\)) | Fuel ratio | H/C ratio | O/C |
|--------|------------|--------------|--------------|-------------|------------|---------------------------------------|------------|-----------|-----|
| Sludge | 29.69      | 4.34         | 3.28         | 1.04        | 31.65      | 12.28                                 | 0.120      | 1.74229   | 0.80014 |
| 180-4  | 30.74      | 3.64         | 2.69         | 0.60        | 24.52      | 12.52                                 | 0.155      | 1.41275   | 0.59887 |
| 200-4  | 31.41      | 3.54         | 2.48         | 0.70        | 22.88      | 12.81                                 | 0.216      | 1.34235   | 0.54694 |
| 220-4  | 35.65      | 4.23         | 2.28         | 0.74        | 21.50      | 15.25                                 | 0.219      | 1.41486   | 0.45267 |
| 240-4  | 31.26      | 3.68         | 2.45         | 0.74        | 24.56      | 12.76                                 | 0.285      | 1.40364   | 0.58962 |

Fig.1 Experimental setup
**Fig. 2** Visual interpretation of sludge and different hydrochars

**Fig. 3** Proximate composition of sludge and hydrochars
Fig. 4 Van Krevelen diagram exhibiting the H/C and O/C ratios

Fig. 5 Solid yield, energy densification and energetic recovery efficiencies of hydrochar

The Hydrochar yields, Energy densification and energetic recovery efficiency of the hydrochar samples were exhibited in the Figure 5. The Hydrochar yield gradually increased over increased temperatures and attained a maximum yield of 62% for 240-4
thereby confirming higher extent of condensation at higher temperature. The energy densification value of 180-4 was 1.01 and attained a maximum value of 1.24 for 220-4. However, 240-4 showed energy densification value lower than other values. The energetic recovery efficiency was used to evaluate hydrothermal carbonization process which followed a proportionality with energy densification. Highest energetic recovery efficiency have been obtained for 220-4 (69.8%) followed by 240-4 (64.4%), 200-4 (60.6%) and 180-4 (57.4%) respectively.

The temperature changes on hydrothermal carbonization showed a significant effect on the energy properties of the hydrochar. It can be seen that 220-4 possessed good fuel property like higher heating value (15.25 MJ Kg⁻¹), lower H/C (1.41) and O/C ratio (0.45) and higher energetic recovery efficiency (69.8%). Also, the energy densification values and hydrochar yield were also taken into consideration. However, certain upscaled studies involving economics of the process need to be carried out so as to promote sustainability.

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