Boger nanofluid: significance of Coriolis and Lorentz forces on dynamics of rotating fluid subject to suction/injection via finite element simulation

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This study briefings the roles of Coriolis, and Lorentz forces on the dynamics of rotating nanofluids flow toward a continuously stretching sheet. The nanoparticles are incorporated because of their unusual qualities like upgrade the thermal transportation, which are very important in heat exchangers, modern nanotechnology, electronics, and material sciences. The primary goal of this study is to improve heat transportation. Appropriate similarity transformations are applied for the principal PDEs to transform into nonlinear dimensionless PDEs. A widely recognized Numerical scheme known as the Finite Element Method is employed to solve the resultant convective boundary layer balances. Higher input in the solvent fraction parameter has a rising effect on the primary velocity and secondary velocity magnitude, and decreasing impact on the distributions of temperature. It is seen that growing contributions of the Coriolis, and Lorentz forces cause to moderate the primary and secondary velocities, but the temperature and concentration functions show opposite trend. The concentration, temperature, and velocities distributions for suction case is prominently than that of injection case, but inverse trend is observed for local Nusselt and Sherwood numbers. These examinations are relevant to the field of plastic films, crystal growing, paper production, heat exchanger, and bio-medicine.

Background study. The fluids which are engineered by the homogeneous dispersion of metal and metallic oxide particles at the nanoscale are known as nanofluids1. The theoretical and experimental investigations confirm from the literature that the existence of nanoparticles in host fluid greatly affects the thermophysical properties of base fluids which exhibits poor conductivity properties2,3. The convective nanofluid heat transfer flow attracts numerous researchers due to their fascinating applications in every field of Science and Engineering. To name a few, the diamond and ceramic nanoparticles are used to upsurge the dielectric properties of the mineral oil, the fluid with nanoparticles can be used for direct absorption of the sunlight in solar collectors, the Zink and Titanium Oxide particles have antibacterial behavior and therefore which can be used for biomedical applications such as drug delivery and cancer therapy, and many more4–6. Ali et al7 discussed convective unsteady hybrid nanofluid flow within an upright channel by using Laplace Transform (LT) technique, in which authors developed fractional Maxwell fluid model is developed by using Caputo fractional differential operator. Awais et al.8 considered nanofluid assisting and opposing flow for exploring the Lie group analysis numerically with Adams-Bash forth technique (ABT). Abdelmalek et al.9 considered Cauchy’s stress tensor for third-grade fluid to investigate the dissipative nanofluid flow past an elongating sheet by adopting built-in Matlab routine bvp4c. Farooq et al.10 adopted a modified Cattaneo–Christov mass and heat flu model for the numerical explora-
tion of the Carreau nanofluid flow by horizontal stretching cylinder subject to the convective conditions. Subba Rao et al.11 studied the nanofluid (Buongiorno model) flow above the isothermal upright cone. There are some articles related to boundary layer flow along a nanoparticles12–14. The non-Newtonian fluids are technological importance. In nature, Boger fluids are also non-Newtonian fluids15,16.

There have been rising fascination in the investigation of the impact of Lorentz force produced due to magnetic field because of its modern applications in fluid engineering, assembling of plastic materials, hot rolling, production of glass fiber, and medical treatment17,18. Magnetic doubly stratified mixed convective flow with heat generation/absorption effects reported by Abbasi et al.19 and Alhussain et al.20 securitized numerically on Cattaneo-Christov flux model for the magneto nanofluid flow past a spinning cone embedded in an anisotropic permeable medium in the presence of cross-diffusion (Soret and Dufour), Navier slip, and Stefan blowing effects. The insight into significance of particles aggregation and carbon nanotube subject to rotating environment studied by Acharya et al.21,22. Jawad et al.23 obtained approximate analytical solutions using HAM for the energy irreversibility analysis on hydromagnetic nanofluid flow past a nonlinearly elongating permeable sheet. Jamshed24 employed Keller Box Method (KBM) to study the MHD nanofluid flow past a nonlinearly stretching sheet with entropy generation and viscous dissipation effects.

In the recent years, the growing interest in the examination of Coriolis force effects on the dynamics of fluid flow over a stretching sheet because of several real applications in astrophysical and geophysical problems, hot rolling, fiber production, and centrifugal bio-reactor25. Chu et al.26 explored numerically on nanofluid flow past a bidirectionally periodically moving surface in the presence of nonlinear radiation and heat source/sink effects by employing (HAM) Homotopy Analysis Method. Ali et al.27 employed GEM (Galerkin Finite Element Method) to explore the buoyant driven transient bio convective Maxwell nanofluid rotating 3D flow above the Riga plate with binary chemical reaction and activation energy. Ahmed et al.28 numerically investigated heat source/sink effects on stagnation point flow over stretching/shrinking rotating disk, Bilal et al.29 studied chemical reaction effects on magnetized nanofluid past a rotating cone with HAM, and khan et al.30 reported on the impact of heat source/sink effects subject to revised mass flux conditions for flow past rotating elongating cylinder. Ali et al.30 employed FEM to explore rotating Casson Carreau nanofluid flow over a sheet with Darcy–Forchheimer medium.

The scrupulous literature assessment cited above confirms that a little attention is made towards the Lorentz force embedded in Bogar nanofluid rotating flow past stretching surface under the influence of the Coriolis force and suction/injection, and present analysis is unique because of solvent fraction, Lorentz and Coriolis impact on dynamic of Bogar nanofluid. To the best of the author's knowledge, all the cited reports are not deliberated on the elaborated problem. Therefore, the prime aim of the current investigation is to investigate the heat and mass transfer effects on transient hydromagnetic rotating nanofluid 3D flow with suction/injection effects. Very recently, the hydromagnetic boundary layer flow for both Newtonian and non-Newtonian nanofluid flow fields was investigated by numerous authors31–33 by employing GEM with a weighted residual approach. The flow governing coupled highly nonlinear PDEs are solved by adopting a control volume approach by employing a Galerkin Finite Element Method34,35 with a weighted residual approach. The various flow field characteristics for numerous significant parameter changes are discussed and depicted pictorially. The computational results obtained through Matlab code blocks are corroborated with the existing literature and found to be a tolerable correlation. The friction factor, Nusselt number, and Sherwood number values are computed and documented in obtained through Matlab code blocks are corroborated with the existing literature and found to be a tolerable correlation. The friction factor, Nusselt number, and Sherwood number values are computed and documented in

Research questions. This study provide answers to below related scientific research questions:

1. To observe the influence of Coriolis and Lorentz forces on the Boger fluid dynamics of temperature, fluid velocity, and concentration distributions with suction/injection?
2. What is the effect of combine affect of Brownian motion, thermophoresis, Coriolis and Lorentz forces on the mass transfer rate, skin friction tensors, and heat transfer rate with suction/injection?
3. Assess the Brownian motion, and thermophoresis parameters effect the temperature and tiny particles concentration profile?

Geometry and mathematical formulation

The transient magnetohydrodynamic 3D rotating flow of nanofluid past a bidirectional stretching sheet is considered. The physical flow configuration and coordinate system of elaborated problem is shown in Fig. 1, and flow is confined to $z \geq 0$. The nanofluid flow rotating about the $z$-direction with angular constant velocity $\Omega$. At $z = t = 0$, the surface is elongated in the direction of $x$ along with velocity $u_\infty = \hat{a}x$. In axial direction ($z$-direction), a static and uniform field of magnetic $B_0$ is applied. Less magnetic filed is induced due to low magnetic Reynolds number, so that Hall current and Ohmic dissipation are insignificant. The ambient concentration and temperature is $C_\infty$ and $T_\infty$, while surface concentration and temperature is represented by $C_\nu$ and $T_\nu$, respectively. The field of velocity for the current elaborate problem is considered by $V = (u_1(x, y, z), u_2(x, y, z), u_3(x, y, z))$. In view of above assumptions and boundary layer approximation, the equations of conservation of mass, linear-momentums, temperature, and concentration are expressed as36,37:

$$\partial_t u_1 + \partial_j u_j + \partial_z u_3 = 0,$$  \hspace{1cm} (1)

$$\rho_0 (\partial_t u_1 + u_j \partial_j u_1 + u_2 \partial_2 u_1 + u_3 \partial_3 u_1 + 2\Omega u_2) = -\partial_z p + \mu_0 \left(1 + \frac{\beta_1}{1 + \beta_2}\right) \partial_{zz} u_1 - \sigma_\eta B_0^2 u_1,$$  \hspace{1cm} (2)
In view of Eq. (10), the Eq. (1) is valid and the Eqs. (2–9) becomes below mention non-linear PDEs into transformed coordinate systems (ζ, η).

\[
\begin{align*}
\rho_n f (\partial_t u_2 + u_1 \partial_z u_2 + u_2 \partial_p u_2 + u_3 \partial_\zeta u_2 - 2\Omega u_1) &= -\partial_p p + \mu_n f \left( \frac{1 + \beta_1}{1 + \beta_2} \right) \partial_{zz} u_2 - \sigma_n f B_0^2 u_2, \\
\rho_n f (\partial_t u_3 + u_1 \partial_z u_3 + u_2 \partial_p u_3 + u_3 \partial_\zeta u_3) &= -\partial_p p + \mu_n f \partial_{zz} u_3, \\
\partial_t T + u_1 \partial_z T + u_2 \partial_p T + u_3 \partial_\zeta T &= \alpha_n f \partial_{zz} T + \tau^* \left( \frac{D_{\zeta} \partial_\zeta T}{T} \right)^2, \\
\partial_t C + u_1 \partial_z C + u_2 \partial_p C + u_3 \partial_\zeta C &= D_n \partial_{zz} C + \frac{D_T}{T_\infty} \partial_{zz} T.
\end{align*}
\]

In the above equations, \( C \) and \( T \) are the tiny particles concentration, and temperature of fluid, \( (D_T, D_b) \) are the thermophoresis, and Brownian diffusion coefficients, \( (\rho_n f, \alpha_n f, \mu_n f, \beta_1, \beta_2) \) are respectively the thermal diffusivity, density, dynamic viscosity of fluid, solvent fraction parameter, and ratio of relaxation time, respectively. The boundary conditions are\(^{36,38}\):

\[
\begin{align*}
t < 0 : u_1 &= 0, u_2 = 0, u_3 = 0, C = C_\infty, T = T_\infty, \\
t \geq 0 : u_1 = a(x), u_2 = 0, u_3 = -w_0, C = C_w, T = T_w, as z = 0, \\
t \geq 0 : u_1 \to 0, u_2 \to 0, C \to C_\infty, T \to T_\infty, as z \to \infty.
\end{align*}
\]

The complexity of elaborated problem is reduced by introducing the below similarity transformations (see Refs.\(^{36,38}\)):

\[
\begin{align*}
u_1 &= \tilde{a}x \frac{\beta F(\xi, \eta)}{\beta}, \quad u_2 = \tilde{a}x G(\xi, \eta), \quad u_3 = -\sqrt{\tilde{a}v \xi F(\xi, \eta)}, \quad \xi = 1 - e^{-\gamma}, \eta = \sqrt{\frac{ax^2}{\xi}}. \\
\Gamma &= \tilde{a}t, T = (T_w - T_\infty) \theta(\xi, \eta) + T_\infty, \quad C = (C_w - C_\infty) \Phi(\xi, \eta) + C_\infty.
\end{align*}
\]

In view of Eq. (10), the Eq. (1) is valid and the Eqs. (2–9) becomes below mention non-linear PDEs into transformed coordinate systems (\( \zeta, \eta \)).

\[
\begin{align*}
\frac{1 + \beta_1}{1 + \beta_2} F'''' + 0.5 \eta F'' - 0.5 \xi \eta F'' + \xi (\xi F'' - F' - M^2 F + 2 \xi G - \xi(1 - \xi) \frac{\partial F'}{\partial \xi} = 0, \\
\frac{1 + \beta_1}{1 + \beta_2} G'''' + 0.5 \eta G'' - 0.5 \xi \eta G'' + \xi (\xi G'' - 2 \xi F' - M^2 G - F' G) - \xi(1 - \xi) \frac{\partial G'}{\partial \xi} = 0, \\
\theta'' + 0.5 \eta(1 - \xi) Pr \theta' + \xi Pr F \theta' + N_t Pr \theta \Phi + N_t Pr \theta^2 - \xi(1 - \xi) \frac{\partial \theta}{\partial \xi} = 0.
\end{align*}
\]
\[ \Phi'' + 0.5\eta Le(1 - \zeta)\Phi' + Le\zeta\Phi' + N_t N_p^{-1}\theta'' - \zeta(1 - \zeta)Le \frac{\partial \Phi}{\partial \zeta} = 0, \quad (14) \]

\[ F(\zeta, 0) = \Gamma, \quad G(\zeta, 0) = 0, \quad F'(\zeta, 0) = \Phi(\zeta, 0) = \theta(\zeta, 0) = 1, \quad \zeta \geq 0, \quad \text{at} \ \eta = 0, \quad F'(\zeta, \infty) \rightarrow 0, \quad G(\zeta, \infty) \rightarrow 0, \quad \Phi(\zeta, \infty) \rightarrow 0, \quad \theta(\zeta, \infty) \rightarrow 0, \quad \zeta \geq 0, \quad \text{as} \ \eta \rightarrow \infty, \quad (15) \]

where primes (',', '') denote the d.r.t. The rotating (\( \lambda \)), magnetic (\( M \)), Prandtl number (\( Pr \)), Lewis number (\( Le \)), Brownian motion (\( N_b \)), thermophoresis (\( N_t \)), and suction/injection (\( \Gamma \)) parameters are defined as:

\[ \lambda = \frac{\Omega}{a}, \quad M = \sqrt{\frac{\sigma_{nj} D^2}{\rho_1 a}}, \quad Pr = \frac{\nu}{\alpha_{nj}}, \quad Le = \frac{\nu}{D_B}, \quad Lb = \frac{\nu}{D_m}, \quad N_b = \tau \nu^{-1} D_B (C_w - C_\infty), \]

\[ N_t = \frac{D_T (\tau T_w - \tau T_\infty)}{\nu T_\infty}, \quad \Gamma = \frac{w_0}{\sqrt{a} v \zeta}. \]

Expressions of local Nusselt number, Sherwood number, and coefficients of skin friction are defined as:

\[ Nu = \frac{x q_w}{\kappa (T_w - T_\infty)}, \quad Shr = \frac{x q_m}{D_B (C_w - C_\infty)}, \quad C_f = \frac{\tau_w}{\rho u_1}, \quad C_f = \frac{\tau_w}{\rho u_1^2}. \quad (16) \]

Here, tensor of skin friction at wall are \( \tau_w = \mu \left( \frac{1 + \beta_1}{1 + \beta_2} \right) (\partial U_1 / \partial z)_{z=0} \) (x-direction) and \( \tau_w = \mu \left( \frac{1 + \beta_1}{1 + \beta_2} \right) (\partial U_2 / \partial z)_{z=0} \) (y-direction), the mass, and heat flux at the sheet are \( q_m = -D_B (\partial C / \partial z)_{z=0}, \) and \( q_w = -\kappa (\partial T / \partial z)_{z=0}. \) Using Eq. (10):

\[ \begin{align*}
C_f_{Lc} Re_x^{1/2} &= \left( \frac{1 + \beta_1}{1 + \beta_2} \right) F''(0) \sqrt{\tau}, \quad C_f_{Lc} Re_x^{1/2} = \left( \frac{1 + \beta_1}{1 + \beta_2} \right) G'(0) \sqrt{\tau}, \\
Nux Re_x^{1/2} &= \frac{\theta'(0)}{\sqrt{\tau}}, \quad Shr_x Re_x^{1/2} = \frac{\Phi'(0)}{\sqrt{\tau}}.
\end{align*} \quad (17) \]

**Numerical solution**

**Finite element method.** This numerical technique is very powerful tool reported by the experts to solve the modern engineering and industrial problems due to its accuracy and computability\(^{38,40}. \) In this technique, below steps are involved:

**Finite-element discretisation.** First, the whole computational domain is distributed into sub-interval of a finite number and these sub-intervals are called elements, and set of these elements represent the finite element mesh.

**Generation of the element equations.**

(i) On the base of finite element mesh, a variational formulation of the problem is performed.

(ii) In above (i), the element equations are generated with the aid of approximation solution.

(iii) Construct a stiffness matrix by using interpolation functions.

**Assembly of element equations.** After generation of the elements equation, we assembled all the generated elements equations through inter element continuity condition, and obtained a model which called global finite element model over a entire computational domain.

**Imposition of boundary conditions.** The elaborated boundary conditions of the current problem are utilized on the obtained assembled equations.

**Solution of assembled equations.** Finally, we solved the assembled equations iteratively. To justify the validity of finite element computations, a study for grid independence is conducted. The whole domain is divided into different mesh density of grids size, and observe no more variation after 100 × 100, so we fixed the all computations on 100 × 100 grid size (see Table 1). The comparison with earlier studies are documented in Tables 2 and 3 in particular cases are carried out to get the conformism of the precision of the solution methodology. It is witnessed that the current numerical computations are in close agreement with the existing literature in some limiting cases. The Finite Element computations for friction factor along with axial and transverse directions \(-F''(0)\) & \(-G(0)\) respectively tabulated in Table 2 for different values of rotation parameter \( \lambda \) = 0, 1, 2, 5 at \( \zeta = 1. \) It is observed from Table 2 that the numerical results so obtained are in good correlation with the results reported by Ali et al.\(^{41}. \) and Wang\(^{42}. \) Further, in Table 3, the Nusselt number \(-\theta(0)\) values are corroborated between Ali et al.\(^{43} \) and Shaflique et al.\(^{44} \), and present FEM results for diverse values \( \lambda, \beta, \text{&} Pr, \) and found that they are in good agreement. Hence, the confidence in the numerical computations and confirm that the Finite Element Computations obtained through Matlab code are attained the good convergence rate.
To solve the Eqs. (11) to (14) along boundary conditions (15), first consider:

\[ F' = H, \]  

The set of Eqs. (11)–(15) reduced to lesser order:

\[ \left( \frac{1 + \beta_1}{1 + \beta_2} \right) H'' + 0.5(1 - \zeta) \eta H' + \zeta (FH' - H^2 + 2\lambda G - M^2 H) = \frac{\partial H}{\partial \zeta} - \zeta^2 \frac{\partial H}{\partial \zeta}, \]  

\[ \left( \frac{1 + \beta_1}{1 + \beta_2} \right) G'' + 0.5\eta G' - 0.5\eta \zeta G' + \zeta (FG' - 2\lambda F' - M^2 G - F' G) = \frac{\partial G}{\partial \zeta} - \zeta^2 \frac{\partial G}{\partial \zeta}, \]  

\[ \Pr^{-1} \theta'' + 0.5\eta(1 - \zeta) \theta' + \zeta F\theta' + N_b \theta' \Phi' + N_t \theta^2 = \frac{\partial \theta}{\partial \zeta} - \zeta^2 \frac{\partial \theta}{\partial \zeta}. \]  

\[ \Phi'' + 0.5Le(1 - \zeta) \eta \Phi' + Le \zeta F \Phi' + N_b N_t^{-1} \theta'^2 = \zeta (1 - \zeta) Le \frac{\partial \Phi}{\partial \zeta}, \]  

\[ F(\zeta, 0) = \Gamma, \ G(\zeta, 0) = 0, \ \Phi(\zeta, 0) = H(\zeta, 0) = 0, \ \theta(\zeta, 0) = 1, \ \zeta \geq 0, \ at \ \eta = 0, \ H(\zeta, \infty) \to 0, \ G(\zeta, \infty) \to 0, \ \Phi(\zeta, \infty) \to 0, \ \theta(\zeta, \infty) \to 0, \ \zeta \geq 0, \ as \ \eta \to \infty. \]  

For numerical computation, the plate length fixed at \( \zeta = 1.0 \) and thickness at \( \eta = 5.0 \). The variational form connected along with Eqs. (18)–(22) can be written as:

\[ \int_{\Omega} \omega H \left[ F' - H \right] d\Omega = 0, \]  

### Table 1. Study of Grid independence for different grid sizes at \( \zeta = 1.0 \).

| Grid size | \(-F''(0, 0)\) | \(-G'(0, 0)\) | \(-\theta'(0, 0)\) | \(-\Phi'(0, 0)\) |
|-----------|----------------|----------------|----------------|----------------|
| 10 × 10   | 2.7911         | 1.9890         | 0.7145         | 3.2679         |
| 40 × 40   | 2.7611         | 1.0827         | 0.6711         | 3.1553         |
| 75 × 75   | 2.7553         | 1.0747         | 0.6865         | 3.0912         |
| 100 × 100 | 2.7550         | 1.0743         | 0.6861         | 3.0908         |
| 120 × 120 | 2.7549         | 1.0740         | 0.6860         | 3.0905         |

### Table 2. Comparison of skin friction \(-G'(0)\) and \(-F''(0)\) for various values of \( \lambda \) at \( \zeta = 1 \) when ignore other involved parameters.

| \( \lambda \) | \( \beta \) | \( \Pr \) | Ali et al. \[41\] | Wang \[42\] | Present |
|--------------|-----------|--------|----------------|----------|---------|
| 0.0          | 1.0       | 0.546683 | 0.54670        | 0.546828 |
| 1.0          | 0.4       | 0.528090 | 0.52809        | 0.5280903|
| 2.0          | 0.6       | –       | 0.51009        | 0.5100870|
| 5.0          | 0.8       | –       | 0.492547       | 0.4925468|

### Table 3. Comparison of Nusselt number \(-\theta'(0)\) for \( \zeta = 1 \) and different values of rotating parameters \( \lambda \) when other parameters are zeros.

| \( \lambda \) | \( \beta \) | \( \Pr \) | Ali et al. \[43\] | Shafique et al. \[44\] | FEM (our results) |
|--------------|-----------|--------|----------------|----------------|----------------|
| 0.2          | 0.2       | 1.0    | 0.546683       | 0.54670        | 0.5466828      |
| –            | 0.4       | –      | 0.528090       | 0.52809        | 0.5280903      |
| –            | 0.6       | –      | 0.51009        | 0.5100870      |                |
| –            | 0.8       | –      | 0.492547       | 0.49255        | 0.4925468      |
where \( \omega \) is given by:

\[
\omega = \sum_{j=1}^{4} F_j \gamma_j(\xi, \eta, \theta) = \sum_{j=1}^{4} G_j \gamma_j(\xi, \eta, \theta).
\]

Here, \( F_j, L_i, H_i, G_i, \) and \( \gamma_j \) are the linear interpolation functions for \( \Omega_\varepsilon \) given by:

\[
\begin{align*}
\gamma_1 &= \left( \frac{\xi - \xi_0}{\xi_1 - \xi_0}, \frac{\eta - \eta_0}{\eta_1 - \eta_0} \right), \\
\gamma_2 &= \left( \frac{\xi - \xi_1}{\xi_2 - \xi_1}, \frac{\eta - \eta_1}{\eta_2 - \eta_1} \right), \\
\gamma_3 &= \left( \frac{\xi - \xi_2}{\xi_3 - \xi_2}, \frac{\eta - \eta_2}{\eta_3 - \eta_2} \right), \\
\gamma_4 &= \left( \frac{\xi - \xi_3}{\xi_4 - \xi_3}, \frac{\eta - \eta_3}{\eta_4 - \eta_3} \right).
\end{align*}
\]

The develop finite-elements model of the equations is given by:

\[
\begin{bmatrix}
L_{11} & L_{12} & L_{13} & L_{14} & L_{15} \\
L_{21} & L_{22} & L_{23} & L_{24} & L_{25} \\
L_{31} & L_{32} & L_{33} & L_{34} & L_{35} \\
L_{41} & L_{42} & L_{43} & L_{44} & L_{45} \\
L_{51} & L_{52} & L_{53} & L_{54} & L_{55}
\end{bmatrix}
\begin{bmatrix}
[F] \\
[Q] \\
[H] \\
[\theta] \\
[\Phi]
\end{bmatrix}
= \begin{bmatrix}
[R_1] \\
[R_2] \\
[R_3] \\
[R_4] \\
[R_5]
\end{bmatrix}
\]
In this section, we show the significance of suction/injection on dynamics of Maxwell rotating fluid subject to Coriolis force, magnetohydrodynamic, and gyrotactic microorganism via finite element simulation. In each of the figures for these quantities, three sets of curves are drawn for varying values of suction/injection parameter: (i) $\Gamma = -0.2$ (suction), (ii) $\Gamma = 0.0$ (static), and (iii) $\Gamma = 0.2$ (for injection and Table 1). The default values of the parameters in the study were: $\lambda = M = 1.0, N_0 = N_f = 0.2, \beta_1 = 0.2, \beta_2 = 2.0, \alpha = 10, Pr = 6.2$.

The primary and secondary velocity distributions for different values of solvent fraction parameter, magnetic field parameter, rotation parameter, and unsteady parameter are portrayed in Figs. 3, 4, 5 and 6, respectively. The velocity distributions for various parameters is portrayed in Fig. 3a,b and figure exhibits that the velocity distributions is upgraded by solvent fraction parameter $\beta_1$. Actually, at low Reynolds number, the flow rate of
Bogar nanofluid increases so at constant viscosity, Bogar fluid is highly elastic. Figure 4a,b displays that $F'(\zeta, \eta)$ and $G'(\zeta, \eta)$ for different values of magnetic field parameter. The existence of the resistive force in the form of Lorentz force is due to the inclusion of enhancing external magnetic field and leads to deceleration of the axial momentum in Fig. 4a while an opposite behavior is perceived for transverse momentum in Fig. 4b. The axial momentum $F'(\zeta, \eta)$ and Transverse momentum $G'(\zeta, \eta)$ for several values of rotation parameter portrayed in Fig. 5a,b respectively. It is witnessed from Fig. 5a that the declining of the axial momentum for growing values of rotation parameter due to Coriolis force whereas an opposed action is alleged for transverse momentum in Fig. 5b. For growing values of time-dependent parameter, the increase in the thickness of momentum boundary layer in the transverse direction and reduction of the thickness of the momentum boundary layer in the axial direction is depicted in Fig. 6a,b respectively. Thus, it confirms that the unsteadiness parameter is vital in controlling the momentum in the axial direction. Moreover from these graphs, it is perceived that the $F'(\zeta, \eta)$
reduces against the strength of $\Gamma = 0.2$ (injection), but it is slightly boosted up directly with $\Gamma = -0.2$ (suction) parameter.

The sketches of $C_f R_{ex}^{1/2}$ (friction factor) along axial and $C_f R_{ex}^{1/2}$ (transverse directions) near the surface for the range of $\zeta (0: 0.2 : 1)$ is represented in Fig. 7a,b for $\beta_1 (0.2 : 0.2 : 0.8)$. Figure 7a shows that for increasing $\zeta (0 \to 1)$, the distribution of $C_f R_{ex}^{1/2}$ is increased gradually up to a constant rate and then after no significant change is observed. Whereas for enhancing $\beta_1$, a significant reduction in $C_f R_{ex}^{1/2}$ near the sheet surface is observed. For increasing $\zeta (0 \to 1)$, the distribution of $C_f R_{ex}^{1/2}$ is reduced gradually up to a constant rate and then after no significant change is observed as shown Fig. 7b, while enhancing $\beta_1$. The significant difference in the values of $C_f R_{ex}^{1/2}$ near the sheet surface is observed. Moreover from these graphs, it is perceived that the values of $C_f R_{ex}^{1/2}$ and $C_f R_{ex}^{1/2}$ for the case of $\Gamma = 0.2$ (injection) are lesser than the case of $\Gamma = -0.2$ (suction).

The $\theta(\zeta, \eta)$ distribution for various parameters is portrayed in Figs. 8, 9 and 10. The influence of effect of solvent fraction parameter ($\beta_1$) and time-dependent ($\tau$) on temperature is shown in Fig. 8a,b, respectively. The

Figure 7. Impact of $\beta_1$ on $C_f R_{ex}^{1/2}$ in x-direction, and $C_f R_{ex}^{1/2}$ in y-direction.

Figure 8. Impact of $\beta_1$ and $\tau$ on $\theta(\zeta, \eta)$ at $\zeta = 1$.

Figure 9. Impact of $M$ and $\lambda$ on $\theta(\zeta, \eta)$ at $\zeta = 1$. 
Figure 10. Impact of $N_b$ and $N_t$ on $\theta(\zeta, \eta)$ at $\zeta = 1$.

Figure 11. Fluctuation of $N_{b\text{e}}R_{e1}^{1/2}$ against $N_b$, $N_t$, $M$, and $\lambda$.

$\theta(\zeta, \eta)$ profiles is decreased along with $\beta_1$, and increased against growing strength of unsteady parameter. Figure 9 exhibits that the temperature distributions is upgraded by magnetic field parameter. The net resulting net force usually known as resistive Lorentz force between the external magnetic field and internal electric field controls the flow momentum, which is depicted in Fig. 9a, while the thickness of the thermal boundary layer is increased for enhancing $\lambda$ as shown in Fig. 9b. The impact of thermophoresis ($N_t$) and Brownian motion ($N_b$) parameters on temperature is shown in Fig. 10a,b respectively. The distribution of temperature profiles is increased along with $N_b$ and $N_t$. Further, from these graphs, it is perceived that the $\theta(\zeta, \eta)$ reduces against the strength of $\Gamma = 0.2$ (injection), but it is boosted up directly with $\Gamma = -0.2$ (suction) parameter. The sketches of local Nusselt number ($N_{b\text{e}}R_{e1}^{1/2}$) at $N_b$&$N_t(0.1 : 0.1 : 0.3)$ is represented in Fig. 11a,b for $M(0 : 1 : 5)$&$\lambda(0 : 1 : 5)$ respectively. For increasing $M$ and $\lambda$, the distribution of ($N_{b\text{e}}R_{e1}^{1/2}$) is decreased gradually. A significant reduction in ($N_{b\text{e}}R_{e1}^{1/2}$) near the sheet surface is observed for growing values of $N_b$&$N_t$. It is also perceived from the figure that the for the case of $\Gamma = 0.2$ (injection) has a larger amount in ($N_{b\text{e}}R_{e1}^{1/2}$).

Figure 12a,b displays that $(\Phi(\zeta, \eta))$ for different values of magnetic field $M$, and rotation $\lambda$ parameters. The concentration profiles are enhanced for increasing values of the magnetic field and rotating parameters as shown in Fig. 12a,b. From Fig. 13a,b revealed that the $\Phi(\zeta, \eta)$ distribution profile is decrease again growing input of $N_b$, and it notably rise against the $N_t$. It is reported notably fall against the Lewis number $Le$, and time dependent parameter ($\tau$) parameters (see Fig. 14a,b). The behavior of local Sherwood number ($Sh_{\text{e}}R_{e1}^{1/2}$) is portrayed in Fig. 15a,b for $M(0 : 1 : 5)$&$\lambda(0 : 1 : 5)$ respectively at $N_b$&$N_t(0.1 : 0.1 : 0.3)$. For increasing $M$ and $\lambda$, the distribution of ($Sh_{\text{e}}R_{e1}^{1/2}$) is decreased. Whereas for increasing $N_b$&$N_t$, an opposite trend is observed and it is also witnessed that the $\Gamma = 0.2$ (injection) case has larger ($Sh_{\text{e}}R_{e1}^{1/2}$) than that of $\Gamma = -0.2$ (suction) case.

Conclusions

In this report, the finite element analysis on the transient magnetohydrodynamic three-dimensional rotating flow of nanofluid flow past a bidirectional stretching sheet with suction/injection, Coriolis, and Lorentz forces has been explored numerically. Based on the observed analysis of outcomes, it is worth concluding that:

1. Higher input in the Coriolis and Lorentz has a decreasing effect on the primary velocity and secondary velocity magnitude, and
   - an increasing impact on the distributions of temperature and concentration.
   - increase the magnitude of $C_f R_{e1}^{1/(\gamma - 1)}$ (skin friction factor).
   - the velocity, temperature, and concentrations components reduce against the strength of injection.

\[ \frac{\partial N_{b\text{e}}R_{e1}^{1/2}}{\partial \lambda} \]
2. Higher input in the solvent fraction parameter has a rising effect on the primary velocity and secondary velocity magnitude, and
- decreasing impact on the distributions of temperature.
- decrease the magnitude of $C_{f_x} R_{e_x}^{1/2}$ (skin friction factor).

3. Simultaneous increase in Brownian motion and thermophoresis parameters have an increasing impact on the distribution of temperature, and
- a negative effects on $Nu_x R_{e_x}^{1/2}$ and positive effects on $Sh_{r_x} R_{e_x}^{1/2}$.
- injection has a larger amount in $Nu_x R_{e_x}^{1/2}$ and $Sh_{r_x} R_{e_x}^{1/2}$ injection case has larger $Sh_{r_x} R_{e_x}^{1/2}$ than that of suction case.

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Figure 12. Impact of $M$ and $\lambda$ on $\Phi(\zeta, \eta)$ at $\zeta = 1$.

Figure 13. Impact of $Nb$ and $N_{t}$ on $\Phi(\zeta, \eta)$ at $\zeta = 1$.

Figure 14. Impact of $Le$ and $\tau$ on $\Phi(\zeta, \eta)$ at $\zeta = 1$. 
4. Tiny particles concentration diminishes against incremented Lewis number, unsteady, and Brownian motion parameters and exhibits rise against thermophoresis.

After successful computational struggle of parametric influence on the fluid dynamics, this study can be extend in future for Maxwell-nanofluid, Oldroyd-B nanofluid, comparative study between tangent-hyperbolic and Maxwell nanofluid, and viscoelastic Jeffrey’s nanofluids.

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B.A. and S.H. float the idea; I.S., D.B. and B.A. did the mathematical formulation and performed the solution; L.A. performed the mathematical formulation; B.A., I.S., D.B. and S.H. wrote the paper. All authors contributed equally. All authors have read and approved the final manuscript.

Competing interests
The authors declare no competing interests.

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