STUDYING GROWTH CHARACTERISTICS OF YEAST STRAINS ON VEGETAL FERMENTATION MEDIA AND WITH VITAMIN SUPPLEMENTATION

J. MOLNÁR* and B. ÁSVÁNYI

Department of Food Science, Agricultural and Food Sciences, Széchenyi István University, H-9200 Mosonmagyaróvár, Lucsony utca 15–17. Hungary

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The primary purpose of these researches was to optimize single-cell protein (SCP) production process using Saccharomyces cerevisiae NCAIM Y.00200 and Kluyveromyces marxianus DSM 4908 strain, and then to analyse the changes in yield of single-cell protein final product using vitamin supplementation. To determine these values, the total sugar content of the fermentation medium, and the protein content of the yeast was determined. During our work, a particular attention was paid to the change of sugar content and yeast protein quantity. Besides, yield (Yₓ,s) values, typical of the whole fermentation, were also measured. Protein yield, as the final product of fermentation, featured the efficiency of our work. The results of our optimized trial settings that were considered as control, using S. cerevisiae NCAIM Y.00200 and K. marxianus DSM 4908 strains, were compared with the results of vitamin-supplemented fermentation processes. On this basis, we can say that during our trials vitamin supplementation did not influence the final product yield of processes. The counted protein yields during fermentation were between 0.4–0.7 g g⁻¹.

Keywords: fermentation, single-cell protein, feed supplement, yeast strain, vitamin solution

Single-cell proteins were first applied during World War II in Germany and Russia to satisfy human protein demand. Nowadays, they are mainly sold as therapeutical product, and as baking yeast (MOLNÁR et al., 2016). These days satisfying protein demand is a bigger and bigger problem, since the population is constantly increasing. In 1950 2.5 billion people lived on Earth, and the number of population will reach 9.15 billion by 2050. It means a 2.25 billion people increase compared to 6.9 billion people in 2010. Along with it, the world’s needs for food will increase by 70–90%, which trends mainly towards calorie intake and meat consumption (HUNGARIAN MINISTRY OF AGRICULTURE, 2016). To satisfy this increasing protein demand, one solution could be implanting SCP (single-cell protein) in human nutrition, apart from traditional protein sources (ANUPAMA & RAVINDRA, 2000). Also, it is utilized as feed supplement to substitute animal feedstuff (KIM et al., 1998). Besides, it also has positive effect on the physiological state of the animal, most significantly in immune system stimulation (Li et al., 2016). Due to the prosperous content values of SCP, its utilization in feed industry, and the vitamin accumulating ability of yeasts, our purpose was to optimize the production process, and then to further analyse the change of final product yield using vitamin supplementation.

* To whom correspondence should be addressed.
Phone: +36 30 6074009; e-mail: molnar.judit@sze.hu

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1. Materials and method

Our experiments were done at the Department of Food Science, Agricultural and Food Sciences of Széchenyi István University, in Biostat A plus (Sartorius AG, Göttingen, Germany) type, in mixed and aerated fermenter with a reactor volume of 5 dm³, employing batchwise fermentation. The applied concentration of anti-foam agent was 0.1 cm³ dm⁻³. During fermentations the possible Crabtree effect did not emerge, there was no sign of its evolvement. The actual values of the set fermentation parameters (temperature, dissolved oxygen, agitation, and pH) were monitored, and also the data were recorded by BIO PAT MFCS/DA (BIOPAT, Göttingen, Germany) software belonging to the equipment. The mathematical statistical analysis was done by MS Excel program (Microsoft, Redmond, WA, USA). Determining the significance level of optimized (control) process results and the vitamin supplemented process results was done by MicroCal Origin 3.0. (MicroCal Software, Northampton, MA, USA) software. According to our previous overview of the literature, \textit{S. cerevisiae} yeast species are mainly applied during the production of alcohol and single-cell protein, therefore our chosen yeast strain was \textit{S. cerevisiae} NCAIM Y.00200. \textit{K. marxianus} yeast species are utilized mainly for solutions based on lactose to produce single-cell protein, although some of the literature deals with the same species utilized for vegetal based solutions to produce single-cell protein. Therefore, our other chosen yeast strain was \textit{K. marxianus} DSM 4908. The \textit{S. cerevisiae} NCAIM Y.00200 strain was acquired in lyophilised state from the National Collection of Agricultural and Industrial Microorganisms (Budapest). The freeze-dried \textit{K. marxianus} DSM 4908 was from the strain collection of Deutsche Sammlung von Mikroorganismen und Zellkulturen (Braunschweig, Germany). We got the strains vacuum packaged, freeze-dried, in double ampoule. First the lyophilised preparation was rehydrated in saline (6.5 g dm⁻³ NaCl) – during trials we used saline to make solutions because they have positive effect on the vital functions of the yeasts –, and then it was inoculated in YGC (yeast-glucose–chloramphenicol) broth and incubated at 25 °C for 48 h. After that the yeasts were transferred from broth to YGC medium to prepare pure culture. After reviving the strains, the inoculum was prepared the following way: one lamella of yeast culture was washed into 50 cm³ saline (6.5 g dm⁻³ NaCl), which ensured the required degree of concentration (10⁶ cell cm⁻³; ALBERTIN et al., 2011). Cell density was checked with Buerker-chamber cell counter, and the final concentration was set with dilution. Molasses for the fermentation media was provided by Győr Distillery Co. Ltd. Its most significant parameters are as follows: sugar content of 45.0 °Bx, pH of 7.35, density of 1.38 g cm⁻³, dry matter value of 71.5 g/100 g, aerobic mesophilic germ count of 5.5×10³ CFU cm⁻³, yeast cell count of 3.1×10² CFU cm⁻³. Also, molasses contain other useful components needed for the growth of yeast. Constituents of molasses recorded by SOLYOM and LASZTITY (1980) can be seen in Table 1.

Molasses were heat-treated (80 °C/ 15 min) prior to use.

Corn steep liquor was provided by Kévés Llc., Soltvadkert, which was also heat-treated (80 °C/ 15 min). Also, the most important content parameters of corn steep liquor were determined as follows: pH of 4.1; dry matter content of 46.3 g/100 g, from which protein is 40.5 g/100 g; sugar content: monosaccharides of maximum 5%, polysaccharides of maximum 20%, lactic acid of 21–25%; aerobic mesophilic germ count of 7.64×10² CFU cm⁻³, yeast cell count of 1.04×10⁴ CFU cm⁻³. Other components present in corn steep liquor needed for growth of yeast are summarized in Table 2 (DEMAIN & SOLOMON, 1986).
Table 1. Constituents of molasses (SÓLYOM & LÁSZTITY, 1980)

| Components                      | Concentration (%) |
|---------------------------------|-------------------|
| Water content                   | 16.5              |
| Saccharose content              | 51                |
| Nitrogen-free non-sugars:       |                   |
| Invert sugar                    | 1                 |
| Raffinose                       | 1                 |
| Nitrogenous components:         | 19                |
| Free and combined acids         |                   |
| Colouring matters               |                   |
| Bios materials                  |                   |
| Others                          |                   |
| Minerals (ash components)       | 11.5              |
| Total                           | 100               |

Table 2. Identifying the contents of corn steep liquor (DEMAIN & SOLOMON, 1986)

| Components              | Concentration          |
|-------------------------|------------------------|
| Dry matter content      | 50%                    |
| Protein content         | 24%                    |
| Carbohydrate            | 5.8%                   |
| Fat                     | 1%                     |
| Fibre content           | 1%                     |
| Ash content             | 8.8%                   |
| Biotin                  | 0.88 mg kg⁻¹           |
| Pyridoxine              | 19.36 mg kg⁻¹          |
| Thiamine                | 0.88 mg kg⁻¹           |
| Panthotenic acid        | 74.8 mg kg⁻¹           |
| Free amino acids        | 4.9%                   |

For each fermentation, 2–2 dm³ of both molasses and corn steep liquor solution was used, with triple dilution to set the proper carbo-hydrate content: 1.345 cm³ of saline (6.5 g dm⁻³ NaCl) was added to the available 655 cm³ of molasses and corn steep liquor, so the final fermentation media used for our experiments were acquired.

First, fermentation parameters of *K. marxianus* DSM 4908 and *S. cerevisiae* NCAIM Y.00200 [25–30 ºC; 4.5–5.5 pH value; 100–200–300–400 r.p.m.; 1–1.5 v.v.m. (vessel volumes per min)] on corn steep liquor and molasses were optimized to produce single-cell protein. These were chosen mainly according to the scientific literature (CÁCERES-FARFÁN et al., 2008; EL-GENDY et al., 2013; TRA VIÑA-MUÑOZ et al., 2013). The optimized (control) values are given in Table 3.

The optimized fermentation process was vitamin supplemented to study the effect of the vitamin solution on the final product yield. Prior to our trials, we had studied the scientific literature, where enrichment was employed during fermentation processes to supplement micronutrients or vitamins (FURUTANI et al., 1953; SIMON & SZILÁGYI, 2003; CHAMPAGNE et al., 2010). Vitamin supplementation according to Wickerham was chosen due to its beneficial effect on microbial growth. Constituents of 100 cm³ vitamin stock solution: 0.2 mg folic acid,
0.2 mg biotin, 40 mg Ca-pantothenate, 200 mg inositol, 40 mg nicotinic acid, 20 mg \( p \)-amino-benzoic acid, 40 mg pyridoxine-HCl, 40 mg thiamine-HCl, and 20 mg riboflavin (Furutani et al., 1953). Our study extends solely to the effect of vitamin supplementation on the yield of the final product.

### Table 3. The optimized (control) fermentation parameters

| A | B | C | D |
|---|---|---|---|
| Temperature (ºC) | 30 | 30 | 30 | 30 |
| Agitation (r.p.m.) | 200 | 400 | 300 | 300 |
| Airflow rate (v.v.m.) | 1.5 | 1.5 | 1.5 | 1.5 |
| pH               | 5.5 | 5.5 | 4.5 | 4.5 |

*: Saccharomyces cerevisiae NCAIM Y.00200 in molasses (A) and corn steep liquor (B) media, and Kluyveromyces marxianus DSM 4908 in molasses (C) and corn steep liquor (D) media

After reaching the set parameters, the inoculum was injected into the raw material solution. The process was carried out for 72 hours, and several samples were taken at the 0th, 24th, 48th, and 72nd h. The experiment was repeated with the supplementation of 1 cm³ dm⁻³ vitamin fermentation medium according to Wickerham of the raw material. Total sugar content of fermentation medium and yeast-derived protein content were determined. In every case there were three parallel measurements done. Protein yield was calculated from the yeast growing relations. For determining the protein content, 5 g purged, washed, and dried at 105 ºC samples were used. All sugar contents were determined also from dried samples by Luff-Schoorl method (Pomeranz & Meloan, 2000), after inverting the complex sugars. The nitrogen content was determined by Kjeldahl method (Pomeranz & Meloan, 2000). The yeast-derived protein content was counted by subtracting nitrogen content of filtered fermentation broth from the nitrogen content of yeast.

### 2. Results and discussion

#### 2.1. Total sugar content of the fermentation medium and protein content of yeast measured for optimized (control) and vitamin supplemented fermentation processes

Total sugar content of the fermentation medium and protein content of yeast were measured from the samples taken at the 0th, 24th, 48th, and 72nd h during optimized (control) and vitamin supplemented fermentation processes. These results are summarised in Tables 4 and 5.

Results given in Table 4 show that A and C trial settings had 53.4±0.4 g/100 g initial total sugar content at the 0th hour, while B and D trial settings had 24.3±0.5 g/100 g initial values at the same time. These results changed to 0.2±0.1–1.9±0.4 by the 72nd hour. Protein contents of yeast, given in Table 5, were 4.5±0.4 g/100 g at the 0th hour, while they were 20.5±0.5 – 30.5±0.3 g/100 g at the 72nd h. We want to highlight that there was a significant (P<0.05) difference between the optimized (control) and vitamin supplemented trials of A and C trial settings at the 72nd h.
Table 4. Comparing total sugar content of fermentation medium employed during optimized (control) and vitamin supplemented fermentation processes (g/100 g)

| Time (h) | A                      | B                      | C                      | D                      |
|---------|------------------------|------------------------|------------------------|------------------------|
|         | Optimized (control)    | Optimized with vitamin supplementation | Optimized (control)    | Optimized with vitamin supplementation |
| 0       | 53.4±0.2a              | 53.4±0.2a              | 24.3±0.5a              | 24.3±0.5a              |
| 24      | 33.5±0.3a              | 32.6±0.2b              | 10.6±0.3a              | 10.5±0.1a              |
| 48      | 10.5±0.3a              | 8.5±0.1b               | 5.6±0.3a               | 5.9±0.5a               |
| 72      | 0.6±0.2b               | 1.9±0.4a               | 0.6±0.3a               | 1.9±0.4a               |

Values are means±SD, based on three observations

\[a,b\]: Subcolumn means within row and experimental setting without a common lowercase superscript differ (P<0.05)

*: *Saccharomyces cerevisiae* NCAIM Y.00200 in molasses (A) and corn steep liquor (B) media, and *Kluyveromyces marxianus* DSM 4908 in molasses (C) and corn steep liquor (D) media

Table 5. Comparing protein content of yeast employed during optimized (control) and vitamin supplemented fermentation processes (g/100 g)

| Time (h) | A                      | B                      | C                      | D                      |
|---------|------------------------|------------------------|------------------------|------------------------|
|         | Optimized (control)    | Optimized with vitamin supplementation | Optimized (control)    | Optimized with vitamin supplementation |
| 0       | 4.5±0.4a               | 4.5±0.4a               | 4.5±0.4a               | 4.5±0.4a               |
| 24      | 8.6±0.2a               | 8.9±0.6a               | 9.2±0.3a               | 9.1±0.5a               |
| 48      | 16.5±0.2a              | 17.0±0.2a              | 16.0±0.2a              | 17.5±0.8a              |
| 72      | 30.3±0.3a              | 28.0±0.5b              | 20.5±0.2a              | 20.2±0.5b              |

Values are means±SD, based on three observations

\[a,b\]: Subcolumn means within row and experimental setting without a common lowercase superscript differ (P<0.05)

*: *Saccharomyces cerevisiae* NCAIM Y.00200 in molasses (A) and corn steep liquor (B) media, and *Kluyveromyces marxianus* DSM 4908 in molasses (C) and corn steep liquor (D) media
2.2. Protein yield (Yx/s) determinations of optimized (control) and vitamin supplemented fermentation processes

Protein yield \([Y_{x/s} \text{ (g g}^{-1})]\) values can be calculated from the functional relationship of the change of the sugar content of the fermentation medium and the cell mass protein measured during fermentation trials.

Based on the protein yield values given in Table 6, vitamin supplementation did not influence the final product yield of the trial settings significantly. Trigueros and co-workers (2016) did fermentation of \(S. \text{cerevisiae} \text{ var. boulardii}\) on cheese whey, where their biomass yield \((Y_{x/s}=0.5 \text{ g g}^{-1})\) was almost equal with our calculated values, whereas there was no significant difference compared to the control. Ásványi (2005) also studied biomass yields during his experiments with \(K. \text{ lactis}\) and \(K. \text{ marxianus}\) yeast species, where the values varied between \(Y_{x/s}=0.2 \text{ g g}^{-1}\) and \(Y_{x/s}=0.6 \text{ g g}^{-1}\), respectively.

### Table 6.

| Trial* | Optimized (control)* | Vitamin supplementation* |
|--------|----------------------|--------------------------|
| A      | 0.5                  | 0.4                      |
| B      | 0.7                  | 0.6                      |
| C      | 0.5                  | 0.5                      |
| D      | 0.6                  | 0.7                      |

*: \(S. \text{cerevisiae NCAIM Y.00200}\) in molasses (A) and corn steep liquor (B) media, and \(K. \text{marxianus DSM 4908}\) in molasses (C) and corn steep liquor (D) media. *: There was no significant difference in protein yields at \(P<0.05\).

3. Conclusions

Results given in Table 4 clearly show that during optimized (control) and vitamin supplemented fermentation processes the total sugar content of the fermentation medium significantly decreased and was practically consumed by the 72\(^{nd}\) hour. Accordingly, we can conclude the sugar conversion of yeast. Yeast protein content values, given in Table 5, increased by the 72\(^{nd}\) h of the fermentation in each trial setting, which also proves the utilization of yeast fermentation medium.

According to the obtained protein yield values (0.4–0.7 g g\(^{-1}\)), which are in accordance with several scientific publications, we came to the conclusion that vitamin supplementation do not have a significant influence on final product yield.

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