Effect of near-wall treatments on airflow simulations

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Abstract—Airflow simulation results depend on a good prediction of near wall turbulence. In this paper a comparative study between different near wall treatments is presented. It is applied to two test cases: (1) the first concerns the fully developed plane channel flow (i.e. the flow between two infinitely large plates). Simulation results are compared to direct numerical simulation (DNS) data of Moser et al. (1999) for \( Re \tau = 590 \) (where \( Re \tau \) denotes the friction Reynolds number defined by friction velocity \( u_\tau \), kinematics viscosity \( \nu \) and the channel half-width \( \delta \)); (2) the second case is a benchmark test for room air distribution (Nielsen, 1990). Simulation results are compared to experimental data obtained with laser-doppler anemometry.

Simulations were performed with the aid of the commercial CFD code Fluent (2005). Near wall treatments available in Fluent were tested: Standard Wall Functions, Non Equilibrium Wall Function and Enhanced Wall Treatment. In each case, suitable meshes with adequate position for the first near-wall node are needed.

Results of near-wall mean streamwise velocity \( U^+ \) and turbulent kinetic energy \( k^+ \) profiles are presented, variables with the superscript of + are those non dimensional by the wall friction velocity \( u_\tau \) and the kinematic viscosity \( \nu \).

Keywords-component; near wall treatment; airflow; simulation;

I. INTRODUCTION

Indoor air quality (IAQ) depends greatly on accurate tools for prediction of airflow and dispersion of particles indoors. These particles have potential harmful effects since they may be inhaled by the occupants.

In some work environments, understanding of dispersion and deposition can improve workers safety. In order to provide exposure assessment, numerical simulations are required to allow a better understanding of particles deposition and dispersion indoors.

Reynolds-averaged Navier–Stokes (RANS) turbulent models (such as \( k-\varepsilon \) models) are still widely used for engineering applications because of their relatively simplicity and robustness. However, these models depend on adequate near-wall treatments.

Airflow simulations depend on a good prediction of near wall turbulence. In our study, different near wall treatments will be assessed and applied to two test cases. The first concerns a fully developed plane channel flow (i.e. the flow between two infinitely large plates), simulations results are compared to direct numerical simulation (DNS) data of Moser et al. (1999) \([1]\) for \( Re \tau = 590 \) (where \( Re \tau \) denotes the friction Reynolds number defined by friction velocity \( u_\tau \), kinematic viscosity \( \nu \) and the channel half-width \( \delta \)). The second case is a benchmark test for 2D room air distribution (Nielsen, 1990) \([2]\). The simulation results are compared with experimental data obtained with laser-Doppler anemometry.

All different near wall treatments available in Fluent will be tested: Standard Wall Functions, Non Equilibrium Wall Function and Enhanced Wall Treatment. We will investigate both effect of meshes and position of the first near-wall node.

Simulations will be performed with the aid of the commercial CFD code Fluent (2005) \([3]\). The \( k-\varepsilon \) turbulence model, which presents the advantage that it doesn’t need excessive computational times, will be used.

II. MODEL EQUATIONS

A. Governing Equations

Airflow is modeled using the \( k-\varepsilon \) model. The general form of the governing equations is:

\[
\frac{\partial (\rho \phi)}{\partial t} + \text{div} (\rho \mathbf{U} \phi) = \text{div} (\Gamma_{\phi} \nabla \phi) + S_{\phi} \quad (1)
\]
Table 1 lists the diffusion coefficients and source terms for the different scalar qualities.

| Term         | Variable | \( c' \) | \( f_2 \) |
|--------------|----------|-----------|-----------|
| Continuity   |          | 0         | 0         |
| x velocity   | \( \beta_x = 2 + \lambda \) | \( \frac{3}{2} \) | \( \frac{1}{2} \) |
| y velocity   | \( \beta_y = 2 + \lambda \) | \( \frac{3}{2} \) | \( \frac{1}{2} \) |
| z velocity   | \( \beta_z = 2 + \lambda \) | \( \frac{3}{2} \) | \( \frac{1}{2} \) |
| Kinetic energy | \( c'_{\bar{k}} \) | \( c'_{\bar{k}} \) | \( c'_{\bar{k}} \) |
| Disruption use | \( c'_{\bar{k}} \) | \( c'_{\bar{k}} \) | \( c'_{\bar{k}} \) |
| Temperature  | \( \bar{c} \) | \( \bar{c} \) | \( \bar{c} \) |
| Concentration| \( \bar{c} \) | \( \bar{c} \) | \( \bar{c} \) |

### III. TEST CASES

Airflow simulations with different near-wall treatments are applied to two test cases:

A. Channel flow

The first test case is the fully developed plane channel flow (i.e. the flow between two infinitely large plates, figure 1). Simulations results are validated by direct numerical simulation (DNS) data of Moser et al. (1999) [1] for \( Re = 590 \).

![Figure 1. Presentation of the channel flow](image)

B. Room air distribution

The second test case is a benchmark test for a room air distribution (Nielsen, 1990 [2], figure 2). The simulation results are validated by experimental data obtained with laser-doppler anemometry.

![Figure 2. Presentation of Nielsen room, H=3m and L=9m.](image)

### IV. RESULTS AND DISCUSSIONS

All different near wall treatments available in Fluent were tested: Standard wall functions “SWF”, Non equilibrium wall function “NEWF” and Enhanced wall treatment “EWT”.

Results of mean streamwise velocity \( u^* \) and turbulent kinetic energy \( k^+ \) profiles are presented in figures (3) and (6).

For the two test cases, channel flow and room air distribution, a fine mesh (respectively 500×57 and 45×38) was used for enhanced wall treatment “EWT”, while a coarse

\[ k^+ = B(y^+)^2e^{\frac{|y^+|}{\bar{c}}} \]  

(2)

B is a coefficient which depends on \( Re \) (Absi, 2009 [10]).
mesh (respectively 500×19 and 45×12) was used for standard wall function “SWF” and non-equilibrium wall function “NEWF” (figure 4).

For the first test case (fully developed plane channel flow), figure 3 presents simulation results: mean streamwise velocity $u^+$ (fig. 3.a) and turbulent kinetic energy “TKE” $k^+$ (fig. 3.b) profiles, with DNS data of Moser et al. (1999) [1] for $Re = 590$.

On the one hand, standard “SWF” and non equilibrium “NEWF” wall functions need a coarse mesh (fig. 4.a). The first node should be at $y^+>30$. Figure (3) shows that standard “SWF” and Non equilibrium “NEWF” wall functions predict well velocity profiles for $y^+>30$ and “TKE” profiles for $y^+>60$. However, these near wall treatments are not able to provide details about velocity and TKE in the viscous and buffer layers. If these treatments are used, it is possible to provide an accurate description of TKE (figure 5, solid line) by equation (2) (Absi, 2008) and velocity by solving an ordinary differential equation “ODE” (Absi, 2009). These treatments could be therefore associated to this simple and efficient analytical method.

On the other hand, enhanced wall treatment “EWT” needs a finest mesh in the viscous sublayer (fig. 4.b). The first node should be at about $y^+=1$. Figure (3) shows that the velocity profile is more accurate and well predicted even in the viscous and buffer layers. However, TKE is underestimated (fig. 3.b). This has no effect on velocity profile but can provide an underestimated eddy viscosity/diffusivity which could be involved in predicted particles concentrations.

In order to investigate the effect of standard $k$-$\varepsilon$ model on the TKE profile which is underestimated by “EWT” (fig. 3.b), figure (6) presents a comparison with Re-Normalisation
Group “RNG” k-ε model. Figure (6) shows that RNG k-ε model provides a very small improvement for velocity and TKE. Since the difference is negligible, the underestimation of TKE seems therefore not related to the used turbulence model but associated to the near wall treatment.

Predicted mean velocity profiles with the different near-wall treatments are quite similar (fig. 7.a, 7.c). Mean velocities obtained with enhanced wall treatment “EWT” seem better particularly near the walls where wall functions are unable to provide values. However, EWT needs more computation time.

In order to improve TKE, we suggest the use of equation (2) for $y^+ \leq 20$. The value of TKE at $y^+=20$ could be used as a boundary condition for the modeled k-equation for $y^+>20$. Since TKE is well predicted until 20 by Eq. (2), the improvement of TKE for $y^+>20$ is expected.

The second test case (benchmark test for a room air distribution), presents simulation results: mean velocity $u^+$ (fig. 7a and 7.c) and turbulence intensity (figure 7.b and 7.c), with experimental data obtained by laser-Doppler anemometry (Nielsen, 1990) [2].

Figures (7.a) and (7.c) present mean velocity $u^+$ respectively at $x=3m$ (1/3 L) and $x=6m$ (2/3 L) while figures (7.b) and (7.d) present turbulence intensity $u'$ (respectively at $x=3m$ and $x=6m$).
Figure 7. Comparison between predicted profiles using standard k-ε model with different wall treatments and experimental data for test case 2 benchmark test for a room air distribution. (a) mean velocity at $x=3m$, (b) RMS velocity at $x=3m$, (c) mean velocity at $x=6m$, (d) RMS velocity at $x=6m$.

More important scatter is shown for RMS (root mean square) velocities at $x=3m$ (fig. 7.b). Non equilibrium wall function seems to be the less accurate. All near-wall treatments fail to predict RMS velocities for $y/H<0.4$ (fig. 7.b). In contrast, at $x=6m$ wall functions seem more accurate for $y/H>0.6$. However, for $y/H<0.2$ wall functions (SWF and NEWF) didn’t provide values, this is due to the required mesh and first near wall node, while EWT seems not accurate in this region.

V. CONCLUSIONS

Airflow simulations with different near-wall treatments were applied to two test cases.

For the first test case (fully developed plane channel flow), simulation results: mean streamwise velocity and turbulent kinetic energy “TKE” profiles were compared to DNS data for $Re_e = 590$. Standard “SWF” and non equilibrium “NEWF” wall functions need a coarse mesh. The first node should be at $y^+>30$. “SWF” and “NEWF” wall functions predict well velocity profiles for $y^+>30$ and “TKE” profiles for $y^+>60$. But they are not able to provide details about velocity and TKE in the viscous and buffer layers. It is possible to provide an accurate description of TKE by equation (2) (Absi, 2008) and velocity by solving an ordinary differential equation (Absi, 2009). Enhanced wall treatment “EWT” needs a finest mesh in the viscous sublayer. The first node should be at $y^+=1$. Velocity profile is more accurate and well predicted even in the viscous and buffer layers. TKE is underestimated which could provide an underestimated eddy viscosity/diffusivity and therefore could had an effect on predicted particles concentrations. Simulations show no difference between standard and RNG k-ε models. The underestimated TKE seems therefore associated to near wall treatments. In order to improve TKE, we suggest the use of equation (2) (Absi, 2008) for $y^+ \leq 20$.

The value of TKE at $y^+ = 20$ could be used as a boundary condition for the modeled k-equation for $y^+ > 20$.

For the second test case (benchmark test for a room air distribution) simulation results for mean velocity and turbulence intensity (at $x/L=1/3$ and $2/3$) were compared to experimental data. Predicted mean velocity profiles with the different near-wall treatments are quite similar. Mean velocities obtained with enhanced wall treatment “EWT” seem better particularly near the walls. However, “EWT” needs more computation time. More important scatter is shown for RMS velocities at $x/L=1/3$. Non equilibrium wall function seems to be the less accurate. All near-wall treatments fail to predict RMS velocities for $y/H<0.4$. In contrast, at $x/L=2/3$ wall functions seem more accurate for $y/H=0.6$. However, for $y/H<0.2$ no values are obtained by wall functions (SWF and NEWF), this is due to the required mesh and first near wall node, while “EWT” seems not accurate in this region. Improved models with adequate near-wall treatments are needed for an efficient simulation of room air distribution.

REFERENCES

[1] Moser R.D., Kim J., Mansour N.N. (1999) “Direct numerical simulation of turbulent channel flow up to $Re_e = 590$”, Phys. Fluids, Vol. 11, N° 4, 943-500.
[2] Nielsen P.V. (1990) “Specification of a two-dimensional test case”, the University of Aalborg, ISSN 0902-7513 R9040.
[3] FLUENT Inc. (2009). FLUENT 6.2 user’s guide.
[4] Launder B. E. and Spalding D. B. (1974) The Numerical Computation of Turbulent Flows, Computer Methods in Applied Mechanics and Engineering, 3:269-289.
[5] Kim S.E. and Choudhury D. (1995) A Near-Wall Treatment Using Wall Functions Sensitized to Pressure Gradient. In ASME FED Vol. 217, Separated and Complex Flows. ASME.
[6] Wolfstein M. (1969) The Velocity and Temperature Distribution of One-Dimensional Flow with Turbulence Augmentation and Pressure Gradient. Int. J. Heat Mass Transfer, 12:301-318.
[7] Chen H. C. and Patel V. C. (1988) Near-Wall Turbulence Models for Complex Flows Including Separation. AIAA Journal, 26(6):641-648.
[8] Kader B. (1993) Temperature and Concentration Profiles in Fully Turbulent Boundary Layers. Int. J. Heat Mass Transfer, 24(9):1541-1544.
[9] Absi R. (2008) “Analytical solutions for the modeled k-equation”, ASME J. Appl. Mech., 75(4), 044501, 1-4.
[10] Absi R. (2009) “A simple eddy viscosity formulation for turbulent boundary layers near smooth walls”, C. R. Mecanique, Elsevier, 337, 158-165.

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