A comparative study on the stability of the furfural molecule on the low index Ni, Pd and Pt surfaces

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We present a comparative density functional theory investigation of the furfural (Ff) molecule on the low index Ni, Pd and Pt surfaces to understand its geometrical and electronic properties to gain mechanistic insights into the experimentally measured catalytic reactivities of these metal catalysts. We show that the number of metal d-states, which hybridize with the nearest C and O p-orbitals of the Ff molecule, can be used to explain the stability of the Ff molecule on these surfaces. We find that the hybridization between atoms with higher electronegativity and the metal d-states plays a crucial role in determining the stability of these systems. Furthermore, we also find electron transfer from metal to the Ff molecule on the Ni and Pd surfaces, with a reverse process occurring on the Pt surface.

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1. Introduction

Harvesting useful products from biomass and renewable feedstocks is a crucial component of the transition from a petroleum-based to a sustainable chemical industry [1–3]. In this regard, furfural (Ff) is an important precursor in the production of biofuels and many chemical intermediates [4,5]. Produced from the xylan contained in lignocellulose via hydrolysis and dehydration [6,7], hydrogenation of Ff gives intermediate chemicals with wide applications [8,9]. One such example is furfuryl alcohol (FA), which is produced from selective hydrogenation of Ff, and has a broad spectrum of applications, including the manufacture of resins, adhesives, fibres [10] and fuel derivatives, such as 1,5-pentanediols [11]. Moreover, it can undergo further hydrogenation to give tetrahydro-FA (THFA), an environmentally friendly solvent used in the automotive and agricultural industries [12,13]. Other intermediates produced from the hydrogenation of Ff include 5-hydroxymethylfurfural, 2-methyl furan and 2-methyltetrahydrofuran (see scheme 1) [1–3,14]. These intermediates are parent molecules for various useful chemicals such as caprolactone, 2,5-dimethylfuran, 2,5-furandicarboxylic acid, etc [15–17].

The nature and distribution of these intermediates is dependent on their affinity for different metal catalysts and preferential adsorption onto catalytic sites (e.g. step edges and kinks) [18,19]. A good metal catalyst should be highly active under mild conditions, withstand multiple cycles before deactivation, use economical materials and have a high selectivity for the desired product. The industrial process of gas phase hydrogenation of Ff using Cu on asbestos was first reported in 1929, and later, Du Pont de Nemours patented the use of copper chromite [20,21]. It is further reported that the Quaker Oats Company then used Cu supported on Na2O · SiO2 to achieve yields of 99% of FA, which set the precedent for many other catalytic systems based on Cu and other metals to be used in this process, providing an alternative to the use of chromites [22].

A wide range of catalysts have now been studied for the hydrogenation of Ff, with Cu-, Ni-, Ru-, Pt- and Pd-based systems being popular. Ni catalysts have been found to favour adsorption of Ff over FA, with the turn over frequency (TOF) almost constant for different average sizes of Ni metal particles, whereas in the conversion of FA to THFA, the smaller Ni particles gave higher TOF values [18]. Pushkarev et al. [23] reported the influence of the size of Pt nanoparticle catalysts on the production of furan and FA, where an increase of Pt nanoparticle size to 7 nm increases selectivity towards hydrogenation of Ff into FA from 1% to 66%. By contrast, the decrease of nanoparticle size was found to favour decarbonylation of Ff to furan, with 1.5 nm producing the highest selectivity (96%). Hydrogenation with SiO2-supported Pd-Ir bimetallic catalysts has been found to give increased TOF values with further addition of Ir as compared with Pd/SiO2, probably owing to the promoting effect of Ir on the adsorption at the carbonyl (C=O) site, whereas the Pd surface was found to strongly interact with the furan ring [24]. At high temperatures, a flat orientation through the furan ring and carbonyl functionality gives decarbonylation of Ff to produce furan and tetrahydrofuran [25].

Selectivity can be controlled by blocking specific sites on the catalyst surface to guide distribution, for example by using thiolates or polymers [26,27]. The use of thiolate self-assembled monolayers was found to strongly suppress Ff decarbonylation with increasing sulfur density [27]. Pang et al. [27] demonstrated the use of thiolates as blocking agents, leaving particle edges/corners exposed. Rogers et al. [26] demonstrated the use of poly(vinyl alcohol) (PVA) to direct selectivity. The nature of the PVA–Pd interactions and the relative proportion of available surface sites direct the reaction towards the hydrogenation of Ff. Jeong et al. [28] reported the use of Ni nanoparticle catalysts capped with organic molecules, wherein steric hinderance of the Ni surface induced by the organic layer gave selective hydrogenation of Ff to FA, with a yield of 95%. Wang et al. [29] recorded the use of zeolite crystals to control selectivity in the hydrogenation of Ff. The catalyst used combined the high activity of Pd nanoparticles with the selectivity of zeolite micropores to give a furan selectivity as high as 98.7%. Xue et al. [30] found that the optimal adsorption configuration of Ff to be the top-Ni-top-Ni site on a Ni/Pd(111) catalyst.

Periodic density functional theory (DFT) calculations have been used to explore further the optimal mechanism of Ff conversion. Ren et al. [31] reported the hydrodeoxygenation and decarbonylation mechanisms of Ff to proceed on the Ni(111) surface via adsorption of both the carbonyl group and the furanic ring. Despite numerous studies on the interaction of the Ff molecule on transition metal catalysts, there are considerable uncertainties on the chemical bonding and charge transfer behaviour between Ff and metal catalysts, which can be crucial in designing novel catalysts. Further to this, in one of our recent studies, we have shown the dual site hydrogenation mechanism in which the hydrogen dissociation takes place on the metal nanoparticles, and after spillover of the adsorbed hydrogen on the support material, hydrogenation of the Ff molecule takes place to yield THFA [32].
Therefore, it is important to clarify how the Ff molecule interacts with the pristine metal surfaces to optimize the catalyst. In this study, we report experimental catalytic studies, which motivated the DFT based theoretical studies with dispersion corrections to investigate the geometries, energetics and the electronic properties of the Ff molecule adsorbed on the low index Ni, Pd and Pt catalyst surfaces.

2. Methodologies

2.1. Experimental

2.1.1. Catalyst preparation

Pd catalyst: solid Na2PdCl4 (0.051 mmol) (Sigma-Aldrich, purity greater than 99.9%) and 1 ml of a PVA solution (1 wt%) were added to 100 ml of H2O (Pd/PVA 1/0.5 wt/wt %). After 3 min, a 0.1 M of NaBH4 solution (Pd/NaBH4 1/8 mol mol\(^{-1}\)) was added to the solution under vigorous magnetic stirring. Within a few minutes of their generation, the colloids (acidified at pH 2, by sulfuric acid) were immobilized by adding the support (TiO\(_2\), Degussa P25) to the vigorously stirring solution. The amount of the support was controlled, in order to obtain a final Pd loading of 1 wt% (on the basis of quantitative loading of the metal on the support). The catalysts were filtered and washed several times and dried at 100°C for 2 h.

Pt catalyst: solid K2PtCl4 (0.051 mmol) (Sigma-Aldrich, purity greater than 99.9%) and 1 ml of a PVA solution (1 wt%) were added to 100 ml of H2O (Pt/PVA 1/0.5 wt/wt %). After 3 min, a 0.1 M of NaBH4 solution (Pd/NaBH4 1/8 mol mol\(^{-1}\)) was added to the solution under vigorous magnetic stirring. Within a few minutes of their generation, the colloids (acidified at pH 2, by sulfuric acid) were immobilized by adding the support (TiO\(_2\), Degussa P25) to the vigorously stirring solution. The amount of the support was controlled in order to obtain a final Pt loading of 1 wt% (on the basis of quantitative loading of the metal on the support). The catalysts were filtered and washed several times and dried at 100°C for 2 h.

Ni catalyst: Ni(NO3)\(_2\)·6H\(_2\)O (5 × 10\(^{-4}\)M) and urea (urea/Ni 10:1 mol mol\(^{-1}\)) were dissolved in 200 ml of water under magnetic stirring in the presence of TiO\(_2\) (Degussa P25). The amount of the support was controlled in order to obtain a final Ni loading of 1 wt% (on the basis of quantitative loading of the metal
on the support). The solution was kept under stirring for 6 h at 80°C. The solid was separated from the solution by filtration and washed several times. The powder was dried at 60°C for 12 h and then calcined at 300°C for 3 h. Successively the catalyst was reduced under H₂ at 300°C for 3 h.

2.1.2. Catalytic activity

As noted, Ni-, Pd- and Pt-based catalysts were prepared using TiO₂ (P25, 50 m² g⁻¹) as support with a loading of 1 wt%. The metal loading was confirmed by atomic absorption spectroscopy. Pd/TiO₂ and Pt/TiO₂ were prepared employing an established sol-immobilization method using PVA as protective agent and NaBH₄ as reducer. Ni/TiO₂ was prepared using a method involving the precipitation of Ni(OH)₂ in aqueous solution, with subsequent calcination at 300°C followed by a reduction step at 300°C. Transmission electron microscopy analysis showed that Pd/TiO₂, Pt/TiO₂ and Ni/TiO₂ catalysts have particle sizes of 2.7, 3.6 and 5.3 nm, respectively [32,33].

Ff (purity 99%, Sigma-Aldrich) hydrogenation was performed at 323 K, using a stainless-steel reactor (30 ml capacity), equipped with heater, mechanical stirrer, gas supply system and thermometer. Ff solution (15 ml; 0.3 M in 2-propanol) was added into the reactor, and the desired amount of catalyst (F/metal ratio = 500 wt/wt) was suspended in the solution. The pressure of the hydrogen was 5 bar.

The mixture was heated to the reaction temperature, 423 K, and mechanically stirred (1250 rpm). At the end of the reaction, the autoclave was cooled down. Samples were removed periodically (0.2 ml) for a HP 7820A gas chromatograph equipped with a capillary column HP-5 30 m × 0.32 mm, 0.25 µm Film, by Agilent Technologies. Identification of products was performed using a Thermo Scientific Trace ISQ QD Single Quadrupole GC-MS equipped with a capillary column HP-5 30 m × 0.32 mm, 0.25 µm Film, by Agilent Technologies. Authentic samples were also analysed to determine separation times. Quantitative analyses with external standard method (n-octanol) were used.

2.2. Computational details

The Vienna Ab-initio Simulation package (VASP) is used to perform all the DFT-based calculations [34,35]. We used the projector augmented wave method, with the plane wave cut off of 550 eV for the expansion of the wave functions, which provided bulk total energies converged to within 10⁻⁵ eV [36]. For the structural optimizations, we chose a convergence criterion of 0.01 eV Å⁻¹. For the exchange correlation functional, we used the Perdew-Burke-Ernzerhof (PBE) generalized gradient approximation [37]. A 3 × 3 × 1 Monkhurst-Pack grid was used. The ideal M(h,k,l) surfaces (M = Ni, Pd, Pt and h,k,l are 0 or 1) were modelled by seven atomic layers slab with a (4 × 4) periodicity. The slabs were constructed using the optimized lattice constants of 3.50 Å (Exp.: 3.50 Å), 3.86 Å (Exp.: 3.89 Å) and 3.93 Å (Exp.: 3.91 Å) for Ni, Pd and Pt, respectively [38]. During the optimization, the top three atomic layers were relaxed, and the bottom four layers were fixed to their respective bulk positions. Along the surface normal direction, a vacuum of approximately 15 Å was inserted, which is sufficient to eliminate spurious interactions with the neighbouring image slabs. The Ff molecule was adsorbed on one side of the slab. The dipole moment due to the adsorbed species was accounted for by using the methods of Neugebauer et al. [39,40]. In this study, we also employed Grimme’s dispersion correction (DFT + D3), as dispersion forces might be significant for adsorption of organic molecules [41].

For the calculations of adsorption energies (Eₐd) of Ff on the M(h,k,l) surface, we used the following equation

\[ E_{\text{ad}} = E_{\text{FF/M}} - E_{\text{M}} - E_{\text{FL}} \]  \hspace{1cm} (2.1)

where \( E_{\text{FF/M}} \) is the total energy of the Ff adsorbed on the metal surface, \( E_{\text{M}} \) is the total energy of the relaxed pristine surface and \( E_{\text{FL}} \) is the total energy of the Ff molecule in the gas phase. To obtain \( E_{\text{FL}} \), the adsorption of Ff was allowed on various sites on the M(h,k,l) surface i.e. the on-top site, in between the on-top sites and on the hollow site with respect to the O-atom of the furan ring of the Ff molecule. On the M(110) surface, the Ff molecule was allowed to adsorb along the ridges and perpendicular to ridges. The atomic charges were calculated using the Bader charge analysis as implemented by Henkelman and coworkers [42]. The VESTA package was used for visualization of the optimized structures and to measure the interatomic distances, bond angles and dihedral angles [43,44].

In addition to the periodic DFT calculations, we also use ORCA on the Ff molecule to obtain the characteristics of the highest occupied molecular orbital (HOMO) and the lowest unoccupied molecular orbital (LUMO) [45]. All the calculations were performed using the PBE functional with Grimme’s D3 dispersion correction and def-2-TZVP basis set. Further to this, partial density of states (PDOS) onto the
molecular orbitals and density of states weighted by the crystal orbital overlap population (COOP) were calculated using the STATE package [46–50]. In the implementation of COOP in the STATE package, the wave functions of the adsorption system are expanded in terms of the molecular orbital of the Ff molecule and the substrate wave functions. This approach is appropriate and effective for characterizing the bonding mechanism of the molecule, especially when the molecular orbitals are localized. These calculations were performed using the geometry optimized using the VASP code, and no further optimizations were performed. A $\Gamma$-centred $4 \times 4$ k-point set was used.

3. Results and discussion

In this section, we will present our results on the catalytic activity of Ni, Pd and Pt, the trends of the calculated adsorption energies of the Ff molecule on the M($h,k,l$) surfaces ($M = \text{Ni, Pd and Pt}$), followed by discussions on the geometrical and local electronic properties of these systems.

Table 1. Furfural hydrogenation in 2 propanol.

| catalyst | activity $^b$ | selectivity (%) | furfuryl alcohol | tetrahydrofurfuryl alcohol | 2-methyl furan | tetrahydro methyl furan | isopropyl furfuryl ether | isopropyl tetrahydro furfuryl ether |
|----------|--------------|-----------------|------------------|--------------------------|---------------|------------------------|--------------------------|----------------------------------|
| Ni/TiO$_2$ | 261 | 14 | 81 | 1 | — | — | 3 |
| Pd/TiO$_2$ | 981 | 69 | 24 | — | 4 | 1 | 4 |
| Pt/TiO$_2$ | 1018 | 85 | 8 | — | — | 6 | — |

$^a$Reaction conditions: furfural = 0.3 M; F/metal ratio = 500 wt/wt, 323 K, 5 bar H$_2$.

$^b$Mol of furfural converted per hour per surface atoms of metal, calculated after 15 min of reaction.

Table 2. The adsorption energy of furfural on the low index Ni, Pd and Pt surfaces.

| configuration | adsorption energy (eV) | Ni | Pd | Pt |
|---------------|------------------------|----|----|----|
| M(111)        |                        |    |    |    |
| 1             | $-1.83$                |    |    |    |
| 2             | $-1.68$                |    |    |    |
| 3             | $-1.69$                |    |    |    |
| 4             | $-1.70$                |    |    |    |
| M(110)        |                        |    |    |    |
| 1             | $-2.72$                |    |    |    |
| 2             | $-2.57$                |    |    |    |
| 3             | $-2.72$                |    |    |    |
| 4             | $-2.34$                |    |    |    |
| 5             | $-2.53$                |    |    |    |
| 6             | $-2.53$                |    |    |    |
| M(100)        |                        |    |    |    |
| 1             | $-2.67$                |    |    |    |
| 2             | $-2.19$                |    |    |    |
| 3             | $-2.67$                |    |    |    |
| 4             | $-2.67$                |    |    |    |
Table 3. The interatomic distances and dihedral angles of the most stable \( Ff/M(h,k,l) \) systems under investigation. (Please refer to table 2 for the most stable configurations.)

| system   | interatomic distance (Å) | dihedral angles (°) |
|----------|--------------------------|---------------------|
|          | \( C-C_{\text{sing}} \) | \( C-O_{\text{sing}} \) | \( C-C_{\text{CHO}} \) | \( C=O \) | \( FF-M \) | \( M-M \) | \( CCCC_{\text{sing}} \) | \( COC_{\text{sing}} \) | \( HCCH_{\text{sing}} \) | \( OCCH_{\text{sing}} \) | \( OCCO \) | \( OCCH_{\text{CHO}} \) |
| furfural | 1.392                    | 1.369               | 1.452               | 1.227   | —        | —       | 0.019               | 0.009               | 0.035              | 180.000            | 0.060               | 180.000            |
| Ni(111)  | 1.450                    | 1.408               | 1.438               | 1.311   | 2.086    | 2.540   | 0.984               | 14.048              | 7.213              | 143.873            | 5.714               | 157.049            |
| Pd(111)  | 1.447                    | 1.405               | 1.454               | 1.270   | 2.228    | 2.772   | 1.147               | 19.231              | 10.149             | 149.353            | 13.201              | 13.201             |
| Pt(111)  | 1.472                    | 1.414               | 1.500               | 1.219   | 2.164    | 2.840   | 1.068               | 28.045              | 6.250              | 138.486            | 11.329              | 169.245            |
| Ni(110)  | 1.444                    | 1.438               | 1.440               | 1.319   | 2.061    | 2.489   | 1.172               | 8.969               | 42.805             | 155.421            | 5.081               | 159.533            |
| Pd(110)  | 1.434                    | 1.390               | 1.432               | 1.268   | 2.220    | 2.769   | 1.189               | 6.086               | 6.578              | 158.912            | 10.959              | 10.959             |
| Pt(110)  | 1.454                    | 1.392               | 1.437               | 1.268   | 2.191    | 2.788   | 0.634               | 8.059               | 6.155              | 149.724            | 18.736              | 161.041            |
| Ni(100)  | 1.446                    | 1.438               | 1.441               | 1.350   | 2.090    | 2.527   | 1.861               | 9.215               | 13.118             | 152.358            | 10.640              | 144.483            |
| Pd(100)  | 1.449                    | 1.422               | 1.458               | 1.274   | 2.206    | 2.804   | 0.634               | 7.193               | 15.297             | 149.782            | 9.647               | 160.868            |
| Pt(100)  | 1.452                    | 1.395               | 1.486               | 1.220   | 2.179    | 2.875   | 1.426               | 8.878               | 1.350              | 144.873            | 10.077              | 169.951            |
3.1. Catalytic activity

The catalysts were evaluated for the hydrogenation of Ff under mild conditions (table 1); Ff 0.3 M, Ff/metal ratio 500 mol mol$^{-1}$, 5 bar H$_2$, 50°C and 2-propanol as solvent. To separate the effect of the nature of the metal and particle size effect, the activity was calculated based on the superficial atoms using a procedure reported previously (table 1) [33].

The catalytic activity demonstrated that the 1 wt% Pt/TiO$_2$ catalyst (1018 h$^{-1}$) and Pd/TiO$_2$ (981 h$^{-1}$) exhibited superior activity as compared to the Ni/TiO$_2$ (261 h$^{-1}$) catalyst. Notably, not only was there a difference in activity, but there was also a pronounced change in the selectivity profile. The Ni/TiO$_2$ catalyst had a preferential selectivity towards THFA (81%), whereas Pd/TiO$_2$ and Pt/TiO$_2$ favoured FA (69% and 85%, respectively). This observation is consistent with studies that have already proved that Ni is able to hydrogenate both the carbonyl group and furanic ring [32]. To understand the reasons behind the observed catalytic activities of the Pt/TiO$_2$, Pd/TiO$_2$ and Ni/TiO$_2$ catalyst, studies on the adsorption of the Ff molecule on these catalysts followed by the mechanism of Ff hydrogenation are required. As a first step towards addressing the detailed reaction mechanism, we focus on theoretical understanding of the nature of the interaction between the Ff molecule and the low index Ni, Pd and Pt surfaces in the following sections.

3.2. Adsorption energies

The calculated adsorption energies of the Ff molecule on the low index Ni, Pd and Pt surfaces are summarized in table 2. For uniformity, similar initial configurations of the Ff molecule on all these surfaces were generated, and the adsorption energies are calculated on the fully relaxed Ff/M(h,k,l) systems. Previously, we have shown that the parallel configuration of Ff on the catalyst surface is more stable as compared to the perpendicular configuration [26]. Therefore, only the parallel configurations at different positions on the M(h,k,l) surfaces are considered in this study. For clarity, all the optimized structures of various configurations used for this study are presented in figures 1–3 and the coordinates are provided in the electronic supplementary materials.

On the M(111) surface, the adsorption energy of Ff is greatest (most negative) on the Pt(111) surface, followed by the Ni(111) and the Pd(111) surface (table 2). We also see that the difference between the highest and lowest adsorption energies is only 0.08 eV on the Pd(111) surface, while it is 0.15 and 0.20 eV for the Ni(111) and the Pt(111) surfaces, respectively, that is, the adsorption energies on different adsorption sites are comparable for Pd (111), while the differences of the adsorption energies on different sites are more significant for Ni(111) and the Pt(111). On the fully relaxed (110) surfaces, the adsorption energy of the Ff molecule follows a similar trend to the (111) surfaces, i.e. adsorption is
most exothermic on the Pt(110) surface, followed by Ni(110) and Pd(110). It is interesting to note that unlike the (111) surfaces, adsorption energies for Pt(110) and Ni(110) are comparable. For the (100) surfaces, however, the Ff molecule is adsorbed most strongly on the Ni surface, which is followed by Pt and Pd. To clearly understand the probable reasons for the differences in the adsorption energies, we explore the geometrical and the local electronic properties of the Ff/M(h,k,l) systems.

### 3.3. Geometrical properties

In this subsection, we present a comparison of the geometries of the adsorbed Ff molecule with respect to the gas phase Ff molecule. For clarity, we will only consider the most stable structures of the Ff/M(h,k,l) systems. In table 3, the interatomic distances and the dihedral angles of the fully relaxed Ff molecules are summarized.

Upon adsorption, the Ff molecule is distorted: the interatomic distances increase and the planarity (measured by the dihedral angles) of the molecules change significantly. However, there is no clear correlation between the overall molecular distortion and the calculated adsorption energies. For example, on the Ni(111) and Pd(111), both carbon atoms of the furan ring and the O-atom of the -CHO group directly interact with the surfaces (see figure 1). However, on the Pt(111) surface, the Ff molecule interacts via the C-atoms of the furan ring only, which consistent with previous studies [31,51]. Similarly, on the M(110) and M(100), the Ff molecule adsorbs via both the C-atoms of the furan ring and the O-atom of the -CHO group (see figure 2). On the (100) surfaces, the adsorption of Ff follows the same trend as on the M(111) surfaces (see figure 3). The distances between the Ff molecule and the surface are also comparable for all the systems. Based on these analyses, we conclude that the geometry of the Ff molecule may

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**Figure 1.** The fully optimized structures of the four configurations of the Ff molecule on the (a) Ni(111), (b) Pd(111) and (c) Pt(111) surfaces. For clarity, the exposed surface including the adsorbed molecule is shown in ball and stick form, and the rest of the model is represented in the CPK form.
change significantly, and the mode of adsorption also varies with the metal catalysts. For example, on the most stable Ff/Ni(111) system, all the C-atoms of the furan ring and the atoms of the -CHO group are close to the Ni(111) surface (unlike the most stable Ff/Pd(111) and Ff/Pt(111) systems), which may indicate the reason for preferential selectivity of Ni towards THFA as reported in the experimental section above. However, to understand the underlying reasons for different stability of the Ff molecule on these metal surfaces, a more detailed investigation on the electronic properties is required.

3.4. Bader charges

The calculated Bader charges are summarized in table 4. To understand fully the charge distribution on the adsorbed Ff molecule, we begin with that in the gas phase. As shown in table 4, we not only consider the total charge on the Ff molecule but also those on the furan ring, furan ring skeleton (without the H-atoms) and the -CHO group, which is considered, as in most of the adsorbed configurations, the C-atoms of the furan ring are close to the surface. From the charge analysis in the gas phase, we find that the Ff molecule has both positive and negative regions i.e. the furan ring is slightly positive and the -CHO group is slightly negative. Based on the charge redistribution in these regions, we aim to understand the charge transfer phenomenon between the Ff molecule and the M(h,k,l) surface.

3.4.1. Furfural on Ni surfaces

The investigation of the charges on the adsorbed Ff molecule on the Ni surfaces show that the overall charge on the Ff molecule is in the range of $-0.06$ to $-0.07$ e. Similarly, the charge on the furan ring and furan ring skeleton is also negative. Furthermore, when we analyse the charges of the surface atom interacting directly with the Ff molecule, we find that it is slightly positive. Clearly, there is charge transfer from the Ni surfaces to the Ff molecule (table 4). We note that in the Ff/Ni(100) system, even though the overall charge on the Ff ring is comparable to the other two systems, the charge on the furan ring, and the furan ring skeleton is more negative and the -CHO group is positive, which is presumably related to the need to facilitate a stronger interaction between the Ff molecule and the Ni(100) surface intra-molecular by a charge redistribution in the Ff molecule. From
the charge analysis, it is clear that slightly positively charged Ni surfaces, and the slightly negatively
charged Ff molecule leads to favourable adsorption energies.

3.4.2. Furfural on Pd and Pt surfaces

In the Ff/Pd(\(h,k,l\)) systems, the directly interacting Pd atoms are positively charged, and the Ff molecule
is negatively charged (table 4). Therefore, there is charge transfer from the Pd surface to the Ff molecule
and the Pd(\(h,k,l\)).

On the Pt(\(h,k,l\)) surfaces, we find an interesting distribution of the charges on the Pt surfaces i.e. the Pt
atoms bound to the Ff molecule are positively charged, and the average charge on the furan skeleton is
negative, clearly indicating that there is strong interaction between the Ff molecule and the Pt surfaces.
However, the average charge on the Pt surface is slightly negative which indicates net charge transfer
from the Ff molecule to the Pt surface (table 4). The negative charge on the furan ring skeleton and
overall, near neutrality of charge on the Ff molecule upon adsorption on the Pt surface may be owing to
charge compensation from the -CHO group. From the Bader charge analysis, we understand that on the

Figure 3. The fully optimized structures of the four configurations of the Ff molecule on the (a) Ni(100), (b) Pd(100) and (c) Pt(100)
surfaces. For clarity, the exposed surface including the adsorbed molecule is shown in ball and stick form, and the rest of the model
is represented in the CPK form.
Ni and Pd surfaces, there is charge transfer from the metal to the Ff molecule. On the other hand, on the Pt surface, there may be charge transfer from the Ff molecule to the metal surface.

### 3.5. Charge density difference

In this section, we present the planar average charge density difference, which is defined by:

\[
\Delta \rho(z) = \frac{1}{A} \int dx dy \Delta \rho(r),
\]

where \( A \) is the area of the surface unit cell under consideration and \( \Delta \rho(r) \) is the charge density difference defined by:

\[
\Delta \rho(r) = \rho_{\text{Ff/M}}(r) - [\rho_{\text{M}}(r) + \rho_{\text{Ff}}(r)],
\]

where, \( \rho_{\text{Ff/M}}(r) \) is the charge density of the total system, which includes the substrate and the adsorbate, and \( \rho_{\text{M}}(r) \) and \( \rho_{\text{Ff}}(r) \) are the charge densities of the pristine surface and the isolated molecule, respectively. Figure 4 shows the fully relaxed Ff/Ni(111) system, along with the planar average charge density. We can see the electron depletion on the surface and electron gain on the Ff molecule, agreeing well with the Bader charge analysis in §3.4. We performed similar analysis on all the other surfaces, and the results are compiled in figure 5, and for clarity, the exposed metal surface and the average molecular surfaces are denoted by red and green lines, respectively. As expected, our analysis shows electron depletion on all the exposed surfaces of Ni and Pd. The \( \Delta \rho(z) \) for the Pt surfaces also display electron depletion even though the exposed surfaces have traces of negative charge on it (table 4). This can be explained by the fact that the directly interacting Pt atoms just below the Ff molecule in the Ff/Pt(\(h,k,l\)) system are positively charged. In addition, it also shows that there is a strong chemical bonding between the Ff molecule and M(\(h,k,l\)) surfaces, which agrees with the calculated adsorption energies which are in the range of \(-1.50\) to \(-2.89\) eV. While our study on Bader charges and planar average charge density difference provide important information on charge transfer and chemical bonding, they do not clarify the reasons for the trends in the calculated adsorption energy in the Ff/Ni(\(h,k,l\)) systems. Therefore, in the next step, we investigate the PDOS to understand the probable reasons for varying stability of the Ff molecule on the M(\(h,k,l\)) surfaces.

### 3.6. Partial density of states and chemical bonding

In this section, we systematically explore the PDOS to understand the trends of the calculated stabilities of the Ff molecules on the metal surfaces. Before presenting the detailed results, we note that in all the Ff/M(\(h,k,l\)) systems, one of the carbon atoms next to the O-atom (C\(_{\text{Oxygen}}\)) of the furan ring has the shortest interatomic distance from the M(\(h,k,l\)) surface, which is related to the fact that owing to the higher electronegativity of...
Figure 5. The planar average charge density difference showing accumulation and depletion of electrons above and below 0 e/Å respectively for the (a) Ff/Pd(111), (b) Ff/Pt(111), (c) Ff/Ni(110), (d) Ff/Pd(110), (e) Ff/Pt(110), (f) Ff/Ni(100), (g) Ff/Pd(100) and (h) Ff/Pt(100) surfaces. The horizontal blue and green lines represent the exposed metal surface and average molecular surface, respectively.
the O-atom, there is electron depletion on this site favouring bond formation with the metal atoms underneath. In some of the systems, the O-atom of the -CHO group (OCHO) is also close to the metal surface. Therefore, in our PDOS analysis, we consider the PDOS of these atoms with the nearest metal atoms.

3.6.1. Stability of furfural on the M(111) surfaces

First, we consider the interaction of the C-Oxygen atom with the nearest metal atom for the Ni(111), the Pd(111) and the Pt(111) surfaces. As shown in figure 6a–c, we find that upon adsorption of the Ff molecule, the C p-states overlap with the surface metal d-orbitals at the lower energy levels. For clarity, this feature is shown using a dotted rectangular box in figure 6a–c. To understand further this effect, we closely monitored this area (as shown in figure 6d–f). In the Ff/Pt(111) system, the overlapping region between the C p- and Pt d-orbitals is in the region between −9.00 and −5.91 eV. In the case of the Ff/Ni(111) and the Ff/Pd(111) system, the major overlapping region is between −9.62 and −5.31 eV and −9.31 to −5.18 eV respectively. To capture a clear picture of the overlapping region, we calculated the number of states of metal d-orbitals, which hybridize with the C p-orbital [52]. As shown in table 5, the number of states for the corresponding Pt d-states is 0.23, which is larger than those in the Ff/Ni(111) and the Ff/Pd(111) systems, suggesting that the chemical bonding between the Ff molecule and the Pt(111) surface is stronger than those for the other systems, leading to the most negative adsorption energy of the Ff/Pt(111) system and hence higher stability.

We further saw that the number of states for the d-orbitals which hybridize with the C p-orbitals for Ff/Pd(111) systems is larger than the Ff/Ni(111), which, however, does not explain the trend of the calculated adsorption energy. As we mentioned earlier, the Ff molecule in the Ni(111) and the Pd(111)
systems interact via the O of the -CHO group as well. Therefore, as shown in figure 7, the consideration of the number of states for the metal d-orbitals which hybridize with the O p-orbitals is also required. As summarized in table 5, the number of states for the metal d-orbitals which hybridize with the O p-orbitals for the Ni(111) system is larger than that for the Pd(111) system. From this analysis, we conclude that the atoms with higher electronegativity (in this case, O as compared to C) play a key role in determining higher stability of the interacting systems.

### 3.6.2. Stability of furfural on the M(110) and the M(100) surfaces

In the case of the Ff/M(110) systems, both C- and O-atoms of the Ff molecule are within the bonding regions of the metal surfaces. Therefore, as explained in the previous section, the number of states for the metal d-orbitals which hybridize with the O p-orbitals is considered. The results show that the

| furfural on | area of d (number of states) | under C | under O |
|------------|-------------------------------|---------|---------|
|            | up | down | up | down |
| Ni(111)    | 0.080 | 0.071 | 0.099 | 0.075 |
| Pd(111)    | 0.100 | 0.099 | 0.063 | 0.063 |
| Pt(111)    | 0.230 | 0.230 | — | — |
| Ni(110)    | 0.058 | 0.050 | 0.103 | 0.084 |
| Pd(110)    | 0.111 | 0.111 | 0.062 | 0.062 |
| Pt(110)    | 0.136 | 0.136 | 0.136 | 0.136 |
| Ni(100)    | 0.071 | 0.059 | 0.296 | 0.306 |
| Pd(100)    | 0.076 | 0.076 | 0.070 | 0.070 |
| Pt(100)    | 0.176 | 0.176 | — | — |

Figure 7. Partial density of states of the O-atom of the -CHO group of furfural to the (a) Ni(111) and (b) the Pd(111) surfaces. The area under investigation (denoted by dotted rectangle) for understanding chemical bonding of the Ff molecule on the Ni(111) and the Pd(111) surfaces is shown in (c) and (d), respectively. The green and black lines represent O p and M d-orbitals respectively.

Table 5. The area under C p and O p orbitals (in number of states) in the major overlapping region.

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number of states for the Ff/Pt(110) system is larger than Ni(110), followed by Pd(110), indicating that the Ff molecule is chemically bonded more strongly to the Pt(110) surface followed by Ni(110) and Pd(110), in line with the calculated adsorption energies shown in table 2. Using the same approach for the Ff/M(100) systems, we find that the Ff/Ni(100) system has the largest number of states for the hybridizing d-orbitals (table 5), enabling the Ff molecule to bond strongly to the Ni(100) surface, followed by Pt(100) and Pd(100) surfaces. Since there is no direct interaction between the O-atoms of the Ff molecule with the Pt(100) surface, the number of d-orbitals hybridizing with the C p-orbitals is considered. The PDOS analysis for the d-orbitals of the surface metal and p-orbitals of the interacting C- and O-atoms allows a more detailed understanding of the trends in the calculated adsorption energy.

3.7. Crystal orbital overlap population

To gain further insight into the bonding mechanism of the adsorption of the Ff molecule on the metal surfaces, we calculated PDOS onto molecular orbital and COOP using the STATE code. COOP

Figure 8. Density of states projected onto molecular orbitals (PDOS) and density of states weighted by crystal orbital overlap population (COOP) for the Ff molecule adsorbed on Ni(110). (a) spin up, (b) spin down. Gaussian broadening with the width of 0.01 eV was used. Origin of the energy is the Fermi level (E_F).
characterizes the interaction between molecular orbital (MO) and the substrate states, and the positive COOP indicates the bonding interaction between MO and substrate states, whereas the negative COOP, an antibonding interaction. Figures 8–10, show PDOS and COOPs of the HOMO-1, HOMO, LUMO and LUMO+1 for the Ff molecule adsorbed on metal (110) surface. Overall, we can see significant hybridization of HOMO and HOMO-1 (figure 11) with the substrate states. At the same time, antibonding parts of the HOMO and HOMO-1 derived states (negative COOP for HOMO and HOMO-1) are partially occupied, indicating Pauli repulsion of HOMO and HOMO-1 with the substrate states. We see that the HOMO hybridizes significantly, and the degree of hybridization correlates with the adsorption strength. In the case of Pt(110), the HOMO derived states distribute broadly (to approx. 7.0 eV below the Fermi level). Furthermore, LUMO and LUMO-1 (figure 10) are partially occupied and hybridize with the substrate states as indicated by the corresponding COOPs, which contributes to the stabilization of the Ff molecule on the surface and is a factor determining the stability of the molecule.

4. Summary and conclusion

In this study, we reported that the Pt/TiO₂ catalyst and Pd/TiO₂ exhibited superior activity as compared to the Ni/TiO₂ catalyst. Furthermore, it was observed that there is a difference not only in their activity but also in their selectivity profile. The Ni/TiO₂ catalyst had a preferential selectivity towards THFA, whereas Pd/TiO₂ and Pt/TiO₂ favoured FA. To understand the fundamental nature of the interaction between the Ff molecule and the low index Ni, Pd and Pt surfaces, we performed DFT analyses and found that the adsorption energy of the Ff molecule is the largest on the Pt(111) surface, followed by those for the Ni(111) and the Pd(111) surface. On the (110) surfaces, the adsorption energy of the Ff molecule follows a similar trend to the (111) surfaces. However, on the M(110) surface, the adsorption energy of the Ff molecule is largest for the Ni surface, followed by those for the Pt and Pd surfaces. To understand better the probable reasons for the calculated trends of the adsorption energies we investigated the geometrical and the local electronic properties of the Ff/M(h,k,l) surfaces. The analyses of the geometrical properties show that depending on the metal surface the Ff molecule may adopt a different configuration, which may lead to different preferential hydrogenation reactions. The Bader charge analysis reveals electron transfer from metal to the Ff molecule on the Ni and Pd surfaces, while a reverse process occurs on the Pt surface, which is indicated by the presence of a
Figure 10. Density of states projected onto molecular orbitals (PDOS) and density of states weighted by crystal orbital overlap population (COOP) for the Ff molecule adsorbed on Pt(110). Gaussian broadening with the width of 0.01 eV was used. Origin of the energy is the Fermi level (E_F).

Figure 11. The wavefunctions for (a) LUMO+1, (b) LUMO, (c) HOMO and (d) HOMO-1 for the fully optimized furfural molecule.
residual negative charge on its exposed surface. From the density of states analysis, we conclude that the stability of the Ff molecule can be directly related to the metal d-states which hybridize with its nearest C and O p-orbitals. Based on our DFT analyses, we further conclude that the interactions between atoms with higher electronegativity and the metal d-states play a key role in determining the stabilities of the Ff/M(h,k,l,J) systems under investigation.

Data accessibility. All data are available from the Dryad Digital Repository: https://doi.org/10.5061/dryad.0zpc866zm [53].

Authors’ contributions. A.Z.K.: data curation, formal analysis; J.A.: data curation, formal analysis; R.G.: data curation, formal analysis; I.H.: formal analysis, visualization, writing—review and editing; P.P.W.: writing—review and editing; N.D.: writing—review and editing; A.V.: conceptualization, data curation, formal analysis, writing—original draft; C.R.A.C.: conceptualization, writing—review and editing; A.C.: conceptualization, data curation, formal analysis, project administration, supervision, validation, visualization, writing—original draft.

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References

1. Lange JP, Van Der Heide E, Van Buijtenen J, Price R. 2012 Furfural: a promising platform for lignocellulosic biofuels. ChemSusChem 5, 150–166. (doi:10.1002/cssc.201100648)
2. Huber GW, Ibarra S, Gurma A. 2006 Synthesis of transportation fuels from biomass: chemistry, catalysis, and engineering. Chem. Rev. 106, 4044–4096. (doi:10.1021/cr0583600)
3. Stöcker M. 2008 Biofuels and biomasses-to-liquid fuels in the biofinef: catalytic conversion of lignocellulosic biomass using porous materials. Angew. Chem. Int. Ed. 47, 9200–9211. (doi:10.1002/anie.200801476)
4. McKendry P. 2002 Energy production from biomass, and engineering. Biorenewables Technol. 83, 37–46. (doi:10.1016/S0960-8524(01)00118-3)
5. Kobayashi H, Otga H, Fukuoka A. 2012 Conversion of lignocellulose into renewable chemicals by heterogeneous catalysis. Catal. Sci. Technol. 2, 869–883. (doi:10.1039/c2cy00500j)
6. Machado G, Leon S, Santos F, Loureiro R, Dullius J, Neillmann ME, Eichler P. 2016 Literature review on furfural production from lignocellulosic biomass. Nat. Resour. 07, 115–129. (doi:10.4236/nr.2016.73012)
7. Hu X, Westerhoff RJM, Dong D, Wu L, Lu CZ. 2014 Acid-catalyzed conversion of Xylose in 20 solvents: insight into interactions of the solvents with Xylose, furfural, and the acid catalyst. ACS Sustain. Chem. Eng. 2, 2562–2575. (doi:10.1021/acsceneng.1c004659)
8. Komanty Y, Kobayashi H, Hera K, Chui WJ, Fukuoka A. 2014 Kinetic study of catalytic conversion of cellulose to sugar alcohols under low-pressure hydrogen. ChemCatChem 6, 230–236. (doi:10.1002/cctc.201300731)
9. Chidambaram M, Bell AT. 2010 A two-step approach for the catalytic conversion of glucose to 2,5-dimethylfuran in ionic liquids. Green Chem. 12, 1253–1262. (doi:10.1039/c00434e)
10. Sithsina S, Pham T, Prasomtn T, Sooknui T, Mallinson RG, Tesasco DE. 2011 Conversion of furfural and 2-methylpentanal on Pd/502 and Pd-Cu/SiO2 catalysts. J. Catal. 280, 17–27. (doi:10.1016/j.jcat.2011.02.006)
11. Adkins H, Conan R. 1931 The catalytic hydrogenation of organic compounds over copper chromite. J. Am. Chem. Soc. 53, 1091–1095. (doi:10.1021/ja13540a041)
12. Matsagari BM, Hsu C, Chen SS, Ahmed T, Alshehri SM, Tsang DCW, Wu KC. 2020 Selective hydrogenation of furfural to tetrahydrofurfuryl alcohol over a Rh-loaded carbon catalyst in aqueous solution under mild conditions. Sustain. Energy Fuels 4, 293–301. (doi:10.1039/c9se00618h)
13. Tiike MA, Mahajani JV. 2007 Kinetics of liquid-phase hydrogenation of furfuryl alcohol to tetrahydrofurfuryl alcohol over a Ru/TiO2 catalyst. Ind. Eng. Chem. Res. 46, 3275–3282.
14. Sithsina S, An W, Tesasco DE. 2011 Selective conversion of furfural to methylenol over silica-supported NiFe bimetallic catalysts. J. Catal. 284, 90–101. (doi:10.1016/j.jcat.2011.09.005)
15. Moroé C, Belgacem MN, Gandini A. 2004 Recent catalytic advances in the chemistry of substituted furans from carbohydrates and in the ensuing polymers. Top. Catal. 27, 11–30. (doi:10.1023/B:TOCA.0000013517.13540.e)
16. Jia J, Zheng W, Lobo RF, Vlachos DG. 2013 Production of dimethylfuran from hydroxymethylfurfural through catalytic transfer hydrogenation with ruthenium supported on carbon. ChemSusChem 6, 1158–1162. (doi:10.1002/cssc.201300288)
17. Chen C, Wang L, Zhu B, Zhou Z, El-Hout SI, Yang J, Zhang J. 2021 2,5-Furandicarboxylic acid production via catalytic oxidation of 5-hydroxymethylfurfural: catalysts, processes and reaction mechanism. J. Energy Chem. 54, 528–554. (doi:10.1016/j.jechem.2020.05.068)
18. Nakagawa Y, Nakazawa H, Watanabe H, Tomishige K. 2012 Total hydrogenation of furfural over a silica-supported nickel catalyst prepared by the reduction of a nickel nitrate precursor. ChemCatChem 4, 1791–1797. (doi:10.1002/cctc.201200218)
19. Nakagawa Y, Tamura M, Tomishige K. 2013 Catalytic reduction of biomass-derived furanic compounds with hydrogen. ACS Catal. 3, 2655–2668. (doi:10.1021/cs400616p)
20. Bao R, Guoan HM. 1939 Process for the manufacture of furfuryl alcohol and methylfuran. US Patent no. 1739919 A.
21. Lazier WA. 1937 Process for hydrogenating furfural. US Patent no. 2 077 422.
22. Swadeshi S. 1956 Catalytic production of furfuryl alcohol and catalyst therref. US Patent no. 2 754 304.
23. Pushkarev VK, Muselwhite N, An K, Alayoglu S, Somorjai GA. 2012 High structure sensitivity of vapor-phase furfural decarboxylation/hydrogenation reaction network as a function of size and shape of Pt nanoparticles. Nano Lett. 12, 5196–5201. (doi:10.1021/ nl3031237)
24. Nakagawa Y, Takada K, Tamura M, Tomishige K. 2014 Total hydrogenation of furfural and 5-hydroxymethylfurfural over supported Pd-Ir alloy catalyst. ACS Catal. 4, 2718–2726. (doi:10.1021/cs500620b)
25. Schoonbaum CA, Schwartz DK, Medlin JW. 2014 Controlling the surface environment of heterogeneous catalysts using self-assembled monolayers. Acc. Chem. Res. 47, 1438–1445. (doi:10.1021/ar500029y)
26. Rogers SM et al. 2017 Tandem site- and size-controlled Pd nanoparticles for the directed hydrogenation of furfural. ACS Catal. 7, 2266–2274. (doi:10.1021/acscatal.6b03190)
27. Pang SH, Schoenbaum CA, Schwartz DK, Medlin JW. 2013 Directing reaction pathways by catalyst active-site selection using self-assembled monolayers. Nat. Commun. 4, 2448. (doi:10.1038/ncomms3448)

28. Jeong H, Kim C, Yang S, Lee H. 2016 Selective hydrogenation of furanic aldehydes using Ni nanoparticle catalysts capped with organic molecules. J. Catal. 344, 69–615. (doi:10.1016/j.jcat.2016.11.002)

29. Wang C, Wang L, Zhang J, Wang H, Lewis JP, Xiao F. 2016 Product selectivity controlled by zeolite crystals in biomass hydrogenation over a palladium catalyst. J. Am. Chem. Soc. 138, 7880–7883. (doi:10.1021/jacs.6b04951)

30. Xue J, Wang Y, Meng Y, Zhou X, Pan G, Xia S. 2020 Theoretical investigation of decarbonylation mechanism of furfural on Pd(111) and Ni(111) surfaces. Mol. Catal. 493, 110554. (doi:10.1016/j.molcatal.2020.110554)

31. Ren G, Wang G, Mei H, Xu Y, Huang L. 2019 A theoretical insight into fural conversion catalyzed on the Ni(111) surface. Phys. Chem. Chem. Phys. 21, 23685–23696. (doi:10.1039/c9cp02486b)

32. Campisi S, Chan-Thaw CE, Chinchilla LE, Chutia A, Botton GA, Prati L. 2017 Diols production from glycerol over Pt-based catalysts: on the role played by the acid sites of the support. Catal. Lett. 147, 2523–2533. (doi:10.1007/s10562-017-2183-5)

33. Villalva, Manzelli M, Violdini F, Chinchilla LE, Botton GA, Prati L. 2017 Dols production from glycerol over Pt-based catalysts: on the role played by the acid sites of the support. Catal. Lett. 147, 2523–2533. (doi:10.1007/s10562-017-2183-5)

34. Kresse G, Hafner J. 1993 Ab initio molecular dynamics for liquid metals. Phys. Rev. B 47, 558–561. (doi:10.1103/PhysRevB.47.558)

35. Kresse G, Furthmüller J. 1996 Efficient iterative schemes for ab initio total-energy calculations using a plane-wave basis set. Phys. Rev. B 54, 11 169–11 186. (doi:10.1103/PhysRevB.54.11169)

36. Blochl PE. 1994 Projector augmented-wave method. Phys. Rev. B 50, 17 953–17 979. (doi:10.1103/PhysRevB.50.17953)

37. Perdew JP, Ruzsinszky A, Csonka GI, Vydrov OA, Scuseria GE, Constantin LA, Zhou X, Burke K. 2008 Restoring the density-gradient expansion for exchange in solids and surfaces. Phys. Rev. Lett. 100, 136406. (doi:10.1103/PhysRevLett.100.136406)

38. Davey WP. 1925 Precision measurements of the lattice constants of twelve common metals. J. Phys. Condens. Matter 3382344)

39. Momma K, Izumi F. 2008 VESTA : a three-dimensional visualization system for electronic and structural analysis. J. Appl. Crystallogr. 41, 653–658. (doi:10.1107/S0021889808012016)

40. Bengtsson L. 1999 Dipole correction for surface based Bader analysis algorithm without lattice documentation. See https://state-doc.royalsocietypublishing.org/journal/rsos.

41. Grimme S, Antony J, Ehrlich S, Krieg H. 2010 A consistent and accurate ab initio parametrization of density functional dispersion corrections to density functional theory. Phys. Rev. B 81, 125160. (doi:10.1103/PhysRevB.81.125160)

42. Tang W, Sanville E, Henkelman G. 2009 A grid-based Badger analysis algorithm without lattice bias. J. Phys.: Condens. Matter 21, 084204. (doi:10.1088/0953-8984/21/8/084204)

43. Momma K, Izuimi F. 2008 VESTA : a three-dimensional visualization system for electronic and structural analysis. J. Appl. Crystallogr. 41, 653–658. (doi:10.1107/S0021889808012016)

44. Momma K, Izuimi F. 2011 VESTA 3 for three-dimensional visualization of crystal, volumetric and morphology data. J. Appl. Crystallogr. 44, 1272–1276. (doi:10.1107/ S0021889810038970)

45. Neese F, Wenmohs F, Becker U, Riplinger C. 2020 The ORKA quantum chemistry program package. J. Chem. Phys. 152, 224108.

46. Morikawa Y, Inagaki K, Hamamoto Y, Hamada I. 2012 Simulation Tool for Atom Technology documentation. See https://state-doc.royalsocietypublishing.org/ on 03 May 2022.

47. Morikawa Y, Ishih K, Seki K. 2004 Theoretical study of n-alkane adsorption on metal surfaces. Phys. Rev. B 69, 041403. (doi:10.1103/PhysRevB.69.041403)

48. Hoffmann R. 1988 A chemical and theoretical way to look at bonding on surfaces. Rev. Mod. Phys. 60, 601. (doi:10.1103/RevModPhys.60.601)

49. Aizawa H, Tsuneyuki S. 1998 First-principles study of CO bonding to Pt(111): validity of the Blyholder model. Surf. Sci. 399, L364–L370. (doi:10.1016/S0039-6028(98)00042-9)

50. Hamamoto Y, Wills SA, Inagaki K, Ablid-Pedersen F, Bilgardi T, Hamada I, Morikawa Y. 2020 Enhanced CO tolerance of Pt clusters supported on graphene with lattice vacancies. Phys. Rev. B 102, 75408. (doi:10.1103/PhysRevB.102.075408)

51. Liu B, Cheng L, Curtiss L, Grieve J. 2014 Effects of van der Waals density functional corrections on trends in furfural adsorption and hydrogenation on close-packed transition metal surfaces. Surf. Sci. 622, 51–59. (doi:10.1016/j.susc.2013.12.001)

52. Chutia A. 2022 A study on the stability of gold bimetallic clusters on the Pd(111) surface. Digital Repository. (doi:10.5061/dryad.oszpc866zm)

53. Khan A, Ait JJ, Germaney R, Hamada I, Wells PP, Dimitratos N, Catlow CRA, Villa A, Chutia A. 2022 Data from: A comparative study of the stability of the furfural molecule on the low index Ni, Pd and Pt surfaces. Dryad Digital Repository. (doi:10.5061/dryad.0gc866zm)