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Thermophoresis and Brownian Effect for Chemically Reacting Magneto-Hydrodynamic Nanofluid Flow across an Exponentially Stretching Sheet

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Abstract: This comparative research investigates the influence of a flexible magnetic flux and a chemical change on the freely fluid motion of a (MHD) magneto hydrodynamic boundary layer incompressible nanofluid across an exponentially expanding sheet. Water and ethanol are used for this analysis. The temperature transmission improvement of fluids is described using the Buongiorno model, which includes Brownian movement and thermophoretic distribution. The nonlinear partial differential equalities governing the boundary layer were changed to a set of standard nonlinear differential equalities utilizing certain appropriate similarity transformations. The bvp4c algorithm is then used to tackle the transformed equations numerically. Fluid motion is slowed by the magnetic field, but it is sped up by thermal and mass buoyancy forces and thermophoretic distribution increases non-dimensional fluid temperature resulting in higher temperature and thicker boundary layers. Temperature and concentration, on the other hand, have the same trend in terms of the concentration exponent, Brownian motion constraint, and chemical reaction constraint. Furthermore, The occurrence of a magnetic field, which is aided by thermal and mass buoyancies, assists in the enhancement of heat transmission and wall shear stress, whereas a smaller concentration boundary layer is produced by a first-order chemical reaction and a lower Schmidt number.

Keywords: exponentially stretching surface; fluid; Brownian motion; Buongiorno model; boundary layer

1. Introduction

The learning of flow and temperature transmission across a stretched surface has piqued the interest of many investigators over the past few decades due to its various important engineering applications. Initially, Crane [1] investigated the boundary layer flow overstretched surfaces theoretically. Das [2] explained the slip movement of nanofluid above a porous enlarging surface. Later on, a slew of researchers [3–7] has stepped up to contribute to various areas of movement and temperature transmission problems concerning stretched surfaces.

Fluids containing nanoparticles of 100 nanometers or smaller in size, like oxides and metals, as well as traditional base fluids including water, kerosene oil, are called nanofluid. Because nano-sized particles have a higher temperature transfer rate than base fluids. They are utilized as efficient coolants in electronics and nuclear plants, lubricants, etc. Choi [8] made an ironic start by studying experimentally and revealing to the public the
increase of temperature conductivity of liquids using nanoparticles. Hussain et al. [9] discussed the nanofluid flow over the rotating cone. Makinde and Aziz [10] utilized the convective surface settings to illustrate the frontier layer movement of a nanofluid across a stretched surface. The boundary-layer movement of nanofluids across stretched sheets was established by Khan and Pop [11]. Buongiorno [12] later developed a heterogeneous symmetry model to represent the temperature transmission increase of nanofluid caused by Brownian movement and thermophoretic distribution of nanoparticles. Hussain et al. [13] discussed the multi-based nanofluid flow over an embrittled cone. Nayak et al. [14] have examined the 3D (three-dimensional) MHD movement of nanofluid across a porous linear expanding surface with free convection with the effect of heat radiation, taking into consideration realistic factors.

Many researchers [15–20] have investigated the nanofluid with MHD movement and temperature transmission possessions in different physical problems until now. This is owing to important uses in industrial processes, such as its wide variety of biological applications, including wound therapy and sterilization. The movement and temperature transmission features of magneto-nanofluid were addressed by Bahiraei and Hangi [21]. Hsiao [22] elaborated the micro polar nanofluid flow with different effects towards a stretching sheet. Akber et al. [23] developed a computational method for modeling MHD transportation of nanofluids via a perpendicular stretching sheet that took into account non-linear temperature-dependent viscosity and buoyancy possessions. Through an exponential enlarging sheet, Nadeem et al. [24] examined the thermo-physical characteristics of water-based nanofluids. Bahiraei [25] stressed the need for studying nanoparticle dispersion concerning effective variables on particle movement and phenomenological coefficients using Lagrangian simulation.

The chemical reaction is crucial because, among other things, it influences the design of chemical processing facilities, food & beverages, chillers, fog production, and distribution. In light of the aforementioned uses, numerous researchers have researched and published their findings on the impact of chemical reactions on the movement of temperature and/or mass transmission through various faces. The stimulus of chemical processes on MHD immobility point movement of water-based in a permeable medium driven by heat radiation and viscid intemperance was studied by Mabood et al. [26]. They discovered that increasing the chemical reaction constraint improves the non-dimensional combination profiles of water-based nanofluids in their research. They also discovered that when the rate of chemical reactions rises, so does the rate of mass transfer. The MHD movement of a viscoelastic fluid across a permeable stretched sheet was described by Nayak [27]. Sheikholeslami & Sadoughi [28] deliberated the Mesoscopic method for MHD nanofluid considering various shapes of nanoparticles. The rotational flow of nanofluid across a nonlinear extending surface was mathematically deliberated by Mushtaq et al. [29]. MHD immobility point movement was reported by Kahn et al. [30]. Bhatti and Rashidi [31] investigated the thermal transmission and effects of heat radiation on non-Newtonian nanofluid. Sui et al. [32] reported the Cattaneo–Christov distribution in viscoelastic nanofluid. The MHD movement of nanofluid across a radiative nonlinear enlarging sheet was presented by Imtiaz et al. [33]. Some of the preceding research’ applications can be viewed in this way via [34–36]. Recently, Hussain et al. [37] made an extra ordinary research for Two-Phase Nanofluid in Brittle Medium and heat transmission analysis. Sulochana et al. [38] numerically investigated the thermophoresis and Brownian movement for MHD flow due to a rotational cone. Raju et al. [39] explained the Jeffrey (MHD) nanofluid movement over a cone with chemical reaction. Makinde et al. [40] described the stagnation point movement of MHD chemically reacting radiative heat.

According to the above-mentioned review of the literature, no one has investigated the stimulus of a flexible transversal magnetic strength and chemical reaction on unrestricted convection of a nano fluid movement via an exponentially enlarging surface using Brownian movement and thermophoretic distribution till now. As a result, the novelty of our research is to look comparatively for water and ethanol due to many industrial applications e.g.,
manufacturing of plastics, polishes, and cosmetics. Similarly ethanol is used in medicine as a topical anti-infective. The impact of a variable transversal magnetic strength and a chemical reaction in a free convective nanofluid flowing above an exponential extending surface is discussed for both fluids. The leading boundary layer equalities are numerically tackled using the bvp4c algorithm at Matlab. The effects of velocity streamlines, non-dimensional concentration, temperature and velocity profiles of nanoparticles, alongside the skin resistance, Nusselt and Sherwood numbers, are explored and illustrated in graphs, and tables.

2. Problem Formulation

Above an exponentially stretching surface, we examine a steady three dimensional (3D) incompressible boundary layer flow of electrically conducing magneto hydrodynamic nanofluid. Assume that an \( B = B_0 e^{\frac{x+y}{L}} \) a variable magnetic field is applied parallel to the z-axis. It is expected that the persuaded magnetic and electric fields would be ignored. Owing to the existence of binary significant velocity-slip factors, such as Brownian movement and thermophoretic distribution of nanoparticles, the Buongiorno model [12] is used in this work to explain the analogues increase of temperature transmission. There are the following main equations for mass, momentum, energy, and nanoparticle concentration:

\[
\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0, \tag{1}
\]

\[
u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} - \nu \frac{\partial^2 u}{\partial z^2} = \frac{\sigma B^2 u}{\rho_f}, \tag{2}
\]

\[
u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} - \nu \frac{\partial^2 v}{\partial z^2} = \frac{\sigma B^2 v}{\rho_f}, \tag{3}
\]

\[
u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} + w \frac{\partial T}{\partial z} = \alpha_f \frac{\partial^2 T}{\partial z^2} + \tau \left[ D_b \frac{\partial C}{\partial z} + D T \left( \frac{\partial T}{\partial z} \right)^2 \right], \tag{4}
\]

\[
u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} + w \frac{\partial C}{\partial z} = D_b \frac{\partial^2 C}{\partial z^2} + D T \frac{\partial^2 T}{\partial z^2} - K_c (C - C_\infty). \tag{5}
\]

The following are the corresponding frontier conditions for the current problem:

\[
u = U_w = U_0 e^{\frac{x+y}{L}}, \quad v = V_w = V_0 e^{\frac{x+y}{L}}, \quad w = 0,
\]

\[
T = T_w = T_\infty + T_0 e^{\frac{2(x+y)}{L}}, \quad C = C_w = C_\infty + C_0 e^{\frac{2(x+y)}{L}} \quad \text{at} \ z = 0 \tag{6}
\]

\[
u \to 0, \quad v \to 0, \quad T \to T_\infty, \quad C \to C_\infty \quad \text{as} \ z \to \infty. \tag{7}
\]

here \( u, v \) and \( w \) are velocity components alongside \( x, y \) and \( z \)-directions respectively. \( \nu \) is kinematics viscosity, \( g \) is gravitational acceleration, \( \beta_T \) is thermal expansion (of volumetric concentration of), \( \beta_C \) is mass expansion (of volumetric concentration). \( T_\infty \) is the of surrounding temperature, \( C_\infty \) is nanoparticle concentration at the free stream, the electrical conductiviness of fluid is \( \sigma \). \( B_0 \) is a consistent magnetic field, \( \rho_f \) is the density of the fluid, \( \alpha_f \) is the temperature distribution of fluid, \( \tau \) is a proportion between effective heat capacitance of nanoparticle material and heat capability of fluid, \( D_b \) is Brownian movement constant, \( D_T \) is thermophoretic distribution constant, \( K_c \) is chemical reaction constraint, \( U_0, V_0, U_w, V_w \) are fixed velocities, \( L \) is locus length, \( T_w \) is the temperature at the surface and \( C_w \) is nanoparticle concentration over the surface of the sheet.
To make the investigation easier, the boundary layer equalities are rendered to dimensionless form utilizing the following similarity transformation:

\[
u = U_0 e^{\frac{x+y}{2L}} f'(\eta), \quad v = V_0 e^{\frac{x+y}{2L}} g'(\eta),
\]

\[
w = -\left(\frac{v_f U_0}{2L}\right) \frac{1}{2} e^{\frac{x+y}{2L}} \{ f(\eta) + \eta f'(\eta) + g(\eta) + \eta g'(\eta) \},
\]

\[
T = T_\infty + T_0 e^{\frac{A(x+y)}{x+y}} \theta(\eta), \quad C = C_\infty + C_0 e^{\frac{B(x+y)}{x+y}} \phi(\eta),
\]

where \( \eta = \left(\frac{U_0}{2\sqrt{T}}\right) \frac{1}{2} e^{\frac{x+y}{2L}} z. \)

here \( A, B \) are temperature and concentration exponents respectively. By using Equation (8) in Equations (1)–(5) we satisfying the continuity equation and gain the following transformed equations:

\[
f'' + (f + g) f'' - 2(f' + g') f' + 2\lambda_1 \theta + 2\lambda_2 \phi - M f' = 0, \quad (9)
\]

\[
g'' + (f + g) g'' - 2(f' + g') g' + 2\lambda_1 \theta + 2\lambda_2 \phi - M g' = 0, \quad (10)
\]

\[
\theta'' + Pr \left[ (f + g) \theta' - A(f' + g') \theta + N_b \theta' \phi' + N_t (\theta')^2 \right] = 0, \quad (11)
\]

\[
\phi'' + S_c \left[ (f + g) \phi' - B(f' + g') \phi - \gamma \phi \right] + \frac{N_t}{N_b} \theta' = 0. \quad (12)
\]

With transformed boundary conditions:

\[
f = 0, \quad g = 0, \quad f' = 1, \quad \phi' = \beta, \quad \theta = 1, \quad \phi = \eta, \quad \text{at} \ \eta = 0,
\]

\[
f' \to 0, \quad g' \to 0, \quad \theta \to 0, \quad \phi \to 0, \quad \text{as} \ \eta \to \infty
\]

here

\[
\beta = \frac{V_0}{U_0}, \quad Pr = \frac{v_t}{\alpha}, \quad Gr = \frac{\varrho B_T (T_w - T_\infty) L^3}{v_t^3}, \quad Gc = \frac{\varrho B_c (C_w - C_\infty) L^3}{v_t^3},
\]

\[
S_c = \frac{v_t}{D_b}, \quad N_b = \frac{\tau D_b (C_w - C_\infty)}{v_t}, \quad N_t = \frac{\tau (T_w - T_\infty)}{v_t T_\infty}, \quad (14)
\]

here \( \beta, \ Pr, \ Gr, \ Gc, \ S_c, \ N_b, \ N_t \) are surface stretching velocity proportion constraint, Prandtl number, temperature and mass Grashof number, Schmidt number, Brownian movement, and thermophoresis constraints respectively. The Hartman coefficient \( M_x \) and \( M_y \) (in x-direction and y-direction) which is defined as: \( M_x = \frac{2\varrho B_e L}{\rho U_0} \) and \( M_y = \frac{2\varrho B_e L}{\rho V_0} \) respectively. Temperature convective constraint \( \lambda_T \) along x and y-axis is defined as: \( \lambda_{Tx} = \frac{Gr}{Re_x^2} \) and \( \lambda_{Ty} = \frac{Gr}{Re_y^2} \) respectively. The mass convective constraints \( \lambda_M \) in x-direction and y-direction is defined as: \( \lambda_{Mx} = \frac{Gr}{Re_x^2} \) and \( \lambda_{My} = \frac{Gr}{Re_y^2} \) respectively. The local Reynold number \( Re \) in x-direction and y-direction is defined as: \( Re_x = \frac{U_0 L}{\nu} \) and \( Re_y = \frac{V_0 L}{\nu} \) respectively. Skin frictions in x-direction and y-direction are defined as:

\[
C_{fx} = \frac{\tau_{wx}}{2 \rho q w^2}, \quad (15)
\]

\[
C_{fy} = \frac{\tau_{wy}}{2 \rho q w^2}. \quad (16)
\]

here \( \tau_{wx} \) and \( \tau_{wy} \) are wall shear stresses in x and y directions respectively.

The non-dimensional forms of Equations (15) and (16) can be written as:

\[
\sqrt{\frac{Re_x}{2}} C_{fx} = f'(0), \quad (17)
\]
\[ \sqrt{\frac{\text{Re}_x}{2}} C_{fy} = g''(0). \] (18)

The Nusselt and Sherwood coefficients are articulated as:

\[ \text{Nu}_x = \frac{xq_m}{k_f(T_w - T_\infty)}, \] (19)

\[ \text{Sh}_x = \frac{xq_m}{D_B(C_w - C_\infty)}. \] (20)

here \( q_w = -k_f \left( \frac{\partial T}{\partial z} \right)_{z=0} \) is wall heat flux and \( q_m = -D_B \left( \frac{\partial C}{\partial z} \right)_{z=0} \) is mass flux from extending sheet respectively. The non-dimensional form of Equations (19) and (20) is written as:

\[ \left( \frac{\text{Re}_x}{2} \right)^{-1/2} \text{Nu}_x = -\frac{x}{L} \theta'(0), \] (21)

\[ \left( \frac{\text{Re}_x}{2} \right)^{-1/2} \text{Sh}_x = -\frac{x}{L} \phi'(0). \] (22)

3. Discussion and Graphical Results

The boundary conditions are specified in Equation (13) and the system of linked nonlinear differential Equations (9)–(12) is solved numerically using the bvp4c algorithm. This technique converts higher-order ordinary differential equations (ODEs) into first-order ODEs and is then tackled numerically at MATLAB.

The current work looked at the impact of a changing perpendicular magnetic strength and a chemical reaction on the free convective movement of fluids across an exponentially extending surface. Additionally, the Buongiorno model is utilized to examine the impact of Brownian movement and thermophoretic distribution. The bvp4c algorithm is employed to tackle the similarity transformed governing boundary layer equalities and related converted boundary conditions. In the tables below and graphs, the acquired results are presented. The configuration of the problem is presented in the following (see Figure 1).

![Exponentially stretching surface MHD flow.](image)

**Figure 1.** Exponentially stretching surface MHD flow.

3.1. Velocity Profiles

The following figures show the effects of flow constraints on non-dimensional velocity, temperature, concentration profiles of nanoparticles. For varying intensity of the Hartman number \( M \), the fluctuation of velocity constituents alongside the \( x \) and \( y \) axes is shown in Figure 2a,b. It is clear that velocity constitutes \( f(\eta) \) and \( g'(\eta) \) gain deceleration by increasing \( M \), which results in a thinner boundary layer for both fluids. This is because the
electromagnetic contact among the magnetic field strength and the electrically conducting fluid produces a resisting Lorentz force, which decelerates the fluid’s velocity across the boundary layer area. To put it another way, if magnetic field is not applied, there would be no contact between the electrically conducting fluid and the magnetic field, and therefore, there will be no velocity slow down and the velocity would remain constant. It is said to have arrived at the deduction that the existence of M alters the fluid velocity significantly. The influence of temperature convective constraint $\lambda_T$ is shown in Figure 3a,b. Basically, thermal convection $\lambda_T$ is the transfer of heat related to conduction and motion of fluid over a given body. So, when thermal convective parameter $\lambda_T$ increases, both velocities $f'(\eta)$ and $g'(\eta)$ accelerate. Convective mass transfer is the movement of material related to the motion of a fluid. Therefore, when the mass convective parameter $\lambda_M$ increases the velocity of the fluid also increases. This behavior can be noted for mass convective parameter $\lambda_M$ in Figure 4a,b. We concluded from this discussion that thermal convective constraint $\lambda_T$ and mass convective constraint $\lambda_M$ both have direct relation with fluid’s velocity constitutes $f'(\eta)$ and $g'(\eta)$.

Figure 2. (a) The effect of M on the velocity profile $f'(\eta)$; (b) The effect of M on the velocity profile $g'(\eta)$. 
Figure 3. (a) The effect of $\lambda_T$ on velocity profile $f'(\eta)$; (b) The effect of $\lambda_T$ on velocity profile $g'(\eta)$.

3.2. Temperature Profile

The effect of Hartmann number or magnetic field constraint $M$, temperature/heat exponent $A$, and thermophoresis constraint $N_t$ for temperature profile $\theta(\eta)$ is presented in the following Figures. The essential conclusion that can be drawn from Figure 5a is that the temperature rises as the Hartmann number $M$ rises. The sole explanation about this phenomenon is because an increment in $M$ generates a rise in electromagnetic force, which restricts liquid motion, causing the temperature to rise and a denser thermal boundary layer to form. In reality, the fluid temperature in the flow field could not be increased if there was no magnetic field. So, magnetic field constraint $M$ and temperature profile have direct relation to each other. It’s worth noting that, just as the fluid temperature rises as $M$ rises, the temperature of the liquid rises as the thermophoresis constraint $N_t$ rises. This is because thermophoretic distribution tends to a rise in the non-dimensional fluid temperature, increasing the fluid’s thermal resistance (see Figure 5b). This phenomenon is
caused by the temperature gradient. As the thermophoresis constraint $N_t$ increases, the particles of fluid move towards the high energy level leaving the colder region and the temperature profile rises. In this way thermophoresis constraint $N_t$ have direct relation with temperature profile. We also argue that in Figure 5c, the temperature exponent $A$, when compared to $M$ and $N_t$, exhibits the opposite tendency on temperature profiles. The temperature exponent $A$ decays the temperature profile decays as the value of $A$ increases. So we arrived at the conclusion that temperature exponent $A$ have inverse relation with temperature profile.

Figure 4. (a) The effect of $\lambda_M$ on velocity profile $f'(\eta)$; (b) The effect of $\lambda_M$ on velocity profile $g'(\eta)$.

Water Pr (Solid) = 6.3
Ethanol Pr (Dotted) = 18.6

$A=B=N_b=\gamma=M=\eta=\lambda_T=\beta = 0.5, Sc = 10$
Figure 5: (a) The effect of $M$ on temperature profile $\theta(\eta)$; (b) The effect of $N_t$ on temperature profile $\theta(\eta)$; (c) The effect of $A$ on temperature profile $\theta(\eta)$.
3.3. Concentration Profile

In terms of concentration profiles, the following Figures shows the variations in concentration constitute for dissimilar values of the thermophoresis constraint $N_b$, the concentration exponent $B$, and the chemical reaction constraint $\gamma$, as well as the variations in the thermal Brownian movement constraint $N_t$, the convective constraint $\lambda_T$, and the Schmidt number $S_c$. The effect of thermophoresis constraint $N_t$, Brownian motion constraint $N_b$, and thermal convective parameter $\lambda_T$ can be seen in Figure 6a. The concentration constitute $\phi(\eta)$ decreases with rising thermophoresis constraint $N_t$ and Brownian motion constraint $N_b$. The frontier layer thickness expands in the case of the thermophoresis constraint $N_t$ as compared to Brownian motion constraint $N_b$. We can to conclude that thermophoresis constraint $N_t$ and Brownian motion constraint $N_b$ have inverse relation with the concentration profile. The effect of concentration exponent and thermal convective parameter $\lambda_T$ can be noted in Figure 6b. The concentration profile get deceleration by rising the concentration exponent $B$ and thermal convective parameter $\lambda_T$. So, concentration profile have inverse relation with concentration exponent and thermal convective parameter $\lambda_T$. The impact of Schmidt number $S_c$ and chemical reaction constraint $\gamma$ is displayed in Figure 6c. It can be noted that enlarge change in $S_c$ shows a decay in the nano-particles concentration. The concentration profile also decays as and chemical reaction parameter $\gamma$ boosts up. The reason behind this phenomenon is that when $\gamma$ increases the particles take part in the chemical reaction and overall concentration profile decreases. So, chemical reaction parameter $\gamma$ and Schmidt number $S_c$ have inverse relation with the concentration constitute.

3.4. Skin Friction

Tables 1 and 2 show the manners of skin resistance for both fluids with the effect of $\beta$, $M$ and $\lambda_T$ in both $x$ and $y$ directions. These tables show that in the absence and presence of the magnetic field. Skin friction and therefore wall shear pressure decrease as the ratio parameter $\beta$ increases. The step-size increment in velocity ratio and Hartman number has decreased the skin friction in $x$-direction for both water and ethanol case. The skin friction for both cases although has decreased but very minor gradual decline is observed have inverse relation with the concentration profile. The skin friction in $y$-direction has been observed decreasing with an increment in ratio of surface velocity, Hartman number and temperature convective parameter (See Table 1). The skin friction in $y$-direction has been observed decreasing with an increment in ratio of surface velocity, Hartman number and temperature convective parameter (See Table 2). In both tables the skin friction decreases rapidly in case of water $Pr = 6.2$ as compared to ethanol $Pr = 18.6$. The reason is that low $Pr$ number fluids behave like Newtonian fluids.

**Table 1.** Skin friction $C_{fx}$ for different values when $\lambda_M = N_t = 0.5$.

| $\beta$ | $\frac{Re}{\tau} \frac{1}{2} C_{fx}$ for Water $Pr = 6.3$ | $\frac{Re}{\tau} \frac{1}{2} C_{fx}$ for Ethanol $Pr = 18.6$ |
|---------|--------------------------------------------------|--------------------------------------------------|
| $M = 0$ | $M = 1$ | $\lambda_T = 1$ | $\lambda_T = 2$ | $M = 0$ | $M = 1$ | $\lambda_T = 1$ | $\lambda_T = 2$ |
| 0.3     | -0.81966 | -1.13441 | -0.98289 | -0.49883 | -0.82226 | -1.13706 | -0.98568 | -0.50034 |
| 0.5     | -0.93333 | -1.23776 | -1.0912 | -0.61669 | -0.93868 | -1.24303 | -1.09667 | -0.62307 |
| 0.7     | -1.04136 | -1.33658 | -1.19446 | -0.72959 | -1.04897 | -1.34401 | -1.20213 | -0.74018 |
| 0.9     | -1.14429 | -1.43126 | -1.29313 | -0.83785 | -1.15374 | -1.44046 | -1.30259 | -0.85204 |

**Table 2.** Skin friction $C_{fy}$ for different values when $\lambda_M = A = 0.5$, $B = 0.8$.

| $\beta$ | $\frac{Re}{\tau} \frac{1}{2} C_{fy}$ for Water $Pr = 6.3$ | $\frac{Re}{\tau} \frac{1}{2} C_{fy}$ for Ethanol $Pr = 18.6$ |
|---------|--------------------------------------------------|--------------------------------------------------|
| $M = 0$ | $M = 1$ | $\lambda_T = 1$ | $\lambda_T = 2$ | $M = 0$ | $M = 1$ | $\lambda_T = 1$ | $\lambda_T = 2$ |
| 0.3     | 0.27341 | 0.14362 | 0.20398 | 0.74152 | 0.25796 | 0.1310 | 0.18974 | 0.72236 |
| 0.5     | -0.12769 | -0.30220 | -0.2197 | 0.28959 | -0.14276 | -0.3152 | -0.23406 | 0.26925 |
| 0.7     | -0.55827 | -0.77472 | -0.6715 | -0.18747 | -0.57277 | -0.7878 | -0.68556 | -0.20838 |
| 0.9     | -1.01725 | -1.27314 | -1.1504 | -0.6890 | -1.03108 | -1.2861 | -1.16398 | -0.71014 |
Figure 6. (a) The effect of $N_t$ and $N_b$ on concentration profile $\phi(\eta)$; (b) The effect of $B$ and $\lambda_T$ on concentration profile $\phi(\eta)$; (c) The effect of $\gamma$ and $S_c$ on concentration profile $\phi(\eta)$. 
3.5. Nusselt and Sherwood Number

Tables 3 and 4 show the manners of Nusselt and Sherwood number under the effect of thermophoresis constraint \( N_t \), Schmidt number \( S_c \), temperature convective constraint \( \lambda_T \), and mass convective constraint \( \lambda_M \). As thermophoresis constraint \( N_t \) rises, the Nusselt number decays in the existence of mass and thermal buoyancies within the thermal boundary layer. Increases in thermal buoyancy assist to decay temperature and increase in mass buoyancy resulting in a rise wall temperature gradient, as seen by the data in Table 3. It is noted low Prandtl liquids have low thermal distribution, high Prandtl liquid have high thermal distribution overstretched surface. It is noteworthy to point out that Nusselt numbers associated with various Pr values are quite comparable to one another, since a change in Pr results in a substantial change in thermal distribution in the thermal frontier layer. Similarly, as the Schmidt number \( S_c \) upsurges, the Sherwood number increases in the existence of mass and thermal buoyancies within the thermal boundary layer. Increases in thermal and mass buoyancies both assist to rise the wall temperature gradient, as seen by the data in Table 4. It is worth noting that Nusselt number decreases rapidly in case of ethanol as compared to water and Sherwood number increases rapidly for water as compared to ethanol.

| \( N_t \) | \( (\frac{Re_s}{\lambda_T})^{-1/2}Nu_x \) for Water Pr = 6.3 | \( (\frac{Re_s}{\lambda_T})^{-1/2}Nu_x \) for Ethanol Pr = 18.6 |
|----------|---------------------------------|---------------------------------|
| \( \lambda_T = 1 \) | \( \lambda_T = 2 \) | \( \lambda_M = 0.5 \) | \( \lambda_M = 0.8 \) | \( \lambda_T = 1 \) | \( \lambda_T = 2 \) | \( \lambda_M = 0.5 \) | \( \lambda_M = 0.8 \) |
| 0.1 | -0.189727 | -0.19614 | -0.19399 | -0.19109 | -0.3750 | -0.3932 | -0.37508 | -0.37487 |
| 0.2 | -0.578127 | -0.60016 | -0.58259 | -0.57955 | -0.841375 | -0.8789 | -0.84131 | -0.84102 |
| 0.3 | -0.984848 | -1.0234 | -0.99254 | -0.98640 | -1.3168 | -1.3755 | -1.31675 | -1.31633 |
| 0.4 | -1.40873 | -1.46464 | -1.41492 | -1.41047 | -1.7938 | -1.8757 | -1.79376 | -1.79326 |

| \( S_c \) | \( (\frac{Re_s}{\lambda_T})^{-1/2}Sh_x \) for Water Pr = 6.3 | \( (\frac{Re_s}{\lambda_T})^{-1/2}Sh_x \) for Ethanol Pr = 18.6 |
|----------|---------------------------------|---------------------------------|
| \( \lambda_T = 1 \) | \( \lambda_T = 2 \) | \( \lambda_M = 0.5 \) | \( \lambda_M = 0.8 \) | \( \lambda_T = 1 \) | \( \lambda_T = 2 \) | \( \lambda_M = 0.5 \) | \( \lambda_M = 0.8 \) |
| 0.1 | 1.07538 | 1.13293 | 1.06523 | 1.07133 | 1.06831 | 1.12197 | 1.05868 | 1.06376 |
| 0.3 | 1.3165 | 1.38272 | 1.30817 | 1.31299 | 1.31053 | 1.37416 | 1.30146 | 1.30673 |
| 0.5 | 1.69772 | 1.7734 | 1.69123 | 1.69479 | 1.69271 | 1.76685 | 1.68599 | 1.68965 |
| 0.7 | 2.00686 | 2.08771 | 2.00139 | 2.00424 | 2.00201 | 2.08156 | 1.99656 | 1.99935 |

4. Conclusions

This article involves the comparative analysis for water and ethanol with different study parameters. Graphs and tables have been used to examine the impact of a changing magnetic strength and a chemical reaction on the free convection movement of an electrically conducting having constant density nano liquid above an exponential expandable surface. The Buongiorno model, which is related to Brownian movement and thermophoretic distribution, is used in this work to improve the heat transmission. The following are the key findings of the recent study:

1. The fluid motion is decelerated by the increasing magnetic strength, while heat and mass buoyancy forces boost up the fluid movement, resulting in a larger momentum barrier layer.
2. Because of the Prandtl number, magnetic field intensity, and thermophoretic distribution increase fluid temperature owing to a rise in thermal opposition, in the case of ethanol this behavior is noted highly when compared to water.
3. In the existence of a magnetic strength, skin resistance reduces in the x and y directions as the magnitude of the thermal and mass convective parameters increases.
4. Increases in the thermophoresis parameter cause concentration to increase.
5. Concentration decreases as an upsurge in the concentration exponent, chemical reaction constraint, Brownian movement constraint, thermal convective constraint, and Schmidt number is noted.

6. Consistent temperature transference rate observed for water as compared to ethanol.

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**Nomenclature**

- \(u, v, w\): Velocity constituents in x, y, z direction
- \(\sigma\): Electrical conductivity
- \(\beta_T, \beta_C\): Thermal and mass expansion coefficients respectively
- \(k_f, \rho_f, \nu_f, \mu_f\): Thermal conductivity, density, kinematic viscosity and dynamic viscosity of fluid
- \(D_T, D_B\): Thermophoretic diffusion, Brownian motion
- \(\tau_{wx}, \tau_{wy}\): Wall shear stress along x and y-direction
- \(\alpha_{nf}\): Thermal diffusivity
- \(Nu_x, Sh_x\): Nusselt number, Sherwood number
- \(g\): Gravitational acceleration
- \(\beta\): Stretching ratio parameter
- \(T_w, T_\infty, C_w, C_\infty\): Temperature and concentration at surface and free stream
- \(B_0\): Magnetic field
- \(C_{fx}, C_{fy}\): Skin frictions along x and y axis
- \(\phi, T\): Particle volume fraction, temperature of fluid
- \(\langle \rho C_p \rangle_f, \langle \rho C_p \rangle_s\): Heat capacitance of fluid and nanoparticles
- \(Pr\): Prandtl number
- \(A, B, M\): Temperature, concentration exponents and Hartmann number
- \(K_c\): Chemical reaction constraint
- \(\eta, Re\): Similarity variable, Reynolds number
- \(s, f, nf, w, \infty\): Solid, fluid, nanofluid, wall free stream

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