1. Introduction

Grinding has been an important operation in several fields such as chemical, pharmaceutical, and material industries. Fine grinding has become even more important due to nanotechnology and nanomaterials. Planetary ball mills, in which rotating jars are installed on the revolving disk, generate fine powder through a high-energy process, which are known as the most powerful tools in synthesizing particles. Some non-traditional applications have emerged as encapsulation and stabilization of β-carotene, purifying multi-walled carbon nanotubes, and mechanochemical synthesis of calcium phosphates. The last two bring an old discussion: dry or wet grinding, which one is better for the process? There is no single answer and everything depends on several factors of the raw material and the applications of the product.

Some experimental studies relate grinding performance and media shape in different types of mill. In a laboratory mill, cylindrical shaped grinding media produces faster breakage rates than ball charges under the same conditions. According to Ipek et al., it might be explained due to the contact mechanism and the higher surface area of the cylindrical media. On the other hand, Kelsall et al. found that cylinder and cubes always produce fewer fines than spheres in a continuous wet ball mill. The authors explain that this difference is due to the change from point contact for spheres to a range of different types of contact for the other shapes. However, all these studies considered powder feed size of hundreds of microns.

The influence of the mean particle size (Dₜₚ) on products properties such as toughness is already well known for decades. Most studies about products obtained by grinding in a planetary ball mill just use Dₜₚ as a reference of grinding performance. However, there are other parameters of a particle distribution that may have effects on the processed product. For example, bulk densities, shrinkage, and strength increase, while radial density gradient diminishes upon increasing the amount of the finest fraction in the raw material of uniaxially die-pressed alumina refractories. Increasing the relative dispersion of the particle size distribution improves the sintering ability of silicon carbide. Particle size has been studied even in environmental issues and found as a key factor to the dustiness of the raw materials (their tendency to generate dust on handling). Moreover, choosing the suitable particle distribution width is an important aspect in the shaping form processes of ceramics. For instance, a slip casting process requires a wider distribution than dry pressing. Choosing the proper grinding media leads to the appropriate grinding product.

Zhang et al. experimentally studied the effect of the ball-to-powder ratio, size of milling balls, medium and rotation speed in the wet grinding of a planetary ball mill considering just the mean particle size concerning particle size distribution. In this manuscript, wet grindings on a planetary mill were performed in order to analyze the influence of media geometry (size and shape) on mean particle size, the width of the particle size distribution, morphology, and phase composition.

2. Materials and Methods

A planetary mill test bench with revolution radius of 150 mm has been manufactured. The equipment was designed to provide rotation-to-revolution speed ratio of -2 (where the negative sign indicates opposite directions). Such ratio
was chosen aiming greater grinding efficiency according to Mio et al. The bench was based on Brazilian Patent BR2020180676232, which project was described by Camargo et al. However, this larger planetary mill should withstand a greater load than the friction wheels would resist, gears were chosen for motion transmission, as shown in Figure 1. The central gear is attached directly to the motor flange and stands still and the rotating parts fixed in the motor shaft.

Figure 1. Mechanical Design of the planetary mill.

In order to evaluate the influence media geometry on wet grinding of a planetary mill, calcined alumina powder, considered a universal hard material reference, was ground under different conditions. The material used was a commercially pure (99.7%) Al₂O₃ powder (APC-G, ALCOA) with a median particle size equal to 4.2 micrometers.

Jars (coated with alumina) with 360 ml (Ø70 mm x h94 mm) were used. In all the tests, the jar was filled with 10 vol% of alumina powder, 23 vol% of distilled water, 33 vol% with zirconia media. In addition, Ammonium Polyacrylate was added as a deflocculant (1 wt% of the mass of the powder).

The ball filling ratio around one-third vol% was chosen according to Rosenkranz et al. which showed that it would lead to a cascading motion and most effective grinding (assuming that the ball motion is not affected by medium or mill feed). Zirconia was chosen as media due to the fact that it has a larger density (5.68 g/cm³) and fracture toughness compared to other ceramic materials, such as alumina (3.95 g/cm³) and Chen et al. showed that higher media density is beneficial to obtain finer products. Thus, zirconia balls (Ø=3 mm, Ø=5 mm and a mixture with half of each) and cylinders (Ø=5 mm x 5 mm) were used as grinding media.

Grinding in a planetary mill is a high-energy process that occurs in jars, which have a high thermal barrier (due to their ceramic coating). According to Takacs et al., jars of the planetary mill can easily exceed 200 °C. Whereas the fluid used as a solvent was water, with a limited boiling point, the temperature inside the jars has to be controlled. The internal temperature was measured after pre-set grinding times: the jar was immediately opened, a probe of a digital thermometer (MT-525, Minipa) inserted, and it was measured temperatures as high as 75 °C after 10 minutes, which was the maximum continuous operating time established. For longer grinding, operating cycles followed by pause were used until the temperature dropped close to room temperature, as suggested by Huller et al. The grinding time in each sample was 30 minutes (3 cycles) and the employed revolution was approximately 400 rpm.

The particle distributions of the raw material and ground alumina were analyzed by a scanning electron microscope. Lastly, a possible change in the phase composition was verified by X-ray powder diffraction. For these two analyzes, 5 grams of each sample were dried in the oven at 110°C for 12 hours. In order to alleviate the usual agglomeration of the drying process, each sample was subsequently submitted to 5 minutes of manual action in the mortars and pistils.

3. Results

Figure 2 shows the media geometry effect on cumulative particle size distribution: smaller media leads to smaller particle size, as seen in dry grinding. Even though smaller balls provide lower impact energy, larger balls cause agglomeration which decreases the particle size reduction. In Figure 3, it can be observed that the only sample with mono-modal curve is the ball with diameter of 3 mm while larger media provided bi-modal curves.

It is interesting to note that a mixture between balls of 3 mm and 5 mm leads to a final product very similar to the one that uses just 5 mm balls. Another interesting point is that cylinders presented a poor performance in the wet grinding of a planetary mill. On the other hand, considering the width of the particle size distribution ($W_{psd}$), that can be calculated using Equation 1, the cylinders have the narrower particle size distribution. $D_{10}$, $D_{50}$, $D_{90}$ and $W_{psd}$ are summarized in Table 1.

$$W_{psd} = (D_{90}-D_{10}) / D_{50}$$

The morphology of the initial powder and grinding samples is shown in Figure 4. Figure 4a shows the raw material. In Figures 4b, 4c, and 4d, corresponding to ground samples with spherical grinding media, the reduction of particle size is observed presenting particles below 0.5 μm and the presence of a remaining fraction of larger particles. In contrast, in Figure 4e, which represents cylindrical media, particles as large as the originals were not observed. This can be explained due to non-point contact, i.e. it preferentially breaks the larger particles that are between the contact lines of the elements. In general, agglomeration of the smaller particles is observed in the milling samples, which may have been caused by the drying process, not necessarily representing the condition of the slurry after grinding.
Figure 2. Cumulative particle size distribution: effect of media size and shape.

Figure 3. Particle size distribution: effect of media size and shape.

Table 1. Particle size distribution summary

|                          | D10 (μm) | D50 (μm) | D90 (μm) | Wpsd (μm) |
|--------------------------|----------|----------|----------|------------|
| Raw Material (Alumina APC-G) | 1.96     | 4.26     | 13.09    | 2.61       |
| Ball (Ø=3 mm)            | 0.14     | 1.08     | 2.45     | 2.14       |
| Ball (Ø=5 mm)            | 0.37     | 1.33     | 2.98     | 1.96       |
| Ball (Ø=3 mm and Ø=5 mm) | 0.31     | 1.30     | 2.86     | 1.96       |
| Cylinder (Ø=5 mm x 5 mm) | 0.28     | 2.07     | 3.61     | 1.61       |

Figure 5 shows XRD patterns of raw and ground alumina, indicating that the peaks are maintained after grinding in the planetary mill, thus not having significantly affected the crystalline structure of alumina. There was some reduction in the intensity of diffracting peaks which can be associated with internal strain and lattice distortion.

4. Discussion

When analyzing the data from the milling experiments, it is clear that a product cannot be characterized just by its mean particle size. Although much effort has been made to predict the effect of grinding parameters on the D of fabricated powders, associating them with (specific) impact energy and frequency of impacts in dry grinding, this set of experiment showed that a deeper study should be made in wet grinding, looking forward to find the relation between the grinding parameters and the final product features, such as D10, D50, D90, distribution span, and morphology.
Figure 4. Scanning electron microscope images. (a) Raw material (alumina APC-G). (b) Ball (Ø=3 mm). (c) Ball (Ø=5 mm). (d) Ball (Ø=3 and 5 mm). (b) Cylinder (Ø=5 mm x 5 mm).

Figure 5. X-ray powder diffraction of the raw material and products.
Although the planetary mill can be used for mechanochemical reactions \(^{14,22}\), the mechanical action in the processes discussed in this work was not sufficient to cause structural changes, which was expected since alpha-alumina is a stable phase.

5. Conclusions

Because of the importance that grinding in planetary mills has been reaching, the effects media geometry (size and shape) on wet grinding of a planetary ball mill were experimentally analyzed in this work. Planetary mill test benches were manufactured and calcined alumina powder (a reference hard material) was ground under different conditions and the particle distributions were analyzed by a sedigraph.

The media geometry exerts significant influence on the grinding rate. Cylindrical media provided a coarser powder with a narrower distribution. On the other hand, small balls leads to smaller particle size. The mean particle size was reduced from 4.2 μm to 1.1 μm in 30 minutes in a mill with 150 mm of revolution ratio using 360 ml jar filled with 3 mm balls. In all grindings there was no significant phase change. The experiments presented in this investigation can be used as an aid in the proper choice of grinding media or even to validate emerging models to study breakage in wet grinding.

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