Study of Flotation Parameters for Copper Recovery from Tennantite Ore

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Abstract: In the present study beneficiation of copper-pyrite ores consisting of tennantite-tetrahedrite series minerals from Southern Ural deposits were critically discussed. Intergrowth of pyrite, sphalerite, tennantite and other copper sulphides, difference in their activity and size created the considerable problems in implementation of selective flotation to obtain conditional copper and zinc concentrates. Since the demand for copper is growing constantly, the need to develop processes and technologies to treat copper resources with high level of arsenic were established. A detailed study was conducted to evaluate the effect of particle size, pH, flotation time, collector type and addition on efficiency of tennantite flotation. It was shown that maximum copper recovery of 95.3% was obtained at pH 12.3 by lime. It was suggested to grind up to 65.72% of -0.074 mm to achieve the optimum recovery of copper and zinc.

Keywords: Refractory Copper-pyrite Ores, Flotation, Tennantite, Arsenic, Recovery

1. Introduction

The treatment processes for the beneficiation of copper-pyrite ores consisting of tennantite-tetrahedrite series minerals along with chalcopyrite, pyrite and sphalerite are generally complex. Tetrahedrite-tennantite minerals generally occur as fine anhedral grains intermixed with or in grains of galena, sphalerite, chalcopyrite, pyrite and other sulfosalts. Members of tennantite-tetrahedrite series minerals known as fahlerz minerals, ranging from tetrahedrite, Cu₁₂Sb₄S₁₃, to tennantite, Cu₁₂As₄S₁₃, are derivatives based upon the sphalerite structure [1]-[3]. One-fourth of the metal atom sites are occupied by As, Sb and rarely Bi. The copper atoms in the pure end members are split equally in two types of sites, one of which is a four-coordinated nearly tetrahedral site, and the other a three-coordinated triangular site [4]. It has been established that tetrahedrite is accommodated in copper-lead-zinc deposits and that tennantite preferentially occurs in ores rich by copper [5], [6].

Several copper-pyrite deposits have been found in Southern Urals, Russia. It differs from other similar copper-pyrite ores by thin mutual "germinating" minerals which create considerable complexities in enrichment. For the majority of these deposits arsenic content in the ore is less than 0.3 %, but a group of deposits as Uzelginskoye, Uchalinskoye, Mezhozernoye can be characterized by higher content of arsenic (up to 0.8-1 %) [7]. Arsenic is a hazardous pollutant and most of the mining companies avoid to exploit these deposits because arsenic can become a serious environmental problem and reduce the economic value of copper resources. On the other hand since the demand for copper is growing constantly, the need to develop processes and technologies to treat copper resources from additional sources such as mine tailings, low grade deposits, industrial wastes and deposits with high impurity levels such as As and Sb will continue to increase [4].

Flotation mechanisms of tennantite-tetrahedrite series minerals are not well understood since there are limited studies involved [9]-[10]. Laboratory and plant practices showed that tennantite and tetrahedrite do not respond well to flotation using xanthate as a collector. Tetrahedrite floats well with acrylmine and mercaptan type of collectors at a pH value between 8 and 10 [11]. Selective separation of sulphide minerals can be achieved using a variety of collectors and modifiers to adjust surface properties [10],[12]-[14]. In practice, when treating complex sulphide ores, the combination of depressants is common, especially when separation of several valuable minerals is required for better selectivity. According to the relevant studies conducting on this issue it is evident that the most troublesome question for researchers remains the discovery the selective reagents for tennantite flotation optimization. The knowledge generated in these studies is extremely helpful in further selection of collectors with desired properties as well as in designing of new reagents schemes.

2. Research Objectives

The objectives of the present study are tennantite and chalcopyrite and butyl xanthate as a collector which are used in practice for copper flotation from Cu-Zn-pyrite ores of...
several deposits treating at Uchaly Mining and Concentration Complex (Southern Urals, Russia). Lime and soda ash are used as modifiers for estimation the effectiveness of flotation operation. Butyl xanthate has been established as a standard reagent for comparison the selectivity of new reagents studied.

Table 1 contains the information about sample ore characteristics related to different types of deposits in Southern Urals where 1- Uchalinskaya Cu-Zn ore; 2- Uzelginskaya lower level ore; 3- Uzelginskaya upper level ore; 4- Uzelginskaya Cu-Zn lower level ore; 5- Uzelginskaya Cu-Zn upper level ore; 6- Molodezhnaya Cu-Zn ore; 7- Ozernaya Cu ore.

| № | Head assay, % | Cu | Zn | S | Fe | As | Sb |
|---|----------------|---|----|---|----|----|----|
| 1 | 1,09           | 3,29 | 41,1 | 30,78 | 0,13 | 0,005 |
| 2 | 1,30           | 2,76 | 21,5 | 32,05 | 0,05 | NA |
| 3 | 2,77           | 0,52 | 49,4 | 42,45 | 0,50 | 0,030 |
| 4 | 1,30           | 2,76 | 21,5 | 32,05 | 0,05 | NA |
| 5 | 1,49           | 2,22 | 45,1 | 38,49 | 0,55 | 0,057 |
| 6 | 1,24           | 1,59 | 28,1 | 25,87 | 0,25 | 0,013 |
| 7 | 2,03           | 0,26 | 25,7 | 36,62 | 0,12 | NA |

Table 2 shows the names and chemical formulas of collectors studied.

| Collectors                     | Abbreviation | Chemical formula |
|-------------------------------|--------------|------------------|
| Butyl Xanthate                | BX           | C₅H₉OS₂K         |
| Di-isobutyl dithiophosphinate | AERO 3418A   | C₉H₁₈NOSNa       |
| Allyl propylthiono carbamate  | AERO 5100    | C₁₇H₂₆NOSNa      |

3. Methods

3.1 Flotation Tests

In the present study laboratory flotation experiments were performed using a mineral separation (MS) type laboratory flotation equipment.

4. Results and Discussion

4.1. Ore mineralogy and the occurrence of tennantite

The mineralized zones of Southern Urals deposits generally correspond with the ore types which are observed: pyrite ores with significant amounts of interstitial chalcopyrite and minor amounts of sphalerite, sulfosalts, and the fahlerz minerals; ores with subequal amounts of dark sphalerite and pyrite with chalcopyrite, sulfosalts, and fahlerz minerals; disseminated ore-dispersed pyrite with sphalerite, chalcopyrite, and tennantite in host silicates. The tennantite-tetrahedrite series (fahlerz minerals) occur in all ore types at these deposits but is much more abundant in ores at Uzelginskoye deposit, some samples of which contain 70% of copper in tennantite form [6].

Tennantite refers to the sulfosalts with complex crystal structure. The lattice contains anions [AsS₃]³⁻ similar to [SO₄]²⁻ which easily can be oxidized. Tennantite as well as tetrahedrite is the second mineral after pyrite which can produce the great number of [SO₄]²⁻ by oxidation at pH 10.7 [15].

Tennantite has less hardness and higher fragility comparing to chalcopyrite which causes to easy over grinding and declining in comminution. The major feature of tennantite mineralogy in such deposits is isomorphism effecting on flotation properties. The fahlerz minerals of tennantite series in Southern Urals deposits are represented by two morphological variations of tennantite. Rounded and elongated tennantite 1 occurs in middle-grained pyrite, often with association of chalcopyrite , with the size range of 10-50 microns. Tennantite 2 prevails in tennantite-containing pyrite ores of Uzelginskoye deposit and occurs in association with chalcopyrite and sphalerite , bornite , and sometimes galena , in the form of veins and nests in aggregates of fine-grained pyrite , performs interstitial 100-500 microns by size [16]. Intergrowth of pyrite, sphalerite, tennantite and other copper sulphides, difference in their activity and size create the considerable problems in implementation of selective flotation, obtaining conditional copper and zinc concentrates.

Despite several of studies that have been done related to this issue, effective selective flotation of tennantite ores is still the subject to investigation.

4.2. Effect of particle size distribution on copper recovery

Chalcopyrite and tennantite ore samples were received from the mine site. The chemical analysis of samples is shown in Table 3.

| Sample          | Head assay, % |
|-----------------|---------------|
| Chalcopyrite type of ore | 1,57 | 0,09 |
| Tennantite type of ore    | 5,55 | 1,75 |

The major sulphides detected by X-ray diffraction were tennantite (88,3%), chalcopyrite (5,8 %) in the tennantite ore sample. The small amount of pyrite, sphalerite were also detected. The tennantite and chalcopyrite ore samples were ground at five different grinding times 5,10,15,20 and 25 minutes. The percentage of particles below 74 microns by size was determined for 5,10,15,20 and 25 minutes, respectively. For flotation tests different conditions were explored in order to search for maximum recovery of copper. The aim of these flotation tests was to obtain the concentrate with a high grade of As and high recovery of Cu. It has been established that butyl xanthate (BX) was uses as a collector at the dosage of 100 g/t , the optimum flotation time was 16 min. Lime was applied as a modifier with residual concentration of 280g/m³. The concentrate and tailings were submitted for chemical analysis. Figure 1 shows the...
relationship between the recovery of copper and particle size. In this study the percentage of particles below 0.074 mm by size was established as a parameter to estimate particle size distribution.

![Figure 1: Recovery of copper as a function of particle size](image)

Figure 1: Recovery of copper as a function of particle size

Obviously the grinding performance significantly affects further separation results. Significant reduction in grinding size would be necessary to achieve good liberation. However, the fineness of grinding depends on the variation in hardness of minerals within the ore. Finer grinding has been expected to improve selectivity for tennantite. It has been established that the increase in the percentage of size in the feed less than 0.074 mm up to 65.72% has produced sufficient copper sulphide liberation and the recovery has increased up to the maximum value of 85%. The further finer grinding up to 99.8% of -0.074 mm led to decrease in copper recovery by about 15%.

Figure 2 represents the relationship between the grade of As and the particle size.

![Figure 2: Grade of As as a function of particle size](image)

Figure 2: Grade of As as a function of particle size

It has been shown that maximum grade of As (3.5%) was achieved at 65.72% of -0.074 mm size. The finer grinding the less is the grade of As in concentrate which lead to desliming and more loss of As in tailings.

4.3. Effect of pH modifiers on ore flotation

In common practice the regulating reagents are using to control the adsorption of collectors in flotation operation. In order to depress zinc and iron sulfides from copper-pyrite ores, flotation process is conducted in an alkaline medium, which is created by pH modifiers. Discovery of optimum type and dosage of a modifier is one of effective way to enhance the flotation performance. The change in pH level influences on mineral surface, behavior of a collector and soluble salts in the pulp. There is the competition between soluble ions in pulp and a collector to adsorb on the mineral surface. It has been established that each pH reflects on different concentration of collector ions leading to maximum recovery of copper [15].

Lime is normally used as a pH modifier in sulphide flotation to depress pyrite. In this case, pyrite in an alkaline solution forms colloidal hydrated iron oxide Fe(OH)₃ on the pyrite surface, thus preventing collector adsorption [11].

In present study two modifiers were used to depress pyrite – soda ash and lime. Experimental results for tennantite and chalcopyrite flotation obtained in the range of pH are shown in Figure 3 and 4, respectively.

![Figure 3: Recovery of copper as a function of pH with lime and soda ash as depressants for tennantite ore](image)

Figure 3: Recovery of copper as a function of pH with lime and soda ash as depressants for tennantite ore

![Figure 4: Recovery of copper as a function of pH with lime and soda ash as depressants for chalcopyrite ore](image)

Figure 4: Recovery of copper as a function of pH with lime and soda ash as depressants for chalcopyrite ore

It had been established that soda ash as a pH modifier did not work successfully for tennantite sample. Maximum recovery of copper about 55 % was reached giving the great

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loss of copper in tailings. However, the application of lime indicated that recovery of copper increased significantly to 95.3 % for pH 12.3 with the residual concentration of lime of 532 g/m³. The later increase in lime dosage led to depression of tennantite and decrease in copper recovery up to 90 %. Copper recovery of around 97 % with both soda ash and lime was achieved from chalcopryite ore sample, indicating that chalcopryite was easily floatable at wide range of pH without visible depression. According to results obtained it is evident that the type of the modifier plays the significant role on tennantite flotation. The optimum flotation was reached with pH range of 10.8-12.3 with lime.

4.4. Flotation Kinetics

There is a large number of approaches to choose the flotation reagents with desirable properties as well as to design new reagents [17]. However, it was established that available collectors for tennantite flotation showed the low level of selectivity. Therefore this study was aimed to investigate the performance of prospective reagents for tennantite. Flotation tests were carried out to obtain the optimum results with the aid of three collectors: BX, AEROPHINE 3418A and AERO 5100. Estimation of reagent schemes was conducted by comparison of relationship between the rate constant and retention time of flotation. It is known that flotation kinetics is based on assumption that the rate of flotation can be considered proportional to flotable amount of minerals.

Flotation kinetics has been taken into account using the equation proposed by Beloglazov (1) with the assumption that all particles have the same flotability.

\[ \frac{1}{1 - \varepsilon} = K \]

Where K – rate constant, \(\varepsilon\) – recovery of copper.

Results obtained by kinetic calculations present in Figure 5.

![Figure 5: Kinetics of flotation of tennantite ore sample with BX, AEROPHINE 3418A and AERO 5100](image)

It was established that tennantite flotation by BX showed the increase in rate by tenth min. Tennantite was successfully concentrated during 13 min by addition of AERO 5100 then the rate of flotation was decreased not considerably. AEROPHINE 3418A effected on flotation only the first four min and the further increase in rate was not considered. It was evident that AERO 5100 and AEROPHINE 3418A started acting at the beginning of flotation operation.

According to studies conducted these reagents can be proposed as prospective collectors for tennantite flotation.

5. Future Scope and Implications of the Study

Taking into account the large number of parameters influencing on tennantite flotation as well as its mineralogy the real flotation process is considered quite complicated. Viewed from the latter perspective it seems that deeper studies should be conducted revealing the mechanism of adsorption of reagents on the mineral surface of tennantite. Knowledge generating in these studies can be useful for greater understanding of current problems and help in improvement in product quality. Nevertheless the way to enhance the flotation performance of tennantite is still under investigation.

6. Conclusions

Copper-pyrite ores consisting of tennantite-tetrahedrite series minerals from Southern Urals deposits, Russia are characterized by thin mutual "germinating" minerals which create considerable complexity in enrichment. The major feature of tennantite mineralogy in such deposits is isomorphism effecting on flotation properties. Studies conducted to evaluate the effect of particle size, pH, flotation time, collector type and addition on efficiency of tennantite flotation showed that maximum copper recovery of 95.3% was obtained at pH 12.3 by lime. It was suggested to grind up to 65.72% of -0.074 mm to achieve the optimum recovery of copper and high grade of arsenic in concentrate. Overgrinding led to desliming and more loss of As in tailings. It was established that allylalkylthionocarbamates and dialkyldithiophosphinates could be considered as prospective reagents for tennantite ore flotation.

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Peter Solozhenkin is an outstanding scientist, who received the MS degree in Mineral Processing Engineering from the Irkutsk Mining Metallurgical Institute in 1957. During 1975-1989 he was a Vice-President of the Tajik Academy of Science. Now he is working in IPCON, Russia. His research interests are devoted to Complex Exploitation of Mineral Resources and Computer Modeling of Flotation Processes. He is the author of 17 books, several hundreds of papers, patents and articles.

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