Novel synthesis of porous Mg scaffold as a reactive containment vessel for LiBH₄†

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A novel porous Mg scaffold was synthesised and melt-infiltrated with LiBH₄ to simultaneously act as both a confining framework and a destabilising agent for H₂ release from LiBH₄. This porous Mg scaffold was synthesised by sintering a pellet of NaMgH₃ at 450 °C under dynamic vacuum. During the sintering process the multi-metal hydride, decomposed to Mg metal and molten Na. The vacuum applied in combination with the applied sintering temperature, created the ideal conditions for the Na to vaporise and to gradually exit the pellet. The pores of the scaffold were created by the removal of the H₂ and Na from the body of the NaMgH₃ pellet. The specific surface area of the porous Mg scaffold was determined by the Brunauer–Emmett–Teller (BET) method and from Small-Angle X-ray Scattering (SAXS) measurements, which was 26.1 and 39.5 m² g⁻¹ respectively. The pore size distribution was analysed using the Barrett–Joyner–Halenda (BJH) method which revealed that the majority of the pores were macropores, with only a small amount of mesopores present in the scaffold. The melt-infiltrated LiBH₄ was highly dispersed in the porous scaffold according to the morphological observation carried out by a Scanning Electron Microscope (SEM) and also catalysed the formation of MgH₂ as seen from the X-ray diffraction (XRD) patterns of the samples after the infiltration process. Temperature Programmed Desorption (TPD) experiments, which were conducted under various H₂ backpressures, revealed that the melt-infiltrated LiBH₄ samples exhibited a H₂ desorption onset temperature (Tₕ₀) at 100 °C which is 250 °C lower than the bulk 2LiBH₄/MgH₂ composite. Moreover, the LiH formed during the decomposition of the LiBH₄ was itself observed to fully decompose at 550 °C. The as-synthesised porous Mg scaffold acted as a reactive containment vessel for LiBH₄ which not only confined the complex metal hydride but also destabilised it by significantly reducing the H₂ desorption temperature down to 100 °C.

1. Introduction

Over the last few years metal hydrides and complex metal hydrides have been extensively investigated as hydrogen storage materials in order to be used in fuel cell technology, applied in transportation. A set of targets, determined by the U.S. Department of Energy suggests that a material system should contain at least 5.5 wt% H₂ to be deemed as suitable for application. LiBH₄ is one such material owing to its high theoretical gravimetric hydrogen storage density of 18.5 wt%. However, one of its greatest limitations as a prospective hydrogen storage medium is that it decomposes at relatively high temperatures (~350 °C) according to eqn (1). The LiH decomposition product is extremely stable and does not decompose until at least 910 °C under 1 bar of H₂ back-pressure. Hence, LiBH₄ when used at lower temperatures (<910 °C) has a practical gravimetric hydrogen storage density of 13.8 wt%. Reversibility of LiBH₄ is also problematic, as temperatures of above 600 °C and 350 bar of hydrogen pressure are required for reabsorption. Overall, if the thermal stability and reversibility problems, were overcome, LiBH₄ would be a very promising material.

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A very common approach that has been extensively applied, in order to decrease the hydrogen desorption temperatures of LiBH₄ is to thermodynamically destabilise it with a second phase such as MgH₂ or Mg₁₂. It is shown that when MgH₂ or Mg is combined with LiBH₄, a new decomposition pathway is created by forming MgB₂ (eqn (2) and (3)). It has been proven...
that MgB$_2$ is thermodynamically more stable in comparison to Mg or B and acts as the destabilising agent for the 2LiBH$_4$ + MgH$_2$ or 2LiBH$_4$ + Mg system.$^{20}$

$$2\text{LiBH}_4 + \text{MgH}_2 \rightarrow 2\text{LiBH}_4 + \text{Mg} + \text{H}_2 \rightarrow 2\text{LiH} + \text{MgB}_2 + 4\text{H}_2 \quad (2)$$

$$2\text{LiBH}_4 + \text{Mg} \rightarrow 2\text{LiH} + \text{MgB}_2 + 3\text{H}_2 \quad (3)$$

When MgH$_3$ is used as the second phase added to LiBH$_4$, two chemical reactions are observed during desorption. First, MgH$_2$ decomposes into Mg and then LiBH$_4$ decomposes to form LiH and MgB$_2$ as seen in eqn (2). The formation of MgB$_2$ only depends on the reactivity between B and metallic Mg, therefore a two reaction step always occurs.$^{30}$ Whereas, when Mg is used as a second phase, the decomposition pathway of LiBH$_4$ occurs in one single chemical reaction (eqn (3)). These decomposition pathways can be manipulated according to the temperature and H$_2$ backpressures applied during the temperature programed desorption experiments.$^{16,17}$

Additional studies have been conducted in order to further reduce the desorption temperature of hydrogen, hasten the kinetics and improve the reversibility of the 2LiBH$_4$–Mg or 2LiBH$_4$–MgH$_2$ system by adding catalyst precursors such as metal salts, metal organic compounds or metal oxides.$^{15,20,21}$

Another approach found in the literature, widely used in order to enhance the kinetics of the 2LiBH$_4$–MgH$_2$ system, is to nanoconfine the bulk composite into a porous scaffold. The reduction of the particle size down to the nanoscale ensures shorter diffusion distances for hydrogen and other light elements within the nanostructure. Hence, the hydrogen desorption and absorption rates improve in comparison to the bulk material.$^{23-26}$

Even though many efforts have been made in order to reduce the H$_2$ desorption temperature of the 2LiBH$_4$–Mg and 2LiBH$_4$–MgH$_2$ system, as demonstrated in the literature, no studies have reported any H$_2$ desorption detected below 140 °C in these bulk or catalysed systems. Moreover, even though the nanoconfined as well as the catalysed nanoconfined 2LiBH$_4$–MgH$_2$ systems exhibited improved kinetics and reversibility in comparison to the bulk one, the values of the desorbed H$_2$ (wt% of H$_2$) were poor and hence do not meet the targets set by the U.S. Department of Energy.$^6$ Furthermore, the carbon aerogels used as scaffolds or activated carbons typically contain between 4 wt% and 14 wt% of oxygen.$^{27-29}$ Therefore, an oxidation reaction between the infiltrated metal hydride system and the oxygen from the scaffold is inevitable and causes H$_2$ capacity loss of the complex metal hydride.

A new type of porous scaffolds have recently made a significant appearance in the literature called porous metal scaffolds. These type of scaffolds have been tested for battery, fuel-cell, energy and catalytic applications due to their robustness.$^{30-31}$

In this study, we report a novel method for the synthesis of a porous Mg scaffold using NaMgH$_3$ as a starting material. The hydride was pressed into a pellet and sintered under dynamic vacuum in order to remove H$_2$ and Na. The morphology of the Mg scaffold was investigated by N$_2$ adsorption/desorption and Small Angle X-ray scattering (SAXS) measurements as well as by a Scanning Electron Microscope (SEM) which revealed an open pore network that consisted mainly of macropores and only a small number of mesopores. LiBH$_4$ was melt-infiltrated into the porous metal scaffold and catalysed the formation of MgH$_2$ as seen from the X-ray diffraction patterns of the melt-infiltrated samples. Scanning Electron Microscopy revealed that the melt-infiltrated LiBH$_4$ was highly dispersed. All melt-infiltrated samples exhibited a H$_2$ desorption onset temperature ($T_{des}$) at 100 °C which is 250 °C lower than the bulk LiBH$_4$ and 330 °C lower than the bulk 2LiBH$_4$/MgH$_2$ composite. Furthermore, the LiBH$_4$ of the melt-infiltrated samples was completely decomposed at 550 °C (under 1.5–2.7 bar of H$_2$ backpressure) showing no LiH present in the samples even though LiH is known to decompose above 910 °C under 1 bar of H$_2$ backpressure or completely decompose to form LiMg alloys when vacuum is applied at 560 °C. The porous Mg scaffold acted as a reactive containment vessel for LiBH$_4$ by simultaneously destabilising and confining it. These novel hydrogen storage composite materials exhibited both low H$_2$ desorption temperatures and high values of experimental desorbed H$_2$ which make them promising candidates for on-board hydrogen storage in vehicles run by a fuel cells.

2. Experimental details

2.1 Sample preparation

All chemicals used for the synthesis were sensitive to both air and moisture. Therefore, all sample preparation and handling was performed using an Ar glovebox with O$_2$ and H$_2$O less than 1 ppm to avoid sample contamination.

NaMgH$_3$ was synthesised by ball milling NaH (Sigma Aldrich, 95%) and MgH$_2$ (Alfa Aesar, 98%) in a 1 : 1 molar ratio under an Ar atmosphere at room temperature using an Across International Planetary Ball Mill (PO-N04) employing stainless steel vials. A ball to powder mass ratio of 30 : 1 was applied by using the same number of 10 mm and 6 mm diameter stainless steel balls. The rotational speed was 350 rpm with a total milling time of 4 hours. The vials changed rotation every 15 min with a 5 min pause between each rotation. The final product was then annealed overnight at 300 °C under 50 bar of H$_2$.

The porous Mg scaffold was synthesised by pressing NaMgH$_3$ into a pellet using an 8 mm stainless steel die under a 2.5 ton load. The NaMgH$_3$ was loaded into the die inside the glovebox and then placed into a sealable plastic bag that was connected, via plastic tubing, to a push-fit valve. The bag was then removed from the glovebox and connect to vacuum before pressing. The resulting pellets were typically pressed to 70% of the crystal density of NaMgH$_3$, were ~1 mm in height and weighed 0.1 g. After disconnecting the vacuum line, the die was immediately returned to the glovebox where the pellets were removed from the die and transferred to steel sample cells and lastly sintered for 3 hours under dynamic vacuum at 450 °C using a Labec VTF 80/12 tube furnace. The ramping rate applied was 5 °C min$^-1$ and after the 3 hours of sintering time the sample was left to cool to room temperature. After removal of Na and H$_2$ by the sintering process, all pellets retained the
shape and size of the initial NaMgH₃ pellet. Using an initial H₂ backpressure of ~60 bar to prevent decomposition, various weight percentages of LiBH₄ (Sigma Aldrich ≥ 90%) were melt-infiltrated into the porous Mg scaffold using a stainless steel reactor heated to 300 °C (ΔT = 5 °C min⁻¹). The samples were held at 300 °C for 30 minutes with a final backpressure of H₂ in the reactor reaching ~70 bar H₂. The samples were then cooled to room temperature. In total, six different weight percentages of LiBH₄ (12.78, 22.50, 26.13, 32.55, 33.95 and 35.05 wt%) were melt-infiltrated into the porous Mg scaffolds. All samples were in a pellet form unless described otherwise. Bulk LiBH₄ and LiBH₄/MgH₂ with a 2 : 1 molar ratio were used as reference materials. Bulk 2LiBH₄:MgH₂ molar ratio and then to the SEM chamber.

2.2 Sample characterisation

Powder X-ray diffraction (XRD) was used for the phase analysis and phase observations of all samples utilising a Bruker D8 Advanced Diffractometer with CuKα radiation. The measured 2θ range (15–80°) was scanned using a 0.03° step size at 1.6 s per step, a rotational speed of 30 rpm and a 0.3° divergence slit. The accelerating voltage and applied current were 40 kV and 40 mA, respectively. Phase identification was accomplished by the EVA software (by Bruker) that uses as a database the Powder Diffraction Files (PDF) (International Centre for Diffraction Data). The low background Si wafer XRD sample holders were used with a poly(methylmethacrylate) (PMMA) airtight hemispherical dome to prevent oxygen/moisture contamination during data collection. The PMMA airtight dome results in a broad hump in XRD patterns centred at ~20° 2θ. Due to the specimen mounting, all samples are ~1 mm higher than the centre of the goniometer, resulting in a 2θ offset to all peak positions. In order to investigate the formation of MgB₂ in the infiltrated samples, Rietveld refinement was conducted using TOPAS Ver.5.34,35

The specific surface area and the porosity of the Mg scaffold was analysed by nitrogen (N₂) adsorption/desorption measurements performed at 77 K using a Micromeritics ASAP 3020 system (Micromeritics, Norcross, GA, USA). The specific surface area of the scaffold was calculated from the N₂ adsorption data, at relative pressures between 0.05 and 0.30, by employing the Brunauer–Emmett–Teller (BET) multi-point method.36 The pore size distributions and volumes in the macro- (>50 nm) and meso-range (2–50 nm) were calculated using the Barrett–Joyner–Halenda (BJH) method from the desorption branch of the isotherm.37

The specific surface area was also investigated by Small-Angle X-ray Scattering (SAXS) with measurements conducted at the Australian Synchrotron. The measured intensities were put onto an absolute scale by use of a glassy carbon standard, scaled by the specimen thickness,38 and an empty capillary subtracted as background. The scattering pattern was modelled with the unified model39 in Irena,40 and the Porod41 slope extracted for the low and mid-q regions. The unified model is applied in order to describe scattering from complex systems that contain multiple levels of related structural features. The extracted Porod slope for the low and mid-q regions provides information about the size and shape of the scattering particles, in this case the pores and their correlations. The specific surface area, σ(r), was calculated following the approach of Hurd (eqn (4)) with the size of the probe used (r) was 21 Å.42 This value of r is the transition size for surface fractals to Porod scattering.42

σ(r) = \frac{S(r)}{V_{p0}} = σ_s r^{2–D} \tag{4} \]

S(r) is the area of fractal surface and is equal to S(r) = S_0 r^{2–D}, where S_0 is a sample-dependent prefactor, D is the surface fractal dimension, V is the volume under consideration and ρ₀ is the density of the Mg.

σ_s which was calculated using eqn (5), as seen bellow.

σ_s = \lim_{q \to \infty} \frac{|q^{D–1} F(q)|}{\pi F(D)(\Delta p) \rho_0} \tag{5} \]

where, q is the scattering vector, q = (4π/λ)sin(θ/2) (λ is the wavelength of the radiation in the scattering medium and θ is the scattering angle), lim( ) denotes the largest q limit and F(D) = {Γ(5 – D)sin[(3 – D)π/2)] / (3 – D)}, where Γ is the gamma function.

Morphological observations were carried out with a Zeiss Neon 40EsB (Zeiss, Germany) scanning electron microscope (SEM). Specimens were prepared by placing an extracted piece from the inner centre of the pellet onto carbon tape before coating them with a 3 nm layer of platinum to produce a conductive layer and reduce charging during DEM data collection. The exposure of the samples to air was minimised by using a custom made ante chamber in which the specimens were transferred from the glovebox to the coating instrument and then to the SEM chamber.

Temperature Programmed Desorption (TPD) measurements were undertaken on a computer controlled Sieverts/volumetric apparatus.43 The sample temperature and pressure was recorded every 30 s using a K-type thermocouple with a calibrated accuracy of 0.1 °C at 419 °C and a digital pressure transducer (Rosemount 3051S) with a precision/accuracy of 14 mbar. Hydrogen desorption data was obtained in the temperature...
range from room temperature to 550 °C with a ramping rate of 5 °C min⁻¹. The temperature was then kept isothermal at 550 °C for 4 hours. Four TPD measurements were applied for the LiBH₄ melt-infiltrated samples under 0, 1, 2 and 3.4 bar of H₂ back-pressure, respectively. Whereas, TPD experiments for the bulk samples were applied under 0 bar of H₂ backpressure.

3. Results and discussion

3.1 Initial phase analysis

The X-ray diffraction pattern of the as-prepared porous Mg scaffold is presented in Fig. 1(a). It can be seen that the NaMgH₃ was completely decomposed to Mg (JCPD 35-0821) after the sintering process. According to the literature NaMgH₃ decomposes in two reaction steps as presented below.⁴⁴-⁴⁶

\[
\text{NaMgH}_3 \rightarrow \text{NaH} + \text{Mg} + \text{H}_2 \quad (6)
\]

\[
\text{NaH} + \text{Mg} \rightarrow \text{Na(l)} + \text{Mg} + _2\text{H}_2 \quad (7)
\]

The first reaction step (eqn (6)) takes place at 371 °C at 1 bar of H₂ back pressure.⁴⁴ It is expected that when dynamic vacuum is applied, this reaction will take place at lower temperature than 371 °C. According to the literature eqn (7) occurs at 427 °C at 1 bar of H₂ back pressure⁴⁸ in which NaH decomposes to Na metal and H₂ (eqn (5)).⁴⁹-⁵³ Na has a vapour pressure of 0.001 bar when it is in a molten state at 450 °C.⁵⁴,⁵⁵ Hence, the vacuum applied during the sintering process, ~1.33 × 10⁻⁵ bar, was low enough in order for the molten Na to be vapourised and removed from the main body of the pellet. The Na vapour was then captured in a cooler part of the reactor with steel wool.

The mass of the pellet on average after sintering was 1.9% higher than the theoretical value calculated by assuming the Na and H₂ were completely removed from the initial NaMgH₃ pellet. This difference in the mass values may be due to the fact that the molten Na was not entirely removed from the initial pellet, even though diffraction peaks attributable to metallic Na are not present in Fig. 1 or due to the fact that the sample is not entirely pure as the starting material (NaMgH₃) contains impurities. The non-presence of Na peaks in Fig. 1 may be due to the fact that it is in low quantity, therefore not detectable by X-ray diffraction or/and it is in a nanocrystalline phase. The broad peaks that correspond to MgO (JCPD 45-0946) are due to the impurities from the starting material.⁴⁴

An obvious concern was that the porous Mg will form MgH₂ under the temperature and H₂ pressure required for the melt-infiltration of LiBH₄. Thus, in order to confirm that the porous Mg scaffold will not form MgH₂ while the melt-infiltration conditions of LiBH₄ are applied (300 °C, initial 60 bar H₃), a blank infiltration test was carried out. The diffraction pattern of the porous Mg scaffold after the blank infiltration is presented in Fig. 1(b). No diffraction peaks of MgH₂ were present. In order to further investigate that there is no formation of MgH₂ also in the inner parts of the porous Mg scaffold away from its surface, the sample was crushed into a powder and further analysed (Fig. 1(c)). No diffraction peaks of MgH₂ were present in this pattern either. According to Bogdanović et al. in order to rehydrogenate a sintered Mg sample, high temperatures (450–500 °C) and pressures (100–110 bar H₂) are required.⁴⁶ Thus, the infiltration conditions applied did not kinetically favour the formation of MgH₂. Moreover, the formation of MgH₂ would have resulted in a volume expansion of the Mg pellet due to its transformation to MgH₂. This would have resulted in the disintegration/decrepitation of the porous Mg scaffold. Such observation was not noted after the blank infiltration test. Therefore, the structural integrity of the porous Mg scaffold acted as an initial confirmation of the non-formation of MgH₂. Diffraction peaks that correspond to Na oxide and NaOH (JCPD 01-075-0642) which are present in both patterns Fig. 1(b and c) are impurities from the starting material (NaMgH₃).⁴⁴

Fig. 2 shows the diffraction patterns of the melt-infiltrated samples in a pellet form with different wt% of LiBH₄. Fig. 2(a)
and b) represent the diffraction pattern of a pellet with 12.78 and 22.50 wt% of infiltrated LiBH4 respectively. Only peaks that correspond to Mg and MgO are present in Fig. 2(a). The lack of LiBH4 peaks in both Fig. 2(a) and (b) indicates that the complex metal hydride has penetrated the surface of the scaffold during the infiltration process and has occupied the inner pores of the scaffold or that it is present at the surface of the pellet that it is either amorphous or nanocrystalline. In Fig. 2(b) small diffraction peaks of MgH2 are present. The XRD pattern of the sample with the highest wt% of infiltrated LiBH4 (32.55 wt%) exhibits diffraction peaks that correspond to LiBH4 (JCPD 04-011-3748), NaBH4 (JCPD 04-012-3346), MgH2 (JCPD 12-0697) and MgB2 (JCPD 04-010-6469). The LiBH4 that has been infiltrated in this sample is close to the maximum amount that can be infiltrated (35.68 wt% of LiBH4) without exceeding the pore volume of the scaffold, (the value of which is mentioned in the pore analysis section of the manuscript). Thus, the concentration of LiBH4 is high enough at the surface to be observed with X-ray diffraction. The formation of NaBH4 is due to the partial reaction of residual Na with the LiBH4 at high temperatures. MgB2 is present either due to the partly decomposition of the complex metal hydride during the infiltration process, even though the appropriate pressure of H2 was applied, in order to avoid the decomposition reaction, or that the H2 backpressure was not high enough to stop the reaction between LiBH4 and Mg to form MgB2. Lastly, even though there was no MgH2 formation observed during the blank infiltration process of the Mg scaffold, MgH2 is present in Fig. 2(c). This comes in contrast to the previous observation, suggesting that LiBH4 acts as a catalyst for the formation of MgH2 during the melt-infiltration process.

In order to compare the surface composition of the infiltrated pellets with their interior, XRD patterns were obtained from the same samples after they were crushed into a powder (Fig. 3). The XRD pattern of PMg13, Fig. 3(a), shows only Mg and MgO diffraction peaks as the amount of infiltrated LiBH4 (12.78 wt%) and its low X-ray scattering power make it difficult to detect. Diffraction peaks of LiBH4, MgH2, and NaBH4 are present in samples PMg23 and PMg33 (Fig. 3(a and b)). The XRD pattern of the crushed sample PMg33 has been analysed by the Rietveld refinement method in order to investigate the formation of MgB2, as MgO and MgB2 have overlapping peaks at 2θ equal to ~43° (Fig. S1†). Moreover, in order to investigate the formation of MgH2 of the melt-infiltrated samples, an X-ray diffraction pattern (Fig. 3(d)) of a crushed Mg pellet that was melt-infiltrated (at 300 °C under 60 bar H2) with LiBH4 in a 2 : 1 molar ratio of LiBH4:Mg was obtained. Diffraction peaks of LiBH4 and NaBH4 are present in this particular sample (Fig. 3(d)) but no formation of MgH2 is evident in the same sample. This observation implies that the formation of MgH2 only occurs due to the intimate contact between porous Mg and the infiltrated LiBH4 and that a 2 : 1 molar ratio of LiBH4:Mg is insufficient for LiBH4 to act as a catalyst for the hydriding of Mg.

3.2 Pore analysis of Mg scaffold

The N2 adsorption/desorption isotherms of the as-prepared porous Mg scaffold is presented in Fig. 4(a). The isotherms belong to a type II with a H3 type hysteresis loop which is associated with samples having large mesoporous and macroporous. The isotherms show no knee at low relative pressures that indicates an extremely weak adsorbate–adsorbent interaction that is representative for samples with no micropores present. In Fig. 4(c) the pore size distribution of the scaffold is presented. It can be seen that the pores present in the scaffold are polydisperse. This observation is in agreement with the SEM micrographs (Fig. 6(a and b)) and the possible reasons for this existing variability is mentioned in more details in the SEM section of this manuscript. It is noticeable that pores with diameters ranging from 1.7 to 3.6 nm form the larger proportion, whereas larger pores ranging between 28–45 nm in diameter have a smaller proportion in the scaffold as a whole. The total pore volume of the scaffold is 1.25 cm3 g−1, including the volume of the voids which were created during the compaction of the starting powder (NaMgH3) into a pellet and it is equal to ~0.42 cm3 g−1. This volume was calculated using the crystal density of NaMgH3 and also the physical (bulk) density of the pellet derived from its physical dimensions. The volume due to the micropores and mesopores with diameter within the range of 1.7–48 nm as calculated from the BJH method (Table 2) is equal to 0.06 cm3 g−1. Finally, the remaining volume is due to the macropores greater than 50 nm in size which are present in the scaffold. The BET surface area of the scaffold is 26.05(1) m2 g−1.

According to SAXS analysis, the average Porod slope in the low and mid q ranges was 3.31, indicating that the pores in the pellet formed a surface fractal (Fig. 5(a)). The surface fractal dimension was D = 2.69 and r = 21 Å. The value of r (r = 2πq/ξ) was calculated using ξ = 0.31 Å−1, which is the value for the transition from power-law 3.31 to 4. A plot of ξq−3.31 vs. q, shown in Fig. 5(b), shows a plateau at q = 0.21 Å−1, with
\[
\lim (l_q) = 2.06 \times 10^{24} \text{ cm}^{-4.31}. \quad F(D) \text{ was equal to } 1.77, (\Delta \rho)^2 \text{ was equal to } 2.13 \times 10^{22} \text{ cm}^{-4} \text{ and } \rho_0 \text{ was equal to the crystal density of Mg that is } 1.75 \text{ g cm}^{-3}. \text{ Substituting these values into the equation of Hurd}^{41} \text{ (eqn (4)) to allow for a direct comparison with the BET results, yields a specific surface area of } 39(5) \text{ m}^2 \text{ g}^{-1}. \text{ This value was observed to be larger than the BET value, as this surface area also includes closed porosity.}
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The SEM micrographs of the as-prepared porous Mg scaffold are presented in Fig. 6(a and b). The pores have a broad range of sizes and are mainly macropores. This observation was also confirmed by the \(N_2\) adsorption/desorption isotherms and the applied BJH method of this particular sample. The Mg scaffold has an open porous network structure similar to a sponge. The walls of the solid Mg that form the pores are thin which makes it easier for the \(H_2\) to diffuse through them when the pores are occupied with \(LiBH_4\) during its thermal decomposition. The voids (1–2 \(\mu\)m), have been created during the compaction of the \(NaMgH_3\) powder into a pellet. The macropores present in the scaffold may have been created from the molten sodium evaporating due to the applied dynamic vacuum during the sintering process. Finally, the mesopores present in the scaffold may have been formed during the desorption of \(H_2\) while the \(NaMgH_3\) pellet was heated under dynamic vacuum. The small number of mesopores may in part, be due to the fact that the \(H_2\) is diffused

| Table 2 | Physical properties of porous Mg scaffold |
|---------|------------------------------------------|
| Sample  | Specific surface area (BET) (m² g⁻¹) | Specific surface area (SAXS) (m² g⁻¹) | Pore volume due to mesopores (cm³ g⁻¹) | Pore volume due to macropores (cm³ g⁻¹) | Pore volume due to voids (cm³ g⁻¹) | Total pore volume (cm³ g⁻¹) |
| Porous Mg scaffold | 26.05(1) | 39(5) | 0.06 | 0.77 | 0.42 | 1.25 |
first at lower temperatures compared to molten Na. Thus, once the H2 is desorbed from the main body of the pellet, the system has enough time to reform the pore structure as the final temperature has not been reached and the Na present is starting to become molten. Therefore, more sintering experiments with various H2 backpressures are required in order to investigate the formation of the pores. The delay of H2 desorption during the sintering of the NaMgH3 pellet will result in the presence of more mesopores present in the scaffold.

Fig. 7 shows the SEM micrographs of the porous Mg scaffolds infiltrated with 12.78, 22.50 and 32.55 wt% of LiBH4 respectively. It is noticeable that the complex metal hydride first occupies the smaller pores (mesopores) via capillary condensation as seen in Fig. 6(a and b). As the amount of the infiltrated LiBH4 increases, the larger pores get occupied with the complex metal hydride (Fig. 7(c and d)). Lastly, Fig. 7(e and f) represents the porous Mg scaffold that has been infiltrated with the highest amount of LiBH4. It can be seen that the complex metal hydride has infiltrated all the pores present in the sample creating a solid pellet.

3.3 Thermal analysis

The TPD curves of the melt-infiltrated as well as the bulk samples are presented in Fig. 8 and 9. In Fig. 8(b) and 9(b) the H2 wt% has been normalised to the amount of desorbed H2 for each sample in order for results to be easily comparable. In Fig. 8(a) it is noticeable that the samples PMg13, PMg23 and PMg33 start desorbing H2 at 100 °C. According to our knowledge, such a result has not been reported in the literature so far. There is no H2 desorption detected for the bulk samples at that temperature range (Bulk LiBH4, Bulk pellet, Bulk powder, Bulk 2LiBH4:Mg). This behaviour is attributed to the LiBH4 melt-infiltrated into the mesopores of the Mg scaffold. The infiltrated complex metal hydride in the pores is not only nanofluid, but also destabilised by the presence of the Mg and MgH2. The volume created by the mesopores in each sample is the same. Thus, the amount of the desorbed H2 in all three samples at the temperature range of 100 to 420 °C is the same (Fig. 8(a)). As the temperature increases, it can be seen that PMg23 and PMg33 have the same desorption profiles as the
bulk samples. This observation is due to the fact that once the infiltrated LiBH₄ for these samples has occupied all the mesopores, it then starts to enter the macropores and voids of the scaffold. Therefore, the complex metal hydride at these macro sizes behaves as a bulk material and has the same H₂ desorption properties as the bulk samples. In contrast, the sample with the least amount of infiltrated LiBH₄ (PMg13) has a different H₂ desorption profile which is due to the fact that the amount of LiBH₄ contained in that scaffold occupies only the pores in the mesoporous range. This particular sample has desorbed 35% of its H₂ wt% at 400 °C whereas the bulk pellet and bulk powder at that temperature is 0.

Moreover, bulk LiBH₄ starts desorbing H₂ after its melting point at 350 °C whereas when it is mixed with MgH₂ the desorption takes place at 430 °C. According to the literature at high temperatures and low pressures, LiBH₄ and MgH₂ simultaneously decompose and form MgB₂. Therefore, the decomposition of LiBH₄ at 350 °C is inhibited and it only takes place at higher temperatures. Lastly, bulk Mg:2LiBH₄ sample starts desorbing H₂ at 350 °C similar to bulk LiBH₄. As there is no MgH₂ present in this sample, MgB₂ is formed simultaneously when LiBH₄ starts to decompose. Hence, the temperature for this reaction is at 350 °C, as for bulk LiBH₄.

Fig. 10 shows the experimental, as well as the theoretical, H₂ wt% of all samples that have been desorbed up to 550 °C. For the samples for which the desorption started at 0 bar of H₂ backpressure, the experimental and theoretical values are the same, taking into account the further decomposition of LiH (eqn (8)).

\[ \text{LiH} + \text{Mg} \rightarrow \text{LiMg} + \frac{1}{2} \text{H}_2 \quad (8) \]

LiH can further decompose at temperatures above 500 °C, as the presence of excess Mg present from the porous scaffold is able to further react with the LiH formed from the first decomposition pathway. These samples exhibited high
desorbed H₂ wt% (PMg23 = 5.09 H₂ wt%, PMg33 = 7.12 H₂ wt%) reaching the targets set by the U.S. Department of Energy,⁹ which makes them promising candidates for on-board hydrogen storage in vehicles run by fuel cells.

The samples for which their decomposition took place under 1, 2, and 3.4 bar of H₂ backpressure, the experimental value of the H₂ wt% is smaller than the theoretical ones derived from eqn (2). The reason for this observation is due to the fact that the kinetics of this reaction slowed down as the H₂ back-pressure increased (Fig. S3†). Finally, the experimental desorbed H₂ wt% of all bulk samples are smaller than the theoretical ones as the formed agglomerations in the metal hydrides hindered the kinetics of the reaction and also the presence of Mg in the sample was not enough to further decompose the LiH. A table of all the values of the desorbed H₂ wt% as well as maximum pressures observed and temperatures are in Table S1 in the ESI.

In Fig. 11 the diffraction patterns of all samples after their TPD experiments are presented. All samples were crushed from a pellet to a powder in order to obtain a more comprehensive phase analysis from the entire sample. The diffraction patterns of the PMg13 and PMg23 (Fig. 8(a and b)) show only diffraction peaks corresponding to Mg, MgO, MgB₂, and LiMg. The H₂ has been completely desorbed and no evidence of LiH, or partially unreacted MgH₂ is present in the sample. These observations also confirm the value of the calculated experimental H₂ wt% which is due to eqn (2) and (3) and matches the theoretical H₂ wt% calculated for eqn (8). The diffraction pattern of PMg33 has MgH₂ diffraction peaks, suggesting that during the cooling of the sample, a small amount of H₂ was reabsorbed from the Mg scaffold to form MgH₂. The experimental value of the desorbed H₂ wt% for this sample is slightly smaller than the theoretical one derived from eqn (6). This indicates that the MgH₂ present in the sample should have been completely desorbed when the sample was reached 550 °C and the remaining MgH₂ could only be formed during reabsorption while cooling down. The presence of LiH in this particular sample indicates that the further decomposition of LiH was incomplete, which is indicative of the slight mismatch of the experimental and theoretical value (from eqn (6)) of desorbed H₂ wt%. The diffraction patterns of the bulk samples show both MgH₂ and LiH, which is due to the incomplete reaction of eqn (2), explains the lower experimental

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Fig. 10  Diagram representing the values of the theoretical as well as experimental H₂ wt% for all samples at 550 °C.

Fig. 11  XRD patterns of (a) PMg13, (b) PMg23, (c) PMg33 (d) bulk 2LiBH₄/MgH₂ in a form of a powder and (e) pellet after TPD experiments conducted under 0 bar of H₂ backpressure.

Fig. 12  XRD patterns of (a) PMg33, (b) PMg26, (c) PMg34 and (d) PMg35 after TPD experiments which were performed under 0, 1, 2 and 3.4 bar of H₂ backpressure respectively.
values of their desorbed H₂ wt% in comparison to the theoretical values.

Fig. 12 shows the diffraction patterns of all samples that were infiltrated with the highest amount of LiBH₄ and were desorbed under different values of H₂ backpressures. For the samples PMg33 and PMg26, the amount of LiH present in the samples is almost undetectable due to the small amount of LiH, as well as its low scattering power. The presence of LiH and MgH₂ is more evident in the diffraction patterns of the samples PMg33 and PMg35 that were desorbed with starting H₂ backpressures at 2 and 3.4 bar respectively. The kinetics of eqn (2) were slower in comparison to the ones of the samples that were desorbed at lower H₂ backpressures (0 and 1 bar of H₂) therefore the amount of MgH₂ and LiH are higher and therefore easier to detect.

4. Conclusion

A porous Mg scaffold was synthesised using a cost effective method by sintering a NaMgH₃ pellet under dynamic vacuum. The created scaffold consisted of pores in the meso and macro range as seen from SEM micrographs and the BJH analysis. The pores were created by the desorption of H₂ and the evaporation of Na. The diffraction pattern after the sintering, showed that the scaffold is composed of Mg. SEM micrographs, as well as diffraction analysis of the infiltrated samples confirmed that the LiBH₄ entered the pores of the scaffold by first occupying the smaller pores, followed by the larger ones. The Temperature Programmed Desorption measurements of all samples showed that the infiltrated samples started desorbing H₂ at 100 °C which is 250 °C lower than the accepted temperature the bulk LiBH₄ and 330 °C lower than the accepted temperature for bulk 2LiBH₄-MgH₂. PMg13 desorbed 35% of its total value of H₂ below the melting point of LiBH₄ (350 °C). The PMg33 sample exhibited enhanced hydrogen storage properties (7.12 H₂ wt%) and exceeded the targets set by the U.S. Department of Energy (5.5 H₂ wt%). Further improvements have to be made regarding the synthesis process of the porous Mg scaffold in order to increase the number of mesopores. This will allow the LiBH₄ melt-infiltrated samples to not only desorb H₂ at 100 °C or less, but also to reach and hopefully exceed the 5.5 H₂ wt% target, making them ideal candidates for on-board hydrogen storage in automobile applications. Lastly, the reversibility of the LiBH₄ melt-infiltrated samples needs to be investigated by rehydrogenating the samples under various H₂ backpressures and temperatures.

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