A noble metal-free proton-exchange membrane fuel cell based on bio-inspired molecular catalysts†

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Hydrogen is a promising energy vector for storing renewable energies: obtained from water-splitting, in electrolyzers or photoelectrochemical cells, it can be turned back to electricity on demand in fuel cells (FCs). Proton exchange membrane (PEM) devices with low internal resistance, high compactness and stability are an attractive technology optimized over decades, affording fast start-up times and low operating temperatures. However, they rely on the powerful catalytic properties of noble metals such as platinum, while lower cost, more abundant materials would be needed for economic viability. Replacing these noble metals at both electrodes has long proven to be a difficult task, so far incompatible with PEM technologies. Here we take advantage of newly developed bio-inspired molecular H2 oxidation catalysts and noble metal-free O2-reducing materials, to fabricate a noble metal-free PEMFC, with an 0.74 V open circuit voltage and a 23 μW cm−2 output power under technologically relevant conditions. X-ray absorption spectroscopy measurements confirm that the catalysts are stable and retain their structure during turnover.

Fig. 1 Structure of the Ni–CNT HOR catalyst based on a synthetic nickel bisdiphosphine complex inspired by the structures of the active sites of FeFe and NiFe hydrogenases shown in the inset.

Proton exchange membrane (PEM) technology currently stands as the most promising fuel cell variety for both portable and automotive applications. PEMFCs have low internal resistance, high compactness and stability. Having been optimized over decades, they display high efficiency, start rapidly and operate at low temperature. However, they require platinum to catalyse both the H2 oxidation reaction (HOR) and the O2 reduction reaction (ORR) which hampers their economic viability and sustainability. Substituting earth-abundant catalysts for noble metals is thus critical. Significant progress has been achieved regarding the development of ORR catalysts1–7 but no PEMFC using earth-abundant catalysts at both electrodes has been reported so far.

We recently reported on noble metal-free catalysts for the HOR9 working under highly acidic conditions compatible with PEM technology. Hydrogenases10,11 are unique metalloproteins that catalyse HOR as efficiently as platinum nanoparticles do and in particular with remarkably high reaction rates (1500–9000 s−1 at pH 7 and 37 °C in water).12 Their active sites (Fig. 1) have inspired the design of new synthetic HOR catalysts, the most efficient ones being bisdiphosphine nickel complexes13 exquisitely combining a nickel centre in an electron-rich environment as found in NiFe hydrogenases with proton relays provided by a pendant base mimicking the aza-propane-dithiolato cofactor of FeFe hydrogenases.14 In both classes of hydrogenases,14 the presence of basic residues at the vicinity of the catalytic metal centre indeed facilitates the activation and heterolytic cleavage of H2. Immobilization of such synthetic catalysts, either covalently or through π–π stacking
interactions, on multiwall carbon nanotubes (CNTs) yielded Ni–CNT HOR catalytic nanomaterials.\textsuperscript{a,8} When interfaced with a Nafton membrane, these nanomaterials show catalytic activity for hydrogen evolution/uptake at the thermodynamic equilibrium, prolonged stability under turnover conditions and resistance to CO poisoning. It was thus tempting to implement these original materials as anode PEMFC catalysts. Here we report the first functional PEMFC based on earth-abundant materials at both anode and cathode.

Deposition of one of these Ni–CNT HOR materials on a Nafton membrane was first achieved through spray coating.\textsuperscript{16} The preparation of a catalytic ink with suitable rheological properties required partial substitution of CNTs with carbon black nanoparticles with lower form factor. The anode Ni–CNT ink was then composed of a [Ni(P\text{Ph}_3\text{N}_2\text{Cl(CF}_3\text{Pyrene})_2]_2[B\text{F}_4]_2/CNTs (Ni–CNT, 30 wt% dry mass) material (Fig. 1),\textsuperscript{9} Vulcan XC-72 (40–50 wt%) and Nafton (20–30 wt%) in a water/isopropanol mixture (80/20 wt%). The use of a 5 : 1 Vulcan XC-72 : CNTs mass ratio led to particles in the 10–100 μm range as measured by dynamic light scattering.

A novel Co–N–C ORR catalyst with suitable rheological properties was obtained through adaptation of a previous procedure developed by some of us.\textsuperscript{13,14} Pyrolysis of a mixture of a N-heterocyclic organic compound (triazolopyridine) and Vulcan XC-72 in the presence of Co(NO\textsubscript{3})\textsubscript{2} (ref. 3 and 17) at 700 °C gave a fine dispersion of 0.1–100 μm particles in Nafton (20–30 wt%) and water/isopropanol as a proper ink for spray coating. By analogy with the previously described material, the ORR activity is assigned to pyridinic-N functional groups located at the surface of the carbon matrix and binding cobalt ions as well as metallic cobalt nanoparticles.\textsuperscript{3} This material displays an overpotential for the ORR ~300 mV higher than Pt/C in a half cell configuration and good stability for more than 15 h during chrono-amperometry measurements. A detailed structural and catalytic study is provided in the ESL.\textsuperscript{†}

![Fig. 2](image-url)

**Fig. 2** Left: schematic description of the PEMFC assembly; right: polarization and power density curves of the Ni–CNT/Co–N–C PEMFC recorded at 60 °C with a supply of partially humidified H\textsubscript{2} (20 mL min\textsuperscript{-1}) at the anode and passive air convection at the cathode.

After spray coating of the catalytic inks (0.44 to 0.64 mg cm\textsuperscript{-2}, corresponding to about 10 μm thickness) on both sides of a NRE-212 Nafton membrane (5.76 cm\textsuperscript{2}) at 60–80 °C, the assembly was hot-pressed (50 °C, 2 × 10\textsuperscript{5} Pa, 3 min) to improve catalyst–electrolyte contact and metal collectors were deposited on each side by evaporation of a gold layer, thin enough to allow for gas permeation. The resulting membrane–electrode assembly (MEA, Fig. 2) was assessed at 60 °C in air under natural convection and ambient humidity in a dedicated micro fuel cell test-rig. Partially humidified hydrogen (20 mL min\textsuperscript{-1} bubbling in water) was supplied to the anode, and air was passively supplied to the cathode.

The polarization and power density curves for the resulting Ni–CNT/Co–N–C PEMFC are shown in Fig. 2. Table 1 compares the performances of this noble metal-free PEMFC with other cells in which one electrode has been replaced by a standard Pt-based electrode similarly prepared from 40% Pt/C catalytic material. The noble metal-free PEMFC proved functional with an open-circuit voltage (OCV) of 0.74 V, to be compared with the 1.0 V OCV value measured for a Pt/Pt PEMFC under the same conditions. The Ni–CNT/Pt and the Pt/Co–N–C control PEMFCs provided OCV values only 150 and 210 mV lower, respectively, than a standard Pt/Pt PEMFC, showing that each noble metal-free catalyst operates at reasonable overvoltages. The maximum power density of the noble metal-free PEMFC was 23 μW cm\textsuperscript{-2} under dynamic conditions and it stabilized at 20 μW cm\textsuperscript{-2} under stationary conditions. From Table 1, it can be concluded that the ORR catalyst, tested against Pt in a full PEMFC device, shows a higher current density (13 mA cm\textsuperscript{-2}) than in half-cell configuration (1–3 mA cm\textsuperscript{-2}, Fig. S4 and S5†) but the reverse is observed for the HOR catalyst (0.224 mA cm\textsuperscript{-2} in a PEMFC versus 1 mA cm\textsuperscript{-2} in half-cell configuration, Fig. S6†). The limitation in terms of current density and output power thus comes here from the bio-inspired anode material and its interface with the membrane rather than from the cathode catalyst, indicating a direction for further improvement of performances.

Finally, the operation of Pt/Co–N–C and Ni–CNT/Pt PEMFCs at temperatures increasing from 25 °C to 60 °C showed a low increase in current density by a factor of ≤1.5, corresponding to an activation energy below 10 kJ mol\textsuperscript{-1} and 20 kJ mol\textsuperscript{-1}, respectively. These low activation energy values show that the current is likely limited by the gas transport processes in the bulk of the electrode materials.

**Table 1** Open circuit voltage (OCV), current density and maximum power density generated by various PEMFCs based on Ni–CNT, Co–N–C or Pt catalysts; PEMFCs were measured at 60 °C with a supply of partially humidified H\textsubscript{2} (20 mL min\textsuperscript{-1}) at the anode and passive air convection at the cathode

| Anode | Cathode | OCV/V | \(\mathbf{I_{\text{max}}}}\) V/μA cm\textsuperscript{-2} | \(\mathbf{P_{\text{max}}}}\) μW cm\textsuperscript{-2} |
|-------|---------|-------|-----------------|-----------------|
| Pt    | Co–N–C  | 0.79  | \(1.3 \times 10^4\) | 2600            |
| Ni–CNT| Pt      | 0.85  | 224             | 70              |
| Ni–CNT| Co–N–C  | 0.74  | 94              | 23              |
| Pt    | Pt      | 1.00  | 1.75 \times 10^3 | 1.05 \times 10^3 |
The as-prepared Ni–C–CNT anode nanomaterial was compared with the molecular Ni catalyst (Fig. 4 and S10†) to gain insight into the molecular state of the metal catalytic centers. Detailed analysis of the Ni K edge XAS signal measured for the complete cell proved impossible, so we turned to previously described half-cell experiments with the Ni–CNT material deposited on a gas diffusion layer.† As previously reported, the Ni-edge EXAFS spectrum of the Ni–CNT material before operation could be decomposed into the weighted addition of the spectra for pure molecular \( \text{Ni}[\text{PPh}2\text{N(CH2)pyrene}]_2 \) catalyst and for NiII ions coordinated to lighter atoms as in \( \text{Ni(H2O)}_2^{3+} \), indicating that about 2/3rd of the Ni complex remains in the NiP4 state (Table S2†). After 1 hour of operation for \( \text{H}_2 \) oxidation at 0.25 V vs. RHE and in direct contact with 0.5 M aqueous H2SO4 electrolyte, the signal assigned to decomposed Ni complex disappears, leaving a pure NiP4 signature (Fig. 4, Fig. S10 and Table S2†). As the current density remains constant during the whole measurement (Fig. S4†), corresponding to 4000 turnovers achieved for each NiP4 species, we conclude that the decomposed Ni compound was washed off from the material during the electrochemical measurement. Additionally this experiment tells us that the bio-inspired NiP4 complex is the only species responsible for catalysis and that it does withstand extensive PEM fuel cell operation with complete retention of its molecular structure.

We have thus successfully demonstrated the potential of the bio-inspired chemistry approach for the development of novel fuel cells based exclusively on non-noble metals. Previously described earth-abundant catalytic HOR and ORR materials have been assessed either in half-cell measurements or in combination with a platinum-based counter electrode material. Here, we report the first example of an operational PEMFC using a bio-inspired Ni-based material at the anode and a Co-based material at the cathode. Importantly, the operation and feeding conditions used in our study correspond to the expected daily use of market-dedicated micro devices and the performances reported here compare well with those of the first generation of \( \text{H}_2/\text{O}_2 \) enzymatic fuel cells. Further improvements of the performances of the devices can be expected from optimization of the ink formulation and control of the tri-dimensional structure of the electrodes as previously demonstrated for \( \text{H}_2/\text{O}_2 \) or glucose/\( \text{O}_2 \) biofuel cells.

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18 The same behavior is observed if the material is simply equilibrated with the aqueous electrolyte during the measure of a few cyclic voltammograms (Fig. S10†) or if the experiment is carried out during 1 h under H2 evolution conditions (Fig. S11 and Table S2†). If the same measurement is carried out on the Ni–CNT material coated with a Nation membrane, the XANES signal is unmodified even after 1 hour of operation for H2 evolution at –0.3 V vs. RHE (Fig. S11 and Table S2†).

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