Response surface based optimization of laccase production from *Bacillus sp.* MSK-01 using fruit juice waste as an effective substrate

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**A B S T R A C T**

Laccases are multicopper oxidases containing four copper atoms per monomer distributed in three redox sites. Because of its tremendous applications in different areas, isolation of new laccases with wide range of industrial implementation. The present study focuses on the optimization of laccase production from *Bacillus* sp. MSK-01 under solid state fermentation conditions using fruit juice waste as the substrate. MSKLAC was produced extracellularly by the bacteria. This laccase was able to oxidize ABTS and syringaldazine. Various nutritional and environmental factors were utilized for increasing the enzyme yield. Plackett Burman was used to study the influence of input parameters on laccase yield. Tween-80, initial moisture ratio and magnesium sulphate were the major influencing factor affecting laccase yield. Central composite design of RSM was used for the modelling of experiment. Desirability approach was used to optimize laccase yield. Maximum laccase yield of 1645 IUg⁻¹ was obtained when 0.55% of tween-80, 1:2.34 initial moisture ratio and 300 μM magnesium sulphate was used. A 470 fold increase in the yield of laccase from unoptimized condition was obtained.

1. Introduction

Laccases (benzenediol: oxygen oxidoreductases; EC 1.10.3.2) are multicopper oxidases (MCOs) which catalyze the oxidation of a wide variety of organic and inorganic compounds with concomitant four electron reduction of molecular oxygen to water. They catalyze the oxidation of both phenolic and non-phenolic substrates [1]. Laccases are very useful enzymes with respect to their applications in industry. They have found uses in biotechnological applications such as biobleaching, xenobiotics bioremediation, decolourization of textile dyes, biosensors, food industry, plastic degradation, degradation of lignin in lignocelluloses for the production of biofuels etc. [2, 3, 4].

Besides stability of an enzyme at industrial conditions, major obstacle in the path of the actual use of an enzyme at industrial level is its production cost. The development of procedures for the production of highly efficient, environment friendly and cost effective enzyme is a primary approach [5]. Solid state fermentation (SSF) is an cost effective method for increasing the enzyme production and is defined as any fermentation process occurring in the absence or near absence of free liquid, using an inert or a natural substrate as a solid support [6]. It is an economical process as it provides higher volumetric productivities [7].

Although most of the times SSF has been observed to be successful for filamentous organisms such as fungi, actinomycetes etc. [7, 8] but recently there are reports where SSF has been found to be useful for the production of enzymes from bacteria [9, 10]. Laccases are known to be secreted intracellularly by the bacteria. Therefore, SSF for laccase production was not reported in previous studies. Recently, it has been found that laccases are also secreted extracellularly by bacteria [11]. Sharma et al. [12] optimized the laccase production from *Lysinibacillus* sp. using SSF. They reported that 10 mg (w/w) of used TATA acti green tea leaves per 5 g of wheat bran, 1% pulp and paper industry effluent (agro based), and 1% wine made from *Sygium cumini* enhanced the laccase production 2.69, 2.61, and 2.09 fold, respectively. Muthukumarasamy et al. [13] optimized laccase production from *B. subtilis* MTCC 2414 using rice bran and wheat bran agroresidues. Maximum production was achieved at temperature 30 °C (270 ± 2.78 U/mL), pH 7.0 (345 ± 3.14 U/mL), and 96 h (267 ± 2.64 U/mL) of incubation. The carbon and nitrogen sources resulted in high enzyme yield at 3% sucrose (275 ± 3.11 U/mL) and 3% peptone (352.2 ± 4.32 U/mL) for rice bran and 3% sucrose (247.4 ± 3.51 U/mL) and 3% peptone (328 ± 3.33 U/mL) for wheat bran, respectively. Nevertheless, due to scarcity of extracellular laccase producing bacteria, utilization of agro-industrial residues for bacterial
laccase production is a rare task. Furthermore, the researchers have employed one factor at a time approach (OFAT) for the optimization of laccase production through SSF [12, 13]. OFAT methods are good in assessing the effect of each variable on response independently but the interactive effect of variables on the response can never be assessed using OFAT. Statistical software’s like response surface methodology is an ideal modeling approach for designing of experiments. In this regard, in the present study, a new Bacillus sp. MSK-01 producing extracellular laccase was isolated and laccase production has been optimized through response surface methodology (RSM) based desirability approach.

Furthermore, the success of solid state fermentation (SSF) process is related to the characteristics of the support/substrate used. Porosity and particle size of the substrate affect the surface area accessible to the organism. The size of the substrate favors gas and nutrient diffusion, rate of colonization, CO₂ removal and downstream extraction [14]. Small substrate particles provide a large surface area for microbial attachment while larger particles provide better aeration but a limited surface for microbial attachment. Therefore, selection of substrate is an important parameter in SSF. The fruit juice industry generates large amount of waste which is of no use. This waste is however is rich in phenolic compounds. Therefore, it has a potency to become good substrate for laccase production. But, till now none of the researchers has reported the utilization of fruit juice waste as substrate for laccase production. Many studies are based on the utilization of wheat bran as substrate [15, 16, 17, 18]. Other substrates like olive leaves [19], rice straw [20], coffee husk [21] etc. were also used for laccase production in the past few years.

By deeply analyzing the literature, it was observed that extracellular laccase producing bacteria are very few till date, RSM was not utilized for the production of laccase by bacteria in SSF and fruit juice waste was not used as substrate. Keeping all this in mind, the present study was designed to optimize laccase production using fruit juice waste as raw material in SSF by using RSM based desirability approach.

2. Materials and methods

2.1. Chemicals

Guaiacol used in the present study was purchased from Sigma (USA). Other chemicals were obtained from Hi-media (India) and were of analytical grade. Fruit juice waste was obtained from a local vendor of fruit juices.

2.2. Laccase assay

Laccase assay was performed at 75 °C for 10 min in 0.1 M Tris-HCl buffer (pH 8.0) using guaiacol (2mM) as substrate [22, 23]. The change in absorbance due to the oxidation of guaiacol was monitored at 465 nm (ε = 12,000 M⁻¹ cm⁻¹) in a UV–Visible spectrophotometer. The enzyme unit was expressed in IU g⁻¹. One unit of laccase (IU g⁻¹) was defined as the amount of the enzyme required to transform 1 μmol substrate per min per gram of substrate.

2.3. Isolation of extracellular laccase-producing bacteria

Extracellular laccase-producing bacteria were isolated on M162 medium supplemented with 0.2 % yeast extract, 0.2 % tryptone, 100 μM CuSO₄, and 2mM guaiacol [24]. The detailed composition of M162 is given in Table 1. Soil samples were collected from different areas where lignocellulosic waste was decomposing. Samples were enriched in M162 medium containing 2mM guaiacol and appropriate dilutions were plated. The plates were incubated at 37 °C for 48 h. The colonies showing reddish brown color were selected.

2.4. Selection of bacterial strains producing extracellular laccase

Selected bacterial cultures were screened for the presence of extracellular laccase activity. For this, 0.1 % of overnight-grown bacterial culture was inoculated in M162 broth containing 0.2 % yeast extract, 0.2 % tryptone, and 100 μM CuSO₄. After 48 h, the culture supernatant was obtained by centrifugation at 7826 x g for 15 min and was used as extracellular enzyme. The laccase activity was examined in extracellular enzyme preparations using guaiacol as substrate. The strains exhibiting extracellular laccase activities were selected. Furthermore, the oxidation of 2,2’-azino-bis[3-ethylbenzthiazoline-6-sulphonic acid] (ABTS) and syringaldazine (SGZ) and tyrosine was also assayed to confirm the presence of true laccase activity.

2.5. Identification of the isolate

The morphology of the isolate was studied by Gram staining. Physiological and biochemical characterization was done according to Bergey’s Manual of Determinative Bacteriology [25]. Furthermore, the organism was identified based on 16S rDNA sequence, wherein the genomic DNA was isolated from the culture. Its quality was evaluated on 1.0% Agarose Gel, a single band of high-molecular weight DNA was observed. Fragment of 16S rDNA gene was amplified by PCR using 27F & 1492 R primers. A single discrete PCR amplicon band of 1500 bp was observed when resolved on Agarose. The PCR amplicon was purified to remove contaminants. Forward and reverse DNA sequencing reaction of PCR amplicon was carried out with forward and reverse primers using BDT v3.1 Cycle sequencing kit on ABI 3730xl Genetic Analyzer. Consensus sequence of 16S rDNA gene was generated from forward and reverse sequence data using aligner software (outsourcing done by Eurofins Genomics India Pvt. Ltd., Bangalore, India). Sequences homologous to isolate MSK-01 were obtained using EzTaxon. Sequences with high query coverage and homology were selected for phylogenetic analysis [26]. Multiple sequence alignment was done using MultAlin (version 5) [27], and phylogenetic tree was constructed using MEGA version 4.0 [28].

2.6. Solid state fermentation of MSK-01 laccase

2.6.1. Inoculum preparation

The inoculum was prepared by inoculating a single bacterial colony from freshly grown plates into M162 medium containing 0.2% yeast extract, 0.2% tryptone and 100 μM CuSO₄ in 250 ml Erlenmeyer flask. The culture was incubated at 37 °C, 150 rpm for 24 h and used as inoculum.

2.6.2. Extraction of laccase

The fermented fruit juice waste from each flask was suspended in 25 ml Tris-HCL buffer (100 mM, pH 8.0) and shaken at 150 rpm for 45 min. The extrudates were squeezed through muslin cloth for maximizing the enzyme extraction and centrifuged at 7826 x g for 20 min. The enzyme solution thus obtained was assayed for laccase activity.

| Table 1 Composition of M162. |
|-----------------------------|----------------|
| **Micronutrient solution (10X)** | (100 ml) |
| H₂SO₄ (conc.) | 5.0 ml |
| Manganese sulphate monohydrate (MnSO₄.4H₂O) | 2.28 g |
| Zinc sulphate heptahydrate (ZnSO₄.7H₂O) | 5.0 g |
| Boric acid | 5.0 g |
| Copper sulphate pentahydrate (CuSO₄.5H₂O) | 250 mg |
| Sodium molybdate dihydrate | 250 mg |
| Cobalt chloride hexahydrate (CoCl₂.6H₂O) | 450 mg |
| M162 (10X) | 0 (L⁻¹) |
| Calcium sulphate dihydrate (CaSO₄.2H₂O) | 0.4 g |
| Magnesium chloride hexahydrate (MgCl₂.6H₂O) | 2.0 g |
| Nitrosoacetic acid 1.0g Micronutrient solution (10X) | 1.0 ml |
| Ferric citrate solution (0.01M) | 5.0 ml |
2.6.3. Selection of significant parameters by Plackett-Burman (PB).

A set of 12 experiments was designed using the Plackett-Burman design of the Design expert (version 9.0.7) software (Stat-Ease Corporation, USA) for 11 variables (Table 2) that were analyzed as possible factors affecting production based on literature search. The parameters evaluated were as follows: A: temperature, B: pH, C: incubation time, D: CuSO₄·5H₂O, E: moisture ratio, F: magnesium sulphate, G: yeast extract, H: manganese sulphate, J: moistening solution, K: Tween 80, L: inoculum. In each experiment, dried fruit juice waste was taken as the basal solid media (5g) in 250 ml erlenmyer falsk. Concentration levels were decided on the basis of literature reports on laccase production. All the trials were carried out in set of three and laccase yield was calculated as mean of these three values. The effect of each parameter on laccase yield was obtained as per following equation:

\[
V_i = \frac{\sum Y_{i+} - \sum Y_{i-}}{N}
\]

where, \(V_i\) is the effect of each input variable \(i\) under study, \(Y_{i+}\) and \(Y_{i-}\) are responses (laccase yield) of trials at which the parameter was at its high and low level, respectively, and \(N\) is the total number of trials. The significance of the model was calculated by ANOVA. From the pareto chart, the factors showing highest positive effects were selected for optimization using Central Composite Design of Response Surface Methodology.

2.6.4. Optimization of laccase production using response surface methodology (RSM)

Central composite design (CCD) of RSM was used from software Design expert (version 9.0.7, Statease Inc., Minneapolis, USA) at \(\alpha\) value of \(\pm 2\) to further optimize the levels of significant variables. Laccase activity was recorded as response. Response data were fed and analyzed by the software to generate 3D plots indicating the optimum conditions and interaction among these factors. Regression analysis was performed on the data obtained. A second-order polynomial equation was used to fit the data by multiple regression procedure. A quadratic model was obtained as per following equation:

\[
Y = \delta_0 + \sum \delta_i V_i + \sum \delta_{ij} V_i V_j + \sum \delta_{ijk} V_i V_j V_k
\]

where, \(Y\) is the predicted response (laccase activity (IU g\(^{-1}\))), \(\delta_0\) is the constant term, \(\delta_i\) the linear coefficients, \(\delta_{ij}\) the squared coefficients and \(\delta_{ijk}\) the interaction coefficients. The quality of fitting by the polynomial model equation was expressed using coefficient of determination \(R^2\). Eq. (2) was used to construct 3D plots.

![Pareto Chart](image)

**Fig. 1.** Pareto chart showing the effect of various factors on laccase production. Positive influencing factors were shown in orange while the negative one were shown in blue.
2.6.5. Prediction of optimum values for maximum laccase production

After getting the model equation that explains the process, it was used for optimization of the laccase production using the numerical optimization option of the software. Criteria were set for each independent variable and the response (dependent variable). The independent variables were kept in the range used by the experimental setup and the response was set maximum. A solution was generated with predicted levels of the independent variables and predicted maximum production.

2.6.6. Validation experiments

To check the validity of the chosen quadratic model, experiments were designed using the predicted optimum values of the parameters from Eq. (2). The laccase activity was measured and compared with the predicted value. Each experiment was conducted in triplicates and the data presented as mean ± SD.

3. Results and discussion

In this present study, a search has been made to isolate novel bacteria that produce extracellular laccase. The productivity of laccase from bacteria depends largely on the medium constituents and their concentration. Concentration of phosphate was found to play a significant role in the isolation of laccase producing bacteria. Other media components such as yeast extract, tryptone and glucose also play significant role. It has been reported in literature that phosphate exerts negative effect on laccase synthesis. M162 media contains no phosphate and is therefore used for the isolation of laccase producing bacteria [29]. A total of 2 bacteria, Isolate MSk-01 and Isolate MSK-03 giving extracellular activity were isolated. To confirm the presence of true laccase activity, isolates

Table 3

| Source               | Sum of Squares | df | Mean Square | F-value | p-value | significance |
|----------------------|----------------|----|-------------|---------|---------|--------------|
| Model                | 25010.64       | 10 | 2501.06     | 6937.12 | 0.0093  | significant  |
| A-time               | 13783.74       | 1  | 13783.74    | 38231.53| 0.0033  |              |
| B-Temperature        | 1244.40        | 1  | 1244.40     | 3451.56 | 0.0108  |              |
| C-pH                 | 430.32         | 1  | 430.32      | 1193.57 | 0.0184  |              |
| E-Moisture ratio     | 1516.05        | 1  | 1516.05     | 4205.02 | 0.0098  |              |
| F-Magnesium sulphate| 1487.86        | 1  | 1487.86     | 4126.83 | 0.0099  |              |
| G-Manganese sulphate| 1765.16        | 1  | 1765.16     | 4895.96 | 0.0091  |              |
| H-yeast extract      | 136.01         | 1  | 136.01      | 377.26  | 0.0327  |              |
| J-Moistening solution| 6.96           | 1  | 6.96        | 19.31   | 0.1425  |              |
| K-Tween 80           | 2383.46        | 1  | 2383.46     | 6610.94 | 0.0078  |              |
| L-Inoculum           | 2256.67        | 1  | 2256.67     | 6299.24 | 0.0080  |              |
| Residual             | 0.3605         | 1  | 0.3605      |         |         |              |
| Cor Total            | 25011.00       | 1  |             |         |         |              |
| Std. Dev.            | 0.6004         |    |             |         | 1.0000  |              |
| R²                   | 0.6481         |    |             |         | 0.9998  |              |
| C.V. %               | 0.9264         |    |             |         |         |              |
| Predicted R²         | 0.9998         |    |             |         |         |              |
| Adeq Precision       | 280.2084       |    |             |         |         |              |

Table 4

| Run | A-Tween 80 | B-Moisture ratio | C-Magnesium sulphate | Yield
|-----|------------|------------------|----------------------|-------|
| %   | %          | ratio | micromolar | IU/g |
| 1   | 1.00       | 2.00   | 100       | 383  |
| 2   | 0.55       | 1.50   | 300       | 1645.8 |
| 3   | 0.10       | 1.00   | 500       | 592  |
| 4   | 0.55       | 2.34   | 300       | 645.83 |
| 5   | 0.10       | 2.00   | 500       | 1327.5 |
| 6   | 0.10       | 2.00   | 100       | 1391.6 |
| 7   | 0.55       | 1.50   | 300       | 1650  |
| 8   | 1.00       | 2.00   | 500       | 300   |
| 9   | 0.55       | 1.50   | 36.36     | 450   |
| 10  | 1.00       | 1.00   | 100       | 975   |
| 11  | 0.55       | 1.50   | 300       | 1625  |
| 12  | 0.55       | 0.66   | 300       | 555.18 |
| 13  | 0.55       | 1.50   | 300       | 1620  |
| 14  | 0.10       | 1.00   | 100       | 340   |
| 15  | 0.55       | 1.50   | 300       | 1630  |
| 16  | 0.55       | 1.50   | 300       | 1630  |
| 17  | 0.55       | 1.50   | 636.36    | 683.34 |
| 18  | 0.55       | 1.50   | 300       | 1664  |
| 19  | 1.00       | 1.00   | 500       | 1160.83 |
| 20  | -0.21      | 1.50   | 300       | 1633.3 |

2.6.5. Prediction of optimum values for maximum laccase production

After getting the model equation that explains the process, it was used for optimization of the laccase production using the numerical

Table 5

| Source               | Sum of Squares | df | Mean Square | F-value | p-value | significance |
|----------------------|----------------|----|-------------|---------|---------|--------------|
| Model                | 5.275E+06      | 9  | 5.861E+05   | 822.15  | <0.0001 | significant  |
| A-Tween 80           | 1.643E+05      | 1  | 1.643E+05   | 230.48  | <0.0001 |              |
| B-Moisture ratio     | 17346.66       | 1  | 17346.66    | 24.33   | 0.0006  |              |
| C-Magnesium sulphate| 34173.83       | 1  | 34173.83    | 47.94   | <0.0001 |              |
| AB                   | 1.312E-06      | 1  | 1.312E-06   | 1840.69 | <0.0001 |              |
| AC                   | 904.61         | 1  | 904.61      | 1.27    | 0.2863  |              |
| BC                   | 42767.89       | 1  | 42767.89    | 60.00   | <0.0001 |              |
| A²                   | 80111.34       | 1  | 80111.34    | 112.38  | <0.0001 |              |
| B²                   | 1.970E+06      | 1  | 1.970E+06   | 2763.69 | <0.0001 |              |
| C²                   | 2.100E+06      | 1  | 2.100E+06   | 2945.42 | <0.0001 |              |
| Residual             | 5968.42        | 5  | 1139.68     | 3.98    | 0.0777  | not significant |
| Pure Error           | 1430.13        | 5  | 286.03      |         |         |              |
| Cor Total            | 5.282E+06      | 19 |             |         |         |              |
| Std. Dev.            | 26.70          |    |             |         | 0.9987  |              |
| Mean                 | 1075.49        | 7  |             |         |         |              |
| Adjusted R²          | 0.9974         |    |             |         |         |              |
| Predicted R²         | 0.9913         |    |             |         |         |              |
| Adeq Precision       | 70.9115        |    |             |         |         |              |
zymes other than laccase as well. Enzymes showing oxidation of ABTS (data not shown); therefore, Isolate MSK-01 was selected as a source of able to oxidize ABTS and SGZ but not tyrosine while MSK-03 was not (SGZ) oxidizing ability of their crude enzymes. Laccase from MSK-01 was [3-ethylbenzthiazoline-6-sulphonic acid] (ABTS) and syringaldazine form of pareto chart (Fig. 1). Length of column represented the signi
cs among them (Table 2). The in
tance of each real factor[31]. There-
coherence with each other. The value of adjusted R² (0.9913) sug-
gested that the variation of 99.13% in the enzyme activity was attributed
to the independent variables and only 0.87% of the total variation could
not be explained by the model.

3.4. Diagnosis of the statistical properties of the model

Statistical properties of the model can be analyzed by the normal plot for residuals. Data points should be approximately linear. A non-linear pattern (such as an S-shaped curve) indicates non-normality in the error term, which may be corrected by a transformation. The residuals of laccase yield show normal distribution (Fig. 2). Their alignment on the drawn line indicates that there are no abnormalities in the data.

3.5. Perturbation plot

The perturbation plot shows how the response changes as each factor moves from the chosen reference point, with other factors were held constant at the reference value. Fig. 3 shows that laccase yield was affected more by tween-80 followed by initial moisture content and concentration of magnesium sulphate. Increasing the concentration of tween-80 resulted in increase in laccase yield while increasing the level of magnesium sulphate and initial moisture content up to the coded reference point of 0.25 increased laccase yield. But further increase beyond the coded point decreased laccase yield.

3.6. Interaction between variables

The interaction between two variables when the third is kept at its optimum value is presented in 3D graphs (Fig. 4). The 3D graphs showed how laccase production is affected by the variation of two factors at a time keeping the other at optimal condition. Laccase production increased with increase in initial moisture content and concentration of Tween-80 individually (Fig. 4a) but both factors resulted in decrease in laccase yields in combination. Initial moisture content also plays an important role in SSF [34]. The availability of initial water in lower or higher amounts affects microbial activity adversely. Initial moisture content of 1:1.5 (45%) was found to be optimum for MSK laccase production. At 1:0.5 moisture content, the organism was unable to grow significantly and at 1:2 moisture ratio, due to high moisture content, growth of bacteria ceases. This can be due to the reason that the porosity of the medium decreases with the increase in moisture content leading to the difficulties of oxygen transfer and heat release in the medium [35]. An initial moisture content of 65% was the optimum for laccase production by Streptomyces psammosicus [7]. Laccase from fungi Tremetes versicolor and Pleurotus sajor-caju was produced maximally at 80% (w/v) moisture level [19, 35].

The use of surfactants for enzyme production in SSF has also been
Surfactants increase the permeability of the membrane's lipid bilayer, which facilitates the secretion of enzymes. Maximum yield of extracellular MSK laccase was achieved when 0.5% tween-80 was supplemented to the medium. Tween 80 has been reported to enhance the secretion of laccases in *Pycnoporus sanguineus* [36], *Ganoderma* sp. KK-02 [37], *Trametes trogii* [38] etc.

Similarly, magnesium sulphate and initial moisture content increased the laccase yield upto central value, further increase resulted in decrease in laccase production (Fig. 4b). Tween-80 and magnesium sulphate resulted in maximum laccase production at central level (Fig. 4c).

### 3.7. Validation of predicted variables for maximum laccase production

As the maximum yield was obtained in central run, therefore the model was internally validated. At the end of RSM, 470 fold (from 3.50 IU/g – 1645 IU/g) increase in laccase yield could be achieved. A remarkable increase in the enzyme activity (470 fold increase) was achieved under optimized conditions. Thus, the results of optimization studies helped in substantial increase in yield of laccase from *Bacillus* sp. MSK-01 which shall help in its industrial application.

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![Fig. 2. Normal probability plot of residuals of laccase yield showing their normal distribution.](image2)

![Fig. 3. Perturbation graph for three factors affecting laccase yield.](image3)
Fig. 4. Three dimensional response surface plots showing the effect of interaction of (a) Tween 80 and Moisture ratio (b) Moisture ratio and magnesium sulphate (c) Tween-80 and Magnesium sulphate on laccase production from Bacillus sp. MSK-01.
4. Conclusions

Bacterial enzyme production through fermentation of solid substrates is a possible solution to the cost related problems encountered in enzyme production. In this study, Bacillus sp. MSK-01 was cultured under SSF conditions using fruit juice waste as substrate. The fruit juice waste is of no value and thus adds no cost to the production. Laccase production in SSF was optimized. Maximum laccase yield of 1645 IUg⁻¹ was obtained when 0.55% of tween 80, 1:2.34 initial moisture ratio and 300μM magnesium sulphate was used. A 470 fold increase in the yield of laccase from unoptimized condition was obtained. Thus, production of MSK-01 laccase under optimized conditions in SSF will be an economically feasible laccase production system.

Declarations

Author contribution statement

Sonica Sondhi: Conceived and designed the experiments; Analyzed and interpreted the data; Contributed reagents, materials, analysis tools or data; Wrote the paper.
Kiranjot Saini: Performed the experiments.

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Competing interest statement

The authors declare no conflict of interest.

Additional information

No additional information is available for this paper.

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References

[1] R. Chandra, P. Chowdhary, Properties of bacterial laccases and their application in bioaccumulation of industrial wastes, Environ. Sci. Process. impacts 17 (2015) 326–342.
[2] V. Buddolla, R. Bandi, J. Avilala, P.K. Arthala, N. Golla, Fungal laccases and their applications in bioaccumulation, Enzym. Res. 2014 (2014) 163242.
[3] S. Sondi, R. Kaur, S. Kaur, P.S. Kaur, Immobilization of laccase-ABTS system for the development of a continuous flow packed bed bioreactor for decolorization of textile effluent, Int. J. Biol. Macromol. 117 (2018) 1093–1100.
[4] T. Kuzdanga, M. Le Roes-Hill, Laccase applications in biofuels production: current status and future prospects, Appl. Microbiol. Biotechnol. 98 (2014) 6525–6542.
[5] J.F. Osma, J.L. Toca Herrera, S.R. Couto, Cost analysis in laccase production, BioResources 4 (2009) 544–562.
[6] H. Risdianto, I. Sufiantini, S.H. Suhardim, T. Setiadi, Optimization of laccase production using white rot fungi and agriculture wastes in solid state fermentation, ITB J. Eng. Sci. 44 (2012) 93–105.
[7] J.C. Gonzalez, S.C. Medina, A. Rodriguez, J.F. Osma, C.J. Almeciga Diaz, O.F. Sanchez, Production of Trametes pubescens laccase under submerged and semi-solid culture conditions on agro industrial wastes, PLoS One 8 (2013) 73721.
[8] S. Sondi, P. Sharma, N. George, P.S. Chauhan, N. Puri, N. Gupta, An extracellular thermo-alkali-stable laccase from Bacillus tequilensis SN4, with a potential to biobleach softwood pulp, 3 Biotech (2015) 175–185.
[9] J.G. Holt, N.R. Krieg, P.H.A. Sneath, J.T. Staley, S.T. Williams, W. Williams, Bergey’s Manual of Determinative Bacteriology, ninth ed., 1994. Waverly Baltimore MD.
[10] J. Chen, J.H. Lee, Y. Jung, M. Kim, S. Kim, B.K. Kim, Y.W. Lim, EzTaxon: a web-based tool for the identification of prokaryotes based on 16S ribosomal RNA gene sequences, Int. J. Syst. Evol. Microbiol. 57 (2007) 2259–2261.
[11] F. Corpet, Multiple sequence alignment with hierarchical clustering, Nucleic Acids Res. 16 (22) (1988) 10881–10900.
[12] K. Tamura, J. Dudley, M. Nei, S. Kumar, MEGA4: molecular evolutionary genetics analysis (MEGA) software version 4.0, Mol. Biol. Evol. 24 (2007) 1596–1599.
[13] K. Kaur, G. Singh, V. Gupta, N. Capalash, P. Sharma, Impact of phosphate and other medium components on physiological regulation of bacterial laccase production, Biotechnol. Prog. 33 (2017) 541–548.
[14] J.W. Gatson, B.F. Benz, C. Chandrasekaran, M. Satomi, K. Venkateswaran, M. Sevanan, Production of laccase from an extracellular, thermo-alkali-stable, metal tolerant laccase from Bacillus tequilensis SN4, with potential for decolorization, Afr. J. Microbiol. Res. 16 (22) (2012) 10881–10900.
[15] H. Patel, A. Gupta, S. Gupte, Effect of different culture conditions and inducers on production of laccase by a basidiomycete fungal isolate Pleurotus ostreatus HP-1 under solid state fermentation, BioResources 4 (1) (2009) 268–284.
[16] A. Masabens, P. Ganasa, C. Polch, M. Avila, L. Salas, R. Vicum, Manganese-assisted laccase: the production in the basidiomycete Carpinopsis adhaerenspora, FEMS Microbiol. Lett. 275 (2007) 139–145.
[17] C.R. Soccol, E.S. Ferreira da Costa, L.A.J. Letti, S.G. Karp, A.L. Woiciechowski, L.F. de Souza Vandenberge, Recent developments and innovations in solid state fermentation, Biotechnol. Res. Innov. (2017).