As featured in: See Shaobin Wang, Lihong Liu et al., Chem. Commun., 2018, 54, 4919.

Showcasing research from the groups of Professor Shaobin Wang at Department of Chemical Engineering, Curtin University, Australia and Professor Xiaoyao Tan at Tianjin Polytechnic University, China.

Atomic-level design of CoOH⁺–hydroxyapatite@C catalysts for superfast degradation of organics via peroxymonosulfate activation

Mesoporous hydroxyapatite nanoparticles wrapped in uniform carbon layers (HA@C) was synthesized and used for simultaneous cobalt removal and organic waste decomposition by in situ formation of CoOH⁺–HA@C and activation of peroxymonosulfate, opening a new strategy for wastewater treatment.
Atomic-level design of CoOH⁺–hydroxyapatite@C catalysts for superfast degradation of organics via peroxymonosulfate activation†

Feng Song, a Huayang Zhang, b Shaobin Wang, b,∗ Lihong Liu, a,∗b Xiaoyao Tan c and Shaomin Liu a,b

We report a strategy for simultaneous cobalt removal and organic waste decomposition by using mesoporous hydroxyapatite nanoparticles wrapped in uniform carbon layers (HA@C). The in situ formation of CoOH⁺–HA@C due to ion exchange greatly improved the degradation efficiency by at least one order of magnitude compared to free Co³⁺.

Toxic heavy metal ions discharged mostly from the foundry and mining industries have underlined the high importance of wastewater treatment. Recent technologies for heavy metal elimination include chemical precipitation, adsorption, ion-exchange, membrane filtration and electrochemical deposition. Among them, adsorption using certain solids to capture specific ions from solutions is widely accepted due to easy operation. For example, hydroxyapatite (HA), with an empirical formula of Ca₁₀(PO₄)₆(OH)₂, has been extensively studied to immobilize many divalent heavy metal ions in wastewater and even in the human body. The stabilization mechanisms of Pb²⁺, Zn²⁺, Co²⁺, Cd²⁺, Cu²⁺, Hg²⁺ and Ni²⁺ on HA involve dissolution–precipitation, ion-exchange, surface complexation and coprecipitation. Although previous techniques work well for simple heavy metal removal, approaches for in situ reuse of the captured metal ions are very limited.

Traditional methods for the synthesis of HA nanoparticles are solid-state reactions, precipitation, sol–gel techniques, electrospinning synthesis, electrodeposition, hydrothermal reactions, and so on. In the past few decades, advancements in biotechnology have led to many sustainable ways to prepare nanomaterials with plant extracts or microorganisms. Several studies have shown that Serratia sp. bacteria derived HA exhibited superior sorption for the removal of Sr²⁺ and Co²⁺. Recently, our research group has simplified the microbial process by using Yeast Mold Broth (YMB) to implement fine control over the carbon- and silver-modified hierarchical ZnO formation. YMB powder has 47.6% dextrose (β-glucose) that can be used as a carbon source. In the present study, we report the synthesis of HA nanorods ([HA@C] with a mesoporous core and a uniform carbon shell structure. The HA@C nanocomposite could effectively remove Co²⁺ from aqueous solution, for instance 83% Co²⁺ removal efficiency from 6 ppm aqueous solution. To make the wastewater treatment process more economical, we propose to use the captured Co²⁺ for further advanced oxidation of organic pollutants via peroxymonosulfate (PMS) decomposition and the subsequently produced more potent radicals. The detailed mechanism of PMS activation by cobalt is generally proposed as follows.

\[
\begin{align*}
\text{Co}^{2+} + \text{H}_2\text{O} & \rightarrow \text{CoOH}^+ + \text{H}^+ \\
\text{CoOH}^+ + \text{HSO}_5^- & \rightarrow \text{CoO}^- + \text{SO}_4^{2-} + \text{H}_2\text{O} \\
\text{SO}_4^{2-} + \text{organics} & \rightarrow \text{intermediate products} \rightarrow \text{CO}_2 + \text{H}_2\text{O}
\end{align*}
\]

CoOH⁺ is one of the most effective species to activate PMS. Thus, the formation of CoOH⁺ is considered as the rate-limiting step in the process. To facilitate the generation of Co–OH complexes, Yang et al. immobilized Co₃O₄ onto TiO₂ nanoparticles. The obtained Co/TiO₂ catalyst demonstrated greatly enhanced heterogeneous PMS activation, due to the ability of TiO₂ to dissociate H₂O for surface hydroxyl group generation.

The HA crystal consists of hydroxyl groups positioned in the channel along the (001) direction. Therefore, in Co²⁺ adsorption, Ca³⁺ replacement by Co²⁺ could result in ready formation of CoOH⁺, which has a high potential function as the PMS catalytic active center. Our experimental results indicate that Co²⁺ substituted HA@C/PMS ([Co²⁺] = 1 ppm) completely decomposed methylene blue in 1 min, while it took 45 min in a homogeneous Co³⁺/PMS system. Electron paramagnetic resonance (EPR) and quenching studies reveal that SO₄•⁻, •OH and O₂ participated in the advanced oxidation process.
X-ray diffraction (XRD) patterns of the synthesized samples are presented in Fig. S1a (ESI†). At room temperature, bare HA particles with poor crystallinity were formed after 20 h. It is clear that the sample 4 × 180 °C 5 h HA (with a molar ratio of KH₂PO₄/dextrose = 4, hydrothermal treatment at 180 °C for 5 h) has intense diffraction peaks that match well with the standard data of JCPDS Card No. 09-0432. The sharp peaks located at 2θ = 26.0, 31.8, 32.2, 32.9, 39.9, and 46.7° can be indexed to the (002), (211), (112), (300), (310) and (222) planes of HA, respectively.²⁷–²⁹ All the samples prepared at 120 °C have similar characteristic peaks, though in relatively broader widths. The XRD patterns confirmed that predominately HA rather than other calcium phosphates has been obtained.³⁰ Fig. S1b (ESI†) shows the absorption bands at ca. 560, 599 and 960 cm⁻¹ corresponding to the vibration of PO₄³⁻ groups in HA.²⁷,³⁰ The IR peak for the hydroxyl groups of HA is observed at around 3628 cm⁻¹. For X-ray photoelectron spectroscopy (XPS) characterization, two peaks with binding energies of 437 and 346 eV are in agreement with the characteristics of Ca 2s and Ca 2p. The peaks near 190 and 132 eV are attributed to P 2s and P 2p, respectively.²⁹ The two peaks near 346 and 350 eV are attributed to the Ca 2p₁/₂ and Ca 2p₃/₂ bands of HA. The O 1s peaks near 530 and 532 eV are associated with the phosphate group in HA and adsorbed water, respectively.

Fig. 1a shows the typical rod-like morphology of 4 × 180 °C 5 h HA nanoparticles with numerous mesopores around 2–3 nm. It can be seen that the nanorod is approximately 20–30 nm in width, with a length varying between 30 and 100 nm. The interplanar spacings of ca. 0.81, 0.27 and 0.34 nm obtained from the HRTEM images were ascribed to the adjacent (100), (112) and (002) planes of HA NPs, respectively.³⁰–³⁴ Additionally, the particles are found to be covered with a uniform layer of amorphous carbon. The thickness of the carbon shell is about 10 nm (Fig. 1c). Important advantages of this structure over bare HA NPs are stabilization and introduction of a C source for PMS activation, which will be discussed later.

Zeta potential measurements of bare HA particles had a range around −36 to −25 mV.³⁵,³⁶ The surface charge of HA@C was approximately −11 mV in this study. The carbon layer may interfere with the OH⁻ in attracting counter ions thus leading to the variation. HA@C NPs were observed to settle gradually over the time course of hours. In terms of operation cost reduction, HA@C may be preferred over highly stable HA NPs in avoiding additional catalyst separation, e.g., centrifugation. Nevertheless, they can be re-dispersed well by just hand shaking and show a high capacity in adsorption of cationic ions.

Fig. S2 (ESI†) depicts the N₂ adsorption-desorption isotherm and the Barrett-Joyner-Halenda (BJH) pore size distribution of HA@C NPs. The isotherm is of type IV with a steep H₃ hysteresis loop occurring in the range of p/p₀ = 0.8–1.0, indicating the existence of irregular mesopores. The specific surface area, adsorption cumulative pore volume, and average pore diameter were found to be 88 m² g⁻¹, 0.41 cm³ g⁻¹, and 18.8 nm, respectively. These values are comparable to previous studies.³⁷

The adsorption and catalytic performance of HA@C NPs are shown in Fig. 2a. PMS itself oxidized 30% MB within the examined time. The HA adsorption capacities of MB and Co²⁺ are 3.5 and 5.0 mg g⁻¹, respectively. At an initial concentration of 5–6 ppm, the Co²⁺ uptake was almost 10 times higher than multiwalled carbon nanotubes.³⁸ When Co²⁺ was mixed with HA@C first, only 27% of MB was removed due to the competition of cationic metal ions and dye molecules for adsorption sites on HA@C.

Metal-free carbon/PMS have been investigated for pollutant degradation. The sp² carbons and O-containing groups on nanocarbons have demonstrated high efficiency in activating HSO₅⁻ for sulfate radical production.³⁹–⁴² In this study, HA@C/PMS gradually degraded 85% MB, which was higher than HA@C adsorption (37%). This suggests that the amorphous carbon layer could possibly activate PMS for MB decomposition.

After Co²⁺ loading, CoHA@C (0.2 g L⁻¹) could activate PMS and completely decolorized MB in 1 min. The system maintained the similar performance from pH 5 to pH 6.5 (Fig. S3, ESI†). This rate was even faster than the homogeneous process, as it took 45, 10 and 6 min for 1, 4 and 6 ppm free Co²⁺ to remove MB, respectively. To exclude the possibility of MB degradation by leached Co²⁺, we measured the [Co²⁺] in the supernatant using ICP-OES. Fig. 2c shows free [Co²⁺] decreasing from 0.8 to 0.4 ppm after the fourth reaction. Catalyst reusability tests were performed by conducting 4 rounds of the reaction. Although it took longer time, 100% MB removal could be achieved within 2 min in the fourth cycle. The decline in the degradation rate may be caused by the consumption of Co²⁺ attached on the carbon layer after the first reaction. However, the surface negative HA core has attracted and accommodated well to Co²⁺ for continuous PMS activation.

In most cases, SO₄²⁻ is accepted as the major oxidizing agent in Co/PMS AOPs. In order to identify the dominating
oxidizing species responsible for MB decontamination, EPR experiments were performed to detect the reactive oxygen species (ROSs) during PMS activation. As shown in Fig. 3a, 1 g L\(^{-1}\) Co\(\text{HA}@C\), 0.1, 0.2, and 1.0 g L\(^{-1}\) Co\(\text{HA}@C\) (corresponding to [Co\(^{2+}\)] of 0.5, 1, and 5 ppm, respectively), 0.24 g L\(^{-1}\) PMS (0.4 mM), pH 5.5, 25 °C.

Ethanol is a widely used scavenger of SO\(_4^{\bullet-}\) and \(\bullet OH\).\(^{43}\) To further verify the existence of the radicals, quenching experiments were conducted by adding ethanol (ethanol:PMS = 1000) and NaNO\(_2\) (3 mM) into the suspension for more efficient quenching of radicals. The degradation rate was notably inhibited as no MB decolorization was observed within 10 min, thus proving that the sulfate radical, hydroxyl radical and singlet oxygen indeed play key roles in the Co\(\text{HA}@C\)/PMS oxidation.

Considering the crystalline structure of HA, a mechanism for MB decomposition in the Co\(\text{HA}@C\)/PMS system was proposed as follows. Co\(^{2+}\) adsorption occurs due to ion exchange with Ca\(^{2+}\) in the surface groups of HA and also within the HA crystals. As depicted in Fig. 4, between the two Ca sites in the unit cell of crystalline HA, where metal ion exchange may happen, the Ca-2 site is normally replaced by Co\(^{2+}\).\(^{44}\) The Co\(^{2+}\) reacts with the adjacent OH\(^-\) to form CoOH\(^+\), resulting in the most efficient catalyst for PMS decomposition. Additionally, an array of PO\(_4^{3-}\) facilitated by CoOH\(^+\) and the nucleophile tetrahedral PO\(_4\).
tetrahedra may act as the nucleophile (Nu) polyphosphate in PMS self-decomposition to generate $^{1}O_{2}$:\textsuperscript{45}

\[
\text{HOSO}_{3}^{-} + \text{Nu} \rightarrow \text{NuOH}^{+} + \text{SO}_{4}^{2-}
\] \hspace{1cm} (4)

\[
\text{HOSO}_{3}^{-} + \text{NuOH}^{+} \rightarrow \text{SO}_{4}^{2-}/\text{HSO}_{4}^{-} + ^{1}O_{2} + \text{Nu} + H^{+}
\] \hspace{1cm} (5)

$^{1}O_{2}$ + methylene blue $\rightarrow$ intermediates + CO$_{2}$ + H$_{2}$O \hspace{1cm} (6)

In EPR characterizations, 6 ppm free Co$^{2+}$ produced stronger radical intensities, but with less efficiency than that of 5 ppm CoHA@C. This could be explained by the radial confinement inside the nanopores of mesoporous HA. Wang et al. prepared nitrogen-doped reduced graphene oxide and investigated its bisphenol elimination efficiency.\textsuperscript{46} By employing methanol and KI as radical scavengers, they confirmed that the surface-bound $\text{SO}_{4}^{2-}$ played a dominant role and only a minimal amount of free $\text{SO}_{4}^{2-}$ was generated in the AOP. Similarly, in our system, the adsorbed MB molecules were firstly degraded by various confined radicals. After releasing the occupied sites, a new adsorption–degradation of MB started again until all MB was decomposed.

In summary, a facile method is established for the bioinspired synthesis of hydroxyapatite nanorods with mesoporous structures and uniform carbon shells. The resultant HA@C composite is stable and efficient in adsorbing Co$^{2+}$ from wastewater. At [Co] $= 1.0$ ppm, the \textit{in situ} formed Co–OH complexes greatly reduce the dye degradation time by a factor of 45 compared to the conventional PMS activation by free Co$^{2+}$. The $\text{SO}_{4}^{2-}$, $\text{•OH}$ and $^{1}O_{2}$ are experimentally confirmed to play a vital role in the AOPs. The ultrafast decontamination rate and excellent reusability make the system a promising candidate for sustainable wastewater treatment.

Conflicts of interest

There are no conflicts to declare.

Notes and references

1. F. Fu and Q. Wang, \textit{J. Environ. Manage.}, 2011, 92, 407.
2. A. Azimi, A. Azari, M. Rezakazemi and M. Ansarpour, \textit{ChemBioEng Rev.}, 2017, 4, 37.
3. M. Vila, S. Sánchez-Salcedo and M. Vallet-Regí, \textit{Inorg. Chim. Acta}, 2012, 393, 24.
4. M. Vila, S. Sánchez-Salcedo, M. Cucíñdez, I. Izquierdo-Barba and M. Vallet-Regí, \textit{J. Hazard. Mater.}, 2011, 192, 71.
5. E. Movapoulos, A. Malta Rossi and A. M. Costa, \textit{Environ. Sci. Technol.}, 2002, 36, 1625.
6. G. Liu, J. W. Talley, C. Na, S. L. Larson and L. G. Wolfe, \textit{Environ. Sci. Technol.}, 2010, 44, 1366.
7. M. Okada and T. Furuozono, \textit{Sci. Technol. Adv. Mater.}, 2012, 13, 064103.
8. H. Peng, J. Wang, S. Lv, J. Wen and J. Chen, \textit{Ceram. Int.}, 2015, 41, 14340.

ChemComm