A review on biodiesel production from microalgae: Influencing parameters and recent advanced technologies

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Microalgae are the important part of carbon cycle in the nature, and they could utilize the carbon resource in water and soil efficiently. The abilities of microalgae to mitigate CO\textsubscript{2} emission and produce oil with a high productivity have been proven. Hence, this third-generation biodiesel should be popularized. This review firstly introduce the basic characteristics and application fields of microalgae. Then, the influencing parameters and recent advanced technologies for the microalgae biodiesel production have been discussed. In influencing parameters for biodiesel production section, the factors of microalgae cultivation, lipid accumulation, microalgae harvesting, and lipid extraction have been summarized. In recent advanced technologies for biodiesel production section, the microalgae cultivation systems, lipid induction technologies, microalgae harvesting technologies, and lipid extraction technologies have been reviewed. This review aims to provide useful information to help future development of efficient and commercially viable technology for microalgae-based biodiesel production.

KEYWORDS
microalgae cultivation, microalgae harvesting, lipid accumulation, lipid extraction, biodiesel

Introduction

The consumption of fossil energy has been on the rise following the rapid development of the society, leading to reduced fossil energy resource reserves and causing severe deterioration of the natural environment (Zhang S. et al., 2020). International efforts to achieve carbon neutrality urgently necessitate the development of new clean energy sources to replace fossil energy (Hou et al., 2021). Biodiesel, produced by renewable resources such as vegetable oil or animal fat, is a new clean and alternative to diesel fuel. This renewable resource primarily consists of esters formed by methanol or ethanol and long-chain saturated and unsaturated fatty acids such as palmitic acid,
stearic acid, oleic acid, and linoleic acid (Šalić et al., 2020). Therefore, the research and development of biodiesel has attracted the attention of scholars worldwide.

The development of biodiesel can be divided into three stages (Figure 1). First-generation biodiesel was prepared using edible crops such as corn, soybean, and sugarcane as raw materials. These materials exhibited low yield and consumed copious amounts of water and land resources, thus straining the resources required for societal sustenance (Li and Guo, 2017). Second-generation biodiesel was mainly produced using lignocellulose, such as straw, hay, and other non-foods, as raw material. Although the production of this generation of biodiesel addressed the limitations of production associated with first-generation biodiesel, it was costly and provided low calorific value owing to the features and collection cost of lignocellulose. Third-generation biodiesel is produced from microalgae, which produce lipid through carbon fixation during photosynthesis and have a yield of lipid up to 70%. In addition, microalgae live in water, and it does not occupy farmland. They also exhibit a short growth cycle and high yield, and their consumption does not threaten human food supply. These advantages of microalgae make it optimal alternative raw material for biodiesel production.

Biodiesel production from microalgae entails reusing and integrating carbon resources from the natural environment, which can contribute to achieving the long-term goal of replacing petroleum use and reducing environmental pollution, thereby contributing significantly to the global carbon neutrality endeavor. Hence, we aimed to review the key technologies of biodiesel production from microalgae in this work, and the schematic diagram of main content is shown in Figure 2.

Characteristics of microalgae

Basic characteristics

Microalgae is microscopic and unicellular microorganisms that have been living on the earth through prolonged geological ages. The photosynthetic mechanism of microalgae is similar to that of plants. Owing to its simple structure, it can efficiently obtain water, carbon dioxide, and other nutrients when submerged in water, thus allowing them to convert solar energy into biomass resources. Generally, microalgae are categorized as freshwater and marine microalgae based on their living environment, among which freshwater microalgae are widely distributed in nature, including rivers, lakes, reservoirs, creeks, ponds, marshes, and soils (Singh et al., 2020). Microalgae have been used in numerous fields (Figure 3), such as food, cosmetics, aquaculture, environmental testing, wastewater treatment, and energy.

As a bioenergy source, microalgae exhibit high photosynthetic efficiency and high yields of biomass and lipid with few environmental restrictions. Microalgae can
live on non-arable land, such as beaches, saline and alkali soils, and deserts, and it could also grow in wastewater and seawater (Zada et al., 2021). In addition, microalgae exhibit remarkable performance in terms of carbon fixation (Zeng et al., 2021). At a growth rate of 25 g/d, microalgae can fix 12 tons of CO₂ per acre per year. The differences in biomass yield, lipid/fat yield, land use, and biodiesel yield among various crops are presented in Table 1. It indicates that microalgae clearly surpass other crops in all aspects. Therefore, microalgae are the most promising alternatives to replace fossil fuels. The lipid in microalgae or the whole microalgae cell can be utilized to produce gaseous fuels such as hydrogen and biogas, or liquid fuels such as ethanol and liquid hydrocarbon fuels (Sanghamitra et al., 2020). Therefore, the development of microalgae biomass energy at this stage includes biodiesel production from microalgae lipid by transesterification (Vignesh et al., 2021), methane production by anaerobic digestion (Qi et al., 2017), and production of hydrocarbon or crude oil-like substances by gasification and pyrolysis (Su et al., 2022; Figure 4).

Biodiesel production from lipid in microalgae through transesterification is characterized by the advantages of high growth rate and lipid yield, tolerance to environmental stress, and low competition for land (Ebhodaghe et al., 2022). Compared with that of traditional diesel, the performance of biodiesel is superior in several aspects: (1) Biodiesel is extracted from vegetable and animal oils and fats, and is therefore renewable. (2) It contains relatively low sulfur and nitrogen content, thereby reducing SO₂ and nitrogen oxide emissions. (3) It also has a high flash point and high combustion performance and efficiency, is not prone to explosion, and is safe to use. (4) It also exhibits adequate performance at low temperature and lubrication. These advantages accord it remarkable application prospects in various fields.

### Table 1: Comparison of microalgae with other feedstocks.

| Plant name       | Lipid content (%) | Lipid yield (L/ha-year) | Land use (m²·year/kg·biodiesel) | Biodiesel yield (kg/ha-year) |
|------------------|-------------------|-------------------------|---------------------------------|-----------------------------|
| Corn             | 44                | 172                     | 66                              | 152                         |
| Cannabis         | 33                | 363                     | 31                              | 321                         |
| Soybeans         | 18                | 636                     | 18                              | 562                         |
| Jatropha         | 28                | 741                     | 15                              | 656                         |
| Camelina         | 42                | 915                     | 12                              | 809                         |
| Canola           | 41                | 974                     | 12                              | 862                         |
| Sunflower        | 40                | 1,070                   | 11                              | 946                         |
| Castor           | 48                | 1,307                   | 9                               | 1,156                       |
| Palm             | 36                | 5,366                   | 2                               | 4,747                       |
| Microalgae (low lipid content) | 30 | 58,700 | 0.2 | 51,927 |
| Microalgae (medium lipid content) | 50 | 97,800 | 0.1 | 86,515 |
| Microalgae (high lipid content) | 70 | 126,900 | 0.1 | 121,104 |

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Lipid metabolic pathways in microalgae

In microalgae cell, the synthesis of fatty acid usually occurs in the plastids, and the synthesis of triacylglyceride (TAG) would occur in both of chloroplasts and endoplasmic reticulum (Figure 5). In contrast to phospholipids in biological membranes, TAG does not have structural roles in cells and are used to store energy and carbon. In microalgae cells, two main TAG synthesis pathways exist: the Kennedy pathway and the Monoacylglycerol pathway. In these two pathways, TAG is synthesized through esterification between acetyl-CoA and hydroxyl groups on glycerol. The biosynthesis of fatty acids begins with the carboxylation of acetyl-CoA and acetyl-CoA carboxylase (ACCase)-mediated catalysis to form malonyl-CoA. ACCase is a critical control factor in fatty acid
synthesis. In microalgae cells, malonyl-CoA is first transferred to the acyl carrier protein (ACP), and then undergoes a series of acyl chain-elongation reactions. Finally, the C16 or C18 products are catalytically synthesized by multiple subunits of fatty acid synthases. The elongation of fatty acids is terminated by two types of enzymes. First, the acyl groups in the chloroplast acyltransferase are removed by ACP, and the newly synthesized fatty acid is directly transferred from ACP to glycerol-3-phosphate (G-3-P). Second, acyl-ACP thioesterase hydrolyzes acyl-ACP and releases free fatty acids. Free fatty acids are transferred out of the chloroplast to generate glycerides.

In the Kennedy pathway, the first acyl group is esterified to glycerol-3-phosphate (Reddy et al., 2010). Phospholipid synthesis occurs in the second reaction. Before conversion to the TAG, phospholipid is dephosphorylated to diacylglycerol (DAG) by phosphatase enzyme. The Monoacylglycerol pathway starts with 2-monoyacylglycerol (sn2-MAG), which is converted to DAG by monoacylglycerol 2 acyltransferase (MGAT). The synthesized DAG is converted to TAG through catalysis by acyl-CoA: DAG acyltransferase, and this is an important step in TAG biosynthesis.

In another potential pathway for TAG synthesis catalyzed by phospholipid: diacylglycerol acyltransferase (PDAT), phospholipid or galactolipid acts as the acyl donor (Dahlqvist et al., 2000). Some plants have been shown to have PDAT activity, however its contribution in TAG synthesis differs between different plants. The PDAT encoding gene has been identified in microalgae, proving that an acetyl-CoA-independent mechanism for TAG synthesis exists in microalgae. Fatty acid methyl esters (biodiesel) are produced through TAG transesterification (Figure 6).

Parameters for biodiesel production

Researches on biodiesel produced from microalgae mainly focus on the production process, which primarily encompasses the upstream process involving microalgae cultivation (growth and lipid accumulation) and the downstream process including microalgae harvesting and lipid extraction (Figure 7). The technology of converting lipid to biodiesel is well established and requires no in-depth discussion in this study. The precursor material of biodiesel—the lipid—is currently research focus. The fatty acid components in microalgal lipid play a crucial role in the quality of biodiesel, which in turn affects the combustion efficiency and heating power of the engine. Under certain stresses, microalgae produce lipids primarily consisting of neutral fatty acids with a low degree of saturation (no more than two unsaturated bonds in most cases), thus confirming the applicability of biodiesel produced from microalgae and its potential to partially replace fossil fuels (Song et al., 2022). Biodiesel exhibits remarkable portability, ready availability, renewability, high combustion efficiency, low sulfur and aromatic content, high cetane number, and adequate biodegradability. It also exhibits more optimized performance in terms of safety and energy balance ratio than regular diesel fuels. The factors affecting each stage of the microalgal biodiesel production process are detailed below (Chhandama et al., 2021).

Microalgae cultivation

Microalgae cultivation can directly affect the yield of lipid. Various factors such as light, carbon sources, nutrients (e.g.,
nitrates, phosphates, and carbohydrates), and trace elements (e.g., Mn, Co, Zn, and Mo) influence the growth of microalgae (Aziz et al., 2020). Additional influencing factors include temperature, pH, O₂ removal, and CO₂ uptake. The comparison of the parameters on microalgae cultivation is in Table 2.

Light

Generally, photosynthesis reaction comprises light reaction and dark reaction. In the light reaction phase, light energy is captured and converted into an energy carrier and then oxygen is released as a by-product (Sung et al., 2022). The electrons provided by oxygen can be transferred to photosystem I (PSI) and photosystem II (PSII) (Ranadheer et al., 2019). High-intensity light can lead to the photo-oxidation of PSII components, reducing the productivity of microalgae (Arun et al., 2021). While, low intensity light is not sufficient for the growth of microalgae. Therefore, an ideal light intensity is one of the essential parameters of the growth of microalgae, and microalgae usually absorb and use natural light with wavelengths ranging from 400 to 700 nm (~43% of solar energy) (Teo et al., 2014).

Temperature

Temperature is an important parameter affecting microalgal growth. High temperature promotes the uptake and fixation of CO₂ by microalgae, while excessively high temperature inhibits the respiratory metabolism of microalgae (Barten et al., 2021). The optimum growth temperature varies for different species of microalgae, but typically ranges from 20–30°C. Some freshwater microalgae can adapt to a broad range of temperature (5–35°C); however, in large-scale culture, the temperature must be restored to the ideal range (25–30°C) (Zhong et al., 2022). Therefore, temperature should be maintained at the optimal state for microalgal growth to prevent adverse effects on the metabolism of microalgae cells and reduction of lipid accumulation.

Salinity, nutrients, and pH

The optimum conditions for salinity, nutrients, and pH depend on the type of microalgae. Optimum salinity conditions are required for the healthy growth of microalgae. Salinity in the culture medium can be increased by adding NaCl and Na₂SO₄, while high salinity usually inhibits microalgal growth. Different species of microalgae have different salinity requirements. For instance, marine microalgae can tolerate higher salinity condition than freshwater microalgae (Maity and Mallick, 2022).

In addition, various nutrients are crucial for the growth of microalgae, including C, O₂, H₂, N, K, Mg, Ca, Fe, S, and P. The most important nutrients are C, O₂, H₂, N, P, and K, with C, O₂, and H₂ obtained from water and air and N, P, and K acquired from the culture medium (Chew et al., 2018; Wang et al., 2018). The main nutrient elements required for the growth of microalgae are N and P, and special types of microalgae also need some specific elements, such as Si element for Diatoms.

The pH in the culture medium also plays an important role in microalgal growth, which regulates enzyme activity, phosphorus availability, ammonia toxicity, and inorganic carbon availability. As microalgae grow, the pH gradually increases, and the culture medium becomes alkaline. As photosynthesis intensifies, OH⁻ ions gradually accumulate and microalgae readily capture CO₂ from the atmosphere for conversion to biomass (Isiramen et al., 2022). Conversely, changes in pH affect the permeability of microalgal cell and the form of hydrated hydrogen ions of inorganic compounds.

Cultivation modes

In autotrophic mode, microalgae utilizes light and inorganic materials (CO₂, water, and inorganic salts) for photosynthesis and synthesize organic materials (Ruiz et al., 2022). In heterotrophic mode, microalgae utilizes external carbon sources to grow in a dark environment. In microalgae mode, microalgae is provided with both CO₂ and organic carbon sources. Compared with those in autotrophic mode, the yields of biomass and lipid in mixotrophic mode were significantly higher. In mixotrophic mode, the cell division of microalgae is also rapid. CO₂ is one of the factors influencing the photosynthesis of microalgae; the increase in CO₂ is beneficial for the improvement of the photosynthetic efficiency of microalgae, thereby increasing their biomass yield (Cheng et al., 2022).

Lipid accumulation

The biological activity of microalgae is highly dependent on the culture conditions, and nutrients, carbon source, salinity, light, temperature, and metal ions all impact the lipid accumulation (Ma et al., 2022).

Nutrients

Nitrogen (N) is an important element impacting the cell structure of microalgae because it is essential in the synthesis of proteins, amino acids, nucleic acids, enzymes, and photosynthetic pigments (Gao et al., 2019). Phosphorus (P) is one of the most important nutritional elements that regulate cell growth and metabolism. It plays an important role in most cellular processes, especially in energy transfer, signal transduction, biosynthesis of macromolecules, photosynthesis, and respiration processes (Wu et al., 2021). Phosphatase converts organic phosphates into orthophosphate on the cell surface and microalgae take up phosphorus in the form of inorganic phosphate. In the presence of sufficient phosphorus, microalgae take up excessive phosphorus in the form of polyphosphate particles, and they can grow in the absence of phosphorus using stored phosphorus (Zhang et al., 2021).
### TABLE 2: Comparison of the mainly parameters and technologies for biodiesel production.

| Main parameters | Factors | Microalgae type | Lipid content | Biomass growth/Productivity |
|-----------------|---------|----------------|---------------|-----------------------------|
| Microalgae cultivation | Light | Chlorella sp. | 2700 lx | 19.44% | 1.05/d |
| | | Chlorella vulgaris | 520 mmol/m² s | 22.2% | 0.56/d |
| | Temperature | Chlorella vulgaris | 25 °C | 14.7% | 0.14/d |
| | | Chaetoceros sp. | 25 °C | 16.8% | 0.87/d |
| | pH | Chlorella sp. | 8 | 23% | 0.1995 g/L |
| | | Chlorella pyrenoidosa | 7 | 30.9% | 1.41 g/L |

| Main parameters | Factors | Microalgae type | Wastewater type | Lipid content | Biomass Growth/Productivity |
|-----------------|---------|----------------|----------------|---------------|-----------------------------|
| Microalgae cultivation systems | Agricultural wastewater | Chlorella sorokiniana | BBM | – | 0.25/d |
| | | Chlorella sorokiniana | POME | – | 0.23/d |
| | Industrial wastewater | Scenedesmus sp. | Diluted swine w | 17.19% | 0.40 g/L |
| | | Chlorella vulgaris | Tofu wastewater | 23.25% | 0.8 g/L |

| Lipid induction technologies | Factors | Microalgae type | Optimum conditions | Lipid intensity/ Productivity | Effects of variation on lipid productivity/content |
|-----------------------------|---------|----------------|-------------------|-----------------------------|--------------------------------------------------|
| Nutrient starvation stress  | Chlorodinium i | 2.9 mM Nitrates | Lipid productivity 3.51 ± 0.16 mg/L/d | Lipid productivity 4.73 ± 0.12 mg/L/d, 40.37 ± 1.01% increase in lipid yield L/day |
| | Chlorodinium saccharophillum | 0.5 mM Phosphate | Lipid productivity 2.31 ± 0.62 mg/L/d | Lipid productivity 3.96 ± 1.04 mg/L/d, 33.57 ± 3.72% increase in lipid yield L/day |
| Salinity stress | Chlorodinium saccharophillum | 10 mM NaCl | Lipid productivity 1.78 ± 0.32 Mg/L/d | Lipid productivity 4.70 ± 0.24 mg/L/d, 40.18 ± 1.97% increase in lipid yield L/day |
| | Chromochloris zofingiensis | 0.25 M NaCl | Lipid content 13 mg/g DW | Lipid content 195 mg/g DW, 15-fold increase in TAG content |
| Light stress | Chromochloris zofingiensis | 400 µE/m² s | Lipid content 13 mg/g DW | Lipid content 195 mg/g DW, 15-fold increase in TAG content |
| | Chlorella sp. | 40 µmol/m² s | – | Higher lipid content of 17.2% achieved |
| Temperature stress | Gracilariaopsis lemaneiformis | High temperature 33 °C | Lipid intensity 5 × E10 | Lipid intensity 7 × E10, Increase in C20:5 fatty acid by 88%, PUFA improved |
| | Porosira glacialis | 2 °C | Lipid content 19.5% | Lipid content peaked at 33.4 ± 4.0% |
| Carbon dioxide supplementation | Nannochloropsis sp. | 5% CO₂ concentration | Lipid production 112.91 ± 17.34 | Maximum lipid production of 782.7 ± 24.49 mg L⁻¹ attained |
| | Arthrospira ZJU9000 | 171.2 mM HCO₃⁻ Concentration | Lipid content 9.5 (Wt%) | 3.8-fold higher expression of gene encoding ATP-synthase. |

| Microalgae harvesting | Technique | Microalgae type | Operating conditions | Recovery efficiency |
|-----------------------|-----------|----------------|---------------------|---------------------|
| Chemical flocculation (Self-floculation) | Chlorella vulgaris | pH adjustment, NaOH, V = 30 L, pH = 10.8, HM = batch, CD = 9 mg/g | pH adjustment, Cat(OH)₂, | 98% Dries et al., 2011 |

(Continued)
| Microalgae harvesting | Technique | Microalgae type | Operating conditions | Recovery efficiency |
|-----------------------|-----------|----------------|----------------------|---------------------|
| Ca(OH)₂, V = 30 L; pH = 10.8; HM = batch; CD = 18 mg/g pH adjustment, Mg(OH)₂, V = 30 L; pH = 9.7; HM = batch; CD = 27 mg/g | Chlorella sp. | P: Polycrylamide; C: High; S: 1000; FD: 34; T: 60 | 98% | Arivalagan et al., 2019 |
| Mg(OH)₂, V = 30 L; pH = 9.7; HM = batch; CD = 27 mg/g | Chlorella vulgaris | P: Polycrylamide; MW: High; C: High; D: 0.26; S: 3000; FD: 3; T: 30 | 100% | |
| Bio-flocculation | Chlorella sp. | pH = 8, chitosan concentration: 180 mg/500 mL, cationic inducer concentration: 50 mg/L, stirring speed: 240 rpm | 96.12% | Hadiyanto et al., 2022 |
| Chlorella pyenoidosa | Citrobacter W4; bacterial-algal ratio: 4:1, G value: 26.30 s⁻¹, harvesting time: 6 h | Citrobacter pyenoidosa | 87.37 ± 2.96% | He et al., 2022 |
| Flotation | Asterionella formosa | Aluminum sulfate: 0.0314 ng Al/cell, pH = 7, Flotation time: 10 min | 98.9% | Henderson et al., 2008a |
| Scenedesmus quadricauda | CTAB: 40 mg/L, pH = 8, Flotation time: 20 min | 90% | Chen et al., 1998 |
| Chlorella vulgaris | CTAB: 0.005 mequiv/L, pH = 7, Flotation time: 10 min | 54% | Henderson et al., 2008b |
| Chlorella | Ferric sulfate: 3.5 mg Fe/L, pH = 5.5, Flotation time: 10 min | 94% | Jarvis et al., 2009 |
| Filtration | M. aerugiosa | CPAM-assisted filtration with a 100-µm sieve | 90% | Cai et al., 2022 |
| Chlorella vulgaris | CF: 78 L/m² h, F: 3 Hz | 68.8% | Zhao et al., 2020 |
| Centrifugation | Chlorella sp. | Duk-stack centrifuge: 15 min | 93% | Abhishek et al., 2016 |
| Chlorella vulgaris | Decanter centrifuges, Energy consumption: 8 kWh/m³, Final slurry Concentration: 22.2% | 92% | Wiley and Campbell, 2011 |
Salinity
Salinity significantly affects the lipid accumulation in microalgae, which not only influences its growth but also resists infection by microorganisms such as bacteria. High salinity leads to increased intracellular osmotic pressure, entailing responses from physiological and biochemical mechanisms (Yang et al., 2022). High salinity impacts the fluidity and permeability of the microalgal cell membrane, under which the entry and exit of ions can be regulated through the cell membrane, and the accumulation of osmoprotective solutes as well as stress proteins becomes active. Salinity affects the cell structure and metabolic functions of microalgae and promotes the accumulation of lipid in microalgae (Zafar et al., 2021).

Metal ions
Trace metal elements have significant effects on the growth rate, as well as the accumulation of lipids and carbohydrates in microalgae. The addition of bioavailable Fe^{3+} to the culture medium can increase the growth rate and lipid accumulation in microalgae (Abd El Baky et al., 2012). While both excessively high and low levels inhibit them. High concentration of Mg^{2+} can enhance the activity of acetyl coenzyme A carboxylase (ACCase), thus promoting lipid accumulation (Qian et al., 2021). Ca^{2+} is more critical in the signal transduction to regulate the synthesis of lipids in microalgae (Di Caprio et al., 2018). Heavy metals such as Cd, Cu, and Zn can alter the lipid metabolism in microalgae and promote lipid accumulation (Urrutia et al., 2019).

Temperature
Seasonal temperature fluctuations, daily temperature changes, and sudden temperature changes due to various reasons can unavoidably change the growth conditions of microalgae, thus affecting its growth efficiency (Xin et al., 2011). Temperature changes impact the metabolic pathways of microalgae, with both high and low temperature stresses promoting lipid accumulation in microalgae (Rehman et al., 2022).

Light
Microalgae is photosynthetic organism and light is essential for its growth. However, microalgae can only absorb a small fraction of the natural light with a wavelength range of 400–700 nm (~43% of solar energy) (Yan et al., 2016). So light with the appropriate wavelength and intensity is the key factor that influences or even controls the growth and lipid accumulation of microalgae.

Microalgae harvesting
Microalgae harvesting, the separation of microalgae from the culture medium, is the main problem in the downstream process of microalgal biodiesel production. Excessively high microalgal concentration leads to overshadowing and results in insufficient light and consequently lower productivity. Hence, the biomass concentration of microalgae in culture medium is generally maintained at a low level (0.5–5 g/L), which means that a large amount of water needs to be removed to harvest microalgae (Liu et al., 2018). Microalgae harvesting is further complicated by their small cell size (2–20 μm) and stable colloid in the suspension. Hence, the sedimentation efficiency of microalgae cell is a function of the microalgal cell size, cation concentration in the culture medium, and extracellular secretions of the microalgal cell (Ortiz et al., 2021).

Cell size
Currently, the studies on flocculation of microalgae focus on single species cultured under specific conditions. Flocculation depends mainly on the surface properties of the microalgae cell, which vary according to the species and culture conditions. The specific surface area of the microalgal cell increases as the cell size decreases (Min et al., 2022). Therefore, the smaller the microalgal cell, the higher the flocculant dose required. Meanwhile, relatively large microalgal cell favors the sedimentation process.

Cation concentration
Divalent cations (such as Ca^{2+} and Mg^{2+}) and trivalent cations (such as Al^{3+} and Fe^{3+}) influence the flocculation efficiency of microalgae. The latter attach to the negatively charged carboxyl groups on the surface of microalgae and form flocs through charge neutralization, while the former mainly bind to the negatively charged extracellular polymeric substance (EPS) on the microalgal surface cells to promote their self-flocculation (Choi et al., 2020).

pH
pH is an important parameter that needs to be carefully considered. The pH affects the charge on the surface of the microalgal cell and also impacts the charge of chemical flocculants. The negative charge on the surface of the microalgal cell gradually decreases as the pH increases. When the pH exceeds 10, the surface of microalgal cell approaches “zero charge,” and the cell transfers from a homogeneous stable phase to an inhomogeneous unstable phase, leading to their flocculation and sedimentation (Liu J. et al., 2014). However, Mg(OH)_{2}, CaCO_{3}, and Ca_{3}(PO_{4})_{2} also precipitate under higher pH.

CO_{2}
Microalgae consumes CO_{2} through photosynthesis resulting in elevated pH, which could cause self-flocculation. Most commercial microalgae culture units typically rely on CO_{2} to enhance the yield of microalgae. The use of CO_{2} in controlling microalgal self-flocculation is a promising
Microalgal technology, and the CO₂ concentration mechanism (CCM) of microalgae is an important determinant of the effectiveness of microalgae absorption of HCO₃⁻ (Liu G. et al., 2014). Most microalgae have a highly active CO₂ concentration mechanism and can sustain photosynthesis as the pH exceeds 10, which in turn causes microalgae self-flocculation (Tran et al., 2017).

 Extracellular polymeric substance

Flocculation of microalgae is usually accompanied by the production of EPS, which mainly contain proteins, polysaccharides, humic substances, and nucleic acids. In fact, EPS play a crucial role in the flocculation of microalgal cell, which acts as a bridge to connect microalgal cell and produce large aggregates, a phenomenon term as self-flocculation. In addition, extracellular secretions of microalgal cell and metal cations in the culture medium can interact to promote sedimentation of microalgae (Wang et al., 2022). The positively charged metal cations combine with the negatively charged carboxyl groups in the cell wall and the carboxyl and hydroxyl groups in the extracellular secretion to form flocs. The production of extracellular secretions by microalgae is a function of nutrient content, growth stage of microalgae, and external environment (Taghavijeloudar et al., 2021).

Lipid extraction

Microalgae cell wall mainly comprise proteins, cellulose, hemicellulose, and pectin. They are thick and hard, and represent the main challenge for microalgae lipid extraction. The mechanical strength and thickness of microalgae cell wall dictate the ability of microalgae cell to resist mechanical fragmentation (e.g., homogenization under high pressure). Furthermore, the properties of the microalgae cell wall are impacted by external conditions such as salinity, nutrients, and light.

Salinity

Munns et al. (1983) found that when microalgae grown in a high salinity culture medium, the cell wall of Chlorella accounted for up to 70% of the total cell, suggesting that cell wall thickness varied according to the microalgae culture conditions. The building block of their cell wall is cellulose, and the enzymes associated with cellulose synthesis are strongly influenced by salinity (Menegazzo and Fonseca, 2019). However, the effect of salinity on the cell wall components and mechanical strength of microalgae has not been studied.

Nutrients

Although the strength and elasticity of the cell walls of various microalgal species differ, the cell size continues to be an important determinant of cell resistance to rupture in high-pressure homogenizers. It might be the stress response from N-deficient microalgae cells to enhance the resistance to rupture. In addition to thicker cell walls, their average size was also larger than that of N sufficient microalgae cells (Enamala et al., 2018). In N-deficient microalgae cells, cell enlargement increased the susceptibility to cell fragmentation. In addition to cell size and cell wall thickness, factors such as the composition of the cell wall may also contribute to the enhanced susceptibility of microalgae to mechanical fragmentation (Ahmed and Kumar, 2022).

Light

Short-wavelength ultraviolet B (UV-B) and ultraviolet C (UV-C) rays are the most destructive and cause cellular damage. Ultraviolet A (UV-A) is less effective and indirectly damages cells by generating reactive oxygen species that may damage DNA, proteins, and lipids (Kuluncsics et al., 1999). UV-B and UV-C cause direct DNA damage through the absorption of photons by DNA bases, causing chemical quenching and the formation of pyrimidine dimers in the sequence (Rastogi et al., 2010). UV-induced cell lysis is attributed to the uptake of UV radiation by DNA, RNA, proteins, and lipids, resulting in structural damage and signaling/metabolic disruption in the cell. Upon exposure to natural light, DNA damage in algal cells can undergo photo repair through the enzyme cyclobutane pyrimidine dimer photolyase (Rastogi et al., 2010). Microalgae are usually stored in the dark after UV irradiation to reduce photo repair and thus maximize cell damage, as this repair mechanism prevents cell lysis. On an industrial scale, the UV radiation of sufficient intensity can irreparably damage microalgae. UV-B radiation causes the formation of pyrimidine dimers in DNA, which can lead to mutations in the cellular genome. In algal cells, if severe mutation occurs, the cells may lyse upon necrosis or apoptosis, leading to the uncontrollable release of intracellular components. This is also commonly referred to as programmed cell death because of its highly regulated nature and is activated if sufficient DNA mutations occur in specific genes. During apoptosis, cell "package" intracellular components, including lipids, into apoptotic bodies that are released into the culture medium (Sydney et al., 2018).

Technologies for microalgae biodiesel production

With advances in microalgae biodiesel production research, the development of microalgae cultivation systems, lipid induction, microalgae harvesting, and lipid extraction technology have become the hot topics (Chhandama et al., 2021).
Microalgae cultivation systems

Microalgae can grow in different aquatic environments, such as freshwater, seawater, industrial wastewater, agricultural wastewater etc., as long as there are adequate amounts of carbon element (organic or inorganic), nitrogen element (urea, ammonia, or nitrate), phosphorus, and other trace elements (Purba et al., 2022). The utilization of wastewater in large-scale microalgae cultivation for biodiesel production has a vast potential. However, considerable uncertainty and challenges remain in microalgae cultivation using wastewater (Cheah et al., 2016), including changes in wastewater compositions caused by the source, infrastructure, weather conditions, and preprocessing methods; uneven nutrient ratios (e.g., those of N/P and C/N); light transmission affected by high turbidity; presence of competing microorganisms and toxic compounds; and deterioration caused by water recycling and reuse, which leads to the accumulation of growth-inhibiting substances. At present, the utilization of domestic wastewater, agricultural wastewater, and industrial wastewater for microalgae cultivation has been widely studied. The comparison of the microalgae cultivation systems is in Table 2.

Agricultural wastewater

A comparison of the mineral composition between livestock wastewater and microalgae culture medium found that the former is an ideal culture medium for microalgae growth (Wang and Zhang, 2022). In the growth, microalgae can effectively remove N and P from the livestock wastewater. As the nutrient uptake efficiency of some benthic microalgae is significantly higher than that of planktonic microalgae, benthic microalgae are more effective in uptake nutrients from pig manure wastewater (Zhou et al., 2022). However, many problems are still associated with the utilization of livestock wastewater for microalgae cultivation (Arutselvan et al., 2022): (a) The presence of a large amount of solid particles affects the light penetration in the wastewater; (b) Very high levels of nutrients, particularly NH3-N, inhibit microalgae growth; (c) A large amount of carbon source is locked in insoluble organic compounds, which make it difficult for microalgae to absorb; (d) A large volume of freshwater would be consumed to dilute livestock wastewater; and (e) Efficient microalgae strains that are adapted to the adverse environment of livestock wastewater have not yet been developed.

To solve these aforementioned problems, many methods and techniques have been developed and employed. Martin et al. (1985) suggested inoculating high concentrations of microalgae strains in diluted pig manure wastewater (diluted 20–100 times) as a way for treating pig manure wastewater and producing protein-rich microalgal biomass. After a suitable dilution, the NH3-N levels in the livestock wastewater is within the ideal range, which would not inhibit microalgae growth. However, the use of a high dilution factor lowers soluble organic and inorganic carbon levels, which are insufficient to maintain microalgae growth. The addition of exogenous carbon dioxide as an inorganic carbon source helps increase microalgae biomass yield and pollutants removal efficiency. When wastewater with high organic matter content (such as pig and cow manure wastewater) is used for microalgae culture, the trophic mode of the microalgae (autotrophic, heterotrophic, and mixotrophic) is critical in determining the microalgae biomass yield and pollutants removal efficiency.

In summary, screening mixotrophic microalgae strains that are well adapted to wastewater environments, developing preprocessing methods that can effectively improve volatile fatty acid composition, and developing efficient culture systems are methods with the greatest potential for treating livestock wastewater and maximizing microalgae biomass yield.

Industrial wastewater

Currently, research topics in the utilization of industrial wastewater for microalgae culture are focused on the removal of heavy metal pollutants (Cd, Cr, Zn, etc.) and organic toxins (hydrocarbons, biological bactericides, and surfactants) from industrial wastewater and not on biomass accumulation and biodiesel production (Japar et al., 2021). Recently, a microalgae cultivation technique was developed to treat wastewater in oil production. The data from United States Department of Energy shows that 56 million barrels of wastewater are produced every day during the onshore production of petroleum and natural gas in the United States. If this wastewater is used for microalgae culture, and microalgae can reach 1 g/L biomass concentration and 30% lipid content, 700,000 gallons of biodiesel can be produced every day, which accounts for a large part of the existing transportation fuel needs. Notably, the wastewater from the food-processing industry, such as the wastewater from the processing of olive oil and molasses, is in a different category from industrial wastewater, as it lacks heavy metal pollutants and toxic organic matters and is very suitable for microalgae cultivation (Sirohi et al., 2022).

In summary, the utilization of wastewater for microalgae cultivation not only reduces the addition of nutrient, but also decreases the concentrations of nitrogen, phosphorus, and other pollutants in wastewater, which is the main method for decreasing the cost of microalgae cultivation. However, there is no “ideal wastewater” that can provide nutrients similar to artificial culture medium and is suitable for microalgae growth to achieve maximum biomass yield and effective pollutants removal. In this technology, wastewater dilution, sterilization, and
oxidation would consume large amounts of freshwater resources and energy.

**Lipid induction technologies**

To improve the lipid yield of microalgae, effective lipid induction techniques, such as nutrient starvation, salinity stress, light stress, temperature stress, and metal stress, were developed. The comparison of these technologies is in Table 2.

**Nutrient starvation stress**

Nutrient starvation is an economically feasible and environmentally friendly method to increase the yield of lipid in microalgae efficiently. So far, nutrient starvation has been the most successful and widely used technique for lipid induction, and N, P, and S starvation are the most widely used methods for lipid induction of microalgae. Large amounts of lipids in microalgae are produced under N stress, while the amino acid content is significantly decreased (Breuer et al., 2012). Lipid content increased from 10 to 29.5% when *Scenedesmus* was cultured under P stress. S stress can regulate the distribution of carbon element in microalgae to promote the lipid accumulation. Except for N, P, and S starvation, the consumption of nutrient elements during microalgae cultivation is another effective starvation technique for lipid production, because all elements can achieve starvation in the culture medium (Srinuanpan et al., 2018). Carbon fixed through photosynthesis can be used for the synthesis of lipids, proteins, and carbohydrates. N is essential for the protein synthesis, and the limiting N concentration affects cell division and photosynthesis and decreases the growth rate of microalgae cell (Wang et al., 2015). N starvation also affects carbon distribution in microalgae. When N element is sufficient, carbon fixed through photosynthesis is 7–10 times that of the N assimilation rate, which is adequate for the synthesis of N-containing cellular components, such as proteins, nucleotides, and pigments (Su, 2021).

**Salinity stress**

Salinity can affect various biochemical reactions associated with growth and metabolism in microalgae. High salinity will impede the absorption of water and nutrient by microalgae, thereby inhibiting growth and ultimately leading to the death of microalgae. There are three types of salinity stress: ionic stress, osmotic stress, and oxidative stress. Ionic stress is caused by ionic homeostatic imbalance. Under salinity stress, the competition between Na\(^+\) and K\(^+\) causes K\(^+\) deficiency in the cytoplasm. Simultaneously, salinity stress also causes an imbalance in reactive oxygen species as well as oxidative stress. In microalgae cells, oxidative stress is often accompanied by an increase in lipid yield. Culturing microalgae under salinity stress can prevent contamination by pollutants and competition by invasive species and other microorganisms (Chen et al., 2022). However, very high salinity can inhibit the growth and change the morphology of microalgae cell (Zafar et al., 2021). Therefore, an ideal salinity range must be determined.

**Light stress**

Microalgae growth requires light. A strong light intensity is beneficial for lipid accumulation in microalgae cell, because it favors storage of excessive photosynthetic products and further converts them to chemical energy. However, the light intensity required to achieve the highest lipid yield differs based on microalgae species, as their light utilization efficiency is different by different microalgae species (Gao et al., 2022). Limiting or saturated light intensity are not favorable for microalgae growth. At a very low light intensity (below a compensation point), microalgae growth is affected, which also has adverse effects on lipid accumulation (Aburai et al., 2021). Conversely, after the compensation point is reached, microalgae yield increases with increasing light intensity, and photosynthetic efficiency is the highest at the saturation point. Therefore, an increase in light intensity has a positive effect on increasing lipid accumulation in microalgae. However, very high light intensity will cause photoinhibition, thereby decreasing lipid accumulation in microalgae (Sousa et al., 2012).

**Temperature stress**

The effects of temperature are similar to light intensity on microalgae growth and lipid accumulation. Both increase exponentially as temperature increases and can reach a maximum. However, the required temperature for maximum yield of microalgae also differs by microalgae species. The lipid content in *Chlorella* reaches a maximum at 25°C, and significantly decreases as temperature decreases (Converti et al., 2009). When the temperature increases from 20 to 27.5°C, lipid content in *Scenedesmus obliquus* increases from 18 to 40% (Vitova et al., 2015). However, not all lipid content increases with increasing temperature.

**Metal stress**

Metal ions play a vital role in microalgae growth and lipid accumulation. Metals such as iron and copper are components of photosynthetic electron transport proteins. However, some metals like cadmium, chromium, lead, mercury and arsenic could cause negative effects (like impairing photosynthetic mechanism, blocking cell division and inhibiting enzyme activity) in algal cells. *Chlorella* has a strong resistance to copper and cadmium ions under heterotrophic conditions, with lipid yield increasing by 93.9 and 21.1%, respectively (Yang et al., 2015). In addition, Mg\(^{2+}\) is also found to affect the cell growth and lipid production in microalgae (Ren et al., 2014). Mg\(^{2+}\) plays an important part in different metabolic processes and physiological pathways of algae and is a major element in microalgae culture medium. Mg\(^{2+}\) is a component
of chlorophyll molecules, and Mg$^{2+}$ level in the culture medium directly affects the bio-formation of chlorophyll. It has been reported that the increase of Mg$^{2+}$ level could enhance the acetyl-CoA carboxylase (ACCase) in vivo activity, and ACCase exerted intense regulation of fatty acid synthesis in microalgae.

Carbon dioxide supplementation

Carbon dioxide ensures a carbon supply for photosynthesis in photosynthetic microalgae, as microalgae growth requires sufficient soluble carbon dioxide. Microalgae content and lipid yield increases when carbon dioxide increases to an optimal level. Limited carbon dioxide content in the culture medium can decrease the metabolic rate, thereby decreasing lipid yield in microalgae (Aghaaliipour et al., 2020). Therefore, a high concentration of carbon dioxide can satisfy the carbon needs of microalgae. To decrease the costs, flue gas (rich in carbon dioxide) can be introduced as a carbon source into the microalgae culture system (Mousavi et al., 2022). However, very high carbon dioxide concentration can negatively affect microalgae growth because unused carbon dioxide is converted to carbonic acid (H$_2$CO$_3$) and decrease the pH of the culture medium. Therefore, an optimal carbon dioxide concentration is needed to maximize the lipid yield in microalgae.

Microalgae harvesting technologies

Techniques for microalgae harvesting include centrifugation, coagulation, flocculation, filtration, and centrifugal or gravitational sedimentation. Microalgae harvesting is usually divided into two stages: mass harvesting and thickening. The objective of mass harvesting is to separate microalgae from the suspension and obtain 2–7% of solid mass through flocculation, foam flotation, or gravitational sedimentation (Fuad et al., 2018). The objective for thickening is to enrich biomass through filtration and centrifugation, and this process requires higher energy input than mass harvesting (Ortiz et al., 2022). The choice of harvesting methods is mainly determined by the characteristics of microalgae, such as cell density and size. The comparison of these technologies is in Table 2.

Chemical flocculation

During the chemical flocculation, chemicals are used to aggregate microalgal cells to induce flocculation. Microalgae cell is negatively charged and repel each other, resulting in the cell suspension, and the introduction of chemical substances can neutralize the charge and cause cell aggregation (Pittman et al., 2011). Coagulants are mainly classified as inorganic and organic coagulants. Inorganic coagulants, such as iron and aluminum salt coagulants, are used to harvest microalgae, such as Scenedesmus and Chlorella. Organic coagulants, such as chitosan, are biopolymers that can increase microalgae dimensions (>100 µm), thereby increasing their sedimentation efficiency. Currently, cation coagulants are optimal for harvesting microalgae, and anions cannot be used for microalgae flocculation due to repulsion between the charges.

Biological flocculation

Biological flocculation is a method that uses extracellular polymers secreted by bacteria or fungi or surface charges on these microorganisms to flocculate microalgae. Compared with other flocculation methods, biological flocculation is a cheap and environmentally friendly method that can be continuously used for large-scale microalgae harvesting. Biological flocculation is affected by pH, temperature, nutrient content, and dissolved oxygen. However, when bacteria are used to aid microalgae flocculation harvesting, additional nutrients need to be added, which may result in a secondary contamination (Wan et al., 2015).

Self-flocculation

Self-flocculation refers to the use of cell surface characteristics or other factors to cause microalgae aggregation. Natural self-flocculation of microalgae may be caused due to environmental stress and changes in N levels, pH, dissolved oxygen content, and Ca$^{2+}$ and Mg$^{2+}$ levels in the culture medium (Enamala et al., 2018). Self-flocculation usually occurs naturally after carbon dioxide is exhausted or in basic pH conditions. Mainly Ca and Mg precipitates are formed as a consequence of natural self-flocculation.

Flotation

Flotation refers to the use of microbubbles to harvest microalgae without the addition of chemicals. During the flotation, air bubbles (diameter < 500 µm) bind to the microalgae cells. Based on air bubble dimension, flotation can be divided into dissolved air and dispersed flotation. In dissolved air flotation, small air bubbles with a mean size of 40 µm (range: 10–100 µm) are generated (Laamanen et al., 2016). Flotation processes are classified according to the method of bubble production as dissolved air flotation (DAF), dispersed air flotation (DiaF), electrolytic flotation, and dissolved ozone flotation (DOF). Sometimes, dissolved air flotation uses flocculants and compressed bubbles to accelerate the aggregation of microalgae, which float to the water surface (Alkarawi et al., 2018). This is an efficient method for harvesting microalgae, but high-pressure requirements result in higher operating costs.

Sedimentation

Sedimentation is commonly used for separating microalgae from water. The density, shape and diameter of microalgae cells are the main factors affecting the velocity of microalgae sedimentation. Lamella settler and settling ponds can increase
the harvest efficiency of microalgae. However, cell density is a limiting factor as high density microalgae cells are easier to harvest through gravitational sedimentation than low density microalgae cells. Sedimentation is a conventional separation technique that has been widely used in water treatment to remove unwanted particles in a cost-effective manner. In this process, particles are left to settle down according to Stokes’ Law (Shelef et al., 1984). In theory, the settling velocity has been reported to be 0.4 and 2.2 m/day. This is because Stokes’ law is considered for the spherical-shaped cells, whereas most microalgae strains in nature have complex morphology (Peperzak et al., 2003).

Filtration

Traditional filtration is used to harvest larger microalgae cells (usually > 70 mm). While microfiltration, ultrafiltration and reverse osmosis can be used to harvest smaller microalgae, and these filtration methods require periodic replacement of expensive membranes, resulting in high costs. Based on the configuration of a feeding flux during a filtration process, there are three types of filtrations, including dead-end filtration (DEF), cross-flow filtration (CFF), and dynamic filtration (DF). Dead-end filtration, also known as frontal filtration or cake filtration, is the most common membrane system in microalgae harvesting. They are particularly effective in recovering microalgal cells with a radius larger than 70 μm (Barros et al., 2015). Cross-flow filtration (tangential flow filtration)—a filtration process in which feed flows tangentially across a membrane surface—is widely utilized in microalgae harvesting depending on the process conditions (Ahmad et al., 2012). Cross filtration works by introducing feed flow under pressure across the membrane surface instead of directly onto the filter. During filtration, any material smaller than the cross-flow membrane pore passes through the membrane, while larger suspended particulates remain in the retentate stream, similar to DEF. Dynamic filtration, also known as shear enhanced filtration, is considered an alternative option to DEF and CFF. Due to fouling in DEF, transmembrane pressure (TMP—the pressure needed to press the flux through a membrane) increases with the formation of the cake layer, resulting in lower filtration efficiency (Cheng et al., 2021). To address this issue, the mechanical movement of devices is applied in DF that creates high shear stress at the membrane surface, resulting in uncoupling between local shear rate and TMP from a feeding flowrate, which leads to higher efficiency compared to the conventional filtration methods.

Centrifugation

Centrifugation uses centrifugal force to separate mixtures and is widely used to harvest microalgae, which produces at maximum yield of 95% under optimal conditions. Centrifugation is energy-intensive (with a range varying from 0.3 to 8 kWh/m³) due to its high capital and operating costs (Najar and Abu-Shamleh, 2020). Centrifugation takes up to 20-30% of the total costs in biofuel production, and these costs are largely associated with the dewatering process (drying of microalgae suspension). In other words, even though the size of cells has a direct relationship with the required g-force, but the technique can still be used in the process. Among sedimenting centrifuges, three types are frequently used for algae separation on industrial scales: disk stack, nozzle-type, and decanters centrifuges (Sharma et al., 2014). Stationery-wall centrifuges (hydrocyclones) separate particles in a liquid suspension with no moving parts. There is also another family of centrifuges, namely benchtop centrifuges, which are commonly used in laboratories (Show and Lee, 2014). The limitations of this method are high operation and maintenance costs. Moreover, it is not suitable for large-scale application.

Lipid extraction technologies

Lipids are extracted after the microalgae are harvested and lyophilized. The principles of lipid extraction from microalgae cell are specific—no disruption to lipid components and ease of scaling up. The lipid extraction process includes cell drying, cell disruption, and lipid extraction. Solvent extraction and supercritical fluid extraction are the common techniques used for extracting lipids from microalgae cell. The Folch method was previously used for lipid extraction from microalgae cell due to its simple operation (Karim et al., 2020). However, this method requires a large volume of solvent and tends to be affected by mineral salts—in the absence of which acidic lipids in microalgae are washed away—in the material used for extraction. Therefore, the modified Bligh & Dyer method is widely used for lipid extraction. The solvents used for lipid extraction should be cheap, non-volatile, non-toxic, and non-polar (Abimbola et al., 2021). Before lipid extraction, the cell wall and membrane of microalgae must be disrupted. This is because the microalgae cell walls are thick and tough and can protect cells from degradation due to the lipid extraction conditions, affecting efficiency.

Preprocessing: Cell disruption

Microalgae must undergo disruption before lipid extraction. The cell disruption methods are determined by the type, status, and scale of the microalgae and divided into mechanical and non-mechanical preprocessing methods (Li et al., 2022).

Mechanical preprocessing

Milling. Milling uses shear force to collide microalgae cell with glass or ceramic beads in the stirrer to disrupt microalgae cell. When the bead size is <0.5 mm or >0.5 mm, increasing bead size can either promote or have adverse effects on algal cell disruption, respectively (Zinkoné et al., 2018). Additionally, high density (zirconium) and low density (glass) beads are
more effective in high- and low-viscosity media, respectively. Increasing stirring duration, stirring speed, and bead quantity has a positive effect on disruption (Liu et al., 2022). Although milling has many advantages, one of its limitations is its high energy consumption. Moreover, the formation of very fine cell debris and biochemical substances in the soluble and solid phases increases downstream processing cost. Therefore, milling is not an ideal cell disruption method.

High-pressure homogenization. High-pressure homogenization on uses the high-pressure impact (shear force) of an accelerated fluid jet on the surface of a stationary valve and hydraulic cavitation due to shear stress induced by pressure decrease to achieve cell disruption. Cavitation is a three-step phenomenon that occurs within a short time interval (microseconds): air bubble formation, growth, and rupture. This leads to the release of large amounts of energy that causes cell disruption (Carullo et al., 2018). Cell density must be low when using high-pressure homogenization to disrupt microalgae cell, and the products must be separated. It increases energy and water consumptions for downstream processing (Spiden et al., 2013).

Ultrasonication. In ultrasonication processing, the energy of high-frequency sound waves causes cavitation, and the transmitted impact waves form jets in the surrounding medium, causing cell disruption through high shear-force. The advantages of this technique are that the cell walls are disrupted at low temperatures and no additional of chemicals are involved. The main disadvantages of ultrasonication are low disruption rate of some types of microalgae and local or global heat generation (Gerde et al., 2012). However, good temperature control can increase the quality of extracted lipid while decreasing the disruption rate of microalgae cell. Combining ultrasonication and solvent use or other disruption methods can increase cell disruption rate and decrease energy consumption.

Non-mechanical preprocessing

Biological enzyme. Biological enzyme has various unique characteristics, such as biological specificity, gentle operating conditions, low energy consumption, and destruction rates, etc. Biological enzyme has great potential in cell disruption. Glycoside hydrolase, glucanase, peptidase, and lipase have been used in the lysis of various microalgae. During lysis, the enzyme binds to specific molecules on the cell membrane or wall to destroy it. However, the treatment duration is long and disruption efficiency is lower than that of mechanical or chemical disruption methods (Li et al., 2022). Additionally, the main limiting factor for biological enzyme is the high cost and the low number types of enzymes available for microalgae cell disruption.

Chemical disruption. Many chemicals can disrupt microalgae cell, such as antibiotics, chelators, detergents, chemical solvents, hypochlorite, acids, and bases (Li et al., 2022). The selectivity, suitability, and efficiency of these chemicals are determined by the wall composition of microalgae cell. Chemicals differ in their mechanism of microalgae cell: For example, antibiotics usually inhibit the synthesis of microalgae cell membrane components, chelators can bind to cations that form molecular cross-linked bridges between neighboring microalgae cell membrane, detergents and membrane molecules form micelles, chemical solvents dissolve or perforate microalgae cell membranes or microalgae wall, bases can saponify membranes, and acids can cause microalgae cell membrane or microalgae cell wall perforation (Phong et al., 2018). However, the problems of efficiency, toxicity, and economical feasibility exist with chemical disruption methods.

Lipid extraction

The lipid in microalgae cell contains different components. Non-polar organic solvents can disrupt hydrophobic interactions between neutral lipids, whereas polar organic solvents, such as alcohols, can disrupt the hydrogen bonds between polar lipids. Solvent selection is based on the type of microalgae and should be cheap and non-toxic. Soxhlet extraction, which uses hexane, and the Bligh & Dyer method, which uses a chloroform/methanol mixture, are the two most commonly used methods for extracting lipids from microalgae cell (Sanyal et al., 2022). Hexane is becoming increasingly popular for lipid extraction due to its low cost. Additionally, ionic liquids (ILs) have been successfully used for lipid extraction.

Soxhlet extraction

Soxhlet extraction method was proposed as early as 1879 and was originally used to quantify the total lipids amount in milk (Soxhlet, 1879) and was further gradually promoted in the fields of food, pharmaceutical and other industries. Hexane extraction can be used alone or in combination with homogenizers. After a homogenizer is used to extract lipids, a mixture of hexane and cyclohexane can be used to extract the lipids. Lipids dissolved in cyclohexane and microalgae residues are filtered out and then separated using distillation. The disadvantage of solvent extraction is that the chemicals used are more hazardous. For example, benzene is carcinogenic and explosive. Although hexane has a lower efficiency than chloroform, it has a lower toxicity and affinity toward non-lipid components, and a higher selectivity toward neutral lipid fractions (Aravind et al., 2021). Although the traditional Soxhlet extraction has low cost and simple operation, it also has disadvantages such as long extraction time and large reagent consumption.

Bligh and d yer extraction

The Bligh-Dyer extraction method is a method based on a two-phase solvent extraction and it can be considered as a variant of Folch (Bligh and Dyer, 1959). In the Bligh &
Dyer extraction, the critical ratio of methanol, chloroform, and water should be 2:1:1.8, under which samples can be homogenized into a monophasic system. Chloroform is added for rehomogenization, and the final ratio of methanol, chloroform, and water is 2:2:1.8. The homogenate is centrifuged and two layers are formed (lipids dissolved in chloroform and methanol dissolved in water) and distillation is used to separate the lipids from chloroform and methanol (Candice et al., 2019). As a method close to Folch, Bligh-Dyer also uses toxic reagents, which generates a large amount of environmentally harmful waste. Therefore, waste recovery and cost need to be considered when it is used for large scale extraction.

Ionic liquid extraction

Ionic liquids are the salts composed of relatively large asymmetric organic cations and smaller inorganic or organic anions. Cations usually consist of nitrogen-containing ring structures (e.g., imidazopyrimidine or pyrimidine), including various functional groups, which determine the polarity of ILs. ILs are known as green solvents, because their non-volatile and heat-stable characteristics make them potential substitutes for volatile organic solvents (Shankar et al., 2017).

Supercritical fluid extraction

Supercritical fluid (such as water, CO$_2$, etc.) extraction is a green technology with the potential to replace traditional organic solvent extraction (Jafari et al., 2021). Among the fluids, CO$_2$ is very fashionable. The extraction apparatus includes a feeding pump used for compressing and transporting liquid carbon dioxide and a heated micro-metering valve. Once heated, the compressed carbon dioxide will be at a supercritical state and can extract lipids from microalgae. Once full decompression occurs, carbon dioxide evaporates into the surrounding environment and the extracted lipids are precipitated out. Supercritical carbon dioxide has high solvation capacity and low toxicity (Obeid et al., 2018). The intermediate diffusion or viscosity of the fluid promotes mass transfer equilibrium, and the extracted lipids do not contain solvents. The disadvantage of this method is the complex equipment required and high cost.

Conclusion

Microalgae could utilize the carbon resource in the water and soil in the nature, and the biodiesel could be produced from microalgae, which provides a more sustainable and environmentally friendly alternative to fossil fuel. This review discusses the influencing parameters and advanced parameters technologies for microalgae biodiesel production. All key parameters affecting microalgae cultivation, lipid accumulation, microalgae harvesting, and lipid extraction were critically listed, and the recent advanced technologies for microalgae biodiesel production including microalgae cultivation systems, lipid induction technologies, microalgae harvesting technologies, and lipid extraction technologies were also compared. While, the use of microalgae as biodiesel feedstock is technically feasible, but not economically viable. The production of microalgae biodiesel in the form of a hybrid refinery along with production of conventional microalgae products can improve the marketability of microalgae. However, more research should be done on long term stability and technical aspects of a hybrid refinery.

Author contributions

SZ, LZ, GX, FL, and XL: conceptualization, writing – review and editing, and resources. SZ and LZ: methodology. SZ: writing – original draft preparation. SZ, LZ, and XL: funding acquisition. LZ and XL: supervision. All authors contributed to the article and approved the submitted version.

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Conflict of interest

The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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