Toxicity Reduction of Reactive Red Dye-238 Using Advanced Oxidation Process by Solar Energy

Riyad Al-Anbari*  Abdul Hamed Al-Obaidy**  Eman Abd***

*Building and Construction Engineering Department, University of Technology, Baghdad, Iraq.
**Environmental Research Center, University of Technology, Baghdad, Iraq.
***Environmental Engineering Department, Al-Mustansiriayah University, Baghdad, Iraq.

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Abstract:
Decolorization of red azo dye (Cibacron Red FN-R) from synthetic wastewater has been investigated as a function of solar advanced oxidation process. The photocatalytic activity using ZnO as a photocatalysis has been estimated. Different parameters affected the removal efficiency, including pH of the solution, initial dye concentration and H2O2 concentration were evaluated to find out the optimum value of these parameters. The results proved that the optimal pH value was 8 and the most efficient H2O2 concentration was 100mg/L. Toxicity reduction percent for effluent solution was also monitored to assess the degradation process. This treatment method was able to strongly reduce the color and toxicity of reactive red dye-238 to about (99 and 80) % respectively. It can be concluded, from these experiments, that the using of ZnO as a photocatalysis was exhibited as economical and efficient treatment method to remove reactive red dye-238 from aqueous solution.

Key words: photocatalysis, reactive dye, zinc oxide, azo dye.

Introduction:
Dyes are common industrial residues present in wastewater of different industries, ordinarily in the textile dyeing process, inks, and photographic industries, among others [1]. Textile industry produces a large volume of colored dye effluent, which is toxic and non-biodegradable [2]. Dyes contain two types of groups, namely chromophore (chromophore is an electron withdrawing group) and auxochromes (are electron releasing groups) which are responsible for their color. The most important chromophores are the azo(-N = N-), carbonyl (C = O), methine (-CH=), and nitro (NO2) groups [3]. Among the different types of dyes used in textile industry, 60–70% is azo compounds [2]. Due to their synthetic nature and structure mainly aromatic, most dyes are non-biodegradable, having carcinogenic action or causing allergies, dermatitis, skin irritation or different tissular changes. Moreover, various azo dyes, mainly aromatic compounds show both acute and chronic toxicity. High potential health risk is
caused by adsorption of azo dyes and their breakdown products (toxic amines) through the gastrointestinal tract, skin, lungs, and also formation of hemoglobin adducts and disturbance of blood formation [5].

There are several available methods to treat this wastewater such as: adsorption, coagulation and precipitation, aerobic and anaerobic process, and others [6]. One difficulty with these methods is that they are not destructive but only transfer the contamination from one phase to another. Therefore, a new and different kind of pollution is faced and further treatments are deemed necessary [7]. An alternative to conventional methods, “advanced oxidation processes” (AOPs) have been developed based on the generation of very reactive species such as hydroxyl radical. The generated hydroxyl radical can oxidize a broad range of organic pollutants quickly and non-selectively [9]. A photocatalyst is defined as a substance, which is activated by adsorbing a photon and is capable of accelerating a reaction without being consumed; these substances are invariably semiconductors [11].

The present study is concerned to monitor the decolorization of the reactive red dye-238 (Cibacron red FN-R) in solution by using ZnO as a photocatalysis under solar light radiation instead of UV-lamp. The effects of important parameters including pH and concentration of H$_2$O$_2$ were examined with respect to the highest efficiency of decolorization of reactive red dye. Reduction in toxicity of azo dye was also monitored during the treatment process.

Materials and Experimental Set-up:

Materials

The reactive red dye-238 RR had been supplied from AL-Kut Textile Factory south of Baghdad, (Department of Dying and Printing). Simulated solutions were prepared by dissolving a defined amount of dye in the required volume of distilled water. The chemical formula for this dye is C$_{29}$H$_{15}$O$_{13}$S$_4$ClFN$_7$Na$_4$ and the colour index number is CI Reactive Red 238[18]. Analytical grade reagents of ZnO, H$_2$SO$_4$, NaOH and H$_2$O$_2$ were used as such without further purification.

Experimental set-up

The suspension of synthetic wastewater and ZnO was kept in an absence of light for about 30 min to achieve the equilibrium of adsorption, after that the degradation was accomplished under sunlight and the average intensity of sunlight was measured by using UV-radiometer (UV-340A, Lutron, USA). The heat up of the solution was not much and the temperature varied within ± 6 °C.
between starting and ending point of reaction. Samples were withdrawn from effluent at regular time intervals and filtered by using 0.45 µm membrane filter then the dye concentration was measured by UV-spectrophotometer (UV-1800 Shimadzu) at a spectrum length of 541nm. Also, the reduction in toxicity of dye solution was monitored by measuring the inhibition in the number of E. Coli colonies. The concentrations of H₂O₂ added were 0, 100, 200, 300 and 400 mg.L⁻¹. The initial concentration of reactive red dye chosen was 25, 50, 75 and 100 mg.L⁻¹. To study the effect of pH, the values of 2,4,6,8 and 10 were selected as initial pH value of the solution.

**Kinetic analysis**

The most suitable model used to describe photocatalytic processes is the Langmuir–Hinshelwood (LH), which is described by the following mathematical relationship:

\[
\frac{dc}{dt} = k_{LH} \frac{KC}{1+KC}
\]  

(8)

Where: \( r \) (mg L⁻¹s⁻¹) represents the reaction rate, \( C \) (mg L⁻¹) the pollutant concentration at time \( t \) during degradation, \( K \) (mg⁻¹L) the equilibrium constant for pollutant adsorption onto catalyst and \( k_{LH} \) (mg L⁻¹s⁻¹) the reaction rate constant at maximum coverage. Under certain experimental conditions, \( KC<<1 \), so that the LH model is usually closer to first-order reaction kinetics and eq.(8) will be simplified to:

\[
\frac{dc}{dt} = -k_{LH}KC = -kC
\]  

(9)

Where, \( K_c \) (min⁻¹) =\( k_{LH} \) K is the pseudo-first-order rate constant [22].

The intensity of solar irradiance was never constant and could not be controlled due to multiple environmental influences (i.e., time of day or atmospheric conditions) and in order to normalize data collected at different solar light intensity and exposure time was used[23]

\[
t_{30W,n} = t_{30W,n-1} + \left( t_n - t_{n-1} \right) \frac{\text{UV} \cdot V_i}{30 \cdot V_T}
\]  

(10)

In eq. (10), \( t_n \) is the experimental time for each sample, UV the average solar ultraviolet radiation measured during \( t_n \), and \( t_{30W} \) is the “normalized illumination time”. In this case, time refers to a constant solar UV power of 30 W/m² (typical solar UV power on a perfectly sunny day around noon), \( V_i \) is the irradiate volume and \( V_T \) is the total volume [24]. In that way, photocatalytic process could be evaluated as a function of time taking into account environmental conditions [23].

**Results and Discussion**

**Effect of pH**

The pH value of the aqueous solution is a key parameter for photocatalytic process. The aqueous solution of dye having 25mg.L⁻¹ concentration were treated by varying the initial pH of solution from pH=2 to 10. The pH value was justified by using 0.1N H₂SO₄ or 0.1N NaOH as required. Figure 2 shows the effect of pH on the removal efficiency of reactive red dye. It can be concluded from this figure that the photocatalytic efficiency was maximized when solution pH reached 8.
This behavior can be explained by the surface charge of catalyst. Each catalyst have point of zero charge (pH_{pzc}) at this pH where the net charge on catalyst surface is equal zero [25] and catalyst surface is positively charged at pH< pH_{pzc} whereas it is negatively charged for pH > pH_{pzc} [26]. The point of zero charge (pHpzc) for ZnO was cited in literatures at pH=8.9 (Zuafuani and Ahmed, 2015).

**Effect of H_{2}O_{2} concentration**

The addition of H_{2}O_{2} has a major effect on the photocatalytic process; this additive increases the rate of reaction by improvement the formation of hydroxyl radical. This is due to inhibition of the recombination of the electron–hole in present of H_{2}O_{2}. The decolorization rate of reactive red dye can be accelerated by increasing the concentration of OH radicals by the addition of oxidant like H_{2}O_{2} [27]. As illustrated in Figure 3, the results show that the decolorization percent increases when the concentration of H_{2}O_{2} increases, the percentage removal becomes maximum at 100 mg/l and after that begins declining with further increase in H_{2}O_{2} concentration.

**Fig. (2). Removal efficiency of reactive red dye at different initial pH.**

This effect is due to the fact that at a higher H_{2}O_{2} concentration, scavenging of OH radicals will take place [28].

**The effect of initial concentration of dye**

The effect of initial concentration of reactive dye was evaluated by choosing different initial concentrations (25, 50, 75 and 100 mg/L) and the other operation conditions were kept constant.

Figure 4 shows, as the concentration of reactive red dye was increased, the decrease of the decolorization percent. The increase in the initial concentration of reactive red dye will reduce the transparency of solution which finally affects the penetration of sunlight through the solution. Another reason is that: increasing in the initial concentration of dye leads to increasing the number of molecules that must be treated while the active catalytic sites still constant and this causes the decrease in the decolorization rate.
The kinetics for photocatalytic process under solar light were predicted at various dye concentrations (25, 50, 75, and 100 mg/L) and the data was fitted the LH model (Figure 5).

The rate constant ($K_o$) for reactive red dye was estimated from the slope of the linear plots of $\ln \left( \frac{C_0}{C} \right)$ vs. $t_{30w}$ . The variation of $(1/K_o)$ as a function of initial concentration of reactive dye are given in Figure 6. The equation and correlation coefficient were estimated and tabulated in Table 1.

### Toxicity Assessment during Photocatalytic

Toxicity determinations were evaluated by measuring the inhibition in the number of colonies of *Escherichia coli* cultures. In the determination of viable numbers of bacteria, the sample of dye solution (treated or untreated) was diluted and inoculated with *E. Coli* at different serial dilutions. The diluted samples were placed on an agar using pour plate technique. These samples were incubated at 37°C for 24 hrs. and the number of bacterial colonies was counted. The variation in toxicity of dye solution during the photocatalytic process was examined. Figure 7 shows that the reduction in toxicity of red dye was plotted against $t_{30w}$. It can be clearly seen that toxicity of effluent samples was decreased gradually during the reaction time as a result of decomposition of dye compounds until the reduction in toxicity reached about 80 % for reaction time, $t_{30w}$=22.5 min. Moreover, it can be concluded from this figure that there is a linear relation between the inhibition percent and the

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**Table 1. The kinetic analysis data**

| Catalysis | Equation for linear fitting | Correlation coefficient $R^2$ |
|-----------|-----------------------------|-------------------------------|
| ZnO       | $Y = -5.229 + 0.3127X$     | 0.83                          |

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**Fig. (4). The effect of initial concentration of blue dye on decolorization percent of reactive red dye.**

**Fig. (5). The LH models for reactive red dye.**

**Fig. (6). Variation of $1/K_o$ vs. $C_o$ of reactive red dye**

**Fig. (7). Variation of $1/K_o$ vs. $C_o$ of reactive red dye**

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reaction time, $t_{30w}$. This observation confirms the results obtained by Le et al. (2016).

Fig (7). Variation in inhibition percent at different reaction time for photocatalytic of reactive red dye.

Conclusions:
Photocatalytic process of reactive red dye was carried out by using ZnO under solar light irradiation. The optimum conditions for decolorization were obtained to be: pH=8, $H_2O_2$ concentration =100mg/L and initial concentration of dye=25 mg/L.

It was observed that the degradation process was strongly affected by pH value and the concentration of $H_2O_2$ was added. Toxicity of dye solution clearly decreased during the reaction time. The decolorization process could be fitted to L-H model and the reaction kinetics were estimated.

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تقليل سمية الصبغة الحمراء-238 باستعمال عملية الأكسدة المتقدمة

رياض الاتباري*  عبد الحميد العبيدي**  إيمان عبد ***

* قسم هندسة البناء والالكترونيات، الجامعة الإلكترونية، بغداد، العراق.
** مركز البحوث البيئية، الجامعة التكنولوجية، بغداد، العراق.
*** قسم هندسة البيئة، كلية الهندسة، الجامعة المستنصرية.

الخلاصة:
تم دراسة عملية إزالة اللون لصبغة الأزو الحمراء (Cibacron Red FN-R) من مياه مخلفات مصنعة في المختبر باستخدام عملية الأكسدة المتقدمة بالطاقة الشمسية. تم تقييم كفاءة التحفيز الضوئي لأوكسيد الخارصين عند استخدامه كعامل مساعد ومن ثم تقييم تأثير عدة عوامل والتي تشمل قيمة الأس الحمضي للمحلول وتركيز الصبغة الأولي وتركيز بروكسيد الهيدروجين المضاف وذلك لإيجاد أفضل قيم لهذه العوامل. لقد تم الوصول إلى أن أفضل قيمة للأس الحمضي للمحلول كانت 8 وأفضل تركيز لبروكسيم الهيدروجين المضاف كانت 100 ملم/لتر. تم ترتبط معادلة نسب الإختلاف في سمية المحلول الخارج من المعالجة وذلك لتقييم عملية تحلل الصبغة. وكانت هذه المعادلة قادرة على تقليل اللون وسمية إلى حد (99 و 80) % على التوالي من التجارب العملية. تم الوصول إلى أن استخدام أوكسيد الخارصين كعامل مساعد لعملية التحفيز الضوئي يمثل طريقة معالجة فعالة واقتصادية لإزالة الصبغة الحمراء الفعالة-238 من المحلول المائي.

الكلمات المفتاحية: التحفيز الضوئي، الأصباغ الفعالة، أوكسيد الخارصين، أصباغ الأزو.