Simulation of Multi-Stage Flash with Brine Circulating Desalination Plant

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Abstract
Multi-stage flash (MSF) desalination is the main process to solve the problem of limited freshwater resources in the world. This work describes the developed steady-state mathematical model for analysing and evaluating the performance of Multistage flashing with brine circulation desalination process (MSF-BC). It is based on the laws of energy balance, material balance, and heat transfer equations with physical properties correlations equations. The nonlinear equations are linearized and arranged into a tridiagonal matrix form. The model solution is obtained by a computer code written by MATLAB program software. It can predict the productivity of the plant with temperature profiles and flow rates for all stages in the unit. The model results were compared with some previous results presented in literature. The comparison shows good agreement with these available data. An MSF desalination plant in Ayoun Mousa, Egypt of capacity 5000 m$^3$/day was presented as a case study.

Introduction
Water plays an important role in all aspects of life including industrial activities. Drinking water is unfairly similar to most other natural resources, which are distributed unequally around the world.

There is increasing worldwide concern about the scarcity of global water resources, day by day. So, desalination of seawater became a major solution for providing arid zones with continuous supply of fresh water.

Multi-stage flash desalination (MSF) is one of the major methods for the desalination industry with a market share of around 60% of the total production capacity worldwide (1).

The MSF desalination process is based on flash evaporation, depends on using vaporization through multi-stage chambers. The MSF desalination process has many advantages such as it can produce high quality of freshwater with TDS of less than 30 ppm. The produced water can be used in many purposes like boiler making water, chemical processes, dairy and food washing, cooling and cleaning (2). Besides the high-water quality, it produces large quantities of fresh water up to 75000 m$^3$/d for each unit.

The MSF desalination plants are composed of two models (3), Once-through MSF (MSF-OT) which consist of two sections (brine heater and heat recovery sections) and Brine recirculation MSF (MSF-BC) which has one extra section (heat rejection section).

Many researches were conducted to enhance the operation of MSF desalination plants as efficiently as possible and, as a result, to reduce the cost of water generated from such plants. Part of this work focuses on mathematical modelling as a cheap alternative for industrial scale applicative. Models of MSF process can be classified into two different categories; Steady state models (simple and rigorous) and dynamic models.

The steady state mathematical model of MSF-BC process that based on the basic laws of thermodynamics is established in the literature. Models can sort from simple steady-state models with constant thermophysical properties of fluid streams (4; 5; 6; 7; 8; 9) to rigorous mathematical models which taking into account the variation of the thermo-physical properties of various fluids with temperature and salinity (10; 11; 12; 13; 14; 15; 16; 17; 18; 19). (20; 21; 22; 23; 24)

The main aim of this paper is to provide an algorithm for solving the large system of algebraic and nonlinear equations which is a rigorous steady-state mathematical model for MSF-BCR. The system will be solved through Linearizing the equations into tri-diagonal matrix form (TDM) using MATLAB software. The results were verified against previous simulation data given by Abdul Wahab, (2012) (25). In addition, we studied the...
performance of actual desalination plant of Ayoun Mousa, Egypt (26).

**Process Description**

The MSF process with brine circulation is shown in Figure 1 (21). The process is divided into three sections: the brine heater, the heat recovery and the heat rejection sections. Stages of heat recovery include heating of the recycled brine stream inside the condenser tubes from the brine blowdown temperature to a higher temperature near to the top brine temperature. So, the amount of steam used in the brine heater is minimized. The heat rejection section consists of three stages. The function of the heat rejection section is to monitor the feed seawater temperature and reject the excess heat added in the brine heater. Feed seawater enters the last stage of the heat rejection section (Fsea) and moves through the condenser tubes to remove heat from the stages. The stream leaving the first stage of the heat rejection section is separated into two streams; the rejected seawater (Cw) and the makeup stream (F) which is mixed with recycled brine (R) from the last stage of the heat rejection section. Cooling brine (W) enters the last stage of the heat recovery section. It heats gradually by the flashing brine in each stage and leaves the heat recovery section from the first stage. Then it enters the brine heater to raise its temperature to the top brine temperature (TBT) and enters into the 1st flashing stage and produce flashing vapor. This continuous till the last stage of the heat rejection section. The brine stream (BN) from the last stage is split into two streams: the blowdown (BD) stream that is settled to the sea and the remaining recycled water stream (R) which is recycled back to mix with the makeup flow. The distillate is collected from each stage to produce the freshwater product at the end (DN).

**Mathematical Model**

The following simplifying assumptions were used in the rigorous steady state modelling,

- **Steady_state_operation** is the common assumption amongst all studies. (18).
- The distillate is free from salt.
- Heat losses to the surroundings are insignificant.
- Brine holdup and brine flow rate are considered as constant along the unit.
- Heat transfer area shall be considered the same for each part of the plant.
- The physical properties such as heat capacity, viscosity, brine densities, boiling temperatures, vapor enthalpy temperature, and heat transfer coefficient depend on temperature and salinity variation.
- Thermodynamic losses include the boiling point elevation (BPE), the non-equilibrium allowance (NEA), and demister losses (DEM).
- The effect of non-condensable gases on heat transfer is negligible.

**Overall Material Balance Equations**

As shown in Figure 1 (21), the overall mass balance for MSF desalination plant is given by,

\[
F_{sea} = C_w + D_N + B_N \tag{1}
\]

The material balance for the splitter is given by,

\[
C_w = F_{sea} - F \tag{2}
\]

Substituting Equation 2 into Equation 1 yields,

\[
F + D_N + B_D \tag{3}
\]

The steady-state model equations consist of a set of energy and material balance equations which include the following (25):

- Overall material balance equations.
- Material balance equation for each stage.
- Salt_balance_equation for each stage.
- Enthalpy balance equations on flashing brine.
- Overall enthalpy balance for any stage.
- Brine heater model.
- Mixing and splitting equations.

Schematics of the MSF variables in the flashing stage and the brine heater are shown in Figures 2 and 3 (21).
\[ FX_F = B_D X_{BN} \]  

(4)

It should be noticed that the Equation 4 assumes that the distillate is free from salt.

**Material and Salt Balance Equations for Each Stage**

The summation of the inlet flashing brine and distillate flow rates will be equal to the summation of those streams leaving the stage (j).

Mass Balance in the flash chamber

\[ B_{j-1} + D_{j-1} = B_j + D_j \]  

(5)

Stage salt balance:

\[ B_{j-1} X_{Bj-1} = B_j X_{Bj} \]  

(6)

Mass balance for distillate tray

\[ \sum_{k=1}^{j} D_k = \sum_{k=1}^{j-1} D_k + D_j \]  

(7)

Enthalpy Balance Equations on Flashing Brine

For the flashing brine at stage (j), the enthalpy balance equation is given by,

\[ B_{j-1} h_{Bj-1} = B_j h_{Bj} + (B_{j-1} - B_j) h_{vj} \]  

(8)

**Overall Enthalpy Balance for Any Stage**

For a steady-state operation, the summation of the enthalpies of all input streams for stage (j) should be equal to the summation of all streams leaving the stage. There is no generation or accumulation of energy in the stage. The overall enthalpy balance for any stage (j) is given by:

\[
WS_{Bj}(T_{Fj} - T_{Fj+1}) = D_{j-1} S_{Dj-1}(T_{Dj-1} - T^*) + B_{j-1} S_{Bj-1}(T_{Bj-1} - T^*) - D_j S_{Dj}(T_{Dj} - T^*) - B_j S_{Bj}(T_{Bj} - T^*)
\]  

(9)

Where,

The specific heat capacity of pure saturated water (SDj) (29) is given by,

\[ S_{Dj} = (1.001183 - 6.61666652 \times 10^{-5} T_{Dj}) + 1.9999989 \times 10^{-7} T_{Dj}^2 + 1.3333336 \times 10^{-9} T_{Dj}^3 \times 4.184 \]  

(10)

The specific heat capacity of flashing brine at each stage (SBj) (29) given by,

\[
S_{Bj} = (4.185 - 5.381 \times 10^{-3} X_{Bj} + 6.26 \times 10^{-6} X_{Bj}^2) - (3.055 \times 10^{-5} + 2.774 \times 10^{-8} X_{Bj} + 10^{-6} X_{Bj}^2 + 0.318 \times 10^{-8} X_{Bj}^3 + 8.44 \times 10^{-7} + 6.527 \times 10^{-8} X_{Bj}^2 + 10^{-8} X_{Bj}^3 - 0.003 \times 10^{-10} X_{Bj}^2)
\]  

(11)

**Heat Transfer Equation**

The heat transferred to the cooling condenser tubes owing to condensation of the flashed vapor in stage(j). Heat transfer equation in the heat recovery section is given by:
\[ WS_{BJ}(T_{fj} - T_{fj+1}) = U_f A_f \text{LMTD}_j \]  (12)

In the heat rejection section, replacing W instead of Fsea. The logarithmic mean temperature difference in the recovery and rejection stages.

\[ \text{LMTD}_j = (T_{fj} - T_{fj+1})/\ln\left(\frac{T_{fj} - T_{fj+1}}{T_{fj} - T_{fj+1}}\right) \]  (13)

**Equilibrium Equation**

The distillate and flashing brine temperature correlation is given by,

\[ T_{BJ} = T_{DJ} + BPE + NEA + DEM \]  (14)

Where,

**Boiling Point Elevation (28)**

The boiling point elevation correlation of seawater is given by,

\[ BPE = AX + BX^2 + CX^3 \]  (15)

\[ A = (8.25 \times 10^{-2} + 1.883 \times 10^{-6}T + 4.02 \times 10^{-9}T^2) \]  (16)

\[ B = (-7.625 \times 10^{-4} + 9.02 \times 10^{-5}T - 5.2 \times 10^{-7}T^2) \]  (17)

\[ C = (1.522 \times 10^{-4} - 3 \times 10^{-6}T - 3 \times 10^{-8}T^2) \]  (18)

Where X is the weight percentage of the salt and T is the temperature in °C.

**Non-equilibrium allowance (28)**

The NEA correlation for the MSF system is given by,

\[ NEA = \frac{0.3281}{\left(0.5\Delta T + NEA_{10}\right)^{0.3281}} \]  (19)

\[ NEA_{10} = \left(0.9784\right)^{T_i} \left(15.7378\right)^{H_i} \left(1.3777\right)^{Vb \cdot 10^{-6}} \]  (20)

**Demister and Other Losses (31)**

The temperature loss that follows the pressure drop through the demister and condenser tubes is calculated from the following equation:

\[ DEM = \frac{\exp\left(1.885 - 0.02063(1.8T_{fj} + 32)\right)}{1.8} \]  (21)

The distillate flashed steam temperature correlation is given by,

\[ T_{fj} = T_{DJ} + DEM \]  (22)

**Brine Heater Model**

As shown in the Figure 4, the performance of brine heater can be described as

**Mass balance (brine):**

\[ W = B_o \]  (23)

**Overall enthalpy balance:**

\[ B_o S_{BJ}(T_{Bo} - T_{F1}) = M_s A_s \]  (24)

Where,

The latent heat of vaporization (28) is given by,

\[ A_s = 2501.897149 - 2.4070640377 + 1.192217 \times 10^3 \]  (25)

Heat transfer equation in the brine heater:

\[ WS_{RH}(T_{Bo} - T_{F1}) = U_f A_f \text{LMTD}_H \]  (26)

The heat transfer coefficient for the brine and vapor side (31) is given by,

\[ U = \frac{4.8857}{y + z + 4.8857F_{fj}} \]  (27)

Where,

\[ z = 0.102 \times 10^{-2} - 0.747 \times 10^{-5}T_{DJ} + 0.997 \times 10^{-7}T_{fj}^2 - 0.430 \times 10^{-9}T_{fj}^3 + 0.620 \times 10^{-12}T_{fj}^4 \]  (28)

\[ y = \frac{(V_f D_j)^{0.2}}{(160 + 1.92T_{fj})^{0.2}} \]  (29)

**Mixer and Splitter Model**

Mass balance on mixer:
\[ W = F + R \]  \hfill (31)

Salt balance on mixer:
\[ WX_{B0} = FX_F + RX_{BN} \]  \hfill (32)

Enthalpy balance on mixer:
\[ Wh_M = Rh_R + Fh_F \]  \hfill (33)

At splitting point:
\[ B_D = B_N - R \]  \hfill (34)

Where,

The specific enthalpy of saturated water (30) is given by,
\[ h_{Bj} = (1.001183T_{Bj} - 3.0833326 \times 10^{-5}T_{Bj}^2 + 4.666663 \times 10^{-9}T_{Bj}^3 + 3.333334 \times \frac{10^{-10}T_{Bj}^4 - 31.92}{1.184}) \]  \hfill (35)

The water vapor enthalpy is given by,
\[ h_v = 2499.15 + 1.955T - 1.927 \times 10^{-3}T^2 \]  \hfill (36)

The specific enthalpy of brine at each stage given by,
\[ h_{Bj} = (4.185 - 5.381 \times 10^{-3}X_{Bj} + 6.26 \times 10^{-8}X_{Bj}^2)T_{Bj} - \left(3.055 \times 10^{-5} + 2.774 \times 10^{-8}X_{Bj} + 4.318 \times 10^{-9}X_{Bj}^2 \right)T_{Bj}^2 + \left(8.44 \times 10^{-7} + 6.527 \times 10^{-9}X_{Bj} + 4.003 \times 10^{-10}X_{Bj}^2 \right)T_{Bj}^3 \]  \hfill (37)

**Solution of the Systems of Equations**

The above mentioned equations composed of algebraic and nonlinear equations. The linearization of MSF-BC plant equations suggested by Helal et al. (10), into tridiagonal matrix arrangement (TDM form) was selected in this work since this approach has the following advantages (26):

- The algorithm has high degree of convergence stability and results in shorter run times compared with calculation approaches which follow stage wise.
- Small number of iterations required

The final form of TDM for stage(j) in the recovery and rejection sections is:
\[ Ay_j T_{Fj-1} + Be_j T_{Fj} + Ce_j T_{Fj+1} = De_j \]  \hfill (38)

Where,

\[ Ay_j = c_{1j} \]  \hfill (39)
\[ Be_j = c_{2j} - 1 \]  \hfill (40)
\[ Ce_j = c_{3j} + 1 \]  \hfill (41)
\[ De_j = -b_{3j} \]  \hfill (42)

The mathematical model for a steady state process, as described above, is used to build MATLAB code for performance analysis of MSF desalination systems. Figure 4 gives the flow chart of the model solution steps used for steady state simulation of the MSF desalination systems by tridiagonal matrix.

**Model Validation**

Figures (5 and 6) Compare the temperatures of the flashing brine (TBj), distillate (TDj), and recirculating brine (TFj) in 24 flashing stages of simulation results reported by Abdul Wahab, (2012) (25) based on Barka MSF desalination plant data with values predicted by developed model. The results show a good agreement.
Results

The presented model was useful to simulate the production of Ayoun Mousa MSF plant in Egypt. The capacity of the unit is 5000 m$^3$/day and the operating conditions are listed in Table 1 (27). Initial guessing values of the mass flow rates and the temperatures of all the process streams were obtained from simple mathematical model suggested by El-Dessouky and Ettouney (2002)(28). After demonstrating the capability of the developed model, it is used to measure the productivity with the profiles of temperatures and flow rates in all the stages of the unit. The simulation results for the operating parameters of this work is shown in the Table 2.

As shown in Figures (7 and 8) because of the flashing cycle, the outlet brine temperature is decreasing. In addition, the brine flow rate is decreasing due to the distillate formed in each stage. Furthermore, the salinity of the product decreases across the stages. That is because the distillate is almost salt free compared to the brine.

Conclusions

Steady-state models are useful for evaluating the plant operating conditions; studying the performance of plant. They also provide traces for improving the plant efficiency. The developed model can be used to analyze the MSF-BC desalination process at steady state operation conditions. The developed MATLAB code can be used to perform the performance analysis of MSF-BC desalination plants by calculating the productivity of the plant with profiles of temperatures and flow rates in all stages of the unit. The developed model is valid when compared with commercial software used for the same purpose. The presented model predictions were compared with vendor simulation results for BARKA MSF desalination plant reported by Abdul Wahab, (2012), and there was a satisfactory matching between them. Ayoun Mousa MSF desalination plant located in Egypt was used as a case study to predict the performance of the plant.

Nomenclature

| Symbol | Definition |
|--------|------------|
| A      | Heat transfer area, m$^2$ |
| BD     | Blow-down mass flow rate, Kg/s |
| BN     | Flashing brine mass flowrate leaving stage N, Kg/s |
| BPE    | Boiling point elevation |
| Cw     | Rejected seawater mass flowrate, Kg/s |
| DEM    | Temperature losses due to demister, °C |
| D      | Diameter of tube, m |
| DN     | Distillate flowrate leaving stage N, Kg/s |
| F      | Make-up seawater mass flow rate, Kg/s |
| Fsea   | Intake seawater mass flow rate, Kg/s |
| h      | Specific enthalpy, Kcal/Kg |
| L      | Length of tubes, m |
| NEA    | Non-equilibrium allowance |
| R      | Recycled brine mass flow rate, Kg/s |
| S      | Specific heat capacity, Kcal/Kg °C |
| T      | Temperature, °C |
| TBT    | Top brine temperature, °C |
| U      | Overall heat transfer coefficient, Kcal/m² h K |
| W      | Cooling brine mass flow rate leaving stage 1, Kg/s |

Subscripts

| Symbol | Description |
|--------|-------------|
| b      | Brine       |
| D      | Distillate product |
| H      | Brine heater |
| j      | Stage number |
| N      | Last stage of the unit |
| R      | Recycled brine stream |

Figure 4: The flow chart for the solution of the developed model (TDM)
Table 1: Design and operational data for Ayoun Mousa MSF desalination plant.

| Parameter                              | Value               |
|----------------------------------------|---------------------|
| 5000 m³/day MSF_BC                     |                     |
| Top brine temperature (TBT) °C         | 110                 |
| Brine blowdown temperature °C          | 39                  |
| Feed seawater temperature °C           | 27                  |
| Cooling water splitter ratio           | 0.482               |
| Sea water salinity, ppm                | 48000               |
| Brine blow down salinity, ppm          | 70000               |
| Number of stages                       | 20(N_R=17, N_j=3)   |
| Brine load Kg/m.s                      | 180                 |
| Vapor velocity m/s                     | 12                  |
| Weir coefficient Cd                    | 0.5                 |
| Tube outside diameter, m              | 0.01949             |
| Tube inside diameter, m               | 0.02199             |
| BH outside diameter, m                | 0.0239              |
| BH inside diameter, m                 | 0.0214              |

Table 2: Model predictions for this operating condition of this work.

| j | T_Bj °C | T_Dj °C | T_Fj °C | B_j kg/s | D_j kg/s | X_j wt% |
|---|---------|---------|---------|---------|---------|--------|
| 1 | 106.45  | 105.28  | 102.71  | 480.2   | 3.071   | 62.4   |
| 2 | 102.99  | 101.67  | 99.121  | 477.2   | 6.122   | 62.8   |
| 3 | 99.39   | 98.06   | 95.489  | 474.2   | 9.154   | 6.32   |
| 4 | 95.62   | 94.36   | 91.787  | 471.2   | 12.16   | 6.36   |
| 5 | 91.96   | 90.68   | 88.111  | 468.2   | 15.16   | 6.40   |
| 6 | 88.27   | 86.97   | 84.411  | 465.2   | 18.13   | 6.44   |
| 7 | 84.59   | 83.26   | 80.718  | 462.3   | 21.09   | 6.48   |
| 8 | 80.98   | 79.53   | 77.013  | 459.4   | 24.03   | 6.52   |
| 9 | 77.22   | 75.80   | 73.313  | 456.5   | 26.95   | 6.57   |
| 1 | 73.50   | 72.09   | 69.626  | 453.6   | 29.85   | 6.61   |
| 2 | 69.98   | 68.39   | 65.950  | 450.7   | 32.73   | 6.65   |
| 3 | 66.34   | 64.70   | 62.284  | 447.9   | 35.59   | 6.69   |
| 1 | 62.73   | 61.04   | 58.657  | 445.1   | 38.44   | 6.73   |
| 2 | 59.21   | 57.41   | 55.060  | 441.5   | 41.27   | 6.78   |
| 3 | 55.78   | 53.83   | 51.512  | 438.2   | 44.08   | 6.82   |
| 4 | 52.22   | 50.19   | 47.914  | 435.9   | 46.87   | 6.86   |
| 5 | 48.82   | 45.18   | 43.81   | 436.7   | 49.65   | 6.91   |

Figure 5: Comparison of our work with Abdul-Wahab(2012) for distillate temperature(TDj)

Figure 6: Comparison of our work with Abdul-Wahab(2012) for flashing stage temperature(TBj)
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Figure 1: Flowrates variation through the stages.

Figure 7: Temperature variation through the stages.
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