Enhanced production of *Aspergillus tamarii* lipase for recovery of fat from tannery fleshings

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Abstract

The influence of various oil cakes has been investigated for high level production of lipase using *Aspergillus tamarii* MTCC 5152. By solid state fermentation in wheat bran containing 2.5% w/w gingili oil cake at 70% v/w moisture content the fungus produced a maximal yield of lipase (758 ± 3.61 u/g) after 5 days of incubation using 2% v/w inoculum containing 10⁶ spores/mL. Wheat bran and gingili oil cake with supplementation of gingili oil (1.0% w/w), glucose (0.5% w/w) and peptone (0.5% w/w) gives an increased enzyme production of 793 ± 6.56 u/g. The enzyme shows maximum activity at pH 7.0, temperature 50 °C and was stable between the pH 5.0-8.0 and temperature up to 60 °C. Crude lipase (3%) applied to tannery fleshing shows 92% fat solubility. The results demonstrate that fat obtained from tannery fleshing, a by-product of the leather industry has a high potential for biodiesel production and the proteinaceous residue obtained can be used as animal feed.

Key words: wheat bran, oil cakes, lipase, tannery fleshing, fat hydrolysis.

Introduction

Leather industries are facing pollution problem due to generation of solid wastes from the beam house operations. Tannery fleshing is a waste, generated mainly after dehairting of animal hides and skins by the mechanical processes in the form of trimming, fleshing and shaving. These fleshings are rich in proteins and fats and generally just dumped or underutilized. Most of the solid wastes occur in the pre-tanning stages. The general composition of solid waste originating from pre-tanning process consist of natural fats, proteins, blood, water, salt and other wastes and become a source of environmental pollution in spite of these wastes carry a high potential for reutilization. Hide fleshing accounts for 50-60% of waste generated in the tannery (Colak et al., 2005). The bovine hide fleshing have been reported to contain 80% water; the protein content of the dry matter was 63%, fat 14% and ash content 8% (Kamini et al., 2000). The byproducts obtained from the fleshing may be used as a poultry feed and biofertilizer after recovering the fat using lipase.

Industrial enzymes are used in detergents, laundry and dishwashing agents, leather dehairting and tanning, desizing of textiles, deinking of paper and degreasing of hides and skins (Dayanandan et al., 2003; Headon and Walsh, 1994). The use of enzymes frequently results in many benefits that cannot be obtained by traditional chemical processes, includes quality improvement in products and minimum manufacturing cost, reduced waste generation and lower energy consumption. The enzymatic process can be controlled through various means, such as dose, temperature and time.

Lipases are a unique group of enzymes that catalyze the hydrolysis of fats and oils. Lipids are water-insoluble complex biomolecules and lipases play an important role in the breakdown of these compounds. Microbial lipases are often more useful than enzymes derived from plants or animals because of the high yield, ease of genetic manipulation and production through the rapid growth of microorganisms on inexpensive media. Microbial lipases are also more stable and their production process is more convenient and safer (Harwood, 1989; Wiseman, 1995). The en-
zyme production could be further enhanced by optimization of physiological and biological conditions. Microbial lipases can be produced from bacteria, fungi and yeast by using processes like solid-state (SSF) and submerged fermentation (SmF) methods (Ramachandran et al., 2007; Graminha et al., 2008). Hence, the current study focuses on solid-state fermentation with the combined effects of various oil cakes and wheat bran for enhanced production of lipase and also studies the potential of this enzyme for the recovery of high value fat from fat rich waste tannery fleshing which may find applications in chemical industries and biodiesel production (Colak et al., 2005; Ozgunay et al., 2007).

Materials and Methods

Materials, microorganism and inoculum

Analytical grade chemicals of Hi-Media and Merck were used for the present study. Wheat bran, gingili, ground nut, cotton seed and coconut oil cakes were purchased from the local supplier. Aspergillus tamarii MTCC 5152 used in the present work was isolated from soil and maintained on Czapek-Dox’s agar medium. Spores from 7 day old cultures raised on Czapek-Dox’s agar plates incubated at 28 ± 2 °C were harvested with sterile distilled water containing 0.1% Tween-80 and used as an inoculum after adjusting to the desired spore count using a haemocytometer. Bovine hides fleshing were obtained from a commercial leather processing unit.

SSF and growth conditions

Erlenmeyer flasks (250 mL) containing 10 g of solid substrates were moistened with water (70% v/w) and sterilized at 121 °C for 15 min. After cooling, the flasks were inoculated with 2% v/w inoculum containing 10⁶ spores/mL. The contents of each flask were mixed thoroughly with a sterile glass rod for uniform distribution of fungal spores in the medium and incubated at 28 °C for the fungal growth. After the incubation period, the contents from each flask were extracted for lipase enzyme and the enzyme activities were estimated every 24 h intervals for a period of 7 days.

Extraction and enzyme assay methods

The moldy wheat bran was thoroughly mixed with 100 mL of 0.1 M phosphate buffer, pH 7.0 containing 0.1% Tween-80 and shaken in an orbital shaker at 28 °C for 1 h. The contents were then filtered through cheese cloth, combined and centrifuged at 10,000 rpm for 15 min at 4 °C in a refrigerated centrifuge (Sigma 3K30) and used as a crude enzyme extract. Two methods were adopted to assay the lipase activity. Enzyme activity was assayed through alkali titration method with olive oil emulsion as the substrate, using a modified version of the procedure described by Saxena et al. (2003). In brief, the assay mixture consisting 5 mL of olive oil emulsion, 4 mL 0.1 M phosphate buffer (pH 7.0) and 1 mL crude enzyme extract was mixed well and incubated for 20 min at 37 °C. The reaction was stopped by the addition of 20 mL of acetone. This mixture was then titrated with 0.05 M NaOH in the presence of 0.1% phenolphthalein (0.1 mL) as the indicator. The titration values were used to calculate lipase activity. One unit of lipase activity is defined as the amount of enzyme required to release 1 μmol of fatty acid per minute under the standard assay conditions.

Lipase activity was also assayed by the spectrophotometric method (Kwon and Rhee, 1986). In short 50 μL of enzyme extract was added to 5 mL of olive oil emulsion and incubated for 15 min at 40 °C. Olive oil emulsion was prepared by mixing 20 g of olive oil and 100 mL of 0.1 M phosphate buffer pH 7.0, containing 10 mM CaCl₂ and 0.25% polyvinyl alcohol (PVA) in a Homogenizer (1500 rpm for 30 min). The reaction was stopped with 1 mL of 6 M HCl and incubated in a boiling water bath for 5 min. The fatty acids released were extracted in 5 mL of isooctane by vortexing for 15 min. To 2.5 mL of organic phase, 0.5 mL of a copper acetate-pyridine solution (50 g/L, pH 6.1 adjusted with pyridine) was added, vortexed for 15 min and centrifuged at 5000 rpm for 15 min and the absorbance of the organic phase was monitored at 715 nm. A calibration curve was drawn using oleic acid as a standard. One unit of activity was defined as the amount of the enzyme, which release 1 μmol of fatty acid per minute in the assay conditions. The results obtained did not show much difference in the values. The alkali titration method of Saxena et al. (2003) was followed throughout the experiments. The protein content of the crude enzyme extract was analyzed by the method of Lowry et al. (1951).

To study the potential of lipase for tannery fleshing hydrolysis, the crude culture extract as an enzyme source was ultra concentrated to 10 fold concentration using 10 Kda cut off cellulose membrane (Millipore, USA). The ultra concentrated liquid enzyme was acetone precipitated using pre chilled acetone at the ratio 1:1.2 v/v. The precipitate was collected after centrifugation at 10,000 rpm for 20 min at 4 °C, lyophilized (Virtis lyophiliser) and used for biochemical characterization.

Optimization of growth parameters for lipase production by SSF

The effect of different parameters to optimize lipase production in SSF were studied by varying one parameter at a time and the growth conditions are as described in Section 2.2. The parameters studied were initial moisture content (40, 50, 60, 70, 80 and 90%), incubation period (24 to 168 h), oil cakes (gingili, ground nut, cotton seed and coconut oil cakes), additional nitrogen sources (ammonium nitrate, ammonium sulphate, peptone, sodium nitrate and yeast extract), oil sources (castor oil, olive oil, coconut oil, gingili oil and sunflower oil) and carbohydrate sources (fructose, glucose, glycerol, lactose and xylose). The pa-
rameters optimized each time were incorporated in subse-
quently experiments. Lipase activities are expressed in units
per gram of dry weight of the fermented substrate.

**pH and temperature related activity and stability of lipase**

To study the potency of lipase to hydrolyze tannery fleshing, the effect of reaction temperature and pH on lipase
activity and its stability at various temperatures and pH were evaluated. The buffers used were: 0.02 M Sodium acet-
etate buffer (pH 4.0, 5.0), 0.02 M Potassium phosphate buffer (pH 6.0), 0.02 M Tris buffer (pH 7.0, 8.0), 0.02 M
Borate buffer (pH 9.0), 0.02 M Borax-NaOH buffer (pH 10). To determine the effect of pH and temperature on
the stability of lipase, the enzyme was pre-incubated for
30 min in various buffer solutions at different pH (5 to 10)
and at various temperatures (30 to 80 °C) and the residual
lipase activity was assayed under standard assay conditions.

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**Determination of total lipid content of tannery fleshing**

The pH of the limed fleshing was around 12-12.5. To
adjust to the required pH, the fleshing was soaked in water for
1.0-2.0 h with intermittent stirring and adjusted to required pH
level using 2 N HCl. These fleshings were used for further in-
vestigation. The total lipid content of the tannery fleshing was
estimated by the modified chloroform/methanol / water ex-
traction method (Bligh and Dyer, 1959).

**Determination of total Kjeldahl nitrogen content (TKN)**

Dried fleshing was chemically hydrolyzed using 6 N
HCl at 110 °C for 18 h till the fleshing was completely
solubilized. After hydrolysis, the total Kjeldahl nitrogen content (TKN) of the fleshing was estimated by the method of Mckenzie and Wallace (1954). The values of TKN were
multiplied by the factor 5.51 to calculate the protein content
(Taylor et al., 1997) and the results are expressed in per-
centage.

**Ash content of tannery fleshing**

The total ash content of tannery fleshing was mea-
sured by the standard test method ASTM D2617-96. Five
grams of dried tannery fleshing were weighed and placed in
a clean pre weighed crucible. The crucible was kept in a
muffle furnace at 600 ± 25 °C for 1 h, cooled in a desiccator
and weighed to constant weight. The percentage of the total
ash content of the tannery fleshing is: Total ash
(%) = weight of the ash/weight of tannery fleshing x 100.

**Fat recovery from tannery fleshing using lipase from A. tamarri MTCC 5152**

A. tamarri MTCC 5152 lipase concentrated by ultra-
filtration was used for fat hydrolysis. Ten grams of fleshing
were suspended in 3 parts of 0.1 M phosphate buffer, pH 7.0 in Erlenmeyer flasks. Enzyme solution containing
750 u/mL of lipase activity at different concentrations were
taken in the same buffer and added to the fleshing and incu-
bated at 50 °C for a specific period of time ranging from 1
to 6 h. After the incubation period, the hydrolyzate was filtered
through pre-weighed Whatman No.1 filter paper and the supernatant was used for the analysis of fat solubility by
using a modified procedure described by Saxena et al.
(2003). The protein remained as a residue in the filter paper.

All experiments were done in triplicate and the values
presented are the means of three independent determina-
tions.

**Results and Discussion**

**Effect of initial moisture content on lipase produc-
tion**

The initial moisture level of the fermentation media
plays a vital role for the optimum production of enzymes
(Pandey et al., 2000). In the present investigation, maxi-
mum lipase production was obtained in wheat bran contain-
ing 2.5% w/w gingily oil cake with 70% moisture content as
growth medium (Figure 1). Increase or reduction of
moisture level in this wheat bran-gingerly oil cake medium
resulted in lower levels of lipase production. A similar
trend was reported by Gutarra et al. (2005) with Penicilli-
num simplicissimum in solid-state fermentation using babassu
cake as the basal medium but Mahanta et al. (2008) re-
ported initial moisture content at 50% of substrate as ideal
for lipase production using Jatropha curcas seed cake.
Therefore, it is evident that the enzyme production depends
on the water holding capacity of the substrate and that it
varies in various fermentation media.

**Effect of combinations of wheat bran with various oil
cakes**

Identification of ideal agro-based oil cakes for lipase
production in a solid-state fermentation process depends
on the cost and availability of such substrates and thus in-
volves screening of several agro-industrial residues. Pan-
dey et al., 2000. The results in the present study revealed
that (Figure 2) maximum lipase activity was found on
wheat bran with 2.5% w/w gingili oil cake combination
compared to wheat bran containing other oil cakes (coco-
nut, cottonseed, groundnut studied at 0.5-10% w/w).
Ramachandran et al. (2007) indicated that lipase produc-
tion pattern varied with the type of agro-waste. This could
be attributed to the solid material’s dual role: supply of nu-
trients for microbial growth and anchorage for the grow-
ing mycelia. Kamini et al. (2000) reported maximum
production of lipase by Aspergillus niger strain
MTCC2594 by solid-state fermentation using gingili oil
cake.
Time course on enzyme production

Lipase production increased with incubation time (Figure 3). Maximum lipase production was obtained with wheat bran containing 2.5% w/w gingili oil cake (740 ± 17.44 u/g) after 120 h. A prolonged incubation time beyond this period did not help to further increase the enzyme yield which might be due to the depletion of nutrients, accumulation of toxic end products and the change in pH of the medium or loss of moisture. These results are in accordance with the observations made by Mahadik et al. (2002) for lipase production by Aspergillus niger. Several researchers have reported different incubation periods for optimal lipase production by solid state fermentation. Cordova et al. (1998) reported maximum lipase activity by R. pullis after 24 h of incubation using mixture of olive oil cake and sugarcane bagasse as substrates. Benjamin and Pandey (1997) obtained maximum production of lipase by Candida rugosa after 3 days of incubation period.

Effect of additional supplementation of oil, carbohydrate and nitrogen sources on lipase production

Results of additional supplementation of oil, nitrogen and carbohydrate sources on enzyme production by A. tamarii MTCC 5152 are shown in Table 1. Maximum lipase activity was found (782 ± 14.73 u/g) when 1% gingili oil was added to wheat bran containing gingili oil cake. Mladenoska and Dimitrovski (2001) tested several lipids for their effect on lipase production by Geotrichum candidum M 2 and obtained highest lipolytic activity using sunflower oil sediments and sunflower oil. Lima et al. (2003) reported that olive oil induces higher yield of lipase by Penicillium aurantiogriseum.

Among the nitrogen sources used peptone (0.5%) showed maximum influence in enhancing the enzyme production (787 ± 5.57 u/g). Benjamin and Pandey (1997) reported that urea was found to be the best nitrogen source for lipase production with Candida rugosa. The addition of other nitrogen sources did not show any supportive effect on lipase production.

Regarding the effects of additional carbon sources on enzyme production the results showed that glucose supported maximum production of lipase (785 ± 9.64 u/g). The addition of gingili oil (1.0%), peptone (0.5%) and glucose (0.5%) to wheat bran and gingili oil cake in SSF supported enhanced production of lipase (793 ± 6.56 u/g). Increasing peptone and glucose to 1% concentration did not show much variation (data not shown).

Effect of pH and temperature on activity and stability of lipase

The pH profile of crude lipase is displayed in Figure 4. A. tamarii MTCC 5152 lipase shows maximum activity at pH 7.0 and the enzyme was also found to retain 100% of activity in the same pH. More than 90% of activity was retained at pH 5, 6 and 8 indicating a very little decrease in activity and at pH 10.0, 72% of residual activity was found. Interestingly, the present lipase was active even at pH
ranges from 5.0 to 8.0. Lipases from *Aspergillus niger* (Sugihara et al., 1988), *Aspergillus terreus* (Ghosh et al., 1996) and *Rhizopus oligosporous* (Ul-Haq et al., 2002) were found to be stable in the pH ranges 3-10.5, 5.5-10 and 7.0-8.5, respectively. The remarkable stability of *A. tamarii* MTCC 5152 lipase at pH 5-8 justifies its potential use in neutral and moderately alkaline conditions.

Lipase activity determined at different temperatures has been presented in Figure 5. The reaction rate increased significantly over the temperature range from 30-50 °C, but then it decreased slightly. The enzyme exhibited maximum activity at 50 °C. The lipase was quite stable at room temperature and the enzyme maintained good stability and was stable up to 50 °C. At 60 °C, 90% activity was retained and above 60 °C the enzyme gradually loses its activity suggesting that the enzyme is thermostable. Moderately thermostable lipases were also reported from *P. wortmanii* and *P. simplicissimum* (Costa and Peralta, 1999; Gutarra et al., 2009). These lipases were found to retain 55% and 90%, of their residual activity at 50 °C.

**Effect of lipase concentration and reaction time on fat solubility (FS) of fleshing**

The composition of bovine hides fleshing was determined and found to contain 63% protein, 14.6% fat and 8% ash. The values are in close agreement with the values reported by Kanagaraj et al. (2006). The effect of enzyme concentration on fat solubility is given in Table 2. Maximum fat solubility (92%) was obtained using 3.0% enzyme concentration.

### Table 2 - Effect of lipase concentration and reaction time on fat solubility (FS) from tannery fleshing.

| Enzyme concentration (v/w) | Time (h) | 0.5% | 1.0% | 2.0% | 3.0% | 4.0% |
|---------------------------|----------|------|------|------|------|------|
|                           | 2        |      |      |      |      |      |
|                           | 4        |      |      |      |      |      |
|                           | 6        |      |      |      |      |      |

Figure 4 - Effect of pH on activity and stability of lipase.

Figure 5 - Effect of temperature on activity and stability of lipase.
(750 u/mL) and 90% at 2.0% enzyme concentration in 6 h of reaction time. These data shows that 92% of the fat in the fleshing can be removed using lipase from \textit{A. tamarii} MTCC 5152. The fat recovered from the tannery fleshing can be utilized as a potential raw material for the production of an environmentally friendly fuel. The residue is a rich source of protein which can be used as an animal feed particularly as a fish and poultry feed (Rai et al., 2010).

**Conclusion**

The production of an extracellular lipase using \textit{A. tamarii} MTCC 5152 cultured in SSF could be enhanced by modification of medium components with an enzyme yield of 793 ± 6.56 u/g dry weight was reached after 120 h of incubation. This production represented a high level increase of lipolytic activity compared to that obtained in earlier reports. These results are promising because this strain produces lipase in an inexpensive medium. Application of this enzyme on tannery fleshing shows 92% of fat solubility. The enzymatically recovered fat can be used for biodiesel manufacture and the residual protein as a fish or poultry feed.

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