Comparison of an Internal Combustion Engine Derating Operated on Producer Gas from Coal and Biomass Gasification

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Abstract— Producer gas is yield gases from gasification that can be burned, composed by CO, H$_2$, and CH$_4$, and non-combustible gases like CO$_2$ and N$_2$. Producer gas utilization for internal combustion engine has been studied, not only from biomass gasification but also from coal gasification. This paper compares the research that has done author using coal gasification with other research results using biomass gasification. Coal gasifier performance test conducted with capacity of 20 kg/h of coal. The proximate and ultimate analysis of raw coal, ash product and producer gas was conducted and compared. The result of analysis shows that the efficiency of the coal gasification was 61% while range of gasifier efficiency for biomass is between 50-80%. Meanwhile, the experimental results on the performance of internal combustion engines using producer gas shows that the derating for power generation using coal producer gas was 46% and biomass was 20-50% depend on compression ratio of engine and characteristic of producer gas. Therefore, concluded from the experiment result, producer gas from coal gasification is more promising as fuel for internal combustion engine.

Keywords— Coal; Biomass; Gasification; Power Generation; Internal Combustion Engine

I. INTRODUCTION

Gasification is a chemical reaction which has a purpose of changing the original solid material into gaseous compounds. By converting solid material into gaseous compounds, the combustion process becomes easier so that the combustion efficiency is increased. The sulphur and nitrogen are also easier separated to obtain cleaner flue gas. Gasification is an effective and clean way to convert coal and biomass into useful fuels and chemical feedstock’s [1], [2]. With purification of the fuels produced, they can be directly used in electricity and heat production devices, such as internal combustion engines, or gas turbines [3], [4].

Numerous studies have dealt with gasification of coal or biomass, and its producer gas for power generation. The influence of biomass producer gas fuel properties on spark ignition engines performances was studied [5] in comparison to the natural gas (methane) and digestion biogas. It was shows that to keep H$_2$ molar quota below the detonation value of 64% for the engines using syngas, characterized by higher hydrogen fraction, the excess air ratio in the combustion process must be increased to 2.2–2.8. As in [6], performance and emissions of a heavy-duty producer gas-fuelled engine are analysed and compared to other data found in the literature related to spark ignition engines. The result of this study shows power de-rating during producer gas operation exceeds 50% because of the significant reduction of the calorific value compared to natural gas operation.

Producer gas utilization for internal combustion engine has been studied, not only from biomass gasification but also coal gasification, however, the derating of the internal combustion engine for each of it has not been compared previously. This paper will discussed the comparison of an internal combustion engine derating when operated on producer gas from coal and biomass gasification.

II. METHODS

This paper compares the research that has done by author using coal gasification with other research results using biomass gasification.

A. Coal Gasifier

Coal gasifier used to generate producer gas (gasification). The gas that coming out from gasifier needs to be further cleaned before it is fed into an internal combustion engine [7]. Producer gas will be passed on purification unit to separate tar and particulate from gas. Also, it will be passed on heat exchangers to reduce the temperature before being inserted into engine. The specification of coal gasifier can be
seen in Table 1 and the parameter that necessary when producer gas will be used for fuel in internal combustion engines (IC engine) can be seen in Table 2 [8], [9].

| No. | Parameter                        | Value         |
|-----|----------------------------------|---------------|
| 1   | Gasifier                         |               |
|     | Diameter                         | 30 cm         |
|     | Height                           | 120 cm        |
|     | Water jacket                     | 10 cm         |
| 2   | Cyclone separator                |               |
|     | Diameter                         | 8 in          |
| 3   | Wind cooler                      |               |
|     | Amount of pipe                   | 24 pc         |
|     | Diameter                         | 2 in          |
|     | Length                           | 200 cm        |
| 4   | Heat exchanger                   |               |
|     | Type                             | Shell and tube|
|     | Shell diameter                   | 8 in          |
|     | Tube diameter                    | 1 in          |
|     | Length tube                       | 300 cm        |
| 5   | Scrubber                         |               |
|     | Diameter                         | 8 in          |
|     | Length                           | 200 cm        |
| 6   | Fog drop                         |               |
|     | a. Type                          | Packed bed    |
|     | b. Diameter                      | 8 in          |
|     | c. Length                        | 200 cm        |
|     | d. Media                         | Ceramic       |
| 7   | Gas holder                       |               |
|     | a. Diameter                      | 76 cm         |
|     | b. Length                        | 120 cm        |
| 8   | Desulphurizer                    |               |
|     | a. Type                          | Packed bed    |
|     | b. Media                         | Activated carbon|
|     | c. Amount                        | 3, paralleled |
|     | d. Diameter                      | 8 in          |
|     | e. Length                        | 200 cm        |

To fulfil the criteria of the gas that going to enter the motor fuel, gas producer passed into cooling and purification unit which consists of a cyclone separator, air cooler, heat exchangers, fog drop, scrubber and desulphurizer.

| Specification | Unit  | Value  |
|---------------|-------|--------|
| Tar content   | mg/Nm³ | <100   |
| Particulate content | mg/Nm³ | <50    |
| Temperature   | °C    | ≤40    |

Design of the gasifier and purification unit can be seen in Fig. 1 and Fig. 2. Cyclone separator was used to separate the particulate that carried in the gas stream. The air cooler and heat exchanger system was used to cool the gas using cooling media (air and water). During this cooling process, condensable components in the gas stream going to condensed, i.e. water, tars and phenols. Condensed component was separated from the gas stream and entered the water seal at the bottom of the air conditioning and water coolers. Scrubber was works to catch the water content, tar and phenols that still carried in the gas stream. The separation of the rest of components was done by contacting the gas and water by spraying it in counter-current mode. Fog drop was functioned to capture residual water content, tars and phenols in the form of small liquid particles (fog) and carried away with the gas flow. Residual water content, tar and phenol, was stick to the surface of the fog drop. Gas holder was used to temporarily store the gas before it passed to the desulphurizer. Desulphurizer was functioned to separate sulphur contained in gas, which consisted of H₂S, COS and R-S.

B. Internal Combustion Engine

This research used 10 kW genset with type of spark ignition engine. The specification of genset engine can be seen in Table III.
To utilize producer gas in the genset engine the fuel feed system was modified, the carburettor was replaced with mixing chamber for air and gas producer. Mixing chamber was basically a venturi pipe that connected to the engine intake manifold as can be seen in Fig. 3.

![Fig. 3 Mixing chamber for air-producer gas](image)

Low pressure of the air flow in the narrow channel at the venturi will suck up the flow of gas producer and producer gas mixed in the air flow. Comparison of air flow rate and gas producer closely arranged so that the combustion reaction was reached. The result of the calculation of producer gas stoichiometric combustion reaction showed that the mass ratio of air to gas producer was 1.25: 1 or volume ratio was 1:1 similar as in [10].

At the time of operation, the pressure was kept constant gas producer approached outside air pressure (atmospheric ± 5mmH2O), with the result that, flow of air and gas producer maintained at a volume ratio of 1:1. The experiment started by operating a motor fuel with a no-load power, for 30 minutes. Furthermore, the genset engine loading was done gradually 1kW/h. Valve opening level was set manually to maintain the flow rate of mixture air-gas producer in accordance with the needs of the power load of the motor fuel. If the power voltage decreases, the valve arrangement mixture flow rate of air - gas producers will more opened. The addition of power load was stopped when the power supply voltage below the value of 370 V.

C. Data Analysis

Coal gasifier performance test conducted with capacity of 20 kg/h coal. The proximate and ultimate analysis conducted, with ASTM D3176 and ASTM D7582, on raw coal to know its properties. It’s also conducted on the ash as a byproduct of the gasification process. The gasification gas producer will be sampled and inspected for its composition using a gas analyzer. The proximate and ultimate analysis of raw coal that used can be seen at Table IV.

### Table IV
| Parameter          | Unit          | Value     |
|--------------------|---------------|-----------|
| Proximate          |               |           |
| a. Water content   | %, a.d.b.     | 11.57     |
| b. Ash content     | %, adb        | 1.66      |
| c. Volatile matter | %, adb        | 43.42     |
| d. Fixed carbon    | %, adb        | 43.35     |

## III. RESULTS AND DISCUSSION

Producer gas is yield gases from coal gasification that can be burned, composed by CO, H2, and CH4, and non-combustible gases like CO2 and N2. Besides producer gas, coal gasification also produces ash as a by-product. The results of the analysis (TABLE V) show that the composition of ash has a volatile matter of 7.46%, water content of 4.82%, and fixed carbon of 34.3%. The calculation conducted for ash-removal rate is 5.39%.

### Table V
| Parameter          | Unit          | Value     |
|--------------------|---------------|-----------|
| a. Water content   | %, a.d.b.     | 4.82      |
| b. Ash content     | %, adb        | 53.42     |
| c. Volatile matter | %, adb        | 7.46      |
| d. Fixed carbon    | %, adb        | 34.3      |
| HHV                | kcal/kg, adb  | 3.011     |

From Table VI, it may be noted that the combustible components of the producer gas constitutes 0.04% of H2, 34.74% of CO and 0.24% of CH4. The non-combustible components of the producer gas constitute 5.09% of CO2 and 58.67% of N2. Among the combustible gases of the producer
gas, CH₄ has a higher calorific value, but its presence is very little in percentage.

TABLE VI
THE SPECIFICATION OF COAL PRODUCER GAS [11]

| Parameter          | Unit    | Value  |
|--------------------|---------|--------|
| N₂                  | % mol   | 58.67  |
| CO₂                | % mol   | 5.09   |
| CO                  | % mol   | 34.74  |
| O₂                 | % mol   | 1.21   |
| H₂                  | % mol   | 0.04   |
| CH₄ ratio          |         | 0.24   |
| HHV                | Kcal/Nm³| 1.013  |
| Tar content        | Mg/Nm³  | 4.04   |
| Particulate content | Mg/Nm³  | 11.17  |
| Temperature        | °C      | 36     |

The results of calculation of mass and energy balance of the gasification process can be seen in Fig. 4. These results show that the efficiency of the coal gasification was 61%. Range of gasifier efficiency is between 50-80% that is for coal and biomass gasification. A comparison of the performance results of the gasifier systems are presented in Table VII.

TABLE VII
A COMPARISON OF THE PERFORMANCE RESULTS OF THE GASIFIER SYSTEMS

| No     | Design parameters       | Unit     | Nurhadi et al [11] | Salam et al [12] | Plis et al [13] | Martinez et al [14] |
|--------|-------------------------|----------|---------------------|------------------|------------------|---------------------|
| 1      | Equivalence ratio       | % Mass   fraction | 36                | 25               | 29               | 29                 |
| 2      | Calorific value of the gas | Kcal/Nm³ | 1,013             | 931.50           | 1,313.65         | 1,242              |
| 3      | Ash charcoal removal rate | % Mass   fraction | 5.39              | 21               | not available    | not available      |
| 4      | Cold gas efficiency     | % Energy fraction | 61                | 49               | 57.9             | 76.7               |

Fig. 4 Mass and energy balance calculation of the coal gasification process.

Internal combustion engine performance test conducted using original fuel with octane number 92 as a comparison fuel for genset engine. It was done for performance comparison of producer gas as a fuel for genset engine with the original fuel. The results can be seen in Figure 4.

Fig. 5 The result analysis of ron 92 and producer gas as a fuel for genset [11].

The differences between the values reported are caused by the characteristics of the producer gas and the engines used. Producer gas is known as lean gas or low calorific value gas. Since, major portion of producer gas is non-combustible; the producer gas engines are operating at a de-rated design capacity. The non-combustible gas present in producer gas affects the engine’s efficiency in two ways. When using the producer gas for operating engines, most of the heat generated during combustion phase is absorbed by the non-combustible components of the producer gas itself. These non-combustible components lower the energy density of producer gas and reduce the adiabatic flame temperature.

In Refs. [19],[20] the used engines diesel and gas respectively, adapted to run with biomass producer gas, and a high CR 17: 1. In Ref [10] that use coal producer gas in spark ignition engine, the CR lower 7:1 this represents a loss of more power in engines when compared with diesel cycle adapted to work with producer gas.

IV. CONCLUSIONS

The efficiency of the coal gasification was 61% and range of gasifier efficiency is between 50-80%. Derating for power generation using coal producer gas was 46%. Meanwhile, in gaseous-fueled engines or dual-fuel engines running with biomass producer gas, the derating of power output is
approximately 20-30% for engine with CR 11:1 and 40-50% for engine with CR 7:1. The differences between the values reported are caused by the characteristics of the producer gas and the engines used. Therefore, producer gas from coal gasification is more promising as fuel for internal combustion engine.

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