STATISTICAL OPTIMIZATION OF CHITIN BIOCONVERSION TO PRODUCE AN EFFECTIVE CHITOSAN IN SOLID STATE FERMENTATION BY Aspergillus flavus

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ABSTRACT

The aim of this study is to develop a bioconversion process of chitin to chitosan in solid-state fermentation. A classical optimization of one factor at a time was performed and revealed that maximum chitin deacetylase (CDA) production can be obtained in corn medium moisturized with mineral salt solution and with an initial moisture of 1:1 level (w/v). Results showed that 3% of spore inoculum contained 1×10^6 provided maximum production of CDA enzyme (219.5 U/g solid medium) after 5 days of incubation. Moreover, process parameters were systematically evaluated to improve the bioconversion of chitin to chitosan by statistical optimization using response surface methodology. The maximum production of chitosan of was reached to 27.3 mg/g media by using 1% chitin after 15 days of incubation with predicted chitosan concentration of 26.2mg/g. From ANOVA table. Time was the most significant factor in chitosan production with F-value 1014.5 and construction of empirical model revealed that the chitosan produced in this study has a broad spectrum of antimicrobial activity against human pathogens: including Streptococcus spp., Staphylococcus aureus, Escherichia coli, Pseudomonas aeruginosa and Candida albicans.

Keyword: Bioconversion; SSF; RSM; Immobilization; CDA enzyme; Antimicrobial

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INTRODUCTION
Chitosan is a (1-4) -2- amino- deoxy-β-glucan biopolymer that broadly used in various applications such as pharmaceutical, biomedicine, food industry, water treatment, agriculture and in cosmetic. It considers as the most second abundant biopolymer after cellulose because of its bio renewability, bio degradability, biocompatibility and hydrophilicity (27). Usually, chitosan produces by an enzymatic method via chitin deacetylase (CDA) which is already obtained from different species of microorganism in particular fungi. The mycelia of various fungi such as Aspergillus niger (19), Mucor rouxii (23), Absidia coerulae, Rhizopus oryzae (24) are valuable sources of this enzyme and chitosan production. The statistical method of response surface methodology (RSM) was effectively applied in several studies to optimize fermentation variables in order to elevate the production of different microbial products. Mainly, this method involves construct an empirical model to investigate the interaction between the effected fermentation variables and the response and then statistically analyse the variance (15). On the other hand, the classical method of one factor at a time (OFAT) include alteration of one variable while keeping all other at a fixed level. This method is therefore, requires a large number of experiments to determine the optimum level which represent a real restriction. The statistical optimization is generally described as the best method to overcome the restrictions in the classical optimization in terms of laborious and time-consuming. In the present study, a statistical optimization based on central composite design was applied to optimize the bioconversion of chitin to chitosan in solid state fermentation by Aspergillus flavus. In addition, a classical method was used to optimize the production of CDA enzyme by Aspergillus flavus in order to affect positively the bioconversion process.

MATERIALS AND METHODS
Microorganism
Aspergillus flavus stock culture was cultivated on potato dextrose agar (PDA) and incubated at 30 °C for 7 days. Spores of A. flavus was prepared by adding 5 ml of sterilized distilled water to the fungal culture vial on potato dextrose agar (PDA). The surface of agar culture was gently streaked using loop. Then spore suspension was transferred to sterilized container and counted by hemocytometer.

Solid-state fermentation and classical optimization
Ten grams of solid substrate was prepared in 100 ml flask and 10ml of moisture solution was added to wet the solid content. The flasks were autoclaved at 121°C for 20 min and then inoculated with 2% of spore suspension contained approximately 1×10^6 and incubated at 30 °C for 7 days. Fermentation parameters were studied and optimized as follow: substrates of rice, corn, rice bran and wheat bran (separately and supplemented with 2% chitin) were tested for supporting growth of Aspergillus flavus and production of CDA enzyme. In addition, four different solutions were tested as a moisture solution involved distilled water, tap water, 1% chitosan and mineral salt solution contained per 1L: 2g K_2HPO_4 and 1g MgSO_4.7H_2O. These solutions were tested at five level (0.5:1, 1:1, 1.5:1, 2:1, 2.5:1 ml: g substrate). Furthermore, inoculation ratio with spore suspension that contains approximately 1×10^6 spores/ml was also tested at five level 0.5, 1, 2, 3, 4 %.

Statistical optimization of chitin bioconversion
Response surface methodology based on central composite design was applied for maximizing chitin bioconversion. Basically, chitin concentration and fermentation time are the most possible factors that may affect the bioconversion of chitin to chitosan therefore, they were selected to generate the experimental matrix by CCD with chitin concentration level from 1 to 3 % and incubation time from 5 to 15 days. The matrix was designed with 12 runs and four replications of centre point, four axial points and four factorial points. All runs (flasks) were prepared as described in the previous section under optimal conditions for CDA enzyme production. At the end of incubation, chitosan weight was measured.

Preparation of chitin
Chitin was prepared from three different sources, which then used as a substrate for the bioconversion process to produce chitosan. The procedures used to prepare chitin sources was based on the methods described by (31)
for fungal chitin; (3) for chitin from mushroom and (26) for chitin from shrimp shell.

**Determination of CDA enzyme activity**

CDA enzyme was first extracted from the solid fermented substrate after 5 days of incubation by adding 40 ml of distilled water and then the mixture was shaken for 2 hr. Thereafter, the mixture was filtered by cotton gauze and then centrifuged at 10000 rpm for 30 min at 4°C. The enzyme activity in the supernatant was measured according to the method described by Sun and Coworkers (22) which based on measuring the amount of 4-nitroaniline released from 4-nitroacetanilide at OD 400 nm. One unit of CDA is defined as the enzyme activity that release 1μg of 4-nitroanilin per hour from 4-nitroacetanilid under standard assay conditions.

**Chitosan determination**

At the end of incubation, solid mass was homogenized, and 1M NaOH (1:30 w/v) was added to extract residual proteins and other alkali insoluble materials (AIMs). The mixture was then autoclaved at 121°C and 15 psi for 15 min. Thereafter, AIMs were recovered and then washed several times with distilled water to obtain neutral pH. Next, the washed AIMs were dried at 60°C overnight and then weighed. Chitosan was extracted from AIM with 2% acetic acid (1:40 w/v) in an autoclave for 15 min followed by centrifugation at 10000rpm for 15 min. AIMs were discarded and pH of the supernatant was adjusted to 10 with 4M of NaOH which then left overnight at room temperature. Thereafter, the liquid was centrifuged to collect the precipitate and then washed with distilled water and weighed. The precipitated chitosan was washed with 95% ethanol (1:20 w/v) and acetone (1:20 w/v) and then dried at 60°C (18).

**Characterization of chitosan**

Fourier transform infrared spectroscopy FT-IR analysis was evaluated for the produced chitosan and compared with a commercial chitosan (company). The analysis was achieved using dried chitosan mixed with KBr powder which pressed into pellet for FTIR spectroscopy with frequency range of 4,000–400 cm⁻¹. Viscosity of chitosan was determined in 2% acetic acid solution using a viscometer (type/C-timing bulbs) at 25°C (19). Degree of deacetylation of chitosan was determined according to Yuan and coworker (32) as follow: 10 mg of chitosan was dissolved in 10 ml of 0.01M HCl-solution. After the chitosan dissolved completely, the solution was diluted to 100 ml with de-ionized water. The concentration of N-acetylglucosamime was determined from the standard curve of different concentrations of N-acetylglucosamine at 199nm. The degree of deacetylation was determined according to equation:

$$DDA = 100\% - C1/C$$

Where:

- $C1 = \text{Acetyl concentration of sample (OD 199nm)}$
- $C = \text{Concentration of sample (0.1 mg/ ml)}$

**Chitosan as an antimicrobial agent**

Antimicrobial activity of chitosan was tested against human pathogenic microorganisms of *Streptococcus*, *Staphylococcus aureus*, *Escherichia coli* and *Pseudomonas aeruginosa*. As well as against *Candida spp.* by well diffusion method as described by Johney et al., (14).

**Chitosan as a support material for enzyme immobilization**

Peroxidase enzyme was immobilized in a covalent linkage to chitosan based on the method described by Carrara and Ruubiolo, (7). one gram of the produced and commercial chitosan, separately, was added to 10 ml of 2% gluteraldehyde solution and mixed for at least 2 hours at 4°C followed by incubation overnight at the same temperature. In order to remove the unbounded glutaraldehyde, the glutaraldehyde-bounded chitosan was washed 4 times with distilled water and then mixed with 10 ml of crude enzyme solution which then left at least 24 hours at 4°C. Next, chitosan – glutaraldehyde – peroxidase conjugate was separated from the solution and the free peroxidase activity was determined. The resulted conjugated chitosan was washed with 50 ml of distilled water under vacuum pump. Immobilization with chitosan was tested by using peroxidase enzyme extracted from red radish by using sodium phosphate buffer (pH 7) according to the method described by Silva and coworkers (20). The activity of peroxidase enzyme was determined based on the method of Whitaker and Bernhard (28). The ratio of enzyme
immobilization for both produced and commercially chitosan was calculated according to the following equation:
\[
\text{Immobilization ratio (\%)} = \frac{\text{free enzyme activity/number of immobilized enzyme unit}}{\text{initial enzyme activity/number of free enzyme unit}} \times 100
\]

**Application of immobilized peroxidase in chitosan for dyes decolonization**

The black, red, yellow and blue textile dyes obtained from Al-diwanyiah textile factory in Iraq, were used for testing the decolorization capability of immobilized peroxidase in chitosan, the method was described by Al-Assadi et al., (1) with some modification as follow: the reaction mixture for the degradation of dyes contained 5 ml (w/v) of each dye and 1 ml of free enzyme or 0.2g of immobilized peroxidase in produced or commercial chitosan. The reaction mixture was incubated at 30°C for 24 hours. The blanks included 5 ml of each textile dye, separately with 1 ml of distilled water. After the end of incubation, centrifuge at 3000rpm for 10 min was performed and then the percentage of removal efficiency for each dye was calculated via measuring the absorbance at max λ according to (33). Then the percentage of dyes degradation was estimated according to the following equation:

\[
\text{Dye decolorization} = \frac{A - B}{A} \times 100
\]

Where:
- A: initial absorbance
- B: final absorbance

**RESULTS AND DISCUSSION**

Chitin deacetylase enzyme (CDA enzyme) catalyzes the bioconversion of chitin to chitosan via the deacetylation of N-acetylglucosamine. Therefore, the amount of this enzyme produced in the medium can basically represent one of the most important parameters that control the bioconversion process. Thus, for the development of a controllable process for the bioconversion of chitin to chitosan, it was necessary to determine the optimal conditions that lead to maximize the production of CDA enzyme in the solid medium. Classical optimization of one factor at a time method was performed in order to determine the solid substrate and moisture solution as well as the level of moisture and inoculum that support maxim production of CDA. As can be seen in fig. (1) corn supporting with 2% chitin showed the highest production of CDA with approximately 219.5 U/g substrate. moreover, initial moisture is a vital parameter in solid substrate fermentation that can significantly affect both the growth and enzyme production. Based on the results presented in figure 1, maximum production of CDA was obtained in culture moisturized with 1:1 level (w/v) of mineral salt solution. Furthermore, five inoculation levels of the fungus spore suspension were examined ranging from 0.5 to 4 % each contains a fixed concentration of spores. According to the results presented in fig. (1), 3 % of spore inoculum provide maximum production of CDA enzyme under the experimental conditions used in this work. Therefore, in order to achieve the bioconversion process in the solid substrate fermentation, and to ensure that maximum amount of chitin can be converted to chitosan, the bioconversion was performed under conditions described in Fig.1. The next step in this work was to find the optimal conditions for chitosan production statistically by RSM via evaluating two fermentation parameters; time and chitin concentration; that basically represent the factors that govern the bioconversion process, Table 1 shows the level and range of each parameter. Twelve experiments were conducted by central composite design matrix as elucidated in Table 2 which also show the actual and predicted response for each run.

| Table 1. Variables and their levels in the experimental design |
|-----------------|---|---|---|---|---|
| factor          | -α | -1 | 0  | 1  | +α |
| Time (day)      | 2.92 | 5  | 10 | 15 | 17.07 |
| Chitin (%)      | 0.58 | 1  | 2  | 3  | 3.4  |
Figure 1. Optimum conditions for CDA enzyme production by *Aspergillus flavus* in solid-state fermentation

Table 2. Central composite design matrix in uncoded units along with actual and predicted response for chitosan production

| Std | Run | point type | Time (day) | Chitin (%) | Chitosan (mg/g) |
|-----|-----|------------|------------|------------|-----------------|
|     |     |            |            |            | Actual | Predict |
| 2   | 1   | Fact       | 15         | 1          | 27.3   | 26.2 |
| 4   | 2   | Fact       | 15         | 3          | 23.38  | 22.7 |
| 9   | 3   | Center     | 10         | 2          | 16.8   | 16.8 |
| 1   | 4   | Fact       | 5          | 1          | 5.25   | 5.1  |
| 6   | 5   | Axial      | 17.07      | 2          | 26.6   | 27.62|
| 11  | 6   | Center     | 10         | 2          | 16.1   | 16.8 |
| 5   | 7   | Axial      | 2.92       | 2          | 0.7    | 0.52 |
| 12  | 8   | Center     | 10         | 2          | 17.5   | 16.8 |
| 10  | 9   | Center     | 10         | 2          | 16.8   | 16.8 |
| 3   | 10  | Fact       | 5          | 3          | 5.39   | 5.65 |
| 7   | 11  | Axial      | 10         | 0.585786   | 15.96  | 16.7 |
| 8   | 12  | Axial      | 10         | 3.414214   | 14.7   | 14.77|

Based on response values and data analysis as well as from the fit summary analysis, quadratic model was the most suggested model for chitosan production according to lake of fit test and P-value (0.169). Analysis of variance, ANOVA, for quadratic improved model was performed to check adequacy and significance of model Table 3. Model fitness was evaluated using determination coefficient \( R^2 \) which was 0.994 indicating that 0.006 of total the variation was not explained by the model. Adequate precision for chitosan was 45.05; this value was used for measuring signal to noise which believed to be desirable greater than 4. The adjusted and predicted determination coefficients for chitosan were
0.989 and 0.962 respectively which are accepted values as the difference between them is less than 0.2. From the table of ANOVA for chitosan production, it can be seen that all terms show significant effect except for B2 (chitin %) which is not significant. Since most of the P value data show 0.001, therefore the highest significant factors can be determined through F-value. A-time shows the most significant factor affecting on chitosan production with F-value 1014.53 followed by A² with F-value 16.4. In addition, a regression equation which is empirical relationship between tested variables and response was generated. After analysis of variance and estimation of regression coefficient, the experimental design was fitted in second order polynomeal equation and in coded factors where A: time, B: chitin concentration

\[
\text{Chitosan} = 16.8 + 9.58 A - 0.695 B - 1.015 A^2 - 0.525 B^2 \ldots 1
\]

| Table 3. ANOVA analysis of quadratic model for chitosan production base on CCD |
|----------------- |---------- |-------- |---------- |-------------- |---------- |
| Source          | Sum of Squares | df | Mean Square | F Value | p-value Prob > F |
| Model           | 755.086     | 5  | 151.0172    | 208.5224 | <0.0001 significant |
| A-Time          | 734.7503    | 1  | 734.7503    | 1014.533 | <0.0001 |
| B-chitin        | 3.866854    | 1  | 3.866854    | 5.339297 | 0.0602 |
| AB              | 4.1209      | 1  | 4.1209      | 5.69008  | 0.0544 |
| A^2             | 11.92464    | 1  | 11.92464    | 16.46537 | 0.0067 |
| B^2             | 1.764       | 1  | 1.764       | 2.435706 | 0.1696 |
| Residual        | 4.345352    | 6  | 0.724225    |         |          |
| Lack of Fit     | 3.365352    | 3  | 1.121784    | 3.434033 | 0.1690 not significant |
| Pure Error      | 0.98        | 3  | 0.326667    |         |          |
| Cor Total       | 759.4314    | 11 |            |         |          |

In addition to correlation, regression analyses can be used to assess the best fit of a line using the equation \(y = b_0 + b_1x\). The ideal line of best fit will have the sum of the squares of the distances from \(x\) to the line of fit as small as possible. The diagnostic of normal residual demonstrated in Fig. 2 indicate that residual behavior followed normal distribution and was quadratic, which is the more important assumption for checking statistical modeling. Moreover, the predicted output values versus actual experimental values for chitosan production are presented in Fig. 3. From this figure, it can be noted that the experimental values were in a significant agreement with values calculated by the predictive quadratic model with a satisfactory correlation. Therefore, it can be said that the developed model is suitable for predicting chitosan concentration under suggested conditions.

Figure 2. Normal probability plot of standardized residuals of quadratic model based on CCD for chitosan production
Design expert 7 software in order to determine the best time and chitin concentration that give maximum concentration of chitosan. Results showed that maximum predicted concentration of chitosan can be produced with the optimum incubation time (15 day) and chitin concentration (1%) is 26.2 mg/g. In order to verify the suggested optimum conditions and determine the accuracy of model, an experiment was conducted in duplicate using chitin from three different sources (Fungus, shrimp shell, mushroom) all were prepared in the laboratory as described earlier in materials and methods. As can be seen in Fig. 5, the amounts of chitosan produced by the bioconversion process were approximately similar ranging from 24.1 to 25.2 mg/g which approximately closed to the predicted value. However, the degrees of deacetylation were different. In addition, Fig. 5 shows the maximum degree of deacetylation was observed in chitosan obtained from fungal chitin (78.4%) whereas the minimum DDA was in the chitosan produced from the shrimp shell (74.8%). In general, the most common sources of chitin were crab shells and from shrimps which are wastes of marine products (2). During the last years, chitin extracted from fungal mycelia has gained more interesting (3). In reviewing the literature, a strong relationship between degree of chitin crystallinity and CDA activity has been reported. In this context, Cai et al., (6) reported that water-soluble chitosan and chitin produced from A. niger were amorphous, whereas the crystallinity of chitin from shrimp was high that made the interaction between its molecules robust. Therefore, in such a case, it is difficult for the CDA enzyme to access the acetyl groups. Thus, in order to increase the deacetylation rate for shrimp chitin, a pretreatment of destroying the crystalline structure is required prior to bioconversion process. In addition, Cai et al., (6) found that enzyme produced from Scopulariopsis brevicaulis had high deacetylating activity on chitin obtained from A. niger mycelium (37% deacetylation), whereas the activity on shrimp crystalline chitin was 3.7%. On the other hand, the degree of deacetylation for the produced chitosan was investigated during the bioconversion process. As can be seen from
the Fig. 6, the amounts of chitosan produced after 3 days of incubation was few (2.1 mg/g) and then increased during the fermentation reaching to the optimum after 15 days of incubation. However, degree of deacetylation was a little high after 3 days of incubation (83.35%) and then decreased slightly to (81%) after 15 days of incubation. Bioconversion of chitin to chitosan were investigated for several years since the first observation of CDA enzyme, though, a high degree of deacetylation is still difficult to attain, principally because of the insoluble and crystalline nature of chitin (4). Therefore, in order to obtain an efficient biotransformation, several techniques were used to improve chitin properties via reducing its crystallinity and hence, effect the amorphous structure of chitin which is necessary for CDA to access and produce chitosan (5). Examples of these techniques involved grinding, interaction with saccharides, sonicating, and heating (29). The degree of deacetylation is an important parameter as it is affecting the physicochemical properties of chitosan. Chitosan with high degree of deacetylation has high positive charges that make it more appropriate for different application in food and medicine (10). It is widely mentioned that, chitosan produced by the thermochemical deacetylation process is non-specific with great inconsistency in the degree of deacetylation (30).

Figure 5. Production and degree of deacetylation of chitosan produced by Aspergillus flavus using chitosan obtained from mold, shrimp shell and mushroom in solid-state fermentation.

Figure 6. Degree of deacetylation of chitosan produced in different time during the bioconversion of fungal chitin in solid-state fermentation by A. flavus

FT-IR spectrum (4000 to 400) cm\(^{-1}\) was used to identify and confirmed the characteristic functional groups of the produced chitosan. The isolated fractions gave IR spectra similar to that of the commercial chitosan from crab shells. As can be seen from the FT-IR spectra presented in Fig. 7, a broad absorption band in the range of 3000 cm\(^{-1}\) – 3500 cm\(^{-1}\) is found which is attributed to O–H stretching vibrations and at 1400-1650 cm\(^{-1}\) refer to C=O bond (9). In addition, the peaks around 2885, 1650, 1589,1326 and 1080 cm\(^{-1}\) are assigned to the stretching vibrations of aliphatic C–H, Amide I (-NH deformation of –NHCOCH\(_3\)), Amide II, Amide III and C–O–C, bonds respectively (11). According to IR spectra results, the basic molecular structure of both produced and commercial chitosan is significantly similar. On the other hand, the dynamic viscosity of the produced chitosan was 5.6 centipoises (cP), which is considerably lower than the viscosity of the commercial chitosan 25.77 (cP). In this context, Khalaf (16) reported that chitosan produced by fungal strain Rhizopus oryzae in rice straw in SSF for 12 days was 6.8 centipoises (cP).

Chitosan as an antimicrobial agent

In recent years, there has been an increasing amount of literature that investigated the spectrum activity of chitosan against different group of human pathogenic microorganisms (14). It is believed that the mechanism of antimicrobial chitosan activity is based mainly on its interaction with anionic groups on the cell surface, due to its polycationic nature, that
causes the formation of an impermeable layer around the cell, which consequently prevents the transport of essential solutes (12). The antimicrobial activity of chitosan produced in this work was evaluated against some human pathogenic microorganisms. As can be seen in Table 4 and Fig. 8, a significant activity was observed for chitosan produced in this study against all tested microorganisms at a level similar to that observed with commercial chitosan. Interestingly, the results, as shown in Table 4, indicate that the inhibitory activity of chitosan was rather more than the antimicrobial activity of Amikacin disc, which certainly has important implications for future work.

Table 4. Antimicrobial activity of chitosan against some pathogenic microorganisms

| Strain                  | Diameter of inhibition zone (mm) |
|-------------------------|----------------------------------|
|                         | Commercial chitosan | Produced chitosan | Amikacin disc (30μg) |
| *Escherichia coli*      | 25                  | 24                | 19                    |
| *Pseudomonas aeruginosa*| 26                  | 25                | 18                    |
| *Streptococcus spp.*    | 25                  | 25                | 19                    |
| *Staphylococcus aureus* | 28                  | 28                | 14                    |
| *Candida spp.*          | 19                  | 20                | 17                    |

![Figure 7. FT-IR spectra of commercial and produced chitosan from A. flavus](image)

![Figure 8. Antimicrobial activity of commercial chitosan (1), produced chitosan (2), Amikacin disc (30μg) (3) and 0.1% acetic acid as a control (4) against different pathogenic microorganisms](image)

Chitosan as a support material in peroxidase immobilization

Peroxidase enzyme catalyze the oxidative polymerization of phenolic compounds resulting insoluble polymers, however the lifetime of this enzyme is generally short (13). In order to overcome this drawback, the enzyme is used in the immobilized form and
therefore, it can be used with a long lifetime (34). The immobilizing process of an enzyme to an activated support is leading to reduce or loss the mobility of the enzyme. This technique causes a rigidification in the enzyme structure which decreased any possible conformational changes in the enzyme that cause inactivation and therefore, rising the stability of enzyme (17). One of the supported materials that successfully used for the immobilization of enzymes is chitosan. Crude peroxidase extract from red radish was immobilized by covalent linkage in chitosan produced in this study. As can be seen in Table 5, immobilization was performed by adding free peroxidase enzyme with an activity of 561.44 U/ml. Results showed that immobilization ratio of the enzyme to the produced chitosan was 63.10% in comparison with commercial chitosan which was 75.50%.

In this context, Chagas et al, (8) reported, based on their results, that chitosan was efficient for covalent immobilization of soya bean hull peroxidase. In addition, Skoronski et al, (21) immobilized laccase enzyme isolated from Asperigellus sp. in gluteraldehyde-activated chitosan with an immobilization ratio of up to 90% at 40°C.

Application of immobilized peroxidase in chitosan for dye decolorization
Nowadays, phenols and their derivatives are discarded into the environment from different sources. These compounds are widely used in the manufacturing process of petroleum refieries, papers, pestisides, dyes, drugs, plastics and textiles. Thus, the handling of indesterial wastes containing aronatic compounded is required prior to their final release into the environment. One of the technique that successfully used in the degradation of phenolic compounds is the utilization of peroxidases enzyme.

Table 5. Peroxidase immobilization using chitosan produced from Asperigellus flavus in comparison with commercial chitosan

|                         | Free peroxidase enzyme | Produced chitosan | Commercial chitosan |
|-------------------------|------------------------|-------------------|---------------------|
| Free enzyme (U/ml)      | 561.44                 | 207.15            | 137.45              |
| Immobilized enzyme (U/mg) | 100.67                 | 125.12            |
| Number of immobilized units | 354.29                 | 423.99            |
| Immobilized ratio (%)   | 63.10                  | 75.51             |

In this study, the degradation capability of immobilized peroxidase with produced and commercial chitosan was studied using yellow, red, blue and black textile dyes at a concentration of 30mg/liter for 24hrs. The absorbance of each dye was recorded at a suitable wave length for each one. As can be seen in Table 6, textile black exhibited higher degradation capacity with peroxidase that immobilized in commercial chitosan with maximum removal extent of 41% after 24 hrs, followed by textile red (31%), then textile blue (24.3%) and finally textile yellow (21%). Whereas, immobilized peroxidase in produced chitosan gave the highest result of removal dye in black, red, blue and yellow textile with removal extent of 34, 27, 22.2 and 19.4% respectively. Moreover, free peroxidase has approximately the same effect to degrade dyes compared with the immobilized form. Furthermore, results in Table 6 revealed that these dyes were not decolorized at the same extent because each dye has different structure and redox potentials. This certainly affect the suitability of their steric structure with the active site of the enzyme and consequently the degradation capability of free peroxidase and that immobilized (25).
Table 6. Dyes decolorization of free and immobilized peroxidase with produced and commercially chitosan after 24 hr at time of incubation

| Dyes          | Free peroxidase | Immobilized enzyme |
|---------------|-----------------|--------------------|
|               |                 | commercial chitosan | produced chitosan |
| Textile black | 32              | 41                 | 34                |
| Textile yellow| 17.3            | 21                 | 19.4              |
| Textile red   | 25.2            | 31                 | 27                |
| Textile blue  | 20              | 24.3               | 22.2              |

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