Article

Entropy Generation via Ohmic Heating and Hall Current in Peristaltically-Flowing Carreau Fluid

Saima Noreen 1, Asif Abbas 1 and Abid Hussanan 2,3,*

1 Department of Mathematics, Comsats University Islamabad, Tarlai Kalan Park Road, Islamabad 44000, Pakistan; saima.noreen@comsats.edu.pk (S.N.); aacbalti@gmail.com (A.A.)

2 Division of Computational Mathematics and Engineering, Institute for Computational Science, Ton Duc Thang University, Ho Chi Minh City 700000, Vietnam

3 Faculty of Mathematics and Statistics, Ton Duc Thang University, Ho Chi Minh City 700000, Vietnam

* Correspondence: abidhussanan@tdtu.edu.vn

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Abstract: The core objective of the present study is to examine entropy generation minimization via Hall current and Ohmic heating. Carreau fluid considerations interpret the unavailability of systems’ thermal energy (for mechanical work). The magneto hydrodynamic flow is in the channel, which is not symmetric. We have solved analytically the resulting nonlinear mathematical model. Moreover, physical exploration of important parameters on total entropy generation, temperature, and Bejan number is plotted and discussed. We observed that the generation of entropy takes place throughout the confined flow field $y = W_1$ and $y = W_2$ because of the viscous dissipation effect. In addition, reducing the operating temperature minimizes the entropy.

Keywords: entropy; peristalsis; Carreau fluid; heat transfer; perturbation; pumping and trapping

1. Introduction

Currently, scientists have a major concern about finding a way to control the wastage of heat energy. In thermodynamics, entropy defines thermal irreversibility, often referred to as the destruction of useful energy. Production of entropy is associated with all real-life processes. Entropy generation analysis is important in exploring the sources and location of irreversibilities, which are responsible for the destruction of useful energy. The losses in heat energy are mainly due to friction, compression and expansion, heat transfer, magnetic field, and chemical reactions. Minimizing the loss of heat and improving the efficiency of the thermal system are possible only through minimization of entropy generation. Therefore, it is extremely important to study entropy in all real processes. Different techniques are being used to decrease the entropy generation, such as the reduction in size of chip components in a computer, cooling fans preventing overheating, porous media, and the heat exchanger.

The laws of thermodynamics define the transformation of energy. The quantity of energy in the heat transfer process is an important factor and is governed by the first law. Hayat et al. [1] studied the impact of the Cattaneo–Christov heat flux model in the flow of variable thermally-conductive fluid. Khan et al. [2] explained the homogeneous-heterogeneous reactions in Casson fluid flow. Most of the engineering problems concern with the quality of energy and the degree of degradation of energy. The second law of thermodynamics defines the decrease in the quality of energy, such as the reduction in the quality of energy measured as entropy. In order to minimize the entropy generation within the fluid flow problem, it is important to learn the distribution of entropy generation. Bejan [3] laid the foundation of entropy generation and analyzed its minimization. Afridi et al. [4] developed the analysis of heat and mass transfer in entropy generation. In another study, Afridi et al. [5] analyzed entropy in hydromagnetic boundary flow. Rashidi et al. [6] studied the entropy generation on peristaltic MHD...
(magnetohydrodynamic) blood flow. In another article, Rashidi and his coworker analyzed the entropy generation of third-grade fluid over a stretching sheet [7]. Entropy generation in the flow of nano fluids with silver and copper nanoparticles was studied by Hayat et al. [8]. Khan et al. in his studies [9,10] also explained the ways of entropy generation minimization. Recently, some research works [11–16] investigated the entropy production numerically by LBM (Lattice Boltzmann Method).

Flows affected by magnetic field have crucial applications in various fields. MRI (magnetic resonance imaging), MHD pumps, the petroleum industry, plasma physics, etc., are few of the many modern applications. Moreover, when the magnetic field is strong, the Hall effect cannot be neglected. The Hall current and magnetic field have a strong effect on flow and heat transmission characteristics. Applications include the Hall accelerator, MHD accelerator, power generator, electric transformer, and refrigeration coils and heating elements. Hall current and the magnetic field are also used in MRA (magnetic resonance angiography), which scans the images of veins and arteries in order to analyze abnormalities of blood vessels, specifically arteries of brain, neck, thoracic aorta, and renal arteries. Abbasi et al. [17] developed numerical analysis for the peristaltic flow in a curved channel. Bhatti and Rashidi [18] examined the mass and heat transfer through the Hall current and Joule heating effects in blood flow. Recently, Noreen et al. [19] studied the effects of Joule heating and ion slip. Hayat et al. [20] studied the MHD viscous fluid flow phenomenon in the rotating channel. Qasim and Noreen [21] discussed the Hall current and viscous dissipation effect of pseudoplastic fluid. Some supplementary studies pursuing the same direction can also be found in [22–24].

Owing to real-life applications, peristaltic fluid motion has received considerable attention in the last few years. Peristaltic flow is a transport phenomenon in which fluid is carried forward through contractions and expansions. Significant industrial applications include the peristaltic pump, roller pump, blood pump, sanitary and sterile transport, etc. Physiologically, movement of food in esophagus, urine in ureter, blood in arteries, bile in bile ducts, etc., are based on this mode. Latham [25] laid a strong foundation for theoretical development in this area. He first addressed the peristaltic flow of viscous fluid. Shapiro et al. [26] extended the generalized concept under certain assumptions on peristaltic pumping. Asghar et al. [27] examined the variable viscosity of a viscous fluid. Vajravelu et al. [28] studied the peristaltically-flowing Phan-Thien–Tanner fluid of porous media in an asymmetric channel. Numerous examinations dealing with peristaltic fluid flows under different assumptions and flow geometry were reported with experimental, numerical, and analytical approaches. Some remarkable decisive studies were mentioned in [29–33].

The non-linear relationship between stress and strain rate is explored by selecting the Carreau fluid model, where the viscosity is dependent on the shear rate. This model is a blend of the power law and Newtonian models, competent for describing the flow behavior of shear thickening, as well as shear thinning fluids. Noreen et al. [34] analyzed peristaltic transport of Carreau fluid in a curved channel. In another article Hayat et al. [35] studied it with different boundary conditions.

In present study, the non-linear relationship between stress and strain rate is explored by selecting the Carreau fluid model, where the viscosity is dependent on the shear rate. This model is a blend of the power law and Newtonian models, competent for describing the flow behavior of shear thickening, as well as shear thinning fluids. Noreen et al. [34] analyzed peristaltic transport of Carreau fluid in a curved channel. In another article, Hayat et al. [35] studied the same model with different boundary conditions.

No study is available in the literature that explores the entropy generation of Carreau fluid flow. We present the state-of-the-art present entropy analysis of flow augmented by Hall current and Joule heating. Flow is in a two-dimensional channel with convective boundaries. The study is organized into five sections:


2. Mathematical Model and Analysis

2.1. Flow Characteristics

The Carreau fluid of constant density, moving in a channel, which is asymmetric in nature, is considered here. The rectangular coordinates are \((X, Y)\) with \(U\) as the axial velocity component. Channel walls are maintained at temperatures \(T_0\) and \(T_1\). The velocity field is mathematically defined by \((U, V, 0)\). The walls of the geometry are given as:

\[
\begin{align*}
W_1 &= b_1 \cos \left( \frac{2\pi}{\lambda} (X - st) \right) + d_1 \\
W_2 &= -b_2 \cos \left( \frac{2\pi}{\lambda} (X - st) + \phi \right) - d_2
\end{align*}
\]

where \(W_1\) and \(W_2\) represent the lower and upper walls, \(b_1, b_2\) the amplitudes, \(\phi\) the phase difference, \(s\) the wave speed, \(\lambda\) the wavelength, and \(t\) the time. The geometry of the flow problem is given in Figure 1.

![Physical model of the problem.](image)

The Lorentz body force and Joule heat affecting the flow are determined by:

\[
\vec{F} = \vec{J} \times \vec{B}
\]

\[
\text{Joule heating effect} = \frac{1}{\sigma} \vec{J} \cdot \vec{J}
\]

Here, \(\vec{J}\) shows the current density \(\vec{B}\) for the magnetic field, and \(\sigma\) represents the electric conductivity of the fluid. The constitutive laws of mass, momentum, and energy via the Joule heating, Hall current, and viscous dissipation are:

\[
\frac{d\rho}{dt} + \nabla \cdot \vec{V} = 0, \quad (4)
\]

\[
\rho \frac{d\vec{V}}{dt} = \text{div } S - \vec{J} \times \vec{B}, \quad (5)
\]

\[
\rho C_p \frac{dT}{dt} = \kappa \nabla^2 T + \tau \cdot \left( \nabla \cdot \nabla \vec{V} \right) + \frac{1}{\sigma} \vec{J} \cdot \vec{J}, \quad (6)
\]

where \(S = - \rho I + \tau, \rho\) shows density, \(\kappa\) is the thermal conductivity, \(C_p\) the specific heat, and \(\tau\) the extra stress tensor.
2.2. Fluid Model

The stress-strain relationship of the Carreau fluid model is:

$$\dot{\tau} = \left[ \eta_\infty + (\eta_\infty - \eta_0) \left( 1 + (\dot{\gamma})^2 \right)^{\frac{\alpha-1}{2}} \right] \dot{\gamma},$$

and here, $\eta_\infty$, $\eta_0$ are infinite and initial shear rate viscosities and $\dot{\gamma} = \sqrt{\text{trace} A_t^2}$. The components of extra stress tensors $\tau_{ij}$ are:

$$\tau_{XX} = -2\eta_0 \left[ 1 + (\dot{\gamma})^2 \right] \frac{\partial U}{\partial x},$$

$$\tau_{XY} = -\eta_0 \left[ 1 + (\dot{\gamma})^2 \right] \left( \frac{\partial U}{\partial y} + \frac{\partial V}{\partial x} \right),$$

$$\tau_{YY} = -\eta_0 \left[ 1 + (\dot{\gamma})^2 \right] 2\frac{\partial V}{\partial y}.$$

2.3. Development Problem

The transformation:

$$\xi = \bar{X} - \bar{c}, \; \eta = \bar{V}(\bar{X}, \bar{Y}, \bar{t}), \; \bar{y} = \bar{Y}, \; \bar{t} = \bar{T}(\bar{X}, \bar{Y}, \bar{t}), \; \bar{u} = \bar{U}(\bar{X}, \bar{Y}, \bar{t}) - \bar{c},$$

convert Equations (4)–(6) to:

$$\frac{\partial \bar{u}}{\partial \xi} + \frac{\partial \bar{v}}{\partial \eta} = 0$$

$$\rho \left( \bar{u} + c \right) \frac{\partial \bar{u}}{\partial \xi} + \bar{v} \frac{\partial \bar{u}}{\partial \eta} = \frac{\bar{F}_{\tau \tau}}{\partial \xi} + \frac{\bar{F}_{\tau \eta}}{\partial \eta} - \frac{\sigma B_0^2}{1 + m_c^2} \left( (\bar{u} + c) - m \bar{v} \right) - \frac{\partial \bar{p}}{\partial \xi},$$

$$\rho \left( \bar{u} + c \right) \frac{\partial \bar{v}}{\partial \xi} + \bar{v} \frac{\partial \bar{v}}{\partial \eta} = \frac{\bar{F}_{\tau \tau}}{\partial \xi} + \frac{\bar{F}_{\tau \eta}}{\partial \eta} - \frac{\sigma B_0^2}{1 + m_c^2} \left( \bar{v} - m(\bar{u} + c) \right) - \frac{\partial \bar{p}}{\partial \eta},$$

$$\rho C_p \left( \bar{u} + c \right) \frac{\partial \bar{u}}{\partial \xi} + \bar{v} \frac{\partial \bar{u}}{\partial \eta} = -\frac{\sigma B_0^2}{1 + m_c^2} \left( (\bar{u} + c)^2 - \bar{v}^2 \right) + \frac{\partial \bar{u}}{\partial \xi} \bar{\tau}_{\tau \tau} + \frac{\partial \bar{v}}{\partial \eta} \bar{\tau}_{\tau \eta} + \frac{\partial \bar{u}}{\partial \eta} \bar{\tau}_{\tau \eta} + \frac{\partial \bar{v}}{\partial \xi} \bar{\tau}_{\eta \eta} + \kappa \left( \frac{\partial^2 \bar{u}}{\partial \xi^2} + \frac{\partial^2 \bar{u}}{\partial \eta^2} \right).$$

Introducing dimensionless variables and parameters:

$$u = \frac{\bar{u}}{c}, \; x = \frac{\bar{X}}{\bar{L}}, \; t = \frac{\bar{t}}{t_0}, \; y = \frac{\bar{Y}}{\bar{L}}, \; v = \frac{\bar{V}}{\bar{V}_c}, \; M_f = \frac{\sigma B_0^2 \bar{c}^2 \bar{L}^2}{\eta_0}, \; p = \frac{\bar{p}}{\bar{c} \bar{L}_0}, \; \tau_{\infty} = \frac{\bar{\tau}_{\tau \tau}}{\bar{c} \bar{L}_0},$$

$$\tau_{xy} = \frac{d_{x,y}}{c_{x,y}}, \; \tau_{yy} = \frac{d_{y,y}}{c_{y,y}}, \; \theta = \frac{\bar{T} - T_0}{T_1 - T_0}, \; Pr = \frac{\mu \bar{c}}{\bar{V}_c}, \; Ec = \frac{c^2}{(T_1 - T_0) \bar{c} \bar{L}_0},$$

$$W_1 = \frac{\bar{W}_1}{\bar{L}}, \; W_2 = \frac{\bar{W}_2}{\bar{L}}, \; \delta = \frac{\bar{\delta}}{\bar{L}}, \; Re = \frac{\bar{c} \bar{L}_0}{\eta_0}, \; u = \frac{\partial \bar{u}}{\partial \xi}, \; v = \frac{\partial \bar{v}}{\partial \xi}.$$

Equations (12)–(15), along with low Reynolds number and long wavelength assumptions, yield:

$$\frac{\partial p}{\partial x} = \frac{\partial}{\partial y} \left[ 1 + \left( \frac{n-1}{2} \right) W_2 \left( \frac{\partial^2 \psi}{\partial y^2} \right) \right] \frac{\partial^2 \psi}{\partial y^2} - \frac{M_f}{1 + m_c^2} \left( 1 + \frac{\partial \psi}{\partial y} \right),$$

$$\frac{\partial p}{\partial y} = 0,$$

$$\frac{\partial^2 \theta}{\partial y^2} + B_1 \left( \frac{\partial^2 \psi}{\partial y^2} \right) \left[ 1 + \left( \frac{n-1}{2} \right) W_2 \left( \frac{\partial^2 \psi}{\partial y^2} \right) \right] - \frac{M_f}{1 + m_c^2} \left( 1 + \frac{\partial \psi}{\partial y} \right)^2 = 0.$$
As \( p \neq p(y) \), therefore Equation (17) yields:

\[
1 + \frac{3(n-1)}{2} W_c^2 \left( \frac{\partial^2 \psi}{\partial y^2} \right)^2 \frac{\partial^4 \psi}{\partial y^4} + 3(n-1) W_c^2 \left( \frac{\partial^2 \psi}{\partial y^2} \right)^2 \left( \frac{\partial^3 \psi}{\partial y^3} \right)^2 - \frac{M_f}{1 + m_e} \left( 1 + \frac{\partial \psi}{\partial y} \right) = 0, \tag{20}
\]

In the above equations, \( B_r, W_c, M_f, m_e, \psi, \) and \( \theta \) are the notations for the Brinkman number, Weissenberg number, Hartman number, Hall parameter, stream function, and temperature, respectively. The associated non-dimensional boundary conditions are:

\[
\begin{align*}
\psi &= -\frac{e}{2}, \quad \frac{\partial \psi}{\partial y} = -1, \quad \frac{\partial \psi}{\partial y} + B_i (\theta - 1) = 0, \quad \text{at} \quad y = W_1, \\
\psi &= \frac{e}{2}, \quad \frac{\partial \psi}{\partial y} = -1, \quad \frac{\partial \psi}{\partial y} + B_i \theta = 0, \quad \text{at} \quad y = W_2, 
\end{align*}
\tag{21}
\]

where \( F = \int_{W_1}^{W_2} \frac{\partial \psi}{\partial y} dy \) is related to the fixed frame by \( F = Q - 1 - d \).

### 3. Analysis of Entropy Generation

Fluid irreversibilities in the current problem are due to heat diffusion, viscous dissipation, and the magnetic field, respectively. Based on these, the dimensional entropy generation is defined as:

\[
S_G = \frac{\kappa}{T} \left[ \frac{\partial T}{\partial X} \right]^2 + \left( \frac{\partial T}{\partial Y} \right)^2 + \frac{1}{T} \left[ \frac{\sigma B_0^2}{1 + m_e^2} (\nabla^2 + \nabla) \right] + \frac{1}{T} [ \tau \cdot (\nabla \nabla) ].
\tag{22}
\]

The characteristic entropy is defined as \( S_0 = \frac{d^2}{dX^2} \). The total entropy generation rate, denoted by \( N_{it} \), is the relation between the actual entropy to the characteristic entropy. In dimensional form, entropy generation via stream function presentation:

\[
N_{it} = \frac{S_G}{S_0},
\tag{23}
\]

\[
N_{it} = \frac{1}{(\theta + \xi)^2} \left( \frac{\partial \psi}{\partial y} \right)^2 + \frac{B_r}{(\theta + \xi)} \left( \frac{\partial^2 \psi}{\partial y^2} \right)^2 + \left( \frac{n-1}{2} \right) W_c^2 \left( \frac{\partial^2 \psi}{\partial y^3} \right)^2 + \frac{B_r}{(\theta + \xi)} \frac{M_f}{1 + m_e^2} \left( 1 + \frac{\partial \psi}{\partial y} \right)^2
\tag{24}
\]

Here, the temperature difference parameter is labelled by \( \xi = \frac{T_m - T_0}{T_m + T_0} \), and \( N_{it} = N_{it} + N_f + N_M \).

The Bejan number identified by \( B_r \) is the proportion of heat irreducibility to the total entropy generation. Basically, the \( B_r \) number comprehends the mechanism of the production of entropy.

\[
B_r = \frac{1}{(\theta + \xi)^2} \left( \frac{\partial \psi}{\partial y} \right)^2 + \frac{B_r}{(\theta + \xi)} \left( \frac{\partial^2 \psi}{\partial y^2} \right)^2 + \left( \frac{n-1}{2} \right) W_c^2 \left( \frac{\partial^2 \psi}{\partial y^3} \right)^2 + \frac{B_r}{(\theta + \xi)} \frac{M_f}{1 + m_e^2} \left( 1 + \frac{\partial \psi}{\partial y} \right)^2
\tag{25}
\]

\( B_r = \frac{1}{2} \) defines equal irreversibility, due to heat and other contributing factors. For dominating heat irreversibilities, \( B_r = 1 \), while \( B_r = 0 \) implies that the contributing factors of fluid friction and magnetic field are noteworthy. The Bejan number ranges between zero and one.

### 4. Solution Methodology

Our problem is non-linear and coupled in nature. The computation of the exact solution is not possible; therefore, perturbation techniques are employed to solve the resulting governing equations. We apply regular perturbation of the fluid parameter, the Weissenberg number \( W_c^2 \) as:
$$\psi = \psi_0 + W_e^2 \psi_1 + O(W_e^2)^2,$$
$$p = p_0 + W_e^2 p_1 + O(W_e^2)^2,$$
$$F = F_0 + W_e^2 F_1 + O(W_e^2)^2,$$
$$\theta = \theta_0 + W_e^2 \theta_1 + O(W_e^2)^2. \tag{26}$$

Substituting these into Equations (19) and (20), we construct the zeroth order and first order systems with reference to the fluid parameter.

### 4.1. Zeroth Order System and Boundary Conditions

$$- \frac{M_f}{1 + m_e^2} \left( \frac{\partial^2 \psi_0}{\partial y^2} \right) + \left( \frac{\partial^4 \psi_0}{\partial y^4} \right) = 0 \tag{27}$$

$$\frac{M_f}{1 + m_e^2} B_r + 2B_r \frac{M_f}{1 + m_e^2} \left( \frac{\partial \psi_0}{\partial y} \right) + B_r \frac{M_f}{1 + m_e^2} \left( \frac{\partial^2 \psi_0}{\partial y^2} \right) + \frac{\partial^2 \theta_0}{\partial y^2} + B_r \left( \frac{\partial^2 \theta_0}{\partial y^2} \right) = 0 \tag{28}$$

$$\psi_0 = \frac{F_0}{2}, \frac{\partial \psi_0}{\partial y} = -1, \frac{\partial \theta_0}{\partial y} + B_i \theta_0 = 0, \text{ at } y = W_1$$

$$\psi_0 = \frac{F_0}{2}, \frac{\partial \psi_0}{\partial y} = -1, \frac{\partial \theta_0}{\partial y} + B_2 \theta_0 = 0, \text{ at } y = W_2 \tag{29}$$

### 4.2. First-Order System and Boundary Conditions

$$- \frac{M_f}{1 + m_e^2} \left( \frac{\partial \psi_1}{\partial y} \right) + 3(n-1) \left( \frac{\partial^2 \psi_0}{\partial y^2} \right) \left( \frac{\partial^3 \psi_0}{\partial y^3} \right)^2 + \frac{3}{2} \left( n-1 \right) \left( \frac{\partial^2 \psi_0}{\partial y^2} \right) \left( \frac{\partial^4 \psi_0}{\partial y^4} \right) + \frac{\partial^4 \psi_1}{\partial y^4} = 0 \tag{30}$$

$$2B_r \frac{M_f}{1 + m_e^2} \left( \frac{\partial \psi_0}{\partial y} \right) + 2B_r \frac{M_f}{1 + m_e^2} \left( \frac{\partial \psi_1}{\partial y} \right) + \frac{\partial^2 \theta_0}{\partial y^2} + \frac{1}{2} \left( n-1 \right) B_r \left( \frac{\partial^2 \psi_0}{\partial y^2} \right)^4 \tag{31}$$

$$+ 2B_r \left( \frac{\partial^2 \psi_0}{\partial y^2} \right)^4 + 2B_r \left( \frac{\partial^2 \psi_0}{\partial y^2} \right)^4 = 0$$

$$\psi_1 = \frac{F_1}{2}, \frac{\partial \psi_1}{\partial y} = 0, \frac{\partial \theta_0}{\partial y} + B_i \theta_1 = 0, \text{ at } y = W_1$$

$$\psi_1 = \frac{F_1}{2}, \frac{\partial \psi_1}{\partial y} = 0, \frac{\partial \theta_0}{\partial y} + B_2 \theta_1 = 0, \text{ at } y = W_2 \tag{32}$$

### 5. Discussion and Results

The impact of different physical parameters, i.e., $B_r$, $W_e$, $M_f$, $m_e$, $B_i$, $B_2$, and $\phi$, on total entropy generation, entropy production due to the friction and heat diffusion, temperature, Bejan number, heat transfer rate, pressure gradient, stream lines, and velocity profile are discussed in this section.

#### 5.1. Analysis of Entropy Generation ($N_{ts}$) and Bejan Number ($B_e$)

The entropy generation $N_{ts}$ and Bejan number $B_e$ are plotted in Figures 2a–d and 3a–d to depict the effects of the Hartman number, Hall parameter, Brinkman number, and temperature difference parameter. Figure 2a,c portrays that $N_{ts}$ was gradually enhancing for increasing values of the Hartman and Bejan numbers. With the application of the magnetic field, the temperature increased. Joule heating produced more heat, so entropy production increased. At the lower wall, entropy generation was maximum as compared to the other wall (due to temperature gradient). It can also be noticed that at the lower wall, fluid friction irreducibility was dominant, whereas at the upper wall, heat transfer reduced the entropy generation. Figure 2b shows the effect of the Hall parameter $m_e$, which reduced the entropy generation. In Figure 2c, as we increased the Brinkman number (the conduction of energy that was produced by viscous dissipation), entropy generation increased. Figure 2d depicts that with an increment in temperature difference, the entropy generation gradually decreased. Figure 3a
indicates the Bejan number for the variation of the Hartman number. It reveals that heat irreversibility at the bulk fluid region was dominant, while at the edges, magnetic and viscous irreversibility were dominating. Figure 3b presents that Bejan number decreased with the Hall parameter \( m_e \) at \( y = 0 \). Figure 3c,d show that with the increase in the Brickman number and temperature difference parameter, the Bejan number decreased.

![Figure 2](image.png)

Figure 2. Entropy generation \( N_{ts} \) versus \( y \) for different values of \( M_f, m_e, B_r \) and \( \xi \) (a–d).

![Figure 3](image.png)

Figure 3. Bejan number \( B_e \) versus \( y \) for various \( M_f, m_e, B_r \) and \( \xi \) (a–d).
5.2. Analysis of Temperature

Figure 4a–f shows the behavior of temperature for different physical parameters, particularly the Hartman number \( (M_f) \), Hall parameter \( (m_e) \), Brinkman number \( (B_r) \), power law index \( (n) \), and Biot numbers \( (B_l_1, B_l_2) \). Figure 4a depicts that the temperature profile gradually rose for increasing values of the Hartman number \( M_f \). Basically, magnetic field lines interacted electrically with the fluid and produced Lorentz force. Lorentz force retarded the fluid motion (transforming the kinetic energy of the electrically conducting fluid to heat energy), and fluid temperature rose. It is found from Figure 4b that the temperature is lowered because of the increase in the electrical conductivity of the fluid. Figure 4c elucidates that under the influence of the Brinkman number, the temperature rose. The reason behind this is that for a large value of the Brinkman number, the frictional force increased (due to the collision of fluid molecules with each other), and as a result, kinetic energy converted into thermal energy, implying a rise in total fluid temperature. The influence of the Biot number on the temperature is presented in Figure 4d,e. Temperature decreased at the upper wall by the increase of \( B_l_1 \), and it had no visible effect on the lower wall. In contrast, the temperature escalated at the lower wall with the increase of \( B_l_2 \), and a negligible difference was observed on the upper wall. In most of the cases, for small Biot numbers, temperature uniformly distributed inside the fluid, whereas for Biot numbers greater than 0.1, irregularity resulted. Therefore, we took a special case for a large value of the Biot number. Figure 4f elucidates that temperature increased for increasing values of the power law index.

![Figure 4a](image1.png)  
![Figure 4b](image2.png)  
![Figure 4c](image3.png)  
![Figure 4d](image4.png)  
![Figure 4e](image5.png)  
![Figure 4f](image6.png)

Figure 4. Temperature \( \theta \) versus \( y \) for different values of \( M_f, m_e, B_r, B_l_1, B_l_2 \) and \( n \) (a–f).
5.3. Analysis of Velocity

Axial velocity serves to provide salient feature of flow behavior. Figure 5a–c portrays the impact velocity profile in a channel with convective boundaries. We observed that the velocity formed a parabolic trajectory for physical parameters, and maximum velocity occurred at \( y = 0 \). Figure 5a portrays that the axial velocity decreased for the increasing value of the Hartman number. Since the Hartman number directly relates the magnetic force and this force is resistive in nature, therefore the velocity decreased. Figure 5b demonstrates the influence of the Hall parameter \( m_e \). Here, the velocity accelerated at the center of the channel while it reduced at the edges, the reasons behind this being that \( m_e \) caused an upsurge of the electrical conductivity of the fluid; hence, the velocity increased. Figure 5c shows the comparison of viscous and Carreau fluids. It gained maximum velocity for a Newtonian fluid, while it reduced for the non-Newtonian Carreau fluid. Furthermore, it restored the symmetry about the center line.

5.4. Analysis of the Pressure Gradient and the Rate of Heat Transfer

The influence of \( M_f, m_e, W_c, \) and \( B_r \) is analyzed through Figures 6a–c and 7a–d to peruse the pressure gradient and rate of heat transfer. Figure 6a reveals that for the increasing value of the Hartman number, the pressure gradient decreased at the narrow part, whereas it increased at the wider region. Figure 6b depicts the influence of the Hall parameter. \( \frac{dp}{dx} \) decreased at the wider region, and a negligible difference was observed at the narrow part. Figure 6c portrays that with the increase of the Weissenberg number, the pressure gradient \( \frac{dp}{dx} \) increased at the narrow and wider region. Figure 7a,d presents that for higher values of the Biot number and Hall parameter, the heat transfer rate reduced; whereas the heat transfer rate increased for the Brinkman number and Hartman number (Figure 7b,c).
5.4. Analysis of the Pressure Gradient and the Rate of Heat Transfer

The influence of $M_f$, $m_e$, and $f$ is analyzed through Figure 6a–c and Figure 7a–d to peruse the pressure gradient and rate of heat transfer. Figure 6a reveals that for the increasing value of the Hartman number, the pressure gradient decreased at the narrow part, whereas it increased at the wider region. Figure 6b depicts the influence of the Hall parameter. $\frac{dp}{dx}$ decreased at the wider region, and a negligible difference was observed at the narrow part. Figure 6c portrays that with the increase of the Weissenberg number, the pressure gradient $\frac{dp}{dx}$ increased at the narrow and wider region. Figure 7a, d presents that for higher values of the Biot number and Hall parameter, the heat transfer rate reduced; whereas the heat transfer rate increased for the Brinkman number and Hartman number.

5.5. Trapping Phenomenon

Streams lines were plotted to depict the flow pattern. The trapping phenomenon for fluid parameters $M_f$ (Hartman number), $m_e$ (Hall parameter) and $W_e$ (Weissenberg number) was described through plotting the streams lines. Figures 8–10 show that the bolus size decreased for increasing values of the Hartman number and Weissenberg number. Figure 10a–c depict the opposite trend that is for higher values of hall parameter bolus size not only increases but number of closed stream lines also increases in count.

Figure 6. (a–c) Pressure gradient $\frac{dp}{dx}$ versus $x$ for different values of $M_f$, $m_e$, and $W_e$.

Figure 7. (a–d) Rate of heat transfer for different values of $M_f$, $m_e$, $B_r$ and $B_i_2$.
5.5. Trapping Phenomenon

Streams lines were plotted to depict the flow pattern. The trapping phenomenon for fluid parameters $M_f$ (Hartman number), $e_m$ (Hall parameter) and $e_w$ (Weissenberg number) was described through plotting the streamlines. Figures 8–10 show that the bolus size decreased for increasing values of the Hartman number and Weissenberg number. Figure 10a–c depict the opposite trend that is for higher values of hall parameter bolus size not only increases but number of closed stream lines also increases in count.

Figure 8. (a–c) Stream lines for different values of $M_f = 0.1$, $M_f = 2$, $M_f = 3$.

Figure 9. (a–d) Stream lines for different values of $m_e = 0.5$, $m_e = 1$, $m_e = 1.5$, $m_e = 2$. 

Figure 7. (a–d) Rate of heat transfer for different values of $M_e$, $m_e$, $B_f$, $B_i$. 

(a) (b) (c) (d)
5.6. Analysis of Entropy Generation due to Heat Diffusion and Viscous Dissipation

The thermal entropy generation rate and viscous entropy generation are very important in entropy generation. The influence of the Hartman number \( M_f \) and Weissenberg number \( W_e \) was studied to configure the entropy generation due to the heat diffusion and viscous dissipation effect. Figure 11a elucidates that for the increasing value of the Hartman number, the heat diffusion rate increased. This physically happens due to the strong magnetic field, which boosts the temperature. Therefore, the diffusion rate increased. Figure 11b illustrates that for higher values of \( W_e \), the heat diffusion rate decreased. Variation in the entropy generation rate due to viscous dissipation for different values of the Hartman number is observed through Figure 12a,b. The increase in the thermal entropy generation rate at the walls was observed due to resistive forces, while heat production dropped off due to low viscosity at the center of the channel.

Figure 10. (a–c) Stream lines for different values of \( W_e = 0, W_e = 0.9, W_e = 0.16 \).

Figure 11. (a,b) Entropy generation rate due to heat diffusion for different values of \( M_f \) and \( W_e \).
The number of closed circular stream lines encircling the bolus increases with an increase in the Hall parameter. The pressure gradient increases in a wider region for both the Hall parameter and the Hartman number. The velocity decreases due to the fluid’s Weissenberg number. Due to the resistive nature of the magnetic field, the velocity profile decreases for the Hartman number, while for temperature, it increases. The velocity decreases due to the fluid’s Weissenberg number. The pressure gradient increases in a wider region for both the Hall parameter and the Hartman number. The number of closed circular stream lines encircling the bolus increases with an increase in the values of the Hall parameter.

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