Progress in Electrolyte-Free Fuel Cells

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Solid oxide fuel cell (SOFC) represents a clean electrochemical energy conversion technology with characteristics of high conversion efficiency and low emissions. It is one of the most important new energy technologies in the future. However, the manufacture of SOFCs based on the structure of anode/electrolyte/cathode is complicated and time-consuming. Thus, the cost for the entire fabrication and technology is too high to be affordable, and challenges still hinder commercialization. Recently, a novel type of electrolyte-free fuel cell (EFFC) with single component was invented, which could be the potential candidate for the next generation of advanced fuel cells. This paper briefly introduces the EFFC, working principle, performance, and advantages with updated research progress. A number of key R&D issues about EFFCs have been addressed, and future opportunities and challenges are discussed.

Keywords: fuel cell, single component/layer fuel cell, electrolyte (layer)-free, research progress, solid oxide fuel cell

INTRODUCTION

Energy crisis and environmental pollution continue to challenge all countries around the world in terms of both the global economy and the planetary environment (Zhang and Cooke, 2010). Fossil energy, which can meet the demand of human energy consumption, will release SO2, NOx, CO, CO2, and other toxic substances. All these emissions will seriously harm the environment. Meanwhile, the utilized efficiency of fossil energy is not high enough, and the fossil resources themselves are limited and not renewable. However, fuel cells (FCs), as one of the most important energy technologies, can convert chemical energy from fossil fuels to electricity by electrochemical reaction. It increases efficiency up to 40–80%, which is very promising without being limited by the Carnot cycle (Dufour, 1998). The characteristics of cleanliness, quietness, and high efficiency, delivered by FCs, make it possible to be one of the most effective methods to resolve the environmental pollution from fossil fuel combustion. Among all types of FCs, SOFC, and proton exchange membrane fuel cells (PEMFC) are considered to be the most promising technologies in stationary and transportation applications (Yi, 1998).

Solid oxide fuel cell (SOFC) is a kind of FC that can operate at high temperatures between 500 and 1000°C. The advantages of SOFC include high efficiency, multi-fuel flexibility, environment-friendly, lower material cost, long service life, and so on. The core part is the three-layered structure of anode,
electrolyte [yttrium-stabilized zirconia (YSZ)], and cathode as shown in Figure 1A. Today, the YSZ electrolyte SOFCs still face commercialization challenges due to high costs. Removal of the electrolyte layer could provide a completely new technology that would be simple and most cost-effective. Recently, an electrolyte (layer)-free fuel cell (EFFC) was invented. It exhibits a new energy conversion technology (Zhu et al., 2011a,b). The novel structure of EFFC is shown in Figure 1B. Of primary importance is that EFFC maintains the core function of traditional SOFC to convert chemical energy from fuel to electricity. However, the single layer structure of EFFC is significantly different from the conventional three-layer structure.

**ELECTROLYTE (LAYER)-FREE FUEL CELL**

**The Working Principle of EFFC**

Traditional FC is constructed by three layers – a typical anode–electrolyte–cathode structure. The porous anode and cathode are separated by an electrolyte that is composed of dense solid oxide YSZ. The electrolyte is employed here to separate oxidant (oxygen) from reductant (fuel) and facilitate the transfer of ions (O\(^{2-}\)), as shown in Figure 2A. The electrolyte is the key component of this structure. Unlike the SOFC structure, there is no macroscopic electrolyte in EFFCs. The structure of EFFC is a homomorphous layer that is constituted by a mixture of semiconductor and oxygen ion conductor. Its working temperature ranges from 300 to 600°C. The different working principle of EFFC has been presented by Zhu et al. (2011c, 2012).

It can be seen from Figure 2B that the EFFC fuel is oxidized and electrons are released at the anode (fuel side). At the cathode (air side), oxygen (oxidant) is reduced to oxygen ions (O\(^{2-}\)), which combine with electrons from external circuit to generate electricity. Hydrogen is employed here to explain this electrochemical process of the EFFC.

In proton conduction case:

At the hydrogen-contacting side:

\[
H_2 \rightarrow 2H^+ + 2e^-
\]

![Figure 1](image1.png) Structures between (A) SOFC and (B) EFFC, or called single component.

![Figure 2](image2.png) Comparison of working principle between (A) SOFC and (B) EFFC, or called single component.
At the air (O\(_2\))-contacting side:

\[
\frac{1}{2}O_2 + 2H^+ + 2e^- \rightarrow H_2O
\]

In oxide-ion conducting case:

At the hydrogen-contacting side:

\[
H_2 + O^2- \rightarrow H_2O
\]

At the air (O\(_2\))-contacting side:

\[
\frac{1}{2}O_2 + 2e^- \rightarrow O^2-
\]

It is also common that the single layer may conduct both proton and oxide ions, in this case:

At the hydrogen-contacting side:

\[
H_2 \rightarrow 2H^+ + 2e^-
\]

At the air (O\(_2\))-contacting side:

\[
\frac{1}{2}O_2 + 2e^- \rightarrow O^2-
\]

To all the above cases, the overall electrochemical reaction in the EFFC is the same as the common FC process:

\[
H_2 + 1/2O_2 \rightarrow H_2O
\]

The electrochemical process of FC can be further construed as 
H\(^+\) transferring from anode to cathode or as O\(^-\) migrating from cathode to anode. Transportation of O\(^-\) in traditional SOFC occurs at the electrolyte between anode and cathode. More specifically, ionic conduction can be enhanced and conducted on the particles’ surface (Veldsink et al., 1995; Suzuki et al., 2005), which is used in the EFFC device with co-ionic H\(^+\)/O\(^-\) transport. This device is named as EFFC according to the new principle. The preparation technology of EFFC is very simple. Only one component is required, which can be fabricated by the mixture of electrode (anode and cathode) and electrolyte, the so-called “Three in one,” highlighted by Nature Nanotechnology (Zhu, 2011). Different from the traditional SOFC constructed by three-layer anode–electrolyte–cathode, this new device with single component/layer can effectively convert fuel to electricity.

**Advantages of EFFCs**

Electrolyte (layer)-free fuel cell is a new energy conversion device showing many advantages that cannot be obtained by traditional SOFC since their operation mechanisms are different (Zhu, 2011, Zhu et al., 2011d, 2013a; Fan et al., 2012, 2013). In brief, some special merits of EFFC can be summarized as follows:

(i) The manufacturing cost is significantly reduced due to its simple structure and preparation method.

(ii) The interfaces of the electrolyte/the anode and the electrolyte/the cathode contribute to major polarization losses in the traditional three-layer structure. In addition, the three-layer device requests strict thermal compatibility and chemical stability among the anode, electrolyte, and cathode, which have different material components. These present a serious SOFC technology challenge resulting in high cost as well. However, there is only one layer in the EFFC. Hence, losses or thermal stress problem from the interface can be avoided here. This ensures the long-term stability of the EFFCs.

(iii) Electrolyte (layer)-free fuel cells fabricated by multifunctional nanocomposite materials include oxygen ion conductor and semiconductor. Ionic conductivity of the cell materials is enhanced greatly for oxygen ion conducts on the surface of the cell and in itself, simultaneously. Meanwhile, there exists a synergistic effect established among the ions, electrons, holes between n-type or p-type semiconductor, and oxygen ion conductor. It helps to prevent short-circuit current and improve ionic conductivity of the single cell. This directly reduces the working temperature of the cell and provides a chance for introducing a wide range of materials.

**Technical Developments on EFFCs**

“Three in one” single layer materials are the key to realize the EFFCs with semiconductor-ion conductivities, which can integrate all anode, electrolyte, and cathode functions into one. In particular, a single layer is constituted by semiconductor materials (n-type or p-type) and oxygen ion conductor composite materials (Zhu et al., 2011e). At present, exploring new multi-functional nanocomposites are one of the main research activities of EFFCs.

**Materials for EFFCs**

At present, most of the EFFC materials are based on composite types consisting of two types of constituent materials, i.e., (1) oxide ion conductors, e.g., Sm\(_2\)O\(_3\)-doped CeO\(_2\) (SDC) or Gd\(_2\)O\(_3\)-doped CeO\(_2\) (GDC) and various ceria-based composites and (2) semiconducting materials, e.g., various transition element metal oxides, e.g., Ni, Cu, Fe, Zn, etc., and their complex or composite types. Recent research shows that the electrochemical performance strongly depends on the properties of the constituent materials, stoichiometric proportions, compositions between the constituent ion and semiconductor, their morphology and microstructure as well as experimental conditions.

**Oxide Ion Conductors**

Sm\(_{2}\)O\(_3\)-Doped CeO\(_2\). At present, chemical co-precipitating method and sol–gel method are mainly carried out in the preparation of SDC. The SDC powder materials within nanoscale were synthesized by one step co-precipitation method (Zhu et al., 2011b). The raw materials of Ce(NO\(_3\))\(_3\)-6H\(_2\)O and Sm(NO\(_3\))\(_3\)-6H\(_2\)O were used (Xia et al., 2012) to prepare the SDC powder materials. In sol–gel process, both ceria and samarium nitrate hydrates formed a mixture solution of Ce(NO\(_3\))\(_3\)-6H\(_2\)O and Sm\(_2\)O\(_3\), the solid citric acid was added into with vigorous stirring at 60–70°C until turning to the gel. The gel was sintered at 800°C to obtain the SDC powder materials by grinding.

Gd\(_{2}\)O\(_3\)-Doped CeO\(_2\). Apart from SDC, GDC is another material for EFFC. The GDC powder materials were obtained by using carbonate co-precipitation method (Zhu et al., 2011a). Ce(NO\(_3\))\(_3\)-6H\(_2\)O and Gd(NO\(_3\))\(_3\)-6H\(_2\)O (Ce\(^{3+}\)/Gd\(^{3+}\) = 9:1) were
first dissolved in deionized water to form a mixed solution. Then, Na₂CO₃ was added into this solution by vigorous stirring to form white precipitate at 120°C. The precipitating precursor was further subjected to washing and drying. The GDC powder materials can be obtained after sintering it at 800°C.

**Modified and Doped Nanomaterials Based on SDC and GDC.** Hu et al. (2014) had prepared MgZn–SDC materials by chemical co-precipitation method. Mg(NO₃)₂·6H₂O and Zn(NO₃)₂·6H₂O were used in the co-precipitation process for nanometer material preparation. The cost of this material has been further reduced by introducing Mg and Zn contents. Zhu et al. (2014) had prepared GDC–KAlZn (KAZ) materials by two-step co-precipitation method. They first dissolved Ce(NO₃)₂·6H₂O and Gd(NO₃)₃·6H₂O(Ce⁴⁺:Gd⁴⁺ = 4:1) in deionized water to get the properly distributed mixture in solution. A 0.5M Na₂CO₃ solution was gradually added into the mixed solution while it was stirring at 120°C. The white precipitate was formed. Following filtering, washing, and drying processes, a GDC precursor was obtained. In parallel, KAZ composite was also prepared by co-precipitation method. Al(NO₃)₃·9H₂O and Zn(NO₃)₂·6H₂O (Al³⁺:Zn²⁺ = 4:3) were dissolved in deionized water, and K₂CO₃ was selected as a precipitant agent to form the co-precipitation. The GDC precursor was added and then dried at 150°C. The GDC–KAZ (KAZ) precursor was thus obtained. After washing, filtrating, drying, and then sintering at 800°C for 4 h, the GDC–KAZ (KAZ) nanocomposite materials were obtained.

**Semiconducting Materials** Up to now, semiconductor materials (n-type or p-type) for EFFCs are selected among those transition metal oxides, e.g., NiO, CuO, FeOₓ, ZnO, and CoOₓ-doped LiNiO₂ (n-type or p-type) for EFFCs are selected among those transition metal oxides, e.g., NiO, CuO, FeOₓ, ZnO, and CoOₓ-doped LiNiO₂ (n-type or p-type). The maximum power output of EFFCs could reach 700 mW/cm² at 550°C (Zhu et al., 2011c). The total conductivity of LiNiZnOₓ–SDC mixed materials of ion conductor and semiconductor is up to 0.1–1 S/cm.

The ceria–carbonate materials were also used to get semiconductor single layer materials. The maximum power output of EFFCs could reach 700 mW/cm² at 550°C (Zhu et al., 2011e) by mixing LiNiCuZnFe–oxide and Na₂CO₃–SDC (NSDC) composite. The maximum power output of EFFC obtained by mixing LiNiCuSr–oxide and MgZnDC, according to a certain mass ratio, can reach 600 mW/cm² at 550°C. Its open circuit voltage (OCV) is up to 1.02 V at the same temperature (Hu et al., 2014). Xia et al. (2011) has developed Sr₂Fe₁.₅Mo₀.₅O₆–SDC (SFM) and NSDC in a certain mass ratio as the single layer material for the EFFC. They reported that to achieve the best device performance the electronic and ionic conductivities must be closely matched, so 30% mass of SFM was able to achieve the best performance of the maximum power output of 360 mW/cm² at 750°C. This result is in agreement to the earlier studies as reported by Xia et al. for the SDC–LiNiZn–oxide single layer conductivities by adjusting the manipulation of concentration rations of ionic SDC to electronic conductors LiNiZn–oxide. They found that the single layer containing 30% mass of LiNiZn–oxide exhibits an almost uniform distribution of the two constituent components to establish a balance between the ionic and electronic conductors (Xia et al., 2012). Hei et al. (2014) investigated a composite of a perovskite oxide proton conductor (BaCe₀.₇Zr₀.₁Y₀.₂O₃−δ and BCZ10Y20) and alkali carbonates (2Li₂CO₃:1Na₂CO₃ and LNC). The cell shows a maximum power density of 957 mW/cm² at 600°C with hydrogen as the fuel and oxygen as the oxidant. The summary of the typical performance demonstrated by various EFFCs are presented in Table 1.

**Table 1 | Overview of EFFC performances.**

| No. | Performance | Temperature (°C) | Article | Key materials | Journal | Year |
|-----|-------------|------------------|---------|--------------|---------|------|
| 1   | 360 mW/cm² (maximum power output) | 750 | Single layer fuel cell based on a composite of Ce₀.₇Sm₀.₃O₂₋δ–Na₂CO₃ and a mixed ionic and electronic conductor SrFe₁.₅Mo₀.₅O₆−δ | SrFe₁.₅Mo₀.₅O₆−δ (SFM) and NSDC | Journal of Power Sources | 2014 |
| 2   | 600 mW/cm² (maximum power output) | 550 | Fabrication of electrolyte-free fuel cell with Mg₀.₅Zn₀.₅O⁻δ Ce₀.₇Sm₀.₃O₂₋δ–Li₀.₁5Ni₀.₄5Zn₀.₄ layer | LiNiCuSr–oxide and MgZnDC | Journal of Power Sources | 2014 |
| 3   | 10 × 10⁻² S/cm (total conductivity) | 600 | Electrical conductivity optimization in electrolyte-free fuel cells by single component Ce₀.₇Sm₀.₃O₂₋δ–Li₀.₁5Ni₀.₄5Zn₀.₄ layer | SDC–LNZ oxides | RSC Advances | 2012 |
| 4   | 450 mW/cm² (maximum power output) | 550 | A fuel cell with a single component functioning simultaneously as the electrodes and electrolyte | LiNiZn–oxide mixed with GDC | Electrochemistry Communications | 2011 |
| 5   | 700 mW/cm² (maximum power output) | 550 | A single component fuel cell reactor | Doped the oxidation-reduction catalyst Fe | International Journal of Hydrogen Energy | 2011 |
| 6   | 600 mW/cm² (maximum power output) | 550 | An electrolyte-free fuel cell constructed from one homogenous layer with mixed conductivity | LiNiZnOₓ–SDC | Advanced Functional Materials | 2011 |
| 7   | 700 mW/cm² (maximum power output) | 550 | Single component and three-component fuel cells | LiNiZnFe–oxide and Na₂CO₃–SDC (NSDC) | Journal of Power Sources | 2011 |
CRITICAL ISSUES ON EFFC

The first critical issue is to address whether penetration of the fuel (H₂) and oxidant (air) through the single layer material causes any electrochemical leakage due to H₂/O₂ thermal combustion. In this case, first, the security of the EFFC is of concern; the second is the electronic short-circuiting problem, by using the homogenously mixed semiconductor-ionic single layer material instead of the purely ionic-conducting electrolyte layer between the anode and cathode.

Non-Potential Safety Hazard

A separate layer of dense electrolyte is crucial for traditional FC. However, the dense electrolyte is not a must as long as it is gas tight, which can prevent gas penetration through it. Here, a major question is concerned: can oxygen and hydrogen pass through the porous single layer device and react directly to cause electrochemical leakage and potentially an explosion? The feasibility of eliminating the potential of explosion is a must for EFFC commercialization. Security level is determined by operating conditions, porosity, catalytic activity, and other features of EFFC. Liu et al. (2012) developed a dynamic model of anode and cathode reactions based on electrochemical impedance spectroscopy (EIS) to assess the performance of EFFCs. The security issue had been analyzed by using the single layer EFFCs by supplying the oxidant and fuel under the situation of open circuit conditions and operating conditions, respectively. The experimental and theoretical results show that the safety of EFFC is guaranteed. Assuming that porosity is equal to 0.5, define the torsion resistance τ is ϵ/τ = ϵ 1.5, under a standard atmospheric pressure. The reaction depth of anode is 5.3–1.0 × 10⁻⁵ m and cathode is 1.4–0.25 × 10⁻⁶ m when the current is changed from 100 to 2000 mA · cm⁻², as shown in Figure 3.

The effect of porosity on the reaction depth is given in Figure 4. The reaction depth of O₂ is in the range of 0.6–1.4 × 10⁻⁶ m with the porosity of 0.2–0.5. For H₂, it is in the range of 2.1–5.3 × 10⁻⁵ m. It is shown that the reaction depth, both of H₂ and O₂, increase with porosity. However, all of them are far below the thickness of EFFC, which is in the microscale/10⁻³ m level. It is decisively proven that there is no risk of explosion under the given operating conditions.

Therefore, the EFFC security level is very high according to the calculations. In addition, there is a quenching distance so that the explosion cannot occur if the distance between the oxygen and hydrogen molecule is smaller than a certain separation distance. According to Janicke et al. (2000), this quenching distance is...
1 mm. However, EFFC is a device constructed in basis of nanostructure. Its pore diameter is up to dozens of nanometer. The maximum micro-distance between the oxygen and hydrogen is far less than the quenching distance in a millimeter level. Hence, it is impossible to explode, even though they have met inside the EFFC device.

Short-circuit Issue and Rectification Effect
Electrolyte (layer)-free fuel cell worked as electron-blocking layer. Does electron produced from fuel side pass through the EFFC single layer device and arrive to the air side? Hence, is there a short-circuit or electrochemical leakage current? As reported in literature, OCVs of the EFFC are higher than that using the pure ionic ceria, e.g., SDC electrolyte FC. These results do not support the existence of the short-circuit current.

The rectification effect for the junction was observed for the EFFC device, which is clearly seen in the measured I–V curve when applying a bias voltage within –5 to +5 V range, as shown in Figure 5. All measurements were taken under the device OCV (open circuit condition) by supplying H2/air. The rectification effect is decreased with increasing the ionic component of NSDC. These results provide evidence that the SJFC single layer device shows the junction barrier in the presence of the constituent semiconducting material phase in the single layer device.

The single layer is constituted by semiconductor-ionic material acting as an electron-blocking layer. Actually, under the FC conditions, supplying the H2 and air, respectively, from both sides of the single layer device, there will form an n-type conducting zone in H2-contacting side, and p-type conducting zone in the air side because the semiconducting transition metal oxides possess amphoteric properties, i.e., the transition metal oxide can behave with n-type conductivity in reducing atmosphere and as p-type conductor in oxidant environment due to their defect properties (Singh et al., 2013). In this situation, a spatial n–p junction could be established, after the fuel and oxidant were supplied over the single layer device. Hydrogen is decomposed into protons and electrons on the surface of n-type semiconductor when inserting the H2 and O2 into the device. Meanwhile, oxygen receives electrons and forms oxygen ion at the surface of p-type semiconductor. More removable negative and positive charges are generated in areas of n-type and p-type semiconductor nanoparticles, respectively. A dynamic space-charge region may be re-formed between them and then internal electric field is generated similar to the traditional p–n junction. The space-charge region has two functions. The first is maintaining the electro dynamic potential of EFFC to ensure the output of electricity. The second is generating p–n junction, which can prevent electron produced at fuel side migrating to air side. It can also prevent the short-circuit current. Thus, the scientific principle is similar to solar cell.

There is still something unique for this single layer FC when compared with solar cell. Also, p–n junction is dynamic in EFFC, but static in solar cell. Spatial distribution of p–n junction is dependent on the composition of the atmosphere. We will give a more complete description about EFFC, including synergy problems of electron, ion, hole and proton, and the dynamic distribution of p–n junction, by updating the latest development in these regards.

Latest Progress on Scientific Studies of EFFCs
The invention of EFFC initiated a new scientific research frontier. However, the understanding of the electrochemistry in the existing FCs is not explicit, e.g., a key issue is how to prevent the electron passing through the device without using the electrolyte separator. The second issue is how to avoid short-circuit and electrochemical leakage when the mixing semiconductor and ionic-conducting layer are both introduced into the single layer. It is known that the mixed ionic and electronic conductors (MIECs) developed for SOFCs cannot replace the electrolyte. Otherwise, the short-circuiting problem will cause serious device OCV and power output losses (Eguchi et al., 1992; Riess et al., 1996; Shen et al., 2014). The true situation in the EFFCs is very different from the MIEC behavior, because the EFFC does not show OCV loss in a proper composition range of doped ceria ionic materials and semiconductor compared to the pure ionic-doped ceria electrolyte device, which usually exhibits rather lower OCV of 0.85–0.9 V due to the ceria-based electrolyte reduced electronic conduction. It was overcome in EFFCs using the doped ceria mixed with semiconductor materials. In our latest development, we have used the Sm-Ca co-doped ceria (SCDC), which has a high O2− conductivity of 0.12 S/cm at 700°C (Banerjee et al., 2007) and perovskite La0.8Sr0.2Co0.2Fe0.8O3−δ (LSCF), a p-type semiconductor that is one of the most promising SOFC cathodes due to its decent electrocatalytic properties for redox reactions (Esquivrol et al., 2004), high electrical (p-type) conductivity, e.g., 230 S/cm at 900°C (Jiang, 2002) as well as good oxygen ion conductivity (0.1 S/cm at 800°C) (Kostogloudis and Pitskos, 1999).

Figure 6 shows typical I–V and I–P characteristics for this device compared to the pure ionic-doped ceria electrolyte device, which was fabricated using conventional FC anode/electrolyte/...
cathode configuration. It can be seen from Figure 6 that the OCV increased from pure ionic conductor SCDC electrolyte device 0.85 V up to 1.1 V at 45% LSCF:55% SCDC. Increasing the weight ratio of LSCF does not cause the OCV and power loss but increased significantly from pure SCDC at 300 mW/cm² up to 496 mW/cm² at 40% LSCF:55% SCDC. Though the OCV is somewhat lower than 0.94 V, it is still higher than that of the SCDC fuel cell 0.85 V, and the power output of the device with 55% LSCF: 45% SCDC raises to 798 mW/cm², see Figure 6. These facts, excluding the SCDC case, are in strong disagreement to the MIEC, which would have acted as a membrane instead of the electrolyte, and would cause significant losses in both voltage and power of the assembled device (Eguchi et al., 1992; Riess et al., 1996; Shen et al., 2014). This has been also proved by using the SCDC electrolyte due to its MIEC behavior in FC environment. But in the LSCF–SCDC membrane, we can see clearly that the incorporation of electronic (hole) conduction into the SCDC to form the semiconductor-ion membrane resulted in much better performance. It indicates a completely new phenomenon because of the unique LSCF–SCDC materials, which may be defined as a new type of functional semiconductor-ionic material. To the best of our knowledge, the semiconductor-ionic material has not been reported in literature so far.

Understanding the scientific principle, the underlying processes have been recently investigated. The device is activated by fuel. Charge carrier ($e^-$) is activated by fuel. When a proton (H$^+$) is formed, an electron is produced at the same time. Negative and positive charges are generated on the surface of air side and fuel side, respectively. The junction between them becomes depleted of charges/carriers, i.e., non-conduction. Consequently, a cell potential is generated, and electric energy can be taken out the device. The device functions based on nano-redox processes, as described by the formation of bulk heterojunction structures (BHJ). The energy band difference between the n and p semiconductors allows the charge separation at particles to prevent the electron crossing over internally to avoid the short-circuit problem (Figure 7) (Zhu et al., 2013b).

Also, Schottky junction has been discovered for the EFFC device. A potential or barrier can be built up at the interface between a metal and an n- or p-type semiconductor, known as the Schottky junction device (Mönch, 1994). Such device is preferably built only on p-type of semiconductor. In this case, it is a compatible anode metal, e.g., Ni or its alloy reduced from FC operation at H₂ side, on the semiconductor surface, typically, p-type semiconducting oxide, e.g., LiNiO-based oxide, as reported (Zhu et al., 2015) in a Schottky type contact/junction. Such junction can directly prevent the electrons crossing over the junction to avoid the short-circuiting problem due to its built-in
field or Schottky junction barrier. The working principle for such type EFFC device is presented in Figure 8.

The bilayer EFFC device was discovered before Zhu et al. (2011e). At that time, no knowledge about the semiconductor junction was possessed, though it was constructed by using LiNiCuZn (Fe)-oxide material mixed with the electrolyte, Sm0.2 Ce0.8 O2 (SDC), and perovskite cathode Ba0.6 Sr0.4 Co0.85 Fe0.15 O (BSCF) (p-type) mixed with SDC were employed without using the electrolyte layer. More than 500 mW/cm2 power output was achieved at 550°C, which is comparable with the performance achieved for conventional anode LiNiCuZn (Fe)/electrolyte, Sm0.2 Ce0.8 O2.6 (SDC), and perovskite cathode Ba0.6 Sr0.4 Co0.85 Fe0.15 O (BSCF) (p-type) mixed with SDC employed in the conventional FC. On the other hand, NCAL can be reduced at the anode zone. Differing from the conventional FCs, the working principle here is unique in combining semiconductor physics and electrochemistry.

**OPPORTUNITIES AND CHALLENGES FOR EFFC**

Reviewing the history of the FC for over 170 years, basic technology and breakthrough are not enough to conquer the technical challenges, hence delaying the commercialization. Eventual barrier is caused or limited by the materials and the three-layer device structure. The appearance of EFFC could be not only a breakthrough but also a revolution in the FC sector. First, we overcome the inherent model that ionic conduction only happens in the electrolyte. The nanocomposite porous super ionic conduction material is built where ions can conduct both in the internal and on the surface to make it fast in transport and charge transfer to realize effectively the redox reaction for power generation. Second, the latest EFFC developments have realized much better power output that that from traditional structure SOFCs. Electrolyte (layer)-free fuel cell was invented in 2010 and provides a new direction for FCs and SOFCs with new commercialization opportunity. It was selected as research highlight on Nature Nanotechnology in 2011 and named as “three in one” (Zhu, 2011). Introducing FC with high efficiency, zero/low emission and low noise into applications early and in large scale is of great importance. It is not only the demand of energy crisis but also for addressing environmental and low carbon emission issues. New science and energy technologies are urgently needed. EFFC semiconductor-ionic materials that can integrate FC all anode, electrolyte, and cathode functions have been invented and developed successfully. It has great potential in the competition of market issues. It is estimated that a cost of 100$/kW is feasible. The EFFC science and technology are expected to have wide application, e.g., other fuel cell technologies, not only for SOFCs,
but also for other electrochemical devices, Fe–air, Al–air, Li–air batteries etc., super-capacitor, electrolysis, photoelectrochemical devices etc. It will exert great influence on the science, technology, and economy.

CONCLUSION

Electrolyte (layer)-free fuel cell is a new energy device and the overall function of generating electricity is done in an analogous way to a FC. It can bring high power efficiency as theoretical calculation and further expectation. On the other hand, it may also function for the electrolysis with high performance to electrolyze water. EFFC can remove the bottleneck from electrolyte, which used to be a barrier for commercialization.

This design of new device aims to conquer the conventional FC drawbacks, such as high cost, complex construction, and so on. The EFFC may rapidly drive FC industrialization and commercialization. The市场化 of EFFCs largely depends on not only the materials but also the improvement of technology and the performance of the devices. There still remains a lot of future work that needs to be carried out. Initiating from the long-term development demanding of science and technology, research activities about EFFC is expanding.

AUTHOR CONTRIBUTIONS

YL’s contribution of this work was to find and read the related literature and write the manuscript. Main idea of this work is from Dr. BZ, who also guided all the writing process. YC, J-SK, and BW’s contribution to this work were to modify the details. JW and YZ mainly focused on investigating the manuscript. JIL’s work about this review was to draw the pictures.

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REFERENCES

Banerjee, S., Devi, P. S., Topwal, D., Mandal, S., and Moneni, K. (2007). Enhanced ionic conductivity in Ce0.5Sr0.5O2: unique effect of calcium co-doping. Adv. Funct. Mater. 17, 2847–2854. doi:10.1002/adfm.200600890
Constantinescu, C., Goldenblum, A., and Sostarich, M. (1973). Photovoltaic effects in laterally illuminated p n junctions. Int. J. Electron. 35, 65–72. doi:10.1080/00207217308938517
Dufour, A. U. (1998). Fuel cells: a new contributor to stationary power. J. Power Sources 71, 19–25. doi:10.1016/S0378-7753(97)02732-8
Eguchi, K., Setoguchi, T., Inoue, T., and Arai, H. (1992). Electrical properties of ceria-based oxides and their application to solid oxide fuel cells. Solid State Ionics 52, 165. doi:10.1016/0167-2779(92)90102-U
Esquivol, A., Brandon, N. P., Kilner, J. A., and Mogensen, M. (2004). Electrochemical characterization of La0.8Sr0.2FeO3−δ cathodes for intermediate-temperature SOFCs. J. Electrochem. Soc. 151, A1847–A1855. doi:10.1149/1.1799391
Fan, L. D., Wang, C. Y., Chen, M. M., and Zhu, B. (2013). Recent development of electrolyte-free fuel cells. J. Power Sources 234, 154–174. doi:10.1016/j.jpowsour.2013.01.138
Fan, L. D., Wang, C. Y., Osmadiziamen, O., Raza, R., Singh, M., and Zhu, B. (2012). Mixed ion and electron conductive composites for single component fuel cells: I. Effects of composition and pellet thickness. J. Power Sources 217, 164–169. doi:10.1016/j.jpowsour.2012.05.045
Hei, Y. F., Huang, J. B., Wang, C., and Mao, Z. Q. (2014). Novel doped barium cerate-carbonate composite electrolyte material for low temperature solid oxide fuel cells. Int. J. Hydrogen Energy 39, 14328–14333. doi:10.1016/j.ijhydene.2014.04.031
Hu, H. Q., Lin, Q. Z., Zhu, Z. G., Zhu, B., and Liu, X. R. (2014). Fabrication of electrolyte-free fuel cell with Mg0.5Zn0.5O/Ce0.8Sr0.2O1.9/δ-Li2O/Ce0.8Sm0.2O1.9–δ-O2 layer. J. Power Sources 248, 577–3581. doi:10.1016/j.jpowsour.2013.09.095
Janicke, M. T., Kestenbaum, H., Hagedorn, U., Schuh, F., Fichtner, M., and Schubert, K. (2000). The controlled oxidation of hydrogen from an explosive mixture of gases using a microstructured reactor/heats exchanger and Pt/Al2O3 catalyst. J. Catal. 194, 282–293. doi:10.1006/jcat.2000.2819
Jiang, S. P. (2002). A comparison of O2 reduction reactions on porous (La0.8Sr0.2)MnO3 and (La0.8Sr0.2)FeO3-δ electrodes. Solid State Ionics 146, 1–22. doi:10.1016/S0167-2738(01)00997-3
Kostogladous, G. C., and Filikos, C. (1999). Properties of A-site-deficient La0.8Sr0.2CoO3-δ based perovskite oxides. Solid State Ionics 126, 143–151. doi:10.1016/S0167-2738(99)00230-1
Liu, Q. H., Qin, H. Y., Raza, R., Fan, L. D., Li, Y. D., and Zhu, B. (2012). Advanced electrolyte-free fuel cells based on functional nanocomposites of a single porous component: analysis, modeling and validation. RSC Adv. 2, 8036–8040. doi:10.1039/c2ra20694c
Mönch, W. (1994). Metal-semiconductor contacts: electronic properties. Surf. Sci. 309–310, 928–944. doi:10.1016/0039-6028(94)90707-2
Riss, I., Gödelkeimer, M., and Gauckler, L. J. (1996). Characterization of solid oxide fuel cells based on solid electrolytes or mixed ionic electronic conductors. Solid State Ionics 90, 91–104. doi:10.1016/S0167-2738(96)00355-4
Shen, S. L., Yang, Y. P., Guo, L. J., and Liu, H. T. (2014). A polarization model for a solid oxide fuel cell with a mixed ionic and electronic conductor as electrolyte. J. Power Sources 256, 43–51. doi:10.1016/j.jpowsour.2014.01.041
Singh, K., Nowotny, J., and Thangadurai, V. (2013). Amphoteric oxide semiconductors for energy conversion devices: a tutorial review. Chem. Soc. Rev. 42, 1961. doi:10.1039/c2cs25339b
Suzuki, T., Jasiniski, P., Petrovsky, V., Anderson, H. U., and Dogan, F. (2005). Impact of anode microstructure on solid oxide fuel cells. J. Electrochem. Soc. 152, A527–A531. doi:10.1149/1.1858811
Veldsink, J. W., van Damme, R. M. J., Versteeg, G. E., and van Swaaij, W. P. M. (1995). The use of the dusty-gas model for the description of mass transport with chemical reaction in porous media. Chem. Eng. J. 57, 115–125. doi:10.1016/0923-447X(94)02929-6
Xia, D., Li, T., Jiang, L., Zhao, Y. C., Tian, Y., and Li, Y. D. (2011). Single layer fuel cell based on a composite of Ce0.8Sr0.2O1.9–δ-Na2CO3 and amixed ionic and electronic conductor Sr2Fe1.5Mo0.5O6–δ. J. Power Sources 256, 43–51. doi:10.1016/j.jpowsour.2014.01.041
Xia, Y. J., Liu, X. J., Bai, Y. J., Li, H. P., Deng, X. L., Niu, X. D., et al. (2012). Electrical conductivity optimization in electrolyte-free fuel cells by single-component Ce0.8Sr0.2O1.9–δ-Li2O/Na2CO3 layer. RSC Adv. 2, 3828–3834. doi:10.1039/c2ra201213h
Yi, B. L. (1998). Status and future of fuel cell. Chin. J. Power Sources 22, 2–6.
Zhang, F. Z., and Cooke, P. (2010). Hydrogen and fuel cell development in China: a review. Eur. Plan. Stud. 18, 1153–1165. doi:10.1080/09658374.2010.518716
Zhu, B. (2011). Nature nanotechnology research highlights. Three in one. Nat. Nanotechnol. 6, 330–330.
Zhu, B., Fan, L. D., and Lund, P. (2013a). Breakthrough fuel cell technology using ceria-based multi-functional nanocomposites. Appl. Energy 106, 163–175. doi:10.1016/j.apenergy.2013.01.014
Zhu, B., Lund, P., Raza, R., Patankas, J., Huang, Q. A., Fan, L. D., et al. (2013b). A new energy conversion technology based on nano-redox and nano-device processes. Nano Energy 2, 1179–1185. doi:10.1016/j.nanoen.2013.05.001
Zhu, B., Fan, L. D., Zhao, Y. F., Tan, W. Y., Xiong, D. B., and Wang, H. (2014). Functional semiconductor – ionic composite GDC-KZnAl/LiNiCuZnOx for single-component fuel cell. *RSC Adv.* 4, 9920–9925. doi:10.1039/c3ra47783e

Zhu, B., Lund, P., Raza, R., Ma, Y., Fan, L. D., Afzal, M., et al. (2015). Schottky junction effect on high performance fuel cells based on nanocomposite materials. *Adv. Energy Mater.* 5, 1401895. doi:10.1002/aenm.201401895

Zhu, B., Ma, L., Wang, X. D., Raza, R., Qin, H. Y., and Fan, L. D. (2011a). A fuel cell with a single component functioning simultaneously as the electrodes and electrolyte. *Electrochem. Commun.* 13, 225–227. doi:10.1016/j.elecom.2010.12.019

Zhu, B., Qin, H. Y., Raza, R., Liu, Q. H., Fan, L. D., Patakangas, J., et al. (2011b). A single-component fuel cell reactor. *Int. J. Hydrogen Energy* 36, 8536–8541. doi:10.1016/j.ijhydene.2011.04.082

Zhu, B., Raza, R., Abbax, G., and Singh, M. (2011c). An electrolyte-free fuel cell constructed from one homogenous layer with mixed conductivity. *Adv. Funct. Mater.* 21, 2465–2469. doi:10.1002/adfm.201002471

Zhu, B., Raza, R., Qin, H. Y., and Fan, L. D. (2011d). Fuel cells based on electrolyte and non-electrolyte separators. *Energy Environ. Sci.* 4, 2986–2992. doi:10.1039/c1ee01202a

Zhu, B., Raza, R., Qin, H. Y., and Fan, L. D. (2011e). Single-component and three-component fuel cells. *J. Power Sources* 196, 6362–6365. doi:10.1016/j.jpowsour.2011.03.078

Zhu, B., Raza, R., Liu, Q. H., Qin, H. Y., Zhu, Z. G., Fan, L. D., et al. (2012). A new energy conversion technology joining electrochemical and physical principles. *RSC Adv.* 2, 5066–5070. doi:10.1039/c2ra01234k

**Conflict of Interest Statement:** The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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