Near-field corrosion interactions between glass and corrosion resistant alloys

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This study explores the corrosion interactions between model nuclear waste glass materials and corrosion resistant alloys, under accelerated conditions that simulate the near field of a nuclear waste repository. The interactions between the corrosion of stainless steel (SS) 316, alloy G30, or alloy 625, and international simple glass or soda-lime silica glass are systematically studied. The dissimilar materials were exposed in close proximity to each other in different electrolytes at 90 °C. After exposure, the glass surface exposed near metals showed different regimes of corrosion, with distinct surface morphologies and chemistries that were likely affected by the local environment created by the localized corrosion of metals. Surface and solution analyses showed that the corrosion rate of glass was enhanced by the presence of metals. Infrared spectroscopy data suggested the local build-up of stresses in the contact area of glass, which may lead to the mechanical instability of the glass alteration layer. On the other hand, the effect of glass on metal corrosion is strongly dependent on the leaching solution. In electrolytes containing abundant aggressive anions such as Cl−, glass seems to suppress the localized corrosion of SS by the precipitation of a Si-rich surface film that protects the SS substrate from solutions. However, in less aggressive electrolytes, the corrosion rate of SS was increased by the presence of glass corrosion products. Overall, our study showed that the hidden and localized damage on glass in contact with metals may enhance the release rate of glass components compared to typical uniform glass corrosion.

INTRODUCTION

The high-level nuclear waste (HLW) existing as the legacy of defense applications and other by-products of spent nuclear fuel reprocessing will be melted into borosilicate glass, and then cast into stainless steel (SS) canisters. These canisters will be enclosed within waste packages and then emplaced in a mined underground geologic repository, which is the approach planned by most countries with such waste. In the U.S. program, the current waste package design includes glass being cast into SS 304 canisters then encased in a SS 316 inner shell and an Alloy 22 outer shell. The repository system is designed to isolate the radioactive waste from humans for hundreds of thousands of years. However, after an extremely long time of exposure, underground water might eventually break down the metallic structures by localized corrosion. Alloy 22 is an extremely corrosion resistant metal alloy, so any environment that could corrode Alloy 22 would also easily penetrate the SS structures within the canister and allow the corrosive environments to attack the encapsulated glass waste forms, leading to the release of radionuclides. Crevice corrosion may also be triggered once aqueous environment exists at the interface between the SS canister and the nuclear waste glass, which may create a series of issues.

The effect of Fe and Fe oxide/oxyhydroxide on the corrosion of nuclear waste glass has been investigated by several studies. The first work was published by McVay et al., who altered PNL 76–68 borosilicate glass and carbon steel together at 90 °C in various aerated solutions, including deionized water, tuff ground-water, and basalt groundwater. They reported that the corrosion rates of glass and steel were both enhanced due to the synergistic reactions of the two materials. The authors attributed the enhanced corrosion rate to the formation of Fe-silicate precipitates, which suppressed the saturation of leaching solution and caused a delay in the onset of the residual rate regime. Burger et al. altered SON68 glass in the presence of pure iron powder in an anoxic clayey environment at 50 °C for 2 years. They found that metallic Fe powders only influenced the immediate vicinity of the Fe and glass interface, where Fe-silicates were observed. Nanosized Fe-silicates precipitates were also found within the pores of the gel. It is believed that iron corrosion products, primarily Fe2O3, Fe3O4, and FeOOH will also affect glass durability in the near field. Werme et al. reported a deleterious effect of Fe2O3 or FeOOH on the durability of nuclear waste glass, with FeOOH exhibiting a stronger effect. The extent of glass corrosion was found to increase as the amount of Fe3O4 increased. In addition to the Fe-silicate formation mechanism, the authors proposed that the adsorption of Si on the surface of Fe2O3 or FeOOH could also play a role, because the acceleration of glass corrosion was diminished when all the adsorption sites on Fe2O3 or FeOOH were completely occupied. We recently described the corrosion interactions between a more realistic SS canister material and a model nuclear waste glass, international simple glass (ISG), under accelerated conditions by pressing the two materials against each other and immersing the assembly in NaCl solution at 90 °C. In addition to the precipitation of Fe-silicates, new mechanisms were revealed. The crevice corrosion of SS resulted in an aggressive acidic environment that could significantly enhance the corrosion of ISG present nearby. A continuous film was observed across the entire SS surface, consisting of elements that originated from SS and ISG corrosion. Meanwhile,
precipitation of Si-bearing minerals was identified, which was likely assisted by the SS cathodic reactions. The precipitation of the Si-bearing surface film and minerals could strongly consume Si from the solution, which may eventually lead to the accelerated glass corrosion that is known as stage III corrosion17,18.

This study aims to further explore the corrosion interactions between two model glass materials (soda-lime silica glass (SLSG) and ISG) and three corrosion resistant alloys (SS, Alloy G30, and alloy 625) to develop a fundamental understanding of the corrosion interactions between dissimilar materials in Cl− ions containing solutions. SLSG is a prevalent type of glass that has vast applications in our daily life, for example tableware and windowpanes. Due to its simplicity in chemistry compared to nuclear waste glass, it was applied in this work. The initial study was then extended to the more corrosion resistant glass ISG19,20, which has been investigated world-wide as a model nuclear waste glass. Alloy G30 and alloy 625 were selected due to their superior corrosion resistance compared to SS21. We have shown that SS crevice corrosion could accelerate the degradation of nearby ISG16, so it would be of interest to explore the corrosion interactions between the model glass and these more corrosion resistant alloys.

RESULTS
Corrosion of soda-lime silica glass
To simulate the corrosion of metal canisters and nuclear waste glass under accelerated conditions, different materials were pressed against each other and corroded in 0.6 M NaCl solution or DI water at 90 °C. Although the initial ion strength may be lower in the actual repository conditions, Cl− and Na+ ions are likely to be enriched at the material interface during corrosion16. The complete experimental groups are listed in Table 1. For simplicity, the terminology A(+B_solution) is used throughout this article to describe the sample assemblies. For example, SS(+SLSGNaCl) means an SS sample that was pressed against SLSG with exposure in NaCl solution. As shown in Fig. 1a, after 14 days of corrosion, a band pattern formed on SS(+SLSGNaCl), located near the boundary of the SS and SLSG contact area. These corrosion patterns are characteristics of the metal crevice corrosion, which is commonly observed on passive metals6.

During metal crevice corrosion, damage usually initiates within the crevice at a particular distance from the crevice mouth area due to the ohmic potential drop. In this region, the protective film breaks down and metal cations, protons, and aggressive anions such as chlorides accumulate, leading to highly aggressive environment that results in self-acceleration of the localized metal corrosion6−8. As a result of this spontaneous change in local chemistry, crevice corrosion is one of the most detrimental forms of metal corrosion, particularly for fabricated structures. Interestingly, similar patterns were also observed on the SLSG(+SSNaCl) surface (Fig. 1a′), where the corrosion was localized along the edge of the contact area, while the center of the crevice region was less corroded according to visual observation. This general observation was also verified by both solution and local surface analyses as described in the following sections. Note that two bands were observed on the SLSG(+SSNaCl): (i) the outer band delineates the boundary of the SS/SLSG contact area, which could be attributed to the alkaline attack caused by the cathodic oxygen reduction reaction (ORR) on the SS coupon surface surrounding the crevice edge, (ii) an inner band that was located a few millimeters deeper from the boundary, which was likely due to the acidic attack induced by SS crevice corrosion. An enlarged view of Fig. 1a′ shows that the inner band region on the glass was more corroded, which was accompanied by partial removal of the alteration layer that probably occurred during sample drying. It has been well documented that glass corrosion rate in diluted solutions is enhanced by several orders of magnitude under both acidic and alkaline conditions relative to neutral conditions22,23. Recent studies showed that this statement is still valid when the glass corrosion reaches a steady state regime (stage II) where the solution is saturated with silica, although the rate-limiting mechanisms are likely not the same for the two regimes24.

Therefore, the corrosion of SS in close proximity to glass could significantly enhance glass corrosion at both the anode and the cathode sites on the SS. It has been known that the sample surface area to solution volume (S/V) ratio can strongly affect glass corrosion25, so a control experiment was carried out by replacing the SS with PTFE (Fig. 1b), which would create a similar crevice with comparative S/V but not be reactive. As shown in Fig. 1b′, only a random corrosion morphology was observed on the SLSG(+PTFENaCl). Apparently, the high S/V ratio cannot fully explain the unique corrosion morphology observed in Fig. 1a, suggesting that SS indeed played an important role.

When DI water was used as the electrolyte, no clear crevice corrosion pattern was observed on SS(+SLSGDIW) (Fig. 1c) but drastically different corrosion morphologies were observed on SLSG(+SSDIW). As shown in Fig. 1c′, uniform corrosion was observed within the center of the contact region. Note that no chloride ions were present in the solution to break down the passive film of SS, so it is unlikely that crevice corrosion could occur here. However, a low amount of Fe2+ or Fe3+ ions could still exist in the occluded crevice environment due to the passive dissolution of SS, which seemed to influence the corrosion of SLSG within the center of the crevice. Interestingly, the size of the visibly discernable corrosion area on the SLSG surface was much smaller than the actual contact area, which may also be associated with mass transport from the edge region. However, different than crevice corrosion, the uniform passive dissolution on the SS in DI water resulted in uniform attack of the glass. For SLSG that was in contact with PTFE in DI water (Figs. 1d–d′), no visible damage was observed on the SLSG surface, which further indicates that the morphology observed in Fig. 1c′ could not be simply attributed to the high S/V ratio. Comparing Fig. 1b′ with Fig. 1d′, it may be concluded that NaCl also enhances the corrosion of SLSG.

Similar crevice corrosion phenomena were observed when the SS was replaced with more corrosion resistant alloys such as G30 (Fig. 1e–g) and alloy 625 (hereafter referred to as A625) (Fig. 1h, j). After 14 days of corrosion, pitting damage was clearly identified at the crevice mouth of both alloys. Meanwhile, localized corrosion was also observed at the crevice mouth of SLSG, while the center

Table 1. List of experimental groups and testing conditions for SS and glass corrosion.

| Sample ID      | Materials            | Solution          | Temperature | Duration |
|----------------|----------------------|-------------------|-------------|----------|
| SLSG-SSNaCl    | SLSG + SS 316        | 0.6 M NaCl 90 °C  | 14 Days     |
| SLSG-PTFENaCl  | SLSG + PTFE          | 0.6 M NaCl 90 °C  | 14 Days     |
| SLSG-SSDIW     | SLSG + SS 316        | DI water          | 14 Days     |
| SLSG-PTFEDIW   | SLSG + PTFE          | DI water          | 14 Days     |
| SLSG-G30NaCl   | SLSG + Alloy G30     | 0.6 M NaCl 90 °C  | 14 Days     |
| SLSG-A625NaCl  | SLSG + A625          | 0.6 M NaCl 90 °C  | 14 Days     |
| ISG-SSNaCl     | ISG + SS 316         | 0.6 M NaCl 90 °C  | 30 Days     |
| SS-PTFENaCl    | SS 316 + PTFE        | 0.6 M NaCl 90 °C  | 30 Days     |
| ISG-PTFENaCl   | ISG + PTFE           | 0.6 M NaCl 90 °C  | 30 Days     |
| ISG-SSDIW      | ISG + SS 316         | DI water          | 30 Days     |
| SS-PTFEDIW     | SS 316 + PTFE        | DI water          | 30 Days     |
| ISG-PTFEDIW    | ISG + PTFE           | DI water          | 30 Days     |
region appeared less altered. This suggests that the influence of metal crevice corrosion on glass is likely universal in these solution conditions and could be difficult to avoid even with extremely corrosion resistant alloys.

Specular reflectance infrared (SR-IR) spectroscopy was used to explore the changes of silicate networks on the corroded SLSG (+SSNaCl) surface. The spectra were collected from five different locations. The results are shown in Fig. 2a. Figure 2b is a macrograph of SLSG(+SSNaCl) showing the analyzed locations. On the pristine SLSG, three major peaks were identified. The peak observed at 1057 cm\(^{-1}\) is attributed to the asymmetric stretch vibrational mode of Si-O-Si (\(\nu_{Si-O-Si, \text{as}, \text{bridging oxygen, or BO}}\))\(^{26}\). The shoulder at \(~942\) cm\(^{-1}\) is associated with stretching vibration of Si–O (nonbridging oxygen, or NBO) group and Si-OH in the glass\(^{26}\). The peak at \(762\) cm\(^{-1}\) corresponds to symmetric vibration of Si-O-Si (\(\nu_{Si-O-Si, \text{s}, \text{BO}}\))\(^{26}\). The corroded SLSG shows some distinct changes in different locations indicative of chemical degradation. In the crevice mouth area, which is located between the inner and outer bands, the highest spectral intensity for the asymmetric vibration peak of Si-O-Si was markedly shifted to
1100 cm$^{-1}$, which is close to that of fused quartz$^{27}$ (1120 cm$^{-1}$). This is indicative of a leaching process (partial dissolution of alkali followed by slow silanol condensation) that is likely associated with acidic attack. During this process, the Na$^{+}$ ions are exchanged with protons originating from water dissociation, which can be accompanied by the shortening of Si-O bond length, causing the build-up of tensile stress in the glass network in the crevice mouth area$^{28}$. Meanwhile, the shoulder peak at $\sim$942 cm$^{-1}$ from the pristine SLSG became more evident, which may be attributed to the conversion of BO to NBO or Si-OH groups after leaching$^{26}$. The spectra are similar for the crevice center and the area outside of crevice, which show only slight shift of the 1057 and 762 cm$^{-1}$ peaks, while the $\sim$942 cm$^{-1}$ peak also became more evident. These two spectra are also close to that of pristine SLSG, suggesting that the two areas are less altered compared to the crevice mouth region. The spectra collected from the two stained bands regions showed clear red shift of the 1057 and 762 cm$^{-1}$ peaks. If this is caused by the ingress of metal cations (such as Fe$^{2+}$, Fe$^{3+}$, or Cr$^{3+}$) with different sizes into the Si network, it could also generate internal stress in the alteration layer and affect the Si-O stretch band position$^{28,29}$. This assumption was supported by the observation of new peaks near 650–660 cm$^{-1}$, which could be attributed to the stretching vibration of Fe-O$^{3+}$$^{30,31}$ or Cr-O$^{32}$. The mismatch of local stress between different regions may explain the rupture of the gel layer observed in the crevice mouth area shown in Fig. 1a$^'$. The presence of metal cations (Fe$^{2+}$, Fe$^{3+}$, or Cr$^{3+}$) on SLSG (+SSNaCl) was further validated by X-ray photoelectron spectroscopy (XPS). As shown in Fig. 2c, it is clear that Fe$^{2+}$ or Fe$^{3+}$ does exist in the inner band region. However, the low resolution (due to low concentration) made the identification of valence state difficult. The composition of SLSG (+SSNaCl) at the abovementioned locations was also quantified by XPS (Fig. 2d). Depletion of Na is apparent across the entire surface and varies slightly with location. Despite the high concentration of Na$^{+}$ in the medium, the partial loss of Na$^{+}$ ions in the altered layer strongly suggests that ions exchange occurred between Na$^{+}$ from the glass and protons generated by water dissociation. Depletion of Ca was observed for all locations except for the crevice center, where Ca was significantly enriched (more than a factor of 2). This further supports the notion that the crevice corrosion primarily occurred near the crevice mouth region, which led to the local acidification in that area. Fe was identified at the inner band area and the crevice center, which was more evident in the crevice center. The presence of Fe in the inner band is consistent with SR-IR results. However, SR-IR results suggest that Fe is absent within the crevice center, which does not agree with the XPS result. This indicates that Fe may exist as a precipitated thin layer in the crevice center, while Fe$^{2+}$ or Fe$^{3+}$ ions were incorporated into Si network in the inner band region. No Fe was found in the outer band region. Instead, a strong Cr signal was detected in this region, which again suggests the ingress of Cr$^{3+}$ ions into the altered glass network, consistent with the SR-IR results.

**Corrosion of ISG**

**Corrosion morphology.** It is evident that SS has substantial effects on the corrosion of SLSG. However, most nuclear waste glass has a more complicated chemistry and the corrosion mechanism may be different than SLSG. Therefore, a model nuclear waste glass, ISG$^{15}$, was studied. The corrosion behavior of this SS + ISG system has been partially described in a previous paper$^{15}$. More results are provided in this study. As shown in Fig. 3a, crevice corrosion characteristics were also observed on ISG(+SSNaCl) after 30 days of exposure at 90 °C. An obvious band corrosion pattern can be seen near the crevice mouth area, while the center region was less corroded. The morphology was similar to what was observed on SLSG(+SSNaCl) as shown in Fig. 1a$^'$. Control experiments were conducted by pressing ISG against SS or PTFE, followed by immersion in 0.6 M NaCl or DI water at 90 °C for 30 days. The surface morphologies of ISG(+SSNaCl), ISG(+TFENaCl), ISG(+SSDIW), and ISG(+PTFEDIW) are shown in Fig. 3b–e, respectively. It is evident that the crevice corrosion characteristics are only present on ISG(+SSNaCl), but not on any other samples. The morphologies are consistent with what was observed on SLSG corroded under similar conditions, suggesting that the corrosion interactions...
suggesting that more corrosion occurred on ISG (–SSNaCl) while the thickness for other samples ranges from 10–40 µm. The degree of corrosion is closely correlated to the thickness of the alteration layer. Therefore, the corroded ISG samples were all sectioned to allow observation of the gel layer cross-sections in a scanning electron microscopy (SEM). As shown in Fig. 3f–i, the gel layer thickness for ISG(+SSNaCl) is ~25–40 µm, while the thickness for other samples ranges from 10–15 µm, suggesting that more corrosion occurred on ISG(+SSNaCl). Note that the cracks visible in the gel were likely formed during the sample preparation, which is generally the consequence of capillary forces after partial dehydration or the build-up of stresses within the gel.

Chemical compositions of altered ISG

The compositional change of the altered ISG was examined by XPS (Fig. 4). For each sample, XPS spectra were obtained from three different locations: the crevice mouth, crevice center, and the non-contact back side. In the previous paper,15, it was shown that, as a result of SS crevice corrosion, localized acidic attack was observed in the crevice mouth area of the ISG(+SSNaCl), where depletion of all major elements except for Si occurred for SI. On the non-contact side of ISG(+SSNaCl), Na and Ca were both depleted due to ion exchange, while Zr and Al were slightly enriched. The back side of the ISG was in contact with the PTFE container with a similar S/V ratio as the contact side, so it serves as a good reference. The drastic compositional difference between the two surfaces indicates the crucial effect of SS. In contrast, the corrosion on ISG(+PTFE_DIW) was relatively more uniform than that of ISG(+SSNaCl). In this study, we show that when DI water was used as leaching solution, the effect of SS crevice corrosion was eliminated. As shown in Fig. 4, no Fe was identified on either ISG(+SSDW) or ISG(+PTFE_DIW). Since no Na + was present in the leaching solution, Na was depleted almost completely from the surface of both samples. Enrichment of Ca was observed on the contact and noncontact sides of both samples, but was more evident on the noncontact side. The presence of Ca in the gel has been known to reduce the reactive diffusion coefficient of water within the gel layer36,37, thus enhancing the durability of glass. Zr was also enriched in the different regions of both ISG(+SSDW) and ISG(+PTFE_DIW). The enrichment of insoluble Zr oxides has been observed in other studies38, which was believed to impact the residual rate of glass alteration39,40. Therefore, the enrichment of Ca and Zr on ISG corroded in DI water, along with the depletion of both elements on ISG corroded in NaCl solution, indicates that NaCl has an adverse effect on ISG corrosion. The Al concentration is generally similar for ISG(+SSNaCl) and ISG(+SSDW), and ISG(+PTFE_DIW). Overall, the chemical distribution observed on ISG(+SSDW) and ISG(+PTFE_DIW) was relatively similar, suggesting that ISG is not strongly affected by contact with SS in the absence of Cl − ions. This is expected because aggressive anions are critical for the onset of crevice corrosion, by causing the breakdown of the protective passive film. Under disposal-relevant conditions, Cl − will be present in the ground water, although in a much lower concentration41. During localized corrosion, Cl − ions will migrate to the occluded anode site to balance the extra charges resulted from metal dissolution, so Cl − ions are likely to be accumulated over time at the interface of the canister and nuclear waste glass. In a typical crevice corrosion event, the local concentration of Cl − can exceed 1 M. Therefore, although the initial Cl − ion concentration may be low (<10 mM42,43) under the real repository conditions with no corrosion interaction between the canister and nuclear waste glass, a highly concentrated salt environment may form in the near field of nuclear waste glass, both resulting from and causing accelerated corrosion at the material interface. More studies are required to validate this hypothesis and to further understand the interfacial corrosion between nuclear waste glass and metallic canisters in more realistic ground water environment for a much longer duration, which will lead to improved understanding of the implications for nuclear waste disposal.
Inductively coupled plasma optical emission spectrometry (ICP-OES) was employed to further estimate the gel properties by measuring the concentration of different elements in the bulk leaching solutions. The results are shown in Table 2. In general, Si, B, Al, and Ca were detected in all solutions containing ISG samples, which is expected. No Fe (<0.1 ppm) was found in solutions containing SS samples, even for SS(PTFENaCl), where severe localized corrosion occurred on SS and brown corrosion products were visible on the walls of the reactors. The absence of Fe in the solution could be attributed to the low solubility of Fe$^{2+}$ or Fe$^{3+}$ ions in alkaline solutions, as the solution pH value was about 8.4–8.6 after the corrosion testing (measured at room temperature). Under open circuit conditions, Fe tends to form insoluble iron oxides or hydroxides in this pH range.

Knowing the elemental concentrations in solution and assuming uniform alteration, the equivalent thickness ($E_{th}$) of altered glass was calculated. B is one of the most soluble species in ISG, so the dissolution rate of B is commonly used to express the corrosion rate of glass. Correspondingly, the equivalent thickness of B, $E_{th}(B)$, can be correlated to the gel layer thickness. Meanwhile, the fraction of each element being retained in the gel can be defined as retention factor (RF), which is given by $1 - E_{th}(i)/E_{th}(B)$. Since one side of ISG samples was shielded by other materials, the total effective surface area was not well defined. Therefore, the $S/V$ value in Eq. 1 is not well defined. The calculation of $E_{th}(i)$ was initially performed by including the contact surface area. The resulting $E_{th}(B)$ values were significantly lower than the actual thickness measured by SEM (Fig. 3f-i). In contrast, when the contact surface area was excluded, the $E_{th}(B)$ values agreed reasonably well with the SEM results, especially for samples corroded in DI water. It is worth noting that the actual thickness of the gel on ISG(PTFENaCl) falls between the $E_{th}(B)$ values calculated using the two methods. However, the actual thickness of gels measured in the crevice mouth area of ISG(NaCl) was significantly higher than the higher estimated $E_{th}(i)$ value, suggesting that the corrosion on this sample was strongly localized. In addition, the $E_{th}(B)$ values for ISG corroded in NaCl solution are approximately twice those corroded in DI water, further validating that NaCl enhances the alteration of ISG, which agrees well with the XPS results. This may be attributed to the ion exchange between Na$^+$ in the solution and the Ca$^{2+}$ ions in the ISG, which explains the strong depletion of Ca from the gel (low RF value). Cl$^-$ anions may also play a role in glass corrosion, but again, this effect is still not certain. Previous studies showed that the effect of cations in the leaching solution on initial dissolution rate dominate over anions. Similar to Ca, Al was almost depleted from the gel for ISG corroded in NaCl, which is more evident for ISG(PTFENaCl). However, for ISG corroded in DI water, over 50% of Ca and Al was retained in the gel. The presence of Ca and Al has been known to limit the reactive diffusion coefficient of water within the gel layer. Therefore, the deficit of these two elements in the gels formed in NaCl again suggests that the NaCl has an adverse impact on the durability of ISG.

Solution analysis

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Si may be more reliable because other elements are soluble in such conditions. Similar trends were observed for the two normalization methods, where Na, Al, and Zr were depleted in an area that is about 2 mm within the boundary of the crevice. This led to the formation of a more silica-like gel, which is consistent with XPS results. The localized corrosion on ISG at a particular distance from the boundary of the crevice may be associated with the competition between SS dissolution, which is depth-dependent, as they were almost completely depleted from the outermost layer as observed by XPS. This Al rich layer was much thinner than the gel, with a different chemistry, so it did not seem to result from gel self-reorganization. Instead, the layer is more likely a consequence of precipitation at the interface of solution and the gel. Given the fact that the solution was not saturated in silica, the occurrence of dissolution and precipitation is likely. Interestingly, Cl− was detected in the gel layer, which could be attributed to the porosity of the gel.

Silicate network changes on corroded ISG surface

SR-IR spectroscopy was used to probe the changes of silicate networks on the corroded ISG surface (Fig. 6). All spectra were collected at the center of the crevice area, as well as the non-contact area to further explore the effect of leaching solutions. For ISG samples altered in NaCl solutions (Fig. 6a, b), B was completely leached out from the surface layer (to a depth of ~10 µm) as no B−O band was observed at 1380 cm−1, which is consistent with the solution analysis and XPS results. However, for ISG that were immersed in DI water (Fig. 6c, d), B-O band still exists although the peak intensity was lower than the pristine ISG. Since the analysis depth for SR-IR is about 10 µm in the B−O stretch region and the gel layers for ISG altered in DI water are slightly thinner than this value, B may originate from the underlying pristine ISG. For pristine ISG, the asymmetric stretch vibrational mode of Si−O−Si shows up at 1038 cm−1. For all corroded ISG samples, this peak shifted to a higher wavelength of 1066 cm−1 due to ion exchange and Si network reorganization. The blue shift of the Si−O−Si peak also implies a shorter length of the Si−O−B bond in the alteration layer, indicating the build-up of tensile stress on the altered glass surface. As the alteration layer gets thicker, such stress may eventually exceed the cohesive strength of the alteration layer causing mechanical instability. For all corroded ISG samples, two new peaks appear near 788 and 896 cm−1, which have been attributed in a previous study to the stretching vibrations of SiO2 (corner-sharing tetrahedra) with A1 (v(SiO4), A1) and T2 (v(SiO4), T2) symmetry, respectively. These two peaks are more evident for ISG corroded in NaCl solution, suggesting a higher degree of network changes. However, no visible changes were identified between ISG(+SSNaCl) and ISG(+PTFEdw), or between ISG(+SSDw) and ISG(+PTFEnaCl). Also, no significant differences were observed between different locations. These results indicate, that within the depth that SR-IR can measure, Na+ ion exchange may be the dominant reaction for ISG corrosion under these testing conditions due to its high chemical durability. Therefore, studies with longer durations are required (currently ongoing) to identify any differences.

Corrosion of stainless steel

It was reported previously that, when SS and ISG were exposed together in NaCl solution, the corrosion of SS was suppressed by ISG (also see Fig. 7a, b). The reduced corrosion rate on SS may be associated with a continuous film formed on SS(+ISGNaCl) surface, consisting of almost all major elements in SS and ISG. This layer may act as a physical barrier and protect the SS matrix from the corrosive medium. In this study, when DI water was used as the leaching solution, no crevice corrosion was identified on SS(+ISGdw) or SS(+PTFEdw). However, pitting corrosion is still visible on multiple locations of SS(+ISGdw) (Fig. 7c), but less evident on SS(+PTFEdw) (Fig. 7d, e), suggesting that elements leached from ISG may accelerate the pitting corrosion of SS under the testing conditions. It is unlikely that B, Na, or Si are the cause of the attack. However, previous studies by Kim et al. showed that

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**Table 2. Analysis of the leaching solutions.**

| Sample | ISG(+PTFEnaCl) | ISG (+SSNaCl) | ISG(+PTFEdw) | ISG (+SSDw) |
|--------|----------------|---------------|--------------|-------------|
| Elemental concentration/ppm | | | | |
| Si     | 9.0            | 18.1          | 9.0          | 8.7         |
| Al     | 1.4            | 0.3           | 2.0          | 2.2         |
| Ca     | 3.7            | 3.7           | 3.6          | 3.5         |
| Solution pH | | | | |
| pH_initial | 6.1           | 6.1           | 6.0          | 6.0         |
| pH_10days | 8.4            | 8.4           | 8.5          | 8.6         |
| Equivalent thickness (including contact area in S/V calculation/µm) | | | | |
| Eth(Si) | 5.2            | 5.2           | 5.2          | 5.2         |
| Eth(B) | 17.9           | 17.9          | 17.9         | 17.9        |
| Eth(Al) | 17.2           | 17.2          | 17.2         | 17.2        |
| Eth(Ca) | 15.8           | 15.8          | 15.8         | 15.8        |
| Retention factor | | | | |
| Eth(Al)/Eth | 0.04           | 0.04          | 0.04         | 0.04        |
| Eth(Al)/Eth | 0.12           | 0.12          | 0.12         | 0.12        |
| Eth(Si)/Eth | 0.71           | 0.71          | 0.71         | 0.71        |

*a*Due to the large ohmic potential drop in DI water, a small amount of KCl salt (0.03 M) was added to DI water for the accurate measurement of solution pH.96.

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Al$^{3+}$ can accelerate the corrosion rate of SS at elevated temperature (80 °C) by lowering the pitting potential while increasing the passive current density. Liu et al. also showed clear evidence that even a low amount of Al$^{3+}$ enhanced the mass transport limited cathodic kinetics of SS at room temperature. A mechanism based on Grotthuss theory was proposed by the authors, where the presence of Al$^{3+}$ ions lowered the bond strength of O-H in water molecules. This process facilitated the transport of protons from the solution to the metal surface, leading to the increased cathodic kinetics. Therefore, when DI water is used as the leaching solution, SS corrosion may be accelerated by ISG corrosion. However, the occurrence of pitting corrosion is still unexpected, since no aggressive anions (e.g., Cl$^{-}$) are present in the solution. None of the dissolved species from ISG corrosion is likely to break down the passive film of the SS. To further study this phenomenon, a separate electrochemical experiment was performed. A SS specimen was potentiodynamically polarized in the 30-day-leaching solution of ISG(PTFE-DIW) with composition shown in Table 2. The polarization curve is given in Fig. 8a. A low corrosion current density on the order of $10^{-7}$ A/cm$^2$ was observed, indicating spontaneous passivity of the SS. The SS remained generally passive in the potential range of 100–500 mV$_{SCE}$, but a small current peak is evident near 150 mV$_{SCE}$. This

**Fig. 5** SEM images and EDS point analysis for the ISG(+SSNaCl). a Surface morphology near the crevice mouth area (contact side). EDS point analysis was collected on three different locations and the results were normalized to b Si and c Al. d Cross-section of gel layer formed on the non-contact side. e EDS point analysis for five selected spots of the gel layer.

| Element | Nominal | Spot 1 | Spot 2 | Spot 3 | Spot 4 | Spot 5 |
|---------|---------|--------|--------|--------|--------|--------|
| O       | 50.1    | 51.9   | 36.9   | 36.2   | 40.4   | 42.9   |
| Na      | 9.0     | 8.0    | 5.7    | 7.7    | 7.5    | 6.5    |
| Al      | 3.2     | 4.2    | 10.2   | 10.8   | 9.2    | 4.7    |
| Si      | 26.3    | 30.7   | 38.6   | 36.3   | 30.6   | 22.0   |
| Zr      | 2.4     | 1.5    | 5.9    | 6.2    | 9.0    | 19.8   |
| Ca      | 3.6     | 3.8    | 1.3    | 0.0    | 0.6    | 1.1    |
| Cl      | 0.0     | 0.0    | 0.8    | 1.8    | 2.1    | 2.4    |

**Table 3.** Chemical composition of gels formed on the non-contact side of ISG(+SSNaCl).
peak is probably not associated with the oxidation of species in the ISG leaching solution, which are likely in their maximum oxidation state. Other authors have reported a similar current when the SS was potentiodynamically polarized in solutions containing $F^-$ ions. Cao et al. observed a similar peak at 380 mV vs. SCE, which only occurred in solutions with high $F^-$ ions (0.1 M). However, the concentration of $F$ in this study was below 0.1 ppm, suggesting a more complicated mechanism probably involving the complexation of dissolved species from ISG. Small current transients likely associated with metastable pitting events were identified from 300 to 500 mV SCE, indicative of passive film instability. A breakdown potential appeared at 500 mV SCE, suggesting that localized corrosion occurred. When the current density approached 1 mA/cm², the increase of current density slowed down, which was associated with ohmic potential drop in the cell. Upon reversal of the scan direction, the current density remained large. This positive hysteresis loop is a diagnostic indication that the breakdown was indeed caused by localized corrosion. After polarization, the SS surface was examined in an SEM. Although pitting corrosion was not observed, extensive crevice corrosion was evident (Fig. 8b), which supports the evidence of localized corrosion provided by the potentiodynamic polarization curve. The presented crevice corrosion occurred in the contact area of the SS and the O-ring, which was a component of the electrochemical cell designed for preventing solution leakage. The occurrence of crevice corrosion is also consistent with the unexpected pitting corrosion identified on the SS (+ISG) (Table 4). These localized corrosion events might be explained by the presence of $F^-$ ions in the ISG (+PTFE) leaching solution, which could have originated from the PFA containers and PTFE specimens. Note that the PFA containers and PTFE specimens were all pretreated to remove $F^-$ ions according to ASTM C1285. However, the $F^-$ ions were probably not completely eliminated because $F$ is one of the primary components of both PFA and PTFE. The observation suggests that localized corrosion could occur at the interface of metal canisters and nuclear waste glass, even with a low amount of aggressive anions that is below the detection limit of ICP-OES. Therefore, the corrosion interaction observed at the metal and glass interface seems to be difficult to avoid, so it should be carefully considered in future models for materials corrosion. Besides crevice corrosion, Si-bearing phases were found to be precipitated on the SS surface (Fig. 8c). Upon closer examination, the particles also contained Ni, Fe, and Cr, which originated from SS corrosion. EDS elemental maps were also collected on the lacy covers surrounding the crevice damage, because these passive film remnants are thin enough and enable the characterization of outermost surface layer without interference from the SS matrix. As shown in Fig. 9, the surface film primary consists of Fe, Ni, Mo, and Cr, which are the major elements from SS. However, a layer of Si is visible across the entire surface, which originated from the ISG leaching solution. The co-precipitation of Si and metal cations in the secondary phases, along with the observation of continuous Si-rich film on SS surface indicates that the corrosion of SS could delay the saturation of silicates near the glass and thus enhance the glass corrosion, which is consistent with the previous results obtained at the open circuit potential.

**DISCUSSION**

An oxic environment was used in this study, which is relevant to the U.S. Yucca Mountain project. Although anoxic disposal conditions have been considered by many countries, an anoxic condition is not likely to be maintained throughout the lifetime of...
Oxygen will be introduced during the excavation and waste emplacement, which is likely to exist for a certain period of time until consumed by corrosion or other processes. The dissolved oxygen has been considered in Canadian waste assessment models, while other oxidants could be present in different environments proposed by other countries. Additionally, the water radiolysis introduced by the incorporated radionuclides within the waste package may generate various oxidants. Due to the mass transport limitation, these oxidants are likely to be depleted within the confined interfacial space between the metallic canisters and encapsulated waste forms, a process similar to oxygen depletion during crevice corrosion. Therefore, although this study was conducted in an oxic environment, the disclosed corrosion mechanism could still be applied to anoxic environments.

Whether water could be present in the repository is also an important and valuable argument. At the potential Yucca Mountain site in the U.S., perched water exists in the rock pores. During the heat up phase of the long thermal cycle that Yucca Mountain will experience, this water will be driven away from the hot drifts. However, in the cooling phase, the water will come back down into the drift. It should be noted that the presence of an aqueous environment is not limited to the U.S. Yucca Mountain repository. For all of the repositories being considered by every nation with nuclear waste, whether in granite, clay or tuff, the most likely scenario involves a first stage of desaturation tied to oxygen depletion during crevice corrosion.

Fig. 7 Corrosion morphologies of SS. a SS(+ISGNaCl), b SS(+PTFENaCl), c SS(+ISGDIW), d SS(+PTFEDIW). e Optical profilometry image showing pitting corrosion observed on a typical area of SS(+PTFEDIW). Visible pits are indicated in black circles.
Table 4. EDS elemental quantification results for Figs. 8 and 9.

| EDS Quantiﬁcation for Fig. 8 | EDS Quantiﬁcation for Fig. 9 |
|-----------------------------|-----------------------------|
| Element | Atomic % | Intensity (counts) | Error % | Element | Atomic % | Intensity (counts) | Error % |
| C K     | 31.9     | 318.4             | 9.5     | Si K    | 2.2      | 96.8             | 7.9     |
| Si K    | 0.7      | 107.6             | 9.1     | Mo L    | 1.5      | 82.3             | 10.2    |
| Cr K    | 13.3     | 2343.2            | 2.1     | Cr K    | 23.9     | 278.5            | 6.7     |
| Fe K    | 47.2     | 6425.6            | 1.9     | Fe L    | 45.4     | 1287.0           | 5.9     |
| Ni K    | 6.3      | 661.3             | 3.2     | Ni L    | 5.6      | 141.1            | 12.6    |

Fig. 8 Effect of ISG on SS corrosion. a Potentiodynamic polarization of SS in the 30-day-leaching solution of ISG(+PTFE<sub>CmH</sub>). b Crevice corrosion damage observed after the polarization. c SEM and EDS elemental mapping of secondary phase precipitated on the SS after polarization. The EDS elemental quantification results are listed in Table 4.

Fig. 9 EDS elemental mapping of the SS surface after potentiodynamic polarization. The EDS elemental quantification results are listed in Table 4.
the heat production from the wastes, followed by a second stage of resaturation by ground water. Therefore, water is highly likely to be present in the repository. The safety demonstration requirements that all corrosion processes in vapor or liquid water that potentially affect the waste form performance must be studied in detail. It is thus a reasonable assumption that water could exist and induce corrosion in the repository.

Preliminary study of metal and glass corrosion interaction was performed with several corrosion resistant alloys and a commercial SLSG, which was used as a model boron-free glass. Although only a few techniques were used to characterize the corroded samples, the corrosion mechanism has been revealed, owing to the high corrosion rate of SLSG. The study was then extended to the more complicated system of ISG, a reference six-oxide borosilicate glass, and SS to gain mechanistic understanding of the potential near-field corrosion interactions between nuclear waste glass and metallic canister materials.

The interactions of SS and glass led to similar corrosion morphologies on SLSG and ISG as shown in Figs. 1 and 3, respectively. However, there are some differences. Visual observation suggests that the band pattern is more evident on SLSG (+SSNaCl), although the exposure time was half that of ISG (+SSNaCl). Two bands were observed on SLSG(+SSNaCl), while only one band was identified on ISG(+SSNaCl). This could be attributed to the different sizes of specimens used. For the SLSG and SS interaction study, the SS specimen was smaller than the SLSG. Therefore, when the two specimens were pressed against each other, crevice corrosion of SS occurred within the contact area, leading to the formation of the inner band. The shape of the outer band matches perfectly with the boundary of the contact area, so it is most likely affected by the cathodic ORR. In contrast, for the ISG and SS interaction study, the SS specimen was intentionally smaller than the SLSG. Therefore, when the two specimens were pressed against each other, crevice corrosion of SS occurred within the contact area, leading to the formation of the inner band. The shape of the outer band matches perfectly with the boundary of the contact area, so it is most likely affected by the cathodic ORR. In contrast, for the ISG and SS interaction study, the SS specimen was intentionally larger than the ISG. A larger SS specimen with a small contact area can result in a larger cathode-to-anode ratio, thereby increasing the rate of localized corrosion on SS and thus accelerating the corrosion of SS altered in close proximity to ISG in DI water. Only the SS (+PTFE2NaCl) leach solution contained Fe at sufficient concentration to be detectable by ICP-OES (~0.6 ppm). The final pH for this solution was 4.6, which explains the stability of Fe2+ or Fe3+ ions. In contrast, no Fe was detected in the SS(+ISG2NaCl) leach solution with a final pH of 8.6. However, as shown in Fig. 7c, d, the pitting damage on SS(+ISG2NaCl) is clearly more severe than that of SS (+PTFE2NaCl). This suggests that Fe2+ ions resulted from the corrosion of SS(+ISG2NaCl) may have been removed from the leaching solution by the precipitation of insoluble Fe-silicates. This mechanism, along with the acceleration effect of Al3+ ions, may explain the enhanced corrosion rate of SS altered in close proximity to ISG in DI water.

Combining all observations, it may be concluded that corrosion interactions exist between the metallic canisters and glass waste form when they are exposed in aqueous environment. The localized corrosion of metals creates an aggressive environment by generating metal cations. These cations could be incorporated into the gel network, leading to the change of gel structure and chemistry, generating local stress that could undermine the mechanical integrity of the gel layer, and eventually result in the release of incorporated radionuclides. The hydrolysis of the metal cations also acidifies the local environment, which significantly affects the corrosion of nearby glass. These interactions could not be avoided even with extremely corrosion resistant alloys. Additionally, these interactions seem to be solution dependent. In a real repository environment, the interactions could be more complicated. For example, this study was conducted in an oxic environment, which is the expected condition for the repository under consideration by the U.S. Yucca Mountain project. However, most other countries are considering anoxic repository conditions, which may lead to different corrosion behaviors.
environments. In such conditions, the hydrogen evolution reaction would be the more likely dominant cathodic reaction on metallic canisters rather than ORR. It would be of interest to study the interactions of metallic canisters and nuclear waste glass in this condition. Additionally, the underground water chemistry is much more complicated than the NaCl solution or DI water used in this study. We have shown here that Al$^{3+}$ originating from ISG corrosion may have an adverse effect on SS corrosion. However, the real nuclear waste glass may include more than half elements from the periodic table, so a wide range of ions could be released into the electrolyte and impact the corrosion of canister materials. More studies are required to better understand these corrosion interactions, which could advance our understanding and eventually lead to improved models for materials corrosion in long-term post-closure disposal conditions.

### METHODS

#### Materials

Soda lime silica glass (SLSG) (Fisherbrand™ 125444) and sodium chloride (NaCl) (crystalline/certified ACS, CAT# S27150) were purchased from Fisher Scientific and used without further modification or purification. ISG blocks were provided by Pacific Northwest National Laboratory and Savannah River National Laboratory. SS 316 (UNS S31600) was purchased from McMaster-Carr. The compositions of materials used in this study are listed in Table 5. All water experiments were replicated at least two times.

#### Corrosion experiment

Prior to corrosion, the SLSG (75 mm × 25 mm × 1 mm) and ISG coupons (25 mm × 11 mm × 3 mm) were cleaned with ethanol and DI water and dried. The SS sheet was cut into 13 mm × 13 mm × 3 mm (for SLSG-SS corrosion) or 25 mm × 25 mm × 3 mm specimens (for ISG-SS corrosion). The alloy G30 and A625 sheets were cut into 13 mm × 13 mm × 3 mm specimens. All metal samples were abraded to 600 grit with SiC paper and cleaned with DI water and ethanol and dried for further usage. The metal samples were placed on top of the glass samples to form a crevice between them by gravity. The assemblies were wrapped with PTFE tape to secure them during corrosion, followed by a complete immersion in 0.6 M NaCl solution or DI water at 90°C. As control experiments, the glass or metal samples were also pressed against PTFE coupons and corroded under the same conditions. A complete list of experimental groups can be found in Table 1. After 14 or 30 days of static immersion, the assemblies were removed from the solutions. Different materials were separated from each other, cleaned with abundant DI water, air dried, and stored in a desiccator at room temperature for further analysis. The corrosion experiments were replicated at least two times.

#### Solution analysis

After the corrosion experiment, the solutions were sampled, and the solution composition was analyzed by ICP-OES, (Perkin-Elmer). The equivalent thickness of each element can be calculated using the following equation:

$$\text{Eth}(i) = \frac{c(i) \times f(i) \times \rho}{S/V}$$

where c(i) is the concentration of each species in µg/mL, S/V is the glass surface area to solution volume ratio in cm$^{-1}$, f(i) is the mass fraction of each element in ISG, and ρ is the density of glass in g/cm$^3$ ($\rho = 2.5$ g/cm$^3$ for ISG$^{10}$).

#### X-ray photoelectron spectroscopy

XPS was employed to characterize the chemical composition of pristine and corroded SLSG and ISG samples. A PHI VersaProbe II spectrometer (Chanhassen) equipped with a monochromatic Al-Kα (1486.6 eV) X-ray source was used. For ISG analysis, the spectra were collected on three different areas: (1) the edge of the contact area of different materials (i.e., crevice mouth area); (2) the center of the contact area, which is the crevice center; (3) the back side of the ISG, which was in contact with the PFA container, as a reference. For each area, the spectra were collected on three random locations. For SLSG analysis, five different locations were examined: (1) the area outside of crevice; (2) the outer band region; (3) the inner band region; (4) the area between inner and outer band; (5) crevice center region. All spectra were calibrated to the adventitious C 1s signal at 284.8 eV. All elemental compositions were normalized to the concentration of Si for better comparison among different samples.

#### Specular reflection infrared spectroscopy

Specular reflection infrared (SR-IR) spectroscopy was used to characterize the changes in silicate network through the surface of the SLSG and ISG. The measurement was performed in the mid-infrared range (4000–500 cm$^{-1}$) using a Bruker Hyperion 3000 µ-FT-IR system with a 15× infrared microscope objective lens (Bruker Optics Inc.). The spectra were collected at a 20° incidence angle at an average scanning rate of 400 scans per spectrum. The probing area was 100 µm × 100 µm, and the spectral resolution was 6 cm$^{-1}$. The spectrum of a clean gold surface with mirror finish was used as a reference.

#### Optical microscopy

The morphologies of altered ISG and SS samples were subjected to analysis by an optical microscopy. A large view of ISG was obtained by manual stitching of multiple micrographs as shown in Fig. 3b–e.

#### Potentiodynamic polarization

The effect of ISG leaching solution on SS corrosion was assessed by potentiodynamic polarization. A three-electrode cell was used, including working, counter, and reference electrodes. The SS (abraded to 1200 grit) specimen was loaded into the electrochemical cell and connected as the working electrode. A rubber O-ring was used between the SS and the cell to prevent solution leakage. The SS specimen was mounted into a

### Table 5. Chemical composition of materials in weight percent.

|       | Si   | B    | Na   | Al   | Ca   | Zr   | O    |
|-------|------|------|------|------|------|------|------|
| ISG   | 26.3 | 5.4  | 9.0  | 3.2  | 3.6  | 2.4  | 50.1 |
| SLSG* | 39.8 | 0    | 7.4  | 0    | 3.3  | 0    | 49.4 |
|       | C    | Mn   | P    | S    | Si   | Cr   | Ni   | Mo   | N    | Fe   |
| SS316 | 0.018| 1.257| 0.037| 0.001| 0.270| 16.669| 10.070| 2.010| 0.052| Balance |
| Co    |     |      |      |      |      |      |      |      |      |      |
| G30   | <5.0 | 1.5  | 2.5  | 2.0  | <0.8 | 30   | Balance| 5.5  | 0.8  | 15   |
| C     |     |      |      |      |      | 20.7 | 23.0 | 23.0 | 23.0 | 23.0 |
| A625  | <0.1 | <0.5 | <0.4 | <0.15| 1.0  | 20.0–23.0 | 58.0 | 8.0–10.0 | 3.15–4.15 | 5.0 |

*The composition of SLSG was obtained by XPS from three random locations on the same clean, uncorroded SLSG.
When the current density reached approximately 1 mA/cm², the sweeping below OCP and proceeded upwards at a scanning rate of 0.167 mV/min. The open circuit potential (OCP) was measured for 30 min prior to the analysis. The analysis depth (R/nm) of EDS was estimated with Kanaya-Okayama Range equation 4: 

\[
R = \frac{2.76 \times 10^{-3} A}{\rho Z^{1/3}}
\]

where \(E\) is the accelerating voltage of electron beam (V), \(A\) is the average atomic weight of the target material (g/mol), \(Z\) is the average atomic number, and \(\rho\) is the density of target material (g/cm³).

**DATA AVAILABILITY**

The data that support the findings of this study are available from the corresponding author upon request.

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AUTHOR CONTRIBUTIONS

X.G., S.G., S.H.K., J.D.V., J.I.V.R. and G.S.F designed the research; X.G., H.L., D.N., J.L., S.S.
analyzed the research; X.G., S.G., H.L., D.N., J.L. and S.H.K. analyzed the data. All authors contributed to the editing of the paper, and approval of the content in its current form.

COMPETING INTERESTS

The authors declare no competing interests.

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