Spreading of Non-Newtonian and Newtonian Fluids on a Solid Substrate under Pressure

Moutushi Dutta Choudhury 1, Subrata Chandra 1, Soma Nag 1, Shantanu Das 2 and Sujata Tarafdar 1

1 Condensed Matter Physics Research Centre, Physics Department, Jadavpur University, Kolkata 700032, India
2 Reactor Control Division, Bhabha Atomic Research Center, Trombay, Mumbai 400085, India
E-mail: mou15july@gmail.com

Abstract. Strongly non-Newtonian fluids namely, aqueous gels of starch, are shown to exhibit visco-elastic behavior, when subjected to a load. We study arrowroot and potato starch gels. When a droplet of the fluid is sandwiched between two glass plates and compressed, the area of contact between the fluid and plates increases in an oscillatory manner. This is unlike Newtonian fluids, where the area increases monotonically in a similar situation. The periphery moreover, develops an instability, which looks similar to Saffman-Taylor fingers. This is not normally seen under compression. The loading history is also found to affect the manner of spreading. We attempt to describe the non-Newtonian nature of the fluid through a visco-elastic model incorporating generalized calculus. This is shown to reproduce qualitatively the oscillatory variation in the surface strain.

1. Introduction
Static and dynamic aspects of wetting and spreading are well studied classical textbook problems. However, forced spreading of a fluid under an impressed load is not widely discussed, though the physics involved is challenging and the problem has important applications in technology as well. In real life many fluids are non-Newtonian, adding further complexity to the problem. General reviews concerning related problems are available [1, 2, 3], but there is scope for more experimental and analytical studies.

In the present work we report studies on spreading of non-Newtonian fluids between two glass plates, when the upper plate is loaded by a weight. We vary the weights, the fluids and the manner of loading.

We observe an interesting oscillation in the area of contact between the fluid and glass plate as a function of time. Earlier study of Newtonian fluids [3, 4] did not show such behavior. Based on the experimental results we try to explain this phenomenon using fractional calculus, which is known to be an appropriate technique to study non-Newtonian, visco-elastic materials [5, 6, 7]. Another remarkable observation is the appearance of a surface instability similar to viscous fingering. Viscous fingering under the condition of lifting, i.e. separating the plates is a well studied phenomenon [8, 9, 10]. In this case the pressure is lower within the fluid, compared to the air pressure outside, satisfying the Saffman-Taylor condition for instability [11]. However, in the present case the fingering develops during compression.
2. Materials and Methods

2.1. Materials

The fluids under study are two non-Newtonian fluids - arrowroot and potato starch gel and a Newtonian fluid ethylene glycol (GR) is also studied for comparison.

Starch granules suspended in water produce a whitish liquid. When heated, the granules of starch, which contain amylose and amylopectin, absorb water and swell up. Finally the starch grain collapses and long chained amylose molecules are leached out. The long chains join to form an amorphous mass with the water trapped inside. This is the gel phase. In the gel phase there are no granules with boundaries that scatter light, so it looks clear.

In order to get a homogenous gel of the starch in water the suspension has to be heated to temperature ($>100^\circ$C). A preliminary set of experiments was done with arrowroot starch (Indo Moulders, India) available commercially for stiffening fabrics. 2.5gm of the starch is dissolved in 100ml of distilled water and it is heated up for 20 minutes and boiled for 2 minutes to get a clear gel. A pinch of dye is added to enhance the contrast and the solution is allowed to cool. Continuous stirring is necessary so that lumps are not formed and a smooth homogenous fluid is obtained.

The second set of experiments was done on a well characterized sample of potato starch ($\left(\left(\text{C}_6\text{H}_{10}\text{O}_5\right)_m\right)$) manufactured by Lobachemie Pvt. Ltd. (Mumbai), the procedure for preparing the gel is the same above but it has to be heated for 10 minutes. During heating and boiling, some water is lost due to evaporation. The ratio water:potato starch (w/w) changes from 40:1 before boiling to 35:1 after boiling and cooling.

The Newtonian fluid that we use is ethylene glycol GR,(E.Merck, India). Here also a little food colouring is added for enhancing contrast.

2.2. Methods

A droplet of the non-Newtonian fluid is placed on a smooth glass plate using a micro-pipette. The mass of the droplet varies from 0.04 gm to 0.06 gm.

The fluid drop is compressed by two different loading processes.

(i) A load of W kg. is placed on another glass plate (identical to the bottom plate and weighing 570 gm). Then the plate and load are placed together on the drop.

(ii) The upper glass plate is first placed on the droplet. Then the weight W is placed on top of the upper plate after an interval of 2 seconds.

Each of the non-Newtonian fluids is subjected to the two loading processes described above. Ethylene glycol is compressed by the second process. The change in area of contact between the fluid and plate is video recorded from below. The area is measured using Image Pro Plus software and plotted as a function of time.

3. Experimental Observations

The strain is defined as the fractional change in area per unit area at $t = 0$.

$$\epsilon(t) = \frac{a(t) - a_0}{a_0}$$

$a(t)$ and $a_0$ being respectively the area at time $t$ and at the initial time $t = 0$. Time $t = 0$ is taken differently for the different loading processes. The results for the different sets of experiments are described below.
Figure 1. Variation in strain with time for arrowroot gel on glass, loaded by $W_1$ tp 5 kg by process (i) (black right triangle - 1 kg, red cross - 2 kg, green up triangle - 3 kg, blue square - 4 kg, magenta square - 5 kg). The inset shows the erratic variations magnified for 4 and 5 kg respectively.

3.1. Set (A) - Arrowroot gel

- Loading process (i) Here the initial time is the instant when the total load - (plate + $W$) is placed in position. The variation in strain for the arrowroot gel is shown in figure(1) for different weights $W$. The area shows erratic noisy oscillations, more prominently displayed in the magnified inset.

- Loading process (ii) Here the initial time $t = 0$ refers to the instant when the weight $W$ is placed, the upper plate already being in position. Figure(2) shows the variation in strain. Here the variation is less erratic, but all sets show that the area initially overshoots the final equilibrium value $\epsilon_\infty$, then approaches $\epsilon_\infty$ after one or two cycles of oscillation. In our experiments, the masses of the initial fluid drop for the different sets, could not be made exactly equal. This leads to some error which makes the data for 1 and 2 kg, as well as 3 and 4 kg appear very close to each other in figure(2).

This video is taken at 4 frames/sec. Though the oscillations are apparent, clearly, recording at higher speed is required. Instead of proceeding with the commercial arrowroot sample, which is not well characterized, we continued the experiments with potato starch.

3.2. Set (B) - Potato Starch gel

All the subsequent results show videos taken at 10 frames/sec.

- Loading process (i) Here again noisy variations, which may be superposed on oscillations are seen in the results (figure(3)).

- Loading process (ii) In this case, the erratic noise is much reduced and clear oscillations are observed in figure(4). The oscillations die down after a few cycles to the equilibrium value $\epsilon_\infty$. The amplitude of the oscillations increases with load $W$. The peak-to-peak differences for the first cycles for each load, were measured as: 0.13 cm$^2$ (2 kg.), 0.15 cm$^2$ (3 kg.), 0.18 cm$^2$ (4 kg.) and 0.27 cm$^2$ (5 kg.). The average frequency over the first 3 cycles was measured, but did not show a definite trend with load variation, the values ranging from
0.35 to 0.75 hz. For the load 5kg, however, all the measurements gave values close to 0.35 hz. There was a problem with the results for 1 kg. load and we have omitted them in the present paper. More careful repeated measurements will be performed in future to verify all the observations.

The experiments are repeated for reproducibility and four such data sets for $W = 5$ kg are shown in figure(5).

3.3. Set (C) - Ethylene glycol

Ethylene glycol has been studied earlier, together with other Newtonian fluids [3, 4]. We have repeated the experiments, recording the video at 10 frames/sec and show the results here(figure(6)) for comparison with the gels. Loading process (ii) is employed here. The results are very clearly different from the previous sets for the non-Newtonian fluids. Here, the area increases smoothly and saturates to the equilibrium value for all loads $W$.

The results show convincingly that these non-Newtonian fluids show an oscillatory spreading, when compressed in a Hele-Shaw cell, unlike Newtonian fluids. It is to be noted that this is not a simple stick slip behavior, where the strain (here this is equivalent to area) would always increase, but in jumps. Here for the gels, the strain, i.e the area, actually decreases after a short time interval during loading and again increases. To establish that the film does shrink and expand in an oscillatory manner, we superpose two snapshots taken at an interval of 2 seconds, and show their difference in figure(7). The weight on the upper plate is 5 kg. Here the outer boundary corresponds to an instant of time earlier than the inner. So the oscillations in strain are genuine and not due to measuremental error. Further, the corrugated appearance of the boundary, demonstrates the Saffman-Taylor like instability developed.

In the subsequent sections we suggest a visco-elastic model to explain our experiments. At present, we focus on the less noisy data for loading process (ii). Presumably, loading process (i) needs a more complicated theory, because the weights are placed on the hemispherical drop directly. So change in shape i.e. flattening of the drop as well as change in area are to be considered in this case.

3.4. Fluid Characterization

It is well known that starch solutions are non-Newtonian [12, 13]. It is interesting that the suspension in water made without heating is shear thickening [14], whereas the gel made by boiling the solution is shear thinning.

Rheological studies of the arrowroot gel and potato starch gel, were done at Central Glass
and Ceramic Research Institute (CGCRI, CSIR) by a Bohlin rotational Rheometer at 25°C temperature. No preshear was applied to the samples prior to measurement. Both gels show strongly shear thinning nature of the fluids with a yield stress. The apparent viscosity of potato starch gel is somewhat smaller than arrowroot for all strain rates.

A log-log plot of strain against shear rate shows a power law relation for both fluids over a wide range (figure(8)). An exponent 1.7 is obtained for arrowroot, while 1.5 is obtained for potato starch, as shown in the best fit power-law straight lines shown in figure(8).

The graphs indicate a non-zero yield stress, but the value of the yield stress was not measured precisely in the present set of experiments.

Figure 3. Variation in strain with time for potato starch gel on glass, loaded by W 1 tp 5 kg by process (i). The insets on the right and left show the erratic variations magnified for 4 and 5 kg respectively.

4. Mathematical Modeling
To analyze the stress-strain behavior we use a basic Kelvin-Voigt model [15, 16] of a spring and dash pot in parallel as a basic unit. The viscous behavior is represented by the dash pot and the elastic nature by the spring. The model is further generalized by taking the qth derivative of the strain, thus introducing non-Newtonian rheology through fractional calculus[5, 17]. Here q may be a fraction, for case q = 1 we have a Newtonian viscosity. The elastic term is assumed to be Hookean at present. The stress is then given by

\[ \sigma(t) = \beta \tau^q \frac{d^q \epsilon}{dt^q} + E\epsilon \]  

(2)

Here \( \epsilon \) is the strain, E the elastic modulus and \( \beta \) a parameter characterizing the effective viscosity of the non-Newtonian fluid and \( \tau \) a characteristic time of the system.

We assume a step function to represent the loading

\[ \sigma(t) = \sigma \text{ for } t \geq 0, \text{ and } \sigma(t) = 0 \text{ for } t < 0 \]
The initial condition for strain is \( \epsilon(t) = 0 \) for \( t < 0 \).

The Laplace transform of equation (2) gives

\[
\epsilon(s) = \frac{\sigma}{E} \left[ \frac{1}{s} - \frac{s^{q-1}}{s^q + E/\beta} \right]
\]

(3)

The inverse Laplace transform of equation (3) gives

\[
\epsilon(t/\tau) = \frac{\sigma}{E} \left[ 1 - ML_q \left( -\frac{E}{\beta} (t/\tau)^q \right) \right]
\]

(4)

where, \( ML(-kt) \) is the one parameter Mittag-Leffler function defined by

\[
ML_1(-kt) = e^{-kt}
\]

\[
ML_q(z) = \sum_{k=0}^{\infty} \frac{z^k}{\Gamma(qk + 1)}
\]

Visco-elastic systems typically have a ‘memory’: the strain at time \( t \) is determined by its previous loading history starting from \( t = -\infty \). The Markovian system without memory is a special case of general non-Markovian systems exhibiting correlation or anti-correlation. The general case can be treated naturally using generalized calculus methods, as follows.

One has to consider the Green’s function for a general relaxation in equation (2), so we write the homogeneous equation with RHS equal to zero. The strain built up for any relaxation, as a function of a scaled dimensionless time \( t_r \), may be treated as convolution integral of a strain variable with integral kernel \( K_q(t) \), as [6, 7]. We use henceforth this reduced dimensionless time \( t_r \), which is the time scaled by some characteristic time of the system.

\[
\frac{d}{dt_r} \epsilon(t_r) = -\int_0^{t_r} K_q(t_r - t) \epsilon(t) dt
\]

(5)

We first consider two special cases, with no memory and infinite memory.

4.1. No memory

If the memory kernel is \( K(t_r) = B_0 \delta(t_r) \), we have the above system 2 without memory [6, 7] and the Green’s function will be

\[
\epsilon(t_r) = \epsilon_0 e^{-B_0 t_r}
\]

that is the impulse response quickly decays to zero. Here \( \epsilon_0 \) is initial strain of the system at \( t_r = 0 \).

This can be derived as follows:

\[
K(t_r) = B_0 \delta(t_r)
\]

\[
\frac{d}{dt_r} \epsilon(t_r) = -\int_0^{t_r} \delta(t - t_r) \epsilon(t) dt = -B_0 \epsilon(t_r)
\]

(7)
Figure 4. Variation in area of contact for potato starch on glass, loaded by $W = 2, 3, 4$ and $5 \text{ kg}$ by process (ii). The curves are shifted along the y-axis with respect to each other for clarity. The inset shows the results for $2$ and $5 \text{ kg}$ only, without the shift. Amplitude of the oscillations increases with load.

$$
\epsilon(t_r) = \epsilon_0 e^{-B_0 t_r}
$$

(8)

The homogeneous strain relaxation equation for no-memory case is a first order Ordinary Differential Equation i.e.

$$
\frac{d}{dt_r} \epsilon(t_r) + B_0 \epsilon(t_r) = 0
$$

(9)

4.2. Infinite memory
If the memory kernel is a constant say $K_2(t_r) = B_2$, then we will have oscillatory Green’s function, which never decays to zero.

$$
\frac{d^2}{dt_r^2} \epsilon(t) = -B_2 \epsilon(t_r)
$$

(10)

$$
\epsilon(t_r) = \epsilon_0 \cos(\sqrt{B_2 t_r})
$$

(11)

4.3. Generalized case
If a generalized memory integral of the following form is taken

$$
K(t) = B_q t_q^{\frac{q-2}{2}} ; \quad 0 < q \leq 2
$$

(12)

one has

$$
\frac{d}{dt_r} \epsilon(t_r) = -\frac{1}{\alpha^q} \left[ \frac{d(1-q)}{dt_r^{1-q}} \epsilon(t_r) \right]
$$

(13)

where,

$$
\alpha^q = \left[ B_q \Gamma(q - 1) \right]^{-1}
$$

(14)
Integrating the equation (13), we have

\[ \epsilon(t_r) - \epsilon_0 = -\frac{1}{\alpha^q} \left[ \frac{d(-q)}{dt(-q)} \epsilon(t_r) \right] \]  \hspace{1cm} (15)

Differentiating this to order \( q \), we get the corresponding generalized differential equation.

\[ \frac{d^q \epsilon(t)}{dt^q} - \epsilon_0 \frac{t^{-q}}{\Gamma(1-q)} = -\alpha^{-q} \epsilon(t) \]  \hspace{1cm} (16)

using the fact that the differentintegral of order \( q \) of the constant \( \epsilon_0 \) gives \( \epsilon_0 \frac{t^{-q}}{\Gamma(1-q)} \).

This is the equation for the system with the memory index entering as fractional order \( q \) of the Fractional Differential Equation with, \( 0 < q \leq 2 \).

\( q = 1 \) corresponds to no memory and \( q = 2 \) corresponds to infinite memory with anti-correlation, or anti-persistence.

In equation (16) above, if the initial stress be \( \epsilon_0 \), assuming Heaviside’s step function as the stress input, it modifies to equation (2), for \( \alpha^{-q} \rightarrow B \).

**Figure 5.** Four separate experiments (a) - (d) performed identically (by process 2), show the reproducibility of the nature of oscillations for potato starch gel loaded by 5 kg.

The non-Newtonian fluids without oscillatory behavior will have \( 0 < q < 1 \), which leads to an equation also of fractional order, and the step-response will have monotonically increasing strain response, given by one argument Mittag-Leffler function. Its impulse response will be a function having a long tailed decay. In other words, the response will have long-range temporal correlation i.e. persistence. In equation (13) \( q = 0, 1 \) and 2 represent cases with respectively memory with complete correlation, no memory and memory with complete anti-correlation. These situations are analogous to a random walk with persistent memory, no memory and anti-persistent memory respectively.

The visco-elastic system with Newtonian viscous behavior can be modeled with a discrete ideal spring and a ideal dashpot. Whereas the more complicated case with non-Newtonian viscosity requires a different representation like a fractal chain of the ideal spring and ideal dashpot combination, or equivalently, a description using generalized calculus [5]. Our experiment clearly shows oscillatory strain and thus we infer the fractional order \( q \) of our system.
Figure 6. Variation of strain in time for ethylene glycol loaded by different $W$ by process (ii). The inset shows that the increase is monotonic even on magnification.

to lie between 1 and 2. Necessity for the use of a non-trivial memory kernel clearly demonstrates that results for strain at $t$ should depend on earlier loading history, rather than the instantaneous load at $t$.

5. Results from the Model

We now plot the strain as a function of time using equation (4). For $q = 1$, the strain increases smoothly and saturates to the value $\epsilon_\infty = \sigma/E$, $\sigma$ represents the load $W$ in our experiment. For $q < 1$, a similar behavior is observed, with a slower variation in strain. For $q > 1$ however, we see an initial increase in strain overshooting $\epsilon_\infty$ followed by oscillations before saturating to $\epsilon_\infty$. The oscillations are more pronounced as $q$ increases. These results are shown in figure(9). The amplitude depends on $q$ and of course the magnitude of the strain changes proportionately to the load $\sigma$, also affecting the amplitude of oscillation.

Considering the parameter $B = \frac{\dot{\epsilon}}{\sigma}$ to represent the relative strengths of the elastic and viscous terms in equation (2), we may see how the system responds to changes in $B$. We find that variation of $B$ changes the time period of the oscillations in strain, without affecting the amplitude. Variation of strain with $W$ and $B$ are shown in figure(10). The time period is smaller when elasticity dominates.

If we assume that the fractional change in area is equivalent to the strain in the system, the results for the starch solutions are reproduced qualitatively by the visco-elastic model with non-Newtonian rheology. Here the $q$th order derivative takes care of the non-linearity in the complex fluid. In the earlier paper [3] the Newtonian fluids were assumed incompressible and the change in film thickness was calculated from the constant volume of the fluid. Here the fluid may have a finite compressibility, so we refer only to the area which is measured directly. Determination of the exact value of $q$ for our systems requires a more detailed analysis, with more information on the rheological properties. From the present study we may say $q$ lies between approximately 1.5 and 1.8, because we observe 3 oscillation cycles. A value of $q$ less than 1.5 would give less cycles, while $q$ larger than 1.8 would give more. However, it is quite clear that $q$ is not 1, i.e. the viscous contribution to the model is not Newtonian.
Figure 7. The figure shows the difference between two outlines of the blob of potato starch gel on glass, when compressed by a 5 kg. weight. The outer contour is of a snap taken 2 seconds earlier than the inner. This shows clearly that the compressed drop shrinks before increasing again.

6. Conclusion
To conclude, this work demonstrates the interesting phenomenon of oscillatory spreading of starch solutions on glass and illustrates how the approach of generalized calculus may be used to analyze it. The qualitative agreement of the variation in strain with time from the experiments and the theory is encouraging and further exploration along these lines promises to be rewarding.

Figure 8. A double logarithmic plot of strain rate versus stress for arrowroot gel and potato starch gel, show that in both cases the fluids follow a power-law over a wide range. The straight lines are best power-law fits with exponents of 1.7 and 1.5 for arrowroot and potato starch respectively.
Figure 9. Variation in strain with time for different values of $q$ from equation (4). An oscillatory behavior is seen, which dies down to the equilibrium value.

Figure 10. Variation in strain with time for different values of $W$ and different values of $B$ from equation (4). $q = 1.7$ in all cases.

Acknowledgments
Tapati Dutta and Prof. S.P. Moulik are gratefully acknowledged for helpful discussion. The authors thank UGC, Govt. of India for supporting this work and for providing a research grant to MDC.

References
[1] Engmann J, Servais C, Burbridge A S 2005 J. Non-Newton. Fluid Mech. 132 1
[2] Bonn D, Eggers J, Mennier J, Rolley E, 2009 Rev. Mod. Phys 81 739
[3] Nag S, Dutta T, Tarañdar S, 2011 J. Colloid Int. Sci. 356 293
[4] Nag S, Dutta S, Tarañdar S, 2009 Applied Surface Science 256 353
[5] Heymans N, Bauwens J C, 1994 Rheologica Acta 33 210
[6] Das S, 2010 *Mathematico-Physics of Generalized Calculus* Limited edition, available at Jadavpur University and University of Calcutta

[7] Das S, 2007 *Functional Fractional Calculus for System Identification and Controls* Berlin: Springer-Verlag

[8] Sinha S, Dutta T and Tarafdar S, 2008 *Eur. Phys. J. E* 25 267

[9] Ben Amar M and Bonn D, 2005 *Physica D* 209, 1

[10] Poivet S, Nallet F, Gay C and Fabre P, 2003 *Europhys. Lett.* 62 244

[11] Vicsek T, 1989 *Fractal Growth Phenomena* (Singapore: World Scientific)

[12] Moorthy S N, Larsson H and Eliasson A C, 2008 *Starch/Starke* 60 233

[13] Singh J, Singh N, Saxena S K, 2002, *J. Food Eng.* 52, 9

[14] Fall A, Huang N, Bertrand F, Ovarlez G. and Bonn D., 2008 *Phys. Rev. Lett.* 100 018301

[15] Christensen R M, 2003 *Theory of Viscoelasticity, 2nd ed.* New York: Dover

[16] Bland D R, 1960 *The Theory of Linear Viscoelasticity* London: Pergamon Press

[17] Glockle W G and Nonnenmacher T F, 1991 *Macromolecules* 24 6426