The effect of different hydration media on magnesia

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Abstract
This paper discusses the rate of hydration of magnesia (CCM1 and CCM2) during the formation of magnesium hydroxide with magnesium acetate and distilled water. The influence of magnesium acetate and the reactivity of the two types of caustic calcined magnesia were studied by thermogravimetric analysis, differential scanning calorimetry, mass spectrometry, particle size detection, and pH. Also, both citric acid and acetic acid test were done to measure the reactivity of magnesium oxide powder. The results indicate that the hydration rate of both oxides in magnesium acetate system are vigorously exothermic compared to the water system. The study shows mechanistically that magnesium acetate enhanced the degree of hydration of magnesium oxide due to the presence of acetate ions and Mg2+ ions when it compared to water. Mathematical models confirm the findings.

Keywords Magnesium acetate · Hydration process · TGA · Magnesium oxide

1 Introduction
Magnesium hydroxide has become of high importance in the field of powder technology. It is used in many industrial applications as filler in the paper industry, flame retardants added to the polymer matrix, antibacterial agent and neutralizer of acidic water pollutants, water wastes and gases. Magnesium hydroxide can be used as catalyst and catalyst support in wastewater treatment [1–3] also common application uses are a source material to produce magnesium oxide [4, 5].

The formation of ultra-superfine magnesium hydroxide powder led to improvement in the mechanical properties of the material such as a high thermal stability, high fire retardant and very low toxicity [6]. The studies performed by Dong et al. [7] showed that nano-sized magnesium hydroxide can be used as an antibacterial agent as well [8]. The origin of magnesium hydroxide is either natural as a mineral or synthetically produced from seawater or brines, or from the hydration of magnesium oxide. Magnesium oxide is an inorganic compound that occurs in nature as the mineral periclase and can be also obtained through heating of the various forms of magnesium carbonate. The reactivity of magnesium oxide depends on the temperature and the duration of heat treatment of the magnesium compounds during the production of magnesium oxide. The rate of MgO hydration depends on its particle size, specific surface area and purity. Mg(OH)2 generated in water is located on the surface of MgO particles, therefore particle size is increasing [9, 10].

The reaction of magnesium oxide in water occurs according to the reaction Eq. (1)

\[
\text{MgO}(s) + \text{H}_2\text{O}(l) \rightarrow \text{Mg(OH)}_2(s)
\]
During the hydration reaction Smithson and Bakhshi [11] observed that there is a growth in the particle size of the powder. The magnesia hydration mechanism is considered similar to the one on the magnesium oxide surface where water molecules absorbed chemically forming a surface layer of magnesium hydroxide [12].

The chemical adsorption of water on metallic oxide surfaces is given by Eq. (2):

\[
\text{MgO(s) + H}_2\text{O(l)} \rightarrow \text{Mg(OH)}_2(s) \rightarrow \text{Mg(OH)} + \text{(surface)} + \text{OH}^- (aq)
\]  

(2)

Filippou et al. [13, 14] Reported that the hydration process is a process of dissolution–precipitation of magnesium oxide. The acetate ions in magnesium acetate solution enhanced the hydration process behavior of magnesium oxide. Magnesium acetate dissociation represented in Eq. (3):

\[
\text{Mg(CH}_3\text{COO)}_2(aq) \leftrightarrow 2\text{CH}_3\text{COO}^- (aq) + \text{Mg}^{2+} (aq)
\]  

(3)

Then followed by magnesia dissolution Eq. (4):

\[
\text{MgO(s) + CH}_3\text{COO}^- (aq) + \text{H}_2\text{O(l)} \leftrightarrow \text{Mg(CH}_3\text{COO)}^+ (aq) + 2\text{OH}^- (aq)
\]  

(4)

Or can react directly by acetic acid formed in solution [Eq. (5)]:

\[
\text{CH}_3\text{COO}^- (aq) + \text{H}_2\text{O(l)} \rightarrow \text{CH}_3\text{COOH(aq)}^+\text{OH}^- (aq)
\]

\[
\text{MgO(s) + CH}_3\text{COOH(aq)} \rightarrow \text{Mg(CH}_3\text{COO)}^+ (aq) + \text{OH}^- (aq)
\]  

(5)

Finally, dissociation of magnesium complexes and magnesium hydroxide precipitation is due to supersaturation as shown in Eq. (6) [15]:

\[
\text{CH}_3\text{COOMg}^+ (aq) \rightarrow \text{CH}_3\text{COO}^- (aq) + \text{Mg}^{2+} (aq)
\]

\[
\text{Mg}^{2+} (aq) + 2\text{OH}^- (aq) \rightarrow \text{Mg(OH)}_2(s)
\]  

(6)

The reactivity of caustic calcined magnesia can be measured by citric acid test or acetic acid test where the time needed for the magnesium oxide sample to neutralize the citric acid/acetic acid solution is measured. Values less than 60 s indicate a highly reactive magnesium oxide. Medium reactive magnesium oxide gives measurements between 180 and 300 s for the standardized test. A low reactivity magnesium oxide gives a value of more than 600 s [16]. The aim of this paper is to study the hydration process in a comparative manner in two different media with two different types of magnesia. The effects of thermogravimetric analysis, differential scanning calorimetry, mass spectrometry, particle size and pH on the degree of hydration were studied. The results give insight on the influence on the amount produced.

### 2 Material and methods materials

The experiments for the hydration process included two types of commercially available caustic calcined magnesia, namely CCM1 and CCM2. The hydration of two types of magnesia in different media of magnesium acetate and water is studied. The composition of the raw material is shown in Table 1.

CCM1 and CCM2 are commercial grades with approx. purity more than 96% MgO content.

| Table 1 Chemical composition of the caustic calcined magnesia |
|-----------------|-----------------|-----------------|
| Name (%)        | CCM1 Europe     | CCM2 Middle East |
| Origin          |                 |                 |
| MgO             | 96.26           | 96.75           |
| CaO             | 2.15            | 1.62            |
| SiO₂            | 1.50            | 0.87            |
| Al₂O₃           | 0.02            | 0.10            |
| LOI             | 2.15            | 0.49            |

LOI loss on ignition
2.1 Citric acid reactivity test

For the determination of the reactivity, 2.0 g of untreated MgO powder were introduced into 100 mL of 0.4 N citric acid solution under stirring and monitored measurement of pH. The time to reach a pH value of 8.6 is recorded and noted as a measure for the reactivity of the caustic magnesia.

2.2 Acetic acid reactivity test

For comparison, also the reactivity vs. acetic acid was investigated. Therefore, 5.0 g of caustic magnesia was added to 100 mL of 1.0 M acetic acid under stirring condition and the time to reach neutralization (pH = 7) was checked with a pH meter.

2.3 Particle size and pH measurements

Particle size distribution of the solid particles within the suspensions was determined using a Malvern Mastersizer 2000. Particle size measurement range: 0.02–2000 Microns with 1000 times/s scanning speed. The measurements were conducted in water and several drops of suspension were introduced into the measurement chamber until the signal to noise ratio was within the acceptable limits. The pH value was recorded at room temperature.

2.4 Transmission electron microscope (TEM)

The morphology and the particle size of the prepared samples were examined by using a transmission electron microscope JEOL JEM-1400 120 kV TEM for both types of caustic calcined magnesia “CCM1 and CCM2”. Using a hydrophobically modified copper grid sample holder.

2.5 Calorimetry

Isothermal calorimetric investigation was conducted on a TAM AIR thermometric calorimeter from TA Instruments. MgO samples were hydrated with tap water and with 0.2 M magnesium acetate solutions as hydrating agent. Each sample contained 1.6 g of solid and 6.4 g of water and magnesium acetate, respectively. Firstly, the samples were mixed with a Vortex test tube shaker for 60 s and then placed in the calorimeter for 24 h measurements of heat evolution.

2.6 Mathematical models

To predict properties of the hydration process, the model tree (MT) method is used, M5 model rules. The comparison parameters are the Mean Absolute Error (MAE), the correlation coefficient (R2) and the Root Mean Squared Error (RMSE).

2.7 Pilot scale hydration temperature and torque recording

Lab scale hydration was conducted within a closed metallic stirred vessel (diameter approximately 22 cm) with temperature and torque recording. Temperature and torque readings were taken in 10 s intervals for ~ 24 h. Stirring was accomplished by a Visco-Jet-type stirrer with diameter of 12 cm and stirring rate of 250 rpm. In each hydration process, 560 g of magnesium oxide were placed in 2240 g water or magnesium acetate (0.2 M) solution. Starting temperature for the hydration was ~ 40 °C.

2.8 Thermogravimetric analysis, differential scanning calorimetry, mass spectrum

The measurements were conducted on a “STA 449 F3 Jupiter” from Netzsch using atmospheric air at 60 mL/min and Al2O3 crucibles starting at room temperature to 700 °C with heating rate of 10 °C/min. Recordings of TGA and DSC, coupled with MS (mass spectrometer) was used to determine the thermal decomposition curves and endothermic as well as exothermic behavior together with the species that are separated from the matrix. Mass fragments recorded were m/z = 18 for water release and m/z = 44 for the release of carbon dioxide. Samples were hydrated for 30 min and 24 h, respectively, prior to measurement. For instance, 30 min samples were hydrated for 15 min under stirring, then centrifuged for 15 min
at 8500 rpm (Biofuge centrifuge) to strip off the water part and then the sample was resuspended in acetone, then again centrifuged for 15 min to obtain the solid part and finally dried at 120 °C for 2 h. 24 h samples were centrifuged for 15 min at 8500 rpm to release the water portion and resuspended in acetone prior to drying at 120 °C for 2 h.

3 Results and discussion

3.1 Reactivity test

The reactivity of caustic calcined magnesia can be measured by citric acid test or acetic acid test, where the time needed for the magnesium oxide sample to neutralize the citric acid/acetic acid solution is measured. Values less than 60 s indicate a highly reactive magnesium oxide.

Medium reactive magnesium oxide gives measurements between 180 and 300 s for the standardized test. A low reactivity magnesium oxide gives a value of more than 600 s.

3.2 Citric acid reactivity test

The citric acid test for reactivity of the CCM1 and CCM2 samples gives a reactivity value of 79.8 s and 81.6 s, respectively which corresponds to the values given for a highly reactive samples.

3.3 Acetic acid reactivity test

The acetic acid test for reactivity of the first type of the CCM1 sample gives a reactivity value of 19.5 s, which corresponds to the values given for a highly reactive sample. The vigorous reactivity of CCM2 was reflected by a reactivity value of 13 s.

3.4 Effect of particle size and pH measurement

The particle size ($D_{50}$) of CCM1 and CCM2 were measured with magnesium acetate system and with water system. As shown in Table 1 the particle size of CCM1 in water system is smaller than in magnesium acetate system (8.5 µm and 13.6 µm, respectively), while the particle size of CCM2 in water system and magnesium acetate system were 7.3 µm and 16.7 µm, respectively. The hydroxide formed from the hydration in water had surface area smaller than hydroxide obtained from magnesium acetate. Rapid hydration occurred due to large particle size and high surface area of hydroxide produced from magnesium acetate system, so the dispersion effect is better [14, 17]. The pH values in magnesium acetate system for both oxides are more acidic than in water system. The hydration degree enhanced in acidic media due to higher concentration of $H^+$ ion in the slurry that increased the solubility of MgO as shown in Table 2 [4, 5].

3.5 Transmission electron microscope (TEM)

The morphology and the particle size of the prepared samples were examined by using a transmission electron microscope JEOL JEM-1400 120 kV TEM for both types of caustic calcined magnesia “CCM1 and CCM2” using a hydrophobic modified copper grid holder.

As shown in Figs. 1, 2 very distinct and finely structured features of platelets and hexagonal sheets for the hydrated CCM samples, there is no significant different observed between the two types of caustic calcined magnesia.

| Table 2 Median particle size D50 and pH of two different CCM types hydrated for 24 h in presence and absence of magnesium acetate (MgAc) |
|---|---|---|---|
| System | $D_{50}/\mu$m | pH(median) |
| | Water | MgAc | Water | MgAc |
| CCM1 | 8.5 | 13.6 | 11.15 | 9.39 |
| CCM2 | 7.3 | 16.7 | 11.8 | 9.37 |

[Springer]
3.6 Calorimetry test

Isothermal calorimetry is a useful technique to monitor the hydration of CCM1 and CCM2 with different hydrating agents, water and magnesium acetate and their impact on the hydration process. The exothermic reaction in the previous two systems is studied over time. As shown in the Fig. 3, after magnesium acetate system is 33 mW, while in water system is 13 mW. The reaction rate decreases with increasing time. The results indicate that the reaction rate of magnesium oxides during the first few hours showed the highest peak in magnesium acetate system, no significant difference between both oxides was observed.
3.7 Lab scale hydration temperature and torque recording

As shown in Fig. 4 this result was confirmed by TGA. The degree of hydration in the magnesium acetate system was higher than that in the water system. As a function of temperature CCM released more heat in magnesium acetate system than that of water in short time range.

The exothermic reaction in magnesium acetate system reached its peak after almost 1 h at 60 °C for CCM1, while 44 °C in water. For CCM2 the exothermic reaction in magnesium acetate system reached 55 °C, while in water it was 40 °C after almost 1.5 h. The two types of magnesium oxide behave the same [12].

The study is reported that the magnesia hydration rates increased with an increase in hydration temperature. An increase in the hydration temperature accelerates the course of hydration. [14].

3.8 Mathematical models

As can be seen in Fig. 5, the Model Tree method applied on the mixtures under investigation revealed that calculated values are in good agreement with experimental data. Despite a slight deviation from the actual heat evolution
compared to the experimental data the results of the mathematical models can be used to identify the hydration paths. The use of M5 Model Rules (MT) has shown greater computational efficiency accuracy of the results [18].

### 3.9 Thermogravimetric analysis, differential scanning calorimetry, mass spectrum

Table 3 summarizes the results obtained. The hydroxide content of CCM1 and CCM2 in magnesium acetate system is significantly higher than that in water system at the same time of hydration. While after 24 h the hydroxide content of both oxides increases. TG results for both oxides (CCM1 and CCM2) show similar tendencies for the two different media [19]. The percentage of hydroxide content after 30 min in magnesium acetate and water system as shown in Table 3: 64.7%, 38.4% respectively, after 24 h the percentage of hydroxide content 85.1%, 76.3% respectively. There is acceleration in the amount of magnesium hydroxide content after 30 min until 24 h [19]. According to stoichiometric considerations, complete hydration of 100% pure material is equal to a mass loss of 30.9%. This assumption is valid only in the case that the magnesium oxide does not contain any other compound in the hydrated form.

![Fig. 6](image-url)

Thermogravimetric analysis of CCM1 in magnesium acetate system (high content of hydroxide obtained)

Table 3  Magnesium hydroxide content calculated from thermogravimetric mass loss of two different CCM types hydrated for 30 min and 24 h in presence and absence of MgAc

| System | Hydration | Mass loss/% | Mg(OH)2 content/% |
|--------|-----------|-------------|-------------------|
|        |           | Water | MgAc | Water | MgAc |
| CCM1   | 0.5       | 11.8  | 20.0 | 38.4  | 64.7 |
| CCM2   | 0.5       | 12.3  | 20.0 | 40.0  | 64.7 |
| CCM1   | 24        | 24.0  | 26.3 | 76.3  | 85.1 |
| CCM2   | 24        | 23.1  | 26.0 | 74.7  | 84.1 |
system is much higher than that in water system. While, after 24 h there is no significant difference in the amount of hydroxide produced.

Figure 9a, b showed the emission of carbon dioxide gas and water vapor in the hydration process of magnesia in magnesium acetate and water system at temperature range (250–500) °C. Fig. 9a reported that, generally the water released (m/z = 18) after 24 h showed higher ion current intensity than that after 0.5 h hydration reaction. No absence of magnesium acetate in hydroxides after 24 h. In Fig. 9b, the carbon dioxide (m/z = 44) emission is enhanced in the hydration reaction that occurred in the magnesium acetate system after 24 h indicating that the ion current signal after 24 h exceeds the signal after 0.5 h of the start of the hydration in the same system. For comparison between the different systems water and magnesium acetate the ion current intensity in magnesium acetate system emits a huge amount of carbon dioxide compared to that of water as shown in Fig. 9b.
4 Conclusion

Experimental data show increasing magnesia hydration rates in presence of magnesium acetate and with increasing temperature. In this study, there is no significant difference observed between the two types of caustic magnesia powder. On the other hand, hydration rate was influenced by the different hydrating media. From the results it seems that after 30 min hydration process is not completed because after 30 min the percentage of magnesium hydroxide accelerated. The hydration rate increased in magnesium acetate system more than that of water due to the additional acetate ions in the solution. In thermal gravimetric analysis the degree of hydration improved from hydration time of 0.5–24 h in water and magnesium acetate from 40 to 74.7% and from 65.7 to 84.1%, respectively.

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Authors' contributions FvH, RF and MM prepared the main manuscript. The experimental data were generated by RF and MM under direct supervision of FvH in the lab and with his methodology and assistance. RMH, FEK and GB are supervisors of these students. All three professors have edited and corrected versions of this manuscript. GB is a visiting professor hosted by FEK and this work has been mainly generated through long-term scientific collaboration between both institutions. GB and FvH are involved in an industrial collaboration. All authors read and approved the final manuscript.
Data availability  All data generated or analyzed during this study are included in this published article.

Declarations

Competing interests  The authors have no competing interests to declare that are relevant to the content of this article.

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