Hot corrosion studies on fully austenitic stainless steel in air oxidation and simulated waste heat incinerator environment at 600 °C, 650 °C and 700 °C

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Abstract

The purpose of the current study is to compare the hot corrosion performance of SMO 254 exposed to air oxidation and molten salt with a eutectic mixture of 40 wt% Na₂SO₄ + 40 wt% K₂SO₄ + 10 wt% NaCl + 10 wt% KCl at 600 °C, 650 °C and 700 °C under cyclic conditions for 50 h period. Kinetics of corrosion were analyzed by thermogravimetric method. By using SEM/EDS, the hot corroded specimens were investigated for surface scales and cross-sectional elemental analysis by point, line mapping methods. An accelerated rate of corrosion rate was noticed in the specimen exposed to molten salt at 700 °C, and the lowest rate of corrosion rate was observed in the specimen subjected to air oxidation at 600 °C. XRD analysis is done to analyze the corrosion products in the oxide scale.

1. Introduction

SMO 254 is widely used in the fields such as petrochemical, desalination, flue gas desulphurization, power generation, seawater piping, wastage incineration plants, and pharmaceutical plant due to its remarkable resistance to crevice and pitting corrosion [1–8].

Sanaa et al [7] studied about the susceptibility of 254 SMO alloys to Crevice Corrosion in NaCl Solution. The author reported that the oxides of Cr, Fe and Mo formed during the crevice corrosion protects and gives resistance to the alloy against the crevice.

Meguid et al [9] investigated the critical crevice potential and the critical protection potential for Alloy 254 using potentiodynamic cyclic anodic polarization technique. The author reported that SMO 254 was resistant to pitting and crevice in 4% NaCl solution till 90 °C.

Katiki et al [10] indicated that the when the salts like K₂SO₄, Na₂SO₄, KCl, and NaCl are combined, their melting point falls well below the actual melting point of the salts, resulting in salt fluxing causing destruction of the protective oxide layer triggering corrosion. The main governing factors which affect high-temperature corrosion are salt mixture composition, coverage of temperature, cyclic heating and cooling, and environmental conditions [11]. Hot corrosion is the main issue faced in the petrochemical sections, industrial waste incinerators and power plant parts such as boilers, internal combustion engines, etc [12]. Author Sidhu T S et al [13] observed that hot corrosion cause reduction in the quantity of material and reduction in the load-bearing capabilities, and finally it turns to catastrophic failure.

It has been found that from a thorough literature survey, the authors have studied the pitting and crevice corrosion on SMO 254. However, though this SMO254 is a candidate material for the high-temperature applications in the waste incinerator and power generation no detailed studies were done on hot corrosion study. The experimental goal of this research work is to investigate the behaviour of SMO 254 in hot corrosion environment in the simulated industrial waste incinerators and the power plant environment. A comparative study on the air oxidation and hot corrosion behaviour in the molten salt eutectic mixture of 40 wt%
Table 1. Chemical composition of the base metal.

|   | Fe    | Cr    | Ni    | Mo    | Mn    | Nb    | Ta    | C     | Others                  |
|---|-------|-------|-------|-------|-------|-------|-------|-------|-------------------------|
|   | 55.16 | 19.61 | 17.59 | 6.17  | 0.36  | —     | 0.01  | —     | Si-0.21; P-0.01; S-0.003; N-0.186; Cu-0.366; Co-0.07; Nb-0.0069; V-0.016; W-0.011 |

Figure 1. Thermo gravimetric analysis of air-oxidized and hot-corroded specimens. (a) Weight gain/area versus number of cycles, (b) weight gain/area² versus number of cycle.

Figure 2. Images of specimen before hot corrosion.
\( \text{Na}_2\text{SO}_4 + 40 \text{ wt\% K}_2\text{SO}_4 + 10 \text{ wt\% NaCl} + 10 \text{ wt\% KCl} \text{ at 600 °C, 650 °C and 700 °C under cyclic conditions} \) is carried out. To derive the corrosion mechanism by a detailed study using the thermogravimetric analysis, surface and cross-sectional analysis using SEM/EDS was done. Also, an attempt is made to identify the corrosion products using EDS along with the SEM/EDS elemental analysis.

| Cycle            | 600°C | 650°C | 700°C |
|------------------|-------|-------|-------|
| 1st Cycle (10 Hours) | Air oxidized |       |       |
|                  | Hot corroded |   |   |
| 2nd Cycle (20 Hours) | Air oxidized |       |       |
|                  | Hot corroded |   |   |
| 3rd Cycle (30 Hours) | Air oxidized |       |       |
|                  | Hot corroded |   |   |
| 4th Cycle (40 Hours) | Air oxidized |       |       |
|                  | Hot corroded |   |   |
| 5th Cycle (50 Hours) | Air oxidized |       |       |
|                  | Hot corroded |   |   |

**Figure 3.** Macrographic images showing the air oxidized and hot corroded samples at the end of 10, 20, 30, 40 and 50 h.

\[ \text{Na}_2\text{SO}_4 + 40 \text{ wt\% K}_2\text{SO}_4 + 10 \text{ wt\% NaCl} + 10 \text{ wt\% KCl} \text{ at 600 °C, 650 °C and 700 °C under cyclic conditions} \] is carried out. To derive the corrosion mechanism by a detailed study using the thermogravimetric analysis, surface and cross-sectional analysis using SEM/EDS was done. Also, an attempt is made to identify the corrosion products using EDS along with the SEM/EDS elemental analysis.
2. Material and experimental procedure

The material SMO 254 was purchased in the plate form from a reputed supplier. The chemical composition of SMO254 is provided in table 1. The base metal was cut in a dimension of 20 mm length 10 mm width and 6 mm thickness. To maintain the uniform surface finish to avoid the effect of surface roughness in the results the samples were polished. Standard procedure was followed using silicon carbide emery papers in the order of 240, 400, 600, 800, 1000, 1200, 1500 and 2000 grits followed by alumina slurry disc polishing. Finally, specimens were cleaned with warm water and acetone. By using a vernier caliper surface area of the specimens was measured and weight was measured by electronic balance with an accuracy of 0.01 mg. Three specimen were coated with 40 wt% Na2SO4 + 40 wt% K2SO4 + 10 wt% NaCl + 10 wt% KCl salt by using camel brush. The salts were applied to the specimen only during the initial stage. The weight of coated salt varies from 3 mg cm\(^{-2}\) to 5 mg cm\(^{-2}\). The alumina boats were annealed at a temperature of 1200 °C for 24 h. Before the hot corrosion studies, specimens were dried in the alumina boats at 200 °C for 2 h to remove moisture content. The experiments were carried out in three different tubular furnaces with the heating system precision of \((+2 \text{ °C to } -2 \text{ °C})\). Both oxidation and hot corrosion were conducted at three different temperatures 600, 650 and 700 up to 5 cycles. Each cycle involves 10 h heating followed by 20 min cooling at room temperature. After completing each cycle weight of specimens along with the boat was measured accurately to find the weight gain/loss corrosion. Proper visual surveillance was made to understand the spalling, sputtering and colour changes of the oxides.

3. Results and discussion

3.1. Kinetics of corrosion

The thermogravimetric charts of the different specimens after air oxidation and hot corrosion is given in figures 1 (a) and (b). The images of the specimens after and before air oxidation and hot corrosion are given in figures 2 and 3.

It is noted that from the macro images at the end of the first cycle (after 10 h) in the air oxidized samples the colour of specimen turned to reddish- brown at 600 and 650 °C. However, in the case of 700 °C it turned in to bluish- black. The hot corroded samples turned to black, however without any spalling of oxide scales.

At the end of 20 h spalling was observed in the specimen subjected to hot corrosion at 700 °C with the other samples in air oxidation and hot corrosion remained unaffected suggesting that the corrosion rate of the hot corroded sample is accelerating.

At the end of the 5th cycle, it is observed that specimen which is exposed at molten salt at 700 °C showed a higher rate of corrosion rate than others. The specimen exposed to air oxidation at 600 °C suffered the lowest.
The parabolic law of oxidation was followed by all the samples in both environments. The equation which is used to find the parabolic rate (Kp) is given below:[11]

$$\left( \frac{\Delta W}{A} \right)^2 = K_p t$$

Where, $\Delta W$ is the variation in the substrate weight with respect to the initial weight. ‘t’ is the time of oxidation in seconds. Here the unit area is indicated by symbol ‘A’. The Kp value of all substrates is given in table 2. Author Nakagawa K et al [14] reported that the eutectic temperature of the molten salt composition is 520 °C. From table 2, it is observed that the total weight gain is higher for specimens exposed to molten salt corrosion at 700 °C and a comparatively lower amount of weight gain for specimens exposed to air oxidation at 600 °C. The samples subjected to air oxidation received lower weight gain than the specimen exposed to the molten salt environment. Also, a higher value of Kp is obtained for the specimen exposed to molten salt corrosion at 700 °C, and the lower value of Kp is obtained for the specimen exposed to air oxidation at 600 °C.

3.2. SEM/EDAX analysis

Surface SEM images of the hot corroded specimens are provided in figures 4(a)–(f). SEM images indicate that formation of the coarse uneven surface. On close observation of the specimen, micropores are noticed on the top
surface. Also, micro-cracks are observed in figures 4(b) and (f). Volatile chlorides diffuse out the surface through these micro-cracks. Cross-sectional SEM images with point analysis, line mapping are represented in figures 5–10. EDS results imply that the scales mainly include oxides of elements such as Cr, Fe, and Ni. It can be noted that the results produced in the EDS report are closer to that of XRD data. Author Muthu S et al [15] reported that NaCl salt is vigorous at the higher temperature. Hence it can create pores in the surface also Cl in the salt react with metal substrate and form corrosive corrosion products such as ClCo2O4P, ClCrKO3, ClCu, ClCuFe24K6S, ClCu2O3, ClK, ClCu4.37Na4 and ClNa which are evaporative and porous owe to greater vapour pressure and low melting point. Arivarasu et al mentioned that these metallic chlorides with O2 create the non-protective oxide layers with porous structure [11]. The chlorine is discharged due to the sulphation of chloride enclosing deposits [16].
Also, the sodium sulphate present in the molten salt dissociates as per the following reaction.

\[
2(K, Na)Cl + SO_2 + O_2 = (K, Na)_2SO_4 + Cl_2
\]

\[
2NaCl + Fe_2O_3 + 1/2O_2 = Na_2Fe_2O_4 + Cl_2
\]

\[
NaCl + Cr_2O_3 + 5/2O_2 = 2NaCrO_4 + 2Cl_2
\]

Also, the sodium sulphate present in the molten salt dissociates as per the following reaction.

\[
Na_2SO_4 = Na_2O + SO
\]

\[
SO_3 = 1/2S_2 + 3/2O_2
\]

The above Na\(_2\)SO\(_4\) dissociation mechanism can be explained based on the lewis acid-base concept, where the initially formed component Na\(_2\)O is a basic part, and SO\(_3\) is acidic. It is clear that SO\(_3\) is in stable condition with oxygen and sulphur. So it can be concluded that when O\(_2\) partial pressure drops, the increment in the partial pressure of S\(_2\) occurs. This result improvement of the partial pressure of S\(_2\) in the molten salt, when the absorption of O\(_2\) has occurred. The S\(_2\) in the Na\(_2\)SO\(_4\) migrate into the base metal and cause degradation of the base metal by increasing the oxidation rate. Which indicates the rapid weight gain the molten salt coated specimen. Cross-sectional SEM
images with EDS results of the specimen exposed to air oxidation at 600 °C after 5 cycles is given in figure 5(a). On analyzing figure 5(a) it can be noted that a higher amount of O2 in location 1 with weight % of 38.95 and lack of oxygen creation was noted in the location 2, 3 and 4. In location 1 it is observed that lower weight % of Cr (5.01) and higher quantity of Mo with a weight % of 42.42. Cross-sectional line mapping images of the specimen exposed to air oxidation at 600 °C after 5 cycles are provided in figure 5(b). Cross-sectional SEM images with EDS results of the specimen exposed to molten salt at 600 °C after 5 cycles are given in figure 6(a). While analyzing figure 6(a) it can understand that higher concentration of O2 is observed in location 1 (weight % of 12.55) and lower weight % of O2 in location 3 (weight % of 2.61). Cross-sectional line mapping of the specimen exposed to molten salt at 600 °C after 5 cycles is provided in figure 6(b). Corrosive nature having Silicon is present in location 3 with 4.61 weight%. Cr and Mo weight % improves in both position 1 and 2. Cross-sectional

Figure 8. (a) Cross-sectional SEM images with EDS results of the specimen exposed to molten salt at 650 °C after 5 cycles. (b) Cross-sectional line mapping images of the specimen exposed to molten salt at 650 °C after 5 cycles.
SEM images with EDS results of the specimen exposed to air oxidation at 650 °C after 5 cycles is given in figure 7(a), and it can be identified that higher concentration of O₂ at position 1 with a weight % of 27.65 and lower weight of O₂ (3.80) in location 2. Also, it is witnessed that the improved rate of Cr in all positions (1–3). Nickel quantity is reduced in both positions 1 and 2, also slight increments of concentration in both 3 and 4 locations. Corrosive element sulfur is present in location 3 with a concentration of 2.27. Cross-sectional line mapping of the specimen exposed to air oxidation at 650 °C after 5 cycles is given in figure 7(b). Cross-sectional SEM images with EDS results of the specimen exposed to molten salt at 650 °C after 5 cycles is provided in figure 8(a) and while analyzing it can be observed that a higher concentration of O₂ in all positions (1–4) with a concentration of (27.58 %, 11.60%, 6.39% and 7.86%). Also, corrosive nature having element Sulphur is present in location 1 and 3 with a concentration of 0.58 % and 3.94%. A higher rate of Cr is observed in all four positions with a concentration of 24%, 27%, 22.81%, and 23.20%. Cross-sectional line mapping of the specimen exposed

Figure 9. (a) Cross-sectional SEM images with EDS results of the specimen exposed to air oxidation at 700 °C after 5 cycles. (b): Cross-sectional line mapping images of the specimen exposed to air oxidation at 700 °C after 5 cycles.
to molten salt at 650 °C after 5 cycles is given in figure 8(b). Cross-sectional SEM images with EDS results of the specimen exposed to air oxidation at 700 °C after 5 cycles is given in figure 9(a) and the EDAX image indicates that higher concentration of O₂ in position 1 with a weight % of 14.81 and reduced quantity of O₂ is observed in the location 4 with a weight % of 1.41. Also, it is noted that a slightly improved rate in the quantity of Ni in location 2, 3 and 4. Cross-sectional line mapping of the specimen exposed to air oxidation at 700 °C after 5 cycles is given in figure 9(b). Cross-sectional SEM images with EDS results of the specimen exposed to molten salt at 700 °C after 5 cycles is given in figure 10(a). Augmented rate of O₂ is observed in figure 10(a) at location 2 with a weight % of 30.96, and increment in the rate of Mo is observed in location 1 and 2 with a concentration of 9.67% and 28.85 %. Also, corrosive nature having element sodium is observed in location 2 with a weight % of 4.72. Cross-sectional line mapping of the specimen exposed to molten salt at 700 °C after 5 cycles is given in figure 10(b).

3.3. XRD analysis
By using D8 Advanced Brunker (Germany), XRD analysis was carried out. XRD pattern of the specimens is given in figure 11. The corrosion products formed during air oxidation at 600 °C are FeNi, Ni₃Si, Cr₀.₄Ni₀.₆, Ni₅P₂, CuNi, Co₀.₃Mo₀.₁, Mo₀.₉Ni₀.₉₁ and Co₀.₀₂Fe₀.₂. And the corrosion products formed during molten salt hot
corrosion at 600 °C are ClCo2O4P, ClCrKO3, ClCu, ClCuFe24K6S, ClCu2O3, ClK, ClCu4.37Na4 and ClNa. The corrosion products such as Fe0.8Mn0.2, Ni3Si, MnSi, Co0.027Fe0.2, CrNi3, CuNi, Mo0.09Ni0.91, and FeNi3 are produced after air oxidation for 50 h at 650 °C. Also, the formation of corrosion products such as ClCuFe24K6S, ClFe24K6S26, ClK, ClKO0.1Na0.9, ClNa, Cl10MO2 was observed after molten salt corrosion for 50 h at 650 °C. The corrosion products obtained after air oxidation for 50 h at 700 °C are FeNi3, Ni3Si, Co0.027Fe0.2, MnSi, Co0.02Fe0.2, CrNi3, MnS, FeNi3, Ni3Si, CrFe, Cu2S, and Fe0.8Mn0.2. This data implies that the formation of beneficial corrosion products helped to stay with reduced corrosion rate on the specimen, which was undergone hot corrosion at 600 °C while comparing with the specimen exposed at the augmented temperature level.

**Figure 11.** XRD pattern of the specimen after 50 h of cycle (a) specimen after air oxidation at 600 °C (b) specimen after molten salt corrosion at 600 °C (c) specimen after air oxidation at 650 °C (d) specimen after molten salt corrosion at 650 °C (e) specimen after air oxidation at 700 °C (f) specimen after molten salt corrosion at 700 °C.
4. Conclusion

1. It can be concluded that overall the hot corrosion is severe compared to oxidation in all the cases, and the severity of hot corrosion at 700 °C is 74.75% times than the hot corrosion at 600 °C suggesting the effect of temperature.

2. The rate of corrosion in the below-mentioned order
   Molten salt corrosion at 700 °C > air oxidation at 700 °C > molten salt corrosion at 650 °C > air oxidation at 650 °C > molten salt corrosion at 600 °C > air oxidation at 600 °C

3. SEM/EDS and XRD analysis have indicated the creation of corrosion products such as FeNi, Cr0.4Ni0.6, Ni5P2, Mo0.9Ni0.91, and CrNi3 helped to increase corrosion resistance and MnS, Cu2S caused reduction of hot corrosion resistance.

4. Formation of spinal oxides Mo0.9Ni0.91, Co1.85SiO1.15, oxide phases provide excellent resistance to corrosion of substrates.

5. Owe to the thermal stress, minor spallation has occurred in the specimen, which is exposed to molten salt corrosion and air oxidation at 700 °C.

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