Turbulent thermal diffusion in strongly stratified turbulence: theory and experiments

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Turbulent thermal diffusion is a combined effect of the temperature stratified turbulence and inertia of small particles. It causes the appearance of a non-diffusive turbulent flux of particles in the direction of the turbulent heat flux. This non-diffusive turbulent flux of particles is proportional to the product of the mean particle number density and the effective velocity of inertial particles. The theory of this effect has been previously developed only for small temperature gradients and small Stokes numbers (Phys. Rev. Lett. 76, 224, 1996). In this study a generalized theory of turbulent thermal diffusion for arbitrary temperature gradients and Stokes numbers has been developed. The laboratory experiments in the oscillating grid turbulence and in the multi-fan produced turbulence have been performed to validate the theory of turbulent thermal diffusion in strongly stratified turbulent flows. It has been shown that the ratio of the effective velocity of inertial particles to the characteristic vertical turbulent velocity for large Reynolds numbers is less than 1. The effective velocity of inertial particles as well as the effective coefficient of turbulent thermal diffusion increase with Stokes numbers reaching the maximum at small Stokes numbers and decreases for larger Stokes numbers. The effective coefficient of turbulent thermal diffusion also decreases with the mean temperature gradient. It has been demonstrated that the developed theory is in a good agreement with the results of the laboratory experiments.

I. INTRODUCTION

Turbulent transport of inertial particles has been a subject of many studies due to numerous applications in geophysics and environmental sciences, astrophysics, and various industrial applications (see, e.g., [1–13]). Different mechanisms of large-scale and small-scale clustering of inertial particles have been proposed. The large-scale clustering occurs in scales which are much larger than the integral scale of turbulence, while the small-scale clustering is observed in scales which are much smaller than the integral turbulence scale.

The large-scale clustering of inertial particles in non-stratified inhomogeneous turbulence occurs due to turbophoresis phenomenon (see, e.g., [14–19]) which is a combined effect of particle inertia and inhomogeneity of turbulence. Turbophoresis results in appearance of a non-diffusive turbulent flux of particles caused by the mean particle velocity proportional to \( V_{\text{turboph}} \propto -f(St, Re) \nabla \langle u \rangle^2 \), where \( u \) is the turbulent fluid velocity, \( St = \tau_p / \tau_\eta \) is the Stokes number, \( \tau_\eta = \tau_0 / Re^{1/2} \) is the Kolmogorov time, \( \tau_p = m_p / (3 \pi \rho d) \) is the Stokes time for the small spherical particles of the diameter \( d \) and mass \( m_p \), \( Re = \ell_0 u_0 / \nu \) is the fluid Reynolds numbers, and \( u_0 \) is the characteristic turbulent velocity at the integral scale \( \ell_0 \) of turbulent motions and \( \nu \) is the kinematic fluid viscosity. As a result of turbophoresis inertial particles are accumulated in the vicinity of the minimum of the turbulent intensity.

Another example of the large-scale clustering of inertial particles in a temperature-stratified turbulence is a phenomenon of turbulent thermal diffusion [20, 21] that is a combined effect of the stratified turbulence and inertia of small particles. This phenomenon causes the appearance of a non-diffusive turbulent flux of particles in the direction of the turbulent heat flux, i.e., opposite to the mean temperature gradient. Turbulent thermal diffusion results in accumulation of the inertial particles in the vicinity of the mean temperature minimum and leads to the formation of inhomogeneous spatial distributions of the mean particle number density. Turbulent thermal diffusion has been intensively investigated analytically [17, 20–26] using different theoretical approaches, in laboratory experiments in oscillating grid turbulence [27–29] and in the multi-fan produced turbulence [30]. This effect has also been detected in direct numerical simulations [31] and in atmospheric [32] and astrophysical turbulence [33].

In spite of intensive studies of this phenomenon, however, turbulent thermal diffusion has been investigated analytically only for small Stokes numbers and for a weak temperature stratification. On the other hand, in laboratory experiments and in direct numerical simulations these conditions are not always satisfied. The goal of the present study is to investigate the phenomenon of turbulent thermal diffusion for arbitrary temperature gradients and various Stokes numbers. The developed theory is validated against the data obtained in laboratory experiments with different sources of the turbulence production and also against the data obtained in the atmospheric measurements.

The paper is organized as follows. In Sect. II we discuss...
the physics of turbulent thermal diffusion. In Sect. III we develop the theory of turbulent thermal diffusion for arbitrary stratifications and Stokes numbers. In Sect. IV we validate this theory in the laboratory experiments in oscillating grid turbulence and in the multi-fan produced turbulence. In this section we also discuss the validation of the theory of turbulent thermal diffusion in the atmospheric observations. Conclusions are drawn in Sect. V.

II. PHYSICS OF TURBULENT THERMAL DIFFUSION

The mechanism of the phenomenon of turbulent thermal diffusion of inertial particles with material density that is much larger than the fluid density is as follows [20, 21]. The particle inertia (i.e., a centrifugal effect) results in a drift out of particles inside the turbulent eddies to the boundary regions between eddies. In these regions the fluid pressure fluctuations as well as strain rate are maximum. On the other hand, there is an outflow of inertial particles from regions with minimum fluid pressure fluctuations (maximum vorticity). In homogeneous and isotropic turbulence a drift from regions with increased concentration of particles by a turbulent flow is equiprobable in all directions, and the fluid pressure and temperature fluctuations are not correlated with the velocity fluctuations.

In a temperature-stratified turbulence with a non-zero mean temperature gradient, the fluid temperature and velocity fluctuations are correlated. Fluctuations of temperature result in the fluid pressure fluctuations. Increase of the fluid pressure fluctuations is accompanied by an accumulation of particles, so that the direction of the mean flux of particles coincides with the turbulent heat flux, toward the minimum of the mean temperature. This causes formation of large-scale inhomogeneous distributions of inertial particles.

Let us discuss the phenomenon of turbulent thermal diffusion in more detail. Motion of inertial particles with the sizes which are much smaller than the fluid viscous scale and their material density, \( \rho_p \), is much larger than the fluid density, \( \rho \), is determined by the following equation:

\[
\frac{dv}{dt} = -\frac{v - u}{\tau_p} + g, \tag{1}
\]

where \( v \) is the particle velocity, \( u \) is the fluid velocity and \( g \) is the acceleration of gravity. The solution of Eq. (1) for small Stokes time is obtained by iterations [22]:

\[
v = u - \tau_p \left[ \frac{\partial u}{\partial t} + (u \cdot \nabla) u \right] + \tau_p g + O(\text{St}^2), \tag{2}
\]

where \( W_g = \tau_p g \) is the terminal fall velocity of particles caused by the gravity field. For large Reynolds numbers, using Eq. (2) we obtain [20]:

\[
\nabla \cdot v = \nabla \cdot u + \frac{\tau_p}{\rho} \Delta p + O(\text{St}^2), \tag{3}
\]

where \( p \) is the fluid pressure. This implies that the particle velocity field is compressible even in incompressible fluid velocity field due to the inertia effects. The instantaneous number density, \( n_p(t, r) \), of inertial particles in a turbulent flow is determined by the following equation [35, 36]:

\[
\frac{\partial n_p}{\partial t} + \nabla \cdot (n_p v) = D \Delta n_p, \tag{4}
\]

where \( D \) is the coefficient of Brownian diffusion of particles. For large Peclet numbers, \( Pe \equiv \ell_0 u_0 / D \gg 1 \), when molecular diffusion of particles in Eq. (4) can be neglected, we get \( \nabla \cdot v \propto -d\ln n_p / dt \). Combining this equation with Eq. (3) we obtain that \( dn_p / dt \propto -n_p (\tau_p / \rho) \Delta p > 0 \). This implies that in the regions with maximum fluid pressure fluctuations, where \( \Delta p < 0 \), there is accumulation of inertial particles, \( dn_p / dt > 0 \). In a stratified turbulence, the fluid velocity fluctuations are correlated with the fluid temperature and pressure fluctuations due to a non-zero turbulent heat flux. This causes a nondiffusive particle turbulent flux towards the regions with the minimum of the mean fluid temperature. This phenomenon results in the large-scale particle clustering in a temperature stratified turbulence.

To investigate the formation of large-scale inhomogeneous structures in particle spatial distribution, we apply a mean-field approach and use the Reynolds averaging. In particular, we average Eq. (4) over the statistics of turbulent velocity field to obtain an equation for the mean number density of particles \( N = \langle n_p \rangle \):

\[
\frac{\partial N}{\partial t} + \nabla \cdot [NW_g + \langle n v \rangle - D \nabla N] = 0, \tag{5}
\]

where \( \langle \ldots \rangle \) denotes ensemble averaging. We assumed here for simplicity vanishing mean fluid velocity. The turbulent flux of particles, \( \langle n v \rangle \), in a temperature stratified turbulence has been determined using different analytical methods, i.e., the dimensional analysis, the quasi-linear approach, the path-integral approach, the spectral \( \tau \) approach, the functional multi-scale turbulence approach, etc (see [17, 24, 26]). The turbulent flux of particles is given by the following expression:

\[
\langle n v \rangle = N V_{\text{eff}} - D_T \nabla N, \tag{6}
\]

where \( V_{\text{eff}} \) is the effective velocity of particles and \( D_T \) is the turbulent diffusion tensor of particles. The term \( -D_T \nabla N \), in the flux of particles is caused by turbulent diffusion:

\[
D_T \nabla N \equiv \langle \tau v_i v_j \rangle \nabla_j N \approx \tau_0 \langle u_i u_j \rangle \nabla_j N. \tag{7}
\]

For large Peclet numbers, \( Pe \equiv \ell_0 u_0 / D \gg 1 \), the turbulent diffusion tensor is

\[
D_T = \tau_0 \langle u_i u_j \rangle , \tag{8}
\]

where \( \tau_0 = \ell_0 / u_0 \). To derive Eqs. (7) and (8) we took into account that for small Stokes numbers, \( \text{St} \ll 1 \), the particle velocity weakly deviates from the fluid velocity,
\( \mathbf{v} = \mathbf{u} + O(\text{St}) \). For an isotropic turbulence the Reynolds stress, \( \langle u_i u_j \rangle \), is given by \( \langle u_i u_j \rangle = (1/3) \langle u^2 \rangle \delta_{ij} \). Substituting this equation in Eq. (3), we obtain the expression for the turbulent diffusion tensor: 

\[
D_T = D_T \delta_{ij}, \quad \text{where} \quad D_T = \tau_0 \langle u^2 \rangle / 3 \text{ is the turbulent diffusion coefficient.}
\]

For small Peclet numbers and large Reynolds numbers, the turbulent diffusion coefficient is 

\[
D_T = \text{Pe} \tau_0 \langle u^2 \rangle / 12 \text{ (see, e.g., Appendix A in [32]).}
\]

The first term, \( N \mathbf{v}^{\text{eff}} \), in Eq. (4) determines the contribution to the turbulent flux of particles caused by turbulent thermal diffusion in a stratified turbulence, where the effective velocity, \( \mathbf{v}^{\text{eff}} \), of inertial particles is 

\[
\mathbf{v}^{\text{eff}} = -\langle \mathbf{u} (\nabla \cdot \mathbf{v}) \rangle = -\alpha D_T \nabla T / T. \tag{9}
\]

Here \( T \) is the mean fluid temperature and \( \alpha \) is the coefficient of the turbulent thermal diffusion. For non-inertial particles or gaseous admixtures the parameter \( \alpha = 1 \), while for inertial particles the parameter \( \alpha \) is a function of the Reynolds and Stokes numbers,

\[
\alpha = 1 + \frac{2W_\lambda \ell_P \ln(\text{Re})}{3D_T} = 1 + \frac{\text{St} \ln(\text{Re})}{\text{Re}^{1/4}} \left( \frac{\ell_{\text{eff}}}{t_0} \right) F(\text{Re}, d), \tag{10}
\]

(see [17, 22, 37]), where \( \ell_P^2 = |\nabla P| / P \) is the inverse scale of the mean fluid pressure variations, \( \ell_{\text{eff}} = 2c_s^2 \tau_0^{3/2} \rho^{1/2} \) is the effective length scale and \( c_s \) is the sound speed. When the particle diameter \( d \geq d_{cr} \), the function \( F(\text{Re}, d) \) is given by \( F(\text{Re}, d) = 1 - 3 \ln(d/d_{cr}) / \ln(\text{Re}) \), where the critical particle diameter is 

\[
d_{cr} = 2c_s^2 \tau_0 \left( \frac{d}{\ell_P} \right)^{3/2}, \quad \ell_P = \text{material density of a particle}, \quad \text{and} \quad t_0 = \text{Kolmogorov viscous scale of turbulence.}
\]

When the particle diameter \( d < d_{cr} \), the function \( F(\text{Re}, d) = 1 \).

The effective particle velocity of inertial particles is directed opposite to the mean temperature gradient as well as the mean heat flux, i.e., towards the mean temperature minimum. This causes accumulation of particles in this region. This effect is called turbulent thermal diffusion because the expression for the turbulent flux \( N \mathbf{v}^{\text{eff}} = -N \kappa_T \nabla T \) with the coefficient \( \kappa_T = \alpha D_T / T \) is similar to the formula for molecular flux caused by the molecular thermal diffusion. These two effects are of statistical nature, whereby particle turbulent flux caused by turbulent thermal diffusion arises from averaging over statistics of turbulent velocity field, while the molecular thermal diffusion flux arises from solving the Boltzmann kinetic equation.

The expression for the effective velocity of inertial particles due to turbulent thermal diffusion has been derived only for small Stokes numbers and for a weak stratification, \( \ell_0 |\nabla T| / T \ll 1 \) (see [17, 22, 24, 32]). In the next Section we develop the theory of this effect for arbitrary stratifications and Stokes numbers.

### III. Theory for Arbitrary Stratifications and Stokes Numbers

#### A. Model of a turbulant particle velocity field

In this section we discuss a model for the second moments, \( \langle v_i(k) v_j(-k) \rangle \), of a particle velocity field in a low-Mach-number homogeneous stratified turbulence with arbitrary gradients of the mean temperature and arbitrary Stokes numbers. In anelastic approximation, \( \text{div} \mathbf{u} = \lambda \cdot \mathbf{u} \), where \( \lambda = -\nabla \rho / \rho \) and \( \rho \) is the mean fluid density. The second moments, \( \langle u_i(k) u_j(-k) \rangle \), of a fluid velocity field in the anelastic approximation in a Fourier space in a homogeneous turbulence with arbitrary gradients of the mean temperature have the following form:

\[
\langle u_i(k) u_j(-k) \rangle = \frac{\langle u^2 \rangle E(k)}{8\pi(k^2 + \lambda^2)} \left[ \delta_{ij} - \frac{k_i k_j}{k^2} + \frac{i A}{k^2} \left( \lambda_i k_j - \lambda_j k_i \right) \right]. \tag{11}
\]

(see derivation of this equation in Appendix A), where \( \delta_{ij} \) is the Kronecker tensor, \( E(k) \) is the energy spectrum function, \( E(k) = (2/3) k_0^{-1} (k/k_0)^{-5/3} \) with \( k_0 \leq k \leq k_p \). This energy spectrum function corresponds to the Kolmogorov turbulence, the wave number \( k_0 = 1 / t_0 \), the wave number \( k_p = \ell_\eta^{-1} \), and \( \ell_\eta = \ell_0 \text{Re}^{-3/4} \) is the Kolmogorov (viscous) scale. Equation (11) follows also from the symmetry arguments (see, e.g., Appendix E in [38]). The first two terms in the quadratic brackets of Eq. (11) determine the incompressible, isotropic and homogeneous part of turbulence, while the other terms depend on \( \lambda \) and correspond to the anelastic approximation for arbitrary gradients of the fluid density.

Now we generalize the model (11) to the case of particle velocity field with arbitrary Stokes numbers and for turbulence with arbitrary mean temperature gradient. In particular, we assume that the second moments, \( \langle v_i(k) v_j(-k) \rangle \), of a particle velocity field in the anelastic approximation in a Fourier space in a homogeneous stratified turbulence have the following form:

\[
\langle v_i(k) v_j(-k) \rangle = \frac{\langle u^2 \rangle E(k)}{8\pi|k^2 + (B\lambda)^2|} \left[ \delta_{ij} - \frac{k_i k_j}{k^2} + \frac{i A}{k^2} \left( \lambda_i k_j - \lambda_j k_i \right) \right], \tag{12}
\]

where we introduced two free parameters, \( A \) and \( B \), that are the functions of the Reynolds and Stokes numbers to be determined in the next section.

#### B. The effective velocity of inertial particles

Using the model of a turbulant particle velocity field given by Eq. (12), we determine the effective velocity of particles,

\[
\mathbf{v}^{\text{eff}} = -\langle \mathbf{u} \text{ div} \mathbf{v} \rangle = i \int \tau(k) k_j \langle v_i(k) v_j(-k) \rangle \, dk,
\]
where \( \tau(k) = 2 \tau_0 k_0^{-2/3} \) is the scale-dependent turbulent time that corresponds to the Kolmogorov turbulence. The details of the calculations of the particle effective velocity are given in Appendix [13], and the final expression for \( V_{\text{eff}} \) has the following form:

\[
V_{\text{eff}} = -A D_T f \left[ (B \delta_r)^{2/3} \right] \lambda, \tag{14}
\]

where \( D_T = \tau_0 (v^2)/3, \lambda = |\lambda| \), and the function \( f(Y) \) is given by the following expression:

\[
f(Y) = \frac{2}{\sqrt{3} Y^2} \left[ \frac{\pi}{6} + \arctan \left( \frac{2Y - 1}{\sqrt{3}} \right) \right] - \frac{\sqrt{3}}{6} \ln \left( \frac{1 + Y^3}{1 + Y} \right). \tag{15}
\]

For small \( Y \ll 1 \), the function \( f(Y) = 1 - Y/4 + O(Y^2) \), while for large \( Y \gg 1 \), this function \( f(Y) = 4\pi/3 + O(Y^{-3}) \), and for arbitrary values of the argument \( Y \) the function \( f(Y) \) is shown in Fig. 1.

The equation of state for a perfect gas yields:

\[
\frac{\nabla \rho}{\rho} = \frac{\nabla P}{P} - \frac{\nabla T}{T}, \tag{16}
\]

where \( P \) and \( T \) are the mean fluid pressure and temperature, respectively. We assume for simplicity that the gradient of the mean fluid pressure vanishes, \( \nabla P = 0 \). In this case Eq. (14) can be rewritten in the following form:

\[
V_{\text{eff}} = -A D_T f \left[ (B \delta_r)^{2/3} \right] \frac{\nabla T}{T}, \tag{17}
\]

where the dimensionless parameter \( \delta_r \) is defined as

\[
\delta_r = \frac{\ell_0}{\sqrt{T}} \frac{\nabla T}{T}. \tag{18}
\]

It follows from Eq. (17) that for a weak stratification, \( B \delta_r \ll 1 \), the effective particle velocity is given by the following expression:

\[
V_{\text{eff}} = -A D_T \left[ 1 - \frac{1}{4} (B \delta_r)^{2/3} \right] \frac{\nabla T}{T}. \tag{19}
\]

while for a strong stratification, \( B \delta_r \gg 1 \), the effective particle velocity is given by the following formula:

\[
V_{\text{eff}} = \frac{4\pi A D_T}{3^{3/2}} (B \delta_r)^{-4/3} \frac{\nabla T}{T}. \tag{20}
\]

To determine the function \( A \), we compare Eq. (14) with Eq. (17) for the particle effective velocity, \( V_{\text{eff}} \), derived for a small Stokes number, \( St \ll 1 \), and a weak stratification, \( \delta_r \ll 1 \) (see [20–24, 37]). This comparison shows that \( A = \alpha \), where the function \( \alpha \) is determined by Eq. (10). Therefore, the expression for the effective particle velocity can be written as follows:

\[
V_{\text{eff}} = -\frac{2 D_T \alpha}{\sqrt{3} (B \delta_r)^{4/3}} \left[ \frac{\pi}{6} + \arctan \left( \frac{2(B \delta_r)^{2/3} - 1}{\sqrt{3}} \right) \right] \frac{\nabla T}{T}, \tag{21}
\]

where we used Eq. (15). To determine the second function \( B \), we assume that

\[
B = \alpha^\beta \varphi(St, Re), \tag{22}
\]

where the exponent \( \beta \) should be larger than 3/4. Indeed, when \( St \to \infty \), the effective velocity should vanish, that occurs when \( \beta > 3/4 \) [see Eq. (20)]. We will see in the next section that a good agreement of the results of laboratory experiments with the theoretical results is achieved when \( \beta = 1 \) (see Sect. [III D]). The ratio \( B/\alpha \) is a free parameter in the theory to be determined in our laboratory experiments and atmospheric observations (see Sect. [IV]).

The effective velocity \( V_{\text{eff}} \) versus the particle diameter \( d \) for conditions pertinent to our laboratory experiments and the atmospheric turbulence is shown in Fig. 2. Note that the characteristic Reynolds numbers based on the turbulent integral scale in the atmospheric turbulence vary from 10⁶ to 10⁷, and in our laboratory experiments the Reynolds numbers vary from 10³ to 10⁵. It follows from Fig. 2 that the ratio of the effective velocity of inertial particles to the characteristic vertical turbulent velocity for large Reynolds numbers is less than 1.

C. Turbulent diffusion of inertial particles

Equation (12) also allows us to determine the turbulent diffusion tensor for particles:

\[
D_{ij}^T = \int \tau(k) v_i(k) v_j(-k) \, dk. \tag{23}
\]

Using Eqs. (B4)–(B7) given in Appendix [13] we obtain:

\[
D_{ij}^T = \frac{3 D_T}{2} \left\{ \delta_{ij} \left[ 1 - \frac{2}{3} f \left( (B \delta_r)^{2/3} \right) \right] - \frac{\lambda_i \lambda_j}{\lambda^2} \left[ 1 - 2 f \left( (B \delta_r)^{2/3} \right) \right] \right\}. \tag{24}
\]
It follows from Eq. (24) that for a weak stratification, $B \delta_x \ll 1$, the turbulent diffusion tensor for particles is given by the following expression:

$$
D_{ij}^T = \frac{D_T}{2} \left[ \delta_{ij} + 3 \frac{\lambda_i \lambda_j}{\lambda^2} + \frac{1}{2} \left( \delta_{ij} - 3 \frac{\lambda_i \lambda_j}{\lambda^2} \right) (B \delta_x)^{2/3} \right],
$$

while for a strong stratification, $B \delta_x \gg 1$, it is given by the following formula:

$$
D_{ij}^T = \frac{3D_T}{2} \left[ \delta_{ij} - \frac{\lambda_i \lambda_j}{\lambda^2} + \frac{8\pi}{3^{5/2}} \left( \delta_{ij} - 3 \frac{\lambda_i \lambda_j}{\lambda^2} \right) (B \delta_x)^{-4/3} \right].
$$

Equations (24)-(26) show that turbulent diffusion tensor for particles is anisotropic for stratified turbulence.

**D. Effective coefficient of turbulent thermal diffusion**

An equation for the mean number density, $N$, of inertial particles reads:

$$
\frac{\partial N}{\partial t} + \nabla \cdot \left[ N (\mathbf{W}_g + \mathbf{V}^{\text{eff}}) - (D + D_T) \nabla N \right] = 0,
$$

(see [17] [20] [24]), where we took into account the effect of gravity for inertial particles and molecular Brownian diffusion. However, for simplicity we neglected the effects of stratification and particle inertia on the particle turbulent diffusion coefficient. The steady state solution of Eq. (27) reads:

$$
\nabla N = \frac{\mathbf{W}_g + \mathbf{V}^{\text{eff}}}{D + D_T},
$$

while for a strong stratification, $B \delta_x \gg 1$, it is given by the following expression:

$$
\frac{\alpha}{\alpha} = \frac{1}{1 + D/D_T} \left[ 1 - \frac{4}{3} (B \delta_x)^{2/3} + \frac{\tau_p g \ell_0}{\alpha \delta_x D_T} \text{sgn} (\nabla_z T) \right],
$$

and for weak stratification, $B \delta_x \ll 1$, the ratio $\alpha^{\text{eff}}/\alpha$ is given by the following formula:

$$
\frac{\alpha^{\text{eff}}}{\alpha} = \frac{1}{1 + D/D_T} \left[ 1 - \frac{4}{3} (B \delta_x)^{-4/3} + \frac{\tau_p g \ell_0}{\alpha \delta_x D_T} \text{sgn} (\nabla_z T) \right].
$$

The dependencies of the effective turbulent thermal diffusion coefficient $\alpha^{\text{eff}}$ versus the particle diameter $d$ for conditions pertinent for atmospheric turbulence and laboratory experiments are shown in Fig. 3. To isolate...
turbulent thermal diffusion from other effects hereafter we do not take into account the gravity effect. Inspection of Fig. 3 shows that for the conditions pertinent for our laboratory experiments the effective turbulent thermal diffusion coefficient $\alpha_{\text{eff}}$ increases for very small particle size $d$, reaches the maximum at small $d$ and slowly decreases for larger particle size. In the atmospheric turbulence the effective turbulent thermal diffusion coefficient $\alpha_{\text{eff}}$ behaves in a similar way, except for $\alpha_{\text{eff}}$ reaches the maximum at much larger particle size $d$.

IV. VALIDATION OF THEORY IN LABORATORY EXPERIMENTS AND ATMOSPHERIC TURBULENCE

To validate the theory of turbulent thermal diffusion in strongly stratified turbulent flows we perform laboratory experiments in different set-ups: in the oscillating grid turbulence (see, e.g., [27–29, 39–41]) and in the multi-fan produced turbulence (see, e.g., [30]). We also validate the theory of turbulent thermal diffusion against data of meteorological observations (see, e.g., [22]).

A. Particles in the oscillating grid turbulence

In this section we describe very briefly the experimental set-up and measurement facilities in the oscillating grid turbulence. The details of the experimental set-up and measurements in the oscillating grid turbulence can be found in [27, 28, 39, 41]. The experiments in stratified turbulence have been conducted in rectangular chamber with dimensions $26 \times 58 \times 26 \text{ cm}^3$ in air flow. In the experiments turbulence is produced by two oscillating vertically oriented grids with bars arranged in a square array. The grids are parallel to the side walls and positioned at a distance of two grid meshes from the chamber walls. They are operated at the same amplitude, at a random phase and at the same frequency up to 10.5 Hz.

A vertical mean temperature gradient in the turbulent air flow was formed by attaching two aluminium heat exchangers to the bottom and top walls of the test section which allowed us to form a mean temperature gradient up to 1.15 K/cm at a mean temperature of about 308 K when the frequency of the grid oscillations $f = 10.5$ Hz. To improve heat transfer in the boundary layers at the bottom and top walls we used heat exchangers with rectangular fins $0.3 \times 0.3 \times 1.5 \text{ cm}^3$. The temperature field was measured with a temperature probe equipped with a vertical array of 12 E-thermocouples in the central part of the chamber in many locations.

The velocity fields were measured using a Stereoscopic Particle Image Velocimetry (PIV) with LaVision Flow Master III system. We obtain velocity maps in the central region of the flow in the cross-section perpendicular to the grids and parallel to a front view plane. An incense smoke with sub-micron particles ($\rho_p/\rho \sim 10^3$), was used as a tracer for the PIV measurements. Smoke was produced by high temperature sublimation of solid incense grains. These particles have an approximately spherical shape and the mean diameter of 0.7 µm.

We determined the mean and the r.m.s. velocities, two-point correlation functions and an integral scale of turbulence from the measured velocity fields. Series of 520 pairs of images acquired with a frequency of 2 Hz, were stored for calculating velocity maps and for ensemble and spatial averaging of turbulence characteristics. We measured velocity in a flow domain $32.8 \times 24.8 \text{ cm}^2$ with a spatial resolution of 0.24 mm/pixel. The mean and r.m.s. velocities for every point of a velocity map were calculated by averaging over 520 independent velocity maps, and then they were spatially averaged over the central flow region. An integral scale of turbulence, $\ell$, was determined from the two-point correlation functions of the velocity field. The characteristic turbulence time in the experiments is much smaller than the time during which the velocity fields are measured (260 s). We performed experiments for different temperature difference, $\Delta T$, between the top and bottom plates.

Spatial distributions for 0.7 µm and 10 µm particles were determined by Particle Image Velocimetry (PIV) system using the effect of Mie light scattering by particles in the flow [27–29]. In order to characterize the spatial distribution of particle number density in the non-isothermal flow, the distribution of the scattered light intensity measured in the isothermal case was used for the normalization of the scattered light intensity obtained in a non-isothermal flow under the same conditions. The scattered light intensities in each experiment were also normalized by corresponding scattered light intensities averaged over the vertical coordinate.

For experimental study of turbulent thermal diffusion of inertial particles we used borosilicate hollow glass particles having an approximately spherical shape, a mean diameter of 10 µm and the material density $\rho_p \approx 1.4 \text{ g/cm}^3$. These particles have been injected in the chamber using an air jet in order to improve particle mixing and prevent from particle agglomeration. We used a custom-made acoustic feeding device for injecting particles into the flow comprising an acrylic glass chamber with a size of $9 \times 9 \times 4 \text{ cm}^3$. Two plastic slabs inside the chamber are used as air guides to achieve optimal flow with entrained particles. Particle dispensation zone (a disk of 25 mm diameter and 5 mm thickness) is located at the bottom of the chamber. A standard woofer (oval 2 × 3.5") at a frequency of 220 Hz sways a latex membrane on which particles are loaded. A cylindrical cavity is used to contain the particles on the latex membrane. The batch of particles on the membrane should roughly fill the cavity. When the membrane vibrates, particles are entrained into air. Particle feeding device has a pressurized air inlet with a bellow having a 8 mm diameter tube with standard quick release connector. The entrained particles leave the chamber with a stream of air through the outlet.
The parameters in the oscillating grid turbulence are as follows: the integral length scales in the vertical and horizontal directions are \( \ell_z = 1.4 \) cm and \( \ell_y = 2.2 \) cm; the characteristic turbulent vertical and horizontal velocities (the root mean square velocity) are \( u_z = 7.8 \) cm s\(^{-1}\) and \( u_y = 17.3 \) cm s\(^{-1}\); the characteristic turbulent times in these directions are \( \tau_z = 0.18 \) s and \( \tau_y = 0.13 \) s; the vertical and horizontal Reynolds numbers are \( \text{Re}_z \equiv \ell_z u_z / \nu = 73 \) and \( \text{Re}_y \equiv \ell_y u_y / \nu = 254 \).

In Fig. 4 we show the effective turbulent thermal diffusion coefficient \( \alpha^{\text{eff}} \) versus the parameter \( \delta_T \) for 0.7 \( \mu \)m particles with the parameter \( B/\alpha = 21 \) (solid) and for 10 \( \mu \)m particles with the parameter \( B/\alpha = 18 \) (dashed). The laboratory experiments with oscillating grid turbulence are performed with 0.7 \( \mu \)m particles (circle) and 10 \( \mu \)m particles (star) for different temperature difference \( \Delta T \) between the top and bottom heat exchangers. For comparison the function \( \alpha^{\text{eff}}(\delta_T) \) is also shown for atmospheric turbulence (dashed-dotted) for 1 \( \mu \)m particles and the parameter \( B/\alpha = 1 \).

In this section we describe very briefly the experimental set-up and measurement facilities in the multi-fan produced turbulence. The details of the experimental set-up and measurements in the multi-fan produced turbulence can be found in [30]. Experiments were conducted in a multi-fan turbulence generator that is the perspex cube box with dimensions \( 40 \times 40 \times 40 \) cm\(^3\). It includes eight fans with rotation frequency of up to 2800 rpm mounted in the corners of the box and facing the center of the box.

At the top and bottom walls of the Perspex box two heat exchangers with rectangular 0.3 \( \times \) 0.3 \( \times \) 1.5 cm\(^3\) fins were installed to improve heat transfer in the boundary layers at the bottom and top walls. The upper wall was heated up to 343 K, the bottom wall was cooled to 283 K. Two additional fans were installed at the bottom and top walls of the chamber in order to produce a large mean temperature gradient (\( \sim 0.92 \) K/cm) in the core of the flow. The temperature was measured with a high-frequency response thermocouple which was glued externally to a wire. Velocity fields and particle spatial distribution were determined using digital Particle Image Velocimetry (PIV) system (see previous subsection). The laboratory experiments with the multi-fan produced turbulence are performed with 0.7 \( \mu \)m particles for \( \Delta T = 50 \) K.

The parameters of the multi-fan produced turbulence are as follows: the integral length scales in the vertical and horizontal directions are \( \ell_z = 1.64 \) cm and \( \ell_y = 1.49 \) cm; the characteristic turbulent vertical and horizontal velocities (the root mean square velocity) are \( u_z = 80 \) cm s\(^{-1}\) and \( u_y = 71 \) cm s\(^{-1}\); the characteristic turbulent times in these directions are \( \tau_z = 2.05 \times 10^{-2} \) s and \( \tau_y = 2.1 \times 10^{-2} \) s; the vertical and horizontal Reynolds numbers are \( \text{Re}_z \equiv \ell_z u_z / \nu = 875 \) and \( \text{Re}_y \equiv \ell_y u_y / \nu = 705 \).

Unfortunately, the region of isotropic and homogeneous turbulence in the multi-fan produced turbulence is not large. The presence of 10 fans in this set-up does not allow us to perform velocity and temperature measurements, and to obtain spatial profiles of particle number density in many locations. This is a reason why we performed only several experiments in the multi-fan produced turbulence.

In Fig. 5 we show the effective turbulent thermal diffusion coefficient \( \alpha^{\text{eff}} \) versus the parameter \( \delta_T \) for 0.7 \( \mu \)m particles (solid line) and for 10 \( \mu \)m particles (dashed line) for the parameter \( B/\alpha = 18 \). The measured value of \( \alpha^{\text{eff}} \) is in an agreement with theoretical predictions.
C. Particles in the atmospheric turbulence

Tropopause in the atmosphere is a well-known region with strong gradients of temperature and also with substantial amount of aerosol particles, which remain there over long time (see, e.g., [32]). The theory of turbulent thermal diffusion for small temperature stratifications and small Stokes numbers has been previously applied in [32] to the GOMOS (Global Ozone Monitoring by Occultation of Stars) aerosol observations near the tropopause in order to explain the shape of aerosol vertical profiles with elevated concentrations located almost symmetrically with respect to temperature profile. The altitude of the GOMOS measurements is in the range from 5 km to 20 km. Analysis of data of simultaneous observations of the vertically-resolved aerosol concentrations and mean temperature in the vicinity of the tropopause shows that the aerosol concentration and temperature profiles are often anti-correlated [32]. These observations are explained using the effect of turbulent thermal diffusion, where the turbulent flux of particles is directed towards to the mean temperature minimum.

In Fig. 6 we show the effective turbulent thermal diffusion coefficient \( \alpha_{\text{eff}} \) obtained from the generalized theory versus the parameter \( \delta_T \) for 1 \( \mu \)m particles and \( B/\alpha = 1 \) (solid) and for 10 \( \mu \)m particles and different values of the parameter \( B/\alpha \): \( B/\alpha = 1 \) (dashed), \( B/\alpha = 2 \) (dashed-dotted), \( B/\alpha = 5 \) (dotted), and other parameters corresponds to the atmospheric turbulence conditions.

![Effective turbulent thermal diffusion coefficient](image)

FIG. 6. Effective turbulent thermal diffusion coefficient \( \alpha_{\text{eff}} \) versus the parameter \( \delta_T \), for 1 \( \mu \)m particles and \( B/\alpha = 1 \) (solid) and for 10 \( \mu \)m particles and different values of the parameter \( B/\alpha \): \( B/\alpha = 1 \) (dashed), \( B/\alpha = 2 \) (dashed-dotted), \( B/\alpha = 5 \) (dotted), and other parameters corresponds to the atmospheric turbulence conditions.

In the present study we have investigated turbulent thermal diffusion of small inertial particles in the temperature stratified turbulence. This effect results in the appearance of a non-diffusive turbulent flux of particles directed towards the turbulent heat flux. The theory of turbulent thermal diffusion has been previously developed only for small temperature gradients and small Stokes numbers [20–26]. In the present study we have generalized the theory of turbulent thermal diffusion for arbitrary temperature gradients and Stokes numbers. We have also performed laboratory experiments in the oscillating grid turbulence and in the multi-fan produced turbulence to validate the theory of turbulent thermal diffusion in strongly stratified turbulent flows.

Turbulent flux of inertial particles caused by turbulent thermal diffusion is proportional to the product of the effective velocity of inertial particles and the mean particle number density. We have shown that the ratio of the effective velocity of inertial particles to the characteristic vertical turbulent velocity for large Reynolds numbers is less than 1. We demonstrated that the effective velocity of inertial particles increases with the increase of the Stokes numbers, reaches the maximum at small Stokes numbers and decreases for larger Stokes numbers. In the laboratory experiments the effective velocity of inertial particles reaches the maximum at \( St = 10^{-4} \), while for the atmospheric turbulence it reaches the maximum at \( St = 0.05 \). The effective coefficient of turbulent thermal diffusion decreases with the mean temperature gradient. For very large Reynolds numbers this dependence on the mean temperature gradient is very weak. The obtained results of the laboratory experiments are in a good agreement with the theoretical predictions. However, the results obtained in our laboratory experiments clearly indicate the difficulty associated with the experimental observation of the phenomenon of turbulent thermal diffusion, i.e., this effect is quite strong only in a certain range of values of Stokes number, flow Reynolds number and temperature gradient.

V. DISCUSSION AND CONCLUSIONS

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Appendix A: Model of turbulent velocity field

The anelastic condition \( \text{div} \mathbf{u} = \mathbf{u} \cdot \lambda \) in the \( \mathbf{k} \)-space implies that \( k_1^{(i)} \langle u_i(k_1) u_j(k_2) \rangle_k = 0 \) and \( k_2^{(j)} \langle u_i(k_1) u_j(k_2) \rangle_k = 0 \), where \( k_1^{(i)} = k_i + i \lambda_i \) and \( k_2^{(j)} = -k_i + i \lambda_j \). We consider the model of the turbulent velocity field in the following form:

\[
\langle u_i(k_1) u_j(k_2) \rangle = -\langle u^2 \rangle \Phi(k) \left[ \delta_{ij} (k_1 \cdot k_2) - k_1^{(i)} k_2^{(j)} \right],
\]

(A1)

where \( k_1 \cdot k_2 = -(k^2 + \lambda^2) \) and \( k_1^{(i)} k_2^{(j)} = -(k_i k_j - i \lambda_i k_j + i \lambda_j k_i + \lambda_i \lambda_j) \), so that

\[
\langle u_i(k_1) u_j(k_2) \rangle = \langle u^2 \rangle \Phi(k) k^2 \left[ \delta_{ij} - \frac{k_i k_j}{k^2} \left( \delta_{ij} - \frac{\lambda_i \lambda_j}{\lambda^2} \right) \right].
\]

(A2)

Here \( \Phi(k) \) is unknown function to be determined below. Integrating the correlation function \( \langle u_i(k_1) u_i(k_2) \rangle \) over \( k \) we obtain

\[
\int \langle u_i(k_1) u_i(k_2) \rangle d\mathbf{k} = 2 \langle u^2 \rangle \int \Phi(k) (k^2 + \lambda^2) k^2 dk = 8 \pi \langle u^2 \rangle \int \Phi(k) (k^2 + \lambda^2) k^2 dk.
\]

(A3)

On the other hand,

\[
\int \langle u_i(k_1) u_i(k_2) \rangle d\mathbf{k} = \langle u^2 \rangle \int E(k) k^2 dk,
\]

(A4)

where \( E(k) \) is the spectrum function of the turbulent velocity field. Comparing Eqs. (A3) and (A4), we obtain the function \( \Phi(k) \):

\[
\Phi(k) = \frac{E(k)}{8 \pi (k^2 + \lambda^2)}.
\]

(A5)

Substituting this function into Eq. (A1), we obtain Eq. (11).

Appendix B: Derivation of equation for the effective velocity

In this Appendix we derive equation for the effective velocity of particles. Using Eqs. (12) and (13), we obtain:

\[
\mathbf{V}^{\text{eff}} = -\langle \tau \mathbf{v} \text{div} \mathbf{v} \rangle = i \int \tau(k) \langle v_i(k) v_j(-k) \rangle dk
\]

\[
= -2D_T A \lambda \int_0^1 \frac{\tau d\tau}{1 + a \tau^3}, \quad (B1)
\]

where \( a = (B \ell_0 \lambda)^2 \), \( \ell_0 = k_0^{-1} \) and \( \tau(k) = 2 \tau_0 \bar{\tau}(k) \). For the integration over angles in \( \mathbf{k} \)-space in Eq. (B1) we used the following integrals:

\[
\int_0^{2\pi} d\phi \int_0^\pi \sin \theta d\theta = 4\pi.
\]

(B2)

\[
\int_0^{2\pi} d\phi \int_0^\pi \sin \theta d\theta \frac{k_i k_j}{k^2} = \frac{4\pi}{3} \delta_{ij}.
\]

(B3)

Now let us calculate the integral over \( \bar{\tau} \) in Eq. (B1):

\[
f(a) = 2 \int_0^1 \frac{\tau d\tau}{1 + a \tau^3} = \frac{2}{a^{2/3}} \left[ \int_0^{a^{1/3}} X dX - \int_0^{a^{1/3}} X^3 dX \right],
\]

(B4)

where \( X = a^{1/3} \bar{\tau} \), and

\[
\int \frac{dX}{1 + X^3} = \frac{1}{6} \ln \left( \frac{1 + X)^3}{1 + X^3} \right) + \frac{1}{\sqrt{3}} \arctan \left( \frac{2X - 1}{\sqrt{3}} \right).
\]

(B5)

\[
\int \frac{dX}{1 - X + X^2} = \frac{2}{\sqrt{3}} \arctan \left( \frac{2X - 1}{\sqrt{3}} \right).
\]

(B6)

Substituting Eqs. (B5) and (B6) into Eq. (B4) we obtain the expression for the function \( f(a) \):

\[
f(a) = \frac{2}{\sqrt{3} a^{2/3}} \left[ \frac{\pi}{6} + \arctan \left( \frac{2a^{1/3} - 1}{\sqrt{3}} \right) \right] \left[ \frac{2}{\sqrt{3} a^{2/3}} \left( \frac{\pi}{6} + \arctan \left( \frac{2a^{1/3} - 1}{\sqrt{3}} \right) \right) - \frac{\sqrt{3}}{6} \ln \left( \frac{(1 + a^{1/3})^3}{1 + a} \right) \right].
\]

(B7)

Therefore, the effective velocity of particles caused by turbulent thermal diffusion is \( \mathbf{V}^{\text{eff}} = -A D_T f \left[ (B \ell_0 \lambda)^2 \right] \lambda \).
