HEXAVALENT CHROMIUM REDUCTION FROM REAL ELECTROPLATING WASTEWATER BY CHEMICAL PRECIPITATION

Bharti Verma* and Chandrajit Balomajumder

Department of Chemical Engineering, IIT Roorkee, Roorkee, India 247667

(Received May 9, 2019; Revised October 17, 2019; Accepted December 22, 2019)

ABSTRACT. The immense use of chromium in the electroplating process leads to the discharge of hexavalent chromium in its effluent. Since Cr(VI) is highly toxic, its exposure poses an acute risk of health. On the contrary, Cr(III) which is naturally occurring, is much less toxic than Cr(VI). Therefore the easiest way to deal with Cr(VI) is to reduce it into its trivalent form. Exhaustive chemical analysis was done to reduce Cr(VI) to Cr(III) by using sodium metabisulfite (Na$_2$S$_2$O$_5$) and ferrous sulfate (FeSO$_4$). And after the reduction process, precipitating agents such as (Ca(OH)$_2$), (NaOH) and a combination of the two were used to precipitate Cr(III) as hydroxides. Various parameters were varied and optimized. It was observed that the % Cr(VI) reduction increased from 88% to 99.97% when the dosage of sodium metabisulfite increased from 40 mg/L to 100 mg/L at a pH of 2. The maximum removal of 98.2% was achieved by using the combination of Ca(OH)$_2$ + NaOH at a pH of 9.

KEY WORDS: Hexavalent chromium, Electroplating, Heavy metal, Chemical precipitation, Wastewater treatment

INTRODUCTION

The enormous application of heavy metals in almost all industries has led to the presence of these toxic heavy metals in industrial effluents beyond their tolerance limit [1]. Due to their non-biodegradability, they keep accumulating in living organisms and pose a threat to their existence by causing chronic disorders [2]. The maximum concentration limits of heavy metals which are acceptable are given in Table 1. Beyond these maximum concentrations, the presence of heavy metals is highly detrimental and leads to life-threatening diseases such as cancer, asthma, brain damage, kidney damage, liver damage, and may even lead to death [3]. Of all the obnoxious heavy metals, hexavalent chromium is one such metal that is widely employed in a vast variety of industrial applications [4]. It is utilized in industries such as in electroplating, stainless steel industries, leather tanning, wood preservation processes, dye, cement and photography industries [5]. According to US EPA, Cr(VI) is recognized as one of the 17 most toxic and life-threatening elements [6]. Long term exposure to a hexavalent form of chromium causes severe damage to both flora as well as fauna. It might be a cause for diseases such as pulmonary congestions, allergic dermatitis, severe diarrhea, etc [7]. Due to the toxicity of Cr(VI), it becomes a major threat to the environment [8]. Unlike Cr(VI), Cr(III) is less mobile, stable and relatively nontoxic. Cr(VI) is almost 300 times more toxic than Cr(III) [9]. The maximum concentration limit for Cr(VI) is not more than 0.05 mg/L [10, 11]. However, the industrial wastewater contains concentrations that are beyond the permissible limit. Some of the heavy metals can be easily removed from the solution as they precipitate readily as insoluble hydroxides in a highly alkaline medium. Therefore, wastewater containing heavy metal is treated with lime, fly ash, or any other alkaline material [12]. However, Cr(VI) forms a chromate complex and does not behave as insoluble hydroxide. Therefore, it is inevitable to reduce Cr(VI) to Cr(III) which is presumably thought of as harmless in comparison to Cr(VI).
Table 1. Maximum concentration limits of various heavy metals [12].

| Heavy metal | MCL (mg/L) |
|-------------|------------|
| Lead        | 0.006      |
| Copper      | 0.25       |
| Arsenic     | 0.05       |
| Chromium    | 0.05       |
| Nickel      | 0.20       |
| Zinc        | 0.80       |

Several heavy metal treatment methods such as reduction and precipitation [13], ion exchange [14], electrolysis [15], membrane filtration [16], adsorption [17, 18], and biological treatment [19] have been suggested in literature. Unlike other technologies such as membrane technology which is a highly energy consuming process, chemical precipitation does not require any energy inputs, is easier to operate and the technology is quite cheap [20]. Besides, chemical precipitation is the most effective of all the technologies and the separation of precipitates from the water can be achieved easily by sedimentation or filtration [21, 22]. Therefore, it is the most widely employed technique for the removal of obnoxious heavy metals, i.e., Cr(VI) is reduced to Cr(III) at a lower pH and precipitation of Cr(OH)₃ at a higher pH. Some authors have reported Cr(VI) reduction by ferrous pentacarbonyl [23], hydrazine [24], Zero-valent iron [25], carboxymethyl cellulose-stabilized zero-valent iron nanoparticles [26] as well as ferric chloride-polymer combination [27]. However, the application of sodium metabisulfite and ferrous sulfate is the most economically feasible of all the reducing agents explored in the literature [28].

The present study focuses on the reduction of hexavalent chromium present in electroplating wastewater to trivalent chromium using reducing agents such as sodium metabisulfite and ferrous sulfate and then precipitating the Cr(III) hydroxides using precipitating agents such as NaOH and Ca(OH)₂.

**EXPERIMENTAL**

*Analysis of electroplating wastewater*

The electroplating effluent used in this study is taken from B.E.L, Kotdwar, Uttarakhand, India. The effluent was analyzed for its various heavy metals, cations, and anions by the use of induction coupled plasma-mass spectroscopy (ICP-MS) and ion chromatography (IC), respectively. The characterization was performed at the Institute Instrumentation Center, Indian Institute of Technology, Roorkee, India.

*Batch reduction experiment*

Batch reduction experiments were performed in 200 mL Erlenmeyer flasks in an incubator maintained at a constant temperature. The contents of the flask were thoroughly mixed by maintaining the speed constant. Sodium metabisulfite, when added to water, forms sodium bisulfite by the following equation:

\[
Na_2S_2O_3 + H_2O \xrightarrow{yields} 2NaHSO_3 \tag{1}
\]

Sodium bisulfite and ferrous sulfate reduce Cr(VI) to Cr(III) by the following equations:

\[
H_2CrO_7 + 3NaHSO_3 + 3H_2SO_4 \xrightarrow{yields} Cr_2(SO_4)_3 + 3NaHSO_4 + 4H_2O \tag{2}
\]
In the batch reduction experiment, several runs were executed on varied pH (1.5 to 3.5) to achieve the most optimum pH of the solution. For each pH, the dosage of both reducing agents was varied (500 to 1100 mg/L for ferrous sulfate and 40 to 100 mg/L for sodium metabisulfite) for the same set of conditions to evaluate the effect of dosage on the reduction process. Since Cr(VI) behaves highly oxidizing in a low pH, therefore reduction is carried out in an acidic medium. All the pH adjustments are done by using 0.05 M H$_2$SO$_4$ and 0.1 M NaOH.

**Chemical precipitation**

After pH adjustment (to around 9), the dissolved metal ions are converted to the insoluble solid phase via a chemical reaction with a precipitating agent. The mechanism behind the precipitation of heavy metal as insoluble hydroxides via chemical precipitation can be explained by the following equation:

$$M^{2+} + 2(OH)^- \leftrightarrow M(OH)_2$$  \hspace{1cm} (4)

where $M^{2+}$ is the metal ion; OH comes from the precipitant and $M(OH)_2$ represents the insoluble metal hydroxide. The precipitation reactions by using NaOH and Ca(OH)$_2$ are as follows:

$$Cr_2(SO_4)_3 + 3NaOH \rightarrow 2Cr(OH)_3 + 3Na_2SO_4$$  \hspace{1cm} (5)

$$Cr_2(SO_4)_3 + 3Ca(OH)_2 \rightarrow 2Cr(OH)_3 + 3CaSO_4$$  \hspace{1cm} (6)

**Analysis of hexavalent chromium**

The concentration of Cr(VI) was determined spectrophotometrically by the diphenylcarbazide method [29]. The wavelength was kept at around 540 nm.

**Analysis of total chromium**

The total chromium was analyzed by inductively coupled plasma mass spectroscopy at Institute Instrumentation Center, IIT Roorkee, Roorkee, India. The Cr(III) was evaluated by subtracting

\[ H_2CrO_7 + 6FeSO_4 + 6H_2SO_4 \rightarrow Cr_2(SO_4)_3 + 3Fe_2(SO_4)_3 + 7H_2O \]  \hspace{1cm} (3)

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Cr(VI) from total chromium. The schematic diagram of the whole process of reduction and precipitation is elaborated in Figure 1.

RESULTS AND DISCUSSION

Characteristics of effluent

The electroplating effluent was analyzed for its constituents by ICP-MS and the characteristics are given in Table 2. Since the chrome plating uses chromium trioxide in an acidic environment, the pH of the effluent is quite low and the concentration of hexavalent chromium is quite high.

Table 2. Characteristics of electroplating effluent.

| Parameter | Value (mg/L) |
|-----------|--------------|
| TDS       | 4300         |
| pH        | 2.02         |
| Cr(VI)    | 122          |
| Ni        | 11.3         |
| Al        | 10.4         |
| Fe        | 3            |
| Cu        | 2            |
| Nitrate   | 8.92         |
| As        | 0.2          |

Optimization of parameters

Figure 2. Effect of pH on reduction by ferrous sulfate.
pH plays a crucial role in the reduction process. As can be seen from Figures 2 and 3, the reduction is maximum at a very low pH for both cases. This can be verified from the Eh-pH diagram of chromium \[23\], that the most prevalent form of chromium at a lower pH is trivalent form. Hence, it is much easier to reduce Cr(VI) to Cr(III) at a lower pH. Also, the percent reduction increased with increasing dosages of reducing agent. This can be explained by the fact that the more reducing agent implies more possibility of collision between the substances.

After the Cr(VI) reduction, the trivalent form was precipitated in a highly alkaline medium. Figure 4, shows that the maximum removal of 98.2% was achieved by using the combination of Ca(OH)$_2$+NaOH.

Also, from Figure 5, it can be seen that the sludge generated in the case of using NaOH is quite high. This is explained by the fact that the sludge produced with NaOH is gelatinous in

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nature. However, sludge generated by using Ca(OH)$_2$ is dense. Therefore, using the combination of both the precipitating agents results in a higher removal efficiency as well less volume of sludge is generated.

**Figure 5.** Volume of sludge generated.

**CONCLUSION**

The electroplating effluent contains a huge amount of hexavalent chromium which is quite toxic. Therefore, the reduction of Cr(VI) to Cr(III) which is less harmful is the easiest thing to do at the site. The sodium metabisulfite is a better reducing agent than ferrous sulfate for the case of Cr(VI) since the amount of reducing agent required to reduce is considerably less. It was observed that 99.86% and 99.97% of Cr(VI) was reduced by using 1100 mg/L ferrous sulfate and 100 mg/L sodium metabisulfite, respectively. The maximum reduction is achieved at a pH of 2. In order to precipitate the Cr(III), precipitating agents are used in alkaline medium (pH around 9). The best combination is Ca(OH)$_2$ + NaOH as the removal efficiency is maximum (98.2%). Also the sludge generated is quite low (9.7 mL/L). Therefore, the electroplating effluent containing huge amounts of Cr(VI) can be first treated with chemical precipitation for the most effective wastewater treatment strategy. However, in spite of its advantages, chemical precipitation requires a large amount of chemicals to reduce metals to an acceptable level for discharge. Therefore, reducing agents with the fast reduction kinetics, and the precipitating agents with less sludge production should be explored for the more efficient treatment of industrial effluent.

**ACKNOWLEDGMENTS**

The authors are grateful to the Department of Chemical Engineering, Indian Institute of Technology Roorkee, India for providing a platform to conduct the series of experiments and analyze the various results. Also, a special thanks to the Ministry of Human Resources and Development to provide the necessary financial support without which this work would not have been possible.

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