Copper-on-nitride enhances the stable electrosynthesis of multi-carbon products from CO2

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Copper-based materials are promising electrocatalysts for CO2 reduction. Prior studies show that the mixture of copper (I) and copper (0) at the catalyst surface enhances multi-carbon products from CO2 reduction; however, the stable presence of copper (I) remains the subject of debate. Here we report a copper-on-copper (I) composite that stabilizes copper (I) during CO2 reduction through the use of copper nitride as an underlying copper (I) species. We synthesize a copper-on-nitride catalyst that exhibits a Faradaic efficiency of 64 ± 2% for C2+ products. We achieve a 40-fold enhancement in the ratio of C2+ to the competing CH4 compared to the case of pure copper. We further show that the copper-on-nitride catalyst performs stable CO2 reduction over 30 h. Mechanistic studies suggest that the use of copper nitride contributes to reducing the CO dimerization energy barrier—a rate-limiting step in CO2 reduction to multi-carbon products.
Electrocatalytic CO₂ reduction has been investigated extensively based on metals such as Au, Ag, Sn, Zn, In, Pd, Cu, and their associated compounds. Among these materials, Cu-based catalysts are promising for olefin and oxygenate production thanks to their moderate CO binding energies. Multi-carbon products such as ethylene (C₂H₄), ethanol (C₂H₅OH), and n-propanol (C₃H₇OH) are of great interest: C₂H₄, for example, is a valuable precursor in the manufacture of polymers. C₂H₅OH can be directly used as fuel, and C₃H₇OH has a higher mass energy density (30.94 kJ g⁻¹) than does gasoline. Furthermore, renewables-derived C₂H₅OH and C₃H₇OH can each be blended with gasoline to deliver a clean fuel.

Polycrystalline Cu metal is known to produce CH₄ with high selectivity, whereas oxide-derived Cu favors C₂H₆ products, a fact attributed to the effects of grain boundaries. Certain prior computational studies have suggested that the Cu⁺/Cu²⁺ mixture synergistically promotes CO₂ reduction to C₂ products due to CO₂ activation and C₂O dimerization. Experimentally, however, the stable presence of the active Cu⁰ species during CO₂ reduction remains the subject of debate.

A Cu⁰–Cu²⁺ core–shell structured catalyst offers an architecture wherein stable Cu⁰ deposited on top of a Cu²⁺ support protects from further reduction. Recently, core–shell catalysts have been widely investigated in electrocatalysis and have achieved significantly improved activity and kinetics. The core–support interactions modify the electronic structure of the surface catalyst, influencing the chemisorption of the intermediates in the electrocatalytic reaction. Copper (I) oxide (Cu₂O), which has been mostly used as a precursor to Cu-based CO₂ reduction catalysts, is a candidate as a Cu⁺ support; however, Cu⁺ from Cu₂O is unstable under CO₂ reduction conditions. Previous reports suggest that transition metal nitrides can be employed not only as a stable catalytic active species, but also as supports.

Here we sought therefore to investigate whether copper (I) nitride (Cu₃N) could be used as Cu⁺ support during CO₂ reduction. We hypothesize that the Cu₃N support affects the electronic structure and oxidation state of the surface Cu, decreasing the energy barrier associated with CO₂ dimerization during CO₂ reduction. This, together with the prolonged presence of Cu⁺ over time, could allow for the realization of increased-stability C₂⁺/CO₂ electrocatalysis systems under CO₂ reduction conditions.

**Results**

**Synthesis and structural characterization.** In order to challenge our hypothesis, we set out to synthesize Cu deposited on Cu₃N (Cu-on-Cu₃N) catalyst as depicted in Fig. 1a. We first synthesized Cu₃N nanocrystals capped with long-chain octadecylamine (ODA) ligands. We then performed a ligand exchange using short-chain azide (N₃⁻) to replace the ODA. An outer oxide was formed at the surface of Cu₃N nanocrystals by exposing samples to ambient air during the ligand exchange process. These nanocrystals were then used in an initial electroreduction process: we swept the cyclic voltammetry (CV) curve from 0 to −1.75 V vs. RHE to obtain the active Cu-on-Cu₃N catalyst.

To investigate surface electronic properties, we conducted X-ray photoelectron spectroscopy (XPS) measurements of the samples (Fig. 1b). In the case of the Cu₃N nanocrystals capped with ODA (Fig. 1b–i), the spectra of Cu 2p and Auger Cu LMM confirm a preponderance of Cu⁺. The sharp peak of N at a binding energy of 399 eV is consistent with that of the metal nitrides. Furthermore, X-ray diffraction (XRD) attests to the formation of Cu₃N nanocrystals (Supplementary Fig. 1).

Implementing the ligand exchange (Fig. 1b–ii and Supplementary Fig. 2) led to a different Cu composition compared to that before ligand exchange. A mixture of Cu²⁺ and Cu⁺ are present as observed in Cu 2p and LMM spectra, which suggests that copper (II) oxide (CuO) is formed in ambient air during the Cu₃N ligand exchange. The new peak in the N 1s spectrum located at 403.1 eV aligns with that of the N₃⁻ group in the ligand at the nanocrystal surface. When taken together with Fourier-transform infrared (FTIR) spectra (Supplementary Fig. 3), these findings reveal that the ODA organic ligands are completely replaced by the N₃⁻ short ligands. In addition, the Cu 2p peak areas indicate that the content of Cu³⁺ is significantly higher relative to the Cu⁺: we propose that CuO exists at the surface and substantially encompasses the Cu₃N. As shown in the O 1s spectrum (Supplementary Fig. 4), the dominant peak at 513.3 eV was assigned to O species in the surface CuO on the sample.

After initial reduction (Fig. 1b–iii), the Cu spectra show the presence of both Cu²⁺ and Cu⁰, which indicates that the surface of the catalyst was reduced to Cu. The N 1s peak at 399 eV remains after reduction, indicating that the Cu₃N phase is intact. The disappearance of the N peak at 403.1 eV, which is the characteristic of the N₃⁻ ligands, can be ascribed to the weak electrostatic interaction between the ligands and the surface of the Cu₃N nanocrystals when a potential was applied.

We used transmission electron microscopy (TEM) to investigate further the structure of the catalyst (Supplementary Fig. 5). Before ligand exchange, Cu₃N nanocrystals have an average diameter of 30 nm. After ligand exchange, a reduced spacing between the nanocrystals is observed, similar to the case of quantum dot ligand exchanges.

The local atomic-scale elemental composition on individual Cu-on-Cu₃N nanoparticle was further examined (Fig. 2a, b). From high-resolution transmission electron microscopy with electron energy loss spectroscopy (HRTEM-EELS, Fig. 2c), we observed that Cu was distributed across the volume of each nanoparticle; while N was concentrated in the core and was notably lower at the surface. The catalyst surface exhibited indications of surface reconstruction following operation under reducing conditions. Our analysis of HRTEM-EELS data indicates a = 3 nm surface Cu layer on top of Cu₃N (Supplementary Fig. 6).

We further investigated the distribution of N using EELS spectra. In a given nanoparticle, looking at two different positions (Fig. 2d), we found that for point A (inner), a strong absorption feature starting from 401 eV was obtained, consistent with the N K-shell absorption edge. No obvious absorption signal was observed for point B (surface), indicating no N at the surface. These observations indicate a Cu-on-Cu₃N structure.

We synthesized Cu deposited on Cu₂O (Cu-on-Cu₂O) and pure Cu catalysts as control samples using a process similar to the synthesis of the Cu-on-Cu₃N catalyst. XRD patterns confirm the formation of Cu-on-Cu₂O and pure Cu after electroreduction (Supplementary Fig. 7a–c). Their morphology and size are similar to those of the Cu-on-Cu₃N catalyst (Supplementary Fig. 7b–d). Double-layer capacitance measurements yielded electrochemical roughness factors of 9.7, 8.0, and 9.3 for the Cu-on-Cu₃N, Cu-on-Cu₂O, and Cu catalysts, respectively, indicating similar surface: geometric area ratios (Supplementary Fig. 8 and Supplementary Table 1).

We also obtained valence band spectra (VBS) to examine differences in the valence electronic structure between the Cu and the composite (Supplementary Fig. 9). Comparing with the case of pure Cu, we found that the Fermi-level ($E_F$) shifted toward the VB₃⁺ by 0.33 eV for Cu-on-Cu₃N and 0.08 eV for Cu-on-Cu₂O, respectively, indicating that the core-level Cu₃N and Cu₂O supports have an effect on the electronic structure of the surface Cu.
Spectroscopic characterization. To investigate the structure and chemical state of the active catalysts with time evolution under CO$_2$ reduction, we obtained in situ X-ray absorption spectra (XAS) of the three catalysts at $-0.95$ V vs. RHE during CO$_2$ reduction.

As depicted in Fig. 3a, b, the Cu K-edge XAS spectrum of the as-prepared Cu-on-Cu$_3$N catalyst presents an absorption edge between Cu (8979 eV) and Cu$_2$N (8980.5 eV)—and in particular exhibits a prominent shoulder at 8980.0 eV. Over the course of CO$_2$ reduction, both Cu and Cu$_3$N features are still present, with a shoulder energy at 8979.4 eV after 2 h. In contrast, the Cu-on-Cu$_2$O catalyst shows a prominent metallic Cu feature after 1 h (Supplementary Fig. 10a). Pure Cu presents a metallic Cu feature under CO$_2$ reduction (Supplementary Fig. 10b).

To gain more insight into the role of the Cu$^{2+}$ support, we acquired in situ Cu K-edge spectra of Cu-on-Cu$_3$N and Cu-on-Cu$_2$O catalysts following 30 min under CO$_2$ reduction (Fig. 3c).

**Fig. 1** Electro catalyst design and the corresponding XPS characterization. a Schematic of preparing the Cu-on-Cu$_3$N catalyst. b XPS spectra of Cu 2p, N 1s, and Auger Cu LMM of the Cu$_3$N nanocrystals with long organic ODA (i), the Cu$_3$N nanocrystals with an oxide layer after N$_3^-$ ligand exchange (ii), and the Cu-on-Cu$_3$N composite after initial electroreduction (iii).

**Fig. 2** TEM characterization of the Cu-on-Cu$_3$N catalyst. a, b HADDF-STEM images. c STEM-EELS Cu and N Element mapping of one individual particle in b. d, EEL spectra of element N K-edge circled as point A and point B in b. The scale bars are 50 nm in a, and 10 nm in b and c.
We found that the absorption edges of the two catalysts are between Cu$^+$ and Cu$^0$, indicating the presence of a mixture during the reaction. However, the absorption edge of Cu-on-Cu$_2$O was at a lower energy than that of Cu-on-Cu$_3$N, with energies at 8979.4 eV and 8979.8 eV, respectively. We also calculated the ratio of Cu oxidation states as function of the reaction time (Fig. 3d). The Cu-on-Cu$_3$N catalyst shows that the structure becomes stable with Cu$_3$N and Cu after the initial 60 min, while Cu-on-Cu$_2$O only presents the Cu component after 1 h. This observation indicates suppression of the partial reduction of the catalyst when we use the Cu$_3$N support.

We sought a method to probe with greater surface specificity catalyst as function of reaction time. We acquired angle-resolved XPS (ARXPS) at a 20° emission angle relative to the sample normal (Supplementary Fig. 11a). The detection depth is below 2 nm. Cu LMM spectra (Supplementary Fig. 11b–f, left column) indicate the presence of Cu$^+$ and Cu$^0$, and the N 1 s spectra (Supplementary Fig. 11 b–f, right column) are consistent with the spectrum of metal nitride, indicating the presence of Cu$_3$N in the first ~2 nm of the surface over the course of CO$_2$ reduction. In the initial 60 min, Cu$^0$ content increased and Cu$_3$N content decreased; thereafter, such as following a 2-h reaction, the catalyst gradually reached a stable surface composition. This result agrees with the observed in situ XAS data (Fig. 3d).

Both in situ XAS and ex situ ARXPS indicate the presence of Cu$^+$ following CO$_2$ reduction. Further, the N signal suggests the presence of Cu$_3$N, and STEM-EELS mapping (Supplementary Fig. 6) shows evidence of Cu$_3$N in the subsurface layer following CO$_2$ reduction. Nevertheless, we point out also that XAS has a bulk penetration depth; and that air-sensitive Cu complicates the interpretation of the ARXPS studies herein. For these reasons, direct and unambiguous confirmation of the presence of Cu$^+$ at the surface of the catalyst remains an ongoing opportunity for further advances in the field of Cu-based electrocatalysis and model development.

**CO$_2$ electroreduction performance.** To verify the effect of the Cu$^+$ support on the surface catalyst, we carried out CO$_2$ reduction using the Cu-on-Cu$_3$N, Cu-on-Cu$_2$O, and pure Cu catalysts, respectively. To analyze the selectivity toward various products with different applied potentials, we performed stepped-potential electrolysis between $-0.55$ and $-1.45$ V vs RHE (with $iR$ correction in Supplementary Fig. 12).

Cu-on-Cu$_3$N gives the highest C$_2$+ production among the three catalysts (Fig. 4a, b). When the applied potential is less negative than $-0.65$ V vs RHE, CH$_4$, and HCOOH are the main products; whereas, when we sweep toward more strongly negative potentials, we obtain production of reduced C$_2$+ species, such as C$_2$H$_4$, C$_2$H$_5$OH, and C$_3$H$_7$OH. This indicates CO dimerization beyond the potential of $-0.65$ V vs. RHE (with $iR$ correction in Supplementary Fig. 12).

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The Cu-on-Cu$_3$N catalyst achieves a 6.3-fold enhancement in the ratio of C$_2$+ to CH$_4$ compared to Cu-on-Cu$_2$O; and a 40-fold

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**Fig. 3** In situ characterization of the structure and chemical state for the catalysts during CO$_2$ reduction. **a** Cu K-edge XAS spectra of the Cu-on-Cu$_3$N catalyst as function of reaction time at $-0.95$ V vs RHE. **b** The first derivatives of the spectra in a. c In situ Cu K-edge spectra during the initial 30 min on the catalysts: Cu-on-Cu$_3$N (green) and Cu-on-Cu$_2$O (orange). Spectra of Cu (red) and Cu$_3$N (yellow) are also listed as references. d Ratio of Cu$^+$ relative to the reaction time at $-0.95$ V vs RHE.
Cu species possess a polycrystalline structure (Supplementary Fig. 13). The Cu-on-Cu2O catalyst shows a suppression in methane selectivity, which can be attributed to increased local pH. Comparing Cu-on-Cu2O and pure Cu catalysts, respectively. Compared to pure Cu, Cu-on-Cu2O catalysts display a suppression in methane selectivity, which can be attributed to increased local pH. Comparing Cu-on-Cu2O and Cu-on-Cu3N catalysts, the geometric current densities are similar in the subsurface layer during the initial reduction (Supplementary Fig. 16), which indicates a nearly identical consumption rate of local protons during CO2 reduction. We propose therefore that differences in local pH do not account for the higher C2+ selectivity for Cu-on-Cu3N relative to Cu-on-Cu2O.

We also considered surface defects as another possible contributing mechanism. For the Cu-on-Cu2O catalyst, we believe that surface defects—grain boundaries—may influence the selectivity toward C2+ in the case of the oxide-derived process. For the Cu-on-Cu3N catalyst, surface defects can also affect the C2+ selectivity. However, compared with Cu-on-Cu2O, which was quickly derived to Cu (Fig. 3d), the Cu-on-Cu3N catalyst retained a higher C2+ selectivity under CO2 reduction. We offer that suppressed reduction of the Cu3N support thus plays a significant part in the high selectivity over the course of CO2 reduction.

Single-crystal studies have also shown that the exposed Cu facets affect selectivity45-47. In this work, we synthesized three catalysts using an initial electroreduction of the surface oxidation layer using a negative cyclic voltammetry (CV) scan. During this process, the Cu species possess a polycrystalline structure (Supplementary Fig. 17). These structures do not exhibit the specific facet orientation. Therefore, we would not expect that these would contribute in a quantitatively significant way to increase C2+ selectivity.

Taking these findings together with those from XPS (including ARXPS and VBS), in situ XAS, and HRTEM-EELS, we propose that the Cu2+ support may play a role in selectivity toward C2+. Due to the change of surface structure with time evolution, the surface Cu layer is no longer uniform and some of Cu2+ may reside in the subsurface layer during the initial reduction (Supplementary Fig. 6), favouring selectivity for C2+. Cu3N as the support stabilizes the Cu+ to a greater degree than does Cu2O during CO2 reduction (Fig. 3d), leading to heightened C2+ production.

Discussion

Recent studies have suggested that the CO2 reduction performance of oxide-derived Cu catalysts can be ascribed to local pH and to derived surface defects19,21,22. Compared to pure Cu, Cu-on-Cu2O catalysts display a suppression in methane selectivity, which can be attributed to increased local pH. Comparing Cu-on-Cu2O and Cu-on-Cu3N catalysts, the geometric current densities are similar (Supplementary Fig. 16), which indicates a nearly identical consumption rate of local protons during CO2 reduction. We propose therefore that differences in local pH do not account for the higher C2+ selectivity for Cu-on-Cu3N relative to Cu-on-Cu2O.

To further compare the CO2 reduction activity of the three samples, we obtained C2+ partial current densities at a variety of potentials between −0.75 and −1.45 V vs RHE (Fig. 4c). The Cu-on-Cu3N catalyst exhibits a higher C2+ partial current density relative to Cu-on-Cu2O and pure Cu across the entire potential window, with a maximum 14 mA cm−2 at −0.95 V vs RHE, 2.2x and 4.4x higher than Cu-on-Cu2O and pure Cu catalysts, respectively.

To test the operational stability of the catalysts, we carried out CO2 reduction over an extended period of time. The Cu-on-Cu3N catalyst exhibits relatively stable Faradaic efficiency over pure Cu (Fig. 4b). CH4 production is thus strongly suppressed for the catalysts that use Cu2O and Cu3N support compared with pure Cu (Supplementary Fig. 13b–c and Supplementary Tables 3–4).

We also considered surface defects as another possible contributing mechanism. For the Cu-on-Cu2O catalyst, we believe that surface defects—grain boundaries—may influence the selectivity toward C2+ in the case of the oxide-derived process. For the Cu-on-Cu3N catalyst, surface defects can also affect the C2+ selectivity. However, compared with Cu-on-Cu2O, which was quickly derived to Cu (Fig. 3d), the Cu-on-Cu3N catalyst retained a higher C2+ selectivity under CO2 reduction. We offer that suppressed reduction of the Cu3N support thus plays a significant part in the high selectivity over the course of CO2 reduction.

Fig. 4 CO2 electroreduction performance of the designed catalysts. a Faradaic efficiency of the C2+ distribution on Cu-on-Cu3N at different potentials. b Comparison of faradaic efficiency for C2+ and the ratio of C2+ to CH4 at −0.95 V vs RHE on Cu, Cu-on-Cu2O, and Cu-on-Cu3N. c C2+ partial current density at different potentials on the three catalysts. d Stability test of C2+ selectivity on the three catalysts. Experiments from a to d were performed in duplicates and the results are shown as mean ± standard deviation.
To understand the role of Cu\(^+\) support in Cu\(^0\)-on-Cu\(^+\) composite catalyst for CO\(_2\) reduction, we performed density functional theory (DFT) computations to calculate the oxidation state of the surface Cu in the models: Cu, Cu\(_3\)N, Cu\(_2\)O, Cu-on-Cu\(_3\)N, and Cu-on-Cu\(_2\)O (Supplementary Figs. 18–22). Bader charge analyses show that both CuO and Cu\(_2\)O as Cu\(^+\) supports modulate the partial oxidation state of the surface copper layer (Supplementary Table 5), with +0.03 extra charge induced by Cu\(_2\)O support and +0.25 by Cu\(_3\)N support on (100) facet, respectively, different from that of pure Cu (0), pure Cu\(_2\)O (+0.26), and pure Cu\(_3\)N (+0.47) on (100) facet. This modulated partial oxidation state enables Cu-on-Cu\(_3\)N to achieve the lowest CO dimerization barrier energy (0.884 eV) among all models (Supplementary Figs. 23–24 and Supplementary Table 5), thereby indicating promise as a candidate for C\(_2\)\_ production. To evaluate further the selectivity of these catalysts for C\(_2\)\_ products compared to the competing C\(_1\) products, we also calculated the energy barriers for CO protonation (Supplementary Methods). The results reveal that the energy barrier for the C\(_1\) pathway for Cu-on-Cu\(_3\)N (0.933 eV) is higher than that of Cu-on-Cu\(_2\)O (0.749 eV) and pure Cu (0.721 eV) on (100) facets (Supplementary Table 5).

Since, the stability of the sublayer Cu\(^+\) is important, we studied the diffusion free energy barrier for nitrogen and oxygen from their original positions in the Cu\(_3\)N and Cu\(_2\)O structures, respectively, to the surface of Cu-on-Cu\(_3\)N and Cu-on-Cu\(_2\)O with 4 Cu top layers. Although there is a large energy barrier (>2 eV) for both O and N to leave their original position, there is no more diffusion barrier for O from the first layer to the surface (Supplementary Figs. 25–26 and Supplementary Table 6). However, for N we observe another energy barrier (~1 eV) to diffuse to the surface (Supplementary Fig. 27 and Supplementary Table 6). This agrees with our observations throughout that N in the sublayer is more stable than O.

In summary, the present work introduces a Cu-based catalyst that enables metallic Cu-on-Cu\(_3\)N to promote the production of C\(_2\)\_ species. Cu\(_3\)N was chosen as the inner support to modify the electronic structure of the surface metal, affecting thereby the adsorption and dimerization of intermediate CO properly in the CO\(_2\) reduction. Together with the suppressed reduction of Cu\(^+\) using Cu\(_3\)N as the support, we were able to achieve higher selectivity for C\(_2\)\_ formation using Cu-on-Cu\(_3\)N compared to the case of Cu-on-Cu\(_2\)O and pure Cu.

### Methods

#### Synthesis of Cu\(_3\)N nanocrystals

Quantity of 0.15 g of Cu(NO\(_3\))\(_2\)-3H\(_2\)O and 4.3 g of 1-octadecylamine (ODA) was dissolved in 15 mL of 1-octadecene. The solution was degassed for 10 min at 150 °C. The temperature was then raised to 240 °C and kept for another 10 min. When it cooled down to room temperature, the product was collected by centrifugation, washed with hexane/acetone (1/4) three times, and finally dispersed in hexane.

#### Transformation of Cu\(_3\)N to CuO-on-Cu\(_3\)N

We used the ligand exchange method in ambient air to achieve the transformation of Cu\(_3\)N to CuO-on-Cu\(_3\)N. Ten milligrams of Cu\(_3\)N nanocrystals with organic ligands was dissolved in 1 mL of hexane (10 mg L\(^{-1}\)), while 10 mg of sodium azide (Na\(_3\)N) was dissolved in 1 mL of NMF (10 mg L\(^{-1}\)). The two solutions were then mixed and stirred overnight. The nanocrystals gradually transferred to NMF. The bottom phase was extracted and washed with hexane three times. The N\(_3\)\_–capped Cu\(_3\)N nanocrystals were then precipitated out using chloroform as the anti-solvent. The precipitate was dried in air and then stored. In the ligand exchange process, we deliberately exposed the materials to ambient air to introduce an oxide layer at the surface of Cu\(_3\)N nanocrystals.

#### Transformation of Cu-on-Cu\(_3\)N to Cu-on-Cu\(_2\)O

We conducted the initial electroreduction for the Cu-on-Cu\(_3\)N sample by sweeping the cyclic voltammetry (CV) curve from 0 to −1.75 V vs RHE at a rate of 50 mV s\(^{-1}\), yielding the Cu-on-Cu\(_3\)N catalyst.

#### Synthesis of control Cu-on-Cu\(_3\)O and pure Cu catalysts

Cu\(_2\)O and Cu nanocrystals were synthesized using 0.5 g of Cu(NO\(_3\))\(_2\)-3H\(_2\)O and 0.05 g of Cu(NO\(_3\))\(_2\)-3H\(_2\)O instead, respectively, while keeping other experimental conditions the same as in the synthesis of Cu\(_3\)N nanocrystals. The ligand exchange and initial electroreduction processes were the same as in the case of the Cu-on-Cu\(_3\)N catalyst.

#### Working electrode preparation

Ten milligrams of the catalyst was dispersed in 1 mL of methanol, including with 20 µL of Nafion solution (anhydrous, 5 wt %) by sonicating for 30 min. Twenty microliter of the homogeneous solution was then loaded on a glassy carbon electrode. The geometric surface area was 0.19 cm\(^2\). The electrode was dried in ambient air for the subsequent CO\(_2\) electroreduction test.

#### Electrochemical measurement

Electrochemical tests were performed in a two-compartment H-cell. A proton exchange membrane (Nafion 117) was used. The electrolyte was 30 mL of 0.1 M KHCO\(_3\) solution saturated with CO\(_2\) gas in the cathode part for at least 30 min prior to the CO\(_2\) reduction test. Platinum was used as the counter electrode and Ag/AgCl as the reference electrode (saturated with 3.0 M KCl, BASi). The glassy carbon electrode loaded with the catalyst served as the working electrode. Liner sweep voltammetry (LSV) with a scan rate of 50 mV/s was conducted first. The gas products were detected using a gas chromatograph (GC, PerkinElmer Clarus 600) equipped with a thermal conductivity detector (TCD) for hydrogen (H\(_2\)) quantification and a flame ionization detector (FID) for methane (CH\(_4\)) and ethylene (C\(_2\)H\(_4\)). Liquid products were quantified using \(^1\)H nuclear magnetic resonance (NMR, Agilent DD2 500). The NMR samples were prepared by mixing 0.5 mL of electrolyte with 0.1 mL of deuterated water (D\(_2\)O), and 0.02 µL of dimethyl sulfoxide (DMSO) was added as an internal standard. Potential \(E\) was converted to the RHE reference electrode using:

\[
E (\text{versus RHE}) = E (\text{versus Ag/AgCl}) + 0.197 \text{ V} + 0.059 \text{ V} \times \text{pH}.
\]

#### Electrochemical active surface area (ECSA) measurement

We used the double layer capacitance method to measure the surface roughness factors \(R_f\) for the samples relative to polycrystalline Cu (\(R_f = 1\)) foil. \(R_f\) was calculated from the ratio of the double-layer capacitance \(C\) of the catalyst electrode and Cu foil electrode (C\(_{\text{Cu foil}} = 29 \mu\text{F}\)) that is, \(R_f \sim C/C_{\text{Cu foil}}\). \(C\) was determined by measuring the geometric current density at a potential at which no Faradaic process was occurring when we varied the scan rate of the CV. CV was performed in the same electrochemical cell with 0.1 M KOH electrolyte separated with a Nafion proton exchange membrane. The linear slope provides ECSA = \(R_f \times S\), where \(S\) stands for the geometric area of the glassy carbon electrode (\(S = 0.19 \text{ cm}^2\) in this work).

#### Characterization

XRD were measured on a Philips X-Pert Pro Super X-ray diffractometer equipped with graphite-monochromatized Cu Ka radiation. X-ray photoelectron spectroscopy (XPS) was conducted at an accelerating voltage of 200 kV. High-angle annular dark field scanning transmission electron microscopy (HAADF-STEM) and high-resolution transmission electron microscope electron energy loss spectroscopy (HRTEM-EELS) were carried out using a cold-field emission Cs-corrected JEOL ARM-200F Atomic Resolution Microscope operating at an accelerating voltage of 200 kV. In situ X-ray absorption of the Cu K-edges was performed at the Soft X-ray Microcharacterization Beamline (SRXRM) at Canadian Light Source (CLS). A homemade in situ electrochemical cell was used, with platinum as the counter electrode and Ag/AgCl as the reference electrode. The electrolyte is CO\(_2\)-purged 0.1 M KOH. The acquisition of each spectrum took 15 min.

#### Data availability

The data that support the findings of this study are available within the article and its Supplementary Information files. All other relevant source data are available from the corresponding author upon reasonable request.

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