Progress in Material Development for Low-Temperature Solid Oxide Fuel Cells: A Review

Mohsen Fallah Vostakola 1 and Bahman Amini Horri 2, *

1 School of Metallurgy and Materials Engineering, Iran University of Science and Technology (IUST), Narmak, 16846-13114 Tehran, Iran; mohsenfallahvostakola@gmail.com
2 Department of Chemical and Process Engineering, Faculty of Engineering & Physical Sciences, University of Surrey, Guildford, Surrey GU2 7XH, UK
* Correspondence: B.Aminihorri@surrey.ac.uk

Abstract: Solid oxide fuel cells (SOFCs) have been considered as promising candidates to tackle the need for sustainable and efficient energy conversion devices. However, the current operating temperature of SOFCs poses critical challenges relating to the costs of fabrication and materials selection. To overcome these issues, many attempts have been made by the SOFC research and manufacturing communities for lowering the operating temperature to intermediate ranges (600–800 °C) and even lower temperatures (below 600 °C). Despite the interesting success and technical advantages obtained with the low-temperature SOFC, on the other hand, the cell operation at low temperature could noticeably increase the electrolyte ohmic loss and the polarization losses of the electrode that cause a decrease in the overall cell performance and energy conversion efficiency. In addition, the electrolyte ionic conductivity exponentially decreases with a decrease in operating temperature based on the Arrhenius conduction equation for semiconductors. To address these challenges, a variety of materials and fabrication methods have been developed in the past few years which are the subject of this critical review. Therefore, this paper focuses on the recent advances in the development of new low-temperature SOFCs materials, especially low-temperature electrolytes and electrodes with improved electrochemical properties, as well as summarizing the matching current collectors and sealants for the low-temperature region. Different strategies for improving the cell efficiency, the impact of operating variables on the performance of SOFCs, and the available choice of stack designs, as well as the costing factors, operational limits, and performance prospects, have been briefly summarized in this work.

Keywords: low-temperature solid oxide fuel cell; low-temperature electrolyte; electrochemical performance

1. Introduction

Deploying more efficient and robust power conversion devices to supply affordable energy with reduced CO₂ emission becomes one of the biggest global challenges in this century. Today, more than 70% of the global energy demand for power generation, transportation, and industrial heating comes from fossil fuels extracted from deep within the Earth’s crust. However, harnessing energy from fossil fuels is associated with two major drawbacks: first, due to the scarcity and exhaustible nature of these fuels, they may fail to satisfy the increasing rate of energy demand in the close future; and second, those fuels eventually lead to an increase in the atmospheric concentrations of greenhouse gases (GHGs) which consequently cause a noticeable change in the climate patterns with a contribution to acid rains, water pollution, air pollution, global warming, etc. [1–6]. Thus, a comprehensive and urgent solution shall be developed to tackle both the energy and environmental challenges based on the renewable energy sources (such as solar, wind, hydroelectric power, etc.), along with the application of more sustainable energy conversion devices. Nowadays, there is a growing interest in developing fuel cells for both...
portable and stationary power applications because of their high efficiency, environmentally-friendly operation, and fuel flexibility [7–10]. A fuel cell is an electrochemical device that can directly convert the chemical energy of fuels into electricity through a more reversible operation. The first fuel cell, so-called “the gas voltaic battery”, was invented by Sir William Grove in 1839, which could generate electricity by combining hydrogen and oxygen gases [7,11]. Offering a relatively higher efficiency (65–85%) and fewer emissions compared to the internal-combustion engines (Carnot cycle, with an efficiency below 45% [12]), fuel cell technology is considered as one of the most promising candidates for replacing the conventional power generation systems [7–10].

Fuel cells are structurally comprised of an electrolyte layer sandwiched between a couple of porous electrodes. The electrolyte layer has an essential role, as the heart of fuel cell, for indicating the cell operating temperature range, the type of the electrochemical reactions taking place at the electrodes, and the type of catalytic constituents of the electrodes. Thus, fuel cells are classified based on the type of their electrolyte material into various categories such as alkaline fuel cell (AFC) [13], direct methanol fuel cell (DMFC) [14], molten carbonate fuel cell (MCFC) [15], proton exchange membrane fuel cell (PEMFC) [16], phosphoric acid fuel cell (PAFC) [13], solid oxide fuel cell (SOFC) [17], and so on. Among the different types of fuel cells, solid oxide fuel cells have attracted great interests because of their unique properties such as offering comparably a higher efficiency, extensive fuel flexibility, more durability, and relatively lower cost of fabrication because of their capability to operate with non-precious metals [8,14,18–22]. SOFCs have a wide range of applications including combined heat and power (CHP) systems, stationary and portable power plants, hybrid vehicles, distributed power sources, etc. [1,20,23,24]. Despite the numerous advantages of SOFC, however, their relatively slower start-up, thermochemical instability of the cell individual layers, and the high-temperature range required for exhibiting adequate ionic activity have been addressed to be their major drawbacks [3,8,24–26].

1.1. Structure of SOFCs
1.1.1. SOFC Individual Layers

Each SOFC consists of three main components, namely, anode, electrolyte, and cathode, along with an interconnect layer integrated as the current collector on top of each electrode. The SOFC single cells should provide high electrochemical performance, acceptable thermochemical stability, and adequate fuel efficiency during the high-temperature red-ox (reduction-oxidation) cycles of operation. Both electrodes should be fabricated with a certain extent of microstructural porosity to allow forming the interfacial areas at the junction of electrolyte, electrode, and the microstructural pores, so-called triple-phase boundary (TPB). The TPBs are believed to be the active sites supporting the electrochemical reactions in the SOFC structure. In SOFCs, the electrochemical oxidation of fuels takes place at the anode TPBs. The SOFC anode layer should possess a fine grain size distribution, suitable porosity, sufficient electrical conductivity, desirable chemical and thermal compatibility, high electrocatalytic activity, acceptable mechanical strength, and a matching thermal expansion coefficient (TEC) with the other cell components. The following steps should take place in order to successfully achieve the electrochemical oxidation of fuels in the SOFC anode layers [27,28]:

- Transportation of fuel molecules into the porous structure of anode and their adsorption onto the anode surface.
- Diffusion of adsorbed fuel species to the TPBs and simultaneously, desorption of the product of electro-catalytically species from the anode surface.
- Transportation of oxide ions (O$_{2}^-$) across the electrolyte, followed by diffusion of them to the TPBs.
- Releasing the electrons from the charged species into the bulk of the anode electrocatalytic constituents at the TPB.
- Extension of active TPBs, which are well-interconnected to the available ionic-electronic conduction paths and mass-transfer channels at the SOFC anode structure.
Generally, the electrical conductivity of anode material should be at least 100 S·m\(^{-1}\) at the operating temperature [27]. The SOFC anode materials should consist of both the ionic- and electronic constituents so-called cermet (ceramic–metal) composites. Nickel/Yttria-stabilized zirconia (Ni-YSZ) is one of the most common anode cermets reported to have an acceptable electrical conductivity in the range of 10\(^{2}\)–10\(^{4}\) S·m\(^{-1}\) for high-temperature SOFCs. In addition to the fact that the SOFC anode cermets encompass a suitable amount of porosity which can accelerate fuel diffusion, they also facilitate oxygen ions migration through the active sites of the anode. In the case of using hydrogen (H\(_2\)) and/or methane (CH\(_4\)) as the fuel, the possible half-cell reactions of the SOFC anode could be written as follows [29–33]:

\[
\begin{align*}
    \text{H}_2 + \text{O}^{2-} &\leftrightarrow \text{H}_2\text{O} + 2\text{e}^- \\
    \text{CH}_4 + \text{O}^{2-} &\leftrightarrow \text{CO} + 2\text{H}_2 + 2\text{e}^- \\
    \text{CH}_4 + 3\text{O}^{2-} &\leftrightarrow \text{CO} + 2\text{H}_2\text{O} + 6\text{e}^- \\
    \text{CH}_4 + 4\text{O}^{2-} &\leftrightarrow \text{CO}_2 + 2\text{H}_2\text{O} + 8\text{e}^-
\end{align*}
\]

Adsorption of oxygen molecules takes place at the active surface of the SOFC cathode. The porous structure of the cathode makes it possible to accelerate the mass migration of air or the other oxygen-containing species as the oxidant. The adsorbed oxide specious would then be electrochemically reduced to oxide ions (O\(^{2-}\)) in the presence of the electrons coming from the current collector at the cathode TPBs (the cathode/electrolyte/gas interfaces). Typically, an ideal SOFC cathode material should provide a high electronic and ionic conductivity, high catalytic activity for oxygen reduction reaction, sufficient porosity, good chemical and thermal stability, matching TEC, and high spatial TPB density. The cathode half-cell reaction can be written as below [27,28,31,33]:

\[
\frac{1}{2}\text{O}_2 + 2\text{e}^- \leftrightarrow \text{O}^{2-}
\]

Thus, the cell overall reaction (sum of the anode and cathode half-cell reactions) in the case of using hydrogen as the fuel can be written as follows:

\[
\text{H}_2 + \frac{1}{2}\text{O}_2 \leftrightarrow \text{H}_2\text{O}
\]

In this case, the open-circuit voltage (\(E_{OCV}\)) can be estimated using the Nernst equation as follows [27,28,31,33]:

\[
\begin{align*}
    E_{OCV} &= E^o + \left(\frac{RT^o}{nF}\right) \ln \left(\frac{P(\text{H}_2)\left(\sqrt{P(\text{O}_2)}\right)}{P(\text{H}_2\text{O})}\right) \\
    E^o &= -\frac{\Delta G^o}{nF}
\end{align*}
\]

where \(E^o\) is the cell standard potential (electromotive force, emf \(V\)); \(R\), the universal gas constant (\(\frac{\text{J}}{\text{mole} \cdot \text{K}}\)); \(T^o\), the cell reference temperature (\(\circ \text{K}\)); \(n\), the valence number of ions (\(\frac{\text{moles of ions}}{\text{mole}}\)); \(F\), Faraday’s constant (\(\frac{\text{C}}{\text{moles of electrons}}\)); \(\Delta G^o\), the standard Gibbs free energy of a reaction (\(\frac{\text{J}}{\text{mole}}\)); and \(P\), the partial pressure of species (\(\text{Pa}\)). Therefore, the cell temperature, the pressure of hydrogen and water at the anode surface, and the pressure of oxygen at the cathode surface can change the cell open-circuit voltage. The maximum theoretical (thermal) efficiency of a cell (\(\eta_{th}\)) can then be expressed using the higher heating value (\(\text{HHV}, \frac{\text{J}}{\text{mole}}\)) associated with the cell overall reaction as the following [34]:

\[
\eta_{th} = \frac{nFE^o}{\text{HHV}}
\]
There are several sources of polarizations and potential losses affecting the performance of an operating cell, mainly including (1) Activation loss ($\epsilon_a$), which is due to the energy used to achieve the self-sustaining electrochemical reactions at the electrodes; (2) Ohmic losses ($\epsilon_\Omega$), which is caused by the sum of ionic, electronic, and contact resistances against electrons migration across the cell components; (3) Concentration loss ($\epsilon_c$), which takes place due to the variation in reactants concentration at the surface of electrodes; (4) Fuel-crossover loss ($\epsilon_{fc}$), which is caused by the fuel diffusion across the electrolyte layer; and (5) Internal-current loss ($\epsilon_{icl}$), which is appeared when the electrolyte suffers from electronic leakage (and/or the presence of any internal short circuit between both electrodes) [34,35]. These polarizations and potential losses could result in gaining a lower emf for an operating cell that can be expressed as

$$E = IR = E_{OCV} - \epsilon_a - \epsilon_\Omega - \epsilon_c - \epsilon_{fc} - \epsilon_{icl}$$

where $E$ is the actual cell voltage ($V$) under the external load ($R, \Omega$) and $I$ is the cell discharge current ($A$) [1,34]. These polarizations and potential losses eventually cause gaining a lower efficiency for a working SOFC compared to the thermal (maximum achievable) efficiency.

The operation of a SOFC relies on the electrochemical reaction between the fuel species and the oxide ions which are transported from cathode to anode by migrating across the whole thickness of the electrolyte. Therefore, the electrolyte microstructural and physical properties, especially its thickness and ion conductivity, can greatly affect the electrochemical performance of SOFCs. Anionic, protonic, and mixed ionic are the three ion transportation mechanisms in the SOFC electrolytes. The electrolyte layer should have a high density to provide an acceptable range of ionic conductivity and also to prevent gas diffusion between the electrodes. Since the ionic conductivity in solid electrolytes is governed by the site-to-site “hopping” mechanism, it can be promoted by thermal excitations of the oxide ion vacancies [33]. Moreover, crystal structure plays an important role in enhancing the oxide ion conductivity; therefore, the larger interionic space, the higher level of point defect disorder, and lower migration enthalpy [8]. The SOFC electrolyte materials should satisfy several requirements such as providing a high oxide ion conductivity (at least 0.1 S·cm$^{-1}$) at the cell operating temperature, enough thermochemical stability in the cell red-ox environment, good mechanical strength (fracture resistance > 400 MPa), high density, minimal volatilization, minimal ohmic loss, negligible electronic conductivity, and a proper TEC value compatible with the other cell components [27,28,31]. Figure 1a schematically shows the fundamental operation of a SOFC using various fuels.

![Schematic of (a) Solid oxide fuel cells (SOFC) operation and (b) Single cells assembly in-series [36].](image_url)
Due to the low output voltage of a single SOFC, they are usually assembled into an array or stack to produce desirable voltage and power output (Figure 1b). An interconnect layer is placed between the single cells to integrate them into multiple arrays in series or parallel with collecting the generated electricity. The interconnect should be cost-effective and since it acts as a barrier between the oxidizing and reducing atmosphere too, it should provide high thermochemical stability, adequate electrical conductivity (ASR < 0.1 Ω cm$^2$), and a TEC well compatible with the other cell/stack parts ($-10.5 \times 10^{-6} \text{K}^{-1}$) [37,38]. Oxide perovskite-based ceramics are still amongst the most suitable interconnect materials for the SOFCs operating at high temperatures. The most prevalent perovskite-based interconnect is Ca-doped LaCrO$_3$ [31]. Although the ceramic materials can be potential interconnect candidates, they are more expensive compared to those made from metals and alloys. Furthermore, the perovskite-based interconnects may not meet the required mechanical strength at the cell operating condition. Graded metal alloys and cermet composites are the other potential candidates which are used widely for fabricating the SOFC interconnect. The metal alloy interconnects are usually preferred for low-temperature SOFC applications. This is mainly because of their high mechanical strength, high thermal conductivity, high electronic conductivity, low cost, facile machining and fabrication properties, and suitable oxidation resistance. Overall, metal alloys containing Cr, Al, and Si can withstand better in a high-temperature oxidizing environment [38].

1.1.2. State-of-the-Art SOFC Materials

Since the first solid oxide fuel cell fabricated by Baur and Preis (in the 1930s) based on zirconia, several ceramic composites have been investigated to improve the electrical conductivity, electrochemical performance, and efficiency of SOFCs. Ni/YSZ cermet is the most common anode material in SOFCs due to its low cost, close TEC to the YSZ electrolyte, and thermochemical stability at high temperature reducing environment. Nickel is used as a catalytic constituent to break the H-H bond of hydrogen fuel and also to provide the electronic conduction path required in the SOFC anode structure [31,36,39]. Copper, cobalt, and phosphorous are the other catalytic materials that can be potentially used for fabricating nickel-free SOFC anodes. Since the electrical conductivity of nickel is about five times greater than the YSZ, the ratio of Ni/YSZ has a significant effect on the electrical conductivity of the final product. In such composite, ionic conductivity and electronic conductivity occurs through YSZ and nickel, respectively. In addition to these factors, microstructural features, thickness, and the spatial density of TPBs can greatly affect the SOFC anode performance [36,40]. Nickel-zirconia (Ni-ZrO$_2$) cermet is another potential anode material that can be used for high-temperature SOFCs. A Ni-ZrO$_2$ anode substrate fabricated with 150 µm thickness and the porosity of 20–40% exhibits a TEC of $12.5 \times 10^{-6} \text{K}^{-1}$ with an electrical resistivity of about $3 \times 10^{-6} \Omega \cdot \text{cm}$ [41]. NiCu-Gd$_2$O$_3$, LaSrFeCo-gadolinium-doped ceria (Gd$_2$O$_3$-CeO$_2$ or GDC), CuNiZn-GDC, ZnFeCu-GDC, and Cu-CeO$_2$/YSZ are some of the anode materials with both ionic and electronic conductivity that have been investigated during the past decade [31,36,39,42,43].

Perovskite composites with a typical ABO$_3$ structure are the most common materials used for the fabrication of cathode. In this structure, A site cations usually have larger ionic radii with a lower oxidation state compared to the cations standing for B site [28,44]. Lanthanum strontium manganite (LSM) is one of the most common perovskite materials used to fabricate high-temperature SOFC cathodes. Doping LSM with alkaline earth cations such as Sr$^{2+}$ or Ca$^{2+}$ can increase the electronic conductivity and the hole concentration of the resulting composite as per the following reaction:

$$\text{SrO} + \text{LaMnO}_3 \rightarrow \text{Sr}^{2+}_{\text{La}} + \text{Mn}^{3+}_{\text{Mn}} + \text{O}^3_\text{O}$$  (11)

where $\text{Sr}^{2+}_{\text{La}}$ indicates a strontium ion sitting on a lanthanum site with a negative charge, $\text{Mn}^{3+}_{\text{Mn}}$ indicates a manganese ion sitting on a manganese site with a positive charge, and $\text{O}^3_\text{O}$ indicates an oxygen ion sitting on an oxygen site with a neutral charge [45,46]. It has
also been reported that doping the perovskite composites with proper cations can improve their TEC values, particularly when it targets affecting the structural A site [28,47]. Doping with transition metal cations is another approach applied for improving the characteristics of perovskites. In this regard, various perovskite composites have been synthesized such as PrSrFeO, SrCeFeNiO, SrCeFeCoO, LaNiFeO, PrSrCoFeO, LaSrFeO (lanthanum strontium ferrite-LSF), LaSrCoFeO (lanthanum strontium cobalt ferrite-LSCF), Zn-doped LSCF, and Bi-doped LaSrNiO [28,48–50].

The defect chemistry of the alkaline earth metal titanates and LSF have been investigated in details by Shi [51] and Schmid and Fleig [52]. Taylor et al. [53] have also investigated the defect chemistry by analyzing the impact of the partial pressure of oxygen ($p_{O_2}$) on the formation enthalpy of intrinsic defects in LaFeO$_3$ crystals. Figure 2 illustrates a typical plot of the point defect diagram for LSF at 600 °C [54]. The plot was obtained using the thermodynamic data such as enthalpy and entropy values predicted based on Equation (12) with an oxygen incorporation value obtained from Equation (13) [52]. In order to explain the trends in Figure 2, chemical capacitance (C$_{chem}$) was defined as the ability of oxide ions to change their stoichiometry when the oxygen chemical potential is varied. The oxygen chemical potential value depends on the concentration of the charge carriers. Each trend in Figure 2 has its own equation. Overall, at high $p_{O_2}$, C$_{chem}$ is dominated by the concentration of oxygen vacancies (with a negative slope of about -0.5). By decreasing the $p_{O_2}$, the electron holes become equally important. C$_{chem}$ decreases with decreasing the hole concentration (with a positive slope of about +0.25) up until a point that it reaches a minimum value and then it again increases with increasing the electron concentration [54]. The defect chemistry can also be helpful to explain the higher electronic conductivity (leakage) of the ceria-based electrolytes at increased temperatures. In the other words, cell operation at higher temperatures may decrease the oxygen chemical potential, and hence result in achieving a lower concentration of the intrinsic vacancies, which finally leads to gain a higher electronic conductivity in the electrolytes.

$$2Fe^{x}_{Fe} \rightarrow Fe^{x}_{Fe} + Fe^{x}_{Fe} \quad (12)$$

$$V_{O} + 2Fe^{x}_{Fe} + \frac{1}{2}O_{2}(g) \rightarrow O^{x}_{O} + 2Fe^{x}_{Fe} \quad (13)$$

![Figure 2. Brouwer diagram of lanthanum strontium ferrite (LSF) at 600 °C [54].](image-url)
Composite materials are amongst the new approaches toward improving the SOFCs efficiency that could play an important role to decrease the electrode overpotentials by offering an increased effective surface area for performing the electrochemical reactions [55]. The mixed ionic-electronic conductors (MIECs) are another class of composite materials that have been mainly developed to improve the electrocatalytic performance of SOFCs. The main idea of creating such materials is to use the oxygen vacancies in the bulk of the materials as well as their higher rate of ion transport. These materials simultaneously offer both electronic and ionic conductivity with high transport properties that could result in gaining a high density of electrocatalytic active sites in their structure. In the case of MIEC cathodes, penetrating the oxygen reduction sites into the bulk of the electrodes can extend the oxygen reduction area from the TPBs to the bulk of the cathode, and hence it reduces the cathode polarization losses [50,56–58]. The electronic conductivity of the MIEC composites can be increased by introducing those dopants that could generate oxygen vacancies in the bulk of the material [59]. An important issue with the MIEC composites is their compatibility with other cell constituents. Thus, heterogeneous MIECs have been developed, which are comprised of a composite mixture of an electron-conducting and an ion-conducting phase. Introducing a non-homogeneous phase in the composite structure can promote the formation of holes and TPBs in bulk and thereby improve SOFC performance [60].

Generally, non-stoichiometric oxides with the perovskite structure (ABO3) are classified as a type of MIECs. For example, La0.5Sr1−xCo1−yFe1−yO3−δ (LSCF)-Ce0.5Gd1−δO2−δ (GDC) composite has been reported to be the state-of-the-art cathode MIEC [56]. Wu et al. [61] investigated the electrochemical performance of La1.5A0.5−δNiO4+δ (A = Ca, Sr or Ba) cathode materials for intermediate- and low-temperature applications. According to the results (Figure 3), Sr-doped and Ca-doped samples exhibited the highest performance in the low- and intermediate-temperature range, respectively. However, the rate of oxygen adsorption can significantly limit the electrochemical performance of an MIEC-based cathode substrate [62].

Bi0.5Sr0.5FeO3−δ−Ce0.9Gd0.1O1.95 composites [63] and infiltrated Ni-YSZ cermets [64] are some other examples of the MIEC materials applied for fabricating the SOFC cathode and anode, respectively. MIEC electrolytes with high ionic and moderate electronic conductivity are suitable candidates for the L-T SOFC applications. In this context, doped ceria-based electrolytes have been known to exhibit higher electronic conductivity (leakage) at increased temperatures that results in a decrease in the cell open circuit voltage (OCV) [65].
To overcome this issue, an electronic blocking layer has been proposed by the commercial SOFC developers like Ceres Power Ltd. [66]. Another issue reported for the MIEC electrolytes is their electronic leakage which is increased with decreasing the thickness of the fabricated electrolyte pellets [67]. Therefore, an optimum MIEC-based electrolyte thickness should be defined as a trade-off between the loss of OCV and the reduced ASR by these electrolytes [16,68].

Perovskite materials can also be potentially considered as proton conductors. In comparison with oxide ion conductors, the proton conductors may offer higher efficiency but suffer from low power density and voltage [69]. Furthermore, because of using a pure stream of fuel (hydrogen), the electrochemical performance of the proton-conducting cells would not be deteriorated [70]. Several proton conductors have been investigated in the past few years such as BaCe0.9Sr0.5Zr0.35Y0.1Sn0.05O3−δ [69], Ba0.8Sr0.2Ce0.6Zr0.3O2−δGd0.1Y0.1O3−δ [71], BaCe0.9Y0.1O3−δ [72], La-doped BaZrYO3−δ [73], etc. Due to the small size of protons (H+), the proton conductors show comparably a lower activation energy; thus, they exhibit a relatively higher conductivity at low temperatures (~1 × 10−2 S·cm−1 at 600 °C) compared to the oxide-ion conducting materials [70,74]. The following equation can show the formation of oxide ion vacancies in the proton-conducting materials [70,75]:

$$\text{H}_2\text{O(g)} + V_{O(s)} + O_{\text{H}_{O(s)}^+} \rightarrow 2\text{OH}_{O(s)} $$ (14)

where $V_{O(s)}$ and $O_{\text{H}_{O(s)}^+}$ represent the oxide ion vacancy and the proton after attaching to the oxygen ion, respectively [70].

1.1.3. Characteristics and Performance of Electrolyte-Supported SOFCs

Nowadays, zirconia-based ceramic composites are the most common electrolyte materials used for the fabrication of SOFCs. Aliovalent doping can increase the concentration of oxide ion vacancies and thereby enhance the ionic conductivity of the electrolyte layer. Yttria (Y2O3) and scandia (Sc2O3) are the most common dopants reported in the literature for zirconia. For high-temperature SOFC applications, Y2O3 doping results in a significant increase in the ionic conductivity and also chemical stability of the resulting composite in both oxidizing and reducing atmospheres. The main problem associated with these materials is their tendency to intercalate with La- and Sr-contained cathode composites, in which the resulting composite can hinder the oxide ion transportation in the fabricated cells [76]. Ionic conductivity and thickness of electrolyte are the other parameters that have a key role in determining the operating temperature of SOFCs. In general, the ceria-based electrolytes exhibit a higher ionic conductivity than that of the zirconia-based composites. This is mainly because of the greater ionic radii of cerium ions (Ce4+/3) compared to the zirconium ions (Zr4+). Similarly, doping with Gd3+, Sm3+, and Y3+ can improve the ionic conductivity and thermochemical stability of zirconia. Amongst these cations, Gd-doped ceria (GDC) has a high ionic conductivity at 500 °C with no significant chemical reaction with LSCF cathodes. However, the reduction of Ce4+ in the reducing atmosphere at high temperatures (above 700 °C) can potentially create some extend of electronic conductivity in the GDC electrolyte layer that eventually results in a decrease in the cell OCV and electrochemical performance [28,77,78]. Yttria-stabilized zirconia, in contrast, exhibits a very low electronic conductivity and high ionic conductivity at elevated temperatures (above 800 °C). In addition, YSZ shows excellent mechanical property with a thermo-chemically stable structure for high-temperature applications [36].

1.1.4. SOFC Fabrication and Geometries

The SOFC stacks can be fabricated into two major geometries called tubular and planar designs. Currently, the development of tubular SOFCs has been limited due to their low power densities and practical challenges associated with integrating the single cells into multiple assemblies [79,80]. Planar SOFCs can comparably provide a higher power density when assembled using various types of single-cell designs such as electrode-supported
(anode-supported and cathode-supported), electrolyte-supported, and metal-supported geometries [35,81]. The supporting layer is the cell individual part that is fabricated thicker than the other cell parts to support the complete cell structure mechanically. In the case of anode-supported SOFCs, the electrolyte and cathode layers are fabricated as thin films by integrating them on top of a thick anode layer, respectively. A thinner electrolyte layer can be advantageous by reducing the cell ohmic polarization, lowering the operating temperature, and better overall cell performance [35,82]. It has been reported that ohmic polarization is one of the main sources of electrical potential loss in SOFCs [4,83–85]. Lowering the cell operating temperature can greatly suppress the material degradation due to thermochemical corrosion and therefore is an effective method to increase cell durability [82,86–88].

Seal leakage, fuel supply interruption, or any other undesirable situations may cause re-oxidation of the catalytic constituent of the supporting anode in SOFCs [89]. These periodic reduction-oxidation cycles can significantly affect the continuous operation and the electrochemical performance of the anode-supported SOFCs. The electrode-supported design is currently the most common geometry for the fabrication of SOFCs. However, many challenges associated with this design, such as delamination at the interface of electrode-electrolyte and the difficulties in gas transportation within the thick layer of electrodes, are yet to be addressed [90,91]. The electrolyte-supported geometry, in contrast, is more robust with providing a better red-ox cycle tolerance compared to the electrode-supported cells. The thick electrolyte layer in an electrolyte-supported geometry can make it easier to seal the cell periphery against fuel diffusion, and therefore it provides better fuel efficiency. The thin anode layer in this geometry could also be an advantage in offering a lower fuel diffusion resistance. Conversely, the thick electrode layer increases the concentration and activation polarization, and therefore the electrode-supported cells may comparably provide a lower power density [89,92]. The area-specific resistance (ASR) of the cell individual layers is usually used to compare the impedance of different types of materials used in the individual parts of a SOFC. The ASR is defined as [93–95]:

\[
\text{ASR} = R_p \times A = \rho \times l
\]

where \(R_p\) is the polarization resistance (\(\Omega\)) of a cell individual part, \(A\) is its effective area (\(m^2\)), \(l\) is the thickness (m), and \(\rho\) is the specific resistance of the material (\(\Omega \cdot m\)) [92,95]. According to this equation, ohmic losses and thickness have a strong effect on the ASR.

The cathode-supported geometry has received less interest in literature, mainly due to the practical issues associated with its step-wise fabrication method. The lifetime of cathode-supported SOFCs has been reported to be the longest amongst all the other geometrical designs. However, compared to the anode-supported geometry, the cathode-supported cells have a more significant activation potential loss [35,80,96]. It has also been reported that the cathode-supported tubular SOFCs could have desirable stability against the thermal expansion and contraction due to their thin electrolyte and anode layers [97]. One of the main challenges associated with developing the cathode-supported SOFCs is their significant tendency to intercalate with the electrolyte constituents during the sintering process and cell operation that can eventually result in obtaining a poor electrochemical performance [84,98]. Chelmehsara et al. [99] employed a numerical method to compare different types of SOFCs geometries for studying this issue. They reported that the cathode-supported SOFC is the best choice if the power density is considered alone, but the electrolyte-supported SOFC can provide the most uniform current density distribution with a peak of current density towards the non-supporting side layers.

Metal-supported SOFCs (M-S SOFCs) were first designed in the 1960s. In M-S SOFCs, the thickness of the ceramic layers is as thick as required for the electrochemical functions [24]. In comparison to the conventional ceramic-supported SOFCs, M-S SOFCs offer more structural robustness as well as good re-oxidation stability. Generally, the metal support should have high mechanical strength, matching thermal expansion coefficient with the other cell individual parts, and good corrosion resistance in the red-ox envi-
Nielsen et al. [65] reported that higher porosity of the supporting metals can improve the anode gas transportation, electrocatalyst loadings, and the cell performance. Due to the similar thermal expansion coefficient of ferritic steels and ceramic constituents, ferritic steels such as SS340L have been widely used as supporting metals in SOFCs; however, these steels are not cost-effective. Other candidates include Ni, FeNi, NiCrAlY, etc. [100,101]. Oxidation of the metal support at high temperatures, thermal expansion mismatch, Cr poisoning, and relatively low efficiency of M-S SOFCs are the most important challenges limited the commercialization of the M-S SOFCs.

Another problem is the inter-diffusion of the elements between the metallic substrate and anode layer in the conventional Ni-YSZ cells, which results in a decrease in the material re-oxidation stability [101–104]. A diffusion barrier layer can be employed to prevent the inter-diffusion of the elements. This barrier should have a matching thermal expansion coefficient in order to prevent the inter-diffusion and the tunable gas/electron transportation between the cell anode and its supporting layer. A variety of materials such as Cu-YSZ cermets, CrO$_2$-based diffusion layers, La$_{0.6}$Sr$_{0.2}$Ca$_{0.2}$CrO$_3$, and CeO$_2$-Ce$_{0.8}$Gd$_{0.2}$O$_2$ composites have been investigated as the diffusion barrier layers. It has been reported that the next generation of M-S SOFC geometry encompasses a Fe–Cr alloy substrate, a diffusion barrier layer, anode, electrolyte, and cathode [57,101,105]. Despite the exciting achievements in the fabrication of M-S SOFCs, further investigations are still needed to develop commercial stacks with high efficiency and durability. Table 1 summarized the major benefits and drawbacks of the common cell fabrication geometries in SOFCs.

| Cell Geometry       | Strength                        | Weakness                           |
|---------------------|---------------------------------|------------------------------------|
| Anode-supported     | Highly conductive anode         | Re-oxidation                       |
|                     | Low operating temperature       | Gas transportation                 |
| Electrolyte-supported | Strong backbone                 | Higher resistance                  |
|                     | Uniform current density         | Requires higher operating temperature for diminishing ohmic losses |
| Cathode-supported   | Low operating temperature       | Low conductivity                   |
|                     | No oxidation                    | Gas transportation issues          |
| Metal-supported     | Excellent structural robustness | Oxidation at high temperatures     |
|                     | High tolerance toward rapid thermal cycling | Moderate the cell electrochemical performance |
|                     | Excellent electrical and thermal conductivity | Thermal expansion mismatch between individual cell parts |
|                     |                                  | High cost of fabrication           |

1.2. Low-Temperature SOFCs (L-T SOFCs)

Among all of the challenges with SOFCs, the high operating temperature is of the greatest importance because of its significant impact on accelerating the cell degradation processes and increasing the cost of maintenance for a fabricated stack [7,27,106]. In general the SOFC materials can be divided into three categories according to their operating temperature including (1) high-temperature (H-T) SOFCs (800–1000 °C); (2) intermediate-temperature (I-T) SOFCs (600–800 °C); and (3) low-temperature (L-T) SOFCs (below 600 °C) [107]. Lowering the operating temperature can tackle many challenges associated with H-T SOFCs, such as widening the choice of functional materials and sealants for fabrication, decreasing the processing and fabrication costs, gaining lower thermal mis-
match between the cell individual layers, and reducing the start-up/shut-down time [1,108]. However, the cells operating at low temperatures usually provide a comparably lower electrochemical performance which is mainly due to the increased red-ox polarizations resistances at low temperatures. In the past few years, therefore, a considerable number of studies have focused on finding new materials with better polarizations behavior and high ionic conductivity at low temperatures. To decrease the operating temperature, the electrode becomes the most important part of the cell due to its high polarizations loss [16,106,107].

Despite the performance behavior of Carnot engines, in which lowering the operating temperature results in gaining a lower efficiency ($\eta = 1 - \frac{1}{T_C}$, where $T$ and $T_C$ are the operating and the sink temperatures, respectively), the SOFC efficiency would be quite oppositely increased due to eliminating the negative impact of temperature on Gibbs free energy [36,41]. In SOFCs, better power densities can be achieved by controlling the ohmic loss of the electrolyte. This can be usually obtained by reducing the electrolyte thickness or applying the solid electrolytes that offer higher ionic conductivity [16]. Regarding the first strategy, there have been some restrictions; for instance, there is a minimum thickness (usually between 1 and 20 $\mu$m) that does not practically allow the fabrication of thinner electrolyte layers [16]. This thickness is directly proportional to the oxygen self-diffusion coefficient and inversely proportional to the oxygen surface exchange coefficient. This minimum thickness is much higher (around 100 $\mu$m) for materials with AO$_2$ fluorite and many other ABO$_3$ perovskite structures [36,109]. Regarding the second approach, so far, many new electrolyte materials with high ionic conductivity such as ErBiO, DyWBiO, GdCeO, SmNdCeO, YZrO, LaSrGaMgO, LaSrGaMgCoO, BiMeVO, Gd(TiZr)O, Ln(SiO)O, AMoO$_4$, and BaCeYO have been proposed [16]. However, the majority of these composites are not enough thermochemically stable in the anode reducing environment. A suitable material for L-T SOFC electrolyte not only should have high thermochemical stability at operating condition but also exhibit minimal electronic conductivity between the SOFC electrodes. The outlook of lowering the operating temperature and improving the electrochemical performance for L-T SOFCs can be summarized as follows [16,36]:

- Maximizing the cell open-circuit voltage by optimizing the physiochemical properties of the electrolyte materials without the side effects like increased ASR
- Compensation of the electrodes thermal activation by manipulating the material microstructure

So far, several approaches have been proposed to lower the operating temperature of SOFCs. One effective method is to implement nanotechnology for synthesizing the electrolyte materials with suitable crystallite size and shape. Due to the large specific surface area, nano-sized particles can leave more grain boundaries after sintering, which is desirable for improving the oxide ion conductivity. In principle, the grain boundary conductivity is greater than that of the bulk of crystals [110]. Thus, polycrystalline materials can exhibit higher ionic conductivity compared to single-crystal materials with higher resistance. In addition, it has been reported that the SOFC nanocomposites with multi-phase constituents could offer a higher ionic conductivity at low temperatures. For example, a mixed ceramic–carbonate composite Sm$_{0.2}$Ce$_{0.2}$O$_{2-\delta}$-Na$_2$CO$_3$ showed a high ionic conductivity of about $1 \times 10^{-1}$ S·m$^{-1}$ at 300 $^\circ$C [111,112]. In another study, the nanocomposite ceramics containing a common SOFC electrolyte and a mixture of aliovalent metal oxides (i.e., SDC-LiNiZnO and NSDC-SrFeMoO) showed an acceptable performance (500–1000 mW/cm$^2$) at 400–650 $^\circ$C [20]. In the case of semiconductor-ionic composites, the interfacial areas of grain boundaries create superionic conduction paths which can improve the electrical characteristics of the operating cell [111]. However, nanomaterials have several critical challenges which should be addressed before their commercialization. One of the most important challenges associated with these materials is their aggregation and grain growth when operating at high temperatures for a long time [113]. The other issues can be listed as their needs for a precise impregnation technique for the formation of
charge carrier transfer channels [114], large-scale fabrication techniques [115], possibility of reducing porosities, low thermal stability, long-term durability, high costs, etc. [21,116].

Fabrication of multi-layered electrolytes such as bi-layering or tri-layering is another approach for developing highly efficient I-T and L-T SOFCs. This concept was first introduced by Virkar et al. who used a low conductive YSZ layer to protect the highly conductive ceria [117]. In bi- or tri-layer cases, two or three individual layers of electrolyte lie on top of each other to promote the cell ionic transport performance. Wachsman et al. proposed the use of Bi$_2$O$_3$-ceria bi-layer [118]. So far, several other bi-layered systems have been investigated such as zirconia-ceria, LSGM-ceria, BaCeO$_3$-ceria, and Bi$_2$O$_3$-ceria [7,119,120]. However, the bi- or tri-layering technique have still several challenges to be addressed such as the diffusion problem between layers, the TEC mismatching issue, and the cell shrinkage and cracking in operation.

The other material and fabrication processing variables such as microstructural manipulation, fabrication method, particle size, morphology, and sintering conditions can also have a significant impact on the performance of the fabricated SOFC. For example, particle size and morphology of the electrolyte powder can change the contact area and thereby change the electrical conductivity of the fabricated electrolyte [20]. Overall, to maximize the electrochemical performance of a SOFC, materials selection for different layers as well as their synthesis conditions and microstructural properties should be carefully considered.

2. Advances in Low-Temperature SOFC Electrolytes (L-T SOFC)

The electrolyte layer is the heart of a SOFC that determines the operating temperature of the cell with a strong impact on its electrochemical performance [121]. Currently, YSZ is the state-of-the-art material used for the fabrication of SOFCs. However, due to the high activation energy (∼1 eV) of YSZ, this classical SOFC electrolyte provides the acceptable range of ionic conductivity (1–10 S/cm) only at a high-temperature range (800–1000 °C) [107,122]. The high operating temperature could be advantageous for developing large-scale power plants, especially the systems based on the combined heat and power (CHP) cycles. However, the current technical challenges associated with operating at high temperatures (such as higher degradation rates and slower start-up and shutdown cycles, etc.), have limited the application of SOFCs for developing portable and auxiliary power systems. Lowering the operating temperature, on the other hand, can significantly reduce the degradation processes associated with the cationic intercalation between the cell individual layers and reduce the minimum voltage needed to keep the stack temperature (thermo-neutral electrolysis voltage) below 1.3 V. In addition, the low-temperature operation can offer a wider choice of sealant materials, as well as a decrease in radiative heat transfer and sintering-rate drop-off, that could reduce the system cost, in overall. [107,123,124]. Therefore, in the past few years, many attempts have been devoted to searching for new materials that can operate at a lower temperature range (below 600 °C). Since the electrolyte layer is well known as the heart of a SOFC, the majority of these attempts have been based on the development of the alternative co-doped electrolyte composites (such as samarium-doped ceria: SDC, gadolinium-doped ceria: GDC, lanthanum strontium gallium magnesium oxide: LSGM, etc.) along with the geometrical modification of the cell structures by minimizing the electrolyte thickness (using the advanced thin-film deposition techniques), and fabrication of the anode-supported SOFCs. The successful attempts for lowering the cell operating temperature should be accomplished with gaining a suitable power density (~1 W·cm$^{-2}$) and proper ASR (<0.3 Ω·cm$^{-2}$) [125]. Thereby, a new generation of electrolytes with enhanced O$^{2-}$ conductivity and electrochemical kinetics should be developed which can operate at low temperatures [120,126].

2.1. Ionic Conductivity and Electrochemical Performance

The ionic transfer number is fundamentally defined as the fraction of the total electrical current that is carried by a particular charged species when an electrical potential difference is applied to a material sandwiched between a couple of electrodes. [127]. Since ionic
conductivity of the liquid-state electrolyte is higher than that of solid-state electrolytes, selecting an electrolyte with high ionic conductivity as well as good chemical stability is of great importance [128]. The higher the ionic conductivity of the materials, the lower the operating temperature of SOFCs [129]. Fluorite-structured oxides with the general formula of \( \text{AO}_2 \), where A is the cation, usually exhibit a high ionic conductivity. The conductivity of these fluorites can be improved by the addition of some lower-valent cations, so-called doping agent (dopant) [130]. In general, the ionic conductivity of a certain electrolyte depends on its structural properties such as lattice parameter, relative density, dopant ratio, grain boundary, impurity, local microstructure, and grain size. In addition, the ionic conductivity is affected by the physical characteristics of the resulting composite such as relaxation time, operating temperature, and frequency [131]. The thermally activated ionic conductivity of the polycrystalline solid electrolytes can be expressed by the following equation [132]:

\[
\sigma T = \sigma_0 \exp \left( \frac{-E_A}{KT} \right)
\]

(16)

where \( \sigma \) is the ionic conductivity, \( \sigma_0 \) is the pre-exponential factor, and \( E_A \) is the activation energy. At low temperatures, \( E_A \) can be given as follows [132,133]:

\[
E_A = E_a + \frac{n}{2}E_m
\]

(17)

where \( n \) is a constant, \( E_a \) is the association energy of defect pairs, and \( E_m \) is the migration energy. Ionic conductivity of a solid-state electrolyte can also be calculated by the following equation [131]:

\[
\sigma = \frac{d}{(R_b \times A)}
\]

(18)

where \( d \), \( R_b \), and \( A \) are the thickness of the electrolyte, bulk resistance, and area of the solid electrolyte pellet, respectively.

To determine the optimum composition for fast oxide ion conductors, Mori et al. defined the effective index as follows [96]:

\[
\text{Effective index} = \left( \frac{\text{avg } r_c \text{ eff } r_o \text{ eff } r_d}{r_h} \right)
\]

(19)

where \( \text{avg } r_c \), \( \text{eff } r_o \), \( \text{eff } r_d \), and \( r_h \) are the cation average radius, effective ionic radius of oxygen, dopants average radius, and the ionic radius of the host, respectively. High ionic conductivity can be achieved when the effective index approaches one [133]. This criterion can be used to evaluate the ionic conductivity of various polycrystalline solid electrolytes. The effective oxygen ionic radius can be expressed as follows [1,134]:

\[
\text{eff } r_o = 1.4 \left( \frac{2 - \delta}{2} \right)
\]

(20)

where the constant number 1.4 stands for the ionic radii of oxygen and \( \delta \) is the stoichiometric oxygen ion vacancy, respectively.

It has also been reported that introducing a small amount of the second phase may enhance ionic conductivity by forming low-temperature compositions that can trap the impurities [110]. Ionic conductivity can be improved by a substantial decrease in the grain size (in the nanometer scale) by increasing grain boundaries and subsequently enhancing the ions mobility and better transport properties [21]. Generally, the concentration of charge carriers and their mobility dominate the overall ionic conductivity [135].

2.2. State-of-the-Art Electrolytes

2.2.1. High-Temperature Electrolytes

High-temperature electrolytes are the most common type of polycrystalline solid composites which usually capable to transfer oxide ions at a temperature ranging from
800 °C to 1000 °C. Since the operating temperature of these materials is relatively high, their fabricated electrolyte layer should have suitable thermochemical stability in the red-ox environments [136]. According to the cell electrochemical performance principles, an increase in the rates of electrode reactions with a decrease in the ohmic resistance of the electrolyte layer could result in a significant gain in the cell discharge power. Furthermore, since the electrolyte layer is dense and the SOFC operating temperature is usually above the autoignition temperature of hydrogen gas, it can immediately react with the oxide ions transferred across the electrolyte, and thereby prevents the accumulation of explosive mixtures [137]. Many high-temperature composites can be structurally modified through co-doping with the other homogeneous or heterogeneous phases (such as multivalence transitional metals, aliovalent dopants, carbonates, alkaline cations, etc.) to form a new electrolyte composite capable to operate at the low-temperature region. For example, doping a homogeneous zirconia-based composite with a foreign aliovalent dopant (as the second phase) can eventually increase the concentration of oxide-ion vacancies, particularly in the near-grain boundary region [112]. Therefore, in this section, the most-common high-temperature SOFC electrolytes would be briefly discussed as an introduction to extend the discussion to the low-temperature electrolytes.

Zirconia-based composites are the most common sort of high-temperature SOFC electrolytes. Zirconia exhibits a temperature-dependent crystallographic structure, where at ambient temperature it shows a monoclinic structure. By increasing the temperature to about 1100–2370 °C, it is transformed in the tetragonal structure; and by a further increase in temperature, it finally gets the cubic structure that offers the minimum activation energy for ionic conduction (above 2370 °C). However, the stabilized cubic structure of zirconia can be obtained by adding low-valence dopants such as Y^{3+}, Ca^{2+}, Mg^{2+}, Sc^{3+}, etc., as the stabilizing agent [122]. Zirconia-based compounds such as YSZ are the most common electrolyte material due to their good chemical stability in reducing and oxidizing atmospheres, good corrosion resistance, low thermal expansion coefficient, and high melting point [28]. Scandia-doped zirconia (ScSZ) has the highest ionic conductivity among the Zr-based electrolytes (~7 × 10^{-2} S·cm^{-1} at 800 °C and 3 × 10^{-1} S·cm^{-1} at 1000 °C) with a desirable ionic conductivity and excellent chemical stability; however, due to a gradual decrease in conductivity at elevated temperatures (so-called thermal ageing) and its high cost, it has limited applications in the fabrication of H-T SOFC. Although, some applications of ScSZ has been reported for the low-temperature region [28,30,138]. Amongst all of the zirconia stabilizers, 8 mol.% yttria-stabilized zirconia (YSZ-8) is the most widely zirconia-based high-temperature electrolyte that exhibits excellent chemical resistance in oxidizing and reducing atmospheres. The ionic conductivity of YSZ-8 is a function of temperature with about 10^{-3}, 2 × 10^{-2}, and × 10^{-1} S·cm^{-1} at 600, 800, and 1000 °C, respectively [138,139].

Ceria-based oxides can also be used as the high-temperature SOFC electrolytes with a stable cubic structure. Due to the low ion conductivity of these electrolytes (which is caused by their low oxygen defects), their ionic conductivity should be improved by adding some trivalent oxide materials such as Gd^{3+}, Sm^{3+}, or Y^{3+}. Introducing these materials can improve the ionic conductivity of ceria; for example, the ionic conductivity of GdO_{3} doped ceria is about five times more than YSZ at 800 °C [138]. Despite all of these advantages, ceria-based electrolytes suffer from partially electronic conductivity at high temperatures as well as the environment with a low partial pressure of oxygen. The reduction of Ce^{4+} to Ce^{3+} at low oxygen partial pressure yields a lower actual OCV value [140]. Samarium-doped ceria system shows better reduction resistance than pure ceria and alkaline earth oxide-doped ceria compounds. The ionic conductivity of the samarium-ceria system is almost twice that of the gadolinium-doped system. However, the reduction of Sm-doped ceria in the reducing environment of the SOFC anode can introduce an additional electronic conductivity to the system that eventually results in a significant power loss for the cells fabricated by this material [127,141].
2.2.2. Intermediate-Temperature Electrolytes

Lowering the SOFC operating temperature can significantly extend the range of materials selection, suppress the degradation of the cell components, and reduce the fabrication and maintenance costs [31]. The operating temperature of intermediate-temperature SOFC (I-T SOFC) electrolytes usually falls in the range of 600–800 °C. In addition to high-temperature electrolytes, scandia-doped zirconia can also be used as an intermediate-temperature electrolyte, but its long-term chemical stability remains unsolved [122]. Many intermediate-temperature electrolytes have been investigated by researchers in the past decade. Yamamoto et al. [142] studied the electrochemical performance of Sc-doped zirconia and reported that 11 mol.% Sc-doped zirconia (ScSZ-11) had no ageing effect. This was explained by adopting a phase transition by SCSZ-11 at about 600 °C; however, this phase transition can be prevented by adding 1 wt.% alumina. The ionic conductivity of alumina-doped ScSZ was slightly lower than the pure one (2.6 × 10⁻¹ S·cm⁻¹ at 1000 °C for pure ScSZ). Cui et al. [143] reported a zirconia-based electrolyte with improved electrochemical efficiency by co-doping YSZ with ytterbia and preparing 8YSZ-4Yb₂O₃ and 8YSZ-4Yb₂O₃-NaCl/KCl composites. Co-doping zirconia with higher valence cations like Y³⁺ and Yb³⁺ is a basic route that could increase the oxygen vacancy concentration in the resulting composites. The result of this work showed the formation of a pure ionic composite with the 8YSZ-4Yb₂O₃-NaCl/KCl sample, as illustrated in Figure 4. The maximum power density obtained from this composite was about 364 W·m⁻W·cm⁻² (at 800 °C).

![Figure 4](image.png)

**Figure 4.** Log(σ) vs. Log (pO₂) for 8YSZ-4Yb₂O₃ and 8YSZ-4Yb₂O₃-NaCl/KCl [143].

Due to the mechanical and thermodynamic stability of ceria and its high ionic conductivity, doped ceria composites have been reported as one of the most promising intermediate-temperature class for the fabrication of SOFC electrolytes. However, the problem of increased electronic conductivity (mainly caused by the reduction of Ce⁴⁺ to Ce³⁺) remains as the main drawback of these electrolytes that contribute to obtaining a lower overall performance for the fabricated cells [34]. Co-doping of ceria, especially with alkaline earth and rare earth ions, is an effective way to further increase its ionic conductivity. Samaria and gadolinia are the most effective dopants for ceria-based electrolytes [78, 144]. Ionic conductivity of gadolinium-doped ceria (GDC) and Samaria-doped ceria (SDC) electrolytes is about 10² S·cm⁻¹ at 800 °C and 4.2 S·cm⁻¹ at 700 °C, respectively [145, 146]. Tao et al. [147] studied the samarium and indium dual-doped ceria and found that the ohmic resistance and the maximum power density increased with increasing...
In$^{3+}$ content. However, its high electronic conductivity can drop the cell OCV value and performance subsequently. The dual-doping of ceria with various pairs of cations such as Sm$^{3+}$-Y$^{3+}$, Sm$^{3+}$-Ca$^{2+}$, Gd$^{3+}$-Sm$^{3+}$, La$^{3+}$-Ca$^{2+}$, and Gd$^{3+}$-Pr$^{3+}$ have also been investigated in the past works [129,148–150]. Despite the interesting improvements obtained by the dual-doping electrolytes, their thermal expansion mismatch as well as the modest electrochemical performance, remain as the major drawbacks of these electrolytes.

Perovskite-based materials have been investigated for their potential application as I-T SOFC electrolyte. Doped BaCeO$_3$ with perovskite structure is a high-temperature proton conductor that can be used as an intermediate-temperature electrolyte. The ionic conductivity of BaCeO$_3$ can further be improved by adding yttrium (0.01 S cm$^{-1}$ at 600 °C for 15–20% Y-doped BaCeO$_3$). However, it suffers from poor chemical stability [151]. Doped BaZrO$_3$, on the other hand, has strong chemical stability but it exhibits low conductivity at the intermediate temperature region [152]. Barison et al. studied the BaC$_{1-x-y}$Zr$_x$Y$_y$O$_3$–δ solid solutions prepared by the sol–gel Pechini method [153]. Their study showed that the solid solutions with Zr and Y content in the range of 20–40% and 15–20% provide the highest chemical stability with a suitable ionic conductivity (>10$^{-2}$ S cm$^{-1}$ at 600 °C). It should be noted that the dopant concentration should be carefully controlled because the excessive loading fractions of dopants may result in the formation of secondary phases that can deteriorate the electrolyte performance [154].

Salt-oxide based composites have also been investigated as the alternative low-cost electrolytes for the I-T SOFCs. For example, Tao et al. have studied the electrochemical performance of Li$_2$SO$_4$-Al$_2$O$_3$ electrolyte in H$_2$/O$_2$ fuel cells [155]. They reported a superionic conductivity behavior for Li$_2$SO$_4$-Al$_2$O$_3$ composite in H$_2$-containing atmosphere with an OCV and maximum current density about 1.2 V and 280 mA cm$^{-2}$, respectively, at 750 °C. However, the reaction between hydrogen and LiSO$_4$ in H$_2$-containing atmospheres deteriorates its long-term chemical stability. In another attempt, they used NaCl-Al$_2$O$_3$ composites as the electrolyte and the maximum current density was about 140 mA cm$^{-2}$ at 700 °C [156]. In another study, GDC-LiCl-SrCl$_2$ composites were investigated by Fu et al. with reporting the maximum conductivity, peak power density, and current density of these composites about 1.3 × 10$^{-1}$ S cm$^{-1}$, 510 mW cm$^{-2}$, and 1250 mA cm$^{-2}$, respectively measured at 650 °C [157]. Although other composite materials, such as GDC-YSZ, YDC-YSZ, SDC-LSGM, etc., have also been used as intermediate-temperature electrolytes, the measured values for the cell performance by these electrolytes were not high enough [78].

Bismuth oxide compounds with cubic fluorite structure exhibited one of the highest ionic conductivities at 800 °C (∼1 S cm$^{-1}$) due to their high oxygen vacancy concentration in δ-Bi$_2$O$_3$ [122]. However, the ionic conductivity of the bismuth-based composites decreases dramatically due to the δ→α phase transformation. Cations with small radii or high valences such as Y$^{3+}$ or Dy$^{3+}$ can hinder ions diffusion and stabilize the presence of δ-Bi$_2$O$_3$ phase at lower temperatures [158]. Some researchers used dual doping to improve the ionic conductivity of the bismuth-based composites. Due to the re-arrangement of dopants, oxygen ions, and vacancies, the dual doping approach can increase the entropy of the composite system by stabilizing the resulting crystal structure for lower temperature applications [138]. Among various types of dual-doped bismuth oxides, those doped with Dy-W and Sr-Nb have shown a relatively higher ionic conductivity (with 5.69 × 10$^{-1}$ S cm$^{-1}$ and 3 × 10$^{-1}$ S cm$^{-1}$ at 700 °C, respectively) [158,159]. Another challenging issue with bismuth oxides is the Bi$^{3+}$ to Bi$^{2+}$ reduction that may lead to high electronic conductivity of this system under reducing atmospheres [160]. Although some studies on W and Nb dual-doped system should an improvement in the stability of δ-phase in the bismuth-based system with a relatively lower impedance in reducing atmospheres, further investigations should be conducted to overcome the instability and decomposition of the bismuth oxide compounds [138].

Lanthanum gallate composites (LaGaO$_3$) with the general ABO$_3$ perovskite structure is another class of composites that have attracted great interest because of their high ionic conductivity in the intermediate temperature region. Doping the A and B sites with the
proper low-valent alkaline earth metal cations can enhance their ionic conductivity [161]. Strontium and magnesium have been widely used as the dopants in lanthanum gallate perovskite structured-electrolytes [78]. Lanthanum strontium gallium magnesium oxide composite (LSGM) was first introduced by Ishihara et al. [162] in 1994. Sr and Mg-doped lanthanum gallate exhibited the lowest solid solution energy amongst the dopants studied so far. Cu and Ni doping into Ga sites also showed low solid solution energy; however, they also pose electronic conductivity to the electrolyte [121]. It was found that Sr-doping up to 10 mol.% in La sites can greatly improve the ionic conductivity of LaGaO$_3$. However, strontium exhibited poor solubility in lanthanum sites and further doping (>10 mol.%) results in the formation of secondary phases that decrease the electrolyte performance [161]. Magnesium not only can be used for doping into Ga sites to generate additional oxide ions but also increase the Sr solubility to 20 mol.% [163]. LSGM composite has also been used as a promising electrolyte material in SOFCs due to its high ionic conductivity, minor electronic conductivity, and excellent chemical stability over a wide range of temperature and O$_2$ partial pressure (~1 to 10$^{-22}$ atm) [107,121]. The improved ionic conductivity of LSGM can be explained by the following defect chemistry equations [138]:

\[
2\text{MgO} + \text{La}_2\text{O}_3 \leftrightarrow 2\text{La}^{\text{Ga}}_\text{Ga} + 2\text{Mg}^{\text{Ga}} + 5\text{O}_\text{O} + V_\text{O} \quad (21)
\]

\[
2\text{SrO} + \text{Ga}_2\text{O}_3 \leftrightarrow 2\text{Sr}^{\text{La}}_\text{La} + 2\text{Ga}^{\text{Ga}} + 5\text{O}_\text{O} + V_\text{O} \quad (22)
\]

where $\text{Mg}^{\text{Ga}}$ stands for an Mg ion substituting Ga ion with a negative charge, $\text{La}^{\text{La}}_\text{La}$ indicates substituting La ion with a neutral charge, and $V_\text{O}$ indicates the formation of a vacancy on the oxygen site with a double positive charge. According to these equations, the ionic conductivity of the composite could be increased by increasing the structural oxygen concentration [138]. LSGM is considered as a proton conductor, oxygen ion conductor, and hybrid conductor (oxygen ion plus proton) in dry-oxygen, hydrogen-, and water vapor containing atmospheres, respectively [11]. Generally, doping A and B sites with lower valence cations generates oxygen vacancies and improves ionic conductivity [161]. Although it has been reported that Mg-site doping with transition metals such as nickel, cobalt, and iron increases the ionic conductivity of LSGM, it can also generate electronic conductivity, decrease reduction stability, and in some cases reduce ionic conductivity [7]. However, the instability of LSGMs under reducing atmospheres at high temperatures, high cost of Ga, the volatility of Ga at high temperatures, and its high reactivity with nickel and the other electronic constituents of the SOFC electrode composites are the major challenges with LSGM electrolytes which limit their application as a potential intermediate-temperature electrolyte [1,8,138,164]. High ionic conductivity of about 1.1 × 10$^{-1}$ S·cm$^{-1}$ at 800 °C was recorded for La$_{0.8}$Sr$_{0.2}$Ga$_{0.85}$Mg$_{0.15}$O$_{2.825}$ (LSGM) which is almost equal to that of GDC or SDC at the same temperature, but higher than YSZ at 1000 °C [165]. Some intermediate-temperature electrolytes and their ionic conductivity are listed in Table 2.
2.2.3. Low-Temperature Electrolytes

Since the electrolyte layer serves as the medium to transfer ions in a SOFC, its ionic conductivity and thickness, as well as electrical, chemical, and mechanical properties determine the durability, operating temperature, and overall performance of a fabricated cell [28,179]. Decreasing the electrode reaction resistance and electrolyte ohmic resistance are currently the main challenges for improving cell performance [122]. This section aims to provide a short review of the major advances and the state-of-the-art electrolytes proposed for low-temperature SOFCs in the last few years.

Ceria-Based Electrolytes

Recently, ceria-based compounds have attracted broad interest as low-temperature electrolytes [180]. Since the 1980s, ceria has been considered as one of the most promising candidates for energy applications. Although the fluorite structure of ceria is retained from room temperature to its melting point, it can release oxygen under a reducing atmosphere and transform into a group of CeO$_{2-\delta}$ compounds. Ceria-based electrolytes exhibit a relatively high ionic conductivity at the low-temperature region of SOFC operation [181]. Doped ceria shows noticeable electronic conduction at temperatures higher than 650 °C or in the environment with a reduced partial pressure of oxygen (low p(O$_2$)) [138]. Since the pure cerium oxide does not have a significant amount of O$^{2-}$ ions, the electrochemical performance of trivalent or sometimes bivalent cationic doped ceria is extensively studied in the literature [1,112,181]. Among all of them, gadolinia and samaria are known as the most effective dopants for ceria [107]. The main reason for the high ionic conductivity of Sm- and Gd-doped ceria can be explained using the concept of “critical ionic radius”. According to Kim, the ideal dopant should not change the lattice constant of the undoped ceria in overall [182]. Kim’s work showed that the critical ionic radius for an ideal trivalent dopant of ceria should be about 0.1038 nm, while the ionic radii of Sm$^{3+}$ and Gd$^{3+}$ are 0.1079 and 0.1053 nm, respectively. The small difference between the dopant and the host ionic size results in obtaining a relatively higher ionic conductivity compared to the other dopant with larger or smaller ionic radii [183]. In principle, the critical ionic radius becomes greater by increasing the valence number and ionic radii of the host cation [182].

Dual doping of ceria not only further improves its chemical stability but also increases its ionic conductivity [8]. In addition to the effective index and critical ionic radius concepts

| Material     | Fabrication Method          | Conductivity (S·cm$^{-1}$) | Temperature (°C) | Ref. |
|--------------|------------------------------|----------------------------|-----------------|------|
| GDC          | -                            | $1 \times 10^{-1}$         | 800             | [146]|
| Ce$_{0.80}$Sm$_{0.10}$O$_{1.90}$ | Pechini method              | $6.009 \times 10^{-3}$    | 650             | [147]|
| Ce$_{0.80}$Gd$_{0.17}$Pr$_{0.03}$O$_{1.90}$ | Spray-freezing/freeze-drying | $3.1 \times 10^{-2}$     | 750             | [166]|
| La$_{0.5}$Ba$_{0.5}$Si$_{1.5}$Al$_{0.5}$O$_{2.5}$ | Solid-state reaction        | $2.21 \times 10^{-2}$    | 800             | [167]|
| La$_{0.4}$Ba$_{0.6}$Si$_{0.6}$O$_{2.6}$ | Solid-state reaction        | $1.1 \times 10^{-1}$     | 750             | [168]|
| La$_{0.83}$Sr$_{0.17}$Fe$_{0.25}$O$_{2.66}$ | Mechanochemical activation | $2.04 \times 10^{-2}$    | 700             | [169]|
| La$_{10}$Sr$_{1.5}$Cu$_{1.5}$O$_{2.78}$ | Sol–gel                    | $4.8 \times 10^{-2}$     | 800             | [170]|
| La$_{10}$Sr$_{8.5}$Mg$_{0.2}$O$_{2.68}$ | Solid-state reaction        | $8.8 \times 10^{-2}$     | 800             | [171]|
| La$_{0.8}$Sr$_{0.2}$Mg$_{0.3}$O$_{2.64}$ | Solid-state reaction        | $7.4 \times 10^{-2}$     | 800             | [171]|
| La$_{0.53}$Sr$_{0.47}$Mg$_{0.3}$O$_{2.6}$ | Solid-state reaction        | $4.4 \times 10^{-2}$     | 800             | [172]|
| La$_{0.8}$Sr$_{0.2}$Ga$_{0.85}$Mg$_{0.15}$O$_{2.825}$ | Solid-state reaction       | $1.77 \times 10^{-1}$    | 800             | [173]|
| La$_{0.85}$Sr$_{0.15}$Ga$_{0.85}$Mg$_{0.15}$O$_{3-\delta}$ | Solid-state reaction       | $1.7 \times 10^{-1}$     | 800             | [174]|
| La$_{0.8}$Sr$_{0.2}$Ga$_{0.85}$Mg$_{0.15}$O$_{2.815}$ | Solid-state reaction       | $1.5 \times 10^{-5}$     | 900             | [175]|
| BaZr$_{0.8}$Y$_{0.2}$O$_{3-\delta}$ | Solid-state reaction       | $2.5 \times 10^{-2}$     | 800             | [176]|
| BaCe$_{0.9}$Y$_{0.1}$O$_{3-\delta}$ | Solid-state reaction       | $4.75 \times 10^{-2}$    | 800             | [177]|
| BaCe$_{0.85}$Sm$_{0.15}$O$_{3-\delta}$ | Solid-state reaction       | $2.391 \times 10^{-3}$   | 700             | [178]|

---

**Table 2.** The fabrication method, operating temperature, and ionic conductivity of low-temperature electrolytes.
discussed above, Yamamura et al. reported that dual doping results in suppressing the oxygen vacancies order and increasing configurational entropy, thereby it can decrease the activation energy and subsequently gain a greater total conductivity [184]. The configurational entropy ($S$) of double doped ceria with the general formula of $\text{Ce}_{1-x-y}\text{M}_x\text{M}_y\text{O}_{2-\delta}$ is higher than single doped ones and can be expressed as ($R$ = gas constant):

$$S = R[(1 - x - y) \ln(1 - x - y) + x \ln x + y \ln y]$$  \hspace{1cm} (23)

Wang et al. studied the ionic conductivity of Ca and Sm-doped ceria (SCDC) as well as $\text{La}_{0.6}\text{Sr}_{0.4}\text{Co}_{0.2}\text{Fe}_{0.8}\text{O}_{3-\delta}$ (LSCF)-SCDC composite [185]. Increasing Sm content linearly increases the lattice constant of the resulting composite. According to the concept of critical ionic radius, the ionic radii of $\text{Ca}^{2+}$ (0.1120 nm) and $\text{Sm}^{3+}$ (0.1219 nm) are larger than their critical ionic radiiuses (0.1038 and 0.1106 nm for $\text{Sm}^{3+}$ and $\text{Ca}^{2+}$, respectively), and hence the lattice constant of Sm- and Ca-doped ceria is increased with double doping. In this case, the ionic conductivity of doped ceria was affected by oxygen ion concentration and distribution, the difference between the ionic radii, and the configurational entropy of the resulting composite. The highest conductivity values measured for SCDC and LSCF-SCDC at 600 °C was about $3.9 \times 10^{-2}$ and $1.88 \times 10^{-1}$ S·cm$^{-1}$, respectively [185]. Kobi et al. prepared Nd and Y dual-doped ceria ($\text{Ce}_{0.80}\text{Nd}_{0.20-x}\text{Y}_x\text{O}_{1.9}$) by citrate/nitrate gel auto-combustion method [132]. The suppressed oxygen vacancy ordering and increased configurational entropy resulted in decreasing the conduction activation energy and thereby increasing ionic conductivity. The highest ionic conductivity of $\text{Ce}_{0.80}\text{Nd}_{0.20-x}\text{Y}_x\text{O}_{1.9}$ composite was recorded for the sample with the composition fraction of $x = 0.02$ ($1.2 \times 10^{-2}$ S·cm$^{-1}$ at 600 °C). Co-doping of ceria with Dy and Ca was studied by Tanwar et al. [186]. The electrolyte powders were similarly synthesized by the citrate–nitrate auto-combustion method. The order of oxygen vacancies changed by Dy and Ca co-doping, thus resulted in increasing the ionic conductivity ($\sim 1.45 \times 10^{-2}$ S·cm$^{-1}$ at 600 °C). Co-doped ceria may suffer from phase thermal instability. Several scholars have investigated the impact of temperature and the solid phase constituents on the long-term thermochemical stability of these materials. It has been reported that the use of appropriate dopants such as scandium can improve the thermal stability of the co-doped ceria composites. Controlled microstructure and morphology can also immensely improve the thermal stability of co-doped ceria [187–189]. Zheng et al. [182] fabricated La and Ca double-doped ceria by solid-state reaction method and investigated the effect of La and Ca addition on the performance of the electrolyte. Amongst various samples analyzed in this work, $\text{Ce}_{0.85}\text{La}_{0.10}\text{Ca}_{0.05}\text{O}_{2-\delta}$ showed the highest ionic conductivity of about $1.8 \times 10^{-2}$ S·cm$^{-1}$ at 600 °C. The high ionic conductivity of this work has been explained by obtaining a decreased lattice strain and proper distribution and concentration of oxygen vacancies in the crystal structure.

Concerning the above-mentioned advances in ceria-based low-temperature electrolytes, it can be concluded that ceria-based materials have great potential to be used as low-temperature SOFC electrolytes provided that the challenges of Ce$^{4+}$ to Ce$^{3+}$ reduction are eventually addressed. The ionic conductivity of some low-temperature electrolytes is shown in Figure 5.
Lytes, it can be concluded that ceria-based materials have great potential to be used as low-temperature SOFC electrolytes provided that the challenges of Ce\(^{4+}\) to Ce\(^{3+}\) reduction are addressed. The ionic conductivity of some low-temperature electrolytes is eventually addressed. The ionic conductivity of the 10Sc1CeSZ sample was 21 mS cm\(^{-1}\) at 600 °C. Kumar et al. developed CSSZ electrolytes comprising 10 mol.% scandia, 1 mol.% ceria, and 89 mol.% zirconia (Sc1CeSZ-10) via tape casting method [193]. The highest ionic conductivity of the 10Sc1CeSZ sample was 21 mS cm\(^{-1}\) at 600 °C. Kumar et al. investigated the effects of double doping, and dopant concentration on the electrochemical performance of scandia stabilized zirconia [194]. Different amounts of Gd, Yb, and Ce were co-doped into SSZ structure containing 9 mol.% scandia. Double-doped samples prevented cubic to rhombohedral phase transition and showed higher conductivity than the binary SSZ composites. Although the XRD analysis of the 1 mol.% Yb and Gd double-doped samples (1Yb-SSZ and 1Gd-SSZ) showed the formation of tetragonal phase and degradation of conductivity, the 2 mol.% doped samples (2Yb-SSZ and 2Gd-SSZ) showed the presence of a pure cubic phase. Due to the large ionic radius of Gd compared to Yb, Gd-containing samples showed lower conductivity than Yb-containing ones. The conductivity degradation in Yb and Gd containing samples has been ascribed by the formation of the tetragonal phase, which offers lower conductivity than the cubic phase SSZ. The Ce-doped samples exhibited the highest conductivity and phase stability among

![Figure 5. Ionic conductivity of various oxide electrolytes against temperature (ESB: Er\(_{0.4}\)Bi\(_{1.6}\)O\(_3\); DWSB: Dy\(_{0.08}\)W\(_{0.04}\)Bi\(_{0.88}\)O\(_1.56\); GDC: Gd\(_{0.1}\)Ce\(_{0.9}\)O\(_1.95\); SNDC: Sm\(_{0.075}\)Nd\(_{0.075}\)Ce\(_{0.85}\)O\(_3\); YSZ: Y\(_{0.16}\)Zr\(_{0.84}\)O\(_1.92\); LSGM: La\(_{0.8}\)Sr\(_{0.2}\)Ga\(_{0.8}\)Mg\(_{0.2}\)O\(_3\); LSGMC: La\(_{0.8}\)Sr\(_{0.2}\)Ga\(_{0.8}\)Mg\(_{0.115}\)Co\(_{0.085}\)O\(_3\); BCY: BaCe\(_{0.92}\)Y\(_{0.08}\)O\(_3\)) [190].]
the double-doped samples. The double-doped zirconia samples have also shown some extents of irregularity in the ionic conductivity and the activation energy values. This irregularity pattern has been explained by the reduced oxygen ion mobility that is caused in the double-doped structures by the increased vacancy concentration and the formation of short-ranged vacancy ordering.

Guo et al. studied the effect of alumina addition on the conductivity and mechanical strength of ceria and scandia-doped zirconia (Al-SCZ) [195]. The ionic conductivity of the Al-SCZ samples increased with increasing alumina content up to 0.5 wt.% due to the reduced grain boundary resistance and grain growth. A further increase in the alumina content of the samples resulted in a slight decrease in ionic conductivity. Moreover, alumina addition significantly improved the flexural strength of the electrolyte from 390 MPa for the alumina-free sample to 500 MPa for the Al-SCZ samples with 0.5 wt.% alumina loading fraction. According to the results of electrochemical and mechanical tests, the sample containing 0.5 wt.% alumina can be considered as a promising low-temperature electrolyte.

Barium zirconate with a perovskite structure has also been investigated for its potential application as a SOFC electrolyte. Ding et al. [175] prepared yttrium-doped barium zirconate (BaZr$_{0.8}$Y$_{0.2}$O$_{3-δ}$) through the conventional solid-state reaction. The BaZr$_{0.75}$Y$_{0.25}$O$_{3-δ}$ samples showed the highest conductivity of about 8 × 10$^{-5}$ S·cm$^{-1}$ at 600 ºC. Yun et al. developed BaZr$_{0.75}$Y$_{0.25}$O$_{3-δ}$ low-temperature electrolytes via solid-state reactive sintering method [196]. The sample sintered at 1485 ºC (for 15 hours) showed the highest conductivity of 3 × 10$^{-3}$ S·cm$^{-1}$ at 600 ºC under a reducing atmosphere. Peng et al. [197] synthesized Zn and Y co-doped barium zirconate and reported high conductivity of 33.1 S·cm$^{-1}$ at 600 ºC under a neutral atmosphere. Zue et al. fabricated Ce, and Y doped BaZrO$_3$ and studied the chemical stability and conductivity of Ba(2Zr$_{0.75}$Y$_{0.25}$)O$_{3-δ}$ (BZCY7) under CO$_2$ + H$_2$ containing atmosphere. BZCY7 was stable at 500 ºC under a reducing atmosphere due to the presence of Ce in the structure of BZCY7. The maximum ionic conductivity measured for this sample was about 9 × 10$^{-3}$ S·cm$^{-1}$ at 500 ºC. From the discussion above it can be seen that the ionic conductivity of the zirconia-based electrolyte is relatively low, which may not be ideal for fabrication of a robust L-T SOFC; however, their excellent thermochemical stability and mechanical strength still reserve some potential applications for these compounds as the possible material for further research in this category.

**ZnO-Based Electrolytes**

Zinc oxide is a semiconductor material with a wide bandgap that has been known as a potential oxygen ion and proton conductor with excellent oxidation resistance and thermal stability [198]. It has been reported that the ionic conductivity of YSZ at 800 ºC improved by about 120% by adding 0.5 wt.% ZnO [153]. Due to the easy ionization of hydrogen to protons in oxide lattice, Norby [199] claims that protons may be present in zinc oxide and doped zinc oxide. Protons have high mobility in oxide lattices, and if the concentration of protons formed form the ionization of hydrogen is high enough, they can affect the defect-dependent properties and improve the proton conductivity of zirconia [199]. Xia et al. [141] fabricated ZnO and ZnO-La/Pr-doped ceria (ZnO-LCP) composites and evaluate cell performance in the range of 450–550 ºC. ZnO samples were prepared via the pre-sintering of commercial ZnO at 650 ºC. For the synthesis of ZnO-LCP samples, La$_{0.33}$Ce$_{0.62}$Pr$_{0.05}$O$_{2-δ}$ powder was first prepared by thermal treatment of a mixture of lanthanum, cerium, and praseodymium carbonates at 800 ºC, followed by blending the prepared powder with ZnO and calcination of the resulting mixture at 800 ºC (for 2 h). The obtained OCV for the fabricated cells using ZnO and ZnO-LCP electrolyte was about 482 and 540 mW·cm$^{-2}$, respectively. Figure 6 shows the electrochemical performance of these samples at various temperatures. The ionic conductivity measured for the ZnO electrolyte at 475 ºC and 550 ºC was about 3.7 × 10$^{-2}$ S·cm$^{-1}$ and 9 × 10$^{-2}$ S·cm$^{-1}$, respectively. The ZnO-LCP electrolytes comparably exhibited boosted ionic conductivity at 475 ºC and 550 ºC with about 8.2 × 10$^{-2}$ S·cm$^{-1}$ and 1.56 × 10$^{-1}$ S·cm$^{-1}$, respectively. Since the activation energy
for ionic conduction was smaller than that of oxygen ion conduction, it was concluded that the zinc oxide-based electrolytes may offer both oxygen ion and proton conductivity. To verify the presence of proton conductivity, an O$^{2-}$-blocking fuel cell configuration was employed, and according to the results, the proton conductivity of the ZnO electrolyte at 550 °C was about 5 × 10$^{-2}$ S·cm$^{-1}$ [141]. Qiao et al. [13] studied the electrical and electrochemical properties of LCP-ZnO composite fabricated by a solid-state blending method. Among various LCP-ZnO composites with different LCP to ZnO weight ratios, the 7LCP-3ZnO sample showed the highest power density and ionic conductivity of about 1055 mW·cm$^{-2}$ and 2.9 × 10$^{-1}$ S·cm$^{-1}$ at 550 °C, respectively. The high electrochemical performance of 7LCP-3ZnO was explained using the triple conductivity concept, denoting the parallel function of oxygen (O$^{2-}$), proton conduction (H$^+$), and interfacial conduction in the complex composites [13]. For the SOFCs fabricated by these composites, obtaining a proper semiconductor to ionic-conductor ratio plays an important role in optimizing the overall cell efficiency [200].

![Figure 6. Electrochemical performance of low-temperature SOFC with ZnO and ZnO-LCP electrolytes at different temperatures [141].](image)

Xia et al. [73] prepared BaCo$_{0.7}$Zr$_{0.1}$Yb$_{0.1}$O$_{3-δ}$ (BCZY), BaCo$_{0.7}$Zr$_{0.1}$Y$_{0.2}$O$_{3-δ}$ (BCZY), and BaCo$_{0.4}$Fe$_{0.4}$Zr$_{0.1}$Y$_{0.1}$O$_{3-δ}$-ZnO (BCFZY-ZnO) composites by a dry processing method and investigated the possible hybrid H$^+$/O$^{2-}$ conductivity as well as the electrochemical performance of the electrolytes. The high conductivity of the electrolyte samples was explained to be attributed to the high interfacial ionic conduction caused by the effect of the p-n junction at the so-called “heterophasic” interfaces. The electrolyte samples fabricated by BCFZY-ZnO showed a relatively higher performance than that of the BCZY composites containing the above electrolyte constituents.

Ma et al. [201] prepared GDC-KAILZn composites via solid-state thermal pyrolysis of the mixture of GDC, K$_2$CO$_3$, Al(NO$_3$)$_3$·9H$_2$O, and Zn(NO$_3$)$_2$·6H$_2$O at 800 °C. Thermal pyrolysis was chosen by the authors due to the potential of the method to produce the final electrolyte with small grain size and high specific surface area. Introducing the carbonate phase to GDC electrolytes could improve the ionic-conductivity of the grain-boundary interfaces [201]. However, adding the insulating alumina phase decreased the electrical conductivity of the fabricated electrolyte [202]. Furthermore, the addition of KAILZn to GDC resulted in suppressing Ce$^{4+}$ to Ce$^{3+}$ reduction, enhancing the chemical stability of the electrolyte, and improving the electrochemical performance of the fabricated
The high conductivity of these low-temperature composites has been attributed to the high cell efficiency at low temperatures due to their superionic conductivity behavior [203,204]. Carbonate-oxide composites, with triple $O^{2-}$–$H^+$–$CO_3^{2-}$ conductivity, have been recently investigated for their potential application in the fabrication of low-temperature electrolytes [205]. The anode and cathode reactions of the carbonate-containing composite electrolyte can be classified into three separate categories, as follows [121]:

\[
\begin{align*}
\text{Cathode half cell reaction} : & \quad \frac{1}{2}O_2 + 2e^- \leftrightarrow O^{2-} \\
\text{Anode half cell reaction} : & \quad H_2 + O^{2-} \leftrightarrow H_2O + 2e^- \quad (O^{2-} \text{ ion – conducting})
\end{align*}
\]

\[
\begin{align*}
\text{Cathode half cell reaction} : & \quad \frac{1}{2}O_2 + 2H^+ + 2e^- \leftrightarrow H_2O \\
\text{Anode half cell reaction} : & \quad H_2 \leftrightarrow 2H^+ + 2e^- \quad (H^+ \text{ ion – conducting})
\end{align*}
\]

\[
\begin{align*}
\text{Cathode half cell reaction} : & \quad \frac{1}{2}O_2 + CO_2 + 2e^- \leftrightarrow CO_3^{2-} \\
\text{Anode half cell reaction} : & \quad H_2 + CO_3^{2-} \leftrightarrow 2H_2O + CO_2 + 2e^- \quad (CO_3^{2-} \text{ ion – conducting})
\end{align*}
\]

In principle, the dissociation of $CO_3^{2-}$ to $CO_2$ and $O^{2-}$ could result in an increase in the oxygen ion transfer efficiency, which can be further boosted by increasing the carbonate content of the composite [206]. The reason for the high performance of carbonate-oxide composites is their tendency for redistribution of ions which results in the formation of highly conductive interfaces in the SOFC electrolytes [207]. At temperatures higher than the glass transition temperature of the carbonate phase, a glassy phase forms that could cover the inter-spaces of the electrolyte as a thin film and hence it increases the density of the electrolytes. However, when the operating temperature decreases to below the glass transition temperature of the carbonate phase, it coagulates with a lower density [208]. The high conductivity of these low-temperature composites has been attributed to the formation of space charge zones in the interfacial regions, which contain higher defects concentration than the bulk. At temperatures higher than the glass transition temperature of the carbonate phase, mobility of the ions increases and results in a superionic conduction behavior in the electrolytes [208,209]. Wang et al. [204] have explained that above the glass transition temperature, the increased rotation and mobility of $CO_3^{2-}$ group in addition to the enhanced C–O bond vibration could facilitate the formation of hydrogen bonds, and hence the carbonate phase serves as a bridge for the migration of protons among the hydrogen bonds.

Amongst the ceramic–carbonate composite, doped ceria–carbonate composites have been extensively investigated in the past few years. Zhao et al. [206] studied the effect of carbonate content on the performance of SDC-Na$_2$CO$_3$ composite. The results showed that the total conductivity of the SDC-Na$_2$CO$_3$ composite is increased by increasing the $CO_3^{2-}$ content. Similar observations were reported for SDC-(Li$_2$CO$_3$-Na$_2$CO$_3$) composites [207] with a power density of 605 mW·cm$^{-2}$ and 817 mW·cm$^{-2}$ at 500 °C and 600 °C, respectively. The highest ionic conductivity in the temperature region of 400–600 °C was about $3 \times 10^{-2}$–2.6 $\times 10^{-2}$ S·cm$^{-1}$. Raza et al. [210] synthesized calcium and samarium dual doped ceria-Na$_2$CO$_3$ composite (Ce$_{0.8}$Sm$_{0.2}$–$\delta$Ca$_x$O$_2$–$\delta$–Na$_2$CO$_3$) via co-precipitation synthesis route.
and recorded high power density and OCV of 1000 mW·cm$^{-2}$ and 1.05 V at 560 °C, respectively. Chockalingam and Basu [180] fabricated GDC-(Li/Na)$_2$CO$_3$ composites through the co-precipitation method. The resistance of the samples decreased with increasing carbonate content up to 30 wt.% and the sample containing 25 wt.% carbonate phase possessed the highest ionic conductivity of 1.75 × 10$^{-1}$ S·cm$^{-1}$ at 550 °C. Zhang et al. [209] investigated the effect of Gd and Y co-doping on the total conductivity of Ce$_{0.8}$Gd$_{0.05}$Y$_{0.15}$O$_{1.9-40}$ wt.% carbonate (52 mol.% Li$_2$CO$_3$ and 48 mol.% Na$_2$CO$_3$) composites. The highest conductivity for this composite was 1.8 × 10$^{-1}$ S·cm$^{-1}$ at 500 °C. The conductivity of LSGM-(Li/Na)$_2$CO$_3$ composite was investigated by Wu et al. [211]. The composite showed triple ion conductivity behavior similar to the other carbonate–oxide composites with the highest ionic conductivity of 1.2 × 10$^{-1}$ S·cm$^{-1}$ at 500 °C. Zhu et al. [212] prepared mixed lanthanum, cerium, and praseodymium carbonates (LCP–carbonates) and reported a maximum power density of about 600 mW·cm$^{-2}$. Other doped ceria–carbonate composites such as SDC–Li$_{0.6}$Na$_{0.4}$CO$_3$ [213] and SDC–(Li/Na/K)$_2$CO$_3$ [112] have also been investigated to determine the effect of different carbonates and their concentration on the electrochemical performance of the composite electrolytes. According to the ionic conductivity of the carbonate-containing electrolytes, the triple conductive composites exhibit the highest electrochemical performance; however, durability and cost are recognized as the key barriers for commercialization of these materials for L-T SOFCs, which are subjected to further research and development.

Apatite-Structured Electrolytes

Apatite-based electrolytes with the general formula of A$_{10}$(BO$_4$)$_6$×2+y (where A is a rare-earth or alkaline earth metal, B is P, Si, Al, Ga, or Ge, and X is O, OH, CO$_3$, or F) have attracted growing attention [9,36,164,167,168,214–216]. These materials have a hexagonal crystal structure with minimal activation energy and a very open structure [136]. Nakayama et al. [217] fabricated RE$_{10}$Si$_6$O$_{27}$ (RE = La, Pr, Nd, Sm, Gd, Dy) ceramics via a solid-state reaction method and studied their conductivity. They concluded that the ionic conductivity increased with an increasing RE$^{3+}$ ionic radius. Due to their open structure, apatites are flexible with extensive aliovalent doping. Increasing the ionic radius of A$^{3+}$ cations enhances the ionic conductivity and decreases the activation energy of a typical apatite composite. Although fully stoichiometric apatites have poor ionic conductivity, A-site deficiency can improve their conductivity by displacing anions from their original site to new interstitial sites and creating vacancies [218]. Despite the ionic conduction behavior in the fluorite- and perovskite-based materials (in which oxygen vacancies are responsible for ionic conduction), the ionic conductivity in the apatite-structured electrolytes is dominated by the interstitial oxide ions migration with a sinusoidal pathway. The nonstoichiometric degree of anions and cations, together with the dopants chemical nature, were found to significantly affect the ionic conductivity of apatites [48].

Yoshioka [172] studied the effect of different dopants and La deficiency on the ionic conductivity of apatite-structured lanthanum silicates (La$_{10}$Si$_6$O$_{26}$). In non-doped compounds, the ionic conductivity was increased with increasing La content. It was found that the La vacancies were filled with La ions and resulted in the formation of excess oxide ions. Thus, the excess oxide ions boosted the ions migration in the conduction channel and improved the ionic conductivity [172,218]. Similar behavior was observed for the Sr- and Nd-doped samples. However, due to the absence of La deficiency, the ionic conductivity of fully stoichiometric compounds such as La$_8$Sr$_2$Si$_6$O$_{26}$ was much lower than that of La-deficient ones such as La$_{0.33}$Si$_6$O$_{26}$. In Al-containing samples, the ionic conductivity increased with increasing Al content up to 1.2 mol.% and Further Al doping decreased ionic conductivity [172]. It has been reported that excessive Al or Ga doping into Si sites reduces La vacancies and forms a fully stoichiometric compound [173]. Doping Mg into Si sites poses a more significant effect on the ionic conductivity than Al doping, even at lower Mg content. The increased ionic conductivity was related to the increasing channel size of the O$_3$ triangle, distances of Si–O bond, and lattice parameter.
Among these samples, $\text{La}_{9.533}(\text{Si}_{5.7}\text{Mg}_{0.3})\text{O}_{26}$ had the highest ionic conductivity of about $7.4 \times 10^{-3} \text{ S cm}^{-1}$ at 500 °C [172]. Najib et al. [219] also investigated lanthanum-silicate apatites with Sr and Ge doping into La and Si sites, respectively. Excess oxygen resulted in higher ionic conductivity; however, the samples with interstitial oxide ions showed higher ionic conductivity than the samples with oxygen vacancies. Amongst the La-site and Si-site doped samples, $\text{LaBaSi}_{5.265}\text{O}_{26.5}$ and $\text{La}_{10}\text{Si}_{5}\text{Ga}_{0.5}\text{O}_{26.5}$ possessed the highest ionic conductivity of $6.6 \times 10^{-3}$ and $6.6 \times 10^{-3}$ at 500 °C, respectively [219]. Despite the recent progress in apatite-structured electrolytes, their commercialization has been hindered because of their complicated processing and low ionic conductivity [220].

Bismuth-Based Electrolytes

Bismuth oxide has six crystallographic polymorphs as follows:

- $\alpha$-$\text{Bi}_2\text{O}_3$ with monoclinic crystal structure;
- $\beta$-$\text{Bi}_2\text{O}_3$ with tetragonal crystal structure (fluorite);
- $\delta$-$\text{Bi}_2\text{O}_3$ with face-centered cubic crystal structure (FCC);
- $\gamma$-$\text{Bi}_2\text{O}_3$ with body-centered cubic crystal structure (BCC);
- $\omega$-$\text{Bi}_2\text{O}_3$ with triclinic crystal structure;
- $\varepsilon$-$\text{Bi}_2\text{O}_3$ with orthorhombic crystal structure.

The room temperature $\alpha$-$\text{Bi}_2\text{O}_3$ phase transforms into $\delta$-$\text{Bi}_2\text{O}_3$ upon heating to above 729 °C. $\delta$-$\text{Bi}_2\text{O}_3$ is stable up to its melting point (824 °C). During cooling, $\delta$-$\text{Bi}_2\text{O}_3$ transforms into either $\beta$-$\text{Bi}_2\text{O}_3$ at 650 °C or $\gamma$-$\text{Bi}_2\text{O}_3$ at 639 °C. While $\beta$-$\text{Bi}_2\text{O}_3$ transforms into $\alpha$-$\text{Bi}_2\text{O}_3$ at 303 °C, $\gamma$-$\text{Bi}_2\text{O}_3$ can be stable down to room temperature by using a very slow cooling rate [221,222]. $\delta$-$\text{Bi}_2\text{O}_3$ has been known to have high $\text{O}^{2-}$ ionic conductivity owing to its high concentration of intrinsic oxygen vacancies (25%) [223]. However, it is unstable at temperatures below 729 °C, and the $\delta \rightarrow \alpha$ transformation results in decreasing conductivity intermitently. Several scholars have been focusing on stabilizing the $\delta$-phase at lower temperatures. Doping rare earth oxides into the fluorite structure of $\delta$-$\text{Bi}_2\text{O}_3$ can stabilize it even at room temperature [224]. Verkerk et al. [225] claimed that $\delta$-$\text{Bi}_2\text{O}_3$ can be stabilized by doping cations with smaller ionic radii than $\text{Bi}^{3+}$. Some other studies showed that co-doping can stabilize the $\delta$-$\text{Bi}_2\text{O}_3$ phase with much lower dopant concentration because of the remarkable increase in the entropy of the resulting composite [223].

Jung et al. [223] studied the phase stability and conductivity of Tb and W dual-doped bismuth oxide (TWSB) prepared by the conventional solid-state reaction method. They found that pure $\delta$-$\text{Bi}_2\text{O}_3$ was only formed in the sample containing 25 mol.% Tb (25TSB) among the Tb-doped bismuth oxide. The addition of the second dopant (W) resulted in dropping the total Tb content needed for stabilizing the $\delta$-$\text{Bi}_2\text{O}_3$. The XRD analysis of the samples containing 8 mol.% Tb and 4 mol.% W (8T4WSB) as well as the sample containing 10 mol.% Tb and 5 mol.% W (10T5WSB) showed the formation of pure $\delta$-$\text{Bi}_2\text{O}_3$ in these samples. However, the 25TSB sample had better long-term stability of ionic conductivity compared to the dual-doped samples. Furthermore, the TWSB experienced an order–disorder transition as well as the possible formation of a non-crystalline phase which decreased its crystallinity [226]. They concluded that despite the higher initial ionic conductivity of the TWSB sample, the TSB sample exhibited better long-term ionic conductivity stability [224].

In another attempt, Dy- and W-doped bismuth oxides were developed by Jung et al. [159] and the effects of dopant concentration on the ionic conductivity and phase stability of the samples were studied. Dy and W selection was based on their ionic radii and dielectric polarizability. The dopant content and the ratio of dopants can greatly affect the purity of the bismuth oxide and the higher Dy: W ratio results in more $\delta$ phase stability. The highest conductivity of $6.6 \times 10^{-2} \text{ S cm}^{-1}$ at 500 °C was observed for the sample containing 10 mol.% Dy and 5 mol.% W (10T5WSB). Dysprosium and tantalum dual-doped $\text{Bi}_2\text{O}_3$ electrolytes were also investigated by Cardenas-Terrazas et al. [227]. According to the results, the highest ionic conductivity belonged to the electrolyte comprising 13 mol.% Dy and 2 mol.% Ta (0.08 S cm$^{-1}$ at 500 °C). Jung et al. also fabricated Gd- and Dy-doped
Bi$_2$O$_3$ (DGSB) and found that the sample containing 8 mol.% Dy and 4 mol.% Gd (8D4GSB) had suitable long-term phase stability and showed the highest ionic conductivity.

Among all of the above-mentioned low-temperature electrolytes, it seems that the ZnO-based ones (e.g., 3ZnO-7LCP composite) could offer the highest power density and ionic conductivity at the lower range of the L-T region. The ceria–molten carbonate composites could also provide a high ionic conductivity, comparable to the zinc oxide electrolytes in the cases with hybrid conductivities. Table 3 summarizes some of the latest results of ionic conductivities obtained for the low-temperature electrolytes.

**Table 3.** The fabrication method, operating temperature, and ionic conductivity of low-temperature electrolytes.

| Material | Fabrication Method | Conductivity ($\text{S}\cdot\text{cm}^{-1}$) | Temperature ($^\circ\text{C}$) | Ref. |
|----------|--------------------|------------------------------------------|-------------------------------|------|
| SCDC     | Co-precipitation   | $3.9 \times 10^{-2}$                     | 600                           | [185]|
| LSCF-SCDC| Co-precipitation   | $1.88 \times 10^{-1}$                    | 600                           | [185]|
| SDC-(Li/Na/K)$_2$CO$_3$ | Co-precipitation | $-0.7 \times 10^{-1}$                   | 550                           | [112]|
| SDC-(35 wt.% lithium-sodium carbonate) | Solid-state reaction | $1.4 \times 10^{-1}$                  | 550                           | [203]|
| SDC-(lithium-potassium carbonate) | Solid-state reaction | $7 \times 10^{-2}$                    | 550                           | [213]|
| SDC-Na$_2$CO$_3$ | Solid-state reaction | $-7 \times 10^{-2}$                    | 550                           | [204]|
| GDC-25 wt.% (Li-Na)$_2$CO$_3$ | Co-precipitation | $1.757 \times 10^{-1}$                 | 550                           | [180]|
| GDC-40 wt.% (Li-Na)$_2$CO$_3$ | Simple one-step dry-processing | $1.8 \times 10^{-1}$              | 500                           | [209]|
| LSGM-(Li/Na)$_2$CO$_3$ | Polyacrylamide gel combustion process | $-1.2 \times 10^{-1}$ | 600 | [211]|
| Ce$_{0.83}$Sm$_{0.17}$O$_2$-Na$_2$CO$_3$ | Tape casting and hot press | $1 \times 10^{-1}$ | 350 | [228]|
| Ce$_{0.83}$Sm$_{0.17}$O$_2$-Na$_2$CO$_3$ | Citrate complexation process | $1.8 \times 10^{-2}$ | 600 | [229]|
| Ce$_{0.83}$Sm$_{0.17}$O$_2$-Na$_2$CO$_3$ | Citrate/nitrate gel auto-combustion | $1.28 \times 10^{-2}$ | 600 | [132]|
| Ce$_{0.83}$Sm$_{0.17}$O$_2$-Na$_2$CO$_3$ | Citrate/nitrate gel auto-combustion | $1.28 \times 10^{-2}$ | 600 | [132]|
| Ce$_{0.83}$Sm$_{0.17}$O$_2$-Na$_2$CO$_3$ | Citrate/nitrate gel auto-combustion | $1.43 \times 10^{-2}$ | 600 | [186]|
| Ce$_{0.83}$Sm$_{0.17}$O$_2$-Na$_2$CO$_3$ | Solid-state reaction | $-1.8 \times 10^{-2}$ | 600 | [150]|
| Ce$_{0.83}$Sm$_{0.17}$O$_2$-Na$_2$CO$_3$ | Solid-state thermal pyrolysis | $6 \times 10^{-2}$ | 580 | [201]|
| Bi/Gd co-doped ceria | Sol-gel combustion synthesis | $1.29 \times 10^{-2}$ | 600 | [189]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Sol-gel | $1.44 \times 10^{-2}$ | 600 | [148]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Tape casting | $2.1 \times 10^{-2}$ | 600 | [193]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Combustion | $-1.1 \times 10^{-2}$ | 600 | [194]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Solid-state reaction | $9 \times 10^{-3}$ | 500 | [230]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Solid-state reaction | $9 \times 10^{-2}$ | 550 | [141]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Solid-state reaction | $1.56 \times 10^{-1}$ | 550 | [141]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Sol-gel | $2.9 \times 10^{-1}$ | 550 | [13]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Sol-gel | $5.8 \times 10^{-3}$ | 500 | [172]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Sol-gel | $7.4 \times 10^{-3}$ | 500 | [172]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Sol-gel | $6.6 \times 10^{-3}$ | 500 | [172]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Sol-gel | $6.6 \times 10^{-3}$ | 500 | [219]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Sol-gel | $2.4 \times 10^{-3}$ | 500 | [219]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Solid-state reaction | $3 \times 10^{-3}$ | 500 | [231]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Solid-state reaction | $8 \times 10^{-2}$ | 500 | [227]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Solid-state reaction | $6.34 \times 10^{-2}$ | 500 | [223]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Solid-state reaction | $9.8 \times 10^{-2}$ | 500 | [159]|
| Bi$_{0.30}$Ce$_{0.70}$O$_{2-\delta}$ | Solid-state reaction | $8 \times 10^{-2}$ | 500 | [227]|

### 3. Modern Low-Temperature SOFC Electrodes and Interconnects

#### 3.1. Electrode and Current Collectors’ Prospects

In addition to the electrolyte, lowering the operating temperature of other individual layers, namely, anode, cathode, and current collector should also be considered for successful deployment of the low-temperature SOFCs. While achieving higher ionic conductivity without increasing the ohmic resistance is the main goal for lowering the operating temperature of the electrolyte, improving O$_2^-$ diffusion properties and reducing the ohmic losses are the main targets for the electrodes. Below, the general characteristics of the electrodes and the current collector would be presented.
3.1.1. Choice of Anodes

Catalyzing the mobility of the ions through the electrolyte, oxidation of the fuel, and conducting electrons to the external circuit are the most important roles of the anode in SOFCs [232]. Reducing anode polarization losses is one of the most important issues with anode materials in the L-T SOFCs [190]. In addition, a suitable anode for L-T region should offer a high porosity, balanced ionic and electronic conductivity, excellent chemical stability, inertness towards the other adjacent layers, and matching TEC with the other cell components. The smaller the particle size, the less surface coefficient resistance and thereby higher electrode–electrolyte interface adherence [232]. It has also been reported that the electrical conductivity of the electrode should be greater than 1 S cm⁻¹ [232].

Iron-based anodes suffer from iron corrosion which results in degradation of the anode and hindering its long-term application. Co-based anodes are among the most stable ones, however, their carbon deposition issue with hydrocarbon fuels and the relatively high cost of cobalt are listed as the main drawback of these anodes. Ni-based anodes have some serious problems with degradation, low chemical stability against sulfur-based fuels (such as hydrogen sulfide), and mechanical breakage [233]. In this context, Cu-based electrodes have received particular attention [234]. Shaheen et al. [232] fabricated Cu₀.₂Sr₀.₅ (CS) and La₀.₂Cu₀.₄Sr₀.₄ (LCS) nanocomposites electrodes via the Pechini method and reported that the symmetrical cells, namely, CS/LSGM/CS and LCS/LSGM/LCS (LSGM as electrolyte) could overcome the mechanical and thermochemical stability issues listed above. Among the CS and LCS electrodes, the LCS nanocomposite exhibited higher electrical conductivity and power density with about 4.7 S cm⁻¹ and 782 mW cm⁻² at 600 °C. Raza et al. [235] reported a high output power of about 1000 mW cm⁻² at 550 °C for Cu₀.₂Zn₀.₈ anode prepared by solid-state reaction between ZnNO₃ and CuCO₃. Batool et al. [236] fabricated hierarchical rod-like BaCuNiZn oxide (BCNZ) anode material through the sol–gel method and reported a higher electrical conductivity of about 10.4 S cm⁻¹; however, the power density was lower than that of Shaheen et al., even at 650 °C (~350 mW cm⁻²).

Another class of low-temperature anode material is Ni- and Zn-based composites which have attracted a considerable interest during the past decade. Zinc oxide is a semiconductor at lower temperatures [237]. Nickel has been reported to have two roles in ZnO: first, it significantly increases the electronic conductivity of the resulting composite and hence it decreases the polarizations losses in the cathode and anode layers. Second, in ZnO-NiO nanocomposite, the high dispersion of NiO in ZnO can improve the chemical stability of the ZnO phase in the composite and enhance the catalytic activation of the anode [238,239]. It has also been reported that the mixed Ni-based composites have high resistance against sulfur poisoning and carbon deposition [240]. Raza et al. [241] studied the concept of mixed conductor electrodes which can simultaneously be used as anode and cathode. They prepared the ZnO-NiO nanocomposite electrodes which have both electronic and oxygen ion conductivity. According to the XRD result of the ZnO-NiO/SDC-Na₂CO₃ cell (SDC-Na₂CO₃ as the electrolyte), no chemical reactions were recorded between the layers. The Zn:Ni molar ratio has been reported to have a great impact on the power density of the electrodes. The optimum Zn:Ni ratio was about 9:12 and the highest power density at this ratio was 1257, 1107, and 840 mW cm⁻² at 520, 500, and 480 °C, respectively. However, the low conductivity is a major drawback of this system. In another attempt [237], they investigated the electrochemical performance of the Zn₀.₆Fe₀.₄Cu₀.₃-GDC mixed conductor electrodes. The highest power density of this electrode was about 1 W cm⁻² at 570 °C (fuel: H₂). However, the conductivity of this electrode was lower than the previous one. The other Cu and Zn oxide-containing anodes investigated in literature include Ni₀.₆Zn₀.₄O₂₋₅-GDC nanocomposite (with the output power density of about 820 and 548 mW cm⁻² at 600 °C using hydrogen and biogas fuel, respectively) [242] and Cu₀.₁₆Ni₀.₇Zn₀.₃₇Ce₀.₁₆Gd₀.₀₄O (with the electrical conductivity and power density of about 4.14 S cm⁻¹ 570 mW cm⁻² at 550 °C, respectively) [243].
Perovskite-based materials have also been of interest by several researchers. Hussain et al. [244] focused their research on the discovery of new oxide perovskite-based low-temperature anodes. Recently, they employed tape-casting and infiltration routes to prepare \( \text{FeO}_2\text{CO}_3\text{MoO}_4\text{O}_3\) (SFCM)-Ce\(_{0.9}\)Gd\(_{0.1}\)O\(_2\) (GDC) composites as a new redox-stable perovskite-based anode material. The OCV and power density of this composite anode under the H\(_2\) atmosphere were about 0.9 V and 500 mW cm\(^{-2}\). \( \text{Y}_{0.7}\text{Ca}_{0.3}\text{Cr}_{1-x}\text{Cu}_x\text{O}_{3-\delta} \) (YCC) is another anode material in this category which was prepared by Hussain et al. [245] through a solid-state reaction method followed by infiltration (Fuel: humidified hydrogen). YCC is an MIEC material which showed high conductivity at low temperature as well as low degradation rate (0.015 V·kh\(^{-1}\) under 0.2 A·cm\(^{-2}\)) and high chemical stability in reducing and oxidizing atmospheres. Despite the high power density of this anode (~1.2 W·cm\(^{-2}\) at 600 °C), its conductivity was not as high enough (2.7 and 1.2 S·cm\(^{-1}\) at 650 and 450 °C). They also studied the electrochemical performance of YCr\(_{3-\delta}\) infiltrated by Ni-GDC electrocatalyst with H\(_2\)/3%H\(_2\)O as fuel [246] and Ba\(_{0.98}\)La\(_{0.02}\)SnO\(_3\) [247], etc.; however, the maximum power density of these anodes was not as high as the previous ones. Wang et al. [248] studied the effect of inject-printing infiltration on the electrochemical performance of Ni-Gd:CO\(_2\) anodes at different temperatures. They reported that GDC nano-decoration percolated by the impregnation of GDC with NiO-GDC composite, could result in obtaining a higher TPB spatial density, and thereby reduce the ASR of the sample (Figure 7). The presence of nano-engineered scaffold and faster reaction sites resulted in a relatively lower OCV (~9 × 10\(^{-2}\) V) and ASR (1.36 × 10\(^{-1}\) Ω·cm\(^{-2}\)) [248].

![Figure 7. The Area Specific Resistance (ASR) as a function of temperature for the NiO-GDC anodes without and with 12 infiltration cycle [248].](image)

Other candidates, such as tungsten oxide infiltrated composite WC\(_u\)-ScYSZ (WCS) [249], nickel-ceria infiltrated Nb-doped strontium titanate [250], Pt, Pd, Ni, and Ru-GDC infiltrated strontium titanate [251], Sr\(_{0.2}\)Na\(_{0.8}\)Nb\(_{1-x}\)V\(_x\)O\(_3\) [252], GDC nanocube–NiO composites [253], etc., have also been studied in detail; however, their power density was below 500 W·cm\(^{-2}\), which needs further development to be appropriate for the fabrication of L-T SOFCs. The development of more robust anode material for the L-T SOFCs is a hot and ongoing field of investigation by the research community in order to achieve stable composites with a higher power density and lower polarization loss.
3.1.2. Choice of Cathodes

The cathodic polarization resistance is one of the most challenging issues for lowering the operating temperature of the SOFC cathodes [107]. To prevent posing undesirable thermo-mechanical stresses to the electrode, the suitable thermal expansion coefficient value of the SOFC cathode has been reported to be in the range of $10 \times 10^{-6}$–$12.5 \times 10^{-6}$ K$^{-1}$ [107]. An ideal SOFC cathode should also provide high phase stability, high electronic conductivity, and minimal ohmic losses [215]. Since the electrocatalytic reactions of cathode and anode are thermally activated, lowering the operating temperature results in an increase in the electrode overpotential. Furthermore, due to the considerable activation energy required for oxygen dissociation at the cathode surface, the reduced operating temperature could significantly decrease the electrochemical performance of the cathode [190].

La$_{1-x}$Sr$_x$MnO (LSM) is the most common cathode material for high-temperature SOFCs owing to its high thermal and chemical stability [21]. However, reducing the operating temperature can significantly deteriorate its performance [254]. Baqué et al. [255] fabricated La$_{0.2}$Sr$_{0.8}$Co$_{0.8}$Fe$_{0.2}$O$_{3-\delta}$ (LSCF) cathode materials using novel HMTA routes and reported that the ASR of the LSCF was of about 0.05 and 0.4 $\Omega\cdot$cm$^2$ at 600 and 450 $^\circ$C, respectively. Afzal et al. [106] prepared Ba$_x$Ca$_{1-x}$Co$_y$Fe$_{1-y}$O$_{3-\delta}$ (BCCF) composite materials via the sol–gel route followed by the auto-combustion method and reported that the Ba$_0.3$Ca$_{0.7}$Co$_{0.3}$Fe$_{0.2}$O$_{3-\delta}$ sample provides the highest electronic conductivity and power density at 550 $^\circ$C. In another attempt, Jiang et al. [256] fabricated SrNb$_{0.1}$Fe$_{0.9}$O$_{3-\delta}$ (SNF) oxide perovskite cathode materials via the modified combustion method. In this work, obtaining an optimized gas transport channel as well as more active areas resulted in reducing the overall ASR of the SNF cathode (with hierarchical porous structure) to around 0.15 $\Omega\cdot$cm$^2$ at 600 $^\circ$C. Due to the variation of cobalt ionic radii at different valence states and the deterioration of ionic transport properties in Co-containing materials, bismuth-doped SrFeO$_{3-\delta}$ materials have also been developed to address the cathode performance issues [257]. However, Bi$_{0.5}$Sr$_{0.5}$FeO$_{3-\delta}$ (BSF) cathodes suffer from their poor electronic conductivity (0.4–2 S cm$^{-1}$ in the temperature range of 300–900 $^\circ$C) [258]. In this regard, Niu et al. [259] developed Ag–Bi$_{0.5}$Sr$_{0.5}$FeO$_{3-\delta}$ (BSF) composite cathodes through EDTA-citrate complexing solution method and reported an acceptable power density out of their fabricated cells. Ag has high oxygen reduction reaction (ORR) activity and is chemically compatible with perovskite materials. Ag addition resulted in increasing the power density of the SOFC cathode twice the magnitude of a single BSF cathode. Acquiring a suitable balance between the electronic conductivity and the drawback of using Co in the cathode is one of the main challenging facing the development of co-based cathodes.

Xia et al. [254] studied the electrochemical characteristics of the interface between strontium-doped samarium cobaltates (SSC) cathode, prepared by the glycine-nitrate route. SSCs are considered as low-temperature cathode materials with YSZ, LSGM, and doped ceria electrolytes. The results showed that the interfacial resistance of the SDC-SSC composite was significantly reduced from 2.0 $\Omega$·cm$^2$ to less than 0.15 $\Omega$·cm$^2$ at 600 $^\circ$C. Since the surface/bulk diffusion and O$_2$ surface exchange are the main cathode parameters, the mixed ionic and electronic conducting (MIEC) materials with a high O$_2$ bulk diffusion coefficient ($D_O$) and oxygen surface coefficient ($k$) have also been investigated as promising low-temperature cathodes [107]. Despite the LSF cathode materials, the oxygen vacancies ($V_O$) can diffuse in the bulk of MIECs composites [190]. The main low-temperature MIEC cathode composites include Ruddlesden–Popper phases, perovskites, and double perovskites with the general formulae of A$_{n+1}$Ba$_n$O$_{3n+1r}$, ABO$_y$, and AA$'$BO$_{y'}$, respectively. Figure 8 shows the crystal structure of the most common MIECs cathode composites [107,260]. Amongst the perovskite materials, the La$_{1-x}$Sr$_x$Co$_{1-y}$Fe$_y$O$_{3-\delta}$ (LSCF) compounds have been extensively investigated due to their high ionic (0.001–0.1 S cm$^{-1}$ at 600 $^\circ$C) and electrical conductivity (100–1000 S cm$^{-1}$ at 600 $^\circ$C) at low temperatures [107,261]. It has been reported that increasing the Sr concentration can simultaneously increase
the electrical conductivity (for $x < 0.4$ in Co-rich and Fe-rich compounds) and TEC of the fabricated cathode substrates. A low TEC value (with about $18.5 \times 10^{-6} \text{K}^{-1}$ in the temperature range of 30–1000 °C) was recorded for an LSCF sample with $x = 0.2$ [262].

To decrease the high TEC values of the LSCF cathodes, the incorporation of excess Fe content has been employed by some researchers. While further addition of Fe can improve the transport properties and TEC of the LSCF cathodes, it can reduce the electrical conductivity of the resulting composite as well [107,263]. Sr or Ba doping in the A site of the MIEC structures can result in gaining a faster oxygen ion transport kinetic [107]. Due to the high rate of oxygen surface exchange, oxygen-ion diffusivity, and electrical conductivity, LnBaCo$_2$O$_{5+\delta}$ attracted great interest among the double perovskite materials for low-temperature cathodes [58,264]. In comparison with the perovskite and double perovskite cathode materials, Ruddlesden–Popper (RP) cathodes with the general formula of $(\text{AO})(\text{ABO}_3)_m$ (A = La, Nd, and Pr; B = Cu, Ni, and Co; m = 1) provide a relatively lower electrical conductivity (~50 to 100 S·cm$^{-1}$) [265]. However, compared to the other MIEC cathodes, the TEC of these cathodes is closer to the common low-temperature electrolytes [266]. The most common RP phase is Ni-based compounds (B = Ni) such as Pr$_2$NiO$_4$ and La$_2$NiO$_4$, which exhibit similar oxygen-ion coefficient and oxygen surface exchange coefficient to those of perovskites [267]. Both the electronic conductivity and the ionic conductivity of 2D K$_2$NiF$_4$-structured La$_{2-x}$Sr$_x$NiO$_{4+\delta}$ (LSN) cathode materials have been studied by Zhu et al. [50]. It has been shown that the bismuth-doped LSN (LSN-Bi) provide an improved electrical conductivity due to the substitution of La by Bi, which affects the chemical diffusion and the surface exchange coefficients of the resulting composite. Moreover, the polarization resistance of LSN-Bi was found to be lower than the parent LSN. The measured electrical conductivity of LSN and LSN-Bi is 99.3 S·cm$^{-1}$ and 100.3 S·cm$^{-1}$ at 550 °C, respectively. The highest power density of about 131 mW·cm$^{-2}$ at 550 °C was recorded for the LSN-Bi samples. The Cu-based RP compounds have also been studied; however, Pr$_2$CuO$_4$ has been known to be the only potential candidate in this family.

Figure 8. Crystal structure of (a) perovskite, (b) double perovskite, and (c) Ruddlesden–Popper phases (Reproduced with permission from [107], Royal Society of Chemistry (RSC), 2016).
with an acceptable oxygen-ion coefficient and oxygen surface exchange coefficient [268].

Overall, despite the exciting properties of MEIC cathodes, their electrochemical properties should be improved to obtain a suitable output power for the L-T SOFCs.

Although MIEC cathodes show higher electrochemical performance in comparison with the conventional LSM cathodes, their ionic conductivity, however, decreases significantly with reducing the operating temperature [211]. Microstructural properties of the cathode, especially the spatial density of TPBs, play an essential role in cathode performance. The high spatial density of TPBs, along with well-percolated electronic and ionic phases distribution, can significantly improve the cathode electrochemical performance. Samson et al. [221] proposed the infiltration of LSC into a porous GDC electrolyte through screen printing to enhance the overall performance of the cathode. They reported that the 17 vol.% infiltrated cathode can boost the cathode performance, while further infiltration may result in a decrease in the overall cell performance. In this work, the maximum polarization resistance measured for the 17 vol.% infiltrated cathode was about 4.4 \times 10^{-2} \, \Omega \cdot \text{cm}^2 at 600 and 400 °C, respectively (Figure 9). Compatibility with the other cell individual layers is another equally important factor for developing suitable cathodes for the L-T SOFCs. Shao and Haile [269] have fabricated (Ba, Sr)(Co, Fe)O₃₋δ as a novel low-temperature cathode composite with low ASR (about 5.5 \times 10^{-1} and 6 \times 10^{-2} \, \Omega \cdot \text{cm}^2). In another work, it has been shown that the Co-based composite could highly react with the Bi-content of the electrolyte layers with a significant drop in the cell performance [67]. Thus, other candidates such as bismuthenates (Bi₂Ru₂O₇–BRO₇) with pyrochlore structure and BRO₇–ESB (Er-stabilized Bi₂O₃) have been proposed as high-performance low-temperature cathode materials with suitable compatibility with Bi-based and Ce-based materials [270]. Another important issue in selecting appropriate materials for the L-T cathode is their TEC that should match the adjacent electrolyte and interconnect layers. Some cathode materials have poor matching TEC; for example, Co-based and ferrite-based cathodes cannot be used with the YSZ electrolyte [260]. The TEC difference between the layers can lead to cathode electrochemical degradation and delamination during the harsh operating condition of SOFCs [86]. Therefore, several aspects of cathode materials, as discussed above, should be considered in choosing an appropriate material for each layer.

![Figure 9. Polarization resistance as a function of operating temperature at different firing temperatures (Reproduced with permission from [271], Institute of Physics (IOP), 2011).](image-url)
Nanocomposite cathode materials have been widely used in the fabrication of SOFCs due to their high surface area as well as quantum tunneling behavior, good thermal stability, high percolation, long-range oxygen-ion/electron transfer pathway, anisotropy, dimensional confinement, and extended TPB, which facilitate the charge transfer and cathode reactions [21]. It has also been reported that the thin-film cathodes can exhibit higher oxygen exchange kinetics due to the increased concentration of oxygen vacancies [21]. In this context, Wang et al. [272] used the pulsed layer deposition technique to fabricate a porous LSC cathode coating with 720 nm in thickness and an average grain size of about 8 nm. The porous layer provided a very low ASR of about 0.09 Ω-cm² owing to its high surface area (80 μm⁻¹). Lee et al. [273] fabricated BSCF-GDC low-temperature core-shell cathode with fiber structure and reported a high output power and low polarization resistance (about 2000 mW-cm⁻² and 4.4 x 10⁻² Ω-cm² at 550 °C, respectively), for an L-T SOFC comprised of a GDC electrolyte and a Ni-GDC anode. Higher power density, conversion efficiency, and superior electrochemical performances have been achieved by using the nanocomposite cathode powders in the fabrication of L-T SOFCs, [274]. Overall, cathode material plays a vital role in order to decrease the operating temperature of SOFCs. This is primarily because of the increased polarization losses at the reduced operating temperatures. Although, the other factors such as the cathode microstructural properties (porosity and grain size), electrical properties (ionic and electronic conductivities), and fabrication specifications (sinterability and thermal expansion coefficient) all affect the performance of a cathode material developed for the L-T SOFCs, as well. So far, several novel materials have been developed in this context that can be mainly classified into the MIEC category in overall; however, the overall efficiency of the L-T cathodes should be further improved to be qualified for commercial applications. Thermal expansion coefficient, availability, and cost of materials are the other requirements to develop a suitable L-T SOFC cathode.

3.1.3. Choice of Interconnects

The essential requirements of the SOFC current-collectors are listed as high thermal conductivity (>0 W·m⁻¹·K⁻¹), excellent electrical conductivity, minimal ionic conductivity, chemical stability in reducing/oxidizing atmospheres, high density, and matching TEC (~10 to 15 x 10⁻⁶ K⁻¹) [139,275,276]. Interconnect materials can be classified into two main categories, including ceramic-based and metal/alloy-based interconnects.

Lanthanum chromite has been known to be the most common ceramic-based interconnect material that can withstand high operating temperature up to 1000 °C [275,277]. La- or Cr-site substituted perovskite-based lanthanum chromite interconnects have been studied by Kolisetty et al. [278]. They investigate the effect of multiple Sr, Ca, Co, Ni, and Fe doping on the electrochemical performance of LaGaO₃ interconnect materials. Different compounds including LaCr₀.₇Co₀.₁Fe₀.₁Ni₀.₁O₃ (LCr7CFN), LaCo₀.₂Cr₀.₁Fe₀.₁Ni₀.₁O₃ (LCo7CFN), LaFe₀.₇Cr₀.₁Co₀.₁Ni₀.₁O₃ (LFe7CCN), LaNi₀.₇Cr₀.₁Co₀.₁Fe₀.₁O₃ (LNi7CCF), and LaCr₀.₂₅Co₀.₂₅Fe₀.₂₅Ni₀.₂₅O₃ (LCCFN) were fabricated via Pechini polymer complexing method. It seems that the mechanism of conductivity in these compounds is based on a thermally activated mobility phenomenon so-called “p-type small polaron hopping”. Amongst various types of interconnects, LCCFN showed the highest conductivity in the temperature range of 300–800 °C. Due to the high relative density (>94%) and good electrical conductivity of LCo7CFN and LCCFN, those materials can be suitable for the fabrication of L-T SOFCs. On the other hand, LNi7CCF with lower relative density of about 82% can be used as cathode material as well. It should also be noted that the highest electrical conductivity measured for this system at 600 °C is about 50–60 S·cm⁻¹. Fergus [279] studied the effect of the alkaline doping agents on lanthanum chromite and found that Ca-doping had a greater effect on increasing the electrical conductivity of lanthanum chromite than Sr doping mainly due to the closer ionic radius of Ca²⁺ (0.134 nm) to La³⁺ (0.136 nm) and also its phase stability. However, the phase stability of Sr-doped samples under low O₂ partial pressure at high temperature was greater than the Ca-doped ones. YCrO₃ [280], PrCrO₃ [281], NdCrO₃ [282], etc., are the other types of perovskite-based interconnects widely used in I-T
SOFCs. Due to the high thermodynamic stability of titanium dioxide in the perovskite over a wide range of temperature, it can also be considered as an interconnect for the L-T SOFCs. In this regard, Nb-doped TiO₂ was synthesized by Michibata et al. [283] with the peak conductivity of about 50 S cm⁻¹ in reducing atmosphere (over 400–1000 °C). Cr-doping into Ti₀.₉₅Nb₀.₇O₂ structure resulted in promoting the conductivity and retarding the degradation of conductivity.

Despite the fact that the advantages of ceramic-based interconnect materials, they suffer from some issues such as high cost of fabrication, low electrical conductivity, and poor sinterability in air (in the case of lanthanum chromite) [128,275,284]. At lower operating temperatures, metallic interconnects offer lower costs, higher mechanical properties, better thermal shock resistance, and better electrical conductivity [285]. High Cr concentration (17–20%) and/or a trace amount of reactive elements such as yttrium results in reducing contact resistance and improving oxidation resistance by promoting the scale adherence at the anode-interconnect interface [275,286]. In this context, Ni-, Fe-, and Cr-based alloys have been widely investigated [275]. Ferritic stainless steels with high Cr content and BCC crystal structure, such as AISI 430, AISI 446, Crofer 22 APU, etc. (with TEC in the range of 10.5 × 10⁻⁶–12.5 × 10⁻⁶ K⁻¹), have been known to be the best candidates [286,287]. Crofer 22 APU is one of the most common ferritic stainless steel used widely as the current collector for SOFCs. It contains about 0.5% manganese which can be sourced from an (Mn, Cr)₅O₄ spinel phase at the top layer and a chromia sublayer phase beneath the substrate [275]. The spinel phase formed on the top of the Crofer 22 APU can significantly boost the electrical conductivity of the substrate [288]. However, one of the main challenges of this sort of interconnect material is the gradual change of its ASR over time. For example, it has been reported that the ASR of Crofer 22 APU increases to about 13 mΩ cm⁻² and then to above 100 mΩ cm⁻² after 1800 and 40,000 h, respectively, which causes an obvious power loss for the cell over time [275].

The austenitic grades of stainless steel with the FCC crystal structure could provide a high oxidation resistance with proper mechanical strength at high temperatures, but their relatively high cost and high TEC values (usually in the range of 15 × 10⁻⁶–20 × 10⁻⁶ K⁻¹) make them unsuitable for the L-T SOFC applications [275]. In addition to the Fe-based alloys, Ni-based alloys have also been used as the interconnect materials. Due to slower oxidation kinetics as well as higher resistance against metal dusting corrosion, the Ni-based alloys have attracted great interest; however, the TEC mismatch between the Ni-based interconnects and the other layers have limited their application [27]. Another class of metal-based interconnect candidate is the Cr-based materials, but those have not been commonly used in the L-T SOFCs because of their high fabrication costs [27]. The most common metal-based interconnects are ferritic steels such as Crofer 22 APU, Plansee Ducralloy, and AISI 441 [14,285].

Metallic interconnect have also some disadvantages, such as Cr poisoning of the cathode, which is the most important problem with metallic interconnects [285,289]. To overcome this problem, a protective layer can be employed to decrease the electrical resistance and reduce Cr diffusion [286]. The protective layer should have a high density to prevent Cr diffusion, suitable chemical/physical stability, high electrical conductivity, and an ASR lower than 0.1 Ω cm⁻² [284,290]. The most common protective layers are spinel oxide composites, earth perovskites, and reactive oxide compounds [286]. Hassan et al. used three different protective coating layers, namely, chromia, spinel, and CuO, to shield the Crofer 22 APU from chromium poisoning, as illustrated in Figure 10 [291]. Tan et al. [287] proposed coating a protective Ba₀.₅Sr₀.₅Co₀.₅Fe₀.₂O₃₋δ-Sm₀.₂Ce₀.₈O₁.₉ carbonate perovskite layer (BSCF-SDCC) which can retard the outward diffusion and reduce its oxidation kinetics. The incorporation of SDCC can improve the conductivity of the resulting compound. Electrophoresis deposition is another technique that can be used for coating the composite on SUS 430 stainless steel. The maximum ASR of the coating layer sintered at 550–650 °C was about 7.3 × 10⁻² Ω cm⁻² after 500 h of operation. The performance of several coating materials such as La₀.₈Sr₀.₂MnO₃₋δ [292], La₀.₈Sr₀.₂FeO₃₋δ [293],
La$_{0.6}$Sr$_{0.4}$Co$_{0.2}$Fe$_{0.8}$O$_{3-\delta}$ \[294\], La$_{0.6}$Sr$_{0.4}$CoO$_3$ \[295\], etc., have also been studied, but the BSCF had the highest Cr poisoning resistance. Zhou et al. \[296\] comprehensively studied the Cr poisoning of the SOFCs as well as the state-of-the-art strategies to alleviate the Cr poisoning. These strategies can be listed as coating with a suitable protective layer, adjusting the cell constituents’ composition, developing new alloys with high Cr poisoning resistance, and using Cr getters at the inlet of air stream to reduce the partial pressure of chromium vapor. Similar to Cr poisoning, sulfur poisoning can also be a risk for the SOFC cathodes. In this regard, Wang et al. \[297\] studied sulfur poisoning of cathode materials and proposed a few remedies to manage the sulfur poisoning risk.

![Figure 10. SEM images of Crofer 22 APU (a) before and (b) after annealing coated with 3 different layers, namely (L1: chromia), (L2: spinel), and (L3: CuO) \[291\].](image)

Spinel coatings have attracted the most interest mainly due to their low cost, suitable area-specific resistance, and Cr prevention \[286\]. Coating the surface of the interconnect material with manganese-based spinels such as CuMn$_{1.8}$O$_4$, (Mn, Co)$_3$O$_4$, and Mn$_{1.5}$Co$_{1.5}$O$_4$ can suppress the Cr vaporization and improve the electrical conductivity of the interconnect \[298,299\]. It has also been reported that Cu and Ni doping can further improve the interconnect performance by promoting the electrical properties and coating adherence to the interconnect \[286\]. However, besides the difficulties with the coating process, it has been reported that coating the interconnect may result in increasing the rate of interconnect degradation \[300\]. Other methods for improving the interconnect performance and decreasing its degradation rate are adding Nb$_2$O$_5$ to ferritic stainless steels \[301\], electroplating Co-2.4 wt.% W layer on type 430 stainless steel \[302\], Ce/Co coated AISI 441 \[302\], etc.

Overall, it can be concluded that both ceramic and metallic materials can be used as the L-T SOFC interconnects. Ceramic-based interconnects have high stability under the oxidizing atmospheres; however, their conductivity is lower than the metallic ones. On the other hand, the metallic based-interconnects offer a comparably higher conductivity, but those are not stable under the oxidizing atmosphere. Metallic interconnects show better efficiency in the L-T SOFCs, while the ceramic-based interconnects are efficient materials to be used at higher temperatures.

### 3.2. Operational and Fuel Prospects

In addition to the different layers of the SOFCs, optimizing the fuel is also essential. In this context, fuel processing, which is defined as the conversion of the fuel to suitable fuel gas, can be employed. This process includes the removal of harmful materials from the fuel (such as sulfur, halides, ammonia, etc.), conversion of the fuel into a fuel gas reformate, and altering the fuel gas reformate to meet the desirable properties of SOFCs \[41,303\]. High thermal (theoretical) efficiency, compactness, quick-start capability, and multi-cycling are the primary consideration in this regard \[304\]. To integrate an effective fuel processor with a SOFCs, several factors such as fuel flexibility, fuel cell size, vaporization of heavy
Different fuel can be used in SOFCs, including natural gas, diesel, gasoline, hydrocarbons, catalyst tolerance, and cost-effectiveness should be considered. A schematic of a fuel processor for the L-T SOFCs is shown in Figure 11 [41].

![Figure 11. Schematic of the steps in a typical fuel processor for low-temperature SOFCs [41].](image)

In summary, while hydrogen is the most common fuel for the closed systems (such as space crafts), natural gas is the most preferred type of fuel for small and stationary plants. In addition, high sulfur diesel can be used in heavy vehicles, jets, and military applications. For light vehicles and low-temperature applications, on-board hydrogen and liquid fuels such as gasoline and methanol are preferred. Other fuels, such as ethanol, biomass, refuse-derived fuels, etc., have also been investigated for their potential applications in the SOFC systems [41,303].

4. Technological Aspects for Low-Temperature Stack Design

4.1. Stack Design Technologies

Solid oxide fuel cell stacks consist of individual cells, sealants, and connectors. Generally, the efficiency of a SOFC stack is remarkably lower than that of the individual cells. The critical factor that has a significant influence on the performance of a stack is the interface contact between the current collector and cell [308]. A single cell cannot obtain a high current and voltage output; thus, the individual cells should be connected in parallel or series to improve the overall voltage and power density [14,41]. In addition to the conventional planar and tubular designs, novel stack design technologies can be divided into several classifications such as integrated planar (IP), cone-shaped, flat-tube, honeycomb, microtubular, etc. The IP design (Figure 12a) is a stack design that can be considered as a cross between the tubular and planar structure and can provide lower weight and costs for the current collector and the whole SOFC. It also offers an improved cell performance mainly due to the short electronic and ionic path [309,310]. However, it needs a careful design and choice of materials as well as optimization of microstructure to overcome the problems with sealing and current collector integrity [311]. The cone-shaped design (Figure 12b) can be considered as a tubular SOFC with high thermal stability. By fitting each cone into another, a self-supported tubular structure will be formed. Thus, the integrated cells in this design can offer flexibility to the stack, along with a high power...
density [312]. However, challenges similar to those in IP-SOFCs remain elusive [311]. The Flat-tube design (Figure 12c) is a modified tubular design with a higher power density and thermal resistance than the conventional tubular design. In this design, the fuel moves through the gas channels while the oxidants pass through a porous media located between the cells [313,314]. The honeycomb design (Figure 12d) possesses the advantages of tubular and planar structure and is composed of several honeycomb channels which serve as the fuel and oxidant paths. This design can be either as the electrode- or electrolyte-supported geometries with delivering a high power density and mechanical strength [315]. The microtubular geometry is a type of tubular design in which the tube diameter is smaller than 3–5 mm [316]. Since the power density inversely proportional to the tube diameter, this design provides a higher power density than the conventional tubular SOFCs [79,311,317]. Moreover, the small size of the tube reduces the thermal gradient; thereby, the microtubular SOFCs can provide a better thermal shock resistance [318,319].

Other types of cell and stack designs, such as SOFCs with novel electrolyte design and wet-impregnated SOFCs, have been investigated by some scholars. These designs may offer higher electrochemical performance compared to the conventional designs; however, their long-term stability and low mechanical strength have yet to be studied in details [311].

![Figure 12. (a) Integrated planar (IP)-SOFC cell design [309], (b) cone-shaped SOFC design (1. anode; 2. electrolyte; 3. cathode; and 4. current collector) (Reproduce with permission from [320], Institute of Physics (IOP), 2007), (c) flat-tube SOFC design, and (d) honeycomb SOFC design (Reproduced with permission from [311], Elsevier, 2016).](image)

The stack designs are complex engineering units that have their own pros and cons. Although the IP-SOFCs could provide a relatively better electrochemical performance at lower costs, the integrity of the current collector and sealing are the main challenges with this design [311]. The cone-shaped design offers higher thermal shock resistance and power density; however, due to the complex design and problems with current collector integrity, its fabrication is complex and challenging [312]. The flat-tube SOFCs could also provide high thermal shock resistance and power density but similar to the cone-shaped design, those suffer from engineering and design complexity issues [311]. The honeycomb design, on the other hand, could improve the durability and mechanical strength of the stack, but the challenges associated with the stack fabrication, current collector integrity, and electrical
lead have hindered its application in SOFCs. The microtubular design could potentially provide high volumetric output power, good thermal shock resistance, and rapid start-up. However, the poor current collection is the main disadvantage of this design [321].

4.2. Synthesis Methods and Conditions

Synthesis conditions (temperature, pressure, dwelling time, etc.) for the ceramic powders and fabrication materials can significantly affect the microstructure and the electrochemical performance of the fabricated SOFCs. Optimizing the cell structure and its properties such as relative density, microdomain formation grain size, grain boundaries, agglomeration, impurities, thermal history, etc., can improve the mechanical and electrical properties of the fabricated cells and stacks [110,322,323]. Shemilt and Williams [324] employed compression-molding and dry-pressing to fabricate SDC electrolytes and found that the compression molded-samples can provide a higher grain boundary activation energy compared to the dried pressed samples. Mori et al. [325] investigated the effect of different morphologies on the electrical conductivity of SDC samples and found that the spherical particles possessed higher conductivity than the elongated ones mainly due to the smaller microdomain in those samples. Gibson et al. [326] reported the grain boundary conductivity linearly correlates to the amount of porosity. It has also been reported that finer microstructure can increase the TPB length and result in a more uniform particle/pore distribution in the bulk of the materials. The synthesis method has a significant impact on particle size and distribution. Optimization of the ratio of the solid phases in the sample can improve the electrochemical performance [327,328]. Naimaster et al. [329] investigated the effect of microstructure on the performance of I-T SOFCs and reported that decreasing the grain size down to 2 µm could improve the current density in the order of 2–3 A·cm$^{-2}$. They also noted that porosity and tortuosity did not have a significant impact on the performance; however, a relationship between these two parameters can be useful for adjusting the constituents of the MIEC composite (particularly in the case of LSCF-GDC). The work also showed that the anode diffusion loss could be lower than that of the cathode layer. This work can be exemplified as a successful microstructural improvement study by obtaining the maximum power density of about 0.162 W·cm$^{-2}$ to about 0.789 W·cm$^{-2}$ and reduced activation overpotential (~29%) and ohmic loss (68%).

As discussed above, the SOFC electrodes should have a suitable amount of porosity, while the electrolyte should be fabricated as dense as possible. Thus, choosing a proper fabrication method is of significant importance in achieving a high-performance SOFC with desirable properties [330]. In addition, the conventional solid-state reaction synthesis, the other fabrication techniques such as sol–gel [331], hydrothermal [332], citrate sol–gel [38], polymeric salt composition [333], co-precipitation [216], combustion synthesis [334], glycine-nitrate and citrate [152,335], impregnation [233], infiltration [249], Pechini [147], spray pyrolysis [334], ionic gelation [25], etc., have been used for the fabrication of various individual SOFC layers. For instance, in the case of microtubular SOFCs, gel-casting, extrusion, cold isostatic press, etc., have been extensively investigated for fabricating the supporting microtubes [330]. As another example, the tape casting method can be used for the fabrication of both electrodes and electrolyte layers with various thicknesses and lower costs. However, this method has some challenges associated with the multiple drying process required, as well as the high crack sensitivity of the fabricated cells [40]. Screen printing can reduce the cracking problems during sintering and is capable to be used for large-scale fabrication of high-quality SOFC films. However, providing a high-quality ink is an important challenge in this method [336]. Onbilgin et al. [337] compared the screen-printing and the tape-casting methods and reported that the tape-cast samples could provide a relatively higher performance compared to those samples prepared by the screen-printing method. Overall, the fabrication method and sintering conditions, as well as the starting materials, have a significant impact on the cell output performance. The preferred method selected for the fabrication of the L-T SOFCs depends on the simplicity, feasibility, and costs [338].
4.3. Choice of Sealant

In stack design technology, sealants are the materials that can be employed to prevent any leakage or the direct mixing of fuel and air. One of the most important parameters in determining the maximum operating temperature of SOFCs is the glass-transition temperature of the sealant [27]. The most important mechanical properties of sealants are minimal gas leakage, matching TEC (~10 to 12 × 10^{-6} K^{-1}), good thermal shock resistance, and suitable resilience and toughness under static/dynamic forces. They should also possess long-term chemical stability (>40,000 h) under the operating environment. Having insulating nature as well as design flexibility, simple processing, and low-cost fabrication are the other important properties of suitable sealants [339,340]. Generally, metal, brazes, glass-ceramics, and mica-based composites have been used in the past years as the sealants for SOFCs [341–343].

Two standard sealing methods have been proposed so far, namely compressive seals and rigid seals. In compressive sealing, the sealant is placed between the surfaces and then compressed by using an external load. In these seals, since there is no tightly bonding between the sealant and the other components, there is no need to have a close CTE to that of the other components [27,285,344]. Metallic seals (such as platinum, gold, and silver), as well as mica-based seals (such as muscovite (KAl_{2}(AlSi_{3}O_{10})(F,OH)_{2}) and phlogopite (KMg_{3}(AlSi_{3}O_{10})(OH)_{2})), are the main types of compressive sealants. Currently, mica-based and glass-ceramics materials have been extensively used as SOFC sealants. However, the oxide scaling and chemical instability in highly reactive environments are the two major drawbacks of these密封ants [27]. On the other hand, rigid seals (such as alloy-based braze materials as well as glass and glass-ceramics) make a strong bonding with the surface and thereby should have a close CTE to that of the other components. They are generally more cost-effective than the compressive ones [341]. Among the rigid seals, glass-ceramics such as borosilicate, phosphor-silicate, and boron-free alkaline earth silicates have been investigated [27]. Glass and glass-ceramics have great advantages over the other types of seals. The main advantages are ease of fabrication, facilitated hermetic behavior due to their viscous and wetting features, improved rigidity of the seal, and tailorability of the thermal properties through compositional modulations [345]. Boroaluminosilicates (T_g = 614–739 °C and TEC = 10.6–11.5 × 10^{-6} K^{-1}), borosilicates (T_g = 623–662 °C and TEC = 10.5–11.4 × 10^{-6} K^{-1}), aluminosilicates (T_g = 730 °C and TEC = 10.7 × 10^{-6} K^{-1}), silicates (T_g = 686–721 °C and TEC = 10.7–12.0 × 10^{-6} K^{-1}), and borates (T_g = 760 °C and TEC = 11.5 × 10^{-6} K^{-1}) are the most common sealants for the SOFCs operating at a wide range of temperature [346–348]. However, the brittle nature of glass and glass-ceramics along with the generation of volatile compounds at high temperatures, poor thermal stability at high temperature, reaction with the adjacent components, and few available compounds, are the main disadvantages of these sealants [346]. Today, novel sealants are the glass-ceramics reinforced by glass fibers [285]. The common doping and coating methods have been suggested to be applied to overcome the brittleness of glass and glass-ceramics.

4.4. Current Challenges, Operational Costs, and Performance Prospects of L-T SOFCs

Although lowering the operating temperature of SOFCs can mitigate the choice of materials as well as operational and fabrication issues concerned with the high-temperature applications, it imposes some new challenges such as an increased overpotential and lower efficiency. Overall, lowering the operating temperature results in emerging new challenges, namely, the cost-effectiveness of SOFCs regarding their output power, stack geometry and its electrical resistance, the electrical conductivity of the electrodes, the electrical and ionic conductivity of interconnect and electrolyte, and other stack constituent materials [284].

According to the US Department of Energy (DOE), the cost of a fuel cell stack should be less than $100 K · W^{-1}$. The perovskite-based cathode is the most expensive component in SOFCs; for example, the cost of LSM is about $50 Kg^{-1}$ [284]. Decreasing the operating temperature increases the electrode polarization, thereby achieving higher power
density may result in higher material costs [349]. Since the current materials that can attain power densities of more than 600 mW·cm\(^{-2}\) are limited, fabricating a cost-effective low-temperature SOFC is very difficult [284]. The operating temperature of SOFCs is indirectly affected by the geometry selected for the single-cell design. Moreover, the ratio of current path length to the cross-sectional area (L/A) affect the ASR of each cell component (Figure 13) [284,350,351]. This geometric ratio should be as low as possible in the L-T SOFCs in order to maximize the cross-sectional area and minimize the electrical path [352]. The short current path and large cross-sectional area of planar SOFCs result in a lower ASR across the internal stack circuit. The tubular design has a longer electrical path; thereby, it shows higher ASR. Depending on the tube length, the ASR of the microtubular design can be higher or lower than the tubular one. Furthermore, achieving perfect gas sealing in the segment-in-series design is much easier than the tubular design. However, this design may have a high ASR depending on its cross-sectional L/A ratio. In addition, it may need a specific current collector to reduce the overall stack resistance [284]. As already discussed (in Section 3), the electrodes operational factors such as the electrochemical oxygen reduction activity, electrical conductivity, life-time, and Cr poisoning of the electrodes, as well as the electrical resistance and oxygen ion conductivity of the electrolyte, all are affected by lowering the operating temperature of SOFCs.

![Figure 13](image-url). The effect of the length to area L/A ratio on the ASR of different cell geometry (Reproduced with permission from [284], Wiley, 2010).

Another important parameter, which should be considered in fabricating the SOFC individual layers, is the availability and costs of the raw materials, especially the rare earth elements. Jaroni et al. [353] investigated the economic feasibility of using rare earth metals outside China, which covers almost 90% of the global market for the rare metals. According to this report, although there are some potential mining sites for extracting rare earth elements throughout the world, China still keeps playing an important role in determining the price and availability of these materials. An overview of the potential rare earth mining sites throughout the world is shown in Figure 14. Overall, in addition to the efficiency and electrochemical performance, availability and cost-effectiveness of the materials should be prioritized by the research policymakers at the top levels (such as the local and global research councils), while working on developing new materials for the L-T SOFCs.
5. Conclusions

- Lowering the operating temperature of SOFCs offers excellent advantages, including broader options for selecting materials, lower costs, lower degradation, etc. However, reducing the SOFC operating temperature can also increase cell polarization losses, resulting in reduced electrochemical performance, overall. Thus, novel and cost-effective materials should be developed for different cell components, namely anode, cathode, electrolyte, and interconnects.

- The L-T SOFC Electrolytes should possess a high ionic conductivity as well as good chemical stability, matching TEC to those of other components, and low ohmic loss. The fabricated electrodes should have high electrical conductivity ($>1$ S cm$^{-1}$), with a matching TEC, high chemical stability, and proper catalytic activity. Interconnect materials for the L-T region should provide a high electronic conductivity along with good chemical compatibility and matching TEC. The most common interconnect materials for low-temperature applications are metal- or alloy-based ones. In addition to the high mechanical and thermal resistivity, sealants should exhibit a desirable electrical conductivity. Two types of sealants, including the rigid and compressive ones, could be used for the L-T SOFCs overall.

- Fuel optimization plays an important role in achieving high electrochemical performance. Fuel flexibility, cost-effectiveness, fuel size, and catalyst tolerance are the most important parameters in obtaining effective fuel from the processor. Diesel, gasoline, hydrogen, ethanol, methanol, ammonia, natural gas, etc., are the most prevalent fuels with their own advantages and disadvantages that should be considered in choosing the right fuel for the system. Generally, hydrogen and liquid fuels are the most common fuel for closed systems and light vehicle operating in the low-temperature region.

- Different stack designs have been developed for the L-T SOFCs, including honeycomb, microtubular, cone-shaped, and flat-tube. The integrated-planar design is one of the most predominant stack designs for the planar and tubular SOFC geometries. The appropriate geometry should be selected according to the engineering and design factors.

- Fabrication of the L-T SOFCs needs to be improved and optimized in terms of the rate of fuel utilization, gas management, electrical collection, etc. Each fabrication method and synthesis condition can result in a distinctive microstructure and electrochemical performance. Some fabrication methods such as tape-casting and screen-printing showed promising potential for the large-scale fabrication of L-T SOFCs. Thus, choosing the appropriate fabrication method for the individual cell layers is crucial in order to lower the operating temperature of the SOFCs.

- In addition to the efficiency and performance of the SOFCs, several other aspects should be considered, including cost-effectiveness, availability, economic feasibility, and the sustainability and priority of the research materials. Regarding the choice of...
fuel, pollution, and environmental aspects of the fuel should be considered along with the other parameters discussed earlier.

**Author Contributions:** Writing—original draft preparation, M.F.V.; conceptualization, writing—review, editing, and supervision, B.A.H. All authors have read and agreed to the published version of the manuscript.

**Funding:** This research was funded by the Department of Chemical and Process Engineering at the University of Surrey as well as the Royal Society Research Grant: RGS\R2\202137.

**Institutional Review Board Statement:** Not applicable.

**Informed Consent Statement:** Not applicable.

**Conflicts of Interest:** The authors declare no conflict of interest.

**References**

1. Singh, B.; Ghosh, S.; Aich, S.; Roy, B. Low temperature solid oxide electrolytes (LT-SOE): A review. *J. Power Sources* 2017, 339, 103–135. [CrossRef]

2. Faro, M.L.; La Rosa, D.; Antonucci, V.; Aricó, A.S. Intermediate temperature solid oxide fuel cell electrolytes. *J. Indian Inst. Sci.* 2009, 89, 363–380.

3. Lee, S.; Lee, K.; Jang, Y.H.; Bae, J. Fabrication of solid oxide fuel cells (SOFCs) by solvent-controlled co-tape casting technique. *Int. J. Hydrogen Energy* 2016, 42, 1648–1660. [CrossRef]

4. Song, C.; Lee, S.; Gu, B.; Chang, I.; Cho, G.Y.; Baek, J.D.; Cha, S.W. A Study of Anode-Supported Solid Oxide Fuel Cell Modeling and Optimization Using Neural Network and Multi-Armed Bandit Algorithm. *Energies* 2020, 13, 1621. [CrossRef]

5. Baldi, F.; Moret, S.; Tammi, K.; Maréchal, F. The role of solid oxide fuel cells in future ship energy systems. *Energy* 2020, 194. [CrossRef]

6. Lerson, S.; Lilien, J.L.; Minne, G. Performance assessment of a 5 kW SOFC cogeneration fuel cell. *Int. J. Environ. Technol. Manag.* 2008, 9, 426–433. [CrossRef]

7. Shri Prakash, B.; Pavitra, R.; Senthil Kumar, S.; Aruna, S.T. Electrolyte bi-layering strategy to improve the performance of an intermediate temperature solid oxide fuel cell: A review. *J. Power Sources* 2018, 381, 136–155. [CrossRef]

8. Jaiswal, N.; Tanwar, K.; Suman, R.; Kumar, D.; Uppadhya, S.; Parkash, O. A brief review on ceria based solid electrolytes for solid oxide fuel cells. *J. Alloys Compd.* 2019, 781, 984–1005. [CrossRef]

9. Da Silva, F.S.; De Souza, T.M. Novel materials for solid oxide fuel cell technologies: A literature review. *Int. J. Hydrogen Energy* 2017, 42, 26020–26036. [CrossRef]

10. Choolaei, M.; Cai, Q.; Slade, C.T.; Horri, B.A. Nanocrystalline gadolinium-doped ceria (GDC) for SOFCs by an environmentally-friendly single step method. *Ceram. Int.* 2018, 44, 13286–13292. [CrossRef]

11. Fabbri, E.; Pergelesi, D.; Traversa, E. Materials challenges toward proton-conducting oxide fuel cells: A critical review. *Chem. Soc. Rev.* 2010, 39, 4355–4369. [CrossRef] [PubMed]

12. Caton, J.A. Maximum efficiencies for internal combustion engines: Thermodynamic limitations. *Int. J. Engine Res.* 2018, 19, 1005–1023. [CrossRef]

13. Qiao, Z.; Xia, C.; Cai, Y.; Afzal, M.; Wang, H.; Qiao, J.; Zhu, B. Electrochemical and electrical properties of doped CeO2-ZnO composite for low-temperature solid oxide fuel cell applications. *J. Power Sources* 2018, 392, 33–40. [CrossRef]

14. Irshad, M.; Siraj, K.; Raza, R.; Ali, A.; Tiwari, P.; Zhu, B.; Rafique, A.; Ali, A.; Ullah, M.K.; Usman, A. A brief description of high temperature solid oxide fuel cell’s operation, materials, design, fabrication technologies and performance. *Appl. Sci.* 2016, 6, 75. [CrossRef]

15. Zakaria, Z.; Mat, Z.A.; Hassan, S.H.A.; Kar, Y.B. A review of solid oxide fuel cell component fabrication methods toward lowering temperature. *Int. J. Energy Res.* 2019, 44, 594–611. [CrossRef]

16. Wachsman, E.D.; Lee, K.T. Lowering the temperature of solid oxide fuel cells. *Science* 2011, 334, 935–939. [CrossRef]

17. Lyu, Y.; Xie, J.; Wang, D. Review of cell performance in solid oxide fuel cells. *J. Mater. Sci. Sci.* 2020, 55, 7184–7207. [CrossRef]

18. Lu, Y.; Zhu, B.; Cai, Y.; Kim, J.S.; Wang, B.; Wang, J.; Zhang, Y.; Li, J. Progress in electrolyte-free fuel cells. *Front. Energy Res.* 2016, 4, 17. [CrossRef]

19. Andújar, J.M.; Segura, F. Fuel cells: History and updating: A walk along two centuries. *Renew. Sustain. Energy Rev.* 2009, 13, 2309–2322. [CrossRef]

20. Fan, L.; Wang, C.; Chen, M.; Zhu, B. Recent development of ceria-based (nano)composite materials for low temperature ceramic fuel cells and electrolyte-free fuel cells. *J. Power Sources* 2015, 234, 154–174. [CrossRef]

21. Fan, L.; Zhu, B.; Su, P.C.; He, C. Nanomaterials and technologies for low temperature solid oxide fuel cells: Recent advances, challenges and opportunities. *Nano Energy* 2018, 45, 148–176. [CrossRef]

22. Al Kharusi, H.; Svensson, M.; Salamatinia, B.; Horri, B.A. Gelling synthesis of NiO/YSZ nanocomposite powder for solid oxide fuel cells. *Adv. Mater. Proc.* 2017, 2, 813–818. [CrossRef]
112. Khan, M.A.; Raza, R.; Lima, R.B.; Chaudhry, M.A.; Ahmed, E.; Abbas, G. Comparative study of the nano-composite electrolytes based on samaria-doped ceria for low temperature solid oxide fuel cells (LT-SOFCs). Int. J. Hydrogen Energy 2013, 38, 16524–16531. [CrossRef]

113. Zhan, Z.; Bierschenk, D.M.; Cronin, J.S.; Barnett, S.A. A reduced temperature solid oxide fuel cell with nanostructured anodes. Energy Environ. Sci. 2011, 4, 3951–3954. [CrossRef]

114. Chen, Y.; Lin, Y.; Zhang, Y.; Wang, S.; Su, D.; Yang, Z.; Han, M.; Chen, F. Low temperature solid oxide fuel cells with hierarchically porous cathode. Nano Energy 2014, 8, 25–33. [CrossRef]

115. Abdalla, A.M.; Hossain, S.; Azad, A.T.; Petra, P.M.; Begum, F.; Eriksson, S.G.; Azad, A.K. Nanomaterials for solid oxide fuel cells: A review. Renew. Sustain. Energy Rev. 2018, 82, 353–368. [CrossRef]

116. Park, J.-Y.; Wachsmann, E.D. Stable and high conductivity ceria/bismuth oxide bilayer electrolytes for lower temperature solid oxide fuel cells. Ionics (Kiel) 2006, 12, 15–20. [CrossRef]

117. Wachsmann, E.D. Stable High Conductivity Ceria/Bismuth Oxide Bilayered Electrolytes. J. Electrochem. Soc. 1997, 144, 233. [CrossRef]

118. Hou, J.; Bi, L.; Qian, J.; Zhu, Z.; Zhang, J.; Liu, W. High performance ceria-bismuth bilayer electrolyte low temperature solid oxide fuel cells (LT-SOFCs) fabricated by combining co-pressing with drop-coating. J. Mater. Chem. A 2015, 3, 10219–10224. [CrossRef]

119. Mori, T.; Ikegami, T.; Yamamura, H. Application of a Crystallographic Index for Improvement of the Electrolytic Properties of the CeO2-Sm2O3 System. J. Alloys Compd. 2015, 658, 513–519. [CrossRef]

120. Chen, G.; Luo, Y.; Sun, W.; Liu, H.; Ding, Y.; Li, Y.; Geng, S.; Yu, K.; Liu, G. Electrochemical performance of a new structured low temperature SOFC with BZY electrolyte. Int. J. Hydrogen Energy 2018, 43, 12765–12772. [CrossRef]

121. Wang, F.; Lyu, Y.; Chu, D.; Jin, Z.; Zhang, G.; Wang, D. The electrolyte materials for SOFCs of low-intermediate temperature: Review. Mater. Sci. Technol. 2019, 35, 1515–1562. [CrossRef]

122. Wachsman, E.D. Stable High Conductivity Ceria/Bismuth Oxide Bilayered Electrolytes. J. Electrochem. Soc. 1997, 144, 233. [CrossRef]

123. Oh, E.O.; Whang, C.M.; Lee, Y.R.; Park, S.Y.; Prasad, D.H.; Yoon, K.J.; Son, J.W.; Lee, J.H.; Lee, H.W. Extremely thin bilayer electrolyte for solid oxide fuel cells (SOFCs) fabricated by chemical solution deposition (CSD). Adv. Mater. 2012, 24, 3373–3377. [CrossRef]

124. Yabihoro, H.; Eguchi, Y.; Eguchi, K.; Arai, H. Oxygen ion conductivity of the ceria-samarium oxide system with fluorite structure. J. Appl. Electrochem. 1988, 18, 527–531. [CrossRef]

125. Yokokawa, H.; Sakai, N. History of high temperature fuel cell development. In Handbook of Fuel Cells–Fundamentals, Technology and Applications; John Wiley & Sons, Ltd.: Aichi, Japan, 2010; pp. 1–13, ISBN 9780470974001. [CrossRef]

126. Morii, T.; Drennan, J.; Lee, J.; Li, J.; Ikegami, T. Oxide ionic conductivity and microstructures of Sm- or La-doped CeO2-based systems. Solid State Ion. 2002, 154–155, 461–466. [CrossRef]

127. Goodmanough, J.B. Oxide-ion conductors by design. Nature 2000, 404, 821–823. [CrossRef] [PubMed]

128. Uddin, M.J.; Cho, S.J. Reassessing the bulk ionic conductivity of solid-state electrolytes. Sustain. Energy Fuels 2018, 2, 1458–1462. [CrossRef]

129. Kobi, S.; Jaiswal, N.; Kumar, D.; Parkash, O. Ionic conductivity of Nd3+ and Y3+ co-doped ceria solid electrolytes for intermediate temperature solid oxide fuel cells. J. Alloys Compd. 2015, 658, 513–519. [CrossRef]

130. Mori, T.; Lee, J.-H.; Li, J.; Ikegami, T.; Auchtelerlonie, G.; Drennan, J. Improvement of the electrolytic properties of Y2O3-based materials using a crystallographic index. Solid State Ion. 2001, 138, 277–291. [CrossRef]

131. Mori, T.; Ikegami, T.; Yamamuro, H. Application of a Crystallographic Index for Improvement of the Electrolytic Properties of the CeO2-δSm2O3 System. J. Electrochem. Soc. 1999, 146, 4380–4385. [CrossRef]

132. Yabihoro, H.; Eguchi, K.; Arai, H. Electrical properties and reducibilities of ceria-rare earth oxide systems and their application to solid oxide fuel cell. Solid State Ion. 1989, 36, 71–75. [CrossRef]

133. Biswas, M.; Sadanala, K.C. Electrolyte Materials for Solid Oxide Fuel Cell. J. Powder Metall. Min. 2013, 02, 10–15. [CrossRef]

134. Brown, J.T. High-Temperature Solid-Oxide Fuel Cells (SOFCs). Assess. Res. Needs Adv. Fuel Cells 1986, 209–229. [CrossRef]

135. Fung, K.-Z. Advanced Materials for High-Temperature Solid Oxide Fuel Cells (SOFCs). In Electrochemical Energy: Advanced Materials and Technologies; Shen, P., Wang, C., Jiang, S., Sun, X., Zhan, J., Eds.; CRC Press: Boca Raton, FL, USA, 2015; pp. 269–305.

136. Haile, S.M. Fuel cell materials and components. Acta Mater. 2005, 51, 5981–6000. [CrossRef]

137. Marrocchelli, D.; Bishop, S.R.; Tullier, H.L.; Yildiz, B. Understanding chemical expansion in non-stoichiometric oxides: Ceria and zirconia case studies. Adv. Funct. Mater. 2012, 22, 1958–1965. [CrossRef]

138. Xia, C.; Qiao, Z.; Feng, C.; Kim, J.S.; Wang, B.; Zhu, B. Study on zinc oxide-based electrolytes in low-temperature solid oxide fuel cells. Materials 2017, 11, 40. [CrossRef]
201. Ma, Y.; Singh, M.; Wang, X.; Yang, F.; Huang, Q.; Zhu, B. Study on GDC-KZnAl composite electrolytes for low-temperature solid oxide fuel cells. Int. J. Hydrogen Energy 2014, 39, 17460–17465. [CrossRef]
202. Chockalingam, R.; Amarakoorn, V.R.W.; Giesche, H. Alumina/cerium oxide nano-composite electrolyte for solid oxide fuel cell applications. J. Eur. Ceram. Soc. 2008, 28, 959–963. [CrossRef]
203. Huang, J.; Mao, Z.; Liu, Z.; Wang, C. Development of novel low-temperature SOFCs with co-ionic conducting SDC-carbonate composite electrolytes. Electrochem. Commun. 2007, 9, 2601–2605. [CrossRef]
204. Wang, X.; Ma, Y.; Li, S.; Kashyout, A.H.; Zhu, B.; Muhammad, M. Ceria-based nanocomposite with simultaneous proton and oxygen ion conductivity for low-temperature solid oxide fuel cells. J. Power Sources 2011, 196, 2754–2758. [CrossRef]
205. Zhao, Y.; Xu, Z.; Xia, C.; Li, Y. Oxide ion and proton conduction in doped ceria-carbonate composite materials. Int. J. Hydrogen Energy 2013, 38, 1553–1559. [CrossRef]
206. Zhao, Y.; Xia, C.; Wang, Y.; Xu, Z.; Li, Y. Quantifying multi-ionic conduction through doped ceria-carbonate composite electrolyte by a current-interruption technique and product analysis. Int. J. Hydrogen Energy 2012, 37, 8556–8561. [CrossRef]
207. Gao, Z.; Liu, X.; Zhu, Z.; Ljungberg, R. Solid oxide fuel cell (SOFC) using industrial grade mixed rare-earth oxide electrolytes. Int. J. Hydrogen Energy 2010, 35, 731–737. [CrossRef]
208. Huang, J.; Mao, Z.; Liu, Z.; Wang, C. Performance of fuel cells with proton-conducting ceria-based composite electrolyte and nickel-based electrodes. J. Power Sources 2008, 175, 238–243. [CrossRef]
209. Zhang, L.; Lan, R.; Xu, X.; Tao, S.; Jiang, Y.; Kraft, A. A high performance intermediate temperature fuel cell based on a thick oxide-carbonate electrolyte. J. Power Sources 2009, 194, 967–971. [CrossRef]
210. Raza, R.; Wang, X.; Ma, Y.; Zhu, B. Study on calcium and samarium co-doped ceria based nanocomposite electrolytes. J. Power Sources 2010, 195, 6491–6495. [CrossRef]
211. Wu, G.; Wang, C.; Xie, F.; Wang, X.; Mao, Z.; Liu, Q.; Zhan, Z. Ionic transport mechanism of La0.95Sr0.1Ga0.8Mg0.2O2.85-(Li/Na)2CO3 composite electrolyte for low temperature SOFCs. Int. J. Hydrogen Energy 2016, 41, 16275–16281. [CrossRef]
212. Zhu, B.; Liu, X.; Zhu, Z.; Ljungberg, R. Solid oxide fuel cell (SOFC) using industrial grade mixed rare-earth oxide electrolytes. Int. J. Hydrogen Energy 2008, 33, 3385–3392. [CrossRef]
213. Zhu, W.; Xia, C.; Ding, D.; Shi, X.; Meng, G. Electrical properties of ceria-carbonate composite electrolytes. Mater. Res. Bull. 2006, 41, 2057–2064. [CrossRef]
214. Inouibili, A.; Kahlauoui, M.; Sobrados, I.; Chefi, S.; Madani, A.; Sanz, J.; Ben Haj Amara, A. Influence of anionic vacancies on the conductivity of La 9.33Si6-xAlxO26-x/2 oxide conductors with an oxyapatite structure. J. Power Sources 2014, 271, 203–212. [CrossRef]
215. Dwivedi, S. Solid oxide fuel cell: Materials for anode, cathode and electrolyte. Int. J. Hydrogen Energy 2020, 45, 23988–24013. [CrossRef]
216. Arshad, M.S.; Raza, R.; Ahmad, M.A.; Abbas, G.; Ali, A.; Rafique, A.; Ullah, M.K.; Rafi, S.; Asghar, M.I.; Mushtaq, N.; et al. An efficient Sm and Ge co-doped ceria based nanocomposite electrolytes. Mater. Res. Bull. 2016, 89, 1129–1136. [CrossRef]
217. Nakayama, S.; Sakamoto, M. Electrical properties of new type high oxide ionic conductor RE10Si6O27 (RE = La, Pr, Nd, Sm, Gd, Dy). J. Eur. Ceram. Soc. 1998, 18, 1413–1418. [CrossRef]
218. Shaula, A.L.; Kharton, V.V.; Marques, F.M.B. Oxygen ionic and electronic transport inapatite-type La10-x(Si,Al)xO26±δ oxide-carbonate electrolyte. J. Solid State Chem. 2005, 178, 2050–2061. [CrossRef]
219. Najib, A.; Sansom, J.; Tolchard, J.R.; Slater, P.R.; Islam, M.S. Doping strategies to optimise the oxide ion conductivity in apatite-type ionic conductors. Dalton Trans. 2004, 2004, 3106–3109. [CrossRef]
220. Preux, N.; Rolle, A.; Vannier, R.N. Electrolytes and ion conductors for solid oxide fuel cells (SOFCs). Funct. Mater. Sustain. Energy Appl. 2012, 370–401. [CrossRef]
221. Durmuş, S.; Çorumlu, V.; Çiçici, T.; Ermiş, I.; Ari, M. Electrical, structural and thermal properties of nanometric (Bi2O3)1-x-y(Ho2O3)x(Tm2O3)y ternary system. Ceram. Int. 2013, 39, 5241–5246. [CrossRef]
222. Gönen, Y.E.; Ermiş, I.; Ari, M. Electrical properties of triple-doped bismuth oxide electrolyte for solid oxide fuel cells. Phase Transitions 2016, 89, 1129–1136. [CrossRef]
223. Jung, D.W.; Lee, K.T.; Wachsmann, E.D. Terbium and tungsten co-doped oxide electrolytes for low temperature solid oxide fuel cells. J. Korean Ceram. Soc. 2014, 51, 261–264. [CrossRef]
224. Jung, D.W.; Lee, K.T.; Wachsmann, E.D. Dysprosium and Gadolinium Double Doped Bismuth Oxide Electrolytes for Low Temperature Solid Oxide Fuel Cells. J. Electrochem. Soc. 2016, 163, F411–F415. [CrossRef]
225. Verkerk, M.J.; Burggraaf, A.J. High oxygen ion conduction in sintered oxides of the Bi2O3-Ln2O3 system. Solid State Ion. 1981, 3–4, 463–467. [CrossRef]
226. Wachsman, E.D. Effect of oxygen sublattice order on conductivity in highly defective fluorite oxides. J. Eur. Ceram. Soc. 2004, 24, 1281–1285. [CrossRef]
227. Cardenas-Terrazas, P.S.; Ayala-Ayala, M.T.; Muñoz-Saldaña, J.; Fuentes, A.F.; Leal-Chavez, D.A.; Ledeizma-Sillas, J.E.; Carreño-Gallardo, C.; Herrera-Ramirez, J.M. High ion conductivity dysprosium and tantalum Co-doped bismuth oxide electrolyte for low-temperature SOFCs. Ionics (Kiel) 2020. [CrossRef]
228. Gao, Z.; Raza, R.; Zhu, B.; Mao, Z.; Wang, C.; Liu, Z. Preparation and characterization of Sm0.2Ce0.8O1.9/Na2CO3 nanocomposite electrolyte for low-temperature solid oxide fuel cells. Int. J. Hydrogen Energy 2011, 36, 3984–3988. [CrossRef]
229. Coles-Aldridge, A.V.; Baker, R.T. Ionic conductivity in multiply substituted ceria-based electrolytes. *Solid State Ion.* 2018, 316, 9–19. [CrossRef]

230. Zuo, C.; Zha, S.; Liu, M.; Hatano, M.; Uchiyama, M. Ba(Zr0.1Ce0.7Y0.2)O3–d as an Electrolyte for Low-Temperature Solid-Oxide Fuel Cells. *Adv. Mater.* 2006, 18, 3318–3320. [CrossRef]

231. Kendrick, E.; Sansom, J. E.H.; Tolchard, J.R.; Islam, M.S.; Slater, P.R. Neutron diffraction and atomistic simulation studies of Mg doped apatite-type oxide ion conductors. *Faraday Discuss.* 2007, 134, 181–194. [CrossRef]

232. Shaheen, K.; Shah, Z.; Galab, H.; Hanif, M.B.; Suo, H. Metal oxide nanocomposites as anode and cathode for low temperature solid oxide fuel cell. *Solid State Sci.* 2020, 102, 106126. [CrossRef]

233. Xing, R.; Wang, Y.; Zhu, Y.; Liu, S.; Jin, C. Co-electrolysis of steam and CO2 in a solid oxide electrolysis cell with La 0.75Sr0.25Cr0.5Sn0.5O3–δ–Cu ceramic composite electrode. *J. Power Sources* 2015, 274, 260–264. [CrossRef]

234. Li, J.; Wei, B.; Yue, X.; Li, H.; Liu, Z. Morphology evolution and exsolution mechanism of a partially decomposed anode for an intermediate temperature-solid oxide fuel cell. *Electrochem. Acta* 2019, 304, 30–41. [CrossRef]

235. Raza, R.; Wang, X.; Ma, Y.; Zhu, B. A nanostructure anode (Cu0.2Zn0.8) for low-temperature solid oxide fuel cell at 400–600 °C. *J. Power Sources* 2010, 195, 8067–8070. [CrossRef]

236. Batool, R.; Gill, R.; Altaf, F.; Ahmad, M.A.; Raza, R.; Khan, M.A.; Hussain, F.; ur Rehman, Z.; Abbas, G. Structural and electrochemical study of Ba0.15Cu0.15Ni0.10Zn0.60 oxide anode for low temperature solid oxide fuel cell. *J. Alloys Compd.* 2019, 780, 653–659. [CrossRef]

237. Raza, R.; Zhu, B.; Fransson, T. H. Zn0.6Fe0.16Cu0.3/GDC composite anode for solid oxide fuel cell. *Adv. Funct. Mater.* 2012, 22, 195–203. [CrossRef]

238. Shaheen, K.; Hashishin, T.; Matsuda, M.; Qiu, N.; Tan, Z.; Ohara, S. High-performance Ni nanocomposite anode fabricated for low-temperature SOFC anodes and analysis on gas diffusion impedance. *Fuel Cells* 2012, 12, 1905–1908. [CrossRef]

239. Mohammed Hussain, A.; Høgh, J.V.T.; Jacobsen, T.; Bonanos, N. Nickel-ceria infiltrated Nb-doped SrTiO3 for low temperature SOFC. *Solid State Ion.* 2008, 181, 2495–2502. [CrossRef]

240. Mohammed Hussain, A.; Sudireddy, B.R.; Høgh, J.V.T.; Bonanos, N. A preliminary study on WO3-infiltrated W-Cu-ScYSZ anodes for low temperature solid oxide fuel cells. *Solid State Ion.* 2007, 180, 2270–2274. [CrossRef]

241. Coles-Aldridge, A.V.; Baker, R.T. Ionic conductivity in multiply substituted ceria-based electrolytes. *Solid State Ion.* 2018, 316, 9–19. [CrossRef]

242. Shaheen, K.; Shah, Z.; Galab, H.; Hanif, M.B.; Suo, H. Metal oxide nanocomposites as anode and cathode for low temperature solid oxide fuel cell. *Solid State Sci.* 2020, 102, 106126. [CrossRef]

243. Xing, R.; Wang, Y.; Zhu, Y.; Liu, S.; Jin, C. Co-electrolysis of steam and CO2 in a solid oxide electrolysis cell with La 0.75Sr0.25Cr0.5Sn0.5O3–δ–Cu ceramic composite electrode. *J. Power Sources* 2015, 274, 260–264. [CrossRef]

244. Li, J.; Wei, B.; Yue, X.; Li, H.; Liu, Z. Morphology evolution and exsolution mechanism of a partially decomposed anode for an intermediate temperature-solid oxide fuel cell. *Electrochem. Acta* 2019, 304, 30–41. [CrossRef]

245. Raza, R.; Wang, X.; Ma, Y.; Zhu, B. A nanostructure anode (Cu0.2Zn0.8) for low-temperature solid oxide fuel cell at 400–600 °C. *J. Power Sources* 2010, 195, 8067–8070. [CrossRef]

246. Batool, R.; Gill, R.; Altaf, F.; Ahmad, M.A.; Raza, R.; Khan, M.A.; Hussain, F.; ur Rehman, Z.; Abbas, G. Structural and electrochemical study of Ba0.15Cu0.15Ni0.10Zn0.60 oxide anode for low temperature solid oxide fuel cell. *J. Alloys Compd.* 2019, 780, 653–659. [CrossRef]

247. Zuo, C.; Zha, S.; Liu, M.; Hatano, M.; Uchiyama, M. Ba(Zr0.1Ce0.7Y0.2)O3–d as an Electrolyte for Low-Temperature Solid-Oxide Fuel Cells. *Adv. Mater.* 2006, 18, 3318–3320. [CrossRef]

248. Wang, C.; Tomov, R.I.; Glowacki, B.A.; Mitchell-Williams, T.B.; Kumar, R.V.; Glowacki, B.A. Inkjet printing infiltration of Ni-Gd:CeO2 anodes for low temperature solid oxide fuel cells. *Electrochim. Acta* 2011, 56, 917–920. [CrossRef]

249. Shaheen, K.; Hashishin, T.; Matsuda, M.; Qiu, N.; Tan, Z.; Ohara, S. High-performance Ni nanocomposite anode fabricated for low-temperature SOFC anodes and analysis on gas diffusion impedance. *Fuel Cells* 2012, 12, 530–536. [CrossRef]

250. Coles-Aldridge, A.V.; Baker, R.T. Ionic conductivity in multiply substituted ceria-based electrolytes. *Solid State Ion.* 2018, 316, 9–19. [CrossRef]

251. Mohammed Hussain, A.; Høgh, J.V.T.; Jacobsen, T.; Bonanos, N. Nickel-ceria infiltrated Nb-doped SrTiO3 for low temperature SOFC anodes and analysis on gas diffusion impedance. *Int. J. Hydrogen Energy* 2012, 37, 4309–4318. [CrossRef]

252. Shaheen, K.; Shah, Z.; Galab, H.; Hanif, M.B.; Suo, H. Metal oxide nanocomposites as anode and cathode for low temperature solid oxide fuel cell. *Solid State Sci.* 2020, 102, 106126. [CrossRef]

253. Xing, R.; Wang, Y.; Zhu, Y.; Liu, S.; Jin, C. Co-electrolysis of steam and CO2 in a solid oxide electrolysis cell with La 0.75Sr0.25Cr0.5Sn0.5O3–δ–Cu ceramic composite electrode. *J. Power Sources* 2015, 274, 260–264. [CrossRef]
352. Koeppel, B.J.; Lai, K.; Khaleel, M.A. Effect of geometry and operating parameters on simulated SOFC stack temperature uniformity. In Proceedings of the ASME 2011 9th International Conference on Fuel Cell Science, Engineering and Technology Collocated with ASME 2011 5th International Conference on Energy Sustainability, Washington, DC, USA, 7–10 August 2011, pp. 475–484.

353. Jaroni, M.S.; Friedrich, B.; Letmathe, P. Economical feasibility of rare earth mining outside China. *Minerals* **2019**, *9*, 576. [CrossRef]