Introduction

So far, many studies have been performed to estimate the roughness coefficient of flow resistance due to the size of the particles, but in these studies, the effect of particle shape is not clearly understood. In alluvial channels of Paul and Jarvis (1976), Bathurst and Ferguson (1986), Petit (1990), San Verida (1991), Robert et al (1992), Prandtl-Karman principle and vertical velocity distribution were used that velocity can be dependent on the logarithm of height. Shear velocity can be calculated according to velocity distribution equations.

\[
\nu^* = \sqrt{\frac{\tau}{\rho}} \quad (1)
\]

where \(\nu^*\) is shear velocity, \(\tau\) is shear stress and \(\rho\) is water density. In totally rough flows, local (spatial) estimation of shear velocity determines the dynamics of sedimentation which may seriously deviate from the results of equation (2). It is due to the significant variability of bed roughness.

\[
\nu^* = \sqrt{gRS_f} \quad (2)
\]

where \(\nu^*\) is shear velocity, \(g\) is gravity, \(R\) is hydraulic radius and \(S_f\) is the energy line slope.

Some literatures studying the effect of sediment particle sizes of the bed and the waterway walls on Manning roughness coefficient (n) are: Strickler (1923), Meyer-Peter and Mueller (1948), Keulegan (1938), Henderson (1966), Anderson et.al (1970) and Huger (1970). They suggested that Manning roughness coefficient is just...
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A function of average bed particle size. Strickler (1923) was the first to present the following equation for determining Manning roughness coefficient \( n \) based on his experimental observations about the rivers with eroded rocky beds in Switzerland:

\[
  n = c_n K_s^{\frac{1}{6}}
\]  

where \( c_n \) is a factor dependent on the definition of \( K_s \), measurement unit, the type of the material covering the floor and walls of the channel. In rivers and sedimentary channels where the bed is made of non-cohesive materials (sand, gravel, pebbles, etc.), the diameter of the particles forming the channel wall \( D \) can be used instead of \( K_s \) (Mahmoodian Shooshtari, 2006). On the effect of slope on Manning roughness coefficient, Hessel, Jeten and Guanxo (2003) conducted some experiments to estimate Manning roughness coefficient for the steep slopes. Jarrett (1984) proposed the following equation to estimate the Manning coefficient:

\[
  n = 0.39 S_f^{0.38} R^{-0.16}
\]

where \( S_f \) is the slope of the energy line and \( R \) is the hydraulic radius in feet. Hydraulically, the flow can be steady, transient or rough. Hydraulically, a steady flow occurs when surficial disturbances are so small that all the roughness elements are generally immersed below the linear layer (Chow, 1959).

Graf (1998), Schlichting and Gersten (2000) defined the flow with smooth, transient and rough beds as follows:

\[
  0 < \frac{u^* K_s}{v} < 5 \quad \text{Smooth (5)}
\]

\[
  5 < \frac{u^* K_s}{v} < 70 \quad \text{Transient (6)}
\]

\[
  \frac{u^* K_s}{v} > 70 \quad \text{Rough (7)}
\]

where \( u^* \) is the shear velocity and \( k \) is the roughness height. Thus, velocity distribution is affected by bed roughness and viscosity (Chow, 1959).

**Materials and Methods**

According to the research objectives, the experiments were conducted using a flume located at Hydraulic Laboratory of Shahrekord University. The flume was rectangular with adjustable slope (length, width and height of 8 m, 40 cm and 40 cm, respectively). To perform the tests, both particle shapes (angular and rounded) were provided in three average grain sizes (10, 20 and 30 mm). Then, for each particle shape, the flume bed was uniformly covered with the intended grading between its both ends with a height that was at least twice the height of \( D_{50} \). Then by creating a uniform flow through the gate located at the end of the flume, water depth readings according to the 4 tested slopes of 0.005, 0.01, 0.015 and 0.02, and the three (initial, intermediate, and final) flow rates of 10, 20 and 30 liters per second, three sections were considered along the flume at a spacing of 2 m. Also, the velocity at every section was measured using pitot tube at 0.2, 0.6 and 0.8 of the water depth at three points of the width of the flume. In order to roughen the river bed by using of sediments, three different gradations in 10, 20 and 30 millimeter sizes were used. Rounded sediments (collected from the river) and angular sediments (produced from the crusher) were employed after they were prepared and graded.

Figure1,2 show an example of angular and rounded particles with 2 gradations, respectively.
The factors affecting Manning roughness coefficient of rough beds are:

\[ n = f \left( \rho, v, y, \mu, g, b, k_s, s_0, SF \right) \]  

(8)

where \( n \) is Manning roughness coefficient, \( \rho \) is unit volume of water, \( v \) is average flow velocity, \( y \) is flow depth, \( \mu \) is mechanical viscosity coefficient of water, \( g \) is gravity, and \( b \) is the width of the channel that was constant in this study (\( b = 0.4 \text{m} \)). \( k_s \) is the average size of the bed particles, \( s_0 \) is the slope of channel floor, and \( SF \) is the shape factor of sedimentary aggregates.

Using Buckingham’s relation and by selecting the three variables of \( \rho, v \) and \( y \) as the repetitive variables, equation 4 can be transformed to equation 5 that includes 5 parameters:

\[ n = f \left( \text{Re}, Fr, S_o, \frac{R}{K_s}, SF \right) \]  

(9)

where \( \text{Re} \) is the Reynolds number, \( Fr \) is the Froude number of flow, \( S_o \) is the channel bottom slope, \( \frac{R}{K_s} \) is the parameter of relative submergence and \( SF \) is the shape factor of the aggregates.

RESULTS AND DISCUSSION

The effect of relative submergence on Manning roughness coefficient

In order to investigate the effect of the shape of sedimentary particles on Manning roughness coefficient, the \((n)\) diagram was plotted versus \( \frac{R}{K_s} \) in Fig. 5 for different flow rates for the bed sediments with the same grading.
As the graph shows, in the same hydraulic conditions, the flow lines are more easily separated from the surface of the angular particles compared to rounded particles, i.e. the separation points of angular particles occur before that of the rounded ones. Thus, the detachment zone created behind every angular particle is larger than that of a rounded particle. As a result, the pressure difference between the front and behind the angular particles is more than that of the rounded particles. As a result, on a rough bed, the total drag forces for angular particles are higher than that of the rounded particles; in another word, the frictional loss of angular particles is higher than that of rounded particles which is consistent with the findings of the study by Shafaei Bajestan (2010).

**The Effect of Grains Size on Manning Roughness Coefficient**

Along a rough bed in the flow direction, both the frictional drag force and the pressure drag of the fluid affect the bed. At the same hydraulic condition, the greater the roughness of the bed, the higher the drag force, since the grain surfaces facing the flow is increased. Therefore, at the same hydraulic conditions, if the particle size increases, Manning roughness coefficient increases. As a result, the drag force becomes smaller which results in reduced drag pressure. Therefore, increased flow rate and depth lead to decreased total drag force, and thereby, decreases the Manning roughness coefficient (Eslamian S. and et al. 2017 & Shayannejad M. and et al. 2015 & Ostad-Ali-Askari and et al. 2015).

As the diagrams in Fig. 6 shows, by increasing the particle size, the Manning roughness coefficient increases; and the increase in roughness coefficient of angular grains is much higher than that of the rounded grains.
The table 1 shows Using SPSS, and with regard to Manning roughness coefficient (n) as the dependent variable, $\frac{R}{K_s}$, $S_0$ and D as independent variables, linear regression analysis was carried out on both rounded and angular beds.

**Table 1. Equivalent roughness on two round and sharp edge beds**

| Particle Size | Round $\alpha = \frac{k_s}{D_{50}}$ | Angular $\alpha = \frac{k_s}{D_{50}}$ | Particle Size |
|---------------|-------------------------------------|--------------------------------------|---------------|
| 4.4           | 5.17                                | 10                                   |
| 3.06          | 5                                   | 20                                   |
| 2.14          | 4.09                                | 30                                   |

**Table 2. Recommended regression equation (multi variant) of Manning roughness coefficient determination in two round and sharp edge beds**

| Fitted equation | R Square |
|-----------------|----------|
| $n = 0.777S_0 - 0.002 \frac{R}{K_s} + 0.3$ | Angular 0.906 |
| $n = 0.723S_0 - 0.001 \frac{R}{K_s} + 0.025$ | Rounded 0.857 |

The table 2 shows This type of regression is a method for finding the relationship between the variable and a set of independent variables.

The equal roughness of the rivers is usually considered equal to a coefficient that is representative of the sedimentary grains of the bed, $k_s = \alpha D_{50}$. The value of $\alpha$ in the rivers with uniform bed materials is equivalent to 1 and $D_{50}$ is assumed as the representative size of the bed materials.

As is clear from the table, the larger the particle, the less the equivalent roughness. For angular beds, the value of this coefficient is higher.

Comparison of the velocity distribution for both rounded and angular cases

The flow with rough bed occurs when the roughness is 6 times $\delta$. In these types of flows, the shear Reynolds $R_s = \frac{u \alpha k_s}{\nu}$ is also greater than 70. These types of flows are also called fully turbulent flows.

As diagram in Fig. 6 shows, the velocity near water surface is greater than the bottom depth of the bed which is due to the existence of secondary flows and fineness ratio.

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Fig7. Dimensionless velocity profiles with 0.015 a slope of 20 mm particle size and discharge of 20 liters per second
Comparison of shear stress distribution of the bed for both rounded and angular cases

As the curve in Fig. 7 shows, the bed shear stress increased with increasing bed particle sizes and the shear stress of angular bed is more than the rounded bed. At the same hydraulic conditions, the flow lines are separated easier from the surfaces of angular particles than that of the rounded particles, i.e. the separation points of angular particles occur before that of the rounded aggregates. Consequently, the pressure difference between the two sides of angular particles is higher than that of the rounded particles. This causes the drag pressure of angular particles to be greater than that of the rounded particles. As a result, the total drag force acting on the rough bed for angular aggregates is higher than the rounded particles, or in other words, the friction losses of angular particles is more than that of the rounded particles. This causes the shear stress of angular particles to be higher than that of the rounded particles.

**Fig8. shear stress with 0.02 slope when discharge is 20 l/s**

**DIMENSIONLESS VELOCITY DISTRIBUTION; ANGULAR AND ROUNDED**

The dimensionless images of velocity distribution in Fig. 9 and 10 suggest that in the rounded bed the slope of velocity variations is milder than the slope of changes in the angular bed. These conditions resemble those of old and young rivers: the angular bed resembles the young rivers whereas the rounded bed is similar to the old rivers.

**Fig9. Chart dimensionless velocity distribution angular**
The Effect of Deposit Particle Sizes on the Shear Velocity of Flow in the Angular and Rounded Beds

Fig. 11 to 13 show the variations of $u/u^*$ versus Reynolds boundary number ($Re^*$) in different gradations for the angular and rounded states. As implied by these Fig., with an increase in $Re$, the value of $u/u^*$ escalates. Moreover, $u/u^*$ is in an inverse relationship with Darcy-Weisbach factor ($f$) and Manning roughness coefficient in Fig. 12 and 17. Therefore, with an increase in Reynolds number, the Darcy-Weisbach factor and the Manning roughness coefficient decline. In addition, as the sizes of bed particles grow, the numerical value of $u/u^*$ as well as the Darcy-Weisbach factor and Manning roughness coefficient escalate. Shafa'i Bajestan and Yar Amadi (2009) also obtained the same results for 4 gradations with the slope. In addition, in this study, velocity profiles were plotted by drawing $u'/u_{\text{max}}$ versus $y'/y_{\text{max}}$ where $u$ denotes the point velocity at a depth of $y$ in the bed, $u_{\text{max}}$ shows the maximum point velocity in each profile and finally $y$ stands for the depth of flow at the bed floor in each profile.

![Figure 10](image_url)  
*Fig10. Chart dimensionless velocity distribution rounded*

![Figure 11](image_url)  
*Fig11. variations of $u/u^*$ versus $Re$ with a 0.01 slope and angular particles*
**Fig12.** The Darcy–Weisbach factor versus \( u/u^* \) with a 0.005 slope and 20 mm particle size

**Fig13.** Manning roughness coefficient versus \( u/u^* \) with a 0.005 slope and 20 mm particle size

**Legends**

| Symbol | Description               |
|--------|---------------------------|
| \( n \) | Manning roughness coefficient |
| \( \rho \) | Density of water |
| \( y \) | Water depth |
| \( R \) | Hydraulic radius |
| \( u^* \) | Shear velocity |
| \( Re \) | Reynolds number |
| \( Fr \) | Froude number |
| \( u_{\text{max}} \) | Maximum speed |
| \( u \) | Average speed |
| \( \tau \) | Shear stress |
| \( \frac{R}{k_e} \) | Relative submergence |
| \( f \) | Darcy-Weissbach factor |
| \( S_0 \) | Bed slope |
| \( D \) | Particle size |
| \( k_e \) | Roughness height |
| \( R^2 \) | Correlation coefficient |
| \( g \) | Gravity |
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