1. Introduction

In large-scale electric energy storage applications, lithium-ion batteries (LIBs) have not met the eventual requirements owing to limited lithium resources, safety hazards, high cost and low power density. Sodium-ion batteries have been brought into focus for renewable energy and smart grids because of the abundant sodium resources and low cost. However, the Na+ has a larger ionic radius (1.06 Å) than Li+ (0.76 Å), which causes sluggish Na+ ion kinetics, reversible intercalation difficulties and electrochemical performances lower than those for Li-ion batteries. Recently, the extensive study of aqueous zinc ion batteries (ZIBs) has begun owing to their low cost, high theoretical capacity (820 mA h g⁻¹) and good cycle stability with a capacity retention of 94% over 500 cycles at 5 A g⁻¹. The good diffusion coefficients and high surface capacity of NaV₃O₈ nanobelts in ZIBs were in favor of fast Zn²⁺ intercalation and long-term cycle stability.

NaV₃O₈ nanobelts were successfully synthesized for Li/Na-ion batteries and rechargeable aqueous zinc-ion batteries (ZIBs) by a facile hydrothermal reaction and subsequent thermal transformation. Compared to the electrochemical performance of LIBs and NIBs, NaV₃O₈ nanobelt cathode materials in ZIBs have shown excellent electrochemical performance, including high specific capacity of 421 mA h g⁻¹ at 100 mA g⁻¹ and good cycle stability with a capacity retention of 94% over 500 cycles at 5 A g⁻¹. The good diffusion coefficients and high surface capacity of NaV₃O₈ nanobelts in ZIBs were in favor of fast Zn²⁺ intercalation and long-term cycle stability.

NaV₃O₈ nanobelts for Li/Na-ion batteries and rechargeable aqueous zinc-ion batteries. Fang Hu, Di Xie, Fuhan Cui, Dongxu Zhang and Guihong Song

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Received 10th June 2019
Accepted 27th June 2019
DOI: 10.1039/c9ra04339j
rsc.li/rsc-advances

Synthesis and electrochemical performance of NaV₃O₈ nanobelts for Li/Na-ion batteries and aqueous zinc-ion batteries

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NaV₃O₈ nanobelts were successfully synthesized for Li/Na-ion batteries and rechargeable aqueous zinc-ion batteries (ZIBs) by a facile hydrothermal reaction and subsequent thermal transformation. Compared to the electrochemical performance of LIBs and NIBs, NaV₃O₈ nanobelt cathode materials in ZIBs have shown excellent electrochemical performance, including high specific capacity of 421 mA h g⁻¹ at 100 mA g⁻¹ and good cycle stability with a capacity retention of 94% over 500 cycles at 5 A g⁻¹. The good diffusion coefficients and high surface capacity of NaV₃O₈ nanobelts in ZIBs were in favor of fast Zn²⁺ intercalation and long-term cycle stability.

NaV₃O₈ nanobelts were successfully synthesized for Li/Na-ion batteries and rechargeable aqueous zinc-ion batteries (ZIBs) by a facile hydrothermal reaction and subsequent thermal transformation. Compared to the electrochemical performance of LIBs and NIBs, NaV₃O₈ nanobelt cathode materials in ZIBs have shown excellent electrochemical performance, including high specific capacity of 421 mA h g⁻¹ at 100 mA g⁻¹ and good cycle stability with a capacity retention of 94% over 500 cycles at 5 A g⁻¹. The good diffusion coefficients and high surface capacity of NaV₃O₈ nanobelts in ZIBs were in favor of fast Zn²⁺ intercalation and long-term cycle stability.
2. Experimental

All chemicals were of analytical grade and were used as received without further purification. In a typical procedure, 0.24 g NaOH, 0.234 g NH₄VO₃ and 0.053 g Na₂CO₃ were added together to a beaker with 50 mL of distilled water and the solution was stirred at 90 °C for 20 min. Then, put the beaker into cool water to room temperature. 1 mL 30% H₂O₂ was dissolved in the solution and stirred about 2 min with the solution color changed to faint yellow. The solution was adjusted to pH = 1.9 by the titration of 2 mol L⁻¹ HCl and kept for stirring about 30 min, the solution color turns to reddish brown gradually. Finally, the solution was thrown into a 50 mL autoclave and subjected to hydrothermal treatment at 200 °C for 24 h. And then, the autoclave was naturally cooled down and red precipitates were collected, followed with wash with distilled water and alcohol for several times, and finally dried at 60 °C. At last, the product was also annealed in air atmosphere at 400 °C for 4 h with an increasing rate of 3 °C min⁻¹.

The crystallographic structure and phase purity of the as-prepared products were measured by a powder X-ray diffraction analyzer (XRD, 7000, Shimadzu) with Cu Kα radiation (λ = 1.5406 Å). The morphology and structure of the samples were characterized by using a scanning electron microscope (SEM, Hitachi-4800) and a high resolution transmission electron microscope (HRTEM, JEM-2100 PLUS) operated at 200 kV. X-ray photoelectron spectra (XPS) measurements were conducted using an ESCALAB250 to investigate the elemental composition using an Al Kα source. The nitrogen adsorption–desorption isotherms at the temperature of liquid nitrogen (77 K) were measured on a NOVA 2200e Surface Area and Pore Porosimetry Analyzer (Gold Spectrum Technology Co., Ltd., China) with prior degassing under vacuum for 4 h at 150 °C. Total pore volumes were determined using the adsorbed volume at a relative pressure of 0.99. The multi-point Brunauer–Emmett–Teller (BET) surface area was estimated from the relative pressure range from 0.05 to 0.2.

Galvanostatic discharge/charge measurements were carried out using Land-2100 automatic battery tester (Land-2100, China). Electrochemical tests were performed by using a coin battery cell, where a metallic lithium foil, sodium foil and zinc foil were used as the anode electrode for Li/Na ion batteries and aqueous zinc ion batteries, respectively. For Li/Na coin cells, NaV₃O₈ active materials (70%, mass fraction) were blended with conductive carbon and 10% poly tetrafluoroethylene (PTFE) onto a carbon paper and dried under air at 60 °C for 12 h. A Whatman grade 3 (47 mm) paper was placed as separator between cathode and anode for Na ion batteries and aqueous zinc ion batteries, respectively. 1 mol L⁻¹ lithium hexafluorophosphate (LiPF₆) dissolved in ethylene carbonate (EC), dimethyl carbonate (DMC) and ethyl methyl carbonate (EMC) (EC : DMC : EMC = 1 : 1 : 8, by v/v ratio) was used as electrolyte. For Na coin cells, the electrolyte was 1 mol L⁻¹ NaClO₄ dissolved in a solvent mixture of ethylene carbonate (EC) and propylene carbonate (PC) (1 : 1 v/v) and 5% FEC. For zinc ion batteries, the coin cells were assembled under room temperature and 1 mol L⁻¹ ZnSO₄·7H₂O and 0.2 mol L⁻¹ Na₂SO₄ mixed solution was used as the electrolyte. Cyclic voltammetry (CV) was carried out using Bio-Logic VSP-300 multichannel electrochemical workstations.

3. Results and discussion

XRD patterns of the as-synthesized NaV₃O₈ (hereafter denoted as NVO) products are showed in Fig. 1a. The diffraction peaks of the as-synthesized NVO could be well indexed to Na₃V₆O₁₆ phase (JCPDS no. 45-0498), and no other impurities are detected. Nitrogen adsorption–desorption isotherms characterization (Fig. 1b) revealed that the Brunauer–Emmett–Teller (BET) surface area of the as-prepared NVO was 25.5 cm² g⁻¹, which could provide large contact area between the materials and electrolyte. XPS analysis of V and O was performed as shown in Fig. 1c and d, respectively. The peaks position of V are centered at 517 eV and 524.5 eV, respectively. The spin–orbit coupling splits the V 2p states into j = 3/2 and j = 1/2 by about 7.5 eV. 28 The peaks located at lower energy of 529.8, 531.3, and 532.5 eV could be assigned to O¹ in NVO, which is similar to the that of V₂O₅. 29 The first one corresponds to O²⁻ ion in the V–O bonding, the second and the third are assigned to OH group in H₂O molecule and C=O on the surface, respectively.

In our experiment, multi-step synthesis of NaV₃O₈ nanobelts can be described by the following reactions:

\[
\begin{align*}
\text{NH}_4^+ + \text{VO}_3^- + 3\text{OH}^- & \rightarrow \text{VO}_4^{3^-} + \text{NH}_3\uparrow + 2\text{H}_2\text{O} \quad (1) \\
\text{VO}_4^{3^-} + 2\text{H}_2\text{O}_2 & \rightarrow [\text{VO}_4(\text{O}_2)_2]^{3^-} + 2\text{H}_2\text{O} \quad (2) \\
2\text{Na}^+ + 4\text{H}^+ + 4[\text{VO}_4(\text{O}_2)_2]^{3^-} + 2[\text{V}(\text{O}_2)_3]^{2+} + \text{H}_2\text{O} & \rightarrow \text{Na}_2\text{V}_6\text{O}_{16} \cdot 3\text{H}_2\text{O} + 5\text{O}_2\uparrow (3) \\
\text{Na}_3\text{V}_6\text{O}_{16} \cdot 3\text{H}_2\text{O} \xrightarrow{\Delta} 2\text{NaV}_3\text{O}_8 + 3\text{H}_2\text{O}\uparrow & (4)
\end{align*}
\]

The reaction (2) showed that [VO₄(Ο₂)₂]³⁻ can be formed by added H₂O₂ with the solution color turned to faint yellow. For the third step, when the pH value of the solution decreased to 1.9, some [VO₄(Ο₂)₂]³⁻ can be converted to [V(O₂)₃]³⁺ with the solution changed to reddish brown. As we known, [VO₄(Ο₂)₂]³⁻ can be converted to [V(O₂)₃]³⁺ totally when the pH value is 1.0.

The SEM image in Fig. 2a and b shows the NVO is composed of long belts-like with lengths of above 50 μm and widths of about 200–300 nm. The TEM results in Fig. 2c show the thickness of NVO nanobelts are about 30 nm. HRTEM in Fig. 2d shows the lattice fringes of 0.195 nm corresponded to the (11–7) planes of NaV₃O₈ and the spot in the SAED pattern was parallel to the length of the NVO nanobelts, indicating the growth direction of the material.

Fig. 3a shows the galvanostatic charge–discharge profiles of NVO nanobelts at a current density of 200 mA g⁻¹ with Li in the voltage range from 4 V to 1.5 V. It can be observed that the
discharge plateaus located at around 3.2, 2.7 and 2.4 V, implying a complex multiphase transition mechanism during the Li-ion insertion process. The initial discharge capacity of NVO nanobelts is about 200 mA h g\(^{-1}\), which corresponds to a 2.26 electron transfer reaction. A high charge capacity of 195 mA h g\(^{-1}\) can be obtained, indicating a high reversibility of NVO nanobelts cathode materials for Li insertion/extraction reactions. After 50 cycles in Fig. 3b, NVO nanobelts can maintain discharge capacity of 153 mA h g\(^{-1}\) with a capacity retention of 76.5% and high coulombic efficiency of 99%. Fig. 3c shows the rate performance of NVO nanobelts with Li at the different current densities of 100 mA g\(^{-1}\), 200 mA g\(^{-1}\), 400 mA g\(^{-1}\) and 800 mA g\(^{-1}\), respectively. The NVO nanobelts electrode presents a high discharge capacity of 76 mA h g\(^{-1}\) at the current density of 800 mA g\(^{-1}\). When the current density finally returned to 100 mA g\(^{-1}\), a capacity of 177 mA h g\(^{-1}\) could be recovered, indicating NVO nanobelts remains stable at high rates. In addition, the electrochemical performance of NVO nanobelts as cathode materials in the voltage range from 4 V to 1.5 V for Na-ion batteries was also investigated. The first three cycled electrochemical Zn-ion storage performance of NVO electrode in Fig. 4a is assessed using CV at 0.1 mV s\(^{-1}\) scan rate in the potential range 0.2–1.6 V. Two strong redox peaks on both cathodic and anodic sweeps are observed, corresponding to continuous reduction (Zn\(^{2+}\) insertion) and oxidation (Zn\(^{2+}\) extraction) of NVO electrode. The redox couple at about 0.80/1.01 V in the cathodic/anodic sweep represents the redox couple at the equilibrium voltage V\(^{5+}\)/V\(^{4+}\) in NVO electrode. Similarly,
the redox couple at 0.46/0.73 V represents the V$^{4+}$/V$^{3+}$ couple. The multiphase vanadium redox couples commonly induce multistep electrochemical intercalation/extraction of various charge carriers in the vanadium-based layered structure. The second and third discharge profiles are similar and slightly different from the first, indicating a steady structure after first

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**Fig. 2** (a) Low magnification SEM images of NVO nanobelts. (b) High magnification SEM images of NVO nanobelts; (c) TEM images of the NVO nanobelts; (d) HRTEM and SAED (inset) image of NVO nanobelts.

**Fig. 3** Galvanostatic charge–discharge profiles (a and d) and cycle performance (b and e) of NVO nanobelts at a current density of 200 mA g$^{-1}$ and 30 mA g$^{-1}$ with Li and Na in the voltage range from 4 V to 1.5 V, respectively. (c and f) The rate performance of NVO nanobelts at the different current density with Li and Na, respectively.
cycle. The largely overlapped CV curves for the NVO electrode suggest the good reversibility of the zinc ions interaction/extraction process and the good retention of crystallinity.

Galvanostatic first charge–discharge profiles of NVO electrodes with Zn are examined at a current density of 100 mA g\(^{-1}\) in the voltage range from 0.2 V to 1.6 V (Fig. 4b). In agreement with the CV curves, the NVO electrode exhibits a profile with two discharge plateau at about 0.84 V and 0.5 V during discharge, respectively. The NVO electrode delivers initial specific discharge capacity of 421 mA h g\(^{-1}\), which is close to the theoretical capacity 529 mA h g\(^{-1}\) of NVO corresponding to 2.37 mol Zn\(^{2+}\) insertion. The calculated first charge capacity is 428 mA h g\(^{-1}\) with a high initial coulombic efficiency (101.7%) for NVO. In the second and third discharge process, these two voltage plateaus of NVO remained in every profile. This phenomenon suggested that the electrochemical reactions might occur without irreversible crystal structure change in the subsequent cycles. The rate performance of NVO electrodes is also tested in Fig. 4c. The average discharge capacities are 400, 303, 270, 231, 166 and 105 mA h g\(^{-1}\) at current densities of 0.1, 0.5, 1, 2, 5 and 10 A g\(^{-1}\), respectively. When the rate is returned to 1 A g\(^{-1}\), the electrode is able to recover a reversible capacity of 270 mA h g\(^{-1}\), indicating a high reversibility of NVO nanobelts cathode materials for Zn insertion/extraction reactions.

Fig. 4d shows the cycling performance and coulombic efficiency of the NVO electrodes at the current density of 200 mA g\(^{-1}\), respectively. After 50 cycles, the discharge capacities are reduced from 400 to 253 mA h g\(^{-1}\), corresponding to the capacity retention of 62%. Fig. 4e shows the cycling performance of NVO in large current density of 5 A g\(^{-1}\). The increase specific capacity of NVO from 139 mA h g\(^{-1}\) to the maximum capacity of 163 mA h g\(^{-1}\) for about the initial 20 cycles is attributed to the activation. After reaching a steady state, the electrode exhibits a decrease in capacity, and at the end of 500 cycles, achieves a capacity of 131 mA h g\(^{-1}\) with retention of 94% of the first discharge capacity, indicating the outstanding rate ability and stable cycling ability of NVO nanobelts electrode.

The Ragone plot in Fig. 4f can be used to evaluate the practical suitability of the NVO electrode along with reported cathode for ARZIBs. This electrode delivers a high specific energy of 302 W h kg\(^{-1}\) at the specific power of 71 W kg\(^{-1}\) based on the active mass of the cathode material, which surpasses those cathodes such as Zn\(_{0.25}\)V\(_2\)O\(_5\), nH\(_2\)O\(_{28}\) V\(_2\)O\(_7\), nH\(_2\)O\(_{29}\) Zn\(_2\)V\(_2\)O\(_7\), nH\(_2\)O\(_{24}\) Na\(_2\)V\(_6\)O\(_{16}\), 3H\(_2\)O\(_{28}\) Na\(_2\)V\(_2\)(PO\(_4\))\(_3\) (ref. 31) and Ca\(_{0.25}\)V\(_2\)O\(_7\), nH\(_2\)O\(_{32}\). The energy density still remained at a high value of 64 W h kg\(^{-1}\) when the power density was as high as 5440 W kg\(^{-1}\), indicating a fast and good electrochemical performance of NVO electrode for ARZIBs.

To further understand the electrochemical kinetics, cyclic voltammetry curves of the NVO electrodes at different voltage scan rates varies from 0.1 to 1.0 mV s\(^{-1}\) with Zn were shown in Fig. 5a. The electrochemical kinetics process can be assumed to fit the following eqn (5).

\[
i = \alpha v^b
\]

where \(i\) and \(v\) are the peak current (mA) and the corresponding scan rate (V s\(^{-1}\)), respectively; \(a\) and \(b\) are variable parameters in which the latter varies in the range of 0.5–1.0. For a given system, the \(b\) value of 0.5 depicts the process of diffusion-limited and the value is 1.0 indicating a capacitive process.
Based on the relationship between log(i) and log(v) for two different peaks, the b-values determined by the slopes of the four redox peaks are 0.61 and 0.79 (Fig. 5b), inferring that the electrochemical kinetics regulation are diffusion-influenced as shown in Fig. 5c.

From eqn (5), to further analyze the combination of surface-controlled capacitive and diffusion-controlled intercalation processes, the following equation is derived:

\[ i = k_1 v + k_2 v^{1/2} \]  

where the first and second compartments in the right side represent the capacity- and diffusion-limited redox reactions, respectively. The calculated capacity- and diffusion-controlled redox values at different scan rates (0.1, 0.2, 0.3, 0.4, 0.5 0.7 and 1 mV s\(^{-1}\)) are calculated as given in Fig. 5c and d. At the scan rate of 0.1 mV s\(^{-1}\), 61% of the capacitive contribution is capacity-limited. When the scan rate improved to 1 mV s\(^{-1}\), nearly 83% of the capacitive contribution is capacity-limited. The results indicate that the capacitance effect play an increasingly important role as the scanning rate is increased. The electrochemical kinetics of NVO indicates that the surface dominated capacitive behaviors of extrinsic NVO nanobelts are in favor of fast Zn\(^{2+}\) intercalation/extraction.

In addition, to determining the average diffusion coefficient around the redox peaks, galvanostatic intermittent titration technique (GITT) measurements are carried out to better understand the kinetics during the diffusion of Zn\(^{2+}\) ions in NVO. The GITT data were collected at a current density of 100 mA g\(^{-1}\) for 10 min and a rest interval of 30 min (Fig. 5e). The ionic diffusion coefficient in NVO electrodes as a function of voltage can be determined by the following equation:\(^{35}\)

\[ \bar{D} = \frac{4}{3} \left( \frac{m_b V_M}{M_b S} \right)^2 \left( \frac{\Delta E_s}{\Delta E_c} \right)^2 \left( \frac{\tau}{L^2} \right) \]  

where \( V_M, m_b, m_b, \) and \( S \) are the molar volume, the molecular weight of the material and the mass, the active surface area of the electrode, respectively. \( L \) is the average thickness of the electrode. If the cell voltage is linearly proportional to \( t^{1/2} \), eqn (8) can be further simplified to the following:\(^{36}\)

\[ \bar{D} = \frac{4}{\pi \tau} \left( \frac{m_b V_M}{M_b S} \right)^2 \left( \frac{\Delta E_s}{\Delta E_c} \right)^2 \]  

where \( \Delta E_c \) and \( \Delta E_s \) represent the total change in the cell voltage during the current pulse and the change in the steady-state voltage of the cell during the step at the plateau potential, respectively. On this basis, one can calculate Zn ions diffusion coefficients of NVO is about 5.0 \( \times 10^{-10} \) cm\(^2\) s\(^{-1}\) to 6.2 \( \times 10^{-12} \) cm\(^2\) s\(^{-1}\) (Fig. 5f). The diffusion coefficients are found to strongly depend on the electrochemical process. The high Zn ions diffusion coefficients would be responsible for the remarkable electrochemical performance of NVO.

Furthermore, \( \text{ex situ} \) XRD analysis in Fig. 6 was carried out to investigate the structure evolution of the NVO nanobelts during the first charge/discharge cycle at the current density of...
100 mA g\(^{-1}\). The obvious reflection peak at 2\(\theta\) = 12.7\(^\circ\) (\(d = 0.69\) nm) as attributed to the (002) plane of NVO. When the electrode was discharged to 0.8 V, a few new peaks appeared at 8.0, 16.1, 24.5, 26.6, 28.7, and 32.9\(^\circ\), which could be indexed to a triclinic \(\text{Zn}_4\text{SO}_4(\text{OH})_6\cdot5\text{H}_2\text{O}\) phase (JCPDS no. 39-0688). The (002) plane of NVO becomes weaker and slightly shifted toward higher 2\(\theta\) positions from 12.7\(^\circ\) to 12.9\(^\circ\). With more \(\text{Zn}^{2+}\) intercalated into the electrode from 0.8 V to 0.2 V, the reflection peaks of \(\text{Zn}_4\text{SO}_4(\text{OH})_6\cdot5\text{H}_2\text{O}\) are gradually strengthened, and the (002) plane of NVO continuously shifted to a higher 2\(\theta\) position (13.0\(^\circ\)), which corresponded to an enlarged interlayer distance of 0.67 nm. This reduction in the interplanar spacing from 0.69 to 0.67 nm indicates an improvement in the structural coordination owing to the strong electrostatic interaction between the intercalated \(\text{Zn}^{2+}\) and the \((\text{V}_3\text{O}_8)^{2-}\) layers. During the subsequent charging process, the reflection peaks of \(\text{Zn}_4\text{SO}_4(\text{OH})_6\cdot5\text{H}_2\text{O}\) gradually disappeared. The formation of this phase can be described by the following reactions:\(^{37}\)

\[
3\text{Zn} + 6\text{OH}^– + \text{Zn}_4\text{SO}_4 \cdot x\text{H}_2\text{O} + (5 – x)\text{H}_2\text{O} – 6\text{e}^– \leftrightarrow \text{Zn}_4\text{SO}_4(\text{OH})_6 \cdot 5\text{H}_2\text{O}
\]

Meanwhile, the (002) plane of NVO shifted back to a lower 2\(\theta\) position from 13.0\(^\circ\) to 12.5\(^\circ\), which demonstrated that the \(\text{Zn}^{2+}\) intercalation and extraction in NVO was highly reversible. The XRD of the electrode after 500 cycles at a current density of 5 A g\(^{-1}\) is investigated in Fig. 6b. The main diffraction peak corresponding to the (002) plane still remains after 500 cycles, indicating a stable structure of the sample and a highly reversible zinc ion intercalation/de-intercalation process in \(\text{NaV}_3\text{O}_8\) electrode.

4. Conclusion

In this work, a facile hydrothermal reaction was developed to prepare \(\text{NaV}_3\text{O}_8\) nanobelts as a promising cathode material for LIBs, NIBs and ZIBs, respectively. Compared to the electrochemical performance for LIBs and NIBs, \(\text{NaV}_3\text{O}_8\) nanobelts cathode materials for ZIBs have shown excellent electrochemical performance, including high specific capacity of 421 mA h g\(^{-1}\) at 100 mA g\(^{-1}\) and good cycle stability with a capacity retention of 94% over 500 cycles at 5 A g\(^{-1}\). \textit{Ex situ} XRD showed that the \(\text{Zn}^{2+}\) intercalation and extraction in \(\text{NaV}_3\text{O}_8\) nanobelts was highly reversible. The capacitive behavior and good \(\text{Zn}\) ions diffusion coefficients played an important role in fast \(\text{Zn}^{2+}\) intercalation/extraction and long cycle stability. This work also indicates that \(\text{NaV}_3\text{O}_8\) nanobelts have a great potential as a cathode material for ZIBs in large-scale electric energy storage applications.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

This work was supported by National Natural Science Foundation of China (No. 51772193) and Nature Science Fund of Liaoning Province (No. 20180550200).

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