Refining bioreactor design using autoclavable glass bonding

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ABSTRACT

Selecting the right design of bioreactors is crucial for guaranteeing the reproducibility of bioprocesses. Up to now, conventionally designed bioreactors consist typically of melted or clamped joints. Since melting of borosilicate glass leads to large deformed areas along the joint, the desired geometric reproducibility is not ensured. Moreover, clamping complicates and greatly restricts the bioreactor design. Bonding, however, is advantageous in that it does not alter the material joined and it is easy to use. Furthermore, it has been recently shown that specially developed glass bonding techniques withstand multiple autoclaving cycles. The current research investigated practice-relevant parameters influencing the lifespan of epoxy- or (urethane) acrylate-bonded glass bioreactors. Hereby, the influence of cleaning and sensitivity to fermentation compounds (ethanol and acetic acid) was quantified using glass-glass and glass-stainless steel specimens. Whereas cleaning did not adversely affect the durability of glass bonds, high concentrations of the fermentation compounds ethanol and acetic acid resulted in accelerated corrosion and subsequent bond failure. Moreover, no effect of eight different epoxy and (urethane) acrylate adhesives was observed on selected model organisms Escherichia coli K12 and Hansenula polymorpha wild type. Another objective of this study was to refine the design of two small-scale bioreactors (ca. 250 mL) by replacing clamps and melted joints by adhesive joints. It was found that the bonded bioreactors yielded a higher geometric reproducibility than that of conventional melted or clamped ones. In conclusion, bonded glass joints greatly enhance the geometric reproducibility of bioreactors and, in turn, the reproducibility of bioprocesses. As glass bonding is easy to handle, it opens up new opportunities to design bioreactors that had been previously too expensive and complicated.

Keywords: Bioreactor; Durability; Borosilicate Glass; Stainless Steel 1.4301; Epoxy Adhesive; Acrylate Adhesive

1. INTRODUCTION

Bioreactor design essentially defines power input, mass transfer, mixing, and, thus, process performance. In particular, for shaken bioreactors, the shape of the reactor wall affects the shape of the rotating liquid and, hence, the mass transfer area [1-4]. Shaken bioreactors are typically applied in screening for optimal strain or process conditions [1,5-8], whereby the differences in performance between the strains and/or conditions are often marginal. Therefore, it is crucial to ensure precise and reproducible environmental conditions for the cultured microorganisms which, in turn, guarantee the reproducibility of bioprocesses. Hereby, the geometry of the bioreactors plays a key role [1,9-11].

Currently, most bioreactors for screening are made of glass, allowing easy visual checking and optical monitoring [1,12-14]. However, the conventional glass joining technologies are problematic. The melting of glass joints lacks geometric reproducibility, because the glass substrate becomes soft in large areas along the joint, resulting in large deformations. Moreover, clamping glass to other materials such as stainless steel, most frequently applied in bioreactors, is complicated, and restricts the whole design. In addition, clamping can lead to gaps at the joint, increasing the risk of contamination of the bioprocess. Since glass is brittle, the clamping exacerbates stress fractures, resulting in fatigue failure at an early stage of use. Furthermore, the different thermal expansions of glass and stainless steel cause problems. All these factors basically reduce the reproducibility and efficiency of experiments in glass bioreactors.

Unlike the conventional glass joining technologies, adhesive bonding presents numerous advantages. Bonding homogeneously distributes stresses. Moreover, the adhesive is easy to apply, has low weight and is inex-
pensive [15-17]. It has been proven that glass adhesive bonds can withstand multiple autoclaving cycles [18].

Nevertheless, the lifespan of bonded glass in bioreactors is not only defined by the long-term durability of the materials but also by practice-relevant parameters such as cleaning, fermentation compounds, and the actual cultivated microorganisms. Thus, this current paper addresses this question. Moreover, in order to improve the reproducibility of experiments in small-scale bioreactors, another principal aim of the current study is to refine the design of two small-scale bioreactors (ca. 250 mL) in terms of enhancing the geometric reproducibility and simplifying their design.

2. MATERIALS AND METHODS

2.1. Materials

Materials tested were borosilicate glass Duran 3.3 ISO 3585 (Duran Group GmbH, Mainz/Germany) and stainless steel 1.4301 (LKT GmbH, Aachen/Germany). As adhesives, the two-component epoxy M-31 CL (Henkel-Löctite, Garching/Germany) and the UV-curable urethane acrylates GB 368 (Delo Industrial Adhesives, Windach/Germany) and Vitralit 7563 (Panacol-Elosol, Oberursel/Germany) were applied.

2.2. Curing Procedure

All surfaces were degreased with 2-butanolone (“MEK” for the non-scientific name methyl-ethyl-ketone) before application of the adhesive. To possibly improve the bond durability, part of the glass and steel components was additionally pre-treated with Pyrosil® [18]. The curing cycles applied to the adhesives were recommended by the manufacturers (confer to Table 1). The M-31 CL was cured at ambient temperature for 5 days or thermally at 65°C for 2 h. In all cases, the adhesive thickness was controlled at 0.2 mm by glass beads (Sigmund Lindner GmbH, Warminsterich/Germany).

2.3. Accelerated Aging by Autoclaving

For accelerated aging tests, shear specimens were produced according to a previous study [18]. The aging of the specimens was accelerated in at least 25 standard cycles of autoclaving (20 minutes at 121°C, 2 bar, saturated steam) in a D-65 autoclave (Systec, Wettenberg/Germany). The shear strength was measured at ambient temperature (RT) according to Bähr et al. [18].

2.4. Investigation of Practice-Relevant Parameters

2.4.1. Cleaning

Specimens made of borosilicate glass/borosilicate glass (”bor-bor”) and borosilicate glass/stainless steel (“bor-st”) were bonded with the urethane acrylate GB 368 or the two-component epoxy M-31 CL after degreasing with MEK or an additional Pyrosil® pre-treatment. The M-31 CL was cured as recommended by the manufacturer as well as cured thermally (Section 2.2).

Since bioreactors with glass bonds are typically applied in biotechnological and medical applications, the following two standard cleaning programs were chosen (Miele & Cie. KG, Gütersloh/Germany): SM1 to clean laboratory equipment and SM2 to clean medical devices such as surgical instruments. These standard programs were adapted to meet worst-case scenarios in terms of temperature and the concentration of cleaning agents. The modifications applied were: 1) utilization of 1% cleaner containing active chlorine (HOCl) in SM1, 2) increased concentration (0.5%) of phosphoric acid for neutralization (normally 0.1% - 0.3%) in both cleaning programs. 3) SM1 is characterized by two alkali cleaning phases while common cleaning procedures for such laboratory equipments contain only one. In SM1, the cleaning material was exposed to maximal temperatures of 80°C during cleaning phase and 85°C during final rinse. In SM2, the cleaning material was exposed to more ambient temperatures <60°C during cleaning phases even to 93°C during the subsequent thermal disinfection.

Ten specimens of each substrate/adhesive/pre-treatment combination were cleaned in 50 cycles of SM1or SM2. After cleaning, five specimens were additionally autoclaved in 50 standard autoclaving cycles (Section 2.3). The shear strength was measured (Section 2.3) immediately after cleaning or after the additional autoclaving.

2.4.2. Loading during Autoclaving

The bond durability under load during autoclaving was investigated, because the equipment is typically loaded with other devices during actual autoclaving e.g. in a tabletop autoclave. To simulate a realistic scenario, spe-

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**Table 1.** Adhesives tested concerning the influence on model microbes.

| Adhesive | Manufacturer | Chemical structure | Curing |
|----------|--------------|--------------------|--------|
| GB 310   | Delo (Windach, D) | Acrylate | UV 320 - 400 nm, 20 s |
| GB 368   | Delo (Windach, D) | Urethane acrylate | UV 320 - 420 nm, 15 s |
| J-20537  | Dymax (Frankfurt, D) | Urethane (meth) acrylate | UV 300 - 500 nm, 20 s |
| Vitralit 6128 | Panacol-Elosol (Oberursel, D) | Acrylate | UV-A 60 mW/cm², 15 s |
| Vitralit 7563 | Panacol-Elosol (Oberursel, D) | Acrylate | UV-A 40 mW/cm², 15 s |
| M-31CL   | Henkel-Löctite (Garching, D) | Two-component epoxy | 5 d, RT |
| Epo-Tek 353 ND | Polytec PT (Waldbronn, D) | Two-component epoxy | 48 h, RT + 1 h, 120°C + 1 h, 150°C |
| EPVP 4611/4 | Polytec PT (Waldbronn, D) | Two-component epoxy | 16 h, RT |
cimens made of bor-bor and bor-st (bonded with GB 368 and pre-treated by MEK degreasing or additionally treated with Pyrosil®) were autoclaved under load of 143 g, which is the weight of a RAMOS flask equipped with caps (confer Section 2.5.1). The load of such specimens was realized as depicted in Figure 1.

2.4.3. Fermentation Compounds
Since there are many fermentation compounds in bio-processes, the investigated substances were restricted to ethanol and acetic acid. Both ethanol and acetic acid are highly reactive and common in microbial processes (ethanol as target product reviewed in [19-22]; acetic acid as target product in [23-26]). Therefore, bor-bor and bor-st specimens bonded with GB 368 or M-31 CL were autoclaved both in 25 and 50 standard cycles, whereby they were immersed in a 120 g/L (15% (w/v)) ethanol/200 g/L acetic acid (20% (w/v)) solution. The concentrations of ethanol and acetic acid were chosen as the maximal concentrations found in the literature for microbial processes [27-29]. To guarantee almost constant concentrations of ethanol and acetic acid during the autoclaving, the solutions were renewed every tenth cycle of steam sterilization. Afterwards, the shear strength of the bonded glass specimens was measured (Section 2.3).

The concentrations of ethanol and acetic acid were monitored using HPLC with an Organic Acid Resin HPLC pre-column (40 × 8 mm) and Organic Acid Resin HPLC column (250 × 8 mm) (both CS Chromatographie, Langerwehe/Germany). 5 mM sulphuric acid was used as eluent (flow rate 0.6 mL/min). The ethanol or acetic acid was detected by UV diode array detector UVD 340S (Dionex Softron, Germering/Germany). Peak analysis and calculation was performed with Chromelopean software version 6.3 (Dionex Softron, Sunnyvale/USA).

2.4.4. Model Microorganisms
Since the applied adhesive could influence the cultivated microbes, the bacterium Escherichia coli K12 (German Collection of Microorganisms 498) and the yeast Hansenula polymorpha wild type strain (German Collection of Microorganisms 70277) were cultivated in presence of disks made of pure adhesive. These cultivations were carried out in a Respiration Activity Monitoring System (RAMOS) [6,30] to monitor possible adverse effects of the adhesive on the metabolic activity of the microbes. RAMOS has already been successfully used for several investigations [6,30-35].

Adhesive disks (see Table 1) were produced as disks having a diameter of 15 mm and a height of 1 mm. Immersed in deionized water, the specimens were sterilized in a standard autoclaving cycle. Then two disks were added to the microbial cultures. As positive controls, cultures without adhesive disks were conducted in parallel. After cultivation, the adhesive disks were washed with deionized water and optically checked with regard to changes of surface topology or color before the microbial cultures were sterilized to kill the microorganisms. Afterwards, the adhesive disks were washed and re-dried in a glass dish at ambient temperature for 24 h. The color and the surface topology of the adhesive disks were documented 1) before and 2) after autoclaving to sterilize the disks, 3) after cultivation, 4) after that second autoclaving, and 5) after re-drying of the autoclaved disks.

Cultivation conditions: Both microorganism strains were cultivated in shake flasks in 10 mL mineral media at 37°C, a shaking frequency of 350 rpm and a shaking diameter of 50 mm. E. coli K12 was cultivated in Wilms MOPS medium at pH 7.5 [36,37] and H. polymorpha wild type in Syn6 MES medium at pH 6.4 [38] prepared according to Jeude et al. [39]. These cultures were inoculated with 4% (v/v) of exponentially growing pre-cultures. The pre-cultures of E. coli K12 were grown in 12.5 mL Luria-Bertani complex medium containing 5 g/L yeast extract, 10 g/L tryptone and 5 g/L sodium chloride. H. polymorpha was pre-cultivated in yeast extract (10 g/L)/peptone (20 g/L) complex medium at pH 6.5 containing 20 g/L glucose [38,40]. All pre-cultures were inoculated with 1 mL glycerol stock (750 µL culture grown on respective complex medium + 250 µL 80% (w/w) glycerol).

2.5. Refining the Design of Two Small-Scale Bioreactors Using Autoclavable Glass Bonding

2.5.1. Bonded RAMOS Flask
The Respiration Activity Monitoring System (RAMOS) allows the online monitoring of respiration activity as the key variable in shake flasks. The respiration rates for oxygen and carbon dioxide are the most suitable measur-
able variables to quantify the physiological state of aerobic microorganisms. The current RAMOS flasks are produced by melting threads to a conventional 250 mL Erlenmeyer flask (Figure 2(a)). The newly designed bonded RAMOS flask (Figure 2(b)) consists of a stumped flask covered by a borosilicate glass plate bonded on top. The stumped flask was produced from a commercial 250 mL Erlenmeyer flask that was cut off at a height of 52 mm using a diamond cutter (Quarzglas Heinrich, Aachen/Germany). The cover plate was equipped with four borosilicate glass connection threads for aeration (GL 18), sensor fixation (GL 32), and sampling (GL 18) (all from Duran, Mainz/Germany). The holes in the cover plate for the threads were drilled with a diamond drill (Quarzglas Heinrich, Aachen/Germany). Furthermore, two aeration tubes in the flask were made of stainless steel 1.4301 (mechanical workshop, AVT. BioVT, RWTH Aachen University). All cut faces were smoothed with corundum 400.

Since it is known that the side of float glass that has been in contact with the tin bath during the production process (referred to as the “tin side”) has altered surface properties [41,42], it may affect the durability of adhesive bonds. This side of the cover plate was identified using UV light at 254 nm (UV lamp NU 4 watt; Roth, Darmstadt/Germany). The tin ions fluoresce and produce a milky white image that is slightly visible to the human eye in a darkened room [43]. The tin side was determined as the bottom side of the flask bonded onto the flask.

Before application of the urethane acrylate adhesive GB 368, all joint faces were degreased with MEK. The curing was performed using a UV lamp NU 4 watt at 366 nm (Roth, Darmstadt/Germany) according to the manufacturer’s specifications. The adhesive thickness was controlled at 0.2 mm by glass beads (Sigmund Lindner GmbH, Warmensteinach/Germany). First, the aeration tubes were bonded on the bottom side of the cover plate and then the threads were bonded on the upper side. After curing of 24 h, the so equipped cover plate was then bonded onto the flask stump.

2.5.2. Validation of the Newly Bonded RAMOS Flask
First, the tight fitting of the aforementioned bonds was checked, whereby the inner pressure of the flasks was increased by 25 mbar and monitored in the RAMOS device for 16.5 h. The maximum oxygen transfer capacity of the newly designed RAMOS flask was determined based on sulfite oxidation according to Hermann et al. [44] and Maier et al. [3]. The measurements were performed at 37°C in a RAMOS device with a shaking frequency of 350 rpm and a shaking diameter of 50 mm. The filling volume was varied from 10 to 15 mL.

To compare the conventionally melted RAMOS flasks and the newly bonded RAMOS flasks in biological experiments, parallel cultivations of the model organisms E. coli K12 (DSM 498) and the yeast H. polymorpha wild type strain (DSM 70277) were performed in the RAMOS device as described in Section 2.4.4.

2.5.3. New Design of COSBIOS Reactor
The Continuous Operated Shaken BIOreactor System (COSBIOS) enables parallel continuous fermentations on a small scale [45]. Figure 3 compares the design and fabrication of the current clamped COSBIOS reactor to that of the newly designed bonded reactor. The newly designed COSBIOS reactor (Figure 3(b)) consists of a borosilicate glass cylinder, an outlet, a screw cap, a bottom plate, and a threaded ring. All of the last three components consist of stainless steel 1.4301. The screw cap is made of poly-ether-ether-ketone. Furthermore, the cover plate (Quarzglas Heinrich, Aachen/Germany) is equipped with five GL 14 threads (Duran, Mainz/Germany). A hole was tangentially drilled into the glass cylinder (Quarzglass Heinrich, Aachen/Germany). The steel outlet was fit to the outer cylinder shape and bonded on

Figure 2. Design of the original melted-joined RAMOS flask (a) and the newly designed bonded one (b); new RAMOS flask bonded with GB 368 (Delo, 15 s cured using UV light (366 nm)), joint faces smoothed with corundum 400 and degreased with 2-butanone.
the hole (Figure 3(b)). Afterwards, the cylinder was bonded into a notch of the bottom stainless steel plate. Finally, the threaded ring below the screw cap was bonded to the top of the glass cylinder. GB 368 was used for all bonds. Curing was performed according to Section 2.5.1.

3. RESULTS AND DISCUSSION

3.1. Investigation of Practice-Relevant Parameters

The lifespan of the bonds [18] is not only influenced by the composition of the adhesive and materials but also by the application conditions. Therefore, the practice-relevant parameters of cleaning and fermentation compounds as well as the effect of adhesive on the actual cultivated microorganisms were investigated in this study.

3.1.1. Cleaning

One of the most important factors affecting the adhesive joints and respective bonded glass devices is multiple cleaning. Thereby, the cleaning process can affect the adhesive or the glass substrate: The cleaning agents can penetrate into the polymer matrix and sharp temperature changes can stress the adhesive polymer. Furthermore, alkaline cleaning agents can cause glass corrosion. In general, cleaning material is longer exposed to high temperatures (up to 85°C) in SM1 than in SM2 which may thermally stress the adhesive bonds. Further load are frequent and rapid temperature changes as well as the additional alkaline cleaning phase. Cleaning programs for medical devices such as SM2 commonly contain two alkaline cleaning steps: one to remove organic debris and one for disinfection (for SM2, at high temperature of 93°C). For disinfection, hydrogen peroxide is used which can also attack the adhesive joint and the glass substrate as well.

For the substrate combination bor-bor, the shear strength of specimens bonded with the urethane acrylate GB 368 (Figure 4(a)) and degreased with MEK decreased from 13.4 MPa to 7.6 MPa after cleaning in SM1 and decreased from 13.4 MPa to 11.0 MPa after...
cleaning in SM2. A similar trend occurred after 50 additional autoclaving cycles, whereby the shear strength changed from 13.4 MPa to 9.4 MPa and to 14.2 MPa for the respective SM1 and SM2 cleaning programs. During the subsequent autoclaving, the shear strength increased almost up to those values of the unaged specimens. Specimens additionally pre-treated with Pyrosil® showed higher shear strengths both before (16.3 MPa) and after the two aging steps (12.7 MPa in SM1 and 13.9 MPa in SM2) where no post-curing occurred. Thereby, a lower loss of shear strength was observed for Pyrosil®-treated samples than the loss of shear strength of only degreased specimens, in particular for GB 368 specimens cleaned in SM2. Consequently, multiple cleaning, both in SM1 and SM2, did not significantly affect the bond durability of the urethane acrylate GB 368. The shear strength loss is lower for cleaning in SM2 indicating that longer exposure to high temperatures and rapid temperature changes of SM1 affect the bond durability more significantly.

By contrast, the specimens bonded with the two-component epoxy M-31 CL (Figure 4(b)) and additionally pre-treated with Pyrosil® lose one-half to two-thirds of their initial shear strength of 23 MPa due to aging during both cleaning programs. Nevertheless, the shear strengths increased during autoclaving, which implies a post-curing by the steam sterilization. Interestingly, the shear strength of specimens degreased with MEK increased after cleaning in both programs as well as after additional autoclaving compared to the initial shear strength tested before treatment. On the other hand, the initial shear strength of those specimens degreased with MEK was extremely low (7.8 MPa) compared to those of Pyrosil® pre-treated specimens (23.2 MPa). Moreover, glass breakage was observed as a material failure, whereby the adhesive bonds stay intact independent of the glass, the steam sterilization corrodes the steel surface, which subsequently catalyzes the polymer degradation of the adhesive [46].

Comparing the shear strengths of bor-bor and bor-st specimens, the shear strength of the bor-bor specimens decreased. However, the shear strength of bor-st samples rose significantly indicating a post-curing. The results concerning the cleaning programs SM1 and SM2 did not differ. To compare the two curing cycles (at ambient temperature and at 65°C, respectively) of the epoxy resin M-31 CL, the residual shear strengths were similar both after cleaning and autoclaving. Thus, the thermal curing did not lead to improved lifespan as has been already observed in a previous study [18].

In summary, cleaning—even in worst-case scenarios—did not adversely affect the shear strength of adhesive joints. Nevertheless, the tested duration of cleaning was rather short with respect to long-term lifespan of adhesive joints in autoclaving (i.e. 800 cycles). It can be expected that multiple cleaning steps will harm the bond itself and hence shorten the lifespan of a bioreactor. In general, it can be concluded that both GB 368 and M-31 CL adhesives are suited for application in biotechnology and medicine. Regarding the substrate combination bor-bor, both tested adhesives behaved similarly during the cleaning procedures in SM1 and SM2. Moreover, the thermal curing had no effect on the M-31 CL bonds. In the bor-st joints, however, the bond shear strength increased during cleaning and, in particular, during the subsequent autoclaving. In this case, differences in shear strength after cleaning in SM1 and SM2 were also observed.

3.1.2. Loading during Autoclaving
The bond durability under load during autoclaving was investigated. Thus, the adhesives tested in a previous study showed only very low shear strength under autoclaving conditions due to softening of the adhesive polymer and, subsequently, resulting in a reduced capability to bear loads [18]. Therefore, bor-bor and bor-st specimens were loaded during the autoclaving process with 143 g, which is the weight of a fully equipped RAMOS flask as one of the reactors refined in this study. All bor-bor specimens already failed in the first 11 autoclaving cycles, whereas the single lap joints of the bor-st substrate combination withstand 100 autoclaving cycles (data not shown). Interestingly, the shear strength loss of the latter combination was significantly higher in the previous study (50% instead of 18%). However, this accelerated failure of the bor-bor specimens can be explained by the shear stress of the bor-bor specimens applied at an angle 90° of the unsupported adherent (Figure 1). By contrast, the joint face of the bor-st specimens was compressively loaded instead of by shear load.
stress and the load can be borne by the second adherent (Figure 1). Consequently, shear loading of unsupported adherents—as in the case of the bor-bor specimens—should be avoided.

3.1.3. Fermentation Compounds
The cultivation medium and metabolic products come into contact with the adhesive and, consequently, can influence it. In this regard, ethanol and acetic acid, both being either potential substrates or products in bioprocesses, were examined in the presence of adhesive bonds.

HPLC measurements showed that the ethanol concentration decreased from 120 g/L to 3.76 g/L during 10 autoclaving cycles because ethanol is highly volatile. The acetic acid concentrations only slightly dropped from 200 g/L to 192.5 g/L.

After 25 and 50 autoclaving cycles, the shear strength of the respective adhesive joints dramatically decreased (Figure 5). Thus, the shear strength of bor-bor specimens, degreased with MEK declined from 13.4 MPa before aging to 7.9 MPa after 25 autoclaving cycles and to 7.0 MPa after 50 autoclaving cycles. A similar trend was observed for Pyrosil® treated bor-bor samples (6.6 MPa after 25 and 50 cycles, respectively).

For the substrate combination bor-st, the shear strength was more dramatic. Here, the shear strength of previously degreased specimens (MEK) dropped from 19.9 MPa to 6.4 MPa after 25 autoclaving cycles and to 2.1 MPa after 50 autoclaving cycles meaning, inferring a shear strength loss of up to 90%. Compared to the shear strength loss of the joints observed after 400 standard cycles of steam sterilization without ethanol or acetic acid, the loss observed in the presence of those fermentation compounds was more than 30% higher [18]. The Pyrosil® treated samples already failed after 50 autoclaving cycles. This development indicates a dramatic attack on the adhesive joints by ethanol and acetic acid. Since high concentrations of these common fermentation compounds lead to that dramatic boost of adhesive joint aging, it can be concluded that other reactive fermentation compounds also adversely affect the bond durability. Therefore, the contact between fermentation compounds and the joint faces should be avoided in the reactor design, if possible.

The shear strength loss for the respective bor-st joints was much more pronounced than that of bor-bor specimens. After 50 autoclaving cycles, the bor-st bonds totally failed. This failure can be attributed to steel corrosion. An additional pre-treatment of the stainless steel substrate could prevent this corrosion. In this context, the Pyrosil® pre-treatment, which physicochemically modifies the surface of stainless steel, did not lead to an improved bond lifespan, although it forms durable joints that withstand frequent autoclaving in the absence of ethanol and acetic acid. When the aggressive compound acetic acid is present, the failure may be attributed to reaction of acetic acid with e.g. the siloxane groups of borosilicate glass formed by the Pyrosil® pre-treatment. Furthermore, this may explain the generally lower residual shear strength of Pyrosil®-treated specimens—indepedent whether bor-bor or bor-st was applied.

3.1.4. Interactions of Adhesives and Cultivated Microorganisms
If microorganisms come into contact with the adhesives, they can metabolize the respective adhesive or their metabolic products can react with the adhesive. To investigate these possible microbial effects, the bacterium E. coli K12 and the yeast H. polymorpha wild type strain were cultivated in the presence of adhesive disks.

Some of the investigated adhesive disks, e.g. the (urethane) acrylates GB 310 and GB 368 and Vitralit 6128, became opaque due to autoclaving during the cultivation processes. Moreover, transparent adhesives discolored during the cultivation itself and/or during the following autoclaving. The degree of discoloring correlates well with the pigmentation of the cultivated microorganisms and the medium. Since the yeast H. polymorpha and its cultivation medium are pigmented more intensively, the adhesive disks cultivated in the respective batches showed a more intense color. Nevertheless, other changes in the adhesive disk surface such as roughening were not observed.

The respective RAMOS curves exemplarily show the same progress for E. coli K12 cultures (Figure 6(a)) in the presence of the acrylate adhesive Vitralit 7563 and the two-component epoxy adhesive EPVP 4611/4 compared to the growth without any adhesive (control batch).
In addition, no differences in the respiration activity of the yeast H. polymorpha (Figure 6(b)) were observed in the presence of the (urethane) acrylates GB 310 and GB 368. Therefore, the tested adhesives did not affect the microbial growth of the chosen model organisms.

3.2. Refining the Design of Two Small-Scale Bioreactors Using the Autoclavable Glass Bonding

Based on previous work [18] and the aforementioned results, the design of two glass bioreactors for small-scale fermentations was refined using the newly developed autoclavable glass bonding technique. The basis for the design optimization was a conventional RAMOS (Respiration Activity MOntoring System) flask with melted bor-bor joints. Moreover, as a second example, a typical COSBIOS (Continuous Operated Shaken BIoreactor System) reactor with clamped glass steel joints served as the starting point for the design refinement.

3.2.1. Bonded RAMOS Flask

To produce the original RAMOS flask, threads for aeration, sensor fixation and sampling were melted onto a conventional 250 mL Erlenmeyer flask (Figure 2(a)). These modifications by melting inherently lead to a poor geometric reproducibility of the top part of the flasks due to the large deformed area by the thermal treatment. To guarantee identical geometries and, therefore, fluid-dynamic conditions in the bottom part of the flasks as in a conventional shake flask, this RAMOS flask has a “buffer zone” between the upper part and the bottom part (Figure 2(b)), defined by the maximal height of the rotating fluid. The buffer zone results in an enlarged head-space volume, reducing the sensitivity of the measuring device.

The design of the RAMOS flask was refined, whereby a conventional 250 mL Erlenmeyer flask was cut down to a height of 52 mm, corresponding to operation conditions as 400 rpm shaking frequency, a 15 mL filling volume, and a 50 mm shaking diameter. Consequently, the buffer zone could be eliminated (Figure 2(b)), thereby increasing the geometric reproducibility and the measuring sensitivity. On this 52 mm high stump, a cover plate made of boro-silicate glass and equipped with connections for aeration, sensor fixation and sampling was bonded. Figure 2 illustrates the comparison of the newly designed RAMOS flask to the conventional joint-melted one. Seven of these bonded prototypes were fabricated.

The geometric reproducibility of the bonded RAMOS flasks was compared to that of the conventional flasks. The average volume of the seven bonded prototypes was 228.3 mL versus 278.5 mL of the conventional RAMOS flasks (56 flasks), which means a volume reduction of 18%. Furthermore, the volume of the bonded flasks deviated maximally 2 mL from the mean value which is within the production tolerance of conventional 250 mL Erlenmeyer flasks; this implies an enhanced geometric reproducibility of the newly designed bonded flasks.

Since these reactors are utilized to monitor the oxygen transfer rate (OTR), the carbon dioxide transfer rate (CTR) and the respiratory quotient (RQ) by an exhaust gas analysis, the tightness of flasks is essential to obtain accurate results. During 16.5 h, the pressure losses in bonded RAMOS flasks amounted 0.0108 mbar/h compared to 0.094 mbar/h in melted-joined flasks (data not shown). Therefore, the bonded RAMOS flasks showed a similar tight fitting as the melted-joined ones and can be applied to RAMOS measurements. Moreover, the maximum oxygen transfer capacity (OTRmax) of the newly designed RAMOS flask was determined as 45 mmol/L/h for a filling volume of 10 mL and as 37 mmol/L/h for 15 mL. Similar values were obtained in the melted-joined flasks with 52 mmol/L/h for a filling volume of 10 mL and 37 mmol/L/h for a filling volume of 15 mL.

The bonded flasks were evaluated in various cultivation experiments by comparison to the joint-melted flasks. Cultivations of the aforementioned model organisms E. coli K12 and H. polymorpha wild type showed no differences between both types of RAMOS flasks, as can be seen from Figure 7. Consequently, the newly bonded RAMOS flasks with a higher geometric reproducibility can indeed replace the conventional RAMOS flasks. The adhesively bonded prototypes have been routinely used in the laboratory and already have withstood quently, the newly bonded RAMOS flasks with a higher geometric reproducibility can indeed replace the con-
The small scale COSBIOS combines the advantages of continuous fermentation 
and rarely performed with conventional equipment [45,47]. Since the reactor cylinder is made of expensive poly-ether-ether-ketone, and weight. Costs are reduced by switching to less expensive borosilicate glass and by reducing the amount of poly-ether-ether-ketone needed.

The weight of reactor was diminished because of less material needed and which minimizing the risk of stress ruptures, the costly quartz glass cylinder is increased, in particular, by the significant differences between the thermal expansions of quartz glass (1 × 10⁻⁶ K⁻¹) and stainless steel (17 ×10⁻⁶ K⁻¹).

Figure 3 compares this conventional COSBIOS reactor to the newly designed one, which is assembled using autoclavable glass bonding. The bonded reactor (Figure 3(b)) consists of a stainless steel outlet instead of a glass one. The stainless steel outlet is bonded to the borosilicate glass cylinder (Figure 3(b), right side). Since this outlet does not have to be welded to the cylinder, the quartz glass cylinder can be replaced by less expensive borosilicate glass material. The use of a stainless steel outlet guarantees an enhanced geometric reproducibility of this component compared to that made of quartz glass, because it can be produced with higher precision. Unlike the conventional COSBIOS reactor, the cylinder was directly bonded onto the bottom plate, which can now be considered as a single-part component. Hence, clamping is no longer necessary and the former three gaskets could be replaced by simply one (between cover plate and the screw cap).

To guarantee a high application flexibility of the bonded reactor and easy cleaning, the cover plate was not bonded to the cylinder but is still fixed by a poly-ether-ether-ketone screw cap. Nevertheless, the number of components was reduced from fourteen to six due to the omission of braces, thus simplifying the design and handling of this new bioreactor. Furthermore, the diameter of the threaded ring and the screw cap could be minimized, thereby saving material, in particular the extremely expensive poly-ether-ether-ketone, and weight.

To summarize the refinements of the COSBIOS reactor achieved using autoclavable glass bonding results in the following advantages:

- The production process is simplified due to omission of braces and drill holes.
- Material is saved due to the minimized diameter of the screw cap and threaded ring.
- Costs are reduced by switching to less expensive borosilicate glass and by reducing the amount of poly-ether-ether-ketone needed.
- The handling is simplified due to reduction of components (six instead of fourteen).
- The weight of reactor was diminished because of less material needed and which minimizing the risk of shaker imbalances, thereby prolonging the lifespan of expensive shakers.
- The risk of stress ruptures is minimized and finally resulting in an improved lifespan of the reactors and, subsequently, in a further cost reduction.
- The risk of contamination is minimized, thereby simplifying the design and handling of this new bioreactor.
enhancing profitability of elaborate and time-con-
csuming continuous fermentations.

These numerous advantages illustrate the high poten-
tial of autoclavable glass bonding to simplify fabrication
and handling as well as the profitability of perspective
bioreactors.

4. CONCLUSIONS

Glass bonding greatly enhances the geometric repro-
ducibility of bioreactors. As it is easy to handle, it opens
up new opportunities to design bioreactors that had been
previously too expensive and complicated. Thus, by of-
fering more degrees of freedom, these autoclavable glass
bonding techniques ultimately break down current de-
sign barriers. Designs can be implemented which have
been impossible so far because of the lack of a suited
technology.

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REFERENCES

[1] Büchs, J. (2001) Introduction to advantages and prob-
lems of shaken cultures. Biochemical Engineering Jour-
nal, 7, 91-99. doi:10.1016/S1369-703X(00)00106-6

[2] Maier, U. and Büchs, J. (2001) Characterisation of the
gas-liquid mass transfer in shaken bioreactors. Biochemi-
ical Engineering Journal, 7, 99-106. doi:10.1016/S1369-
703X(00)00107-8

[3] Maier, U., Losen, M. and Büchs, J. (2004) Advances in
understanding and modeling the gas-liquid mass trans-
fer in shake flasks. Biochemical Engineering Journal,
17, 155-167. doi:10.1016/S1369-703X(03)00174-8

[4] Galindo, E., Flores, C., Larralde-Coronah, P., Corkidi-
Blanco, G., Rocha-Valadez, A.J. and Serrano-Carréon, L.
(2004) Production of 6-pentyl-α-pyrone by Trichoderma
harzianum cultured in unbaffled and baffled shake flasks.
Biochemical Engineering Journal, 18, 1-8. doi:10.1016/
S1369-703X(03)00115-3

[5] Calam, C.T. (1996) Shake flask fermentations. In: De-
main, A.L. and Solomon, N.A. Eds., Manual of Indus-
trial Microbiology and Biotechnology, American Society
for Microbiology, Washington, DC, 59-65.

[6] Anderlei, T., Zang, W., Papaspyrou, M. and Büchs, J.
(2004) Online respiration activity measurement (OTR,
CTR, RQ) in shaken flasks. Biochemical Engineering Jour-
nal, 17, 187-194. doi:10.1016/S1369-703X(03)00181-5

[7] Peter, C.P., Lotter, S., Maier, U. and Büchs, J. (2004)
Impact of out-of-phase conditions on screening results in
shaking flask experiments. Biochemical Engineering Jour-
nal, 17, 205-215. doi:10.1016/S1369-703X(03)00179-7

[8] Losen, M., Frölich, B., Pohl, M. and Büchs, J. (2004)
Effect of oxygen limitation and medium composition on
Escherichia coli fermentation in shake-flask cultures.
Biotechnology Progress, 20, 1062-1068. doi:10.1021/bp034282t

[9] Gaden, E.L. (1962) Improved shaken flask performance.
Biotechnology and Bioengineering, 4, 99-103. doi:
10.1002/bit.260040112

[10] McDaniel, L.E., Bailey, E.G. and Zimmerli, A. (1965)
Effect of oxygen supply rates on growth of Escherichia
coli. Part I. Studies in unbaffled and baffled shake flasks.
Applied and Environmental Microbiology, 13, 109-114.

[11] Delgado, G., Topete, M. and Galindo, E. (1989) Interac-
tion of cultural conditions and end-product distribution in
Bacillus subtilis grown in shake flasks. Applied Microbio-
logy and Biotechnology, 31, 288-292. doi:10.1007/BF00258411

[12] Moore, J.H., Davis, C.C. and Coplan, M.A. (1991) Build-
ing scientific apparatus—A practical guide to design and
construction. Perseus Books, Reading, Massachusetts,
55-58.

[13] Storhas, W. (1994) Bioreaktoren und periphere Enrich-
tungen. Vieweg Verlag, Braunschweig/Wiesbaden, 165-166.
doi:10.1007/978-3-642-57973-8

[14] Krahe, M. (2007) Biochemical engineering. Ullmann’s
Biotechnology and Biochemical Engineering, 1st Edition,
Wiley-VCH, Weinheim, 2, 655.

[15] Adams, R.D., Comyn, J. and Wake, W.C. (1997) Struc-
tural adhesives joints in engineering. 2nd Edition, Cha-
pinn & Hall, London.

[16] Gleich, D.M., Van Tooren, M.J.L. and Beukers, A. (2002)
Structural bonded joint analysis: An overview. In: Mittal,
K.L. Ed., Adhesive Joints: Formation, Characteristics and
Testing, 2, VSP BV, Utrecht, 159-199.

[17] Pocius, A.V. (2002) Adhesion and adhesives technology—
An introduction. 2nd Edition, Hanser, München, 2-5.

[18] Bähr, C., Stammen, E., Thiele, R., Böhm, S., Dilger, K.
and Büchs, J. (2011) Withstanding frequent steam ster-
erilisation: Innovative technique to bond glass and stainless
steel composites in biotechnology and endoscopic medici-
ne, International Journal of Adhesion and Adhesives, paper
unpublished.

[19] Dien, B.S., Cotta, M.A. and Jeffries, T.W. (2003) Bacte-
ria engineered for fuel ethanol production: Current status.
Applied Microbiology and Biotechnology, 63, 258-266.
doi:10.1007/s00253-003-1444-y

[20] Mielenz, J.R. (2001) Ethanol production from biomass: Tech-
nology and commercialization status. Current Opinion
in Microbiology, 4, 324-329. doi:10.1016/S1369-5274(00)00211-3

[21] McMillan, J.D. (1997) Bioethanol production: Status and
prospects. Renewable Energy, 10, 295-302. doi:
10.1016/0960-1481(96)00081-X

[22] Wiegel, J. (1980) Formation of ethanol by bacteria. A
pledge for the use of extreme thermophilic anaerobic bacteria in industrial ethanol fermentation processes. *Cellular and Molecular Life Sciences*, 36, 1434-1446. doi:10.1007/BF01960144

[23] Han, K., Lim, H.C. and Hong, J. (1992) Acetic acid formation in Escherichia coli fermentation. *Biotechnology and Bioengineering*, 39, 663-671. doi:10.1002/bit.260390611

[24] Fukaya, M., Park, Y.S. and Toda, K. (1992) Improvement of acetic acid fermentation by molecular breeding and process development. *Journal of Applied Microbiology*, 73, 447-454. doi:10.1111/j.1365-2672.1992.tb05004.x

[25] De Ory, I., Romero, L.E. and Cantero, D. (1999) Maximum yield acetic acid fermenter. *Bioprocess and Biosystems Engineering*, 21, 187-190. doi:10.1007/s004490050661

[26] Park, Y.S., Ohtake, H. and Toda, K. (1990) A kinetic study of acetic acid production by liquid-surface cultures of Acetobacter aceti. *Applied Microbiology and Biotechnology*, 33, 259-263. doi:10.1007/BF00164518

[27] Devantier, R., Pedersen, S. and Olsson, L. (2005) Characterisation of very high gravity ethanol fermentation of corn mash. Effect of glycoamylase dosage, pre-saccharification and yeast strain. *Applied Microbiology and Biotechnology*, 68, 622-629. doi:10.1007/s00493-005-1902-9

[28] Fleury, K., Kalina, V. and Zell, J.J. (1997) Vinegar production. European Patent EP 0548552, 15 January 1997.

[29] Salek, A.T. (2002) Classic techniques for improvement of industrial yeast strains. Part I: Construction of ethan-ol-resistant and osmophilic industrial strains of Saccharomyces cerevisiae by electrofusion. *Biotechnology and Bioengineering*, 73, 95-103. doi:10.1002/bit.1041

[30] Anderlei, T. and Büchs, J. (2001) Device for sterile cell cultures. In: Smith, R. Ed., *Cell Technology for Cell Applications of an improved continuous parallel shaken bioreactor system for three microbial model systems. *Bioprocess and Biosystems Engineering*, 31, 193-205. doi:10.1007/s00449-005-0090-9

[31] Rechmann, H., Friedrich, A., Forouzan, D., Barth, S., Schnabl, H., Biselli, M. and Boehm, R. (2007) Characterization of photosynthetically active duckweed (Wolfia Australiana) in vitro culture by Respiration Activity Monitoring System (RAMOS). *Biotechnology Letters*, 29, 971-977. doi:10.1007/s10529-007-9330-9

[32] Jänicke, G., Sauter, C., Bux, R. and Haas, J. (2007) Characterisation of shake flasks for cultivation of animal cell cultures. In: Smith, R. Ed., *Cell Technology for Cell Products*, Springer, Dordrecht, 727-731.

[33] Peña, C., Peter, C.P., Büchs, J. and Galindo, E. (2007) Evolution of the specific power consumption and oxygen transfer rate in alginate-producing cultures of Azotobacter vinelandii conducted in shake flasks. *Biochemical Engineering Journal*, 36, 73-80. doi:10.1016/j.beij.2007.02.019

[34] Guez, J.S., Müller, C.H., Danze, P.M., Büchs, J. and Jacques, P. (2008) Respiration activity monitoring system (RAMOS), an efficient tool to study the influence of the oxygen transfer rate on the synthesis of lipopeptide by Bacillus subtilis ATCC6633. *Journal of Biotechnology*, 134, 121-126. doi:10.1016/j.jbiotec.2008.01.003

[35] Scheidle, M., Jeude, M., Dittrich, B., Denter, S., Kentsy, F., Suckow, M., Klee, D. and Bächs, J. (2010) High-throughput screening of Hansenula polymorpha clones in the batch compared with the controlled-release fed-batch mode on a small scale. *FEMS Yeast Research*, 10, 83-92. doi:10.1111/j.1567-1364.2009.00586.x

[36] Wilms, B., Hauck, A., Reuss, M., Syldatk, C., Mattes, R., Siemann, M. and Altenbuchner, J. (2001) High-cell-density fermentation for production of L-Ncarbamoylase using an expression system based on the Escherichia coli rhoBAD promoter. *Biotechnology and Bioengineering*, 73, 178-186. doi:10.1002/bit.21012

[37] Jeude, M. (2007) Entwicklung und anwendung einer fed-batch-betreiberweise mit nährstofffreisetzungssyste- men zur kontrollierten kultivierung und zum screening von mikroorganismen in schüttelkolben. Ph.D. Dissertation, RWTH Aachen University, Aachen.

[38] Gellissen, G. (2004) Production of recombinant proteins. *Wiley-VCH GmbH, Weinheim, 307-314. doi:10.1002/3527603670*

[39] Jeude, M., Dittrich, B., Niederschulte, H., Anderlei, T., Knocke, C., Klee, D. and Bächs, J. (2006) Fed-batch mode in shake flask by slow-release technique. *Biotechnology and Bioengineering*, 95, 433-436. doi:10.1002/bit.21012

[40] Stöckmann, C., Maier, U., Anderlei, T., Knocke, C., Gellissen, G. and Bächs, J. (2003) The oxygen transfer rate as key parameter of Hansenula polymorpha screening cultures. *Journal of Industrial Microbiology and Biotechnology*, 30, 613-622. doi:10.1007/s10295-003-0090-9

[41] Le Bourhis, E. (2008) Glass—Mechanics and technology. *Wiley-VCH, Weinheim, 208-212.*

[42] Frischat, G.H. (2002) Tin ions in float glass cause anomalia. *Comptes Rendus Chimie*, 5, 759-763. doi:10.1016/S1631-0748(02)01436-4

[43] Yates, B.W. and Duffy, A.M. (2008) Statistical analysis of the metrological properties of float glass. In: Khoun-sary, A.M., Morawe, C. and Goto, S. Eds., *Advances in X-Ray/EUV Optics and Components III*, Proceedings of SPIE, 7077, 23 September 2008.

[44] Hermann, R., Lehmann, M. and Büchs, J. (2003) Charaacterization of gas-liquid mass transfer phenomena in microtiter plates. *Biotechnology and Bioengineering*, 81, 178-186. doi:10.1002/bt.10456

[45] Akgün, A., Müller, C., Engmann, R. and Büchs, J. (2008) Application of an improved continuous parallel shaken bioreactor system for three microbial model systems. *Bioprocess and Biosystems Engineering*, 31, 193-205. doi:10.1007/s00449-007-0183-3

[46] Armstrong, K.B. (1997) Long-term durability in water of aluminum alloy adhesive joints bonded with epoxy adhesives. *International Journal of Adhesion and Adhesives*, 17, 89-105. doi:10.1016/S0143-7496(96)00038-3

[47] Akgün, A., Maier, B., Preis, D., Roth, B., Klingelhöfer, R. and Büchs, J. (2004) A novel parallel shaken bioreactor system for continuous operation. *Biotechnology Progress*, 20, 1718-1724. doi:10.1021/bp034289a