Tannery Wastewater Treatment by Coagulation-Flocculation Technique Using Combination of Calcium Polysulfide and Ferrous Sulphate

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Abstract: Effluents from the tannery industry have been a major source of environmental pollution. There is a need to evaluate the performance of wastewater treatment plant against regulatory standards. If in compliance found with standard, Employing appropriate treatment technique to meet the permissible discharge is important. In this reaction, performance evaluation of Tannery Wastewater and Treatment by coagulation technique of wastewater was investigated. Chemical oxygen demand (COD), Dissolved oxygen (DO), Total dissolved solids (TDS), Total suspended solids (TSS), chromium III and VI were the parameters selected to characterize the tannery waste water. From the characterization result of the factory effluent treatment plant it was found that; the factory effluent treatment plant meets the permissible discharge value in DO, Chromium III and VI. However, COD, TDS and TSS are far from the standards. Calcium polysulfide (CaSₓ) and ferrous sulphate (Fe(SO)₄) were the chemicals used for coagulation purpose. Treatment of 500ml original tannery waste with 400mg iron sulphate and variable calcium polysulfide concentrations (one, two and four v/v %) was conducted and characterized. From characterization result, 400mg iron sulphate and 20ml of calcium polysulfide treatment yields water that full fill the standard of discharge limit except for COD. In addition, at this treatment the best closer value of COD (1340mg/l) to the standard value (250mg/l) was found.

Keywords: Waste Parameter, Effluent Treatment, Sedimentation, Calcium Polysulfide, Coagulation

1. Introduction

The leather industry is one of the major economic sectors, which the developing countries has given due consideration for the development. For instance, Ethiopia was able to export above US$132million in the year 2017 from its leather and leather products industry [1]. Currently there are 30 tanneries, which are operational in this sector employing about 6000 workers. The current production capacity based on 15 tanneries is estimated at 6,000,000 to 8,000 000 kilograms of hides and 20, 000, 000 to 25,000,000 skins [2]. The hides are processed up to wet blues, crust and finished leather. The wet blues and crust hides are produced for export and the remaining low quality are finished for local market in the form of garments uppers and linings [3]. However, the industrial establishments for sustained economic development have been constrained ascribed to improper designed and operation in sustainable. In Ethiopia, the annual volume of liquid waste discharge from the 15 tanneries based on their annual production capacities is estimated to vary between 2,000,000 and 2,500,000 cubic meters [4]. Almost every tannery industry uses significant amounts of chemicals in the process of transforming animal hides into leather [5]. Usually the effluents from such tanning industries possess extremely high values (above the permissible standards of discharge) of Chemical Oxygen Demand (COD), Total Dissolved Solids (TDS), chromium ions, and Total Suspended Solids (TSS) [6]. Tannery waste water contains a complex mixture of both organic and inorganic pollutants, which brings serious environmental impact on water (with its
high oxygen demand, discoloration and toxic chemical constituents, terrestrial and atmospheric systems [7]. For example, Nitrate loads from wastewater treatment and oxidative treatments affect heavily marine eutrophication (0.69 g N eq/ kg crust leather) [8].

Most of tanneries do not have treatment facilities and environmental management systems, as a result simply discharging their wastes into the environment. Thus, they are causing serious environmental and public health problems in particular in urban centers. It is obvious that the effect will further extend to rural areas as well. Besides, the loss of economic benefits that derived from this sector, cannot survive a growing challenge of environmentally sound competitive business unless appropriate environmental management system is introduced [9]. Chemicals used for tanning processes are the main sources of negative impacts. The tanning industry gives rise to two types of hazard involving chemicals. These are, firstly, those concerning particular chemicals used in the various tanning processes, and secondly, chemical substances produced as byproducts by the chemical reactions occurring when a hide undergoes the tanning process [10].

Even though the government forced the tanning industries to treat their wastes and meet the standard requirement before discharging to the environment, very small numbers of Ethiopian tanneries have used treatment plant which full fill the discharge standard of the nation. Therefore, evaluating the tannery WWTP against standard of discharge and proposing treatment method, which is less costly and with no side effects on the environment is timely and important. In this paper, the wastewater from Debre Birhan Tannery was characterized and treated with coagulant chemicals for sedimentation of water pollutants.

2. Materials and Methods

2.1. Waste Water Characterization (WWTP Evaluation)

In order to evaluate the WWTP performance, influents and effluents wastewater samples were collected from WWTP of a local chrome-based tannery while it was working with its full capacity. Before getting to the treatment plant, the wastewater passes through some physical treatment/screening processes. The treatment plant uses alum and polyelectrolytes to remove pollutants using coagulation-floculation systems before discharging into the nearby river. The wastewater characterization was evaluated by Chemical Oxygen Demand (COD), Dissolved Oxygen (DO), Chromium ions, Total Dissolved Solids (TDS), Total Suspended Solids (TSS); because these are the common waste water pollution parameters [11, 12] and even difficult to minimize their values by preliminary treatment plants [13]. The two wastewater samples characterization was performed in Ethiopian Leather Industries Development Institute (ELIDI), Addis Ababa for these parameters and corresponding test methods (Table 1). Three replicates were conducted for each parameter and average value was taken as actual value.

| S. No | Type of test       | Test method       |
|-------|--------------------|-------------------|
| 1     | Chemical oxygen demand (COD) | APHA5220-COD B     |
| 2     | Dissolved oxygen (DO)      | APHA4500-OG       |
| 3     | Total dissolved solids (TDS) | SLC 13         |
| 4     | Total suspended solids (TSS) | APHA2540-D     |
| 5     | Chromium hexavalent (Cr⁶⁺) | SLC 22          |
| 6     | Chromium trivalent (Cr³⁺)  | SLC208           |

2.2. Waste Water Treatment with Calcium Polysulphide

Iron sulfate (FeSO₄) and calcium polysulphide (CaSn) combination effect reduces leachability and toxicity of hexavalent chromium (Cr(VI)) in contaminated soil [14]. These coagulant chemicals combined effect also have a possibility of simultaneous removal of pollutants in waste water [15]. Effluent sample from the tannery before inflowing to the WWTP was taken for chemical treatment. Chemicals and materials used as inputs while conducting this treatment were: Calcium poly sulfide solution (Ca(S)n) (20%, v/v), Iron (II) sulfate (FeSO₄) and calcium hydroxide (CaOH), sulfuric acid (H₂SO₄). All these analytical grades were procured from different chemical supply shops, Addis Ababa. Distilled water was used throughout the whole experiments. The treatment experiment was done at Debre Berhan University, Chemical Engineering Department Laboratory.

2.3. Methods

Waste water sample was poured in to three equal size measuring cylinders of 500ml for investigation of varying dose of calcium polysulphide [16]. The PH of these wastewater samples was adjusted to 12 PH using calcium hydroxide or sulfuric acid. Constant Iron sulfate dose of 800mg/L was added in to each of the three prepared samples followed by vagarous stirring for about 10 minutes [17]. Then calcium polysulphide dose of 1, 2 and 4% v/v of wastewater was added in to sample 1, sample 2 and sample 3 respectively. After 5 minutes stirring the samples were let to sediment for 12 hours [18]. The supernatants were taken for characterization of dissolved oxygen, chemical oxygen demand, chromium (III), chromium (VI), total suspended solids and total dissolved solids in Ethiopian Leather Industries Development Institute (ELIDI), Addis Ababa. All experiments were carried out at room temperature and were performed twice to ensure repeatability of the data. The settling rate of these three samples were also recorded.

3. Results and Discussions

3.1. Characterization of Factory Waste Before and After Treatment with the WWTP Treatment Plant (WWTP)

The tannery waste characterizations are summarized in Table 2. The value of several parameters is higher than standards set by environmental protection authority for discharge. The waste characterization result is useful in order
to analyze: (1) the waste load generated from the factory, (2) how much the current factory treatment plant treat its waste and (3) the effectiveness of the waste treatment (iron sulfate and calcium poly sulfide simultaneously) used in this research work. Characterization result of the local tannery wastewater is presented in Table 3. The factory treatment plant minimizes the waste load generated at least by 15% and at most by 99.9% before discharge to the surrounding. In chromium treatment, the plant is effective and it meets the standard of discharge in chromium trivalent and very closer for chromium hexavalent. However, the organic wastes are too far from the discharge allowance.

Table 2. Wastewater characterization before and after treatment at Debre Berhan Tannery.

| Parameter | Waste water before treatment by WWTP | Waste water after treatment by WWTP | Standard value [19] |
|-----------|-------------------------------------|------------------------------------|---------------------|
| DO (mg O₂/L) | 8.081 | 6.85 | 4.5 |
| COD (mg O₂/L) | 9670.6 | 4150 | 250 |
| Cr⁺⁶ (mg/L) | 0.384 | 0.106 | 0.1 |
| Cr⁺³ (mg/L) | 970.5 | ND | 2 |
| TSS (mg/L) | 14084 | 968 | 600 |
| TDS (mg/L) | 8000.3 | 4900 | 2100 |

The WWTP eliminates all the generated trivalent chromium and has negligible discharge. However, the organic wastes are still in huge quantity in the discharge. This is because the factory uses flocculants and treating agents like polyelectrolyte, alum and lime but not as such effective. The treatment plant does not full fill the permissible discharge in TSS, TDS and COD parameters. COD, TSS and TDS parameters have 368, 2800, and 3900mg/L differences respectively from the discharge standards.

3.2. Characterization of the Tannery Waste After Treating with Calcium Polysulfide (CPS) and Iron Sulphate

Characterization result of the above categories of wastes, which are generated waste from factory, waste from factory treatment plant and waste after treatment with iron sulfate and calcium poly sulfide are significantly different and it is reasonable. This is an indication of treatment capacity for each treatment method. Combination of calcium polysulfide and iron sulfate as a wastewater treatment minimizes the generated waste from the factory by more than 85% in all parameters of waste.

Treating the tannery waste with iron sulfate and calcium polysulfide shows appreciable minimization of the generated waste load from the factory. The treated waste meets the discharge standard for waste parameters discussed so far except COD.

Table 3. Characterization result of wastewater after treating with calcium poly sulphide at different concentration levels.

| Parameter | Calcium poly sulphide concentration |
|-----------|-------------------------------------|
|           | 1% (V/V) | 2% (V/V) | 4% (V/V) |
| DO (mg O₂/L) | 4.8 | 4.4 | 4.6 |
| COD (mg O₂/L) | 2490 | 1870.4 | 1340.7 |
| Cr⁺⁶ (mg/L) | 0.1 | 0.05 | 0.02 |
| Cr⁺³ (mg/L) | ND | ND | ND |
| TSS (mg/L) | 730 | 0.7 | 0.2 |
| TDS (mg/L) | 2200 | 93.3 | 86.2 |

This treatment technique involves in only a single tank, which means Removal of heavy metals, and settlement of organic wastes occurs simultaneous. This is due to the multipurpose of calcium polysulfide. Calcium polysulfide with higher concentration (4%V/V) gives the best discharge waste parameter. Therefore, this is the optimum dosing for the given waste load treatment. The only parameter that does not meet the discharge limit is COD. By this combined effect of iron sulphate and calcium polysulfide, 86.13% removal of COD is achieved, which is comparable to removal 95.95% by electrocoagulation [15] and 95.4% removal by combined process of biological, chemical coagulation and oxidation [20]. However, there is a significant minimization of load. The comparison of the original, standard, ETP and 1, 2, 4 V/V% CPS treatment is shown in the figure below.

![COD comparison with different treatments](image-url)
As it can be seen from the above figure, the treatment technique which yields the possible closer value to the standard is treatment of waste with four V/V % of calcium poly sulfide. An average settling rate data for sedimentation process is tabulated as below.

**Table 4. Height of clear liquid interface as the function of settling time.**

| Settling time (hr.) | 0   | 1   | 2   | 3   | 4   | 5   | 6   | 7   | 8   | 9   | 10  | 11  | 12  |
|---------------------|-----|-----|-----|-----|-----|-----|-----|-----|-----|-----|-----|-----|-----|
| Height of clear liquid interface (mm) | 500 | 350 | 250 | 220 | 200 | 190 | 184 | 180 | 178 | 177 | 176 | 175 | 175 |

The settling rate is very high for the first 2 hours of sedimentation. After that, there is low sedimentation for the chemical treatment process. Therefore increasing the settling time beyond 12 hours is time taking only.

**4. Conclusions**

In conclusion, it has been found that, local Tannery factory’s effluent treatment plant (ETP) is effective in trivalent chromium removal. The ETP also minimizes other wastes at least by 50% of the waste generated. When the generated waste of the factory was treated with 4% v/v of calcium polysulfide and 800mg/l of iron sulfate, at least 85% of the generated waste was removed. All the selected waste parameters except COD, meets the standards of discharge when this treatment method is applied. To achieve the COD level biological or secondary treatment required. The different pollutants present in the tannery waste can be separated using small amount of calcium polysulfide, iron sulfate and lime if necessary in a single tank the so-called sedimentor or clarifier. The treatment efficiency of wastewater can be affected by different factors like pH, temperature, concentration of iron sulfate or effect of any other flocculants. Therefore, the effect of several factors on tannery waste treatment can be studied in future.

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**Conflict of Interest**

The authors declare that there is no conflict of interest regarding the publication of this paper.

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