Synthesis and Evaluation of Ca-doped Sr$_2$Fe$_{1.5}$Mo$_{0.5}$O$_{6-\delta}$ as Symmetrical Electrodes for High Performance Solid Oxide Fuel Cells

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Abstract: A series of Ca-substituted Sr$_2$Fe$_{1.5}$Mo$_{0.5}$O$_{6-\delta}$ oxides, Sr$_2$xCa$_x$Fe$_{1.5}$Mo$_{0.5}$O$_{6-\delta}$ (SCFMO, x=0, 0.2, 0.4 and 0.6), were synthesized and evaluated as potential electrodes for symmetrical solid oxide fuel cells. X-ray diffraction examination showed that all samples maintained cubic perovskite structure in both air and wet hydrogen atmospheres. Temperature programmed reduction measurements indicated that the Ca$^{2+}$ substitution promoted the catalytic activity of SCFMO toward oxygen evolution reactions. Symmetrical anode fuel cell measurements showed the lowest polarization resistance in humidified hydrogen emerged at x=0.6. Single cells-SC$_{0.6}$FMO|La$_{0.8}$Sr$_{0.2}$Ga$_{0.8}$Mg$_{0.2}$O$_3$(LSGM)|SC$_{0.6}$FMO, fabricated via tape-casting and impregnation methods, produced peak power densities of 1.05 W·cm$^{-2}$ at 800 °C and 0.41 W·cm$^{-2}$ at 650 °C when operating on hydrogen fuels and air oxidants. These results demonstrate SC$_{0.6}$FMO is a potential electrode material for symmetrical solid oxide fuel cells.

Key words: Symmetrical Solid Oxide Fuel Cells; perovskite; electrode materials

Solid Oxide Fuel Cells (SOFCs) have attracted considerable attention as a promising power generation technology due to their high efficiencies and low emissions[1-3]. However, high manufacturing cost and poor long-term stability prevent their widespread implementation. SOFCs were typically composed of three ceramic components: a porous anode, a porous cathode and the dense electrolyte sandwiched between two electrodes to separate fuels from air[4]. Different materials were usually adopted for anode and cathode due to their different requirements, resulting in at least two separate thermal processing steps for fabrication of single cells. Recently, some materials appeared suitable as both electrodes in the symmetrical SOFCs (SSOFCs)[5]. Compared with the traditional SOFCs, SSOFCs showed advantages of simplified production process, reduced manufacturing cost as well as improved thermo-mechanical compatibility with only one type of interface present[6]. Nonetheless, the very different operating conditions of anodes and cathodes posed harsh requirements on the symmetrical electrodes. For example, the symmetrical electrode materials should show adequate chemical stability and acceptable electronic conductivities in both the oxidizing and reducing atmospheres with high catalytic activities towards both oxygen reduction and fuel oxidation reactions[7-8].

Until now, only a few number of oxides could fulfil almost all requirements for symmetrical electrodes. In particular, LaCrO$_3$ based perovskite exhibited good stability and conductivities over a wide range of oxygen partial pressures. Partial substitution of Ca or Sr in the A-site, and Mn or Fe in the B-site yielded promising symmetrical electrodes such as La$_{0.7}$Ca$_{0.3}$Cr$_{0.9}$O$_{3-\delta}$[9], La$_{0.7}$Sr$_{0.2}$Co$_{0.5}$O$_{3-\delta}$[10], and La$_{0.7}$Sr$_{0.2}$Fe$_{0.7}$Co$_{0.3}$O$_{3-\delta}$[11] with good catalytic activities for both electrode reactions. Maximum power densities of 300 mW·cm$^{-2}$ were achieved in humidified hydrogen for the symmetrical La$_{0.7}$Sr$_{0.2}$Co$_{0.5}$O$_{3-\delta}$ fuel cell at 900 °C[10]. La(Sr)TiO$_3$-based oxide were usually used as anodes due to their high conductivities in hydrogen and excellent catalytic activities for hydrogen oxidation reactions. Doping Fe or Co in the B-site substantially improved their conductivities under oxidizing atmospheres. La$_{0.7}$Sr$_{0.2}$Ti$_{0.5}$Fe$_{0.5}$O$_{3-\delta}$[12] and La$_{0.7}$Sr$_{0.2}$Ti$_{0.5}$Co$_{0.5}$O$_{3-\delta}$ (LSTC)[13] were explored as symmetrical electrodes with maximum power densities of 110 mW·cm$^{-2}$ obtained at 800 °C for symmetrical cells-LSTC|LSGM|LSTC[13]. Alternatively, introducing the chemically stable metal element Mo in the B-site of commonly used SOFC cathodes could also enhance their structural stability under highly reducing anode atmospheres, e.g., SrFe$_{0.75}$Mo$_{0.25}$O$_{3-\delta}$ (SFMO)[14]. Power densities as high as 0.83 W·cm$^{-2}$ were achieved at 900 °C for symmetrical SFMO electrode fuel cells in...
were synthesized via Sol-Gel method\cite{20}. Stoichiometric amounts of Sr(NO$_3$)$_2$, Ca(NO$_3$)$_2$, Fe(NO$_3$)$_3$·9H$_2$O and (NH$_4$)$_6$Mo$_7$O$_24$·4H$_2$O were dissolved in deionized water to form gel. The gel was then dried at 250\degree C for 2 h to obtain the final SCFMO powders. The precursor solutions were evaporated at 80\degree C to form gel. The gel was then dried at 250\degree C for 10 h to obtain dry precursor followed by calcination at 1100\degree C in air for 5 h to obtain the final SCFMO powders. Crystal structure of the as-synthesized and hydrogen-reduced powders were examined by X-ray diffractometer (XRD, Rigaku Smartlab9, Japan) at room temperature. Temperature-programmed reduction (TPR, Micromeritics ChemiSorb 2720) measurements were carried out to analyze the catalytic activity of SCFMO anodes. 60–80 mg SCFMO powders were loaded into the quartz U-tube. After being pre-treated with high-purity He flow at 450\degree C for 30 min, the samples were measured under 5vol% H$_2$/He (20 mL·min$^{-1}$) flow with a linear heating rate of 10\degree C·min$^{-1}$ from room temperature up to 850\degree C.

Symmetrical fuel cells were fabricated with thin LSGM electrolytes and SCFMO catalysts, based upon the “porous/dense/porous” LSGM tri-layer backbones. Powders of LSGM (Praxair) and rice starch used as the fugitive material for the porous layers were ball-milled in a weight ratio of 60:40 for 12 h with appropriate amounts of dispersant, binder, plasticizer and solvent. The tri-layer structures were produced by laminating three tape-cast ceramic green tapes with subsequent co-firing at 1400\degree C to produce the final ceramic structures. The electrode catalysts SCFMO were added by liquid infiltration method. The precursor solutions were simultaneously impregnated into both porous LSGM backbones, and then calcined at 700\degree C for 30 min. The impregnation-calcination procedure was repeated until catalyst loading achieved 25wt% relative to the porous LSGM backbones, with a final calcination at 850\degree C for 2 h to obtain the symmetrical cells. The cross-sectional morphologies of single cells were examined using the scanning electron microscopy (SEM, FEI Inspect F50, USA).

For electrochemical measurement at 650–800\degree C, the symmetrical cells were sealed to alumina tubes using ceramic adhesive (Aremco, Ultra-Temp 552). Current-voltage curves (I-V) and electrochemical impedance spectra (EIS) were obtained by using Electrochemical Workstation (ZAHNER IM6e, Germany) with the cathode exposed to dry air (100 mL·min$^{-1}$) and the anode to humidified (3vol% H$_2$O) hydrogen (100 mL·min$^{-1}$). To determine the individual electrode polarization resistances, impedance measurements were also performed on symmetrical cells in homogeneous environments, i.e., in dry air for symmetrical cathode cells and in humidified (3vol% H$_2$O) hydrogen for symmetrical anode cells. The impedance data were recorded at open circuits over the frequency range from 0.1 Hz to 100 kHz with a 20 mV AC perturbation.

2 Results and discussion

Fig. 1(a) summarized the room temperature XRD patterns of as-synthesized SCFMO powders, showing cubic perovskite crystal structure for all powders as previously reported\cite{19}. In order to examine their structural stability as the SOFC anode, these powders were thermally treated in 97vol% H$_2$–3vol% H$_2$O at 800\degree C for 4 h, with XRD patterns of the reduced powders summarized in Fig. 1(b). Notably, the cubic perovskite structures for all samples were well maintained with little impurities detected, indicating that SCFMO oxides could be adopted as the symmetrical electrodes in SOFCs. The magnified XRD patterns at 67.5° in Fig. 1(c) showed that the peak shifted toward higher angle with Ca$^{2+}$ substitution increasing, due to smaller ionic radius of Ca$^{2+}$ compared with Sr$^{2+}$. Fig. 1(c) also showed increased lattice parameter after reduction in hydrogen due to the reduction of Fe and Mo elements as previously reported for the SFMO-based oxides\cite{21}.
Temperature programmed reduction measurements were used to evaluate the stability and catalytic activities of the SCFMO anode materials. Fig. 2 showed the TPR profiles of all SCFMO samples, showing only one peak for the pure SFMO and two peaks for the $\text{Ca}^{2+}$-substituted samples. Similar profiles were observed by Xiao, et al[22] and Wang, et al[23] in the TPR curves of SFMO materials, related to reduction of $\text{Fe}^{3+}$ and $\text{Mo}^{6+}$. Kubo, et al[24] assigned the ~550 °C peak to the reduction of $\text{AMoVI}_{4}$O to $\text{AMoIVO}_{3}$. Thus it was reasonable to attribute the peaks at ~490 and ~550 °C in TPR curves to reductions of $\text{Fe}^{3+}$ and $\text{Mo}^{6+}$, respectively. TPR curves shifted towards lower temperature with increasing $\text{Ca}^{2+}$ substitution, indicative of enhanced OER catalytic activity[23]. Furthermore, no reduction peak reflecting the formation of metal Fe was observed in the TPR profiles, confirming the structural stability of all the SCFMO oxides in hydrogen as consistent with the XRD results.

Fig. 3(a) showed SEM micrograph of the thin LSGM electrolyte fuel cell with symmetrical SCFMO electrodes. The LSGM electrolyte layer was fully dense with ~35 μm thickness. Higher-magnification micrograph (Fig. 3(b)) of the impregnated composite electrode showed a homogeneous distribution of 70 nm SCFMO catalysts on the internal surfaces of the porous LSGM backbones. Fig. 3(b) also showed well-connected catalysts and sufficient porosities that were conducive to current collection and gas transport.

The catalytic activities of SCFMO nano particles toward hydrogen oxidation at the anode and oxygen reduction at the cathode were evaluated by electrochemical impedance spectroscopy (EIS). Fig. 4(a) showed Nyquist plots of impedance data measured on the symmetrical anode cells at 800 °C in the homogeneous environment of 97vol% $\text{H}_2$–3vol% $\text{H}_2\text{O}$, where the ohmic resistances were omitted for easy comparison among different samples. The anode polarization resistances ($R_p$,A) were 0.23, 0.21, 0.20 and 0.18 $\Omega\cdot\text{cm}^2$ for SCFMO at $x = 0, 0.2, 0.4$ and 0.6, respectively. Fig. 4(b) showed the temperature dependence of the $R_p$,A value on the substitution amounts of $\text{Ca}^{2+}$. $R_p$,A decreased with the $\text{Ca}^{2+}$ substitution increasing over the whole temperature range from 650 to 800 °C with the minimized $R_p$,A values observed at
$x=0.6$. Moreover, the slope of Arrhenius plots in Fig. 4(b) also decreased with increasing Ca$^{2+}$ substitution. The activation energy decreased from 0.93 to 0.77 eV, which were slightly smaller than 1.07 eV in previous report$^{[25]}$. These results indicated that Ca$^{2+}$ substitution could effectively enhance the anode catalytic activities with reduced anode polarization resistances, especially at lower temperatures.

Fig. 5(a) showed Nyquist plots of impedance data measured on the symmetrical cathode cells at 800 °C in homogeneous air environment. The cathode polarization resistances ($R_{p,c}$) were 0.104, 0.056, 0.058 and 0.077 Ω·cm$^2$ at $x=0$, 0.2, 0.4 and 0.6, respectively. Fig. 5(b) showed the temperature dependence of the $R_{p,c}$ value on the substitution amounts of Ca$^{2+}$ at 650–800 °C. Minimized $R_{p,c}$ values emerged at $x=0.2$ with all temperatures, similar to the observation in previous report$^{[19]}$. However, the slope of the curve in Arrhenius plots was close to each other for all SCFMO cathodes, indicating that Ca$^{2+}$ substitution might not alter the cathode reaction mechanism. And the increase in conductivity may be the reason for improvement of cathode performance$^{[19]}$. However, compared with the resistance of cathode, higher anode impedance of the SCFMO electrode showed more significant impact on the cell performance, especially at lower temperatures. Although the cathode impedances of the electrode were low at $x=0.2$, the minimum value of the total polarization impedance of the cells was achieved at $x=0.6$.

Fuel cell performances were measured in humidified hydrogen fuels and dry air oxidants both at a flow rate of 100 mL·min$^{-1}$. Fig. 6(a) showed the polarization curves of the cell voltages ($V$) and power densities ($P$) as a function of current densities ($J$) measured over 650–800 °C for the symmetrical SCFMO electrodes with $x=0.6$. The open circuit voltage (OCV) values increased from 1.103 V at 800 °C to 1.127 V at 650 °C, which were close to the theoretical values (1.12–1.15 V) calculated from Nernst equation over the very temperature range. The maximum power densities were 1.05, 0.88, 0.66 and 0.41 W·cm$^{-2}$ at 800, 750, 700 and 650 °C, respectively. Fig. 6(b) showed Nyquist plots of impedance data obtained at open circuit, and the combined anode and cathode interfacial polarization resistances were 0.155, 0.179, 0.230 and 0.359 Ω·cm$^2$ at 800, 750, 700 and 650 °C, respectively. The polarization impedance and the ohmic impedance increased gradually with the operating temperature decreasing in Nyquist plots, indicating decrease in the catalytic activity of the electrodes and the electrical conductivity of the electrolyte.
3 Conclusion

In summary, we synthesized and evaluated a series of Sr$_{2}$Ca$_x$Fe$_{1.5}$Mo$_{0.5}$O$_{6-\delta}$ oxides as potential electrode catalysts for symmetrical fuel cells. These oxides maintained cubic perovskite crystal structure under both oxidizing and reducing conditions. H$_2$-TPR measurements indicated that substituting Ca$^{2+}$ for Sr$^{2+}$ reduced the onset temperature of hydrogen oxidation reactions. Impedance analysis showed that Sr$_{1.4}$Ca$_{0.6}$Fe$_{1.5}$Mo$_{0.5}$O$_{6-\delta}$ exhibited the lowest anode polarization resistances among all samples with slightly higher cathode polarization resistances than those of Sr$_{1.6}$Ca$_{0.4}$Fe$_{1.5}$Mo$_{0.5}$O$_{6-\delta}$. Fuel cell measurements also showed the highest power densities for symmetrical Sr$_{1.4}$Ca$_{0.6}$Fe$_{1.5}$Mo$_{0.5}$O$_{6-\delta}$ electrodes, e.g., 1.05, 0.88, 0.66 and 0.41 W·cm$^{-2}$ at 800, 750, 700 and 650 °C, respectively. These results indicate that Ca$^{2+}$ substitution is effective in enhancing the catalytic activity of SFMO oxides toward hydrogen oxidation and oxygen reduction reactions, and Sr$_{1.4}$Ca$_{0.6}$Fe$_{1.5}$Mo$_{0.5}$O$_{6-\delta}$ is a promising symmetrical electrode material.

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Ca掺杂Sr_{2}Fe_{1.5}Mo_{0.5}O_{6-δ}材料的合成与作为对称固体氧化物燃料电池电极催化剂的性能研究

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摘 要: 对称固体氧化物燃料电池由于生产过程简单、成本低，受到了研究者的广泛关注。然而较低的电极催化性能制约了其进一步的发展。本研究利用溶胶-凝胶法合成了一系列钙取代Sr_{2}Fe_{1.5}Mo_{0.5}O_{6}的钙钛矿材料(Sr_{2-x}Ca_{x}Fe_{1.5}Mo_{0.5}O_{6-δ}, x=0, 0.2, 0.4, 0.6), 并研究了其作为对称固体氧化物燃料电池电极催化剂的性能。X射线衍射(XRD)测试表明所有样品在空气与氢气气氛中均能保持立方钙钛矿结构。而在程序升温还原(TEMP)过程中, Ca^{2+}的掺入能有效降低还原温度，提升其对析氧反应的催化活性。对称阳极电池在氢气气氛中的测试表明, 当Ca^{2+}的掺入量为0.6时电池极化阻抗最小。利用流延骨架与湿化学浸渍法制备了单电池SC_{0.6}FMO|La_{0.9}Sr_{0.1}Ga_{0.8}Mg_{0.2}O_{3}(LSGM)|SC_{0.6}FMO。以氢气作为燃料时, 单电池在800与650℃的最大功率密度分别为1.05与0.41 W∙cm^{-2}。以上结果表明Sr_{2-x}Ca_{x}Fe_{1.5}Mo_{0.5}O_{6-δ}可以作为高效对称燃料电池的电极催化剂。

关 键 词: 对称固体氧化物燃料电池; 钙钛矿结构; 电极材料

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