Leaching of Polymetallic Cu-Zn-Pb Concentrate with Sodium Nitrate in Sulphuric Acid

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The results of polymetallic sulphide Cu-Zn-Pb concentrate leaching with sulphuric acid in the presence of sodium nitrate as an oxidizing agent, at atmospheric pressure, are presented and discussed. Chemical composition and phase ratio of the starting concentrate and solid residuals after the leaching process are shown. Chemical reactions of leaching and their thermodynamic probabilities are predicted based on the calculated Gibbs energies and analysis of E-pH diagrams. The influence of temperature and time on the leaching degree of the concentrate’s components is experimentally determined. It is shown that it is possible to obtain copper, zinc and iron in a solute form, while lead in the anglesite (PbSO₄) form remains in the solid residual after the leaching process. The iron is being oxidized to Fe(III)-sulphate, which takes part in a sulphide leached minerals and turns into Fe(II)-sulphate.

Key words: polymetallic Cu-Zn-Pb concentrate, leaching, sodium nitrate, sulphuric acid

1. INTRODUCTION

Non-ferrous metals and iron usually appear in a form of sulphide complex ores. Large deposits of complex ores often contain chalcopyrite, sphalerite, galena and pyrite, which are fine-grained structures complexly fused with tailings minerals in complex mineral forms [1]. Sometimes, when it is difficult to prepare flotation concentrates of the individual minerals, then it is easier to prepare bulk concentrates [2]. Although treatments by pyrometallurgical process are not attractive, because a large amounts of SO₂ is produced, approximatelly 80-85% of world’s total copper is produced pyrometallurgically, and 80% of world’s total zinc is produced by roasting-leaching-electrowinning process, and 20% is produced by Imperial Smelting Process [3-4].

Hydrometallurgical processes offer a great potential for treating complex sulphide ores, and it results in increased metal recoveries and reduced air pollution hazards. Recently, an increased interest is remarked related to the possible application of various reagents in a hydrometallurgical processing of sulphide concentrates. Ferric [5-11] and cupric [12, 13] ions, bacteria [14-17], and other oxidants [3, 4, 18-26] were used as oxidative leaching agents of complex sulphides in su-
Table 1. Hydrometallurgical processes for treatment of copper ores and concentrates

| Process                          | Temperature (°C) | Pressure (atm) | Regrind D80 (µm) | Special conditions                                                                 |
|----------------------------------|------------------|----------------|------------------|-------------------------------------------------------------------------------------|
| Activox (McDonald at al., 2007; Corrans at al., 1993; Strehlovä at al., 2003) | 100-110          | =12 P(O3) =10   | 5-15                          | Fine grinding combined with high oxygen overpressure overcomes chalcopyrite passivation |
| Albion (Hourn at al., 1999)      | 85               | 1              | 5-10              | Atmospheric ferric leaching of very finely ground concentrate                         |
| Anglo-American – University of British Columbia (McDonald at al., 2007; Dreisinger, 2003; Dreisinger at al., 2002) | 150              | 10-12           | 10-15                         | Modest regrind combined with surfactants for chalcopyrite leaching                   |
| Bactech / Mintek low temperature bioleach (Miller at al., 2006) | 35               | 1              | 5-10                          | Low T bioleach (35-50°C) requires very fine grind to overcome chalcopyrite passivation |
| BIOCOP® (Dew at al., 2003)       | 65-80            | 1              | 37                            | High T bioleach (65-80°C) uses thermophilic bacteria                                |
| Cymet (Kruesi at al., 1973)      | 80-100           | 1              | /                             | Electrochemical dissolution in the presence of ferric chloride, which finally produces copper powder |
| Cyprus (Anon, 1977))            | 80-100           | 1              | /                             | Chalcopyrite concentrate leach in two-stages using a mixed solution of ferric chloride and copper chloride |
| CELS copper (McDonald at al., 2007; Jones, 1996) | 140-150         | 10-12           | 37                            | Chloride catalyzed leach of chalcopyrite producing basic copper sulphate precipitate in the autoclave |
| Dynatec (Kofluk at al., 1998; Stiksma at al., 2000) | 150              | 10-12           | 37                            | Chalcopyrite and sphalerite is leached using low grade coal as an additive            |
| Minimet (Demarthe at al., 1976)  | 90-100           | 1              | /                             | Atmospheric cupric chloride leaching of complex concentrate. To keep CuCl, PbCl2 and AgCl in solution, NaCl was added to the leaching agent. |
| Mount Gordon (Richmond at al., 2002; Dreisinger at al., 2002) | 90               | 8              | 100                           | Pressure oxidation of chalcopyrite/pyrite ore or bulk concentrate in an iron-sulfate rich electrolyte |
| NITROX (Van Weert at al., 1986)  | 80-100           | 1              | /                             | Atmospheric leach refractory gold ores and concentrates by hot nitric acid           |
| NSC (Sunshine Mine) (McDonald at al., 2007; Ackerman, 1990; Anderson, 2003; Anderson at al., 1992, 1996) | 130-150          | 7 P(O3) = 4    | 10                            | Nitrite catalyzed leach of chalcopyrite by sulphuric acid leaching agent containing cupri and feri chloride with oxygen pressure |
| PLATSOL (Fleming at al., 2001)   | 220-230          | 30-40           | 15                            | Total pressure oxidation in the presence of 10-20 g/dm³ NaCl. Precious metals leached at the same time as base metals |
| Sepon copper (Baxter at al., 1978) | 80-Copper 220-230-Pyre | Atm 30-40      | 100                           | Atmospheric ferric leach for copper from chalcocite. Pressure oxidation of pyrite concentrate to make acid and ferric sulphate for copper leach |
| Sherritt-Cominco (Swinkels at al., 1978) | 150              | =25 P(O3) =10   | /                             | A two-stage process starting with the removal of sulphur and iron from low grade Cu concentrate. Than a high-grade Cu concentrate leach by sulphuric acid under oxygen pressure |
| Sherritt-Gordon (Bolton at al., 1979) | 150              | P(O3)=3.5    | 44                            | Oxygen pressure oxidation complex concentrate. Copper and zinc go into solution, lead is transformed into PbSO4 and lead jarosite is retained in the residue |
| Total pressure oxidation (McDonald at al., 2007; King at al., 1995; Marsden at al., 2003) | 200-230          | 30-40           | 37                            | Extreme conditions of T and P designed to rapidly destroy refractory gold ores and concentrates in the presence of NaCl in the leaching agent |

Some of the hydrometallurgical processes developed for copper ores and concentrates treatment can also be considered for a treatment of complex sulphides. The previous and current developments are discussed in references [5, 14, 15, 18, 23, 24, 27-44]. The main processes and parameters are presented in Table 1.
Much attention has been given to the development of nitric acid based processes for sulphide ores and concentrates, e.g. Habashi discuss that metal sulphide oxidation by nitric acid can be achieved in two ways [45]. In the first case, NO$_3^-$ ion is oxidant, and during the reaction it is reduced to NO or NO$_2$. In the second case, oxygen which arises from nitric acid decomposition is the oxidant.

Van Weert et al. [46] developed the NITROX process, which utilizes nitric acid to recover gold from refractory pyrite and arsenopyrite ores. They found that sulphide sulphur formed mainly elemental sulphur, while a smaller part formed sulphate. The NO gas that is produced is directly oxidized by the air into the NO$_2$, which dissolves in the solution and reacts with water to form HNO$_3$, thereby completing the NITROX cycle. The most significant problem was high sulphate production. Droppert and Shang [47] showed that sulphate formation could be minimized by addition of a small excess of HNO$_3$, followed by slow addition of HNO$_3$ keeping the acid concentration at a constant low level.

Some industrial operations use the nitric or nitrous acid added in a small concentration to the sulphuric acid, e.g. in oxygen extended pressure leach processes. At Sunshine Precious Metals, silver and copper are recovered from a complex sulphide concentrate at temperatures between 145$^\circ$ and 155$^\circ$ C and at total pressure of 709kPa [24, 39, 48]. In that case, nitrous acid were found to enhance the solubilization of minerals at lower temperatures and pressures, and the nitrous/sulphuric acid leach process is used with success.

Following successful operation in the Sunshine Pressure Leach plant, the catalysis under the extended pressure oxidation, using nitrogen species, is promoted as a nitrogen species catalysed (NSC) technology [23, 48]. It was demonstrated that the addition of nitrite ion in a small amounts catalyses the oxidation of sulphides in the presence of oxygen; recent data show that it is a fast reaction, typically less than 30 min, for slurry containing 100 g/L of solids [23]. The leaching process of metal sulphides by nitric acid as oxidant is more efficient in presence of NO$^+$ ions. The addition of NO$^2$- ions instead of NO$_3^-$ ions accelerates the formation of NO$^+$ ions, which further oxidises sulphide minerals at lower temperatures to the elemental sulfur [40, 48].

Oxidative dissolution of a sulphide concentrate using nitrate as the leaching agent in an acid medium take place with formation of elemental sulphur, and it can be represented by one of the following chemical reactions [20, 21, 49]:

\[ 3\text{MeS} + 2\text{NO}_3^- + 8\text{H}^+ = \]
\[ = 3\text{Me}^{2+} + 3\text{S}^0 + 2\text{NO} + 4\text{H}_2\text{O} \quad (1) \]

or

\[ \text{MeS} + 2\text{NO}_3^- + 4\text{H}^+ = \]
\[ = \text{Me}^{2+} + \text{S}^0 + 2\text{NO}_2 + 2\text{H}_2\text{O} \]

Initially the rate of reaction is controlled by a surface chemical reaction and later on changes into a diffusion controlled.

General flow sheet for the treatment for the complex Cu-Zn-Pb concentrates is presented in Fig 1.

The objective of this work is performance of the leaching process using the selected complex Cu-Zn-Pb sulphide concentrates, from "Rudnik" flotation plant, by sulphuric acid solution in the presence of sodium nitrate.

![Figure 1 - General flow sheet for the treatment of the complex Cu-Zn-Pb concentrates](image-url)

2. CHEMICAL REACTIONS AND THERMODYNAMICS

Based on the literature data and on the characterization of both produced solution and leaching solid residues, obtained by leaching of polymetallic concentrate containing chalcopyrite, sphalerite, galena and pyrrhotite in oxidized acidic medium, following chemical reactions were chosen in this study and then analyzed in the H$_2$SO$_4$-NaNO$_3$-H$_2$O system.

Chalcopyrite (CuFeS$_2$) leaching system


\[ CuFeS_2 + 4/3NaNO_3 + 8/3H_2SO_4 = \]
\[ = CuSO_4 + FeSO_4 + 2/3Na_2SO_4 + 2S^0 + \]
\[ + 4/3NO + 8/3H_2O \]  

(3)

\[ CuFeS_2 + 4NaNO_3 + 4H_2SO_4 = \]
\[ = CuSO_4 + FeSO_4 + 2Na_2SO_4 + 2S^0 + 4NO_2 + 4H_2O \]  

(4)

\[ CuFeS_2 + 5/3NaNO_3 + 10/3H_2SO_4 = \]
\[ = 0CuSO_4 + 1/2Fe_2(SO_4)_3 + 5/6Na_2SO_4 + \]
\[ + 2S^0 + 5/3NO + 10/3H_2O \]  

(5)

\[ CuFeS_2 + 5NaNO_3 + 5H_2SO_4 = \]
\[ = CuSO_4 + 1/2Fe_2(SO_4)_3 + 5/2Na_2SO_4 + \]
\[ + 2S^0 + 5NO_2 + 5H_2O \]  

(6)

Sphalerite (ZnS) leaching system

\[ ZnS + 2/3NaNO_3 + 4/3H_2SO_4 = \]
\[ = ZnSO_4 + 1/3Na_2SO_4 + S + 2/3NO + 4/3H_2O \]  

(7)

\[ ZnS + 2NaNO_3 + 2H_2SO_4 = \]
\[ = ZnSO_4 + Na_2SO_4 + S + 2NO_2 + 2H_2O \]  

(8)

Galenite (PbS) leaching system

\[ PbS + 2/3NaNO_3 + 4/3H_2SO_4 = \]
\[ = PbSO_4 + 1/3Na_2SO_4 + S + 2/3NO + 4/3H_2O \]  

(9)

\[ PbS + 2NaNO_3 + 2H_2SO_4 = \]
\[ = PbSO_4 + Na_2SO_4 + S + 2NO_2 + 2H_2O \]  

(10)

Pirrhotite (FeS, S) leaching system

\[ (1/3x-1)FeS + 4/3H_2SO_4 + 2/3NaNO_3 = \]
\[ = FeSO_4 + 1/3Na_2SO_4 + (x/3-1)S + 2/3NO + 4/3H_2O \]  

(11)

\[ (1/3x-1)FeS + 2H_2SO_4 + 2NaNO_3 = \]
\[ = FeSO_4 + Na_2SO_4 + (x/3-1)S + 2NO_2 + 2H_2O \]  

(12)

\[ (1/3x-1)FeS + 2H_2SO_4 + NaNO_3 = 1/2Fe_2(SO_4)_3 + \]
\[ + 1/2Na_2SO_4 + (x/3-1)S + NO + 2H_2O \]  

(13)

\[ (1/3x-1)FeS + 3H_2SO_4 + 3NaNO_3 = 1/2Fe_2(SO_4)_3 + \]
\[ + 3/2Na_2SO_4 + (x/3-1)S + 3NO_3 + 3H_2O \]  

(14)

Thermodynamic analysis included calculation of standard Gibbs energy change and E-pH diagrams. In order to clarify the occurrence probability of quoted reactions (3)-(14), Gibbs energy change was calculated within a temperature range of 25 up to 90 °C and the obtained values are given in Table 2.

**Table 2. The calculated values of standard Gibbs energy change at temperatures 298 and 363 K (HSC) of the analysed reactions in the poly metallic concentrate-H_2SO_4-Na_2SO_4 system**

| Eq. no. | \( \Delta G_{298 \circ C} \) (kJ/mol) | \( \Delta G_{363 \circ C} \) (kJ/mol) | Eq. no. | \( \Delta G_{298 \circ C} \) (kJ/mol) | \( \Delta G_{363 \circ C} \) (kJ/mol) |
|---------|----------------------------------|----------------------------------|---------|----------------------------------|----------------------------------|
| (3)     | -330.978                         | -341.369                         | (9)     | -236.464                         | -241.964                         |
| (4)     | -352.302                         | -391.600                         | (10)    | -247.126                         | -267.079                         |
| (5)     | -396.085                         | -408.423                         | (11)    | -235.312                         | -240.721                         |
| (6)     | -422.741                         | -471.211                         | (12)    | -245.974                         | -265.836                         |
| (7)     | -191.784                         | -196.993                         | (13)    | -300.420                         | -307.775                         |
| (8)     | -202.446                         | -222.108                         | (14)    | -316.413                         | -345.448                         |

HSC Chemistry software and its data base of thermodynamic values of reaction participants were used in calculations.

The negative values of Gibbs energy change \( \Delta G_T \) for reactions (3)-(14) show that they are all thermodynamically feasible at standard pressure and temperature range of 30-100°C. Higher negative \( \Delta G_T \) value of the reaction (4) than that of the reaction (3) suggests its occurrence with higher thermodynamic probability. NO and NO₂ ratio in gaseous products and elemental sulphur and sulphate ratio after leaching depend on concentration of nitrate ion (Droppert et al. 1995). E-pH diagrams show the thermodynamic stability of water solution components and the correlations electrochemical potential - pH values. E-pH diagrams for the behavior of copper, zinc, lead and iron in Cu-Zn-Pb-Fe-S-H₂O system are presented in Fig. 2.

**Figure 2 - E-pH diagrams for Cu-Zn-Pb-Fe-S-H₂O system at 80°C**

From Fig. 2 it can be concluded that copper, zinc, lead and iron leach from their minerals at low pH values and under the given oxidizing conditions. Under these oxidizing conditions at high electrode potential and low pH values, Cu²⁺, Zn²⁺, Fe³⁺ and Fe²⁺ ions exist in water solutions, while Pb²⁺ exists in sulphate form in the resι-de. The increase of temperature lowers the possibility of Fe³⁺ ion existance in the system.

3. EXPERIMENTAL

The concentrate enriched during the flotation of a CuFeS₂-PbS-ZnS poly metallic ore in the “Rudnik” flotation plant (Rudnik – Serbia) was used. All leaching experiments of poly metallic concentrate at atmospheric pressure and temperatures up-to 90°C were carried out using experimental set-up, which provides the stable hermetic conditions and allow the heating at constant temperature.

The liquid volume was kept co-nstant during the experiments. The calculated volumes of H₂SO₄ and
NaNO$_3$ solutions were put into the glass reactor and heated-up to the selected temperature. When the tem-
perature was reached, the solid conce-ntrate was added and that moment is taken for the begi-
nning of rea-
tion.

After finite time intervals, during the leaching process, the solution samples were taken for chemical
analysis which was carried out with AAS (Perkin El-
mer).

The solid residues were carefully fil-tered out, washed with distilled water, dried and their phase con-
tent was determined by AAS, X-ray analysis using diffractometer (Siemens D500), light micro-scropy
(Carl Zeiss-Jena JENAPOL-U) and thermal DTA / TG analysis on a NETZSH 409 Ep.

4. RESULTS AND DISCUSSION

4.1. Characterization of Polymetallic Concentrate

Chemical composition of the polymetallic concen-
trate, which was used in the leaching process, is pres-
ented in Table 3.

| Element | Cu | Zn | Pb | Fe | S  | Bi |
|---------|----|----|----|----|----|----|
|         | 8.92% | 8.79% | 12.66% | 19.07% | 21.02% | 0.083% |
| Sb      | 0.012% | 0.065% | 0.034% | 0.021% | 0.0006% |

X-ray diffraction (XRD) analysis was used for the
phase fraction determination in the polymetallic con-
centrate; the result is shown in Figure 3.

Figure 3 - X-ray diffraction (XRD) analysis of the polymetallic concentrate from “Rudnik” flotation plant [20]

The presence of chalcopyrite, sphalerite, galena,
pyrrhotite and qu-artz is registered. Prepared sample
microphotograph of polyme-tallic concentrate from „Rudnik” flotation plant is presented in Figure 4.

Figure 4 - Microphotograph of the polymetallic sulphide concentrate: 1-chalcopyrite, 2-pyrrhotite, 3-sphalerite,
4-quartz and 5-galena

Sulphide monominerals are predominantly irregu-
lar in shape, with dimensions in the range 10-100µm.
Besides, there can be observed simple and complex
adherent minerals, with different combinations; mu-
tually adhered beneficial minerals or minerals adhered
with gangue minerals, predominantly quartz. Ther-

omgram of polymetallic concentrate obtained at a hea-
ting rate of 10 °C/min in air and shown in Figure 5.
When the concentrate is heated, there is an increase in mass, which is accompanied by more or less pronounced exothermic effects (up to 730°C), which are the result of the presence of several types of sulfides that oxidize differently. Further heating leads to a sudden loss of mass, which also occurs in several stages, which indicates that more different sulfates are present. These mass losses are accompanied by endothermic effects, of which they are clearly expressed at 776°C (CuSO₄ dissociation) and 855°C (CuSO₄·CuO dissociation).

4.2. Influence of the Operating Parameters

The experimental results on determination of leaching parameters of polymetallic concentrate from „Rudnik“ flotation plant with sulphuric acid in the presence of sodium nitrate were performed in the temperature range of 20-90°C and during the time intervals 60-240 min. Further, the optimum values were: the phase ratio solid/liquid (S:L) = 1:5, the starting sulphuric acid concentration 225g/dm³, the sodium nitrate content exceeds 30% of the stoichiometric calculated value.

The influences of temperature and time on the leaching degrees of the zinc, copper and iron are presented in Figure 6.

![Figure 5 - DTA/TG analysis of polymetallic concentrate](image)

![Figure 6 - Temperature and the leaching time influence on the leaching degrees: S:L=1:5, the starting concentration of H₂SO₄=225g/dm³, NaNO₃ content 30% above the stoichiometrically needed, the stirring speed 300r/min](image)
It is well known that the oxidative dis-solution of galena produces insoluble PbSO₄ in the sulphuric acid leaching medium [51]. Low leaching degree is obvious for all three metals, but for copper it is extremely low (Fig. 6.a). The similar situation occurs for the influence of time on the leaching degrees at the temperature of 40°C (Fig. 6.b).

Onset of leaching degrees is noticeable at the temperature of 60°C (Fig. 6.c), where the zinc leaching degree is the highest. Further temperature increasing contributes that all three metals leaching degrees increase (Fig. 6.d), and finally reaching the temperature of 90°C at time of 240 min (Fig. 6.e). It is important to notice that in contrast to the lower temperatures, when the process goes on above 50°C the zinc leaching degree is higher than that for iron.

4.3. Characterization of the Solid Residuals

Characterization of the solid residuals after the leaching process included chemical and mineralogical analyses. The samples were chosen to be representative regarding a wide range of possible leaching products. Chemical analysis of the solid residual after the leaching is presented in Table 4, as well as the overall mass of the solid residual after the leaching process.

Table 4. Chemical analysis of the solid residual: \( t=90^\circ\text{C}, \ \tau=240 \text{ min}, \ S:L=1:5, \) the starting concentration of \( \text{H}_2\text{SO}_4=225 \text{ g/dm}^3, \) NaNO₃ content 30% above the stoichiometrically needed, the stirring speed 300 r/min

| Mass of the concentrate (g) | Mass of the solid residual (g) | Composition of solid residual (%) |
|----------------------------|-------------------------------|----------------------------------|
| 100.00                     | 59.90                         | Zn 1.41 Cu 3.88 Fe 8.97 Pb 20.93 |

X-ray diffraction (XRD) analysis, presented in Fig. 7, was used for determination of the mineral composition of the solid residual after the leaching process.

![Figure 7 - X-ray diffraction (XRD) analysis of the solid residual after the leaching: \( t=90^\circ\text{C}, \ \tau=240 \text{ min}, \ S:L=1:5, \) the starting concentration of \( \text{H}_2\text{SO}_4=225 \text{ g/dm}^3, \) NaNO₃ content 30% above the stoichiometrically needed, stirring speed 300 r/min [20]](image)

![Figure 8 - Microphotograph of the solid residual after leaching (X Nicols, in oil): \( t=90^\circ\text{C}, \ \tau=240 \text{ min}, \ S:L=1:5, \) the starting concentration of \( \text{H}_2\text{SO}_4=225 \text{ g/dm}^3, \) NaNO₃ content 30% above the stoichiometrically needed, stirring speed 300 r/min](image)
Microphotographs were taken on a prepared sample of the solid residuals after the leaching process for detection of the present phases. A microphotograph of a selected sample is shown in Fig. 8. For the reason of better phases recognition, the cedar oil was used.

The presence of sulphur and greater amount of anglesite, which shines milky white, is evident in Fig. 8, and corroded chalcopyrite and pyrrhotite are situated next to the right figure’s margin. Thermogram of the solid residual after leaching obtained at a heating rate of 10 °C/min in air and shown in Figure 9.

![Figure 9 - DTA/TG analysis of polymetallic concentrate](image)

When the sample is heated, an endothermic peak characteristic of elemental sulfur is observed at a temperature of 118°C. After that, there is a large loss of mass in the range of 250-350°C, which is a consequence of the oxidation of a large amount of sulfur to SO$_2$. The increase in mass followed by exo-thermic effects takes place in the range of 350-600°C and is much smaller than the increase in mass in polymetallic concentrate, which indicates the presence of a small amount of unleaded sulfides. The mass loss above 700°C is the result of the dissociation of the present sulphates (mainly anglesites) and is much smaller in relation to the analogous mass loss in concentrates before leaching.

5. CONCLUSION

Based on the chosen leaching chemism of the polymetallic sulphide Zn-Pb-Cu concentrate and its thermodynamical analysis, the assumed chemical reactions mechanism for zinc, copper and iron leaching is confirmed.

The phases detection in both, the starting concentrate and the products after the leaching process with H$_2$SO$_4$ and NaNO$_3$, were performed for better understanding of the chemical reactions that took place in the system.

The presence of the anglesite, elemental sulphur, gangue and unleached sulphide minerals, was registered using X-ray diffraction (XRD) analysis of the solid residual. This fact points out that leaching product of any sulphide mineral is elemental sulphur, which does not oxidize to sulphate in the temperature range (20-90°C) and the time interval (60-240 min).

After the leaching process, copper and zinc are in the form of copper(II) sulphate and zinc(II) sulphate. Iron is being oxidized to form iron(III) sulphate, which then acts as a leaching agent for the present sulphide minerals, and at the same time become reduced to iron(II) sulphate. Lead from the galena reacts to form the lead sulphate (anglesite), which is insoluble and remains in the precipitate.

Detailed mineralogical investigations indicate a polymetallic concentrate complexity and explain weak leaching effect of sulphide minerals in the final leaching stage. The main reasons for that are:

- elemental sulphur and anglesite, formed during the process and precipitate at the grain boundaries, fine grained mineral structure and complex mutual inter-growth of chalcopyrite, sphalerite, galena and pyrrhotite (inclusion, impregnation, simple and complex inter-growth),
- complex adhered beneficial sulphide minerals with gangue minerals (predominantly quartz).

The accomplished leaching degrees under the given conditions (temperature of 90°C, time of 4 hours, phase ratio S:L=1:5, the starting H$_2$SO$_4$ concentration of 225g/dm$^3$, with sodium nitrate addition in the content of 30% above the stoichiometric needed) are as follow: Zn – 89.25%, Cu – 73.08% and Fe – 70.80%.

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REZIME

LUŽENJE POLIMETALNOG CU-ZN-PB KONCENTRATA NATRIJUM-NITRATOM I SUMPORNOM KISELINOM

U radu su prikazani i diskutovani rezultati luženja polimetalnog sulfidnog Cu-Zn-Pb koncentrata rastvorom natrijum-nitrata i sumporne kiseline pri atmosferskom pritisku. Prikazan je hemijski i mineraloški sastav polaznog koncentrata i čvrstih ostataka nakon procesa luženja. Hemijske reakcije luženja i mogućnosti njihovog odvijanja analizirane su primenom termodinamičke analize na osnovu izračunatih Gibbsovih energija i analize E-pH dijagrama. Eksperimentalno je analiziran uticaj temperature i vremena na stepen izluženja korisnih metala iz sulfidnog koncentrata. Pokazano je da je moguće dobiti bakar, cink i železo u rastvoru u obliku sulfata, dok olovo u obliku anglesita (PbSO4) ostaje u čvrstom ostatku nakon procesa luženja. Železo se oksidiše u Fe (III) - sulfat, koji učestvuje u luženju sulfidnih minerala i prelazi u Fe (II) - sulfat.

Ključne reči: polimetalni Cu-Zn-Pb koncentrat, luženje, natrijum-nitrat, sumporna kiselina