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Emission Abatement Technology Selection, Routing and Speed Optimization of Hybrid Ships

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Abstract: This paper evaluates the effect of a large-capacity electrical energy storage, e.g., Li-ion battery, on optimal sailing routes, speeds, fuel choice, and emission abatement technology selection. Despite rapid cost reduction and performance improvement, current Li-ion chemistries are infeasible for providing the total energy demand for ocean-crossing ships because the energy density is up to two orders of magnitude less than in liquid hydrocarbon fuels. However, limited distance zero-emission port arrival, mooring, and port departure are attainable. In this context, we formulate two groups of numerical problems. First, the well-known Emission Control Area (ECA) routing problem is extended with battery-powered zero-emission legs. ECAs have incentivized ship operators to choose longer distance routes to avoid using expensive low sulfur fuel required for compliance, resulting in increased greenhouse gas (GHG) emissions. The second problem evaluates the trade-off between battery capacity and speed on battery-powered zero-emission port arrival and departure legs. We develop a mixed-integer quadratically constrained program to investigate the least cost system configuration and operation. We find that the optimal speed is up to 50% slower on battery-powered legs compared to the baseline without zero-emission constraint. The slower speed on the zero-emission legs is compensated by higher speed throughout the rest of the voyage, which may increase the total amount of GHG emissions.

Keywords: optimization; mathematical programming; ship design; emission abatement; hybrid propulsion; speed optimization; maritime routing; energy storage

1. Introduction

Maritime transport exerts a negative external impact via emissions that accelerate global warming and contribute negatively to air quality in urban coastal areas. Although shipping emissions are regulated nowadays, they are nevertheless estimated to account for 250,000 deaths and 6.4 million asthma cases annually [1]. Due to the pressure to reduce emissions, and the high cost of abatement systems, identifying least-cost strategies for meeting reduction targets has received considerable attention [2–12].

In recent years, Li-ion batteries have emerged as an option for reducing emissions and increasing the energy efficiency of ships. The average Li-ion pack price fell 85% from 2010 to 2018, while energy density increased by 150% from 2008 to 2014 [13,14]. Nevertheless, current Li-ion-based chemistries are infeasible for providing the entire energy demand for ocean-crossing ships because the energy density is 25–100 times less than in liquid hydrocarbon fuels [15]. However, short-distance zero-emission port arrival, mooring, and port departure are potential applications. A few shipowners have already adopted megawatt-hour scale batteries for this purpose [16,17].

This paper focuses on investment cost, operation cost and emissions trade-offs in ships equipped with large capacity batteries aimed at supplying complete propulsion and hotel energy demands for selected legs in a voyage. A mathematical programming
(optimization) model is developed for identifying routing, speed and technology choices that meet voyage objectives and emission constraints at least cost.

1.1. Related Work and Background

The International Maritime Organization (IMO) enforces international regulations on emissions to water and air in the maritime sector. The IMO targets a shipping-related greenhouse gas (GHG) emissions reduction by 50% by 2050 compared to the 2008 baseline level [18]. To reach this target, The International Convention for the Prevention of Pollution from Ships (MARPOL) Annex VI limits shipping-related carbon dioxide emissions via an energy efficiency design index (EEDI) that applies to newbuilds. A planned amendment for MARPOL Annex VI extends the regulation to existing ships through the energy efficiency design index for existing ships (EEXI). The primary technical measure to conform to EEXI is expected to be the de-rating of main engines and the adoption of energy efficiency improving technologies. A carbon intensity indicator (CII) is also planned to be put into effect, limiting measured carbon dioxide emissions [18]. In addition, in June 2021, the European Union announced a plan to add shipping to the carbon trading market [19].

MARPOL Annex VI also regulates sulfur oxides (SO$_x$), nitrogen oxides (NO$_x$), and particulate matter with a diameter of less than 2.5 micrometers. Similar to EEDI, the limit for emitted NO$_x$ is ship-specific, dependent on rated engine speed. Different levels (Tiers) of NO$_x$ control apply based on ship construction date (2011, 2016, or 2021) and operating area [20]. Other types of regulated emissions to water or air include noxious liquid substances, sewage, garbage, and ballast water [3]. Since these types of emissions do not depend on the energy system configuration, they are not discussed further in this work.

Stricter emission standards for NO$_x$ and SO$_x$ are in place when operating inside a designated emission control area (ECA), all of which are located in North America, the Caribbean, and Europe. While the Tier II NO$_x$ emission standard applies globally for engines installed in 2016 or later, the Tier III limit applies in North American and the US Caribbean Sea ECA. For new engines installed from 2021, the Tier III limit also applies in the North Sea and Baltic Sea ECA. According to MARPOL Annex VI, the maximum global fuel sulfur limit for all ships is currently 0.5% in weight for all fuels used for propulsion. The limit in SO$_x$ emission control areas (SECA) is 0.1%, which covers all the previously mentioned ECAs supplemented with the English channel [20].

The term air emission control applies to any measure that reduces the amount of harmful emissions being released into the air [4]. The two major categories of technical controls are energy efficiency and emissions reduction. The measures in the first category reduce fuel consumption. Here, the primary measures are hull form optimization, hull coating, propeller flow optimization, waste heat recovery, and wind assistance. Interestingly, adoption in the industry has been scarce, despite most measures generating positive cash flow for shipowners [2]. The second category contains measures that reduce one or more pollutants compared to unregulated combustion of heavy fuel oil. Low sulfur fuels and liquified natural gas (LNG) fall into this group as well as exhaust gas treatment devices, humid air motor, fuel–water emulsion, direct water injection and exhaust gas recirculation. Comprehensive compiled lists of control measures and discussions of their characteristics are available in the literature [2,3].

The three primary options to comply with IMO SO$_x$ regulations are low sulfur fuels, scrubbers, and LNG. Scrubbers and LNG are more attractive choices for new ships, while low sulfur fuels are typically adopted for older ships since retrofit conversion to LNG or scrubber installation may be infeasible or economically unattractive. The reaction from shipowners to Baltic Sea SO$_x$ regulations, which entered into force in 2015, has been mainly fuel switching [21]. An exception is roll-on/roll-off ferries, in which scrubber retrofits have been a popular choice. This was explained by stability from long term contracts, high service speed, and a fixed route entirely inside ECA [21]. Ship size has no impact on choices, but significant differences appear by ship type [22].
Logistics based (operational) measures include optimizing speed, route, and fleet deployment [23]. Enforcement of sulfur oxide emission limits in SECAs has given rise to a novel routing problem. Fagerholt et al. [24] evaluated the impact of ECA regulations on speed and routing decisions. Alternative means of complying with the regulations were switching to a more expensive low sulfur fuel or navigating along a longer route that bypasses the ECA. The work showed that the total amount of fuel consumed and CO₂ emitted may increase in some routes because shipowners choose to sail longer routes that bypass ECA. Furthermore, cost-optimal speed is lower inside the ECA than outside due to the higher cost of sailing inside the ECA. The approximate cubic relation between speed and propulsion power (and fuel mass flow) means that variation in speeds between sailing segments results in higher overall fuel consumption compared to a constant speed throughout the voyage.

Ships with varying operation profiles and dynamic positioning achieve significant fuel consumption and emission reduction by use of hybrid power supply and hybrid propulsion architectures [25]. Hybrid power supply, consisting of a Li-ion battery and generating sets, has been studied in ferries for spinning reserve [8], and for transient loading and peak shaving in tugs [26], fishing boats [27], and ferries [28]. Minimization of transient loads and load leveling by a battery for ocean-going bulk carriers has also produced promising results [29]. Hybrid propulsion allows reducing local NOₓ and particulate matter emissions in coastal areas by shutting down the 2-stroke main engine and supplying propulsion power from 4-stroke auxiliary engines via a shaft motor [30].

Works addressing the challenge of reducing the environmental impact of shipping from a decision-making perspective have appeared at a growing pace in the last decade. Multiple-criteria decision analysis, in general, and the analytical hierarchy process are the most widely used approaches [10–12]. The analytical hierarchy process relies on designers’ experience with assigning relative weights to decision criteria. Pruyn et al. [3] label these methods evaluative and contrast them to optimization methods. These approaches formulate a mathematical objective function to be minimized, which is typically economical, and a set of constraints for the decision variables. The emission control option selection gives rise to a nonconvex integer or mixed-integer programming problem because the choice to select or omit a given control option is a binary decision. Branch-and-bound and simplex methods are algorithm choices for integer linear programming problems.

Integer linear programming problem formulations are widely used because they can be solved efficiently, and the global solution is guaranteed (within a tolerance) if the problem is feasible. However, the linearity requirement is a limitation if the original problem is nonlinear and needs to be approximated. The previously discussed routing and speed optimization fall under integer linear programs. Similarly, Balland et al. [4] address the selection of emission controls subject to gradually tightening regulations. Baldi et al. [5] extend the analysis to alternative fuels and fuel cells that offer a path towards zero emissions. Winebreake et al. [6] present a nonlinear problem for selecting controls for a fleet of coastal ferries. However, sulfur emissions are not addressed, and the algorithm is not discussed either.

1.2. Aim and Contribution

The literature on operational decision-making (routing, speed, and fuel choice) is well established, but work that combines operation and design decisions is scarce. However, installation and sizing decisions are emphasized for energy storage with high investment costs. In particular, the trade-off between battery capacity and speed on a zero-emission area has received limited attention in the literature that mostly relies on simulations and fixed operation profiles [31]. While the potential of a battery to reduce local emissions has been highlighted, the effect of total voyage GHG emissions requires systematic analysis.

Within the context of increasing deployment of local zero-emission areas and onboard energy storage units, this paper proposes a nonlinear mixed-integer programming model for simultaneously optimizing routing between a predetermined sequence of ports, speed
on each sailing leg, fuel selection and sizing of exhaust gas cleaning units and energy stor-
gages. The developed model takes the shipowner’s perspective and minimizes a weighted
objective of investment and operation costs. The solution to the optimization problems
reveals the response of shipowners and is applied to address the impact of zero-emission
areas on total emissions. Furthermore, the paper provides a decision support tool for
shipowners for managing the novel ship design and operation problems arising from
stricter environmental regulations. Two groups of numerical case study problems are
formulated to address the research questions.

2. Model Formulation

2.1. Modelling Approach

In this work, we investigate trade-offs in emission-restricted shipping by mathematical
programming. The solution of the optimization problem represents an assignment of
technology choices and operation strategy to the ship that achieves performance goals at
the least total annualized cost for a shipowner. The set of technology choices consists of
engines and exhaust gas treatment units. Operational choices include routing, speed, fuel
and battery charging or discharging power. Performance goals are related to emission
limits and voyage duration upper bounds. Discrete technology choices and nonlinear
relationships between variables give rise to a mixed-integer nonlinear programming model.

We consider a single ship with a given sequence of port calls and an upper bound for
total voyage duration. Figure 1 illustrates how alternative routes are assembled from sailing
legs. A route from one port to next consists of two or more sequential legs when the route
crosses a border, such as an ECA. Another reason for sequential legs is the incorporation of
a speed limit on a fairway. Zero-emission port arrival and departure schemes also require
leg splitting.

![Figure 1. Construction of alternative routes from a set of sailing legs.](image)

Each leg has a constant speed that is subject to optimization. Arrival to the destination
port must not exceed a given arrival time, regardless of the route chosen. However,
the arrival and departure times to ports between the first and last depend on speeds
used on the legs. Time window constraints are not included in the model or the analyses
conducted in this paper, although the constraints for such windows are linear and, thus,
easy to model [24].

Following the convention in the literature, we model the required propeller thrust
force as a quadratic function of speed. Consequently, shaft power and fuel consumption
are cubic functions of speed. This approach is deemed reasonable, although inaccuracies
have been recognized in the literature for near zero speeds and high speeds typical for
some container ships [32]. The required thrust also depends on external conditions, such
as hull fouling, wind direction and wind speed. We discard these other sources since
they are not central to the research questions addressed in this work. Auxiliary power for
electricity is assumed constant and generated by either a shaft generator, auxiliary engines
or discharged from a battery.

2.2. Model Description

2.2.1. Notation

We use $\mathbb{R}_+$ to denote the set of nonnegative real numbers, $\mathbb{Z}_+$ the set of whole numbers
and $\mathbb{Z}_2$ the set of binary numbers. The set of $n$-vectors is denoted by the superscript $n,$
and the set of $m \times n$ matrices is denoted by the superscript $m \times n$. For example, the set of nonnegative real $m \times n$ matrices is denoted by $\mathbb{R}_{+}^{m \times n}$. A subvector of a vector $x$ with entries from $r$ to $s$ is expressed as $x_{r:s}$. The symbol $\mathbf{1}$ denotes a row vector whose entries are all ones. Its dimension is determined by context. The symbol $\preceq$ denotes componentwise inequality between vectors and the symbol $\odot$ the elementwise (Hadamard) multiplication. Finally, Table 1 shows the indexing set cardinalities, decision variables and parameters of the optimization model.

Table 1. Model notation. EGT stands for exhaust gas treatment.

| Indexing          | Number of fuels |
|-------------------|-----------------|
| $n \in \mathbb{Z}^{+}$ |                 |
| $m \in \mathbb{Z}^{+}$ |                 |
| $k \in \mathbb{Z}^{+}$ |                 |
| $p \in \mathbb{Z}^{+}$ | Number of pollutant types |
| $s \in \mathbb{Z}^{+}$ | Number of engine types |
| $r \in \mathbb{Z}^{+}$ | Number of exhaust gas treatment unit types |
| Variables         | Speed on legs $1 \ldots s$ (km/h) |
| $v \in \mathbb{R}_{+}^{s}$ |                 |
| $t \in \mathbb{R}_{+}^{s}$ | Sailing duration on legs $1 \ldots s$ (h) |
| $f \in \mathbb{R}_{+}^{n \times s}$ | Power output from use of fuels $1 \ldots n$ on legs $1 \ldots s$ (MWh) |
| $e \in \mathbb{R}_{+}^{p \times s}$ | Utilization rate of EGT units $1 \ldots p$ on legs $1 \ldots s$ (MWh) |
| $q \in \mathbb{R}_{+}^{s+1}$ | Battery charge on legs $1 \ldots s+1$ (MWh) |
| $\bar{q} \geq 0$ | Battery capacity (MWh) |
| $\Delta q^{(+)} \in \mathbb{R}_{+}^{s}$ | Charged energy to battery on legs $1 \ldots m$ (MWh) |
| $\Delta q^{(-)} \in \mathbb{R}_{+}^{s}$ | Discharged energy from battery on legs $1 \ldots m$ (MWh) |
| Parameters        | Decision to install engines $1 \ldots k$ |
| $y \in \mathbb{Z}_{k}^{s}$ |                 |
| $g \in \mathbb{Z}_{p}^{s}$ | Decision to install EGT units $1 \ldots p$ |
| $z \in \mathbb{Z}_{r}^{s}$ | Decision to sail on routes $1 \ldots r$ |
| $o \in \mathbb{Z}_{n}^{s}$ | Energy drawn from onshore power supply on legs $1 \ldots s$ (MWh) |
| $S \in \mathbb{Z}_{2}^{s \times r}$ | Allocation of legs to routes |
| $F \in \mathbb{R}_{+}^{m \times n}$ | Mapping between fuels and pollutants (kg/MWh) |
| $K \in \mathbb{Z}_{n \times k}^{s}$ | Compatibility of fuels with engines |
| $P \in \mathbb{R}_{+}^{m \times p}$ | Reduction of pollutant streams in EGTs (kg/MWh) |
| $U \in \mathbb{R}_{+}^{m \times s}$ | Specific pollutant limits on legs (kg/MWh) |
| $Q \in \mathbb{R}_{+}^{n}$ | Lower heating values of fuels (MWh/ton) |
| $E \in \mathbb{R}_{+}^{p}$ | Electricity consumption of EGT units (%/100) |
| $D \in \mathbb{R}_{+}^{s}$ | Leg distance (km) |
| $O \in \mathbb{Z}_{2}^{s}$ | Onshore power supply availability |
| $C_{\text{ENG}} \in \mathbb{R}_{+}^{k}$ | Engine investment costs (EUR) |
| $C_{\text{EGT}} \in \mathbb{R}_{+}^{p}$ | EGT investment costs (EUR) |
| $C_{\text{USE}} \in \mathbb{R}_{+}^{p}$ | EGT operating costs (EUR/MWh) |
| $C_{\text{FUEL}} \in \mathbb{R}_{+}^{n}$ | Fuel prices (EUR/ton) |
| $C_{\text{EES}} \geq 0$ | Battery investment cost (EUR/MWh) |
| $C_{\text{OPS}} > 0$ | Onshore power supply electricity cost (EUR/MWh) |
| $T > 0$ | Total voyage duration (h) |
| $A > 0$ | Auxiliary electric power (MW) |
| $R > 0$ | Hull resistance coefficient |
| $\eta > 0$ | Battery charging and discharging efficiency |
| $\eta' > 0$ | Engine efficiency |
| $\Psi > 0$ | Investment cost scaling factor |
2.2.2. Energy Use

The ship energy system model consists of the following primary groups:
- Main engines as mechanical energy sources,
- Propellers as mechanical energy sinks,
- Auxiliary engines and battery (in discharge mode) as electrical energy sources,
- Hotel load, exhaust gas treatment units and battery (in charge mode) as electrical energy sinks.

We work with interchangeable mechanical and electrical energies when balancing the sources with sinks. Excluding electric propulsion, this approach is viable with power take-out and power take-in functions of a shaft generator/motor. In its basic form, the energy balance is a nonconvex equality constraint due to the quadratic hull resistance term. By relaxing the constraint to inequality, we express it as a convex quadratic constraint that holds with equality:

\[
f^T_{ij} 1 + \Delta q^{(-)}_i + o_i \geq \Delta q^{(+)}_i + D_i R t_i^2 + A t_i + E^T e_{ij}, \quad \forall i \in \Omega,
\]

where \( \Omega = \{1 \ldots s\} \) denotes the set of sailing legs. The first term on the left-hand side is an inner product that gives a scalar for total engine power output for the \( i \)th leg. Battery discharge and onshore power supply are the other energy sources. The terms on the right-hand side account for battery charging, hull resistance, hotel and exhaust gas treatment unit electricity consumption, respectively.

Electricity can be drawn from onshore power supply only on legs in which the ship is docked, expressed as

\[
o \preceq OM,
\]

where \( M \) is a sufficiently large scalar. Decision variable \( o \) and problem data \( O \) are vectors in \( \mathbb{R}^s \), and the inequality between them means componentwise. Thus, (2) is equivalent to both of the following expressions:

\[
o_i \leq O_i M, \quad \forall i \in \Omega,
\]

\[
\begin{bmatrix}
o_1 \\
o_2 \\
\vdots \\
o_s
\end{bmatrix} \preceq
\begin{bmatrix}
o_1 \\
o_2 \\
\vdots \\
o_s
\end{bmatrix} M.
\]

For the remainder of the paper, we apply the componentwise inequality without explicitly pointing it out.

2.2.3. Emissions

The emission limit constraint enforces the geographical location-specific upper bounds on pollutant streams according to IMO regulations. The constraint has three terms: (1) pollutant streams generated from combustion of fuels, (2) pollutant streams removed by exhaust gas treatment and (3) upper bound for the quantity of pollutant exiting the ship to air:

\[
F f_{ij} - P e_{ij} \preceq f^T_{ij} 1 U_{ij}, \quad \forall i \in \Omega.
\]

We defined a problem data matrix \( F \) to map pollutant streams to a combustion of fuels. The matrix-vector product \( F f_{ij} \) is a vector in \( \mathbb{R}^m \), where the elements are the quantities of different pollutant streams from combustion of all fuels on the \( i \)th leg. In the second term, the data matrix \( P \) maps exhaust gas treatment units to emission streams. These streams are cleaned from exhaust gas in proportion to the load of the cleaning units.
2.2.4. Battery Operation

Battery operation is governed by constraints for the time-integration element, boundary conditions and charging limits. We can bundle changes in the state of charge and initial and final state to the same constraint according to

\[
q = \left[ \begin{array}{c} q_s \\ q_{1:s-1} \end{array} \right] + \eta \left[ \begin{array}{c} 0 \\ \Delta q^{(+)} \end{array} \right] - \frac{1}{\eta} \left[ \begin{array}{c} 0 \\ \Delta q^{(-)} \end{array} \right].
\]

At each leg, the state of charge is determined by the previous level and the change in electrical energy during the period. Moreover, the initial charge equals the final charge. Charged energy cannot exceed installed capacity, which is expressed simply as

\[
q \leq 1q.
\]

Due to the routing functionality in the model, charging and discharging must be prohibited on legs that do not belong to the selected route according to

\[
\Delta q^{(+)} + \Delta q^{(-)} \leq MSg,
\]

where \(S\) is a problem data matrix that allocates legs to routes and \(g\) is a vector of binary variables for route selection.

2.2.5. Unit Installation

The binary variables \(y\) and \(z\) encode engine and exhaust gas treatment unit installation decisions. Consumption of fuels in a unit can be nonzero at any voyage leg only if the corresponding unit is installed. The same logic governs exhaust gas cleaning system installation and emission streams. These constraints are expressed as

\[
MKy \geq f_{i,j}r, \quad \forall i \in \Omega,
\]

\[
Mz \geq e_{i,j}, \quad \forall i \in \Omega,
\]

with data matrix \(K\) mapping fuels to conversion units. Both rows and columns of \(K\) may possess more than one nonzero element to support fuel switching and supply of a given fuel to different engine types. The scalar \(M\) receives a sufficiently large value to cover the maximum output of all units.

2.2.6. Routing and Speed

The relationship between ship speed and leg sailing duration variables is expressed as

\[
D_iS_{i,g} \leq t_i, \quad \forall i \in \Omega,
\]

with problem data matrix \(S\) allocating legs to alternative routes. Binary vector variable \(g\) selects which legs are activated on a voyage. Since a ship can only sail along a single route, we allow only one element of the vector \(g\) to take the value of one. In addition, the total duration of the voyage is bounded. These two constraints are formulated as

\[
g^T1 = 1,
\]

\[
t^T1 \leq T,
\]

where the parameter \(T\) is the maximum voyage duration.

2.2.7. Objective Function

The objective is to minimize total cost:

\[
\text{minimize} \quad c^{\text{TOT}} = c^{\text{INVESTMENT}} + c^{\text{OPERATION}},
\]
where the operational cost components are the fuel consumed by the engines, chemicals consumed by the exhaust gas treatment units and onshore power supply electricity, according to

$$c_{\text{OPERATION}} = 1^T \left[ \begin{array}{c} f e \end{array} \right]^T \left[ \begin{array}{c} C_{\text{FUEL}} \\ C_{\text{USE}} \\ C_{\text{OPS}} \end{array} \right] \circ \left[ \begin{array}{c} 1 \\ \eta' \end{array} \right] \circ \left[ \begin{array}{c} 1 \\ Q \end{array} \right],$$  

(15)

with the symbol/\(\circ\)/denoting elementwise division. The first vector-matrix product on the right-hand side produces a column vector with entries of fuel use, exhaust gas cleaning unit utilization and onshore power supply energy summed over all the sailing legs 1 \ldots s. The last two terms on the right-hand side are \((n+p+1)\)-vectors, in which \(Q\) and \(\eta'\) are \(n\)-vectors.

Investment cost is a function of the installed units in the system:

$$c_{\text{INVESTMENT}} = \Psi \left[ \begin{array}{c} y \\ z \end{array} \right]^T \left[ \begin{array}{c} C_{\text{ENG}} \\ C_{\text{EGT}} \end{array} \right],$$  

(16)

with the parameter \(\psi\) applied for scaling the investment cost on a voyage basis.

### 2.3. Problem Form and Solution Approach

The optimization problem defined by constraint set (1)–(13) and the objective (14) is nonlinear and nonconvex. Nonlinearity arises from the convex quadratic terms in (1) and the bilinear product terms in (11). Nonconvexity arises from the binary decision variables and the bilinear terms (11). Thus, the problem belongs to the group of nonconvex mixed-integer quadratically constrained programs (MIQCP). In this case, the problem is nonconvex even after the binary variables are relaxed to continuous variables. Nonconvex problems are in general intractable or solved locally at best. However, nonconvex MIQCPs allow deterministic algorithms that guarantee the global solution, unlike heuristic evolutionary algorithms (e.g., NSGA-II) [33,34]. Various commercial solver packages are available for code implementations. We make use of Gurobi 9.1.

### 3. Problem Data

This section presents data from the literature regarding emissions, cost of engines, exhaust gas treatment units and fuels. The focus is on extracting parameter values for the model that represent the properties of fuels and characteristics of equipment cost as a function of installed power. Component performance and cost models are first discussed, and the last subsection summarizes cost parameter values applied in numerical case studies.

#### 3.1. Emissions

The primary pollutants accounting for global warming are carbon dioxide, methane (\(\text{CH}_4\)) and nitrous oxide (\(\text{N}_2\text{O}\)). For GHG emissions, the whole fuel life cycle is included in this study, from raw material extraction, production, storage and distribution to combustion in medium-speed marine engines. The processes from raw material extraction to distribution are termed well-to-tank, and the combustion in an engine for ship propulsion is termed tank-to-propeller. Local pollutants \((\text{NO}_x)\) and \((\text{SO}_x)\) are considered from the tank-to-propeller perspective, meaning only the emissions released during ship operation are taken into account. Particulate matter emissions are excluded from the analysis.

Table 2 outlines the emission data. The presented figures are motivated in the following subsections.
Table 2. Specific emission factors for greenhouse gas (GHG) emissions and local pollutants at cruising load (85%). Fuel options are high sulfur fuel oil (HSFO), marine gas oil (MGO), liquified natural gas (LNG). Greenhouse gases are carbon dioxide (CO₂), methane (CH₄) and nitrous oxide (N₂O). Local pollutants are sulfur oxides (SOₓ) and nitrogen dioxide (NO₂). EGT stands for exhaust gas treatment and means that both a scrubber and selective catalytic reduction (SCR) system are installed. SFOC stands for specific fuel oil consumption.

|                      | HSFO     | HSFO + EGT | MGO       | MGO + SCR | LNG       | Source       |
|----------------------|----------|------------|-----------|-----------|-----------|--------------|
| Well-to-tank GHG     |          |            |           |           |           |              |
| CO₂ (g/MJ fuel)      | 13.2     | 13.2       | 14.1      | 14.1      | 13.7      | [35,36]      |
| CH₄ (g/MJ fuel)      | 0.028    | 0.028      | 0.028     | 0.028     | 0.15      | [35,36]      |
| CO₂-eq (g/MJ fuel)   | 14.2     | 14.2       | 15.1      | 15.1      | 18.8      |              |
| Combustion GHG       |          |            |           |           |           |              |
| CO₂ (g/kWh)          | 564      | 570        | 551       | 551       | 416       | [37]         |
| CH₄ (mg/kWh)         | 4        | 4          | 4         | 4         | 1000      | [38,39]      |
| N₂O (mg/kWh)         | 31       | 31         | 27        | 27        | 17        | [35]         |
| CO₂-eq (g/kWh)       | 573      | 581        | 560       | 560       | 456       |              |
| Local pollutants     |          |            |           |           |           |              |
| NOₓ (g/kWh)          | 11.7     | 2.0        | 9.6       | 1.9       | 1.7       | [38,39]      |
| SO₂ (g/kWh)          | 8.11     | 0.17       | 0.34      | 0.34      | 0.01      | [35]         |
| Inputs to propulsion  |          |            |           |           |           |              |
| SFOC (g/kWh)         | 181      | 184        | 172       | 172       |           | [37]         |
| Natural gas (g/kWh)  |          |            |           |           | 149       | [39]         |
| Pilot fuel (g/kWh)   |          |            |           |           | 2.1       | [39]         |
| Urea 100% (g/kWh)    | 6.3      |            |           |           | 5.0       | [40]         |
| NaOH 50% (g/kWh)     | 17.5     |            |           |           |           | [41]         |

3.1.1. Well-to-Tank Greenhouse Gasses

The production steps of crude-oil-based fuels include drilling and extracting the crude oil, pre-treatment, and transportation to market, refining, and distribution. Table 2 presents well-to-tank GHG emissions for fuels refined from crude originating from the Middle East. Marine gas oil (MGO) is assumed to follow the diesel pathway, and high sulfur fuel oil (HSFO) is equal to the average of petrol and diesel pathways.

The LNG supply chain covers natural gas production and processing, including well drilling, pipeline transport, purification and liquefaction, LNG carrier transport, and LNG terminal operations and maritime bunkering [35]. In Table 2, total well-to-tank GHG emissions are presented in terms of CO₂-equivalents, using 100-year global warming potential factors of 34 for (CH₄) and 298 for (N₂O) [42].

3.1.2. Tank-to-Propeller Greenhouse Gasses

Carbon dioxide originates from fuel combustion and can be directly linked to the engine fuel consumption and fuel carbon content. While other types of emissions can be reduced to low levels through control technologies, reducing CO₂ emissions is primarily dependent on reductions of fuel consumption. In Table 2, brake specific CO₂ emissions from fuel combustion are presented. When HSFO is used with the scrubber, the additional fuel needed to operate the scrubber is 1.0% [43]. CH₄ emissions in LNG operation correspond to a (CH₄) slip rate of 0.7%, which is typical for design point engine loading [39].

3.1.3. Power Generation Greenhouse Gasses

While a ship is docked, it draws electricity from the onshore power supply for supplying hotel load and battery charging. Although local emissions are zero, the emission from grid power generation must be accounted for. Fuel combustion in electricity generation in Finland was estimated to contribute 156 g/kWh CO₂-eq emissions to the atmosphere in 2017 [44]. When the supply chain is accounted for, from the extraction process to delivery,
the figure increases to 206 g/kWh. Moreover, the emission factor for electricity generation with the average EU electricity mix is more than double compared to Finland, which originates from different shares of renewable sources. Nevertheless, we apply the latter reported figure 206 g/kWh.

3.1.4. Nitrogen Oxides

The thermal mechanism is responsible for the majority of NO\textsubscript{x} emissions from fuel combustion. Therefore, NO\textsubscript{x} emissions are strongly affected by the temperature and the exposure time of the combustion gases to high temperatures [45]. A small portion of the resulting NO\textsubscript{x} originates from the nitrogen content of the fuel, which is higher in HSFO compared to MGO [46]. The brake specific NO\textsubscript{x} emissions in LNG operation are well below the accepted Tier III value, which is, e.g., with an engine speed of 600 rpm 2.5 g/kWh. In HSFO and MGO operations, Tier III limits are achieved using selective catalytic reduction (SCR) technology.

3.1.5. Sulfur Dioxide

Sulfur dioxide (SO\textsubscript{2}) emissions are linked to the sulfur content in the fuel. SO\textsubscript{2} emissions reported in Table 2 are derived from fuel consumption using a stoichiometric approach, assuming that all sulfur reacts to SO\textsubscript{2} according to

\[ \text{S + O}_2 \rightarrow \text{SO}_2. \]

Since the molar mass of a sulfur atom is 32 (g/mol), and 16 (g/mol) for an oxygen atom, one gram of sulfur in the fuel results in two grams of SO\textsubscript{2} [35].

The limits on the sulfur content of marine fuels are 0.5% globally and 0.1% in ECAs according to IMO regulations. An alternative way to meet the sulfur limit is by removing pollutants from the ship’s exhaust via a scrubber, allowing the use of a fuel with higher sulfur content. Table 2 presents the case in which a scrubber removes SO\textsubscript{x} emissions from the exhaust after combustion of HSFO. The scrubber efficiency of 97% is applied.

3.2. Scrubbers

The alkalinity of seawater in the ship’s operating area is a key factor for selecting the appropriate scrubber system. High seawater alkalinity is a prerequisite for the operation of an open loop scrubber. For low alkalinity waters, such as in the Baltic Sea, closed loop scrubbers consuming additive chemicals are available [47]. We work with closed loop scrubbers exclusively because the environmental impact of open loop scrubbers, which discharge process water overboard, remains an open issue [48].

Typical installation costs range from 200 to 400 EUR/kW, depending on scrubber type, market conditions, installed engine power and the ease of scrubber installation on a ship [49,50]. Scrubber retrofitting on existing ships is generally more challenging and 40% more expensive than newbuild installation [41,49]. In this study, the data for newbuild closed loop scrubber investments are used for calculations [50]. In addition to scrubber machinery and equipment costs, investment costs cover engineering design, installation, commissioning, documentation, and training. Revenue lost due to reduced cargo or passenger capacity is discarded.

Consumables, including power and chemicals, account for the majority of running costs. Electrical power consumption for closed loop systems is 0.5–1% of the engine power [43]. Alkali consumption depends on the sulfur content of the fuel used. In closed loop mode, 50% NaOH consumption is 5 kg per megawatt hour per sulfur reduction percentage [41]. Scrubber operation cost is 6 EUR/MWh in the most demanding scenario in which a ship sails inside SECA, runs on 3.5% sulfur HSFO and alkali price is 350 EUR/ton.

The additional maintenance and lubricating oil costs associated with HSFO operation, scrubber maintenance and sludge disposal costs are calculated by Spoof-Tuomi [51]. However, these costs are minor compared to power and alkali and are discarded in this study.
3.3. Selective Catalytic Reduction System

The SCR investment cost for marine engines is typically 30 to 100 EUR/kW [50,52]. The investment cost increases non-linearly with respect to engine power due to economy of scale. This study applies the cost figure 46 EUR/kW, which assumes newbuild installation and 30 MW engine installed power with optional HSFO operation [50]. HSFO operation requires larger catalysts and soot blowers resulting in 5% higher costs.

SCR operating costs comprise urea cost, maintenance cost, and catalyst replacement cost. The reducing agent in marine applications is 35–40% solution of urea in de-ionized water [53]. Urea dosing for target reduction $\Delta \text{NO}_x$ (g/kWh) is given by multiplying the target by 0.652. This multiplier is determined based on stoichiometric dosing, assuming 1:2 for urea:NH$_3$ stoichiometry and 1:1 for NO$_x$:NH$_3$ stoichiometry and molar mass for urea of 60 (g/mole) and molar mass for NO$_x$ of 46 (g/mole) [40]. SCR operating cost is 3.5 EUR/MWh, when the NO$_x$ target reduction rate is calculated for a medium speed engine running on HSFO or MGO, with the exhaust gas constituting 9.68 g/kWh NO$_x$ reduced to 2.5 g/kWh for compliance with Tier III in ECAs [54]. The urea price is 600 EUR/ton [55].

Maintenance requirements for the SCR system include regular cleaning of soot blowers and injection nozzles and filters in the urea handling system [47]. However, the costs associated with these activities are negligible [56]. In contrast, the activity of the catalyst decreases with time, resulting in costly repairs where the catalyst is replaced. The typical lifespan of a catalyst block is between two and five years [47]. Estimates of the catalyst replacement cost in the literature range from 0.28 to 1.09 EUR/MWh [52,57]. In this paper, the average value of 0.7 EUR/MWh is used.

An SCR after-treatment system can cause increased exhaust backpressure, typically by around 12–15 mbar at 100% engine load [58]. Any fuel penalties that may arise due to this slight increase in backpressure were not included. Another consideration is the compatibility of SCR with SO$_x$ scrubbers. Due to the backpressure generated by the scrubber and the low temperature at which the exhaust gas leaves the scrubber, the SCR must be installed upstream of the scrubber [58]. In this configuration, the SCR unit must be designed to operate with high-sulfur HSFO as well.

3.4. Fuels

HSFO blends are the conventional marine fuels. The most common grade is RMG 380, which has maximum 380 cSt viscosity at 50 °C and maximum 3.5% sulfur. The bunker price for this grade is quoted as IFO 380. This is the default fuel to be used with a scrubber in this study. IMO 2020 0.5% global sulfur limit and ECA 0.1% limit compliant fuels are available both in residual blends and distillates, in accordance with ISO 8217 specifications. A historical price data comparison of, e.g., 0.1% sulfur fuels marine gas oil distillate (DMA or DMZ ISO grade) and ultra low sulfur fuel oil residual (RMG 380 ISO grade), reveals that these two fuels are priced almost identically [59]. In this study, very low sulfur fuel oil (VLSFO) and low sulfur marine gas oil (LSMGO) are the options for meeting the 0.5% and 0.1% regulatory limits of fuel sulfur, respectively.

Historical price trends of marine fuels exhibit large fluctuations with changing market conditions [60]. Nevertheless, the price difference between various grades remains nearly constant (Figure 2). On the other hand, the LNG price in European ports is generally tied to European pipeline gas prices, supplemented by the additional costs of liquefaction and logistics. For the sake of simplicity, we fix the prices of conventional fuels according to quoted prices at the beginning of June 2021 and apply a range of values for LNG [59]. Table 3 presents the selected prices in euros per metric ton.
Figure 2. Price development of intermediate fuel oil (IFO) 380, 0.1% sulfur marine gas oil (MGO) and European Union (EU) natural gas from 1 August 2014 to 1 February 2021. The source price data in the unit $/mmBTU from [60] has been converted to EUR/GJ with USD to EUR exchange rate 0.943 and 1 mmBTU = 1.06 GJ.

Table 3. Prices of fuel grades from the Port of Rotterdam and onshore power supply electricity from the Port of Helsinki.

| Type                        | Abbreviation | Sulfur (%) | Price          | Source |
|-----------------------------|--------------|------------|----------------|--------|
| High sulfur fuel oil        | HSFO         | 3.5        | 386 EUR/ton    | [59]   |
| Very low sulfur fuel oil    | VLSFO        | 0.5        | 505 EUR/ton    | [59]   |
| Low sulfur marine gas oil   | LSMGO        | 0.1        | 560 EUR/ton    | [59]   |
| Liquified natural gas       | LNG          | 0          | 378–733 EUR/ton| [59]   |
| Electricity                 | OPS          | 0          | 84.8 EUR/MWh   | [61]   |

A ship equipped with a large capacity electrical energy storage draws multiple gigawatt-hours of electricity from an onshore power supply annually. Retail electricity prices for industrial customers consuming up to 20 GWh annually are reported in [61]. The reported prices consist of electric energy, distribution charge, and taxes. Although electric energy is traded on the spot market on an hourly basis with large price fluctuations, the historical monthly average price is highly consistent at 80 EUR/MWh. In this study, the onshore power supply connection electrical energy cost receives a value of 84.8 EUR/MWh, which was the average price in 2020 in Finland.

3.5. Li-Ion Battery System

Various lithium-based chemistries are commercially available for marine applications. They offer different trade-offs between cost, life span, specific energy, specific power, safety, and thermal performance [62]. LiNiMnCoO2 (NMC) offers high specific energy and energy density, which has high utility in ships with limited space, while the power output is sufficient for transient loads. NMC chemistry with a C-rate of four is assumed in the case studies. The battery investment cost is 400 EUR/kWh based on a realized marine pilot project with NMC chemistry [28].

The aging effect is a key factor to take into consideration in Li-ion batteries. In this work, the aging effect is accounted for by applying a scaling factor of 1.25 to the battery cost per unit of installed capacity, which accounts for a 20% decrease in capacity over the lifetime of the battery while sustaining the performance implied in the model formulation.

Table 4 summarizes cost data for installation and operation of diesel and dual fuel engines, Li-ion battery and exhaust gas treatment units. The scaling factor due to aging has not been applied in the presented figure for battery investment cost.
Table 4. Performance and cost data of energy conversion, storage and exhaust gas cleaning units. MS stands for medium speed and $\eta$ for efficiency.

| Unit Type             | $\eta$ (%) | Investment       | Operation        | Source |
|-----------------------|------------|------------------|------------------|--------|
| MS diesel engine      | 45         | 240 EUR/kW       |                  | [5]    |
| MS dual fuel engine   | 45         | 470 EUR/kW       |                  | [5]    |
| Li-ion battery        | 97         | 400 EUR/kWh      |                  | [28,63]| |
| Closed loop scrubber  |            | 375 EUR/kW       | 6 EUR/MWh        | [49]   |
| SCR system            |            | 46 EUR/kW        | 3.5 EUR/MWh      | [50]   |

3.6. Hull Resistance

Measurement data acquired from a 58,376 gross tonnage roll-on/roll-off passenger ferry is the basis for the resistance parameter value applied in the model instances. The ship sails in the Baltic Sea, with open sea cruising at 18 knots constituting most of the voyage. The ship is equipped with a conventional diesel mechanical propulsion, with four 4-stroke medium speed diesel engines that drive two main propeller shafts through reduction gearboxes. The primary electricity consumers are the three tunnel thrusters and the hotel load at a continuous rate of 2 MW. A more detailed description of the case ship is provided in [8].

4. Numerical Example Problems

The first problem group studies a voyage departing from Florø, Norway and arriving at Nantes, France (Figure 3). The voyage is similar to the one studied by Fagerholt et al. [24]. If a shipowner chooses to comply with the ECA SOx limit by fuel switching, they have three alternative route options to choose from in the North Sea. This route selection involves a trade-off between distance traveled and fuel expenditure. In Figure 3, the solid line illustrates the long distance option entirely outside ECA, the dotted line the option with a short ECA leg and the dashed line the shortest alternative traveling inside ECA in the North Sea. The shipowner chooses the minimum cost alternative based on the price difference between VLSFO and LSMGO. However, if the ship is equipped with a gas engine running on LNG or a diesel engine with a scrubber running on HSFO, the shortest route inside the ECA is always chosen.

The second problem group involves two actual shipping routes in the Baltic Sea arriving at Stockholm, Sweden and departing from Turku, Finland (orange trace in Figure 4) and Helsinki, Finland (blue trace, Figure 4). The Stockholm archipelago leg bounded by the red cone in Figure 4 has a distance of 80 km and a speed limit of 12 kn. Some problems in this group designate it as a zero-emission leg requiring battery-powered propulsion. The route departing from Turku has a 184 km open sea sailing leg, while in the Helsinki route, the open sea leg is 340 km. In this case, there are no alternative leg options because both routes sail entirely inside the Baltic Sea ECA.

The optimization model was implemented with Python interface functions of the commercial software Gurobi. Problem instances were solved with the Gurobi 9.1 solver with the default settings. The solution times for all test problems were less than five seconds. Thus, further reporting of solution times is omitted from the following sections.
Figure 3. Map of the route from Florø to Nantes and the alternative legs in the North Sea. ECA border is shown as light blue in the North Sea and the English channel. The red cones represent 10 km port arrival and departure legs which may be designated as zero-emission areas [9]. Background satellite image by Google.

Figure 4. Map of the Baltic Sea routes. Background satellite image by NASA.

5. Results and Discussion

5.1. North Sea Route

Tables 5 and 6 give the solutions to the speed, routing and technology selection optimization problems for the route from Florø to Nantes. The columns represent alternative legs for the voyage and a column populated with only zeros means that the selected route
does not include the corresponding leg. The rows for power output omit the constant auxiliary power. Moreover, the fuel rows give the contribution of the fuel to engine shaft output. Fuel consumption is not stated but can be calculated by dividing the former value by engine efficiency.

In the baseline case (Table 5), the cost optimal solution is achieved by scrubber installation, HSFO and the sailing along the shortest leg option in the North Sea. In this case, the scrubber is selected despite the availability of only the more expensive closed loop design, and that investment cost is weighted heavily (3 year payback) compared to operation cost.

Runs with forced compliance via fuel switching result in a higher objective value. However, even with fuel switching, the same route inside ECA is selected instead of the two slightly longer alternatives outside ECA that allow lower-priced VLSFO use. All the previously discussed results apply the LNG price from the top of the range in Table 3. The LNG price sweep run shows that the threshold LNG price is 569 EUR/ton, which is close to the middle of the range.

### Table 5. Baseline solution of the North Sea route. EGT stands for exhaust gas treatment. The column headers denote leg identifiers.

|   | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 |
|---|---|---|---|---|---|---|---|---|
| Speed, kn | 0.0 | 17.91 | 0.0 | 0.0 | 0.0 | 17.91 | 17.94 | 17.9 |
| Time, h | 0.0 | 0.3 | 0.0 | 0.0 | 0.0 | 14.03 | 14.04 | 14.1 |
| Power, MW | 0.0 | 14.03 | 0.0 | 0.0 | 0.0 | 14.04 | 14.1 | 14.02 |
| HSFO, MWh | 0.0 | 4.88 | 0.0 | 0.0 | 0.0 | 807.82 | 170.38 | 4.88 |
| VLSFO, MWh | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 |
| LSMGO, MWh | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 |
| LNG, MWh | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 |
| EGT-S, MWh | 0.0 | 4.88 | 0.0 | 0.0 | 0.0 | 807.82 | 150.34 | 4.88 |
| EGT-N, MWh | 0.0 | 4.88 | 0.0 | 0.0 | 0.0 | 807.82 | 0.0 | 4.88 |
| Obj, kEUR | 99.5 |
| CO₂-eq, ton | 588.82 |

### Table 6. Solution of the North Sea route with zero-emission port departure and arrival. ESS stands for electrical energy storage (battery) and OPS for onshore power supply.

|   | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 |
|---|---|---|---|---|---|---|---|---|
| Speed, kn | 0.0 | 9.52 | 0.0 | 0.0 | 0.0 | 18.07 | 18.1 | 9.52 |
| Time, h | 0.0 | 0.57 | 0.0 | 0.0 | 0.0 | 14.42 | 14.49 | 0.57 |
| Power, MW | 0.0 | 2.1 | 0.0 | 0.0 | 0.0 | 14.42 | 14.49 | 2.11 |
| HSFO, MWh | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 819.52 | 175.38 | 0.0 |
| VLSFO, MWh | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 |
| LSMGO, MWh | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 |
| LNG, MWh | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 |
| ESS (−), MWh | 0.0 | 4.88 | 0.0 | 0.0 | 0.0 | 819.52 | 154.75 | 0.0 |
| ESS (+), MWh | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 |
| OPS, MWh | 2.4 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 2.4 |
| EGT-S, MWh | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 819.52 | 154.75 | 0.0 |
| EGT-N, MWh | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 819.52 | 0.0 | 0.0 |
| Obj, kEUR | 104.05 |
| CO₂-eq, ton | 593.47 |

The introduction of 10 km zero-emission port departure and arrival (legs 2 and 8) results in 2.4 MWh capacity battery installation (Table 6). Compared to the baseline case, the optimal sailing speed is only half on the 10 km legs. This speed reduction allows a saving in battery investment cost, but on the other hand, increases the required speed on
the other legs to satisfy the voyage duration upper bound constraint. Remarkably, the total GHG emissions increase, despite the green emission profile of the onshore power supply electricity generation.

5.2. Baltic Sea Routes

The Baltic Sea routes from Helsinki and Turku to Stockholm sail entirely inside ECA. In contrast to the Florø–Nantes route, the baseline least-cost solution is attained by LSMGO fuel instead of HSFO and scrubber (Table 7). The speed on the Stockholm archipelago (Leg 4) follows the limit of 12 knots.

Table 7. Baseline solutions of the Baltic Sea routes.

|            | Helsinki | Turku |
|------------|----------|-------|
| Speed, kn  |          |       |
| 1          | 0.0      | 0.0   |
| 2          | 16.54    | 16.38 |
| 3          | 16.58    | 16.37 |
| 4          | 12.0     | 12.0  |
| Time, h    |          |       |
| 1          | 0.0      | 0.0   |
| 2          | 0.33     | 0.33  |
| 3          | 11.07    | 6.07  |
| 4          | 3.6      | 3.6   |
| Power, MW  |          |       |
| 1          | 0.0      | 0.0   |
| 2          | 11.06    | 10.74 |
| 3          | 11.13    | 10.71 |
| 4          | 4.22     | 4.22  |
| HSFO, MWh  |          |       |
| 1          | 0.0      | 0.0   |
| 2          | 0.0      | 0.0   |
| 3          | 0.0      | 0.0   |
| 4          | 0.0      | 0.0   |
| VLSFO, MWh |          |       |
| 1          | 0.0      | 0.0   |
| 2          | 0.0      | 0.0   |
| 3          | 0.0      | 0.0   |
| 4          | 0.0      | 0.0   |
| LSMGO, MWh |          |       |
| 1          | 0.0      | 0.0   |
| 2          | 4.28     | 4.22  |
| 3          | 146.15   | 77.54 |
| 4          | 22.51    | 22.51 |
| LNG, MWh   |          |       |
| 1          | 0.0      | 0.0   |
| 2          | 0.0      | 0.0   |
| 3          | 0.0      | 0.0   |
| 4          | 0.0      | 0.0   |
| EGT-S, MWh |          |       |
| 1          | 0.0      | 0.0   |
| 2          | 4.29     | 4.22  |
| 3          | 146.15   | 77.54 |
| 4          | 22.51    | 22.51 |
| EGT-N, MWh |          |       |
| 1          | 0.0      | 0.0   |
| 2          | 15.26    | 0.0   |
| 3          | 101.0    | 60.9  |

As previously observed in the North Sea route, the introduction of zero-emission sailing legs gives rise to speed increase in unrestricted legs and speed reduction in battery-powered legs (Table 8). Although speed is reduced by 1.51 kn below the 12 kn speed limit in the Helsinki route and 1.36 in the Turku route, the required battery capacity is still large, exceeding 20 MWh in both routes. The capacity is determined only by the longer Stockholm archipelago zero-emission leg. The energy discharged at the 10 km port departure leg is charged at the next unrestricted leg. Another interesting result is evident from the comparison of the Helsinki and Turku routes. Although the unrestricted open sea leg is almost twice as long when departing from Helsinki compared to Turku, the selected speed and battery capacities are almost the same.

While total propulsion energy (and fuel mass) required for sailing a leg is reduced when speed is reduced, a contrary relationship holds for auxiliary energy. Slowing down increases leg sailing duration, which is multiplied by the constant 2 MW auxiliary power to calculate the total auxiliary energy. Comparing the Stockholm 80 km leg in the baseline and zero-emission Helsinki cases, auxiliary energy is 7.2 MWh in the former, where speed is 12 kn, and 8.24 MWh in the latter, where speed is 10.49 kn. Interpolating this trend further leads to a conclusion that auxiliary energy approaches infinity as speed approaches zero. In more practical terms, a shipowner faces a lower bound for the sailing speed on the zero-emission legs, battery capacity and investment cost when a constant auxiliary power is in effect.

Figure 5 illustrates the propulsion (blue trace), auxiliary (red trace) and the total (black trace) energy demand on the 80 km leg as a function of speed. The speed corresponding to the minimum total energy demand 17.5 MWh is roughly 7.5 kn. The energy demand, in this case, is lower than 20.46 and 20.68 MWh in Table 8. However, the decision to sail at the lower 7.5 kn speed would increase total costs, which is evident from the solution of the optimization problem. Nevertheless, a shipowner may prefer lower battery investment cost and higher fuel cost over the minimum total cost of the optimal choice. This decision is constrained by the 17.5 MWh lower bound of the battery capacity.
Table 8. Solutions of the Baltic Sea routes with zero-emission port arrival and departure.

|           | Helsinki | Turku |
|----------|----------|-------|
|          | 1        | 2     | 3     | 4     | 1    | 2    | 3     | 4     |
| Speed, kn| 0.0      | 17.44 | 17.37 | 10.49 | 0.0  | 17.16| 17.66 | 10.64 |
| Time, h  | 0.0      | 0.31  | 10.57 | 4.12  | 0.0  | 0.31 | 5.62  | 4.06  |
| Power, MW| 0.0      | 12.96 | 12.79 | 2.82  | 0.0  | 12.35| 13.47 | 2.94  |
| HSFO, MWh| 0.0      | 0.0   | 0.0   | 0.0   | 0.0  | 0.0  | 0.0   | 0.0   |
| VLSFO, MWh| 0.0    | 0.0   | 0.0   | 0.0   | 0.0  | 0.0  | 0.0   | 0.0   |
| LSMGO, MWh| 0.0    | 0.0   | 162.13| 0.0   | 0.0  | 0.0  | 92.25 | 0.0   |
| LNG, MWh | 0.0      | 0.0   | 162.13| 0.0   | 0.0  | 0.0  | 92.25 | 0.0   |
| EES (−), MWh| 0.0  | 4.78  | 0.0   | 20.46 | 0.0  | 4.65 | 0.0   | 20.68 |
| EES (+), MWh| 20.46 | 0.0   | 4.78  | 0.0   | 20.68| 0.0  | 4.65  | 0.0   |
| OPS, MWh | 21.09    | 0.0   | 0.0   | 0.0   | 21.32| 0.0  | 0.0   | 0.0   |
| EGT-S, MWh| 0.0    | 0.0   | 0.0   | 0.0   | 0.0  | 0.0  | 0.0   | 0.0   |
| EGT-N, MWh| 0.0    | 0.0   | 162.13| 0.0   | 0.0  | 0.0  | 92.25 | 0.0   |
| Obj, kEUR| 33.51    | 26.83 |       |       | 97.75| 58.27|
| CO₂-eq, ton| 97.75  | 58.27 |       |       | 33.51| 26.83|

Figure 5. Total energy demand on the Stockholm archipelago leg as a function of speed.

6. Conclusions

This paper presented a rigorous algorithmic decision support tool for designing and operating a ship’s energy system with environmental constraints. The problem structure gives rise to nonconvexities from binary variables and bilinear product terms. Thus, the problem is not easy to solve globally. We show that this problem belongs to a class for which non-heuristic algorithms are available. This guarantees convergence to the global optimum and supports interactive use of the tool by providing results nearly instantaneously.

The first applications of the model focused on routing, speed, and NOₓ compliance when sailing on routes with alternative legs inside and outside the ECA area. The original version of this problem, without zero-emission zones, has been addressed in the literature. The works were completed before the IMO 2020 global 0.5% sulfur limit came into force. Heavy fuel oil and ECA compliant low sulfur oil price difference incentivized shipowners to bypass ECAs by sailing a longer route, increasing fuel consumption and emissions. Today, the fuel switching decision is made between 0.1% and 0.5% sulfur fuels. Our results
indicate that the price difference is not significant enough to justify longer routes outside ECA. Thus, we conclude that the ECA routing problem has minimal relevance nowadays.

A shipowner considering transitory battery-powered zero-emission sailing needs to evaluate the trade-off between battery investment cost and fuel cost. Namely, reducing speed in a zero-emission leg translates to lower battery capacity (and cost) but higher speed (and fuel cost) outside the zero-emission area, given that the total voyage duration is the same. The optimal trade-off is achieved by large, even 50% speed reduction in zero-emission areas. Moreover, the zero-emission legs are typically located in archipelagos, fjords, and narrow shipping lanes that enforce a 10–12 knot speed limit. In all cases studied in this work, the optimal speed is lower than the limit.

A zero-emission area can have a negative impact on total voyage GHG emissions. A shipowner, who aims to minimize total costs, benefits from reducing speed in battery-powered legs, trading off battery investment cost to fuel cost. This increases speed, energy consumption, fuel use, and emissions when sailing outside the zero-emission areas. The result is in line with previous work with respect to trading off between local NO\textsubscript{x} and total GHG emissions by propulsion power source switching [30]. Nevertheless, the improvement in local air quality may justify the increase in total emissions.

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**Abbreviations**
The following abbreviations are used in this manuscript:

| Abbreviation | Description                              |
|--------------|------------------------------------------|
| CII          | Carbon Intensity Indicator               |
| ECA          | Emission Control Area                    |
| EEDI         | Energy Efficiency Design Index           |
| EES          | Electrical Energy Storage                |
| EEXI         | Energy Efficiency Design Index for Existing Ships |
| EGT          | Exhaust Gas Treatment                    |
| GHG          | Greenhouse Gas                           |
| HSFO         | High Sulfur Fuel Oil                     |
| IFO          | Intermediate Fuel Oil                    |
| LSMGO        | Low Sulfur Marine Gas Oil                |
| LNG          | Liquefied Natural Gas                    |
| MS           | Medium Speed                             |
| NMC          | Nickel Manganese Cobalt                  |
| OPS          | Onshore Power Supply                     |
| SCR          | Selective Catalytic Reduction            |
| SFOC         | Specific Fuel Oil Consumption            |
| VLSFO        | Very Low Sulfur Fuel Oil                 |

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