Comparison of Carbonic Anhydrases for CO\textsubscript{2} Sequestration

Franziska Steger\textsuperscript{1,*}, Johanna Reich\textsuperscript{1,2}, Werner Fuchs\textsuperscript{1}, Simon K.-M. R. Rittmann\textsuperscript{3}, Georg M. Gübitz\textsuperscript{1}, Doris Ribitsch\textsuperscript{2,3,*} and Günther Bochmann\textsuperscript{1,*}

Abstract: Strategies for depleting carbon dioxide (CO\textsubscript{2}) from flue gases are urgently needed and carbonic anhydrases (CAs) can contribute to solving this problem. They catalyze the hydration of CO\textsubscript{2} in aqueous solutions and therefore capture the CO\textsubscript{2}. However, the harsh conditions due to varying process temperatures are limiting factors for the application of enzymes. The current study aims to examine four recombinantly produced CAs from different organisms, namely CAs from Acetobacterium woodii (AwCA or CynT), Persephonella marina (PmCA), Methanobacterium thermoautotrophicum (MtaCA or Cab) and Sulphuriphilus hydrogenibium (SspCA). The highest expression yields and activities were found for AwCA (1814 WAU mg\textsuperscript{-1} AwCA) and PmCA (1748 WAU mg\textsuperscript{-1} PmCA). AwCA was highly stable in a mesophilic temperature range, whereas PmCA proved to be exceptionally thermostable. Our results indicate the potential to utilize CAs from anaerobic microorganisms to develop CO\textsubscript{2} sequestration applications.

Keywords: carbonic anhydrase; CO\textsubscript{2} sequestration; thermostability; activity assay; recombinant expression

1. Introduction

Due to the rapid growth of the world economy, there is a continual escalation in its carbon intensity. Carbon dioxide (CO\textsubscript{2}) emissions are rapidly increasing, making CO\textsubscript{2} the most abundant greenhouse gas emitted by human activities [1–3]. Reducing the CO\textsubscript{2} content in the atmosphere is imperative in meeting the UNFCCC climate goal of limiting the global temperature increase below 2 °C above pre-industrial levels [4]. Strategies for capturing CO\textsubscript{2} from flue gases are essential, until the ultimate goal of transition from non-renewable energy sources, such as natural gas and coal, to renewable energy sources is reached. Currently, there are various technologies and advances for capturing CO\textsubscript{2} from flue gas, including chemical absorption of CO\textsubscript{2} by solvents [5–7]. Through this method, a great fraction of CO\textsubscript{2} can be depleted from the flue gas by passing it through a solvent, such as monoethanolamine (MEA), where CO\textsubscript{2} molecules are extracted [8]. In the second step, the solvent is regenerated, and pure CO\textsubscript{2} is released. A significant detrimental effect when utilizing MEA is the side generation of toxic wastes and aerosols [8,9]. Another disadvantage is the high amount of energy required for the release of CO\textsubscript{2} from the solvent at high temperatures up to 120 °C [10], leaving CO\textsubscript{2} capture with MEA unfavorable from an economic and sustainable standpoint [11].

An alternative is the “biomimetic” approach to capture CO\textsubscript{2}. Enzymes, such as carbonic anhydrases (CAs), accelerate the hydration of CO\textsubscript{2}, consequently facilitating the application of energy-efficient but kinetically-limited aqueous solvents, such as salt solutions (e.g., CaCl\textsubscript{2}, KOH) [8,12]. Biomimetic CO\textsubscript{2} capture has previously been described,
studied and implemented as a more sustainable and more economic option [12–14]. The temperature needed to release pure CO$_2$ from aqueous salt solutions can be significantly reduced to 80 $^\circ$C or less in biomimetic applications due to the decreased binding of CO$_2$ compared to MEA solutions [15,16]. An existing critical challenge is to maintain the stability of the enzymes during varying temperatures from 30 $^\circ$C to 80 $^\circ$C in the process [15,17].

CAs are mainly zinc-containing metalloenzymes [18] and hydrate CO$_2$ to hydrogen carbonate (HCO$_3^-$) according to the following two-step mechanism [19,20]:

\[
\begin{align*}
EZnOH^- + CO_2 &\leftrightarrow EZn(OH^-)CO_2 \leftrightarrow EZnHCO_3^- \leftrightarrow EZnH_2O + HCO_3^- \\
EZnH_2O &\leftrightarrow H^+EZnOH^- + B \leftrightarrow EZnOH^- + BH^+
\end{align*}
\]

CAs are ubiquitously found in prokaryotes as well as in eukaryotes. There are eight distinct classes of carbonic anhydrases (α, β, γ, δ, ζ, η, θ, ι), which vary in their roles in different crucial physiological processes, amino acid sequences and 3-D tertiary structures [18,21]. CAs from extremophiles, existing at high temperatures, are a specific focus of interest, because they have been proven to be particularly active and thermostable [12,22]. The following three CAs from thermophilic organisms were selected based on literature research: PmCA originates from the bacterium *Persephonella marina* EX-H1, which exists in the deep-sea in an environment with excessive temperatures up to 133 $^\circ$C and high pressures. Under laboratory conditions, *P. marina* grows in temperatures up to 80 $^\circ$C [23]. SspCA is an enzyme from the bacterial strain *Sulphurihydrogenibium yellowstonense* YOSAOP1, which occurs in hot springs with a growth optimum at 70 $^\circ$C and can grow autotrophically with CO$_2$. PmCA and SspCA are α-type CAs and have been studied intensely with existing patents that have been published for their uses in biomimetic CO$_2$ capture applications [24–28]. Both enzymes have been demonstrated to have high hydratase activities and to be exceptionally thermostable [24,29,30]. MtaCA, also referred to as Cab in the literature, was selected to extend the study with a β-type, thermostable CA [31], originating from the extreme thermophilic archaeon *Methanobacterium thermoautotrophicum*, which grows at up to 75 $^\circ$C and metabolizes CO$_2$ to methane [32]. The fourth CA selected for this study was AwCA, also referred to as CynT in the literature. It originates from the bacterium *Acetobacterium woodii* DSM 1030 with a growth optimum at 30 $^\circ$C [33]. According to the NCBI’s Conserved Domain Database (CDD), AwCA belongs to the β-type class [34]. Despite AwCA originating from a mesophilic organism, it was selected due to its stated exceptional activity [35].

The recombinant expression of genes was the pivotal breakthrough allowing for the mass production of enzymes paving the way towards the industrial implementation of enzymes [36]. The current study aimed to examine these four recombinantly produced CAs from different organisms for biomimetic CO$_2$ sequestration. Firstly, expression yields were determined using a single expression strategy in *Escherichia coli*. The effect of the CA addition on CO$_2$ hydration at different temperatures was explored by applying the three CAs with the highest expression yields. A novel straightforward assay for the determination of CA activity was applied in this study, where measurement occurs close to industrial process conditions and temperatures [37]. The new assay allowed the characterization of CAs at temperatures exceeding 0 $^\circ$C, which is unique concerning the commonly used Wilbur Anderson assay [38]. In the end, the thermostability of the two best performing CAs was compared, under the given conditions.

2. Results

2.1. Selection, Expression and Purification

Four CAs were selected for comparison regarding their ability to convert CO$_2$ into HCO$_3^-$, namely CAs from *Acetobacterium woodii* (AwCA), *Persephonella marina* (PmCA), *Methanobacterium thermoautotrophicum* (MtaCA) and *Sulphurihydrogenibium yellowstonense* (SspCA). The selected CAs belong to different types of CAs and share only low homologies among each other, as shown in the phylogenetic tree built on published CA protein
sequences (Figure 1). PmCA and SspCA have been identified as α-type CAs originating from Gram-negative organisms. The two CAs share 45% homology and thus the highest similarity among the selected protein sequences. AwCA and MtaCA, however, are β-type CAs derived from Gram-positive organisms or archaea, respectively, and share only 20% homology among each other. Homologies between α-CAs and β-CAs are below 15%.

![Figure 1. Phylogenetic tree of α-type and β-type CAs.](image)

Both α- and β-CAs are metalloenzymes, which use Zn(II) ions for chemical catalysis. Despite their shared CO$_2$ hydratase activity, the two classes demonstrate major structural differences, which are also seen in alignments of CAs investigated in this study (Supplementary Materials Section S3). The Zinc ion, for instance, is tetrahedrally coordinated by three histidines in α-CAs but by one histidine and two cysteines in β-CAs. A water molecule or hydroxide ion acts as a fourth ligand and nucleophile in the catalytic reaction in both CA classes. Similarly to all other α-CAs described in literature, the three histidines are present in PmCA (His89, His90, His108) and SspCA (His99, His101 and His118), which are relatively close to each other in the protein sequence. Additionally, a highly conserved histidine (His74 in PmCA and His64 in SspCA) is presently proposed to act as the proton shuttle. AwCA and MtaCA, however, are displaying the Zn(II) coordinating histidine (His110 and His87, respectively) and cysteines (Cys57 and Cys113 in AwCA, Cys32 and Cys90 in MtaCA) in their protein sequences, as expected for β-CAs. Besides, AwCA displays the highly conserved DSRV motif (residues 59–62) and Gln48, which are...
proposed to be involved in the catalytic reaction. Interestingly, Val62 is exchanged for Leu36 in this motif in MtaCA (residues 33–36) and also, Gln is not present at the corresponding amino acid position.

The protein sequences of PmCA and SspCA exhibit natural N-terminal signal peptides, comprising amino acids 1–19 in PmCA and 1-20 in SspCA, which were removed for the production of recombinant proteins in \textit{E. coli}. Removal of the signal peptides of PmCA and SspCA was previously described as a tool to enhance expression yields [25,29,30]. The influence of the removal on hydratase activity was not evaluated during this study. Unlike the CAs mentioned above, AwCA and MtaCA do not reveal natural signal sequences. According to the analysis of the protein sequences, evidence for transmembrane domains or membrane anchors was not found in either of the applied CAs. According to Capasso and Supuran (2015), bacterial \(\alpha\)-CAs are localized in the periplasmic compartment of Gram-negative bacteria. Contrastingly, bacterial \(\beta\)-CAs are mainly localized in the cytoplasm [40]. The alignment of sequences without signal peptides but fused to the StrepTag, as expressed in this study, can be found in the Supplementary Materials Section S3.

All CA encoding genes (Supplementary Materials Section S4) were codon optimized for expression in \textit{E. coli} and fused to a C-terminal StrepTag, except for SspCA, which carried an N-terminal StrepTag. The synthetic genes were cloned into pET-vectors and expressed in \textit{E. coli} BL21-Gold (DE3) at 37 °C. An SDS-PAGE analysis of samples withdrawn from \textit{E. coli} liquid cultures at several time points (Supplementary Materials Figures S2, S5, S8 and S11) revealed high production levels of soluble protein at the expected molecular masses for AwCA (22.0 kDa), MtaCA (19.9 kDa) and PmCA (26.9 kDa), but only low production of SspCA (27.5 kDa). All CAs formed inclusion bodies, as determined by the SDS-PAGE analysis of insoluble cell fractions.

Purification of CAs from cleared \textit{E. coli} cell lysates was achieved by a single step affinity chromatography through the StrepTag. Fractions containing the CAs were pooled and analyzed by SDS-PAGE (Figure 2). For SspCA, a double protein band on the SDS PAGE of cleared cell lysate and purified enzyme indicated a proteolysis on the N-terminal end during expression. The second protein band of cleared cell lysate and purified enzyme of AwCA in Figure 2 is attributed to the unspecific binding of \textit{E. coli} proteins, whereas the second protein band in Supplementary Materials Figure S4 (elution fraction, line 7) is attributed to the formation of dimers of AwCA, which were not separated due to overloading of the SDS gel. AwCA belongs to the \(\beta\)-class, which is known to form dimers, tetramers and octamers [41], while \(\alpha\)-CAs are usually monomers [40].

Typically, 25 mg AwCA, 15 mg PmCA, 18 mg MtaCA and 0.6 mg SspCA were obtained from 100 mL \textit{E. coli} liquid culture according to the calculation based on purified enzymes. The yields are thus significantly higher than those from the literature, based on 100 mL liquid culture, which are 4.8 mg for AwCA when produced in \textit{A. woodii} [35], and 0.129 mg or 0.93 mg of PmCA after production with and without signal peptide, respectively, in \textit{E. coli} [29]. Around 10 mg MtaCA were obtained from diluted \textit{E. coli} cell paste in 20 mL buffer [31]. In the study of Capasso et al. (2012), 12 mg SspCA were produced from an unknown volume of \textit{E. coli} liquid culture using the expression vector pET15-b. Hence, the production of SspCA may be optimized in future studies.

SspCA was excluded from the following experiments after a change of an initial C-terminal StrepTag (not shown) to the N-terminal StrepTag resulted in similarly low expression yields. A further investigation to find the optimal expression system for SspCA was not conducted due to the fact that three out of four CAs demonstrated high expression yields under the chosen conditions. An optimization of the expression and vector system for SspCA may be conducted in future studies to assess the expression yields of SspCA.
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Figure 2. SDS-PAGE of CAs produced in E. coli. Samples of cleared cell lysate and after purification by affinity chromatography. Expected molecular masses are 22.0 kDa (AwCA), 26.9 kDa (PmCA), 19.9 kDa (MtCA) and 27.5 kDa (SspCA).

2.2. Effect of CAs on CO$_2$ Hydration at Different Temperatures

The effect on CO$_2$ hydration at different temperatures (25 °C, 30 °C, 40 °C and 50 °C) was investigated for AwCA, PmCA and MtaCA. Figure 3 displays the pH courses over time when 0.1 mol L$^{-1}$ Tris-sulfate buffer was sparged with CO$_2$ at different temperatures. At each temperature, the blank without CA showed the slowest decrease in pH compared to the measurements where CAs were added. When CO$_2$ is introduced into aqueous solutions it partly forms carbonic acid, which almost completely deprotonates into HCO$_3^-$ + H$, which causes a pH drop. CAs catalyze the direct conversion of CO$_2$ to HCO$_3^-$ + H$^+$ and vice versa [18]. Therefore, at a surplus of CO$_2$, the more active the CA is, the faster the pH drops. The difference between the blank and CAs was most obvious at 25 °C to 40 °C, demonstrating that all enzymes had an accelerating effect on CO$_2$ hydration in this temperature range. However, it is noticeable that the effect of MtaCA was constantly minor compared to PmCA and AwCA.

The advantage of the method used in this study is that the measurement is conducted at relevant temperatures of industrial processes (25–50 °C), in contrast to the widely used Wilbur Anderson assay, which is conducted solely at 0 °C [38]. Hence, the effect of CAs at temperatures close to process conditions can be investigated. Comparing the four diagrams (Figure 3), it is visible that with temperature elevation the equilibrium pH is rising because the solubility of CO$_2$ is decreasing [42]. The starting pH at 40 °C and 50 °C was also lower being close to 8.0. The buffer stock solution (500 mL) was only preheated at the respective temperature before pH adjustment. For future measurements, it is recommended to keep the buffer stock solution in a temperature-controlled vessel during pH adjustment to avoid temperature-dependent pH shifts.

As illustrated in Figure 3, at higher temperatures the course of the blank becomes steeper and more similar to the curves in which CAs were added. At higher temperatures, the uncatalyzed formation of HCO$_3^-$ + H$^+$ is faster than at lower temperatures. Whereas in total, less CO$_2$ is solubilized, leading to a lower substrate concentration. At 50 °C, only a minor difference between the measurements with and without CAs can be observed. Another
potential reason might be that the CAs are eventually less active at elevated temperatures. In this publication, the activity was calculated at 25 °C (Section 2.3). Calculation of activities at 30 °C, 40 °C and 50 °C was not performed. However, it might be unlikely that CAs that originate from thermophilic organisms (PmCA and MtaCA) lose their activity at 50 °C. As visualized in Figure 3, the effect of CA addition to CO2 capture at higher temperatures (>40 °C) is marginal and therefore not advisable. Fradette et al. (2017) reported that the absorption of CO2 takes place at 30–40 °C, while the desorption is conducted at 80 °C [15]. Hence, when CAs are recirculated together with the solvent, the thermostability of CAs is of higher interest than their activity at temperatures exceeding 40 °C.

![Figure 3](image_url)

**Figure 3.** Time-dependent course of pH when 0.1 mol L\(^{-1}\) Tris-sulfate buffer was sparged with 100% CO2 (200 mL min\(^{-1}\)) at different measurement temperatures: (a) 25 °C; (b) 30 °C; (c) 40 °C; (d) 50 °C. Without enzyme (black, solid line), with 0.25 mg L\(^{-1}\) AwCA (blue, dashed line), with 0.25 mg L\(^{-1}\) PmCA (red, dotted line), with 0.25 mg L\(^{-1}\) MtaCA (orange, dashed-dotted line). \(n = 3\).

The results for PmCA and MtaCA are in accordance with the literature where both enzymes are described to be thermophilic [29,31]. In prior studies, however, hydratase activity was only investigated at 0 °C (PmCA) [24,29,43] or room temperature (MtaCA) [31] utilizing the Wilbur Anderson assay [38] or an undescribed modification thereof [44], respectively. AwCA has not yet been described to be active at high temperatures. In contrast to PmCA and MtaCA [23,32], AwCA originates from a mesophilic organism [35], leading to the assumption that AwCA is only active at moderate temperatures around 30 °C. The results shown in Figure 3, however, indicate that AwCA has an accelerating effect on CO2 hydration at temperatures up to at least 40 °C. Notably, the enzymes were kept on ice before the measurements, so the effect at different temperatures cannot prove the thermostability of the enzymes for more than a few minutes; incidentally, this was the time one measurement required. The thermostability over a longer period was determined in the following experiments, which will be described in Section 2.4.
2.3. Calculated Hydratase Activities at 25 °C

To evaluate the different hydratase activities at 25 °C in commonly used units, turnover rate per mg enzyme and WAU per mg enzyme were calculated for AwCA, MtaCA and PmCA (Table 1). When comparing WAU per mg enzyme, it becomes visible that AwCA (1814 WAU mg⁻¹) and PmCA (1748 WAU mg⁻¹) were about three times more active than MtaCA (580 WAU mg⁻¹). High hydratase activities are essential for the success of CO₂ capturing applications. MtaCA was excluded from further investigations because of its lower measured and reported hydratase activities compared to AwCA and PmCA [31].

**Table 1.** Calculated hydratase activities at 25 °C for AwCA, MtaCA and PmCA in turnover rate per mg enzyme and WAU per mg enzyme.

| Enzyme | Total Turnover Rate in µmol s⁻¹ L⁻¹ | Turnover Rate Minus Blank in µmol s⁻¹ L⁻¹ | Turnover Rate per mg Enzyme in µmol s⁻¹ mg⁻¹ | WAU per mg Enzyme |
|--------|----------------------------------|------------------------------------------|------------------------------------------|--------------------|
| Blank  | 793 ± 16                         | 0                                        | n. a.                                    | n. a.              |
| AwCA   | 1502 ± 45                        | 710 ± 48                                 | 2839 ± 97                                | 1814 ± 228         |
| MtaCA  | 1204 ± 32                        | 411 ± 36                                 | 1646 ± 73                                | 580 ± 102          |
| PmCA   | 1490 ± 13                        | 698 ± 21                                 | 2790 ± 42                                | 1748 ± 63          |

2.4. Thermostability of AwCA and PmCA

Thermostability is a crucial factor for the implementation of CAs in CO₂ capture applications [15,17]. In Figure 4, residual hydratase activities after incubation at different temperatures over 24 h to 144 h are shown. The corresponding calculated activities can be found in Supplementary Materials Table S1. The Figure 4a shows the results for AwCA and the Figure 4b shows the results for PmCA. When AwCA was incubated at 30 °C for 144 h, 89 ± 10% of residual activity was retained. Incubation at 40 °C decreased residual activity to 59 ± 11% within 144 h. At 50 °C and 60 °C, residual activity drastically decreased to 4 ± 6% and −7 ± 7% after 144 h and 48 h of incubation, respectively. However, it is notable that AwCA retained 42 ± 11% residual after incubation at 60 °C for 24 h. Incubation at higher temperatures was not performed for AwCA due to the low stability at 60 °C compared to 30 °C and 40 °C (Figure 4). In contrast, PmCA turned out to be exceptionally thermostable, retaining 91 ± 19% residual activity after incubation at 70 °C for 144 h and 90 ± 14% residual activity after 96 h at 80 °C. When incubation time at 80 °C was prolonged to 144 h, PmCA still retained 52 ± 19% residual activity.

**Figure 4.** Residual hydratase activity over incubation time at different temperatures compared to unincubated enzyme for (a) AwCA at 30 °C, 40 °C and 50 °C; (b) PmCA at 50 °C, 60 °C, 70 °C, 80 °C. n = 3.
The thermostability of AwCA was tested in this study for the first time and therefore cannot be compared to the data in the literature. Regarding PmCA, the literature confirmed that this type of CA is fully active after incubation at 80 °C for 2 h [24]. Jo et al., 2014, tested the long-term stability of PmCA at 40 °C and 60 °C for 60 days, where PmCA retained 57% and 27% residual activity, respectively [43]. The current study further elucidates the insights on thermostability of PmCA, illustrating that significant amounts of activity were retained at 30 °C to 80 °C for up to 6 days (144 h). In summary, AwCA was stable long-term in a mesophilic temperature range and only short-term at temperatures exceeding 40 °C. In contrast, PmCA proved to be stable long-term at temperatures up to 80 °C.

3. Discussion

Thus far, α- and β-class CAs have been purified from various species [40,45]. Functional prokaryotic CAs have the advantage of being easily produced in E. coli, as in the cases of, e.g., β-class Caut-bCA from Clostridium autoethanogenum [46] and α-class HC-aCA from Hahella chejuensis. For the latter, expression yields (24.5 mg per 100 mL liquid culture) were similarly high as in the current study [47]. Contrastingly, bacterial α-class BhCA and β-class BCA were obtained from cell extracts of Bacillus halodurans and Bacillus subtilis SA3 cultures, respectively [48,49]. α-CA (Dca) from the green algae Dunaliella salina was functionally expressed in E. coli to a total amount of 15 mg. The culture volume was not given, but 1 g of wet E. coli cell pellet was reported to yield 1 mg of CA [50]. Marine species, such as mussels, diatoms and sea urchin exhibit functional CAs, which were mainly designated to the α-class [51–54]. In the literature, primarily their esterase activity rather than their hydratase activity was determined. CA of the marine diatom Thalassiosira pseudonana was successfully expressed in E. coli [53]. Expression yields were not reported. CAs from higher plants were mainly expressed in the original species for characterization, and hydratase activities were not reported [55,56]. For CO₂ capture, prominent α-CAs from other eukaryotes were human hCAII, which was produced using bacterial vectors [13], and BovCAII, which was simply purified from bovine erythrocytes [57].

α- and β-class CAs differ in their structures, also demonstrated by the low homologies between the selected α- and β-CAs. Generally, the catalytic site of α-CAs was reported to be larger compared to β-CAs, thus resulting in higher hydratase activities [40]. When comparing the α- and β-CAs mentioned above, reported hydratase activities of α-class BhCA (3425 WAU mg⁻¹) [48] and BovCAII (1749 WAU mg⁻¹) [57] were higher compared to β-class BCA (1140 WAU mg⁻¹) [49]. Accordingly, hydratase activities of α-class SspCA and hCAII were described to be amongst the highest with 7254 WAU mg⁻¹ and 8000 WAU mg⁻¹, respectively, in the literature [30,58]. However, there are exceptions, such as α-class HC-aCA (478 WAU mg⁻¹) [47], Dca (400 WAU mg⁻¹) [50] and CA from T. pseudonana (266 ± 49 WAU mg⁻¹) [53], which exhibit comparably low hydratase activities. Although exhibiting very high hydratase activities (e.g., hCAII), the major drawback of eukaryotic α-CAs is that they are typically not thermostable [26].

In the current study, β-class AwCA (1814 WAU mg⁻¹) demonstrated similarly high hydratase activity as the α-class PmCA (1748 WAU mg⁻¹), whereas hydratase activity of the β-class MtaCA (580 WAU mg⁻¹) was significantly lower. When comparing the protein structures, AwCA exhibited the typical features of β-CAs, whereas MtaCA varied by an exchanged Val62 for Leu36 in the highly conserved DSRV motif and missed Gln48. Both original amino acids are proposed to be involved in the catalytic reaction, potentially explaining the lower hydratase activity of MtaCA compared to AwCA. The highly conserved regions of α-CAs were found both in PmCA and SspCA. The lower hydratase activity of MtaCA compared to AwCA and PmCA during this study was in accordance with literature [31].

Kim et al. (2019) proposed that the enhanced thermostability of PmCA likely derives from the compactly folded homodimeric structure of α-CAs, which is stabilized by hydrophobic interactions, intramolecular disulfide bonds and interfacial networks of hydrogen bonds [59]. The current results confirm the exceptional thermostability of α-class
PmCA compared to the mesophilic β-class AwCA. An exception might be the β-class MtaCA, which originates from a thermophilic organism and has been described to be stable after incubation for 15 min at up to 75 °C [31]; this is potentially explained by the closer relation to α-CAs in the phylogenetic tree (Figure 1). In the literature, SspCA was described as α-CA with one of the highest long-term thermostabilities while retaining its CO₂ hydration activity after incubation at 100 °C for 3 h and 10% residual activity after incubation at 70 °C for 28 days [26,60]. However, due to the significantly lower expression yield of SspCA at the chosen conditions, the thermostability of SspCA was not evaluated in this study.

Consistently, CAs from thermophilic prokaryotes were already presented as the favorable candidates for biotechnological applications due to their enhanced thermostability in the literature, whereas CAs from other species are yet to be improved by protein engineering [12]. Immobilization may be an option to improve the thermostability of AwCA in future studies [61]. Production of SspCA may be increased significantly by using other expression vectors, as reported by Capasso et al. (2012) [30].

4. Materials and Methods

4.1. Chemicals and Reagents

All chemicals used in this work were of analytical grade. IPTG, ZnSO₄, kanamycin, biotin and the buffer components were purchased from Sigma–Aldrich (St. Louis, MO, USA). Ampicillin and Nutrient Agar were purchased from Merck Millipore (Darmstadt, Germany). SDS buffer and the SDS-PAGE gels were purchased from Bio-Rad (Hercules, CA, USA). LB media was purchased from Carl Roth (Karlsruhe, Germany) and the protein marker for SDS PAGE from VWR International (Radnor, PA, USA). Bottled CO₂ (purity 99.5%) was derived from Messer (Bad Soden, Germany).

4.2. Cloning, Expression and Purification

Genes coding for AwCA (accession number WP_014354989), PmCA (WP_015898908), MtaCA (AAB86055) and SspCA (ACD66216.1) were codon optimized and cloned over NdeI and HindIII restriction sites fused to a StrepTag for rapid purification by affinity chromatography. In the case of SspCA and MtaCA, the natural signal peptides were removed before cloning. Synthesis of genes and cloning into the expression vectors were provided by a commercial service (GenScript Biotech, Leiden, The Netherlands). Genes encoding AwCA, PmCA and MtaCA were cloned into vector pET26b(+) carrying a C-terminal StrepTag and the gene coding for SspCA into vector pET16b(+) providing a N-terminal StrepTag. The plasmids were transformed into E. coli BL21-Gold (DE3) (Agilent Technologies, Santa Clara, CA, USA). Freshly transformed E. coli cells were used to inoculate 20 mL LB-medium supplemented with 0.5 mmol L⁻¹ ZnSO₄ and 40 mg mL⁻¹ Kanamycin for pET26b(+) or 100 µg mL⁻¹. Ampicillin for pET16b(+) and cultivated overnight at 37 °C and 150 rpm. The overnight culture was used to inoculate 200 mL of the same medium in a 500 mL shake flask to an OD600 = 0.1. The culture was incubated at 37 °C and 150 rpm until an OD600 = 0.8 was reached. At this point, cells were induced by addition of IPTG to a final concentration of 0.1 mmol L⁻¹ and incubated at 20 °C for 20 h (AwCA and PmCA) or 22 h (MtaCA and SspCA). Cultures were harvested by centrifugation at 4000 rpm and 4 °C for 30 min.

Enzymes were purified by affinity chromatography according to the manufacturer’s protocol (IBA GmbH, Goettingen, Göttingen, Germany). The elution fractions were collected, pooled and concentrated by vivaspin 20 columns (Sartorius, Germany). The buffer was exchanged by PD-10 desalting columns (GE Healthcare, Buckinghamshire, UK) with 0.1 mol L⁻¹ Tris-HCl at a pH of 7. Enzymes were aliquoted to 500 µL and frozen at 20 °C until further usage.
4.3. CO$_2$ Hydration Assay at Different Temperatures

Investigation of the effect of the CA addition on CO$_2$ hydration at different temperatures was made by monitoring the pH change in buffered solution due to the formation of carbonic acid using the method as described by Fuchs et al., 2021 [37]. The reactions were conducted in a temperature-controlled vessel and the temperature was varied between 25–50 °C. Frozen enzyme stock solutions were thawed, diluted to 0.1 mg mL$^{-1}$ with 0.1 mol L$^{-1}$ Tris-HCl (pH 7) and kept on ice until the measurement. The reaction mix contained 40 mL reaction buffer (0.1 mol L$^{-1}$ Tris-sulfate, pH 8.2) and 0.1 mL of the respective enzyme stock solution. The purified enzyme concentration in the reaction mix was 0.25 mg L$^{-1}$, as determined by NanoPhotometer® (NP80, IMPLEN, Westlake Village, CA, USA). For blank measurements, only the reaction buffer was measured. The pH of the reaction buffer was set to 8.2 at the respective measurement temperature before the experiments. CO$_2$ gassing was started and the decline of pH during the experiment due to CO$_2$ entry was recorded (Methrom Titrino, pH electrode: LL-Viscotrode and Software TiNet 2.5). Each measurement with or without CA was performed as a triplicate, and in the figures the mean values are shown.

4.4. Calculation of Hydratase Activities at 25 °C

Hydratase activities at 25 °C were calculated using the logged pH data. HCO$_3^-$ (mol L$^{-1}$) was calculated according to the formula provided by Fuchs et al., 2021 [37]. Subsequently, HCO$_3^-$ was converted to µmol L$^{-1}$ and depicted against time in a diagram. The slope of the graph between 7–18 s was taken as µmol CO$_2$ converted to µmol HCO$_3^-$ L$^{-1}$ s$^{-1}$. The total turnover rate (µmol HCO$_3^-$ L$^{-1}$ s$^{-1}$) of the blank measurement was subtracted from the measurements with CAs before the calculation of the turnover rate per mg enzyme (µmol HCO$_3^-$ s$^{-1}$ mg$^{-1}$). To give the values in generally used units, a calibration curve with a standard enzyme (CA from bovine erythrocytes, Sigma–Aldrich, Taufkirchen, Germany) was used for conversion to Wilbur Anderson Units (WAU), as in Fuchs et al., 2021 [37].

4.5. Determination of Thermostability

Determination of thermostability was conducted using the same set-up as in Section 4.3. The measuring temperature was 25 °C. CA stock solutions were diluted to 0.1 mg mL$^{-1}$ with 0.1 mol L$^{-1}$ Tris-HCl at a pH of 7. Prior to the tests, aliquots of 1 mL were incubated at 30 °C, 40 °C, 50 °C, 60 °C, 70 °C or 80 °C in a heating block (Thermomixer comfort, Eppendorf, Hamburg, Germany) for up to 144 h. Prior to the CO$_2$ hydration assay, the samples were cooled down to RT. For the calculation of the residual activity, the turnover rate per mg enzyme (µmol s$^{-1}$ mg$^{-1}$) was used.

5. Summary and Conclusions

Four CAs from different organisms were recombinantly produced in E. coli. Considering a later industrial application, the production and purification of the CAs were easy to perform and provided high yields using standard procedures. Under the chosen conditions, the expression yields of AwCA, PmCA and MtaCA were at least 25 times higher than for SspCA. Hence, SspCA was excluded from further experiments during this study. Nevertheless, a variation of the expression strategy for SspCA can potentially maximize the expression yield and should be part of future studies, as SspCA was reported to be one of the most active and thermostable CAs characterized so far in the literature.

A comparison of the effect on CO$_2$ hydration at different temperatures, similar to industrial conditions, was performed for AwCA, PmCA and MtaCA using a novel assay. An accelerating effect on CO$_2$ hydration was observed at 25 °C, 30 °C, 40 °C and up to 50 °C when enzymes were added to the buffer. However, there was only a minor difference between the CAs and the blank measurement at 50 °C, leading to the conclusion that the CA addition to CO$_2$ capture at temperatures exceeding 40 °C is inapplicable. At 25 °C, hydratase activities were calculated for evaluation in general units. AwCA (1814 WAU mg$^{-1}$) and PmCA (1748 WAU mg$^{-1}$) were about three times more active
than MtaCA (580 WAU mg\(^{-1}\)), which led to the exclusion of MtaCA for the following thermostability experiments. AwCA was highly stable in a mesophilic temperature range with residual activities of 89 ± 10% and 59 ± 11% after incubation at 30 °C and 40 °C, respectively, for 144 h. PmCA was discovered to be exceptionally thermostable with residual activities of 91 ± 19% and 90 ± 14% after incubation at 70 °C for 144 h and at 80 °C for 96 h, respectively. The results of this study indicate that AwCA and PmCA might be suitable candidates for biomimetic CO\(_2\) sequestration at either mesophilic (AwCA and PmCA) or thermophilic (PmCA) temperature ranges. Further investigation of CAs from other species, especially those from thermophilic, anaerobic prokaryotes, is endorsed for broadening the range of possible candidates for CO\(_2\) sequestration.

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