Phase-Separating Binary Polymer Mixtures: The Degeneracy of the Virial Coefficients and Their Extraction from Phase Diagrams

Arjen Bot, Belinda P. C. Dewi, and Paul Venema*

ABSTRACT: The Edmond–Ogston model for phase separation in binary polymer mixtures is based on a truncated virial expansion of the Helmholtz free energy up to the second-order terms in the concentration of the polymers. The second virial coefficients ($B_{11}$, $B_{12}$, $B_{22}$) are the three parameters of the model. Analytical solutions are presented for the critical point and the spinodal in terms of molar concentrations. The calculation of the binodal is simplified by splitting the problem into a part that can be solved analytically and a (two-dimensional) problem that generally needs to be solved numerically, except in some specific cases. The slope of the tie-lines is identified as a suitable parameter that can be varied between two well-defined limits (close to and far away from the critical point) to perform the numerical part of the calculation systematically.

INTRODUCTION

Phase separation of a binary mixture of polymers in a common solvent into two liquid phases is a well-established phenomenon and is discussed in many recent and older reviews. It is a topic of both fundamental interest and practical importance, with applications in diverse fields like polymer physics, cell biology, and food technology. Particularly, when phase separation is incomplete on a macroscopic scale (also known as microphase separation), phase-separated polymer mixtures show properties that the individual polymers do not possess, for example, large deformation and rupture properties in gelled phase-separated systems.

The simplest theoretical descriptions of phase separation in polymer mixtures are the Flory–Huggins and the Edmond–Ogston models. Such models are useful because they are the minimal models necessary to capture all of the essential physics and properties of phase separation with reasonable accuracy. Clark showed that both models are equivalent up to the second order of the expansion in the concentrations. The present paper focuses on the Edmond–Ogston model rather than on the Flory–Huggins model because the former has a slightly more straightforward basis in thermodynamics, is not formulated on a lattice, and can in principle be readily extended to higher-order terms in concentration.

The Edmond–Ogston model is based on a truncated virial expansion of the Helmholtz free energy up to the second-order terms in the concentration of the polymers and is therefore sometimes referred to as the virial model. The use of the Helmholtz free energy implies that the demixing of the mixed polymer solution does not cause a change in the total volume of the system, which is reasonable as the typical system under consideration consists mostly of solvent. The three parameters in the model, describing the pair interactions between the polymers, are the so-called virial coefficients ($B_{11}$, $B_{12}$, $B_{22}$). In principle, the virial coefficients can be obtained experimentally from, e.g., membrane osmometry, static light scattering, or analytical ultracentrifugation. It is noted that these measurements are often experimentally challenging for reasons depending on the specific technique used.

Also, the small number of parameters involved raises the hope of being able to generate a database of virial coefficients that allow for a fair (if not fully quantitative) prediction of the phase behavior for a wide range of binary polymer mixtures. Such a database could be generated by extracting the virial coefficients from experimental data. This requires a thorough understanding of the mathematical structure of these models. However, some gaps exist within this area that need to be filled. The database does not require the highest level of accuracy but needs to be sufficiently precise to guide a
researcher evaluating a large number of potential biopolymer combinations.

In a recent paper, a number of new results were obtained for the Edmond—Ogston model (analytical expressions for the critical point and for the binodal in the “symmetrical” case, where $B_{11} = B_{22}$). It was shown that provided one of the virial coefficients is known, the other two virial coefficients can be determined from either (1) the location of the critical point or (2) the composition of a pair of co-existing phases. If none of the virial coefficients is known, an infinite number of solutions for the triplets of virial coefficients ($B_{11}, B_{12}, B_{22}$) is found. It is shown here that this stems from a degeneracy in the mathematical formulation of the problem, where all of the triplets derived from the specific properties (1) or (2) above are located on lines in $(B_{11}, B_{12}, B_{22})$-space or $B$-space. These lines in $B$-space intersect at a single point, corresponding to the actual set of virial coefficients. It is noted that given the equivalence of Edmond—Ogston and Flory—Huggins models, this degeneracy is also essentially present in the latter model.

The properties of the phase diagram are described by a set of nonlinear algebraic equations that are, even numerically, not trivial to solve. It turns out that progress can be made by parametrization of the governing equations by introducing the slope of the tie-lines (i.e., the lines connecting the co-existing phases located on the binodal in the phase diagram) as a new parameter. By introducing this parameter, a symmetry property of the equations is revealed, thereby simplifying the original problem to basically a two-dimensional problem. We have chosen to sketch the main line of thought in the main text and have given the mathematical details of the derivations in the Appendices I–X.

## RESULTS AND DISCUSSION

**Characteristics of the Phase Diagram.** The overall phase diagram of a binary polymer mixture in a common solvent displays a number of key features (see Figure 1). The binodal indicates the border between the stable and metastable regions, whereas the spinodal separates the metastable and unstable regions in the diagram. Binodal and spinodal share a common tangent at the critical point, which is the only point where the stable region directly borders the unstable region. In the metastable region, phase separation takes place via a nucleation and growth mechanism and only proceeds when concentration fluctuations are large enough to overcome the free energy barrier that hinders phase separation. In the unstable region, phase separation takes place spontaneously by a process called spinodal decomposition, when concentration fluctuations increase unhindered because no free energy barrier exists. In the stable region, no phase separation occurs. A polymer mixture formulated to be in either the metastable or unstable region ultimately separates in a pair of distinct co-existing phases, which can be displayed in the phase diagram as being connected through a so-called tie-line. Any mixture formulated along the same tie-line ends up with compositionally identical pairs of co-existing phases, the difference being their relative volumes that can be derived from the so-called lever rule. Furthermore, all mixtures formulated along the same tie-line have identical osmotic pressure because all of these separate in the same pair of co-existing phases (albeit at different relative volumes) that have the same osmotic pressure. A more detailed explanation on the calculation of the critical point, spinodal, binodal, tie-lines, and phase volumes is given below. In a previous study, we have derived several characteristics of the phase diagram in dimensionless concentration units. In the next sections, these results are extended and given in terms of molar concentrations, allowing for a more direct comparison with experimental phase diagrams. Molar concentrations were chosen because this allows for virial coefficients, osmotic pressure, and chemical potential to be expressed in familiar units as well.

**Governing Equations.** In the present model, the Helmholtz free energy $F(J)$ of the mixture reads

$$F = RT \left[ n_1 \ln \left( \frac{n_1}{V} \right) + n_2 \ln \left( \frac{n_2}{V} \right) + \frac{n_1^2 B_{11}}{V} + \frac{2n_1 n_2 B_{12}}{V} + \frac{n_2^2 B_{22}}{V} \right]$$

where $R$ is the gas constant ($1 \text{ K}^{-1} \text{ mol}^{-1}$), $T$ is the absolute temperature ($\text{K}$), $V$ is the total volume of the system ($\text{m}^3$), $n_1$ and $n_2$ are the number of moles ($\text{mol}$) of polymers 1 and 2, respectively, $B_{11}$ is the second virial coefficient of polymer 1 ($\text{m}^3 \text{ mol}^{-1}$), $B_{22}$ is the second virial coefficient of polymer 2 ($\text{m}^3 \text{ mol}^{-1}$), and $B_{12}$ is the second cross-virial coefficient between polymer 1 and polymer 2 ($\text{m}^3 \text{ mol}^{-1}$). Only situations where all virial coefficients are positive are considered. Although only the terms up to the second order in the concentration are taken into account, this simple model still captures all essentials of phase separation with fair accuracy. The above expression for the Helmholtz energy leads to a set of co-existence equations that are the same as derived earlier by Edmond and Ogston. If higher accuracy is required, this model can be straightforwardly extended to include higher-order concentration terms in a consistent way. For the Flory—Huggins model, such an extension is not obvious as binary interaction parameters already show up in the higher-order

![Figure 1. Typical phase diagram for a polymer mixture for $(B_{11}, B_{12}, B_{22}) = (1, 3, 4)$ (m$^3$/mol). The binodal (red solid line) separates the stable region (below the binodal) from the metastable and unstable regions. The unstable region can be found above the spinodal (blue dashed line). The binodal and spinodal intersect at the critical point (solid circle), where they share a common tangent. The tie-lines (dashed-dotted line) connect the co-existing phases located on the binodal.](https://dx.doi.org/10.1021/acsomega.1c00450)
concentration terms, and the Maxwell relation does not seem to be fulfilled (see Appendix I). It is noted that the higher-order virial coefficients are difficult to be determined experimentally because they reflect the effects of interactions between three polymer particles for the third order, between four for the fourth order, etc. The contribution of such higher-order interactions is usually small, especially in the dilute-to-semidilute regime, making an extension to higher-order concentration terms to be of limited practical value.

The second virial coefficient $B_i$ is defined by

$$B_i = 2\pi N_a \int_0^\infty (1 - e^{-\omega_i(r)/k_B T}) r^2 dr$$

(2)

where $N_a$ is Avogadro’s number ($6.02 \times 10^{23}$ mol$^{-1}$), $\omega_i(r)$ is the potential of mean force as a function of the distance $r$ between segments of polymer $i$ and polymer $j$, $k_B$ is Boltzmann’s constant ($1.38 \times 10^{-23}$ J/K), and $T$ (K) is the absolute temperature. In eq 2, it is, without loss of generality, assumed that the force is isotropic.

Using the thermodynamic relation for the osmotic pressure $\Pi$, the following expression is obtained

$$\frac{\Pi}{RT} = -\frac{1}{RT} \left[ \frac{\partial F}{\partial n_i} \right]_{n_{i},v}$$

$$= c_i + c_2 + B_{11} c_1^2 + B_{22} c_2^2 + 2B_{12} c_1 c_2$$

(3)

where $c_i = n_i/V$ is the molar concentration of polymer $i$ (mol m$^{-3}$) with $i = 1, 2$ for polymers 1 and 2. This is a hyperbola with asymptotes $c_2 - c_1$, $-(B_{11}/B_{22})(\sqrt{B_{11} B_{22}}/(\sqrt{B_{11} B_{22}} \pm 1))(c_1 - c_2)$, where $c_{1,2} = (1/2)(B_{22} - B_{12})(B_{11} B_{22})/B_{22}^2$ and $c_{2,1} = (1/2)(B_{11} - B_{12})(B_{11} B_{22})/B_{11}^2$.

The chemical potentials $\mu_i$ (with $i = 1, 2$) relative to the standard chemical potentials are given by

$$\frac{\mu_1}{RT} = \frac{1}{RT} \left[ \frac{\partial F}{\partial n_1} \right]_{n_2,V} = \ln c_1 + B_{11} c_1 + 2B_{12} c_1 + 1$$

(4)

$$\frac{\mu_2}{RT} = \frac{1}{RT} \left[ \frac{\partial F}{\partial n_2} \right]_{n_1,V} = \ln c_2 + 2B_{22} c_2 + 2B_{12} c_1 + 1$$

(5)

It is noted that eqs 4 and 5 satisfy the Maxwell relation, confirming that the Helmholtz free energy $F$ is a state variable

$$\left( \frac{\partial}{\partial n_1} \left( \frac{\mu_1}{RT} \right) \right)_{T,n_2} = \left( \frac{\partial}{\partial n_2} \left( \frac{\mu_2}{RT} \right) \right)_{T,n_1} = \frac{2}{V} B_{12}$$

(6)

When the system separates into two phases, I and II, the following co-existence equations hold

$$\Pi^I = \Pi^II$$

(7)

$$\mu_1^I = \mu_1^II$$

(8)

$$\mu_2^I = \mu_2^II$$

(9)

Alternatively, eq 7 can be formulated in terms of the chemical potential $\mu_i$ and the partial molar volume $\nu_i$ of the solvent using the thermodynamic identity

$$\mu_i = -\nu_i \Pi$$

(10)

It is noted that the Gibbs phase rule for binary mixtures (see Appendix II) in principle allows for a three-phase equilibrium without any degrees of freedom left and therefore corresponds to a fixed composition of the three co-existing phases. This situation is not taken into consideration.

From the conservation of mass for both polymers, two additional equations are found that correspond to the so-called lever rule

$$\gamma c_1^I + (1 - \gamma) c_1^II = c_1$$

(11)

and

$$\gamma c_2^I + (1 - \gamma) c_2^II = c_2$$

(12)

where $c_1^I$ and $c_2^II$ denote the molar concentrations of polymer $i$ in phases I and II, respectively, and $c_i$ still reflects the total concentrations of polymer $i$ (with $i = 1, 2$). Here, $\gamma$ is defined as

$$\gamma = \frac{V^I}{V^I + V^II}$$

(13)

where $V^I$ is the volume of phase I and $V^II$ is the volume of phase II.

Equations 11 and 12 correspond to the lever rule

$$V^I = \frac{L_2}{L_1 + L_2} V^T; \quad V^II = \frac{L_1}{L_1 + L_2} V^T$$

(14)

where $V^T$ is the total volume after phase separation. $L_1$ and $L_2$ are the line segment lengths on the tie-line on which the polymer mixture $(c_1, c_2)$ would be located without phase separation (cf. Figure 1). From eqs 7–9 and 3–5, the following co-existence equations are found from which the co-existing phases can be calculated

$$c_1^I + c_2^I + B_{11} c_1^I + B_{22} c_2^I + 2B_{12} c_1 c_2$$

(15)

$$= c_1^II + c_2^II + B_{11} c_1^II + B_{22} c_2^II + 2B_{12} c_1^I c_2^I$$

$$\ln c_1^I + 2B_{11} c_1^I + 2B_{12} c_2^I = \ln c_1^II + 2B_{11} c_1^II + 2B_{12} c_2^II$$

(16)

$$\ln c_2^I + 2B_{22} c_2^I + 2B_{12} c_2^I = \ln c_2^II + 2B_{22} c_2^II + 2B_{12} c_2^II$$

(17)

The criterion for phase separation is given by

$$\frac{B_{12}}{B_{11} B_{22}} > 1$$

(18)

This set of equations (eqs 15–17) is invariant under the transformation

$$(B_{11}, B_{22}, c_1^I, c_2^I, c_1^II, c_2^II)$$

$$\rightarrow \left( k B_{11}, kB_{22}, k B_{12} c_1^I/k c_1^II, k c_2^I/k c_2^II \right)$$

(19)

where $k$ is a constant, and to interpret the physical meaning of this invariance, the special case of a hard-sphere dispersion can be considered. The volume fraction $\phi_i$ of a hard-sphere dispersion equals $B_{11} c_i^I/4$. This implies that eqs 7–9 can be written completely in terms of volume fractions, making the phase behavior of hard-sphere mixtures length-scale-independent. In the general case, the physical meaning of the invariance is less obvious but still holds mathematically. This consideration was also the reason for introducing reduced variables (e.g., $x = \frac{B_{12} c_1}{k} = 2B_{11} c_1$ and $\alpha = \frac{k B_{11}}{k B_{22}} = \frac{k c_2}{k c_1}$) in the previous...
study.\textsuperscript{31} It is noted that within the Flory–Huggins theory, the governing equations are usually formulated in terms of volume fractions.

**Critical Point.** There are different expressions available relating the molar concentrations of the critical point ($c_{1c}$, $c_{2c}$) to the virial coefficients. By means of stability analysis,\textsuperscript{38} the critical point was previously found to be a solution of a third-order polynomial in terms of $\sqrt{S_c}$ (either eq A.8 or eq 40 in Dewi et al.\textsuperscript{31})

$$B_{22}\sqrt{S_c}^3 + B_{12}\sqrt{S_c}^2 - B_{12}\sqrt{S_c} - B_{11} = 0 \quad (20)$$

or

$$B_{11}\frac{1}{\sqrt{S_c}} + B_{12}\frac{1}{\sqrt{S_c}^2} - B_{12}\frac{1}{\sqrt{S_c}} - B_{22} = 0 \quad (21)$$

These two expressions are equivalent and can easily be converted into each other by division by a factor $-\sqrt{S_c}^3$. It is also noted that the substitution $(B_{11}, B_{12}, B_{22}, S_c) \rightarrow (B_{22}, B_{12}, B_{11}, 1/S_c)$ transforms eq 20 into eq 21 and vice versa. Here, $-S_c$ corresponds to the slope of the binodal and spinodal at the critical point (in molar concentration units), which is given by

$$S_c = \left(\frac{3\frac{b_{11}}{b_{12}}}{2\sqrt{1 + 3\frac{b_{11}}{b_{12}}\cos(\theta) - 1}}\right)^2 \quad (22)$$

with

$$\theta = \frac{1}{3}\cos^{-1}\left(\frac{1}{2}\left[\frac{27}{2}\frac{b_{11}}{b_{12}} + 1 - 3\left(1 + \frac{3\frac{b_{11}}{b_{12}}}{3}ight)^3\right] \right) \quad (23)$$

(Note that to simplify the notation, the accent for the slope in molar coordinates was dropped in the present paper. Therefore, the quantity referred to as $-S_c$ in the present paper is the same as $S_c$ in the previous work.\textsuperscript{31,32})

Explicit expressions were derived for the coordinates of the critical point (eqs 47 and 48 in Dewi et al.\textsuperscript{31}), which read in molar concentration units

$$c_{1c} = \frac{B_{22} + \frac{b_{12}}{b_{11}}}{2(B_{12} - B_{11}B_{22})} = \frac{1}{2(B_{12}S_c - B_{11})} \quad (24)$$

$$c_{2c} = \frac{B_{11} + \frac{B_{12}}{\sqrt{S_c}}}{2(B_{12}^2 - B_{11}B_{22})} = \frac{1}{2\left(\frac{b_{12}}{S_c} - B_{22}\right)} \quad (25)$$

The equivalence of the second and third terms in eqs 24 and 25 is demonstrated in Appendix III and requires the use of eq 20 or 21. The expressions in the third terms in eqs 24 and 25 are the most convenient ones to be used when working in molar concentrations.

The invariance of eqs 15–17 under multiplication of the virial coefficient $B_i$ by the same factor $k$ (cf. eq 19) further implies that the slope $-S_c$ at the critical point remains the same under this transformation. However, the critical point, binodal, and spinodal shift simultaneously by a factor $1/k$ closer to the origin (cf. Figure 2). The explicit expressions for the critical point, eqs 24 and 25, can also be used to verify the useful relation given in the work of Edmond and Ogston (eq 5a,b in Edmond and Ogston\textsuperscript{28}), which reads in the present notation

$$\frac{1}{c_{1c}} + 2B_{11} = 2B_{12}\left(\frac{c_{2c}}{c_{1c}}\right)^{2/3} \quad (26)$$

$$\frac{1}{c_{2c}} + 2B_{22} = 2B_{12}\left(\frac{c_{1c}}{c_{2c}}\right)^{2/3} \quad (27)$$

In Appendix IV, it is demonstrated that these equations are equivalent to eq 20 or 21. Since the critical point ($c_{1c}$, $c_{2c}$) is determined from two equations containing three virial coefficients ($B_{11}$, $B_{12}$, $B_{22}$), it follows that for every critical point there is an infinite number of solutions for the virial coefficients triplets ($B_{11}$, $B_{12}$, $B_{22}$) that correspond with this critical point. Therefore, to uniquely determine the virial coefficients from just the location of the critical point, at least one of the virial coefficients should be known.\textsuperscript{31} Suppose that triplet $(B_{11}, B_{12}, B_{22})$ gives the same critical point as triplet $(B_{11}^*, B_{12}^*, B_{22}^*)$, they have to satisfy the relation

$$(B_{12} - B_{12}^*) = \frac{1}{S_c}(B_{11} - B_{11}^*) = S_c(B_{22} - B_{22}^*) \quad (28)$$

as a consequence of eqs 24 and 25. This corresponds to a line in "virial coefficient space" or $B$-space that can be written in vector notation as

$$\left(\begin{array}{c} B_{11}^* \\ B_{12}^* \\ B_{22}^* \end{array}\right) = \left(\begin{array}{c} B_{11} \\ B_{12} \\ B_{22} \end{array}\right) + \lambda \left(\begin{array}{c} S_c \\ \frac{1}{S_c} \\ \frac{1}{S_c} \end{array}\right) \quad (29)$$
with $\lambda_i$ being any real number, while ensuring that $\frac{c_{i,sp}^{11}}{B_6} > 1$
and that all $B_i$’s are larger than zero. A support vector $\begin{pmatrix} B_{11} \\ B_{12} \\ B_{22} \end{pmatrix}$ can
be found by choosing an arbitrary real value for $B_{11}$ (i.e., $B_{11} = 1$) from which $B_{12}$ and $B_{22}$ can be calculated from eqs 24 and
25 or 26 and 27. All triplets $(B_{11}^*, B_{12}^*, B_{22}^*)$ lead to the same critical point with the slope $-S_m$ at the critical point, as is
demonstrated in Appendix V. Note that for this to be a critical point as well, the new virial coefficients also have to satisfy the criterion with the third-order polynomial for the critical point (cf. eq 20).

\[
B_{22}^* \sqrt{S_c}^3 + B_{12}^* \sqrt{S_c}^2 - B_{12}^* \sqrt{S_c} - B_{11}^* = 0
\]  
(30)

which is also proven in Appendix V.

**Spinodal.** The condition for the spinodal $(c_{1,sp}, c_{2,sp})$ is given by (see, e.g., Ersch et al.\(^{30}\) or Dewi et al.\(^{11}\))

\[
4(B_{12}^2 - B_{11}B_{22})c_{1,sp}c_{2,sp} - 2B_{11}c_{1,sp} - 2B_{22}c_{2,sp} - 1 = 0
\]  
(31)

or

\[
c_{2,sp} = \frac{2B_{11}c_{1,sp} + 1}{4(B_{12}^2 - B_{11}B_{22})c_{1,sp} - 2B_{22}}
\]  
(32)

Thereafter, every point on the spinodal can be written in the following form

\[
(c_{1,sp}, c_{2,sp}) = \frac{\left(\frac{B_{22} + B_{12}}{S_{op}} \ln \frac{B_{22} + B_{12}}{S_{op}}\right) - B_{11} + B_{12}\sqrt{S_{op}}}{2(B_{12}^2 - B_{11}B_{22})c_{1,sp} - 2B_{22}}
\]  
(33)

where $-S_m$ is the tangent to the spinodal in this point and $S_{op}$ ranges from $\infty$ to 0, as can be demonstrated by substituting eq 33 in eq 31. Now, it is easy to determine the asymptotes of the spinodal. For $c_{1,sp} \rightarrow \frac{B_{11}}{2(B_{12}^2 - B_{11}B_{22})}$, the absolute value of the slope of the spinodal behaves as $S_{op} \rightarrow \infty$ and $c_{2,sp} \rightarrow \infty$. For $c_{2,sp} \rightarrow \frac{B_{22}}{2(B_{12}^2 - B_{11}B_{22})}$, the absolute value of the slope of the spinodal behaves as $S_{op} \rightarrow 0$ and $c_{1,sp} \rightarrow \infty$. Note that due to the phase separation criterion in eq 18, the asymptotes for phase-separating mixtures are always found at positive (and physically relevant) concentrations $c_{1,sp}$ and $c_{2,sp}$.

**Tie-Lines.** Suppose that the molar composition of two co-existing phases $(c_1^1, c_2^1)$ and $(c_1^2, c_2^2)$ are known. These values can be substituted in eqs 15–17, and a set of three linear equations in the three virial coefficients are obtained as

\[
(c_1^1 - c_1^{11}) + (c_2^1 - c_2^{11}) + B_{11}(c_1^1 - c_1^{11}) + B_{22}(c_2^1 - c_2^{11})
\]

\[
+ 2B_{12}(c_1^1 - c_1^{11})(c_2^1 - c_2^{11})
\]

\[
= 0
\]  
(34)

\[
(ln c_1^1 - ln c_1^{11}) + B_{11}(c_1^1 - c_1^{11}) + 2B_{12}(c_2^1 - c_2^{11})
\]

\[
= 0
\]  
(35)

\[
(ln c_1^1 - ln c_2^{11}) + 2B_{22}(c_2^1 - c_2^{11}) + B_{12}(c_1^1 - c_1^{11})
\]

\[
= 0
\]  
(36)

When the virial coefficients are considered as the variables, the determinant of these sets of equations equals zero (cf. eq 104 in Dewi et al.\(^{11}\), leading to the conclusion that there is not a unique solution but an infinite number of solutions for the virial coefficients $(B_{11}, B_{12}, B_{22})$. The condition for having an infinite number of solutions is expressed by the condition

\[
(c_1^1 - c_1^{11}) + (c_2^1 - c_2^{11})
\]

\[
= \frac{1}{2}(c_1^1 + c_1^{11}) \ln \frac{c_1^1}{c_1^1} + \frac{1}{2}(c_2^1 + c_2^{11}) \ln \frac{c_2^1}{c_2^1}
\]  
(37)

Interestingly, this equation does not contain the virial coefficients explicitly and provides an excellent check on the accuracy of the experimental or numerical determination of the composition of the co-existing phases, since it holds for all co-existence phases. The set of virial coefficients $(B_{11}, B_{12}, B_{22})$ can be obtained from eqs 35 and 36, when one of the virial coefficients is known.

If phase separation takes place, eqs 34–36 can be used to determine the composition of the co-existing phases. In a previous study, it was shown that the composition of the co-existing phases could be determined numerically using the method of steepest descent.\(^{31}\) Here, it is shown that the structure of the equations for the co-existing phases becomes clearer by introducing the slope of the tie-lines explicitly. As a first step, corresponding to the requirement of equal osmotic pressure for the co-existing phases, eq 34 is written as

\[
(B_{11}(c_1^1 + c_1^{11}) + B_{12}(c_2^1 + c_2^{11} + 1))(c_1^1 - c_1^{11})
\]

\[
+ (B_{11}(c_1^1 + c_1^{11}) + B_{22}(c_2^1 + c_2^{11}) + 1)(c_2^1 - c_2^{11})
\]

\[
= 0
\]  
(38)

The slope of the tie-lines $-S_m$ is given by

\[
-S_m \equiv \frac{c_2^1 - c_2^{11}}{c_1^1 - c_1^{11}} = \frac{B_{11}(c_1^1 + c_1^{11}) + B_{12}(c_1^1 + c_1^{11}) + 1}{B_{12}(c_1^1 + c_1^{11}) + B_{22}(c_2^1 + c_2^{11}) + 1}
\]  
(39)

where the tie-lines connect the co-existing phases $(c_1^1, c_2^1)$ and $(c_1^2, c_2^2)$. The last term in eq 39 follows directly from eq 38. (Note that $S_m$ is defined here in terms of molar units and is the same as the parameter $S_m$ used in Dewi et al.\(^{11}\).) By introducing $(c_{1,m}, c_{2,m})$ as the midpoint of the tie-line by

\[
c_{1,m} = \frac{(c_1^1 + c_1^{11})}{2} \text{ and } c_{2,m} = \frac{(c_1^1 + c_1^{11})}{2}
\]  
(40)

equation 39 can be rewritten as

\[
-S_m = \frac{2B_{11}c_{1,m} + 2B_{22}c_{2,m} + 1}{2B_{12}c_{1,m} + 2B_{22}c_{2,m} + 1}
\]  
(41)

After introducing the variables $(c_{1,s}, c_{2,s})$ as

\[
c_{1,s} \equiv \frac{1}{2(B_{12}S_m - B_{11})} \text{ and } c_{2,s} \equiv \frac{1}{2(B_{12}S_m - B_{22})}
\]  
(42)

equations 41–42 can be combined, and the following relation is obtained

\[
\left(\frac{c_{2,m}}{c_{2,s}} - 1\right) = \frac{1}{S_m} \left(\frac{c_{1,m}}{c_{1,s}} - 1\right)
\]  
(43)
This can be written, using eq 40 and reframing from a formulation in terms of midpoints of the tie-lines again, as

$$\frac{c_1^{II}}{c_{2,s}} - 1 + \frac{c_1^{I}}{c_{2,s}} - 1 = \frac{1}{S_m} \left( \frac{c_1^{I}}{c_{1,s}} - 1 + \frac{c_1^{II}}{c_{1,s}} - 1 \right)$$  (44)

Also, the definition in eq 39

$$-S_m \equiv \frac{c_1^{I} - c_1^{II}}{c_1^{I} - c_1^{II}}$$  (45)

can be rearranged as

$$\frac{c_1^{II}}{c_{2,s}} - 1 - \frac{c_1^{I}}{c_{2,s}} + 1 = \frac{1}{S_m} \left( \frac{c_1^{I}}{c_{1,s}} - 1 - \frac{c_1^{II}}{c_{1,s}} + 1 \right)$$  (46)

The expression for eqs 44 and 46 can be combined using matrix notation as

$$\begin{pmatrix} \frac{c_1^{II}}{c_{2,s}} - 1 + \frac{c_1^{I}}{c_{2,s}} - 1 \\ \frac{c_1^{II}}{c_{2,s}} - 1 - \frac{c_1^{I}}{c_{2,s}} + 1 \end{pmatrix} = \begin{pmatrix} \frac{1}{S_m} & 0 \\ 0 & \frac{1}{S_m} \end{pmatrix} \begin{pmatrix} \frac{c_1^{I}}{c_{1,s}} - 1 + \frac{c_1^{II}}{c_{1,s}} - 1 \\ \frac{c_1^{I}}{c_{1,s}} - 1 - \frac{c_1^{II}}{c_{1,s}} + 1 \end{pmatrix}$$  (47)

By adding and subtracting the rows in eq 47, the above matrix equation can be rearranged in the form

$$\frac{c_1^{II}}{c_{2,s}} - 1 = \left( \frac{1}{2} \frac{1}{S_m} + \frac{c_1^{II}}{c_{2,s}} \right) \left( \frac{1}{2} \frac{1}{S_m} + \frac{c_1^{I}}{c_{2,s}} \right) - \frac{c_1^{I}}{c_{2,s}} - 1$$

$$\frac{c_1^{II}}{c_{2,s}} - 1 = \left( \frac{1}{2} \frac{1}{S_m} - \frac{c_1^{II}}{c_{2,s}} \right) \left( \frac{1}{2} \frac{1}{S_m} - \frac{c_1^{I}}{c_{2,s}} \right) - \frac{c_1^{I}}{c_{2,s}} - 1$$

Introducing the parameter $S_m$ may seem like a step back, since it adds a fourth equation to the co-existence eqs 15–17. However, the expressions for $(c_{1,s} c_{2,s})$, eq 42, can be used to rewrite eqs 16 and 17 in a solvable form (see Appendix VI)

$$\ln \frac{c_1^{II}}{c_{1,s}} - \ln \frac{c_1^{I}}{c_{1,s}} = \ln \frac{c_1^{II}}{c_{2,s}} - \ln \frac{c_1^{II}}{c_{2,s}}$$  (49)

$$\ln \frac{c_1^{II}}{c_{2,s}} - \ln \frac{c_1^{I}}{c_{2,s}} = \ln \frac{c_1^{II}}{c_{2,s}} - \ln \frac{c_1^{II}}{c_{2,s}}$$  (50)

As a result, the original three co-existence eqs 15–17 are now replaced by four equations (eqs 49–50). The solutions of eqs 49–50 can be expressed in terms of the so-called Lambert-W function, previously already invoked to solve the symmetrical case where $B_{11} = B_{22}$, as

$$\begin{pmatrix} \frac{c_1^{II}}{c_{1,s}} \\ \frac{c_1^{II}}{c_{2,s}} \end{pmatrix} \begin{pmatrix} -W_{-1}(-\frac{c_1^{II}}{c_{1,s}} e^{-\frac{c_1^{II}}{c_{1,s}}}) \\ -W_{-1}(-\frac{c_1^{II}}{c_{2,s}} e^{-\frac{c_1^{II}}{c_{2,s}}}) \end{pmatrix} = -W_{-1}(-\frac{c_1^{II}}{c_{2,s}} e^{-\frac{c_1^{II}}{c_{2,s}}})$$

$$\begin{pmatrix} \frac{c_1^{II}}{c_{1,s}} \\ \frac{c_1^{II}}{c_{2,s}} \end{pmatrix} \begin{pmatrix} -W_{-1}(-\frac{c_1^{II}}{c_{1,s}} e^{-\frac{c_1^{II}}{c_{1,s}}}) \\ -W_{-1}(-\frac{c_1^{II}}{c_{2,s}} e^{-\frac{c_1^{II}}{c_{2,s}}}) \end{pmatrix} = -W_{-1}(-\frac{c_1^{II}}{c_{2,s}} e^{-\frac{c_1^{II}}{c_{2,s}}})$$  (51)

where, for the remainder of this paper, the (arbitrary) convention is used that the “lower right” phase with $c_1^{I} > c_{1,s}$ and $c_2^{I} < c_{2,s}$ is labeled I and the “upper left” phase with $c_1^{I} < c_{1,s}$ and $c_2^{I} > c_{2,s}$ is labeled II, in line with Figure 1. This convention can be used because the co-existing phases $(c_1^{I}, c_2^{I})$ and $(c_1^{II}, c_2^{II})$ should always be in diagonally opposite quadrants relative to the point $(c_{1,s}, c_{2,s})$. Substitution of eq 51 in eq 48 leads to

$$\begin{pmatrix} -W_{-1}(-\frac{c_1^{II}}{c_{1,s}} e^{-\frac{c_1^{II}}{c_{1,s}}}) - 1 \\ -W_{-1}(-\frac{c_1^{II}}{c_{2,s}} e^{-\frac{c_1^{II}}{c_{2,s}}}) - 1 \end{pmatrix} = \begin{pmatrix} \frac{1}{2} \frac{1}{S_m} + \frac{c_1^{II}}{c_{2,s}} \frac{1}{2} \frac{1}{S_m} - \frac{c_1^{II}}{c_{2,s}} \\ \frac{1}{2} \frac{1}{S_m} - \frac{c_1^{II}}{c_{2,s}} \frac{1}{2} \frac{1}{S_m} + \frac{c_1^{II}}{c_{2,s}} \end{pmatrix}$$

$$\begin{pmatrix} -W_{-1}(-\frac{c_1^{II}}{c_{1,s}} e^{-\frac{c_1^{II}}{c_{1,s}}}) - 1 \\ -W_{-1}(-\frac{c_1^{II}}{c_{2,s}} e^{-\frac{c_1^{II}}{c_{2,s}}}) - 1 \end{pmatrix}$$  (52)

Equation 37 becomes in this notation

$$\begin{pmatrix} 2 + \left( -W_{-1}(-\frac{c_1^{II}}{c_{1,s}} e^{-\frac{c_1^{II}}{c_{1,s}}}) - W_{0}(-\frac{c_1^{II}}{c_{1,s}} e^{-\frac{c_1^{II}}{c_{1,s}}}) \right) \\ -W_{-1}(-\frac{c_1^{II}}{c_{1,s}} e^{-\frac{c_1^{II}}{c_{1,s}}}) + W_{0}(-\frac{c_1^{II}}{c_{1,s}} e^{-\frac{c_1^{II}}{c_{1,s}}}) \end{pmatrix}$$

$$\begin{pmatrix} \ln \left( -W_{-1}(-\frac{c_1^{II}}{c_{2,s}} e^{-\frac{c_1^{II}}{c_{2,s}}}) \right) \\ -W_{-1}(-\frac{c_1^{II}}{c_{2,s}} e^{-\frac{c_1^{II}}{c_{2,s}}}) \end{pmatrix}$$  (53)

Progress has been made by parametrization of the problem, where the original four-variable problem $(c_1^{I}, c_2^{I}, c_1^{II}, c_2^{II})$ has been effectively reduced to a two-variable problem $(c_1^{I}, c_2^{I})$ in eq 52), where $S_m$ acts as a parameter that has to be chosen in the interval $[S_{m0} S_{m∞}]$ or $[S_{m∞} S_{m0}]$, depending on whether $S$, or $S_{m0}$, is smaller. Here, $S_{m0}$ is the absolute value of the slope of the tie-line in molar units far away from the critical point, as demonstrated in the Appendix VII section (cf. eq 115 in Dewi et al.15)

$$S_{m0} = \frac{B_{11}}{B_{22}}$$  (54)
Once \((c_1, c_2)\) is determined for a certain \(S_{\infty}\) the values for \((c_1^\|, c_2^\|)\) can be determined analytically from eq 51. Note that in the symmetrical case, where \(S_m = 1\) for all tie-lines, the solution is given directly in Dewi et al.\(^{31}\). Care has to be taken that the correct branch of the Lambert-W function is chosen, \(W_{-1}\) or \(W_{0}\), as indicated in eqs 51 and 52. In addition, the parametrization of the problem reveals the symmetry properties of the equations that are hidden in the initial co-existence equations. These symmetry properties allow us to find explicit solutions for specific cases, but these expressions in eq 52 still have to be solved numerically in the general case to find the properties of the phase diagram. It should also be emphasized that eq 52 is invariant under the transformation \((c_1^1, c_2^1, S_m) \leftrightarrow (c_2^1, c_1^1, 1/S_m)\). Table 1 summarizes the values for \((c_{1,\infty}, c_{2,\infty})\) in three well-defined limits of \(S_{\infty}\). Note that the matrix in eq 52 simplifies in the symmetrical case, where \(B_{11} = B_{22} = B, S_{m} = 1\), and \(c_{1,\infty} = c_{2,\infty} = c_{2,\infty} = \frac{1}{2(B_0 - B)}\), and eq 48 reduces to

\[
\begin{bmatrix}
\frac{1}{c_2^{\|}} - 1 \\
c_{2,\infty} - 1
\end{bmatrix}
= 
\begin{bmatrix}
1 & 0 \\
0 & 1
\end{bmatrix}
\begin{bmatrix}
\frac{1}{c_1^{\|}} - 1 \\
c_{1,\infty} - 1
\end{bmatrix}
\]

leading to diagonalization of the matrix

\[
\begin{aligned}
c_2^{\|} &= c_1^{\|} \\
c_2 &= c_1
\end{aligned}
\]

Substitution of eq 56 in eqs 49–50 leads to the analytical result for the binodal that was previously reported for the symmetrical case as\(^{31}\)

\[
\frac{c_{2,\infty}}{c_{2,\infty}} = -W_{-1} \left( \frac{c_{1,\infty}}{c_{1,\infty}} \right) e^{-c_{1,\infty}/c_{1,\infty}} \quad \text{for} \quad c_{1,\infty} \leq c_{1,\infty}
\]

and

\[
\frac{c_{2,\infty}}{c_{2,\infty}} = -W_{0} \left( \frac{c_{1,\infty}}{c_{1,\infty}} \right) e^{-c_{1,\infty}} \quad \text{for} \quad c_{1,\infty} \geq c_{1,\infty}
\]

where \((c_{1,\infty}, c_{2,\infty})\) represent the coordinates of the binodal.

Although other formal limits exist in which the matrix in eq 52 diagonalizes as

\[
\begin{bmatrix}
\frac{1}{c_2^{\|}} - 1 \\
\frac{1}{c_1^{\|}} - 1
\end{bmatrix}
= 
\begin{bmatrix}
\frac{1}{S_{\infty}} & 0 \\
0 & \frac{1}{S_{\infty}}
\end{bmatrix}
\begin{bmatrix}
\frac{1}{c_1^{\|}} - 1 \\
\frac{1}{c_1^{\|}} - 1
\end{bmatrix}
\]

when \(c_1\) and/or \(c_2 \to \infty\), or when \(B_{12} \to \infty\) for a fixed critical point, both limits are unphysical in the sense that they describe situations in which the total equivalent hard-sphere volume fraction \(\varphi = (B_{11}c_1 + B_{22}c_2)/4\) is vastly larger than \(O(1)\). Since the maximum packing for hard spheres is about 0.7, depending on the details, it is reasonable to expect that \((B_{11}c_1 + B_{22}c_2)/4\) should not exceed a value of \(O(1)\) by many orders in other cases. Therefore, the cases for these formal limits are not addressed here, except for a short note on the behavior of the slope of the tie-lines in one of these limits in the next section.

**Degeneracy in the Virial Coefficients for the Critical Point.** Consider two sets of virial coefficients that give rise to the same critical point, \((B_{11}, B_{12}, B_{22})\) and \((B_{11}^*, B_{12}^*, B_{22}^*)\). Using eq 28, an expression for \(S_{\infty}\) can be obtained

\[
S_{\infty} = \frac{B_{11}}{B_{22}} \frac{B_{12}^*}{B_{22}^*} - \frac{B_{11} B_{22}^*}{B_{22}^* + B_{12}^* B_{22}}
\]

and

\[
S_{\infty}^* = \frac{B_{11}^*}{B_{22}^*}
\]

When \(B_{12} \neq B_{12}^*\), it follows that \(S_{\infty} \neq S_{\infty}^*\), which means that the tie-lines far away from the critical point are generally not parallel to each other for two sets of virial coefficients that give rise to the same critical point. However, numerical evidence shows that the changes in the slope of the tie-lines tend to be modest over most of the range of \(B_{12}\). This is quantified below.

From eqs 26 and 27 and the requirement that \((B_{11}, B_{22}) > 0\), a bound on \(B_{12}\) can be directly derived as

\[
B_{12} > \max \left( \frac{1}{c_{1,\infty}}, \frac{1}{c_{1,\infty}^{\|}}, \frac{1}{c_{2,\infty}}^{\|} \right)
\]

Using the following expressions that were derived from eqs 24 and 25

\[
B_{11} = B_{12} S_{\infty} - \frac{1}{2c_{1,\infty}^{\|}}; \quad B_{22} = \frac{B_{12}}{S_{\infty}^{\|}} - \frac{1}{2c_{2,\infty}^{\|}}
\]

the slope of the tie-line far away from the critical point, \(-S_{\infty}\), can be written as

\[
S_{\infty} = \frac{B_{11}}{B_{22}} - \frac{S_{\infty} - \frac{1}{2B_{12}^{\|}c_{1,\infty}^{\|}}}{S_{\infty}} + \frac{1}{S_{\infty}^{\|}} - \frac{1}{2B_{12}^{\|}c_{2,\infty}^{\|}}
\]

or

\[
S_{\infty} = \left( \frac{1}{S_{\infty}^{\|}} - \frac{1}{S_{\infty}} \right) \frac{S_{\infty} - \frac{1}{2B_{12}^{\|}c_{1,\infty}^{\|}}}{S_{\infty}} + \frac{1}{S_{\infty}^{\|}} - \frac{1}{2B_{12}^{\|}c_{2,\infty}^{\|}}
\]

For large \(B_{12}\), the above equation can be expanded in a Taylor series to linear order as
\[
\frac{S_{\infty}}{S_c} = 1 + \frac{1}{4B_{12}} \left( \frac{S_c - \frac{1}{S_{c,1,c}}}{c_{2,c}} \right) + \text{higher order terms in powers of } \frac{1}{B_{12}}
\]  

(66)

From eq 66, it follows that \( S_{\infty} \to S_c \) for \( B_{12} \to \infty \) and \( S_{\infty}/S_c - 1 \) decays proportionally to \( 1/B_{12} \), for large \( B_{12} \). \( S_{\infty}/S_c \) varies only in a relatively narrow range of \( B_{12} \) close to the value where one of the pair \( B_{11} \) and \( B_{12} \) becomes zero. The phase separation criterion behaves for large \( B_{12} \) as

\[
\frac{B_{12}^2}{B_{11}B_{22}} - 1 = \frac{1}{2B_{12}} \left( \frac{S_c}{c_{2,c}} + \frac{1}{S_{c,1,c}} \right) + \text{higher order terms in powers of } \frac{1}{B_{12}}
\]  

(67)

Therefore, as \( B_{12} \) increases to large values, the phase separation criterion reaches its critical value of 1, edging closer and closer to stability.

Figure 3 shows the behavior of eqs 66 and 67 for a specific choice of virial coefficients.

![Figure 3](image)

Figure 3. (Solid line) \( S_{\infty}/S_{11} - 1 \) and (dashed-dotted line) \( \frac{B_{12}^2}{B_{11}B_{22}} - 1 \) as a function of \( B_{12} \) for a fixed critical point with \( c_{1,c} = 2.0521 \text{ mol/m}^3 \), \( c_{2,c} = 0.0445 \text{ mol/m}^3 \), and \( S_c = 0.0777 \); (dotted line) limits for large \( B_{12} \) according to eqs 66 and 67; and (red solid circle) \( S_{\infty}/S_{12} - 1 \) for the systems for which the phase diagrams are described in Figure 6.

### Degeneracy in the Virial Coefficients for a Single Tie-Line

In case the composition of the co-existing phases is known, but none of the virial coefficients is known, an infinite number of solutions is found for the virial coefficients. It can be shown (the Appendix VIII section) that the same tie-line (or co-existing phases) is obtained for two triplets of virial coefficients \((B_{11}, B_{12}, B_{22})\) and \((B_{11}', B_{12}', B_{22}')\), provided

\[
(B_{12} - B_{12}') = \frac{1}{S_m} (B_{11} - B_{11}') = S_m (B_{22} - B_{22}')
\]  

(68)

(which is similar to eq 28). This corresponds to a line in \( B \)-space that can be written in vector notation as

\[
\begin{align*}
B_{11}' & = B_{11} \\
B_{12}' & = B_{12} + \lambda_2 \left( \frac{1}{S_m} \right) \\
B_{22}' & = B_{22} + \lambda_2 \left( \frac{1}{S_m} \right)
\end{align*}
\]  

(69)

with \( \lambda_2 \) being any real number, ensuring that \( \frac{B_{12}'}{B_{11}'B_{22}'} > 1 \) and all \( B \)'s are larger than zero. A support vector \((B_{11}', B_{12}', B_{22}')\) can be found by choosing an arbitrary real value for \( B_{11} \) (i.e., \( B_{11} = 1 \)) from which \( B_{12} \) and \( B_{22} \) can be calculated from eqs 35 and 36.

### Removing Degeneracy in Virial Coefficients Using More Than One Experimental Result: Intersection of the Lines in \( B \)-Space

In the previous sections, it was shown that a single data point (like the critical point or a tie-line) is insufficient to determine a unique set of virial coefficients. There is always a line in \( B \)-space that satisfies the requirements for one of these requirements. Next, the use of two data points (a critical point and a tie-line or two tie-lines) to obtain a unique set is discussed. It is shown that this approach is possible in theory, as it involves finding the intersection of two nonparallel lines in \( B \)-space, but it requires an experimental accuracy that is not likely to be achieved in practice. The case where the critical point and one of the tie-lines is known is considered below, but the example can easily be adapted for the case where two tie-lines are known.

First, consider a phase diagram that is characterized by a set of virial coefficients \((B_{11}, B_{12}, B_{22})\). As the discussion in the previous sections has shown, each critical point (cf. eq 29) or tie-line (cf. eq 69) in the diagram can be represented by triplets of virial coefficients situated on lines in \( B \)-space. These lines fan out from a single point in \( B \)-space that corresponds with the actual virial coefficients \((B_{11}, B_{12}, B_{22})\). In theory, no more than two lines in \( B \)-space are needed to determine the actual triplet \((B_{11}, B_{12}, B_{22})\).

Next, consider the inverse case: two sets of virial coefficients that satisfy the individual requirements for a critical point \((U_{11}, U_{12}, U_{22})\) and a tie-line \((V_{11}, V_{12}, V_{22})\) are known and are points on lines in \( B \)-space that give rise to the same critical point or tie-line. The intersection of the two lines of individual solutions, \( P_{1} \) and \( P_{0} \), is the common solution and can be found from

\[
P_{1} = \begin{pmatrix}
U_{11} \\
U_{12} \\
U_{22}
\end{pmatrix} + \frac{S(V_{11} - U_{11} + U_{12} - V_{12})}{(S - S_m)} \begin{pmatrix}
\frac{S_c}{1/S_c} \\
1/S_c
\end{pmatrix}
\]  

(70)

\[
P_{0} = \begin{pmatrix}
V_{11} \\
V_{12} \\
V_{22}
\end{pmatrix} + \frac{S(V_{11} - U_{11} + U_{12} - V_{12})}{(S - S_m)} \begin{pmatrix}
\frac{S_m}{1/S_m} \\
1/S_m
\end{pmatrix}
\]  

(71)

From the discussion above, it can be concluded that in the nonsymmetrical case \((B_{11} \neq B_{12})\), in theory, two tie-lines or a tie-line and a critical point can be used to determine a unique set of virial coefficients. In practice, however, the range over which \( S_m \) varies is small and the experimental inaccuracy in the determination of the composition of the co-existing phases is too high to exploit this approach.
Sensitivity of the Shape of the Phase Diagram to the Choice of the Virial Coefficients in Degenerate Cases.

Above, it was established that in the general case it is possible to have an infinite number of combinations of virial coefficients that give rise to the same feature in a phase diagram (a critical point, a tie-line). It was also established that two features (the critical point + a tie-line, two tie-lines) fix the choice of the virial coefficients and therefore the phase diagram. For the special symmetric case \( B_{11} = B_{22} \), a single feature is sufficient to fix the choice of the virial coefficients.

What was not established is whether the phase diagram in the first case (virial coefficients based on a single feature) is sensitive to the choice of a triplet \((B_{11}, B_{12}, B_{22})\) on the corresponding line in \( B \)-space. Numerical calculations are presented below to address this question. The near-symmetrical and asymmetrical cases are distinguished.

Near-Symmetrical Cases. In near-symmetrical cases, where \( B_{11} \approx B_{22} \), the binodal is almost mirror-symmetrical relative to the line \( c_1 = c_2 \). This is illustrated in Figure 4, where the phase diagrams are calculated for the different sets of virial coefficients \((B_{11}, B_{12}, B_{22}) = (4, 3, 1) \) (m^3/mol) and \((B_{11}, B_{12}, B_{22}) = (1, 3, 4) \) (m^3/mol). Figure 4 shows that the binodals nearly superimpose, although the tie-lines and spinodals are distinctly different. It is noted that the spinodal is sensitive to the choice of the virial coefficients, as was to be expected from the expressions for their asymptotic values (see discussion below eq 33).

In near-symmetrical cases, it is possible to find a binodal for a symmetric case, where \( B_{11} = B_{22} \), that nearly overlaps the original binodal; in this example, \( B_{11} = B_{22} = 1 \) (m^3/mol), \( B_{22} = 1.948 \) (m^3/mol) was used. The method to determine the virial coefficients to find the corresponding symmetrical binodal is described in the Appendix IX section (eq 144).

Clearly Asymmetrical Cases. Typically, \( B_{11} \) and \( B_{22} \) differ substantially \((B_{11} \ll B_{22} \text{ or } B_{11} \gg B_{22})\) and the binodal becomes asymmetric. Even though each point on the binodal can be interpreted as a new critical point for a different set of virial coefficients (cf. Appendix X), the binodals through this new critical point generally do not superimpose on the binodal of the original critical point. This is illustrated in Figure 5.

Focusing on binodals for the same critical point, but different virial coefficient combinations (cf. Figure 3), it was shown that \( S_\infty \) is the same (Appendix V). Triplets of virial coefficients that lead to the same critical point do not lead to the same slope of the tie-lines far away from the critical point, \(-S_\infty = -\sqrt{(B_{11}/B_{22})}\). As a result, triplets of virial coefficients that lead to the same critical point do not lead to the same phase diagram. In practice, \( S_\infty \) only varies significantly if either \( B_{11} \) or \( B_{22} \) get very close to zero. When \( B_{12} \to \infty \), we find that the binodal converges to the analytical expression given in eq 66. It is noted that when \( B_{12} \to \infty \), all tie-lines become parallel to each other with a slope \(-S_\infty \) and the phase diagrams for a fixed critical point converge to the same phase diagram for \( B_{12} \to \infty \). This is illustrated in Figure 6. Three phase diagrams are shown for the virial coefficient triplets. Label A: \((B_{11}, B_{12}, B_{22}) = (0.0052, 3.2000, 29.9146) \) (m^3/mol), label B: \((B_{11}, B_{12}, B_{22}) = (1.00, 16.00, 194.7) \) (m^3/mol), and label C: \((B_{11}, B_{12}, B_{22}) = (5.9774, 80, 1017.5) \) (m^3/mol). These parameter combinations show the same critical point \((c_{11}, c_{12}) = (2.3521, 0.0445) \) (mol/m^3). The spinodals are sensitive to the choice of the virial coefficients. The spinodal and tie-lines B and C nearly superimpose, whereas A and B are clearly different. The same is true for the binodals, although the differences are smaller. One could question whether any of the differences would be sufficiently large to be discerned experimentally. Also, the tie-lin-
Furthermore, the present formulation of the problem revealed that individual properties of the phase diagram (e.g., the critical point or tie-line) are described by an infinite number of triplets \((B_{11}, B_{12}, B_{22})\) of virial coefficients. The properties of these triplets were investigated and were found to be represented by straight lines in “B-space”. If the features of the phase diagram are determined with infinite precision, two properties of the phase diagram (e.g., two tie-lines, one tie-line plus a critical point) suffice to determine the actual virial coefficients. In practice, the data is not accurate enough to achieve this, echoing an observation previously made by Clark.\(^{29}\)

It is found that nearly any choice of virial coefficients gives rise to the same critical point and a similar phase diagram. The binodal and tie-lines for all of these choices almost superimpose, making it unlikely that one could distinguish between the calculated binodals experimentally. The calculated spinodals do depend on the choices of virial coefficients but are experimentally less accessible. Only for choices where \(B_{11}\) or \(B_{22}\) nearly vanish (before they become negative), meaningful differences are observed between phase diagrams.

It was also established that every point on the binodal can be considered as a critical point for another choice of virial coefficients. However, generally, the binodals through these critical points do not superimpose, except if the values of \(B_{11}\) and \(B_{22}\) are close, leading to a nearly symmetrical binodal.

Although the present paper focused on the Edmond–Ogston model, the observations should essentially hold for the Flory–Huggins model too, given the equivalence between both models up to the second order of the expansion in the concentrations as identified by Clark.\(^{29}\)

The present paper also provides a procedure to calculate the various properties of the phase diagram, in particular the tie-lines. The critical point and spinodal can be calculated analytically through eqs \(24\), \(25\), and \(33\). The present results indicate that the best method to calculate the properties of the binodal and tie-lines involves the following steps:

- Calculate the minimum and maximum slope of the tie-lines, \(S_{\text{min}}\) and \(S_{\text{max}}\) using eqs \(22\), \(23\), and \(54\) (note that \(S_{\text{min}}\) is not necessarily smaller than \(S_{\text{max}}\)).
- Choose the slope \(S_{\text{min}}\) of an intermediate tie-line having a value between \(-S_{\text{max}}\) and \(-S_{\text{min}}\).
- Calculate \(c_{12}\) and \(c_{22}\) using eq \(42\).
- Solve matrix eq \(52\) for \(c_{1}^{\text{II}}\) and \(c_{2}^{\text{II}}\).
- Determine \(c_{1}^{\text{II}}\) and \(c_{2}^{\text{II}}\) by means of eq \(51\).

From a practical point of view, the present results indicate that although the two coordinates for the critical point are insufficient to determine the model parameters accurately, they are sufficient to determine most features of the phase diagram with fair accuracy. The shape of the binodal seems to be least sensitive to the choice of the virial coefficients in the Edmond–Ogston model. The slope of the tie-lines shows variations only in a relatively narrow range of values for \(B_{22}\). The spinodal is the most sensitive to the choice of the three virial coefficients.

The obtained results reveal the intricacies of the Edmond–Ogston model, especially in the context of degeneracies within the model. This deeper understanding of the model helps to assess the possibilities and limitations of the use of phase diagrams from the literature to extract virial coefficients and in this way build a database of parameters to describe the phase behavior of many polymer mixtures.

**CONCLUSIONS**

This paper investigated the solutions of the Edmond–Ogston model, a virial model that takes into account virial coefficients up to the second order and which can be used to describe phase separation in binary mixtures of polymers in a common solvent. The real strength of this model is for relatively low polymer concentrations. The model becomes more qualitative when the polymer concentrations exceed the overlap concentrations. The model can be taken as a critical point for another virial coefficients. In practice, the data is not accurate enough to achieve this, echoing an observation previously made by Clark.\(^{29}\)

The present paper also provides a procedure to calculate the various properties of the phase diagram, in particular the tie-lines. The critical point and spinodal can be calculated analytically through eqs \(24\), \(25\), and \(33\). The present results indicate that the best method to calculate the properties of the binodal and tie-lines involves the following steps:

- Calculate the minimum and maximum slope of the tie-lines, \(S_{\text{min}}\) and \(S_{\text{max}}\) using eqs \(22\), \(23\), and \(54\) (note that \(S_{\text{min}}\) is not necessarily smaller than \(S_{\text{max}}\)).
- Choose the slope \(S_{\text{min}}\) of an intermediate tie-line having a value between \(-S_{\text{max}}\) and \(-S_{\text{min}}\).
- Calculate \(c_{12}\) and \(c_{22}\) using eq \(42\).
- Solve matrix eq \(52\) for \(c_{1}^{\text{II}}\) and \(c_{2}^{\text{II}}\).
- Determine \(c_{1}^{\text{II}}\) and \(c_{2}^{\text{II}}\) by means of eq \(51\).

From a practical point of view, the present results indicate that although the two coordinates for the critical point are insufficient to determine the model parameters accurately, they are sufficient to determine most features of the phase diagram with fair accuracy. The shape of the binodal seems to be least sensitive to the choice of the virial coefficients in the Edmond–Ogston model. The slope of the tie-lines shows variations only in a relatively narrow range of values for \(B_{22}\). The spinodal is the most sensitive to the choice of the three virial coefficients.

The obtained results reveal the intricacies of the Edmond–Ogston model, especially in the context of degeneracies within the model. This deeper understanding of the model helps to assess the possibilities and limitations of the use of phase diagrams from the literature to extract virial coefficients and in this way build a database of parameters to describe the phase behavior of many polymer mixtures.
APPENDICES

Appendix I: Comparison of the Flory–Huggins and (Extended) Edmond–Ogston Models for Binary Polymer Mixtures in a Solvent

The aim of this appendix is to compare the Flory–Huggins model to the (extended) Edmond–Ogston model. The extension includes the third-order terms in concentration because issues with the Flory–Huggins model arise there. Symbols not explained in this appendix have the same meaning as in the main text.

Starting from the expression for the Helmholtz free energy (cf. eq 1)

$$ F = RT \left[ n_1 \ln \left( \frac{n_1}{V} \right) + n_2 \ln \left( \frac{n_2}{V} \right) + \frac{n_1^2 B_{11}}{V} + \frac{2n_1 n_2 B_{12}}{V} \right] $$

$$ + \frac{n_2^2 B_{22}}{V} + \frac{n_1^3 C_{111}}{V^2} + \frac{3n_1^2 n_2 C_{112}}{V^2} + \frac{3n_1^2 n_2 C_{122}}{V^2} $$

$$ + \frac{n_2^3 C_{222}}{V^2} $$

(72)

where $C_{111}$, $C_{112}$, $C_{122}$, and $C_{222}$ are the third-order virial coefficients, leads to the following equations for the extended Edmond–Ogston model

$$ \Pi = -\frac{1}{RT} \left( \frac{\partial F}{\partial n_1} \right)_{n_2, V} $$

$$ = c_1 + c_2 + B_{11} c_1^2 + B_{12} c_1 c_2 + 2B_{12} c_1 c_2 + C_{111} c_1^3 $$

$$ + 3C_{112} c_1^2 c_2 + 3C_{122} c_1 c_2^2 + C_{222} c_2^3 $$

(73)

$$ \Pi_1 = \frac{1}{RT} \left( \frac{\partial F}{\partial n_1} \right)_{n_2, V} $$

$$ = \ln c_1 + 2B_{11} c_1 + 2B_{12} c_2 + 1 + 3C_{111} c_1^2 + 6 $$

$$ + C_{112} c_1^2 c_2 + 3C_{122} c_1 c_2^2 $$

(74)

$$ \Pi_2 = \frac{1}{RT} \left( \frac{\partial F}{\partial n_1} \right)_{n_2, V} $$

$$ = \ln c_2 + 2B_{12} c_2 + 2B_{11} c_1 + 1 + 3C_{122} c_2^2 + 6 $$

$$ + C_{112} c_1^2 c_2 + 3C_{122} c_1 c_2^2 $$

(75)

For the Flory–Huggins model, the notation of Clark was used, except that the subscripts have been changed and the solvent is referred to as component 0 and both polymers as components 1 and 2; furthermore, $\Delta$ in the expressions for $\Delta \mu_i$ was dropped.

$$ \frac{\mu_0}{RT} = \ln \varphi_0 + \left( 1 - \frac{1}{p_1} \right) \varphi_1 + \left( 1 - \frac{1}{p_2} \right) \varphi_2 $$

$$ + (1 - \varphi_0) (\chi_{10} \varphi_0 + \chi_{12} \varphi_2) - \chi_{12} \varphi_0 \varphi_2 $$

(76)

$$ \frac{\mu_1}{RT} = \ln \varphi_1 + (1 - p_1) \varphi_0 + \left( 1 - \frac{1}{p_1} \right) \varphi_2 $$

$$ + p_1 (1 - \varphi_1) (\chi_{10} \varphi_0 + \chi_{12} \varphi_2) - p_1 \chi_{10} \varphi_0 \varphi_2 $$

(77)

$$ \frac{\mu_2}{RT} = \ln \varphi_2 + (1 - p_2) \varphi_0 + \left( 1 - \frac{1}{p_2} \right) \varphi_1 $$

$$ + p_2 (1 - \varphi_2) (\chi_{20} \varphi_0 + \chi_{12} \varphi_1) - p_2 \chi_{12} \varphi_0 \varphi_1 $$

(78)

Here, $p_1$ and $p_2$ are the molecular weights of polymers 1 and 2; $\chi_{10}$ and $\chi_{20}$ are the Flory–Huggins interaction parameters between polymers and solvent and $\chi_{12}$ between both polymers; and $\varphi_0$, $\varphi_1$, and $\varphi_2$ are the volume fractions of the solvent and both polymers.

The osmotic pressure in the Flory–Huggins model can be obtained from eq 76 and using the substitution

$$ \varphi_0 = 1 - (\varphi_1 + \varphi_2) $$

(79)

which leads to (cf. eq 10)

$$ \Pi_0 = -\frac{\mu_0}{RT} $$

$$ = -\left( \ln(1 - (\varphi_1 + \varphi_2)) + \left( 1 - \frac{1}{p_1} \right) \varphi_1 ight) $$

$$ + \left( 1 - \frac{1}{p_2} \right) \varphi_2 + (\varphi_1 + \varphi_2) (\chi_{10} \varphi_1 + \chi_{20} \varphi_2) $$

$$ - \chi_{12} \varphi_0 \varphi_2 $$

(80)

Expansion of $\varphi_0$ around 1 (because the total polymer concentration can be considered small) using

$$ \ln(1 - (\varphi_1 + \varphi_2)) $$

$$ = -(\varphi_1 + \varphi_2) - \frac{1}{2}(\varphi_1 + \varphi_2)^2 - \frac{1}{3}(\varphi_1 + \varphi_2)^3 $$

$$ - \sum_{n=4}^{\infty} \frac{(\varphi_1 + \varphi_2)^n}{n} $$

(81)

and truncating to the third order results in

$$ \Pi_0 = \left( \frac{1}{p_1} \varphi_1 + \frac{1}{p_2} \varphi_2 + \left( 1 - \chi_{10} \right) \varphi_1^2 ight) $$

$$ + \left( 1 - \chi_{10} - \chi_{20} + \chi_{12} \right) \varphi_1 \varphi_2 + \left( 1 - \chi_{10} \right) \varphi_2^2 $$

$$ + \frac{1}{3} \varphi_1^3 + \frac{1}{3} \varphi_2^3 $$

(82)

The chemical potential for polymer 1 in the Flory–Huggins model can be obtained from eq 77 as

$$ \frac{\mu_1}{RT} = \ln \varphi_1 + (1 - p_1) \varphi_0 + \left( 1 - \frac{1}{p_1} \right) \varphi_1 $$

$$ + \left( 1 - \frac{1}{p_2} \right) \varphi_2 + (\chi_{10} - \chi_{20}) \varphi_1 \varphi_2 + \chi_{10} \varphi_0 \varphi_1 $$

(83)

A similar relation for polymer 2 can be obtained from eq 78 as
free energy is a state variable. This relation is fulfilled for the extended
Edmond–Ogston model, which can be demonstrated using eqs 74 and 75

\[
\frac{\mu_i}{RT} = \ln \phi_2 + \left(1 - p_2 + p_2x_{20}\right) + \left(1 - \frac{1}{p_2} - 2x_{20}\right)p_2\phi_2
\]

\[
+ \left(1 - \frac{1}{p_1} + x_{12} - x_{20} - x_{10}\right)p_2\phi_1 + x_{20}p_2\phi_2^2
\]

\[
+ \left(x_{10} + x_{20} - x_{12}\right)p_2\phi_1\phi_2 + x_{10}p_2\phi_1^2
\]

(84)

It is now possible to match the parameters in both models. The results are summarized in Table 2.

To match the equations for the osmotic pressure and the chemical potentials in the Flory–Huggins model consistently up to the second order, one has to make the (reasonable) assumption that \(1/p_1 \ll 1 - 2x_{10}\) and \(1/p_2 \ll 1 - 2x_{20}\). The absolute value of the chemical potentials is shifted by a constant, but this does not matter as the differences between the chemical potentials in two phases are compared, and the chemical potentials are shifted in each phase by the same value.

To ensure that the coefficients are consistent up to the third order, one has to assume that \(\chi_{10} = \chi_{20} = \chi_{12} = \mu_v\). This is a problem because this fixes all of the adjustable parameters in the Flory–Huggins model. In addition, it is surprising that the third-order parameters in eqs 77 and 78 in the Flory–Huggins model are expressed in terms of the binary interaction parameters.

The Maxwell relation (cf. eq 6) reflects that the Helmholtz free energy is a state variable. This relation is fulfilled for the extended Edmond–Ogston model, which can be demonstrated using eqs 74 and 75

\[
\left(\frac{\partial}{\partial n_i} \left(\frac{\mu_i}{RT}\right)\right)_{T,\mu_j} = \left(\frac{\partial}{\partial n_i} \left(\frac{\mu_i}{RT}\right)\right)_{T,\mu_k}
\]

\[
= \frac{2}{V}B_{12} + \frac{6}{V}C_{112} \phi_1 + \frac{6}{V}C_{122} \phi_2
\]

(85)

For the Flory–Huggins model, however, it is found that

\[
\frac{\partial}{\partial n_i} \left(\frac{\mu_1}{RT}\right)_{T,\mu_j} = \left(\frac{\partial}{\partial n_i} \left(\frac{\mu_1}{RT}\right)\right)_{T,\mu_k}
\]

\[
= \frac{2}{V}B_{12} + \frac{6}{V}C_{112} \phi_1 + \frac{6}{V}C_{122} \phi_2
\]

\[
= \frac{2}{V}B_{12} + \frac{6}{V}C_{112} \phi_1 + \frac{6}{V}C_{122} \phi_2
\]

(86)

and

\[
\frac{\partial}{\partial n_i} \left(\frac{\mu_2}{RT}\right)_{T,\mu_j} = \frac{2}{V}B_{12} + \frac{6}{V}C_{112} \phi_1 + \frac{6}{V}C_{122} \phi_2
\]

From eqs 86 and 87, the validity of the Maxwell relation requires that

\[
\frac{1}{\mu_1} + \left(1 - \phi_2\right)(\chi_{20} - \chi_{12}) + \chi_{10}(1 - \phi_2 - 2\phi_1)
\]

\[
= \frac{1}{\mu_2} + \left(1 - \phi_1\right)(\chi_{10} - \chi_{12}) + \chi_{20}(1 - \phi_1 - 2\phi_2)
\]

(88)

which is only valid in special cases (e.g., when the properties of polymer 1 are indistinguishable from those of polymer 2). Therefore, in general, the Maxwell relation does not seem to hold for the Flory–Huggins model.

**Table 2. Matching of Terms between Flory–Huggins and Extended Edmond–Ogston Models**

| extended Edmond–Ogston model parameters | Flory–Huggins model parameters, from eq 76 | Flory–Huggins model parameters, from eq 77 | Flory–Huggins model parameters, from eq 78 |
|----------------------------------------|------------------------------------------|------------------------------------------|------------------------------------------|
| \(c_1\) | \(\frac{1}{\phi_1} - 1\) | \(\frac{1}{\phi_1} - 1\) | \(\frac{1}{\phi_1} - 1\) |
| \(c_2\) | \(\frac{1}{\phi_2} - 1\) | \(\frac{1}{\phi_2} - 1\) | \(\frac{1}{\phi_2} - 1\) |
| \(B_{11}\) | \(\frac{1}{\phi_1} - 1\) | \(\frac{1}{\phi_1} - 1\) | \(\frac{1}{\phi_1} - 1\) |
| \(B_{22}\) | \(\frac{1}{\phi_2} - 1\) | \(\frac{1}{\phi_2} - 1\) | \(\frac{1}{\phi_2} - 1\) |
| \(B_{12}\) | \(\frac{1}{\phi_1} - 1\) | \(\frac{1}{\phi_1} - 1\) | \(\frac{1}{\phi_1} - 1\) |
| \(C_{111}\) | \(\frac{1}{\phi_1} - 1\) | \(\frac{1}{\phi_1} - 1\) | \(\frac{1}{\phi_1} - 1\) |
| \(C_{112}\) | \(\frac{1}{\phi_1} - 1\) | \(\frac{1}{\phi_1} - 1\) | \(\frac{1}{\phi_1} - 1\) |
| \(C_{122}\) | \(\frac{1}{\phi_1} - 1\) | \(\frac{1}{\phi_1} - 1\) | \(\frac{1}{\phi_1} - 1\) |

ACS Omega 2021, 6, 7862–7878
Appendix II: The Gibbs Phase Rule for a Mixture of N Components Distributed in F Phases

(A) For the chemical potentials, we find from thermodynamic equilibrium requirements that

$$\mu^1(c_1, c_2, \ldots, c_N) = \mu^2(c_1, c_2, \ldots, c_N) = \cdots = \mu^F(c_1, c_2, \ldots, c_N)$$

This gives \(N(F - 1)\) equations with \(NF\) unknowns.

(B) For the osmotic pressures, we find from thermodynamic equilibrium requirements that

$$\pi^1 = \pi^2 = \cdots = \pi^F$$

This gives \((F - 1)\) equations.

We find from A and B a total of \((N + 1)(F - 1)\) equations and \(NF\) unknowns. The number of equations can never be greater than the number of unknowns, from which it follows that

$$(N + 1)(F - 1) \leq NF$$

or \(F = N + 1\). The degree of freedom \(D\) is introduced as

$$D = N - F + 1 \geq 0$$

When \(N = 2\) and \(F = 2\), it follows that \(D = 1\), which implies that one of the concentrations can be varied to find the binodal.

When \(N = 2\) and \(F = 3\), it follows that \(D = 0\), which implies that there can be a three-phase equilibrium for a binary mixture, but it corresponds to a point (or points) in the phase diagram since \(D = 0\).

Appendix III: The Expressions for the Critical Point (Equations 24 and 25) Are Equivalent to the Expressions Used in Dewi et al.\(^{31}\)

Here, it is demonstrated that

$$c_{1,c} = \frac{1}{2(B_{12}s_1 - B_{11})}$$

and

$$c_{2,c} = \frac{1}{2B_{22} \left( \frac{B_{12} s_1}{s_2} - B_{22} \right)}$$

can be written in the form used for the critical point by rewriting the expressions for the requirement for the critical point, eqs 20 and 21 (or eq A.8 in Dewi et al.\(^{31}\)), as

$$\frac{B_{12}}{B_{11}} \sqrt{s_1^2 - 1} = \frac{B_{12}}{B_{11}} s_1 - \frac{B_{22}}{B_{11}} \sqrt{s_1^3}$$

(94)

$$\frac{B_{12}}{B_{22}} \frac{1}{\sqrt{s_2^2 - 1}} = \frac{B_{12}}{B_{22}} \frac{1}{\sqrt{s_2}} - \frac{B_{22}}{B_{22}} \frac{1}{\sqrt{s_2^3}}$$

(95)

respectively. In this case

$$c_{1,c} = \frac{1}{2(B_{12}s_1 - B_{11})} = \frac{1}{2B_{11}} \left( \frac{B_{12} s_1}{s_2} - B_{22} \right)$$

$$c_{2,c} = \frac{1}{2(B_{12}s_1 - B_{11})} = \frac{1}{2B_{22} \left( \frac{B_{12} s_1}{s_2} - B_{22} \right)}$$

(96)

and

$$2B_{12} c_{1,c} = \frac{1}{(\alpha^2 \beta - 1)}$$

(98)

$$2B_{22} c_{2,c} = \frac{1}{(\alpha^2 \beta - 1)}$$

(99)

where \(\alpha = B_{12}/B_{11}, \beta = B_{12}/B_{22}\), and \(s_e = \sqrt{\beta/\alpha} - s_s\). Note that the slope at the critical point in normalized units, \(-s_s\), was written with a capital \(-s_e\) in our previous paper.\(^{31}\)

Appendix IV: The Third-Order Stability Polynomial (Equation 20 or 21) Is Equivalent to the Edmond–Ogston Expression Involving the Critical Point

Equation 20 can be rewritten as

$$\sqrt{s_e^3} \left( \frac{B_{12}}{s_e} - B_{22} \right) = (B_{12} - B_{11})$$

(100)

or

$$s_e^{3/2} = \frac{(B_{12} s_e - B_{11})}{(B_{12} s_e - B_{22})}$$

(101)

Equation 101 can be substituted in the rather convoluted identities for \((2B_{12} s_e)^3\) and \((2B_{12}/s_e)^3\)
\[(2(B_{12}S_{l} - B_{11}) + 2B_{11})^3 = (2B_{12})^3 \left( \frac{2(B_{12}S_{l} - B_{11})}{2(B_{12}S_{l} - B_{22})} \right)^2 \]
\[(\text{102})\]

\[
\left( \frac{B_{12} - B_{22}}{S_{l}} \right)^3 + 2B_{22}^3 = (2B_{12})^3 \left( \frac{2(B_{12} - B_{22})}{2(B_{12}S_{l} - B_{11})} \right)^2 \]
\[(\text{103})\]

Since the critical point is given by (cf. eqs 24 and 25)

\[
c_{1,c} = \frac{1}{2(B_{12}S_{l} - B_{11})} \]
\[(\text{104})\]

\[
c_{2,c} = \frac{1}{2(B_{12} - B_{22})} \]
\[(\text{105})\]

Equations 104 and 105 can be rewritten as eq 5a,b in Edmond and Ogston \(^\text{28}\) by introducing the notation of Edmond and Ogston \(^\text{28}\) for the virial coefficients

\[
a = 2B_{12} \]
\[(\text{108})\]

\[
c = 2B_{11} \]
\[(\text{109})\]

\[
d = 2B_{22} \]
\[(\text{110})\]

By ultimately taking the cube root, the desired result is obtained

\[
\left( \frac{1}{c_{1,c}} + e \right)^3 = a \left( \frac{c_{2,c}}{c_{1,c}} \right)^2 \]
\[(\text{106})\]

\[
\left( \frac{1}{c_{2,c}} + d \right)^3 = a \left( \frac{c_{1,c}}{c_{2,c}} \right)^2 \]
\[(\text{107})\]

(where the indices in the notation of Edmond and Ogston \(^\text{28}\) were changed to the present convention, \((2,3) \rightarrow (1,2)\)). Therefore, it can be concluded that eq 5a,b in Edmond and Ogston \(^\text{28}\) is an alternative representation of eq 20, the third-order polynomial defining the critical point.

**Appendix V: If Two Triplets of Virial Coefficients Give Rise to the Same Critical Point, They Also Give Rise to the Same Slope for the Binodal and Spinodal at the Critical Point**

To define a valid critical point using an alternative set of virial coefficients \((B_{11}, B_{12}, B_{22})\), this set needs to satisfy eq 20

\[
B_{22}^* \sqrt{S_{l}^3} + B_{12}^* \sqrt{S_{l}^2} - B_{11}^* \sqrt{S_{l}} = 0 \]
\[(\text{113})\]

From

\[
(B_{12} - B_{12}^*) = \frac{1}{S_{l}}(B_{11} - B_{11}^*) = S_{l}(B_{22} - B_{22}^*) \]
\[(\text{114})\]

it follows that

\[
B_{11}^* = B_{11} - S_{l}(B_{12} - B_{12}^*) \]
\[(\text{115})\]

\[
B_{22}^* = B_{22} - \frac{1}{S_{l}}(B_{12} - B_{12}^*) \]
\[(\text{116})\]

or

\[
\left( B_{22} - \frac{1}{S_{l}}(B_{12} - B_{12}^*) \right) \sqrt{S_{l}^3} + B_{12}^* \sqrt{S_{l}^2} - B_{11}^* \sqrt{S_{l}} - B_{11} = S_{l}(B_{12} - B_{12}^*) = 0 \]
\[(\text{117})\]

The original set of virial coefficients satisfies the third-order polynomial (with \(S_{l}\) not changed), therefore

\[
\left( \frac{1}{S_{l}}(B_{12} - B_{12}^*) \right) \sqrt{S_{l}^3} + (B_{12}^* - B_{12}) \sqrt{S_{l}^2} - (B_{11}^* - B_{11}) \sqrt{S_{l}} + (S_{l}(B_{12} - B_{12}^*)) = 0 \]
\[(\text{118})\]

The term \(B_{12}^* - B_{12}\) can be divided, leading to

\[
\left( \frac{1}{S_{l}} \right) \sqrt{S_{l}^3} + \sqrt{S_{l}^2} - \sqrt{S_{l}} - S_{l} = 0 \]
\[(\text{119})\]

which is true and proves the assertion.

**Appendix VI: Demonstration on How Equations 49 and 50 Follow from Equations 16 and 17**

Starting from eq 16, the terms in \(B_{13}\) can be moved to the same side of the equation. Applying the definition of \(S_{m}\) from eq 45 leads to

\[
\ln c_{1,i} + 2B_{12}c_{1,i} = \ln c_{1,ii} + 2B_{11}c_{1,ii} - 2B_{12}S_{m}(c_{1,ii} - c_{1,i}) \]
\[(\text{120})\]

Placing all terms for phase I on one side and those for phase II on the other side leads to

\[
\ln c_{1,i} - 2(B_{12}S_{m} - B_{11})c_{1,i} = \ln c_{1,ii} - 2(B_{12}S_{m} - B_{11})c_{1,ii} \]
\[(\text{121})\]

Using the definition for \(c_{1,i}\) in eq 42 and subtracting a term \(\ln(c_{1,i})\) on both sides, this can be written in the form of eq 49. Similarly, it is possible to rewrite eq 17 as

\[
\ln c_{2,i} - 2(B_{12}/S_{m} - B_{22})c_{2,i} = \ln c_{2,ii} - 2(B_{12}/S_{m} - B_{22})c_{2,ii} \]
\[(\text{122})\]

yielding eq 50.

**Appendix VII: The Value of \(S_{m}\) at the Critical Point and Far Away from the Critical Point**

Here, the values of the slope \(-S_{m}\) are given in two limits. First, the case close to the critical point is addressed, where the following expression can be written by substitution of eqs 24 and 25
Co-existing Phases

For an alternative set of virial coefficients $B_{ij}$, $c_{ij}$ to result in the same co-existing phases, the new virial coefficients need to satisfy the equivalent of eqs 15–17

$$c_1^i + c_2^i + B_{1i}c_1^i + B_{2i}c_2^i + 2B_{12}c_1^i c_2^i = c_1^{i+1} + c_2^{i+1} + B_{1i}c_1^{i+1} + B_{2i}c_2^{i+1} + 2B_{12}c_1^{i+1} c_2^{i+1}$$

$$\ln c_1^i + 2B_{1i}c_1^i + 2B_{2i}c_2^i = \ln c_1^{i+1} + 2B_{1i}c_1^{i+1} + 2B_{2i}c_2^{i+1}$$

Using a similar approach as previously for the critical point (cf. eqs 115 and 116)

$$B'_{1i} = B_{1i} - S_m(B_{12} - B'_{12})$$

$$B'_{2i} = B_{2i} - \frac{1}{S_m}(B_{12} - B'_{12})$$

The original equations for the set $(B_{11}, B_{12}, B_{22})$ can be subtracted now

$$(-S_m(B_{12} - B'_{12}))c_1^2 + \left(-\frac{1}{S_m}(B_{12} - B'_{12})\right)c_2^2 - 2(B_{12} - B'_{12})c_1^i c_2^i = (-S_m(B_{12} - B'_{12}))c_1^{i+1} + \left(-\frac{1}{S_m}(B_{12} - B'_{12})\right)c_2^{i+1} - 2(B_{12} - B'_{12})c_1^{i+1} c_2^{i+1}$$

$$2(-S_m(B_{12} - B'_{12}))c_1^2 - 2(B_{12} - B'_{12})c_2^2 = 2(-S_m(B_{12} - B'_{12}))c_1^{i+1} - 2(B_{12} - B'_{12})c_2^{i+1}$$

$$2\left(-\frac{1}{S_m}(B_{12} - B'_{12})\right)c_2^2 - 2(B_{12} - B'_{12})c_1^i c_2^i = 2\left(-\frac{1}{S_m}(B_{12} - B'_{12})\right)c_1^{i+1} - 2(B_{12} - B'_{12})c_2^{i+1}$$

In eqs 136–138, $(B_{12} - B'_{12})$ can be divided and the following equations are obtained after rearranging

$$(S_m c_1^i + c_2^i)^2 = (S_m c_1^{i+1} + c_2^{i+1})^2$$

$$\frac{1}{S_m} c_1^i + c_1^i = \frac{1}{S_m} c_2^{i+1} + c_2^{i+1}$$

Each of the eqs 139–141 can be rewritten in the form of eq 45. A similar observation can be made here as for the critical point: from the form of the coordinates in eq 42, it can be concluded that if all virial coefficients $B_i$ are multiplied by the same factor $k$, the coordinates in eq 42 are divided by a factor $k$. In contrast to the situation for the critical point, however, the slope $-S_m$ changes because not every term in the right-hand side of eq 39 for $S_m$ features is a virial coefficient.
Appendix IX: The Intersection of a Binodal with the Line $c_1 = c_2$

The critical point $(c_{1,0}, c_{2,0})$ is given by eqs 24–25 or 104–105. A critical point for the symmetrical case $(C_0, C_0)$ can always be expressed as

$$c_i = \frac{1}{2(B_{12}^* - B^*)}$$

Equations 57 and 58 provide an analytical expression for the binodal in the symmetrical case through the critical point. Substituting $(C_1, C_1)$ for the critical point belonging to the symmetrical binodal and $(c_{1,0}, c_{2,0})$ for the nonsymmetrical point that should be placed on the symmetrical binodal, the following expression is obtained

$$c_{2,i} = \frac{1}{W} \left( -\frac{c_{1,i}}{C_i} e^{-c_{1,i}/C_i} \right)$$

Substituting the explicit expressions for $(c_{1,0}, c_{2,0}, C_0)$, eqs 104, 105, and 142 result in

$$\frac{(B_{12}^* - B^*)}{(B_{12}^* - B_{22})} = \frac{-(B_{12}^* - B^*)}{(B_{12}^* - B_{22})} e^{-(B_{12}^* - B^*)/(B_{12}^* - B_{22})}$$

Substituting $i = 0$ for $c_1 \geq C_i$

Substituting $i = -1$ for $c_1 \leq C_i$

Equation 144 allows for the determination of $B_{12}^* - B^*$ since $(B_{11}, B_{12}, B_{22})$ are known. $B_{12}^* - B^*$ specifies a line in $B$-space resulting in the same (symmetrical) critical point, similar to eq 28.

Appendix X: Any Point on the Binodal Can Be Written as a Critical Point for a Different Triplet of Virial Coefficients

Points on the binodal can be expressed as

$$(c_{1,b}, c_{2,b}) = \left( -W \left( -\frac{c_{1,b}}{c_{1,s}} e^{-c_{1,b}/c_{1,s}} \right), c_{2,b} \right)$$

If the critical point in the phase diagram is the same, the following equation can be obtained

$$c_{1,s} = \frac{1}{2(B_{12}^* - B_{22}^*)} \quad \text{and} \quad c_{2,c} = \frac{1}{2(B_{12}^* - B_{22}^*)}$$

where the terms $(B_{12}^* - B_{11}^*)$, $(B_{12}^* - B_{11}^*)$, $(B_{12}^* - B_{22}^*)$, and $(B_{12}^* - B_{22}^*)$ are constant within the sets $(B_{11}, B_{12}, B_{22})$ and $(B_{11}, B_{12}, B_{22})$. This leads to

$$-W \left( -\frac{c_{1,b}}{c_{1,s}} e^{-c_{1,b}/c_{1,s}} \right) (B_{12}^* - B_{11}^*) = (B_{12}^* - B_{11}^*)$$

$$-W \left( -\frac{c_{1,b}}{c_{1,s}} e^{-c_{1,b}/c_{1,s}} \right) (B_{12}^* - B_{22}^*) = (B_{12}^* - B_{22}^*)$$

The left-hand side can be interpreted as the set of virial coefficients $(B_{11}^*, B_{12}^*, B_{22}^*)$ that map on the same critical point (cf. Appendix V), whereas the right-hand side can be interpreted as the set of virial coefficients $(B_{11}, B_{12}, B_{22})$ that map on the same point on the binodal (cf. the Appendix VIII section). The equation expresses the relation between the virial coefficients if one wants to switch the role of a point from being just on the binodal to being a critical point. A consequence of the existence of this relation is that any point on the binodal can also be a critical point if an alternative set of virial coefficients is chosen.

**AUTHOR INFORMATION**

**Corresponding Author**

Paul Venema — Laboratory of Physics and Physical Chemistry of Foods, Department of Agrotechnology and Food Sciences, Wageningen University and Research, NL-6708 WG Wageningen, The Netherlands; Email: paul.venema@wur.nl

**Authors**

Arjen Bot — Laboratory of Physics and Physical Chemistry of Foods, Department of Agrotechnology and Food Sciences, Wageningen University and Research, NL-6708 WG Wageningen, The Netherlands; Unilever Foods Innovation Centre, NL-6708 WH Wageningen, The Netherlands; orcid.org/0000-0002-2065-8964

Belinda P. C. Dewi — Laboratory of Physics and Physical Chemistry of Foods, Department of Agrotechnology and Food Sciences, Wageningen University and Research, NL-6708 WG Wageningen, The Netherlands; orcid.org/0000-0003-0340-3131

Complete contact information is available at: https://pubs.acs.org/10.1021/acsomega.1c00450

**Notes**

The authors declare no competing financial interest.

**ACKNOWLEDGMENTS**

The authors would like to thank Erik van der Linden for fruitful discussions. B.P.C.D. acknowledges financial support by the Indonesia Endowment Fund for Education (LPDP—Lembaga Pengelola Dana Pendidikan) scholarship, Ministry of Finance, The Republic of Indonesia.

**REFERENCES**

(1) Semenova, M. G. Equilibrium in Colloidal Systems. In Thermodynamics of Phase Equilibria in Food Engineering; Gambini Pereira, C., Ed.; Academic Press: Cambridge, MA, 2018; Chapter 12, pp 507–528.
(2) Hu, W. Polymer Phase Separation. Polymer Physics; Springer: Vienna, 2012; pp 167–185.

(3) Cheng, S. Z. D. Metastable States in Phase Transitions of Polymers. Phase Transitions in Polymers—The Role of Metastable States; Elsevier, 2008; Chapter 4, pp 77–155.

(4) Frith, W. J. Mixed biopolymer aqueous solutions—phase behaviour and theology. Adv. Colloid Interface Sci. 2010, 164, 48–60.

(5) Levitt-Sengers, J. How Fluids Unmix. Discoveries by the School of Van der Waals and Kamerlingh Onnes. History of Science and Scholarship in the Netherlands; Koninklijke Nederlandse Akademie van Wetenschappen: Amsterdam, 2002; Vol. 4.

(6) Norton, I. T.; Frith, W. J. Microstructure design in mixed biopolymer composites. Food Hydrocolloids 2001, 15, S43–S53.

(7) Doublier, J. L.; Garnier, C.; Renard, D.; Sanchez, C. Protein-polysaccharide interactions. Curr. Opin. Colloid Interface Sci. 2000, 5, 202–214.

(8) Tolstoguzov, V. B. Functional properties of food proteins and role of protein-polysaccharide interaction. Food Hydrocolloids 1991, 4, 429–468.

(9) Tombs, M. P.; Peacocke, A. R. The Osmotic Pressure of Biological Macromolecules; Clarendon Press: Oxford, U.K., 1974.

(10) Cui, K.; Nan Ye, Y.; Liu, S.; Zhang, H.; Selzer, M.; Nestler, B. Progress report on phase separation in polymer solutions. Adv. Mater. 2019, 31, No. 1806733.

(11) Shi, W.; Weitz, D. A. Polymer phase separation in a microcapsule shell. Macromolecules 2017, 50, 7681–7686.

(12) Wang, F.; Altschuh, P.; Ratke, L.; Zhang, H.; Selzer, M.; Nestler, B. Progress report on phase separation in polymer solutions. Adv. Mater. 2019, 31, No. 1806733.

(13) Xia, Y.; Friend, R. H. Controlled phase separation of liquid−liquid phase separation in solutions of two macromolecular solute species. J. Phys. Chem. B 2020, 124, 2363–2370.

(14) Philippe, A. M.; Cipelletti, L.; Larobina, D. Mucus as an underlying the complex biology of intracellular phase transitions. Annu. Rev. Biophys. 2020, 49, 107–133.

(15) Lee, I. H.; Imanaka, M. Y.; Modahl, E. H.; Torres-Ocampo, A. P. Lipid raft phase modulation by membrane-anchored proteins with inherent phase separation properties. ACS Omega 2019, 4, 6551–6559.

(16) Edelman, M. W.; van der Linden, E.; Tromp, R. H. Phase separation of aqueous mixtures of poly(ethylene oxide) and dextran. Macromolecules 2003, 36, 7783–7790.

(17) Lorén, N.; Hermansson, A. M.; Williams, M. A. K.; Lundin, L.; Foster, T. J.; Hubbard, C. D.; Clark, A. H.; Norton, I. T.; Bergström, E. T.; Goodall, D. M. Phase separation induced by conformational ordering of gelatin in gelatin/maltodextrin mixtures. Macromolecules 2001, 34, 289–297.

(18) Choi, J. M.; Holehouse, A. S.; Pappu, R. V. Physical principles underlying the complex biology of intracellular phase transitions. Annu. Rev. Biophys. 2020, 49, 107–133.

(19) Gorin, V. Z.; Tolstoguzov, V. B. Thermodynamic incompatibility of proteins and polysaccharides in solutions. Food Hydrocolloids 1997, 11, 145–158.

(20) Alberti, S.; Dormann, D. Liquid-liquid phase separation in disease. Annu. Rev. Genet. 2019, 53, 171–194.

(21) Hyman, A. A.; Weber, C. A.; Ji, L. J.; Burger, L. Analytical Ultracentrifugation of Polymers and Nanoparticles; Springer: Heidelberg, 2006.

(22) Grinberg, V. Y.; Tolstoguzov, V. B. Thermodynamic incompatibility of proteins and polysaccharides in solutions. Food Hydrocolloids 1997, 11, 145–158.

(23) Edelman, M. W.; van der Linden, E.; Tromp, R. H. Phase separation of aqueous mixtures of poly(ethylene oxide) and dextran. Macromolecules 2003, 36, 7783–7790.

(24) Lorén, N.; Hermansson, A. M.; Williams, M. A. K.; Lundin, L.; Foster, T. J.; Hubbard, C. D.; Clark, A. H.; Norton, I. T.; Bergström, E. T.; Goodall, D. M. Phase separation induced by conformational ordering of gelatin in gelatin/maltodextrin mixtures. Macromolecules 2001, 34, 289–297.

(25) Choi, J. M.; Holehouse, A. S.; Pappu, R. V. Physical principles underlying the complex biology of intracellular phase transitions. Annu. Rev. Biophys. 2020, 49, 107–133.

(26) Tuchet, T. J.; Cosgriff-Hernandez, E. M. Hierarchical Structure—Property Relationships of Segmented Polyurethanes. In Advances in Polyurethane Biomaterials; Cooper, S. L.; Guan, J., Eds.; Woodhead Publishing: Cambridge, U.K., 2016; Chapter 1, pp 3–22.

(27) Flory, P. J. Principles of Polymer Physics; Cornell University Press: Ithaca, NY, 1953.

(28) Edmond, E.; Ogston, A. G. An approach to the study of phase separation in ternary aqueous systems. Biochem. J. 1968, 109, 569–576.