Impact of low-frequency ultrasound technology on physical, chemical and technological properties of cereals and pseudocereals

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A B S T R A C T

Cereals (CE) and pseudocereals (PSCE) play a pivotal role in nourishing the human population. Low-frequency ultrasound (LFUS) modifies the structure of CE and PSCE macromolecules such as starch and proteins, often improving their technological, functional and bioactive properties. Hence, it is employed for enhancing the traditional processes utilized for the preparation of CE- and PSCE-based foods as well as for the upcycling of their by-products. We report recent advances in LFUS treatments for hydration, germination, extraction of bioactive compounds from by-products, and fortification of CEs and PSCE, including kinetic modelling and underlying action mechanisms. Meta-analyses of LFUS influence on compounds extraction and starch gelatinization are also presented. LFUS enhances hydration rate and time lag phase of CE and PSCE, essential for germination, extraction, fermentation and cooking. The germination is improved by increasing hydration, releasing promoters and eliminating inhibitors. Furthermore, LFUS boosts the extraction of phenolic compounds, polysaccharides and other food components; modifies starch structure, affecting pasting properties; causes partial denaturation of proteins, improving their interfacial properties and their peptides availability. Overall, LFUS has an outstanding potential to improve transformation processes and functionalities of CE and PSCE.

1. Introduction

Ultrasound (US) is a mechanical wave with frequency higher than 20 kHz, i.e., beyond the audible frequency range of humans. It can be differentiated in three frequency ranges: 1) 20 to 100 kHz, conventional high-power or low-frequency ultrasound (LFUS); 2) 100 kHz to 2 MHz, sonochemistry range and 3) 5 to 10 MHz, medical or analytical range [1].

Over the past 20 years, the application of LFUS has gained significant potential interest in many industrial sectors because of the versatility in modifying as well as generating microstructures. Thanks to its adaptability, relative simplicity, low energy requirements and limited impact on the environment, LFUS has a very promising future in food technology and has already been applied to solve technical issues such as increasing yield, reducing treatment time [2-4], extracting with non-toxic solvents [5] and limiting energy needs [6].

LFUS can be employed to make changes in liquids, dispersions, solid and gaseous media, but they are particularly efficient when applied through a liquid [7]. LFUS effects in liquid systems are mainly related to the cavitation phenomenon: during the negative pressure half-wave (rarefaction) the medium is stressed by tensile forces that increase the distance among molecules; once the cavitation threshold is reached, the liquid breaks down and empty bubbles form. When a cavity cannot tolerate the surrounding liquid pressure, it implodes violently, and energy is immediately released. Cavities collapse is far more rapid than heat diffusion, creating a localized hot spot while the liquid bulk remains cold [8]. Inside the cavities, temperatures of 1700–4700 °C and pressures of 180–300 MPa are reached [1]. As temperature rises, cavitation threshold goes down due to drops in surface tension and viscosity, thus a liquid will start to cavitate at lower sound pressure. However, water vapor pressure will be higher and vapor-filled bubbles will form, reducing pressure difference and cushioning bubbles implosions [9]. Very high tensile forces are needed for cavitation. Energy and intensity, along with medium viscosity, surface tension, vapor pressure, nature

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and concentration of dissolved gas, presence of solid particles, temperature, and treatment pressure, determine the extent of cavitation [10]. Gas-filled bubbles or particulate produce weak spots in the liquid that allow the process to begin; alternatively, pre-generated cavitation bubbles can be starting points.

The most common frequency range applied is 20–40 kHz, because cavitation is hardly achieved at high frequencies unless very great intensities are adopted [8]. The true mechanical power in the liquid is usually far lower than the nominal one; in addition, devices with different efficiencies can be used and the volume may change as well. Therefore, to compare results it is necessary to experimentally evaluate the specific amount of energy per volume unit, an often-overlooked aspect [11]. The volumetric power can be estimated by the following formula [11,12]:

\[ P = mC_p \frac{dT}{dt} \]

where \( m \) is the water mass (kg), \( C_p \) its specific heat (4.186 kJ/(kg °C)) and \( \frac{dT}{dt} \) (°C/s) the temperature increase during the first 90 s of sonication.

Besides the mechanical effect, LFUS generates free radicals through water homolytic cleavage: \( \text{H}_2\text{O} \rightarrow \text{H}^\cdot + \text{OH}^\cdot \) [1,8]. However, free radicals are produced at the fastest rate from water at around 200 kHz (sonochemistry range) [1], while at 20 kHz their development is minimal [1,13].

Food processing procedures using LFUS have been applied to improve product quality, including bioactivity, and process efficiency in cereal and pseudocereals. However, to the best of our knowledge, a

| Study or Subgroup | Weight | IV, Random, 95% CI | Yield ratio |
|------------------|--------|-------------------|-------------|
| 1.1.1 Phenolic compounds |
| [107] | 4.7% | 3.50 [3.40, 3.61] | |
| [109] (black rice) | 4.6% | 2.11 [1.91, 2.34] | |
| [109] (purple rice) | 4.5% | 2.14 [1.92, 2.39] | |
| [111] | 4.7% | 1.36 [1.33, 1.39] | |
| [115] | 4.6% | 1.01 [0.96, 1.07] | |
| [116] | 4.6% | 1.70 [1.57, 1.84] | |
| [96] | 4.6% | 1.18 [1.14, 1.23] | |
| [75] | 4.6% | 1.18 [1.14, 1.23] | |
| [76] | 4.6% | 1.32 [1.26, 1.39] | |
| [72] | 4.6% | 1.02 [0.94, 1.12] | |
| [76] | 4.6% | 1.66 [1.57, 1.74] | |
| [88] | 4.6% | 1.27 [1.22, 1.33] | |
| Subtotal (95% CI) | 55.4% | 1.52 [1.19, 1.94] | |
| Heterogeneity: \( \tau^2 = 0.19 \), \( \chi^2 = 4002.21 \), df = 11 (\( P < 0.00001 \)), \( \Gamma = 100\% \) Test for overall effect: \( Z = 3.34 \) (\( P = 0.0008 \)) |
| 1.1.2 Oil |
| [120] | 4.7% | 1.23 [1.20, 1.26] | |
| [85] | 4.7% | 1.28 [1.25, 1.32] | |
| [86] | 4.6% | 1.79 [1.62, 1.97] | |
| [88] | 4.5% | 1.22 [1.06, 1.39] | |
| Subtotal (95% CI) | 18.4% | 1.35 [1.23, 1.49] | |
| Heterogeneity: \( \tau^2 = 0.01 \), \( \chi^2 = 55.78 \), df = 3 (\( P < 0.00001 \)), \( \Gamma = 95\% \) Test for overall effect: \( Z = 6.20 \) (\( P < 0.00001 \)) |
| 1.1.3 Polysaccharides |
| [89] | 4.5% | 1.88 [1.71, 2.07] | |
| [94] | 3.4% | 9.53 [6.26, 14.52] | |
| [95] | 4.6% | 1.00 [0.91, 1.10] | |
| [99] | 4.6% | 1.40 [1.35, 1.45] | |
| Subtotal (95% CI) | 17.1% | 2.01 [1.42, 2.84] | |
| Heterogeneity: \( \tau^2 = 0.11 \), \( \chi^2 = 161.15 \), df = 3 (\( P < 0.00001 \)), \( \Gamma = 98\% \) Test for overall effect: \( Z = 3.95 \) (\( P < 0.0001 \)) |
| 1.1.4 Protein |
| [100] | 4.7% | 2.05 [2.02, 2.07] | |
| Subtotal (95% CI) | 4.7% | 2.05 [2.02, 2.07] | |
| Heterogeneity: Not applicable Test for overall effect: \( Z = 120.42 \) (\( P < 0.00001 \)) |
| 1.1.5 Tocopherols |
| [104] | 4.4% | 0.84 [0.72, 0.98] | |
| Subtotal (95% CI) | 4.4% | 0.84 [0.72, 0.98] | |
| Heterogeneity: Not applicable Test for overall effect: \( Z = 2.28 \) (\( P = 0.02 \)) |
| Total (95% CI) | 100.0% | 1.54 [1.33, 1.78] | |
| Heterogeneity: \( \tau^2 = 0.12 \), \( \chi^2 = 6651.39 \), df = 21 (\( P < 0.00001 \)), \( \Gamma = 100\% \) Test for overall effect: \( Z = 5.81 \) (\( P < 0.00001 \)) Test for subgroup differences: \( \chi^2 = 205.17 \), df = 4 (\( P < 0.00001 \)), \( \Gamma = 98.1\% \) |

Fig. 1. Forest plot for random-effects meta-analysis of extraction yield: LFUS-assisted extraction vs. a similar control group of non-US-assisted extraction or vs. traditional extraction. The projection of each point on the abscissa axis represents, if higher than 1, the \( n \) of an \( n \)-fold increase in the extraction yield.
review focused on the effect of LFUS on key cereal and pseudocereal processes like hydration, germination and fortification is not available. Additionally, we summarize as forest plots the effect of LFUS on the extraction of bioactive compounds from cereal and pseudocereal by-products. Finally, we report and discuss the influence of LFUS on structural changes of starch, protein, and dietary fibre.

2. Methods

2.1. Research and selection criteria

Literature research from 1994 to 2022 was carried out on Scopus and Web of Science databases. The keywords used were Ultrasound OR Ultrasonic followed by common or Latin name of each cereal and pseudocereal (i.e., Wheat, Rice, Corn or Maize, Barley, Rye, Oat, Sorghum, Teff, Triticale, Millet, Quinoa, Amaranth, Buckwheat, and Chia). All articles concerning the application of low-frequency ultrasound to cereals and pseudocereals, or to derived ingredients, aimed at improving processing, increasing yield, or determining a modification in their chemical and technological behaviour were considered. Sources which presented LFUS as an ameliorating technique but without providing control trials were considered biased and were excluded.

2.2. Statistical elaboration

On two occasions the results were summarized through meta-analysis by creating forest plots with the software RevMan v5.4.1 (https://www.cochrane.org).

For Fig. 1, the effect size was standardized by computing log response ratios and standard errors as illustrated by Borenstein et al. [14]:

\[
\ln R = \ln (\bar{X}_1) - \ln (\bar{X}_2)
\]

\[
SE_{\ln R} = \sqrt{\frac{S^2_{\text{pooled}}}{n_1 (\bar{X}_1)^2} + \frac{1}{n_2 (\bar{X}_2)^2}}
\]

When the studies provided multiple non-independent outcomes the effect size was computed as their mean log response ratio, while the variance was determined as follows [14]:

\[
\text{var} \left( \frac{1}{m} \sum_{i=1}^{m} Y_i \right) = \left( \frac{1}{m} \right)^2 \sum_{i=1}^{m} V_i + \sum_{i=1}^{m} \left( r_{ij} \sqrt{V_i} \sqrt{V_j} \right)
\]

where \( m \) is the number of correlated variables and \( r \) is the correlation coefficient; when not calculated, \( r \) was cautiously assumed to be 1, resulting in a lower weight of the study. The data were plotted with the generic inverse variance method by RevMan, which provides automatic antilogarithm.

For Fig. 2, the effect size (i.e., the raw mean difference) and standard error were computed as described by Borenstein et al. [14]:

\[
D = \bar{X}_1 - \bar{X}_2
\]

\[
SE_D = \sqrt{\frac{S^2_1 + S^2_2}{n_1}}
\]

3. Low-frequency ultrasound application in cereals and pseudocereals processing

Because of ease of utilization, energy-saving, and relatively low costs, high-power LFUS has been proposed for processes as different as analysis, extraction, chemical and technological properties modification, emulsification, drying, freezing [15] and even microbial decontamination [16]. In the cereals area, the research is focused mainly on the effects of LFUS on physical and chemical changes of proteins [17–20] and starch [21,22], enzymatic activity [23], antioxidant compounds retrieval [24] and biofortification [25–27], hydration and germination [11,28–30] as well as food technological and sensorial quality improvement [17,31–34].

3.1. Hydration

Hydration is essential for many processes, such as cooking, extraction, fermentation, germination and malting [35]. During kernels hydration, the water uptake follows preferential paths, according to grain shape and structure. For instance, in barley caryopses the water penetrates through the hilar fissure and the micropyle, while in maize kernels...
enters by the tip cap, filling the empty space between germ and endosperm [29,36].

Several studies suggest that LFUS treatments enhance hydration. Miano et al. [37] proposed two different mechanisms: a) direct, related to inertial flow and sponge effect, where the ultrasound-induced cavitation creates a compression-rarefaction turnover that squeezes and releases the matrix, pumping water through pre-existing pores; and b) indirect, leading to the formation of new micro-channels because of physical damage to the tissues. However, low water activity does not allow cavitation, hence dry caryopses (a\textsubscript{w} ~ 0.65) undergo a slow hydration [37]. In fact, new cavities begin to form in the matrix only when an adequate a\textsubscript{w} is reached, accelerating the hydration process. For the above-mentioned reason, LFUS treatments are more effective when applied on pre-soaked kernels [38]. The relative extent of direct and indirect effects on the kernels varies according to the species [29]. Generally, cereals hydration kinetics exhibit a downward concave curve with one or two steps [35] that can be modelled by the Peleg model [39]:

where $M_t$ is the moisture (% dry weight) at t time, $M_0$ the initial moisture, $k_1$ and $k_2$ are Peleg’s constants. The $k_1$ is equal to the inverse of the initial moisture uptake rate and the $k_2$ is inversely related with equilibrium moisture.

As an alternative the Weibull model, an exponential empirical model useful for its simplicity and good accuracy in describing complex processes with high variability, may be used. [11]:

where $M_{eq}$ is the equilibrium moisture, $\beta$ the scale parameter and $\alpha$ the shape parameter; $\alpha$ describes the initial water uptake behavior and $\beta$ represents the time needed to achieve 63% moisture; both parameters are inversely related to the process rate [40]. The parameter $\alpha$ is related to moisture migration during hydration: when $\alpha > 1$ the process is governed by internal moisture diffusion as well as external mass transfer, while when $\alpha < 1$ the external mass transfer is negligible [11].

Both Peleg and Weibull models have been used to model the hydration kinetic of wheat treatment with LFUS [11]. The LFUS technology accelerates the hydration process by increasing the hydration rate and reducing the lag phase, contributing to reach a higher final moisture. Li et al. [41] examined the initial 120 min of rice water uptake and observed that ultrasounds hastened the maximum absorption rate in a power-dependent manner and that the moisture absorption rate increased according to a Peleg-like curve. Miano et al. [29] reported a 300 min drop in hydration time for flint maize kernels, albeit no new cavities were formed because of their extremely vitreous endosperm, while Patero and Augusto [42] observed a decrease from 320 to 190 min in sorghum kernels. The combination of LFUS and temperature may further improve these results. Kalita et al. [28] compared paddy rice hydration by soaking and LFUS-assisted soaking at different temperatures and noticed that the process was abridged from $> 24$ h (traditional) to 3 h (LFUS). Similarly, Guimarães et al. [11] observed that LFUS per se shortened wheat hydration time by 28–42%, while the combination of LFUS and temperature (25 °C) cut it by 72%. Patero and Augusto [42] determined that the temperature (53 °C) had a greater effect than LFUS on sorghum hydration, and a similar result was obtained by Shafaei et al. [43] in wheat at different temperatures (from 30 °C to 70 °C). Nevertheless, high temperatures may have relevant drawbacks, including protein denaturation, starch gelatinization or industrial plant insulation costs. Moreover, the increase of processing temperature above 60 °C reduces cavitation, because the amount of water vapor inside the bubble increases and a collapse occurs [8,44]. Hence, a 35–40 °C range is generally appropriate to accelerate the process without damaging seed properties [36]. In barley malt production, the combination of LFUS and mild temperatures (20–25 °C) accelerates the steeping phase; the LFUS intensity affects water absorption mainly in the early phase (Pelec’s $k_1$), while the temperature has a stronger effect on higher final moisture. Overall, their combination reduces the hydration time by half [45] or even more [36]. Temperatures above 40 °C worsen malt quality, therefore LFUS represents a promising approach to reduce steeping time; additionally, the LFUS mechanical power is dissipated as heat, reducing the energetic costs.

3.2. Germination

Germination is the sum of events that break the seed quiescence status and allow the embryonic axis to appear. As a first step, the seed hydrates so the pre-existent enzymes are activated and initiate the Krebs cycle or, in rice, even anaerobic pathways, the endosperm reserves are mobilized, and the protein synthesis becomes intensive. The germination ends with cells elongation, that leads to root and shoot emission [46].

From the point of view of food sciences, the activation of dormant enzymes during germination leads to significant changes in biochemical and nutritional characteristics. The $\alpha$- and $\beta$-amylases rapidly degrade the carbohydrates, with a consequent surge in reducing sugars, while other enzymes decompose cell walls and enhance the accessibility of internal nutrients [47]. The proteins are hydrolyzed, increasing peptides and amino acids availability [47]. Different bioactive compounds, such as tocols, thiamine, riboflavin, folic acid, vitamin C and carotenoids, are biosynthesized to generate the nutrients necessary for seedling growth [47,48]. The metabolic activities fuel phenolic compounds biosynthesis [49,50], while the degradation of cell walls leads to an increase of readily available free phenolic compounds [51]. The abundant presence of bioactive molecules boosts the antioxidant capacity [52]. Furthermore, sprouting increases phytase activity, leading to phytic acid degradation and better micronutrients absorption in the gastrointestinal tract [47,53]. Overall, controlled germination improves the nutritional composition of the kernels, but the enzymatic activity has a negative impact on some technological properties of the flours (e.g., leavening), stressing the importance of a carefully controlled process to avoid excessive hydrolysis [47].

US, together with high pressure, cold plasma, and pulsed electric fields, is an emerging technology used to regulate seeds germination [30]. The LFUS treatment enhances germination primarily by its positive effect on hydration. In fact, cavitation appears to cause fissures in the pericarp, augmenting the availability of water and oxygen [54,55]. The absorbed water stimulates the embryo to release gibberellic acid, a chemical promoter of germination [55]; at the same time, the hydration promotes the leakage of germination inhibitors, such as the abscisic acid [46]. With regards to other phytohormones, Wei et al. [56] observed that LFUS decreased the indole-3-acetic acid (IAA)/cytokinin ratio in Dendrobium officinale protocorms. IAA is a root growth promoter while cytokinin stimulates shoot growth [46], therefore a higher IAA presence may lead to earlier germination. Moreover, LFUS probably acts facilitating the mobilization of endosperm nutrients by disrupting cell membranes [55], as corroborated by the sonication-induced erosion at the joint between cells observed by Ananthakrishnan et al. [57], which would stimulate a faster flow of water and nutrients. Finally, Chen et al. [58] documented that LFUS-treated wheat seeds exhibited greater antioxidant activities of catalase, superoxide dismutase and glutathione reductase. Apparently, reactive oxygen species (ROS) generated by cavitation elicit an antioxidant response that enhances plant vigor. Other improvements were found in number of germinated seeds, protein and total chlorophyll content, shoot length, fresh and dry biomass, and levels of cell damage indicators [58].

Although the mechanism that induces faster germination is not fully understood, numerous observations have been collected (Table 1). Ding et al. [54] found that LFUS improves rice sprout growth speed by 22.3–26.9%, Xia et al. [30] reported that an additional 10–15% of rice
seeds sprouted in the initial 32 h, while Goussous et al. [59] described an enhanced wheat germination rate of about 60% compared to plain water soaking; in addition, a positive interaction between LFUS and temperature was found. Similarly, Yaldagard et al. [55] observed that LFUS reduced barley steeping time from the usual 46 h to 25–30 h, depending on the applied intensity, and that the percentage of germinated seeds increased from 93.3% (control) up to 99.4% in the most intensely treated group. Furthermore, the hair roots were luxuriant and, at the highest intensity, the germination period was shortened from 7 to 4 days. A slight increase in barley germinated seeds was observed also by Miano et al. [60] and was attributed to porosity increment, since plastic bags insulated the seeds from the water during the sonication. Similarly, Hassan et al. [61] observed that 5 min LFUS treatment greatly increased the number of germinated sorghum grains from 78% (control) to 94%; a longer process decreased the germinated seeds, therefore they inferred that at high amplitude the treatment damaged cells and/or enzymes. Kratovilav et al. [62] studied LFUS application to different cereals and noticed significant effects on coleoptile and mesocotyl elongation. Oat and rye caryopses were very sensitive to LFUS stimulation (+119% and +65% growth, respectively), while triticale and wheat showed smaller increases. In a comparison among different pre-treatment, LFUS proved to be better than microwaves or heat in enhancing buckwheat germination by 4–4.5% [63].

Beyond the described effect, sonication before or during germination in rice and wheat appeared to increase the synthesis of γ-aminobutyric acid, a health-enhancing compound, by 1.7 and 3-fold respectively [64,65].

### 3.3. Extraction

The most popular LFUS application is improving the extraction of different compounds. Table 2 summarizes a variety of LFUS-assisted extraction trials with their respective optimized experimental conditions. Fig. 1 reports a forest plot for random-effects comparisons. In a comparison among different pre-treatment, LFUS proved to be better than microwaves or heat in enhancing buckwheat germination by 4–4.5% [63].

An overall pooled increase of 54% in yield is achieved by implementing LFUS. Extraction of phenolic compounds, especially from by-products and waste materials, was the most studied process. Although in some cases yield improvements are negligible, other advantages must be considered. In fact, LFUS-assisted extraction generally allows to shorten the extraction period, to employ food-grade non-hazardous solvents and to use lower temperatures. For instance, in Balasubramaniam et al. [66] experiments, although yields were similar, the phenolic compounds extraction from millet was performed in half the time (30 vs. 60 min) and at lower temperature (50 vs. 60 °C). Izadifar [67] found that a 30 s sonication increased the extracted phenolics content from wheat by 14.3%. Further reductions in time were reported by Wang et al. [68], from 15 h of Soxhlet extraction to 25 min; Giopato Viel et al. [69], 5 min instead of 10; Teslić et al. [70], 30 min instead of 24 h, with 11% higher yield; Chen et al. [71], 32.5% higher yields in half the time; Melini and Acquistucci [72], 15 min instead of 1 h. As reported by Chen et al. [73], even though the highest yields were achieved at high temperature (70 °C), at 20 °C LFUS extracted in 5 min 54% more phenolics than a 65 min control trial. Therefore, LFUS represents a strategy to perform shorter low-temperature extractions and deserves to be introduced in analytical protocols to ensure correct quantification of phenolics [74].

LFUS-assisted extraction in some cases can efficiently use ethanol in place of chlorinated methanol [66,71]. On the other hand, a certain amount of methanol contributes to lower the average viscosity of solvent mixture, thus facilitating cavitation [69]. In addition, with LFUS, green new developed deep eutectic solvents (DESs) may substitute or outperform the traditional ones. DES was 13% more effective than 30% ethanol in extracting ferulic and sinapic acid from corn silk [75] and extracted phenolic compounds from wheat bran better than 60% EtOH (+33%) and alkaline hydrolysis (+71%) [76]. Besides, properly formulated DESs can be compatible with HPLC as dilution solvent [77].

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LFUS ability at improving extraction is probably due to cavitation-driven cellular damage (especially cell walls), particle size reduction, strong mixing, increase in porosity and in specific surface area. These power- and time-dependent events allow the solvent to easily access tissues and dissolve phenolic compounds [67,72,76,78]. In enzyme-assisted extraction, cavitation leads to higher available surface for enzyme digestion [78]. Giopato Viell et al. [69] suggested that part of extracted flavonoids from tef could come from release of bound fraction because of cavitation, while Chen et al. [73] inferred that at

| Sample      | Device       | Frequency (kHz) | Nominal power (W) | Amplitude (%) | Volume (L) | Specific power (W/L) | Time (min) | T (°C) | Reference |
|-------------|--------------|----------------|-------------------|---------------|------------|----------------------|------------|--------|-----------|
| Barley      | Bath         | 37             | 154               | 5.7           |            | 30-480               | 35, 40     |        | [36]      |
| Barley      | Bath         | 20             |                   | 28            |            | 240                  |            |        | [60]      |
| Buckwheat   | Bath         | 300            |                   |               |            | 30                   | 29         |        | [63]      |
| Corn        | Bath         | 25             | 300               |               | 4           | 41                   | 180–300    | 29     | [29]      |
| oat, rye, triticale, wheat | Bath | 30–40         | 300               | 2             | 2          | 15                   | 25         | 62     | [62]      |
| paddy rice  | Bath         | 35             | <225              | 50            | 10-120     | 25-40                |            |        | [28]      |
| paddy rice  | Bath         | 40             | 150–600           |               |            | 10-120               | 4          | 41     | [41]      |
| rice        | Bath         | 40             | 150–600           | 28            | 120        |                      |            |        | [37]      |
| sorghum     | Bath         | 40             |                   | 26            | 30         | 25; 53               |            |        | [42]      |
| wheat       | Bath         | 45             | 160               | 8             |            | 5-20                 |            |        | [58]      |
| wheat       | Bath         | 40             | 100               |               |            | 5-60                 | 25         |        | [59]      |
| wheat       | Bath         | 25; 40         | 360–480           | 10            |            | 30-70                |            |        | [43]      |
| barley      | Probe        | 20             | 750–1500          | 1             | 51.1; 84.7 | 30–270               | 10-25      |        | [45]      |
| barley      | Probe        | 20             | 460               | 20-60         | 0.08       | 5-15                 | 30         |        | [55]      |
| rice        | Probe        | 25             | 2000              | 125           | 5          | 23; 24               |            |        | [54]      |
| sorghum     | Probe        | 20             | 750               | 40; 60        | 0.5        | 5; 10                | 35         |        | [61]      |
| wheat       | Probe        | 20             | 500–1500          | 1             | 61.5; 83.6; 102.4 | 15–25      |            | [11]      |
| wheat       | Probe        | 22             | 227 W/L           |               |            | 3                    |            |        | [65]      |
| rice        | transducer box x2 | 25       | 16 W/L            | 152           |            | 5                    | 23–24      |        | [64]      |
| rice        |              | 28             | 400               |               |            | 5–30                 |            |        | [30]      |

* Determined by the calorimetric method.
Table 2
Optimized experimental conditions and yields (mean ± SD) of LFUS-assisted extraction. Experiments marked with asterisk employed LFUS along with another major technique or lasted longer than the net LFUS treatment time.

| Raw material               | To be extracted | Device | Power (W) | Amp. (%) | Time (min) | T (°C) | Extraction medium | Ratio (ml/g) | Yield (mg/g) | Unit | Reference |
|----------------------------|-----------------|--------|-----------|----------|------------|--------|-------------------|-------------|-------------|------|-----------|
| barley flour               | total phenolics | bath   | 200       | 20       | 50         | 97 %   | ethanol/acetone/water 7:7:6 | 37          | 24.76 ± 0.15 | mg/g | [107]     |
| barley flour               | phenolic acids  | bath   | 200       | 18       | 50         | 100 %  | ethanol               | 60          | 19.65 ± 0.09 | mg/g | [107]     |
| hull-less barley seeds     | total phenolics | bath   | 2x10      | 20       | 50         | 80 %   | choline chloride/ triethylene glycol 1:4 | 50          | 21.1 ± 1.2   | mg/g | [77]      |
| buckwheat sprouts          | flavonoids      | bath   | 700       | 40       | 56         | 80 %   | ethanol/acetone/water 7:7:6 | 10          | 173         | mg/g/100 g | [73]      |
| oat bran                   | total phenolics | bath   | 600       | 15       | 70         | 80 %   | ethanol/acetone/water 7:7:6 | 10          | 70.3 ± 0.5   | mg/g/100 g | [108]     |
| hull-less oat seeds        | total phenolics | bath   | 2x10      | 20       | 80 %       | 80 %   | ethanol/acetone/water 7:7:6 | 20          | 236.37 ± 5.26 | mg/g | [74]      |
| black quinoa               | total phenolics | bath   | 2x10      | 20       | 23         | 76.6 % | choline chloride/1,4-butenediol 1:6 | 27          | 9.3         | mg/g | [75]      |
| purple rice bran           | total phenolics | bath   | 230       | 23       | 36         | 23.8 % | ethanol (pH 2.5)         | 20          | 1978 ± 101 | mg/g | [109]     |
| purple rice bran           | phenolic acids  | bath   | 230       | 16       | 31.7       | 31.2 % | ethanol              | 20          | 2232 ± 115  | mg/g | [109]     |
| black rice husk            | total phenolics | bath   | 10        | 49.5     | 67.3 %     | 67.3 % | ethanol              | 40.8        | 1.72       | mg/g | [110]*    |
| black rice husk            | flavonoids      | bath   | total     | 49.5     | 67.3 %     | 67.3 % | ethanol              | 40.8        | 3.01       | mg/g | [110]*    |
| black rice husk            | anthocyanins    | bath   | 10        | 49.5     | 67.3 %     | 67.3 % | ethanol              | 40.8        | 3.36       | mg/g | [110]*    |
| wild rice flour            | flavonoids      | bath   | 200       | 51.2     | 76.6 %     | 76.6 % | choline chloride/1,4-butenediol 1:6 | 30          | 189.2      | mg/g/100 g | [108]     |
| rye seeds                  | total phenolics | bath   | 2x10      | 20       | 53 %       | 53 %   | ethanol/acetone/water 7:7:6 | 30          | 49.74 ± 0.88 | mg/g | [111]     |
| rye seeds                  | phenolic acids  | bath   | 2x10      | 20       | 45         | 80 %   | glycerol/citric acid/glucose 4:1:1 mol/mol/mol in water (pH 2.9) | 30          | 49.4       | mg/g | [108]     |
| wheat bran                 | phenolic acids  | bath   | 120       | 40       | 50         | 80 %   | glycerol/citric acid/glucose 4:1:1 mol/mol/mol in water (pH 2.9) | 30          | 8.7 ± 0.9  | mg/g | [76]*     |
| wheat germ                 | total phenolics | bath   | 120       | 40       | 50         | 80 %   | glycerol/citric acid/glucose 4:1:1 mol/mol/mol in water (pH 2.9) | 30          | 94.6 ± 3.0 | mg/g | [76]      |
| wheat germ                 | phenolic acids  | bath   | 120       | 40       | 50         | 80 %   | glycerol/citric acid/glucose 4:1:1 mol/mol/mol in water (pH 2.9) | 30          | 49.4       | mg/g | [108]     |
| teff seeds                 | flavonoids      | bath   | 120       | 40       | 50         | 80 %   | glycerol/citric acid/glucose 4:1:1 mol/mol/mol in water (pH 2.9) | 30          | 8.7 ± 0.9  | mg/g | [76]*     |
| teff seeds                 | anthocyanins    | bath   | 120       | 40       | 50         | 80 %   | glycerol/citric acid/glucose 4:1:1 mol/mol/mol in water (pH 2.9) | 30          | 94.6 ± 3.0 | mg/g | [76]      |

(continued on next page)
| Raw material          | To be extracted     | Device          | Power (W) | Amp. (%) | Time (min) | T (°C) | Extraction medium                     | Ratio (ml/g) | Yield (%) | Unit     | Reference |
|-----------------------|----------------------|-----------------|-----------|----------|------------|--------|----------------------------------------|---------------|-----------|----------|-----------|
| tartary buckwheat     | flavonoids           | 2x5 (30/10 s on/off) | 200       | 21       | 60         | 72% methanol | 250             | 3.94 ± 0.62 | g/100 g  | [117]     |
| red rice bran         | anthocyanins         | 400             | 55.2      |          |            |        | acidified ethanol 78.37 % (pH 2.3)    | 17.5          | 5.51      | mg/g     | [118]     |
| corn silk chia seeds  | flavonoids           | bath            | 500       | 21.5     | 60         | 33.75% ethanol | 20             | 1.13      | g/100 g  | [119]     |
| corn germ             | oil                  | bath            | 176       | 40       | 50         | 12     | ethyl acetate                         | 12.71 ± 0.08  | 66.25 ± 0.77 | % recovery | [85]     |
| rice                  | oil                  | bath            | 123       | 37       | 42         |        | cellulase and α-amylase in water      | 10            | 76.93 ± 0.52 | % recovery | [87]     |
| rice bran             | oil                  | bath            | 100       | 60       | 25         |        | n-hexane                              | 5             | 20.35      | g/100 g  | [121]     |
| rice bran             | oil                  | bath            | 300       | 30       | 45         |        | water (pH 12)                         | 12            | 17.2       | g/100 g  | [84]     |
| rice bran             | probe                | 93              | 26 (5/5 s on/off) | 35 | ethanol   | 6      | water                                  | 10            | 9.0 ± 5.5   | g/100 g  | [86]     |
| rice bran             | oil                  | bath            | 160       | 40       | 40         |        | supercritical CO₂ 14.82 g/min water   | 32            | 12.65      | g/100 g  | [88]*     |
| wheat chaff           | xylo-oligosaccharides| bath            | 500       | 25       | 10         |        | 0.1 mg/g ammonium sulfate              | 34            | 16.02 ± 0.74 | mg/g     | [89]     |
| wheat chaff           | xylo-oligosaccharides| bath            | 500       | 25       | 10         |        | 4.5 g/l endoxylanase                   | 20            | 142.6 ± 1.7 | mg/g     | [90]*     |
| wheat bran            | arabinoxylan         | bath            | 180       | 70       | 50         |        | 2 M KOH                                | 12            | 56.2 ± 1.2 | g/100 g  | [91]     |
| hull less barley      | flour                | probe           | 99        | 48       | 50         |        | water (pH 5)                           | 10            | 3.87       | g/100 g  | [96]     |
| enzyme free barley    | flour                | probe           | 400       | 16       | 55         |        | 55 % NaOH                              | 10            | 65.6 ± 1.2 | % recovery | [92]     |
| brewer's spent grain  | arabinoxylan         | probe           | 750       | 10       | 50         |        | 2 M KOH                                | 25            | 20.3 ± 0.4  | g/100 g  | [95]*     |
| corn cob              | xylan                | probe           | 200       | 70       | 10         |        | 5 % NaOH                               | 25            | 36.8       | g/100 g  | [90]*     |
| corn bran             | arabinoxylan         | probe           | 500       | 70       | 25         |        | 50 % NaOH                              | 10            | 27.78 ± 0.17 | g/100 g  | [97]     |
| dried corn silk       | polysaccharides      | 250             | 17        | 56       |            |        | water                                  | 20            | 6.02 ± 0.02 | g/100 g  | [98]     |
| wheat bran            | heteroxylans         | probe           | 100       | 35       | 40         |        | 55 % NaOH                              | 30            | 25.5       | g/100 g  | [94]     |
| de waxed wheat straw  | hemicellulose        | probe           | 100       | 35       | 5          |        | 0.5 KOH                                | 15            | 45.6       | g/100 g  | [91]*     |
| chia seeds            | hetero-poly saccharides| protein   | 400       | 40       | 60 (1/1 s on/off) | 50 | water (pH 9)                           | 30            | 10.39 ± 0.57 | g/100 g  | [93]*     |
| quinoa                | bath                 | 320             | 20        | 25       |            |        | water buffered pH 9                    | 5             | 4.10 ± 0.18 | g/100 g  | [101]    |
| rice dreg             | protein              | probe           | 448       | 20       | 10/6 (s on/off) | 50 | 0.08 M NaOH                            | 20            | 88.44 ± 0.40 | % recovery | [100]    |
| defatted wheat germ   | protein              | 363             | 24 (2.4/2 s on/off) | 38 | Na-docusate/isoctane/KCl reverse micelles in water | 6             | 213.46 μmol/(min g) | | [102]    |
| corn meal             | carotenoids          | probe           | 900       | 38       | >60        |            | 50 mM Na carbonate phosphate pH 8     | 5.3           | 213.46      | μmol/(min g) | [103]    |
| corn gluten meal      | zeaxanthin           | bath            | 250       | 56       | 45         | 95% ethanol                         | 7.9           | 212 ± 18 | μg/g     | [122]    |
| corn gluten meal      | lutein               | bath            | 250       | 56       | 45         | 95% ethanol                         | 7.9           | 185 ± 18 | μg/g     | [122]    |
| malted barley flour   | α-amylase            | probe           | 200       | 25       | 20 (5/5 s on/off) | 30 | 50 mM Na carbonate phosphate pH 8     | 5.3           | 213.46      | μmol/(min g) | [103]    |
| quinoa seed hulls     | betacyanins          | probe           | 70        | 9.2 x (0.6 cycle) |            |        | water                                  | 100           | 96.5       | % recovery | [104]    |
| quinoa seed hulls     | betaxanthins         | probe           | 90        | 40 x (0.7 cycle) |            |        | water                                  | 100           | 201 ± 101 | mg/100 g wb | [103]    |
| rice bran             | γ-oryzanol           | probe           | 500       | 40       | 40         | 45       | soybean oil                            | 5             | 493 ± 44 | μg/g oil | [104]    |
| rice bran             | α-tocopherol         | probe           | 500       | 40       | 40         | 45       | soybean oil                            | 5             | 139 ± 18 | μg/g oil | [104]    |
| rice bran             | γ-tocopherol         | probe           | 500       | 40       | 40         | 45       | soybean oil                            | 5             | 212 ± 31 | μg/g oil | [104]    |
| rice bran             | δ-tocopherol         | probe           | 500       | 40       | 40         | 45       | soybean oil                            | 5             | 247 ± 23 | μg/g oil | [104]    |
| red rice seeds        | melatonin            | probe           | 200       | 40       | 10 (0.2 cycle) | 40 | 50% methanol in water pH 3.5          | 2.5           | 72.67 ± 1.46 | % recovery | [124]    |
| red rice seeds        | tryptophan and       | probe           | 200       | 30       | 5 (0.7 cycle) | 30 | 8% methanol in water pH 3             | 5             | 100 ± 5   | % recovery | [125]    |
| sorghum husk          | derivatives biocolorants | probe   | 360       | 55       | 20 (2/2 s on/off) |            |        | acidified ethanol/water 70/30         | 30            | 16.7 ± 0.6 | g/100 g  | [105]    |
70 °C heat-led cleavage of glycosidic bonds could have freed phenolics from bound forms.

Nevertheless, a LFUS overtreatment may worsen the extraction because of phenolics oxidation or destruction [67,79] due to temperature increase [67] and radicals generation [78,80]. According to Dzah et al. [81], although above 65 °C the phenolic molecules are degraded by hydrogen peroxide and their antioxidant activity decreases, the sonication time has not a direct impact on them.

Improving oil extraction is another LFUS application. In a study by Cravotto et al. [82], alkaline aqueous extraction with LFUS support outperformed hexane, resulting in 22% higher yield. The extraction time was also cut by 8-fold (4 h to 30 min). Additionally, in the presence of LFUS rice wax was hydrolyzed to policosanols mixture under milder temperature and alkali concentration [82,83]. Khoei and Chekin [84] tested LFUS as pre-treatment in aqueous extraction carried out at 45 °C and pH 12 for 15 min, and achieved an 20% yield, similar to a Soxhlet extraction (23.4%) which, nevertheless, used hexane. In addition, the small Soxhlet extraction surplus in yield appeared linked to free fatty acids content, 3.2% in hexane-extracted oil vs. almost zero in aqueous-extracted oil. It is suggested that the aqueous extraction is selective against free fatty acids, Han et al. [85] confirmed that LFUS, being more efficient than steam and heat, could be a viable pre-treatment also in enzyme-led aqueous extraction. In Krishnan et al. [86] experiments, LFUS-assisted extraction of oil with ethanol achieved a yield 29% higher compared to the traditional process with hexane, and 78.5% higher compared to non-US ethanol extraction. Additionally, no changes in oil composition or modification in peroxide value were found [86,87]. Therefore, a green solvent like ethanol could be conveniently used in oil extraction. By implementing a LFUS phase in their supercritical CO2 extraction, Soares et al. [88] improved the yield by 27% and cut by 60% the time, while extracting four oryzanol precursors, campesterol, β-sitosterol, stigmasterol and 4-methylene cycloartenol.

As mentioned, sometimes LFUS over-treatment may lead to poor performances. According to Xu et al. [87], a power excess lowers yields since cavitation bubbles act as hindrance for wave propagation, while too long a treatment increases the quantity of suspended impurities and worsens solvent penetration. An over-treatment could also result in lipids emulsification, hence lower extraction yield [84]. Lastly, Khoei and Chekin [84], Han et al. [85] and Xu et al. [87] pointed out the cushioning effect as one of the major factors preventing yield enhancement by raising temperature.

Polysaccharides are a third class of compounds whose LFUS-assisted extraction has been studied. Dordevic and Antov [89] developed a protocol to extract at the same time xylo-oligosaccharides and phenolic compounds from wheat chaff, and the LFUS treatment improved by 2 and 1.3-fold the respective yields. In xylan extraction from corn cob, a 10 min LFUS pre-treatment at 70 °C could substitute the traditional one at 95 °C for 1 h [90]. In a more recent work, Hromadkova et al. [91] confirmed that, thanks to LFUS implementation, heteroxylans extraction from wheat bran could be hastened by 55 min and with minor yield loss. Successively, Benito-Roman et al. [92] found that LFUS-assisted extraction of β-glucans from barley outperformed the stirred tank technique by improving yield up to 58% and hastening the processing time from 3 h to 16 min. Conversely, Sun and Tomkinson [93] found a negligible increase in hemicellulose extraction yield from wheat straw. Wang et al. [94] optimized the extraction of mucilage (i.e., hetero-polysaccharides) from chia seeds and observed that the adoption of LFUS as pre-treatment accelerated the extraction yield.

Besides yields, LFUS proved to be energy-efficient and timesaving. Reis et al. [95] designed a 25 min-long LFUS-assisted extraction from brewer’s spent grain that yielded the same amount of arabinoxylan they got with a 7 h optimized alkaline extraction. In another case the LFUS-assisted extraction of β-glucan from hull-less barley gave a 6% lower yield, but was still convenient because lasted 5 min instead of the standard 90 min [96]. Shorter times often allow to save energy because heating is needed for a briefer period. According to Benito-Roman et al. [92], LFUS could cut energy demand by at least 52%.

The yield loss, in case of over-treatment, seems to be the main LFUS drawback [97–99]. Although the most drastic ultrasound conditions resulted in lower polysaccharides molecular weight, due to cavitation-driven chain-breaking, experimental parameters could be adjusted to minimize unwanted depolymerization [90,92]. In addition, at the highest amplitude, unspecific disruption of cell compartments results in different polysaccharides release, thus threatening the extract purity [96].

As detailed in the last rows of Table 2, LFUS-assisted extraction was tested for a variety of other compounds as well. Protein can be extracted efficiently with LFUS: Li et al. [100] reported a 2-fold increase in yield, thanks to better solvent penetration. Similarly, Quintero-Quiroz et al. [101] saw a 2.4-fold higher yield, while Zhu et al. [102] stated that LFUS improved forward mass transfer in reverse micelles extraction. Laquívela et al. [103] extracted betalains from quinoa seed hulls in 10–40 s instead of 10 min. Lopipimai et al. [104] developed a LFUS-assisted soybean oil enriching process: the oil was directly employed as green solvent to simultaneously extract tocopherols and γ-oryzanol from rice bran; the yields were slightly lower than with conventional extraction, but this technique simplified the process and avoided the use of hazardous solvents. Wizi et al. [105] recovered 3.6-fold higher red colorants, mainly apigeninidin and luteolinidin, from sorghum husk by coupling ultrasound and microwave technologies. Ye et al. [106] extracted carotenoids from corn meal and observed that LFUS were better than magnetic stirring, inasmuch that after 60 min they achieved 0.08 mg/ml vs. 0.004 mg/ml. However, the experiment did not last enough to find out the optimum conditions.

3.4. Fortification

Because of its capacity to produce cracks and pores, LFUS has also been tested as a method to fortify grains. Bonto et al. [25] treated polished white rice in a 53 Hz ultrasonic bath: a time-dependent fragmentation of the cells external layer was observed, and the starchy endosperm arrangement was disrupted, but no starch granules were damaged. Although at first sonication led to complete B-vitamins loss, after soaking in pantothenic acid the LFUS-treated grains absorbed and retained 140% more vitamin B6 than non-sonicated rice. Similarly, Tizzon et al. [27] fortified rice by soaking it in 800 ppm folic acid solution after 5 min-long sonication. Brown rice absorbed about 1982-fold its natural folic acid content, while a 4054-fold increase was seen in white rice; in addition, after washing and cooking, they retained 93.5% and 86.5% folic acid, respectively. Yanova et al. [126] attempted mineral fortification of barley and oat grains by LFUS treatment with 65 mg/L solutions of Fe2+ and Zn2+. A positive linear relationship between amount of absorbed minerals, temperature and treatment duration was found; furthermore, at higher ultrasound frequency an additional amount of iron and zinc was soaked up, possibly because of the higher number of impingement cycles. In must be stressed that higher frequencies are less likely to produces grains fractures because cavitation collapses are less violent [1].

3.5. Other applications

Cui et al. [32] and Dang et al. [127] suggested LFUS as a viable alternative to reduce brown rice cooking time by about 16%, with the additional advantage that less vitamins and other solids are lost; the LFUS pre-treatment resulted also in higher grain expansion volume, water uptake and softness. The rice cooking time reduction was confirmed by Yang et al. [128]. In addition, the glycemic index was subjected to negligible changes with respect to untreated brown rice [127,129]. LFUS washing at acidic pH improved rice bran quality by reducing lipase and lipoygenase activities, heavy metals contaminants, phytic acid and coliforms [130]. Habus et al. [131,132] confirmed that the shelf life of wheat bran can be extended with an ultrasound
treatment thanks to the reduction of the enzymatic activities of lipase, lipooxygenase and polyphenol oxidase. However, the effect is partly due to thermal denaturation from the heat generated, because when the sample was cooled the LFUS treatment appeared less effective than the conventional heating.

According to Yüksel and Elgün [33] submitting wheat to 30 s sonication during tempering should improve its bread-making quality, although the wet gluten amount was slightly diminished, its quality was better as higher gluten index, dough stability, energy, loaf volume and specific volume were observed. In addition, LFUS-assisted mixing may result in better air incorporation and thus higher loaf development [31]. Similarly, sonication during pre-mixing of corn bread dough resulted in better softness, porosity, general sensory acceptability and yellower crust and crumb [133]. Hence, LFUS treatment of wheat and quinoa flour suspension could produce tailored-made flours with defined rheological properties, such as decrease in gelatinization enthalpy, lower viscosities and lower gel hardness and cohesiveness [134,135].

The use of LFUS during corn nixtamalization cooking, reduced the steeping time needed to reach the correct kernel softness from 20 to 1 h; a slight inferior mass leaching was also observed [136]. A further study confirmed that LFUS reduces steeping time (from 18 to 1.5 h) and does not affect nixtamal quality as well as sensory acceptability of derived products like tortilla chips [17].

4. Effect of low-frequency ultrasound on cereals and pseudocereals components

4.1. Starch

Table 4 reports the broad range of different conditions tested for modifying cereal starches. Ultrasound treatments induce pores, depressions and cracks in starch granules because of the rapid water jets produced by the cavitation bubbles collapse. Yang et al. [137] even reported that rice starch granules were peeled off as power increased. However, LFUS augmented the total pores volume but not their average diameter [19] and affect mainly the largest granules [138,139]. Additionally, in the range 25–55 °C the temperature effect is inversely correlated to the damage [140] because the collapse of the bubbles favors cavitation but is less violent at higher temperature [1]. Conversely, the application of multiple frequencies is more effective due to the sum of cavitation events [141,142].

Boufi et al. [143] reported that LFUS ruptured starch particles into smaller ones: a 15 min treatment reduced both 1200 nm and 950 nm granules to 600 nm, while a 90 min process trimmed them down to 40 nm, a size reduction easily visualized by beam light scattering, because the starch suspension becomes clearer over the time. Similar observations were reported by Kang et al. [144] for waxy starches, but the amylose-rich samples underwent a slight particles diameter increase due to amylose aggregation, as observed also by Li et al. [145]. The correlation between granule size and degree of polymerization is not clear. For instance, Yang et al. [137] reported a decrease in particle size but no changes in chain-length. However, many studies describe a depolymerization process. According Kang et al. [144] and Li et al. [146], LFUS first disrupts weak interactions and then cleaves covalent C-O-C α-1,6 glycosidic bonds (apparently less stable than α-1,4 bonds) thus leading to amylpectin debouching [147]. Coherently, Li et al. [145] saw a roughly halved weight average molar mass (\(M_w\)) and Huang et al. [146] reported a drastic increase in hydrolysis degree. Furthermore, the number average molecular weight (\(M_n\)) and polydispersity (\(M_w/M_n\)) diminished with sonication time and their decreasing rate was related to temperature and power [149]. Due to these events, Zhou et al. [150] indicated LFUS as the best alternative to produce flavonoids-enriched starch complex from Tartary buckwheat. In addition, they saw an increase in resistant starch (+20%) and a slower starch digestion.

Swelling power and solubility were generally increased by LFUS [138–140,151–153] and the temperature-time interaction was positively correlated to these parameters [140]. A slight increase in suspension transparency was noticed by Sukja and Jamroz [139], Amini et al. [140] and Li et al. [154]. Jambrak et al. [151] observed that the sonicated suspension became clear after one-day storage. However, Dey and Sit [155] stated that LFUS turned starch 21% darker.

Fig. 2 reports the forest plot for random effects performed considering fourteen different studies related to LFUS effect on starch gelatinization enthalpy (\(\Delta H\)); the raw mean difference between the control and the LFUS-treated group was used as the effect size.

The overall pooled LFUS treatment causes a slight decrease (0.97 J/g) in \(\Delta H\), a tendency also observed by Amini et al. [140], Boufi et al. [143], Li et al. [145], Huang et al. [148], Zhou et al. [150] and Yu et al.
The decrease in T_H was related to the loss of amylopectin double helices, essential structures for granule integrity preservation [157]. Controlled-temperature LFUS treatments allow to obtain starches that demand lower energy when residual helical structures unfold [156]. The decrease in their disappearance could determine a temporary higher crystallinity, although an opposite behavior has been observed at very high power (600–1000 W) probably because small amounts of amylose leaked out from the granules and gelled, insulating the surface from external water [137,156].

These behavioral discrepancies may be explained by the different nature of starch granules: A-type granules are characterized by a tight monoclinic lattice, while B-type granules have a hexagonal arrangement enclosing a cavity with freezeable water. Consequently, A-type granules are more resistant, while B-types are more susceptible to LFUS-induced disruption [152,160], Yang et al. [137], Yang et al. [147] and Hu et al. [158] provided observations that support this crystallinity changes theory, Karwasra et al. [138], Hu et al. [142] and Luo et al. [152] did not observe any significant modification: probably, different experimental conditions (e.g., ultrasound power, time, volume treated, higher efficiency of the probe system with respect to bath) led to higher total energy per volume unit. In fact, conclusive evidence from Boufi et al. [143] showed that LFUS flattened thermogram and x-ray diffraction spectrum, thus supporting the formation of amorphous particles.

Because of LFUS-induced starch modification, the pasting properties of cereal starches and flours are also modified. LFUS treatment decrease starch paste peak viscosity, breakdown, and setback, but did not affect pasting temperature [141,145–149,152,154,161]. However, Cui et al. [32], Yang et al. [137] and Park and Han [162] reported lower pasting temperature, higher peak viscosity, and breakdown. According to Li et al. [146] and Zuo et al. [161] the viscosity drop is due to amylose and long linear amylopectin depolymerization, a finding consistent with the results by Luo et al. [152], who saw no modification in waxy maize starch, but a viscosity fall in amylose-rich Amylomaize V. Amylose is mainly responsible for the viscosity increase during setback [163,164], therefore its hydrolysis will result in a weaker network. The magnitude of changes in pasting behavior varies from almost negligible to complete starch liquefaction, as in thermal assisted (60 °C) sonication [149]. The LFUS and temperature interaction effect on pasting properties was confirmed by Zuo et al. [161], who reported a peak viscosity decrease down to a quarter. These findings encourage the use of LFUS to further improve starch saccharification, as described by Montalbo-Lomboy et al. [165] and Shewale and Pandit [166].

### 4.2. Proteins

Ultrasound-assisted modification of cereal and pseudocereal protein isolates has been extensively studied. Table 4 reports the broad range of conditions tested for modifying cereals and pseudocereals proteins. The results demonstrate that cavitation disrupts weak interactions (electrostatic bonds, hydrogen bonds, hydrophobic effect), thus leading to conformational changes in the secondary and tertiary structures. The proteins unravel and the hydrophobic cores, rich in phenylalanine, tyrosine, and tryptophan, are exposed, thus augmenting the surface hydrophobicity [168,185]. Covalent disulphide bonds are also affected by LFUS, and the amount of free-sulphydryls and disulphides depends on the power intensity used [186]. In fact, far higher energy is required to reduce S-S bonds (226 kJ/mol) than to break weak interactions (13 kJ/mol) [175]. An increase in SH groups, accompanied by a less evident decrease in S-S, was reported [168,179,180,183–185,187], leading to conclude that the breaking of disulphide bonds LFUS led to a much looser gluten matrix [20,180,182].

With regards to the secondary structure, the relative number of α-helices decreases in favor of β-sheets and random coils [20,171,173,178,180,183,185], while intramolecular β-sheets are converted to intermolecular β-sheets [20]. Ultrasound-induced denaturation may result in better digestibility due to increased accessibility for the digestive enzymes: in fact, Jin et al. [170] observed an improvement from 41.4% (control) to 58.2% (LFUS-treated) with buckwheat protein isolate.

### Table 4

Conditions tested in ultrasound processing for modifying cereal proteins.

| Sample | Suspension concentration (g/100 ml) | Frequency (kHz) | Device | Power (W) | Amplitude (%) | Time (min) | T (°C) | Reference |
|--------|----------------------------------|----------------|--------|-----------|---------------|------------|--------|-----------|
| corn gluten meal | 3 | 20–28:40 | bath | 100 | 240 | 30 | [189] |
| amaranth | 10 | 24 | probe | 100 | 30–90 | 15:30 | 3 | [168] |
| buckwheat protein | 4 | 20 | probe | 60 | 10 (5/5 s on/off) | 20 | [170] |
| corn germ defatted | 5 | 20–52 | probe | 28–80 | 15 | 30 | [193] |
| corn gluten meal | 3–7 | 20:20:40 | probe | 150 W/L | 2–10 (5/5 s on/off) | 60 | [196] |
| millet | 10 (w/w) | 20 | probe | 100 | 20–100 | 5–20 | 20–30 | [174] |
| oat | 0.5–6 | 20 | probe | 250–1250 | 10–50 (2/2 s on/off) | 27 | [192] |
| quinoa | 5 | 20 | probe | 200–600 | 20 | 21–40 | [173] |
| quinoa | 50 | 20 | probe | 360 | 19 kJ/mol | 20 | [181] |
| rice | 4 (w/w) | 28 | probe | 58 W/L | 15 (3/2 s on/off) | 50 | [171,172] |
| rice | 4.6 | 20–50 | probe | 50 W/L | 10 | 53 | [179] |
| rice | 6 | 20–60 | probe | 300x64 | 95 | up to 2 | [178] |
| wheat | 0.1–3 (w/w) | 20 | probe | 750 | 5–60 (2/2 s on/off) | 25 | [184] |
| wheat germ | 10 | 20 | probe | 200–1800 | 20 (2/2 s on/off) | 169 | |
| wheat germ defatted | 1 | 20 | probe | 900–1800 | 20 (2/2 s on/off) | 169 | |
| wheat gluten | 6 | 20 | probe | 540–900 | 60–100 | 10 | 25 | [34] |
| wheat gluten | 3 | 20 + 35 | probe x2 | 80–160 W/L | 30 (5/5 s on/off) | 30 | [186] |
| wheat gluten | 1–5 | 20 | probe x5 | 450 | 20 (4/3 s on/off) | 30 | [20] |
| wheat gluten | 3 | 20–50 | probe x5 | 100–300 W/L | 5–25 (5/5 s on/off) | 30 | [183] |
| wheat gluten | 1–5 | 20–50 | probe x5 | 100–300 W/L | 15 | 30 | [182] |
| wheat gluten | 8 | 20 | probe | 150–300 | 0.16–1 | [187] |
| wheat gluten | 3 | 20–80 | probe | 67 W/L | 10 (5/5 s on/off) | 30 | [186] |
| wheat gliadin | 0.2 in 65% ethanol | 20–25 | probe | 200–600 | 10 (5/5 s on/off) | 30 | [185] |
| zein | 1 | 22–68 | probe | 600 | 30 | 25 | [191] |
| zein | 1 | 33–68 | probe | 600 | 40 (10/3 s on/off) | 25 | [177] |
| zein | 1 | 40 | probe | 600 | 40 (10/3 s on/off) | 25 | [176] |
These changes do not affect protein molecular weight but disrupt aggregates [185]. Nevertheless, overtreatment may result in new intermolecular disulphide and hydrophobic bonds that increase the dimensions of the aggregates [101,168,175,184,185,188]. Constantino and García-Rojas [168] suggested that hydrogen peroxide generated by hydroxy radical addition could act as an oxidizing agent, thus converting free sulfhydryl into disulphide bridge.

Unexpectedly, LFUS denaturation increases protein solubility in water [168,173,174,176,180,188]. Nazari et al. [174] suggested that sonication leads to the emergence of hidden residues with a negatively-charged side chain, thus explaining the more negative zeta potential (25% and 14%) observed by Vera et al. [188] and Zhang et al. [181], respectively. Alterations in spatial arrangement improve the interfacial properties of the protein because expose residues in accordance with polarity, thus acting like surfactants [168,181]. LFUS-treated wheat gluten increased foam capacity (+138%), foam stability (+42–118%), emulsion activity index (2-fold) and emulsion stability (>3-fold) [182]. Similarly, LFUS improved millet protein foam capacity (2.75-fold), foam stability (22-fold), emulsion activity index (almost 2-fold) and emulsion stability (4.4-fold) [174]. By emulsifying finer oil droplets in water, LFUS enhanced wheat proteins foaming even better than Tween 80 [175]. Recently, Zhang et al. [181] produced a high internal phase emulsion, which mimics a solid fat, using quinoa protein nanoparticles as an emulsifier whose interfacial properties were adjusted by varying the ultrasonic density.

The low-power high-frequency ultrasound has often been utilized as pre-treatment to produce bioactive peptides from cereals. The LFUS-assisted enzymolysis was very effective at enhancing the ACE inhibitory activity of peptides by 8–99% [20,169,176–178,182,183,189–191]. Protein denaturation, as mentioned above, leads to enhanced exposure of the enzymatic cleavage sites, improving the quality of the digested products, because hydrophobic-ending peptides have higher ACE inhibitory activity [169,178,189]. Furthermore, cavitation disaggregates protein-starch complexes, thus exposing larger attack surfaces [190]. Enzymatic affinity is increased, because of the reduction (13–42%) in Michaelis-Menten constant [20,169,190,192]. This change is accompanied by a higher initial hydrolysis rates [20,169,192,193]. The affinity towards the substrate may also be raised by conformational changes in the enzymes [190].

### 4.3. Dietary fibre

Ultrasound modification of dietary fibre was experimented by Has-san et al. [194] on the insoluble fraction pre-extracted from chia seeds, and by Wei et al. [195] on purified soluble fraction from millet bran: the LFUS treatments produced about two-fold increases of both water and oil holding capacity. Those effects were attributed to the shear stress leading to disruption of structure and fragmentation of particles, with the consequent increase of hydrophilic functional groups, but also to a greater access to hydrophobic cavities where oil can be retained. LFUS capability to shatter dietary fibre was evidenced by Vaitkevičienė et al. [196]: they ultrasonicated rice bran and observed an average 10% decrease of insoluble fibre, and an increase of the soluble fraction; formation of resistant starch, likely due to chains rearrangement, was also detected. Similarly, Zadeiske et al. [197], documented a coarse surface with multiple fractures in LFUS-treated rice bran and an increase in its absorption of water and oil. Li et al. [198] observed a reduction in the number-average molecular weight of wheat bran arabinoxylan (AX) treated with LFUS (120–160 W for 15–45 min) and hypothesized a power and time-dependent chain-breaking effect because of cavitation, while Fan et al. [199] confirmed the LFUS role in the reduction of AX molecular weight; both group of authors suggested that this could represent an alternative way to regulate the rheological properties of AX fraction. In addition, AX covalently binds phenolic acids [198], thus its heightened depolymerization could imply a transition of phenolic compounds from insoluble to soluble forms. In fact, Fan et al. [199] observed an increase in ferulic acid after sonication, but being AX a major component of wheat bran [200] this phenomenon deserves further, more detailed examination.

### 5. Conclusions

Low-frequency ultrasound (LFUS) is a promising green technology for improving key processing steps in cereals and pseudocereals as well as for modifying structural, physical, chemical, technological, functional, and biological properties of macromolecules such as carbohydrates and proteins. Moreover, in addition to saving energy and reducing processing time in agreement with its environment-friendly nature, LFUS allows to improve many extraction processes and to obtain value-added ingredients from cereal and pseudocereal by-products in the frame of a circular economy.

LFUS enhances the hydration rate and the time lag phase during pre-treatments essential for cooking, extraction, fermentation, and germination of cereals and pseudocereals. Additionally, it improves and accelerates sprouting by increasing hydration, which in turn releases promoters and eliminates inhibitors of germination. Therefore, LFUS could be easily employed to speed-up the synthesis of bioactive compound (e.g., phenolics) in cereals and pseudocereals during the germination under stress-inducing condition that promote the production of antioxidants. Additionally, LFUS boosts the extraction rate of bioactive compounds, such as phenolic compounds and polysaccharides, is compatible with the use of some green solvents and improves the fortification with vitamin and minerals due to its ability to produce cracks and pores. However, the mechanism underlying such improvements still need be investigated in detail to increase scientific knowledge and optimize LFUS treatments.

An important property of LFUS is that it can improve and regulate the technological properties of fundamental food macromolecules like carbohydrates (starch and dietary fibre) and proteins. Peptides produced from the enzymatic hydrolysis of proteins denatured by LFUS present enhanced bioavailability and bioactivity. Therefore, LFUS may represent an efficient and viable alternative to produce nanoparticles of proteins or carbohydrates and bioactive compounds with improved bioavailability and bioactivity. Nevertheless, to scale-up similar processes to future industrial applications, LFUS conditions should be carefully assessed and measured by calorimetric and chemical dosimetry, rarely studied in cereals and pseudocereals.

Although LFUS has demonstrated numerous possible applications in cereals and pseudocereals, its use in manufacturing has been scarcely developed. The challenge currently is to go beyond basic research and to transfer the promising lab results to pilot and industrial scale.

### Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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