Microbiological analysis of the population of extremely haloalkaliphilic sulfur-oxidizing bacteria dominating in lab-scale sulfide-removing bioreactors

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Abstract Thiopaq biotechnology for partial sulfide oxidation to elemental sulfur is an efficient way to remove H\textsubscript{2}S from biogases. However, its application for high-pressure natural gas desulfurization needs upgrading. Particularly, an increase in alkalinity of the scrubbing liquid is required. Therefore, the feasibility of sulfide oxidation into elemental sulfur under oxygen limitation was tested at extremely haloalkaline conditions in lab-scale bioreactors using mix sediments from hypersaline soda lakes as inoculum. The microbiological analysis, both culture dependent and independent, of the successfully operating bioreactors revealed a domination of obligately chemolithoautotrophic and extremely haloalkaliphilic sulfur-oxidizing bacteria belonging to the genus Thioalkalivibrio. Two subgroups were recognized among the isolates. The subgroup enriched from the reactors operating at pH 10 clustered with Thioalkalivibrio jannaschii–Thioalkalivibrio versutus core group of the genus Thioalkalivibrio. Another subgroup, obtained mostly with sulfide as substrate and at lower pH, belonged to the cluster of facultatively alkaliphilic Thioalkalivibrio halophilus. Overall, the results clearly indicate a large potential of the genus Thiolalkalivibrio to efficiently oxidize sulfide at extremely haloalkaline conditions, which makes it suitable for application in the natural gas desulfurization.

Keywords Thiopaq · Sulfide removal · Haloalkaliphilic · Sulfur-oxidizing bacteria (SOB) · Soda lakes · Polysulfide · Thioalkalivibrio

Introduction

The presence of H\textsubscript{2}S in fuel gases causes many environmental and technical problems demanding its removal before combustion. Usually, it is done by a catalytic oxidation. An alternative bioprocess based on lithoautotrophic sulfide-oxidizing bacteria (SOB) as a catalyst has been developed and successfully applied at full scale in The Netherlands for biogas desulfurization (Buisman et al. 1990; Janssen et al. 1995, 1999). The major principle of the Thiopaq technology is regulation of sulfide oxidation at the level of elemental sulfur by low redox potential, which provides two advantages over the complete oxidation to...
sulfate: (1) The oxidation does not generate protons but regenerates hydroxyl ions, thereby allowing to save on caustic absorbent; (2) formation of elemental sulfur allows easy separation of the final oxidation product and recirculation of the liquid phase. In case of biogas, the bioprocess is performed at relatively low salt concentrations and pH, i.e., at 0.5 M total Na\(^+\) and pH 8.2–8.5, with bicarbonate as the dominant anion in solution. At these conditions, marine-type SOB, such as Halothiobacillus neapolitanus W5 (Visser 1997), function very well. However, for the removal of H\(_2\)S from high-pressure natural gas and sour gas streams produced in the petrochemical industry, the total alkalinity must be substantially increased to make scrubbing process more efficient. This dictates a shift in a type of biocatalyst from neutrophilic marine SOB to natronophilic (soda-philic), highly salt tolerant SOB (Banciu et al. 2004a; van den Bosch et al. 2007, 2008). Such SOB have recently been discovered in the sediments of hypersaline soda lakes (Sorokin and Kuenen 2005; Sorokin et al. 2006a). One out of three genera of haloalkaliphilic SOB described so far, the genus Thioalkalivibrio, is characterized by the ability to grow in saturated soda brines containing up to 4 M total Na\(^+\) and pH from 7 to 10.5. All but one out of nine described species of this genus are obligatory alkaliphilic and soda-philic; that is, they can only grow in carbonate brines and at a pH above 8. A single species, Thioalkalivibrio halophilus, is a facultative halophile capable of growth at neutral pH in NaCl brines as well as in soda brines at pH 10 (Banciu et al. 2004b). All previously described high salt-tolerant Thioalkalivibrio strains were obtained from the enrichments with thiosulfate as substrate and high redox potential, since batch cultivation at low redox potential with sulfide as an electron donor is much more complicated. Therefore, such organisms might be unsuitable for application in the Thiopaq process module, where the redox potential is as low as ~350 mV and sulfide/polysulfide is the actual electron donor.

This paper describes results of a microbiological investigation of lab-scale bioreactors oxidizing sulfide/polysulfide at pH 8.5–10 and a salt content of 2–3 M Na\(^+\)/K\(^+\). It is shown that the populations were dominated by extremely salt-tolerant alkaliphilic SOB, represented by two subgroups of the genus Thioalkalivibrio.

**Materials and methods**

Inoculum for the bioreactors

Surface sediment samples (0–10 cm) were obtained from hypersaline soda lakes in northeastern Mongolia, southwestern Siberia, and Wadi al Natrun in Egypt. Eight to 12 samples from individual lakes in each region were combined into a single pool. The pH of the brines varied from 9.2 to 10.6, total salt concentration from 60 to 400 g l\(^{-1}\), and total soluble alkalinity from 0.05 to 3 M.

**Bioreactors**

Two types of lab-scale bioreactors were used for oxidation of sulfide at oxygen-limited conditions. One was a 5-L gas-lift column (FBR) fed by H\(_2\)S gas where oxygen supply was controlled by a redox electrode (vs Ag/AgCl; van den Bosch et al. 2007, 2008). Another type was a 1-L stirred tank reactor (SL-BR) where sodium sulfide was fed in sequential fed-batch mode (1 mM shots) and oxygen was supplied by limited diffusion through a loop from silicon tubing (Supplementary Fig. 1). The major difference between these two types of bioreactors was the concentration of polysulfide. In the FBR, it was generally maintained at a relatively low level of 100 μM sulfane using redox control. The fraction of free sulfide as compared to polysulfide was minimal at pH 10 and increased toward pH decrease. In the SL-BR, the concentration of polysulfide reached 1 mM right after addition of sulfide due to a rapid spontaneous reaction with sulfur formed during the previous stage, decreasing gradually to zero due to biological activity of the SOB. Therefore, the latter conditions were selective for high polysulfide/sulfide resistance and polysulfide as a substrate.

**Operating conditions**

The duplicate FBR were run during 2 years at variable modes at pH starting from 10.1 and ending at 8.8 (Table 1). The redox potential was maintained most of the time below ~390 mV (vs Ag/AgCl). The mineral medium was based on bicarbonate/carbonate buffer containing 70% K\(^+\) and 30% Na\(^+\), 2 M in total. The presence of so much potassium is certainly unusual and never occurs in natural soda lakes. The reason behind employing such an unusual buffer is the much higher solubility of potassium carbonates as compared to sodium carbonates, especially when pH is decreased below 9 and bicarbonate is the dominant anion. Our preliminary tests with extremely haloalkaliphilic cultures of the genus Thioalkalivibrio demonstrated that many strains can withstand up to 50% replacement of Na\(^+\) by K\(^+\) at 2 M total cation in the form of carbonates, and a few strains even tolerated 90% replacement. This is in contrast to the neutrophilic halophilic SOB, which cannot grow already at 30% replacement of NaCl by KCl (Sorokin 2008). The N source in the bioreactors was urea. A more detailed description of these bioreactors is given elsewhere (van den Bosch et al. 2007, 2008). The duplicate 1-L SL-BRs were run within 2 months at 1.2–3.0 M of K/Na carbonates, 70% K, and pH 10.1. The N source was ammonia.
Isolation and cultivation of pure cultures of extremely haloalkaliphilic SOB

Two approaches were used for the enrichment and isolation of pure cultures of haloalkaliphilic SOB. One was based on using thiosulfate as substrate (20 mM), which is stable at aerobic conditions. Alternatively, sulfide (2 mM) was used as a substrate. Use of sulfide is much more difficult because of its volatility, toxicity, and spontaneous oxidation. The former effects, however, are reduced at highly alkaline pH, while the spontaneous oxidation was reduced by a ten times decrease in trace metal content and the use of only 1% oxygen in the gas phase. To standardize the enrichment procedure, the same conditions were also used in the thiosulfate enrichments. The liquid mineral medium used for enrichment and isolation contained carbonate buffer with 2 M K/Na (70% K), pH 10, 1 g/L of K₂HPO₄, and 4 mM of either NH₄Cl or urea. After sterilization, the medium was supplemented with trace metals (Pfennig and Lippert 1966), 1 mM MgCl₂, and a sulfur substrate. Serial dilutions were incubated at 30°C in 20-mL Hungate tubes with 2 mL medium and a headspace containing 1% O₂ in argon. When turbidity appeared in a highest dilution, it was plated into a solid agar medium of the same composition. The plates were incubated in closed jars (3 L) under the atmosphere of argon containing 1% O₂. In case of sulfide enrichments, the plates did not contain any substrates. Instead, 4 mL of 1 M sodium sulfide solution was placed into the jar in a 10-mL vial. During the prolonged incubation (2–4 weeks), H₂S entered the gas phase and was absorbed by the alkaline agar creating optimal conditions for sulfide-utilizing SOB. Dominating colony types were picked under the binocular and placed into the liquid medium. The purity of the culture was checked by repeated plating.

Metabolic profiles of the reactor biomass and pure cultures

The activity and the stoichiometry of oxidation of various sulfur compounds was studied with an oxygen electrode.

| Bioreactors                         | Mode                  | pH   | K⁺/Na⁺ (M) | Viable count | Strain | Substrate | Sulfur autotrophy |
|-------------------------------------|-----------------------|------|------------|--------------|--------|-----------|-------------------|
| 5-L gas-lift column                 | Chemostat             | 10.0–10.1 | 2.0       | 10¹⁰        | ALR1-1 | Thio      | +                 |
|                                     |                       |      |            | 10¹¹        | ALR1-2 | Thio      | +                 |
|                                     |                       |      |            |             | ALR 2  | HS⁻       | +                 |
|                                     |                       |      |            |             | ALR6   | Thio      | +                 |
|                                     |                       |      |            |             | ALR7   | HS⁻       | +                 |
|                                     |                       |      |            |             | ALR8   | HS⁻       | +                 |
|                                     |                       |      |            |             | ALR9   | HS⁻       | +                 |
| Fed-batch                           |                      | 9.7  | 10⁸        | 10¹⁰        | ALR3   | Thio      | +                 |
|                                     |                       |      |            |             | ALR4   | HS⁺       | +                 |
|                                     |                       |      |            |             | ALR5   | HS⁺       | +                 |
|                                     |                       |      |            |             | ALR13  | Thio      | +                 |
|                                     |                       |      |            |             | ALR14  | HS⁺       | +                 |
|                                     |                       |      |            |             | ALR15  | HS⁻       | -                 |
|                                     |                       |      |            |             | ALR16  | HS⁻       | +                 |
|                                     |                       |      |            |             | ALR20  | HS⁻       | +                 |
|                                     | Sequential batch      | 9.8  | 10⁸        | 10¹¹        | ALRU1  | Thio      | +                 |
|                                     |                       |      |            |             | ALRU2  | HS⁺       | +                 |
|                                     |                       |      |            |             | ALRU3  | HS⁺       | +                 |
|                                     |                       |      |            |             | ALR10  | Thio      | +                 |
|                                     |                       |      |            |             | ALR14  | HS⁺       | +                 |
|                                     |                       |      |            |             | ALR15  | HS⁻       | -                 |
|                                     |                       |      |            |             | ALR16  | HS⁻       | +                 |
| 1-L silicon-loop reactor            | Sequential batch      | 10.1 | 2.0        | nd          | ALBR1  | Thio      | +                 |
|                                     |                       |      |            | nd          | ALBR2  | HS⁺       | +                 |
|                                     |                       |      |            |             | ALBR3  | Thio      | +                 |
|                                     |                       |      |            |             | ALBR4  | Thio      | +                 |
|                                     |                       |      |            |             | ALBR X1| Thio      | +                 |
|                                     |                       |      |            |             | ALBR X2| Thio      | +                 |
|                                     |                       |      |            |             | ALBR X3| HS⁻       | +                 |
|                                     |                       |      |            |             | ALBR5  | HS⁻       | +                 |
|                                     |                       |      |            |             | ALBR6  | HS⁻       | +                 |
|                                     |                       |      |            |             | ALBR7  | HS⁻       | +                 |
|                                     |                       |      |            |             | ALBR8  | HS⁻       | +                 |
|                                     |                       |      |            |             | ALBR9  | HS⁻       | +                 |
|                                     |                       |      |            |             | ALBR10 | Thio      | +                 |
|                                     |                       |      |            |             | ALBR11 | Thio      | +                 |

| Reactors and isolates data          |                      | Thio | HS⁻       |              |        |           |                   |
|-------------------------------------|-----------------------|------|-----------|--------------|--------|-----------|-------------------|
| Bioreactors                         | Mode                  | Viable count | Strain | Substrate | Sulfur autotrophy |
| 5-L gas-lift column                 | Chemostat             | 10¹⁰ | ALR1-1    | Thio        | +                  |
|                                     |                       | 10¹¹ | ALR1-2    | Thio        | +                  |
|                                     |                       |      | ALR 2     | HS⁻        | +                  |
|                                     |                       |      | ALR6      | Thio        | +                  |
|                                     |                       |      | ALR7      | HS⁻        | +                  |
|                                     |                       |      | ALR8      | HS⁻        | +                  |
|                                     |                       |      | ALR9      | HS⁻        | +                  |
| Fed-batch                           |                      | 10⁸  | ALR3      | Thio        | +                  |
|                                     |                       | 10¹⁰ | ALR4      | HS⁺         | +                  |
|                                     |                       |      | ALR5      | HS⁺         | +                  |
|                                     |                       |      | ALR10     | Thio        | +                  |
|                                     |                       |      | ALR14     | HS⁺         | +                  |
|                                     |                       |      | ALR15     | HS⁻         | -                  |
|                                     |                       |      | ALR16     | HS⁻         | +                  |
| 1-L silicon-loop reactor            | Sequential batch      | 10⁸  | ALBR1     | Thio        | +                  |
|                                     |                       | 10¹⁰ | ALBR2     | HS⁺         | +                  |
|                                     |                       |      | ALBR3     | Thio        | +                  |
|                                     |                       |      | ALBR4     | Thio        | +                  |
|                                     |                       |      | ALBR X1   | Thio        | +                  |
|                                     |                       |      | ALBR X2   | Thio        | +                  |
|                                     |                       |      | ALBR X3   | HS⁻         | +                  |
|                                     |                       |      | ALBR5     | HS⁻         | +                  |
|                                     |                       |      | ALBR6     | HS⁻         | +                  |
|                                     |                       |      | ALBR7     | HS⁻         | +                  |
|                                     |                       |      | ALBR8     | HS⁻         | +                  |
|                                     |                       |      | ALBR9     | HS⁻         | +                  |

a Correspond to FBR1
b Correspond to FBR2
c Correspond to SL-BR2
using washed cells as described previously (Banciu et al. 2004b). The pH dependence was examined at 2 M total Na\(^+\), using the following buffers: for pH 6–8, 0.1 M 4-(2-hydroxyethyl)-1-piperazineethanesulfonic acid and NaCl; for pH 8–11, a mixture of sodium bicarbonate/sodium carbonate containing 0.1 M NaCl. To study the influence of salt concentration, sodium carbonate buffer with pH 10 containing 0.1 and 4.0 M of total Na\(^+\) was applied. All buffers contained 50 mM K\(^+\) and 1 mM Mg\(^{2+}\). Cell membranes were obtained by ultracentrifugation of the sonified cells at 144,000×g for 2 h (Beckman). The membranes were resuspended in soda buffer at pH 9 containing 0.5 M total Na\(^+\) and used to measure several enzyme activities. Cytochrome c oxidase was measured by the rate of oxidation of 1 mM \(N,N,N',N'\)-tetramethyl p-phenylenediamine (TMPD) spectrophotometrically at 610 nm. Sulfide-quinone reductase (SQR) activity was determined in a discontinuous assay of anaerobic decyl-ubiquinone-dependent oxidation of sulfide (0.2 mM each). Cytochrome c content in the membranes was estimated from spectroscopic measurements of dithionite-reduced minus air-oxidized preparations using UV-visible diod-array spectrophotometer (Vectra 8453, HP, Amsterdam) and molar absorbance coefficient \(E_{550}^{\text{cm}^{-1}}\).

Analytical procedures

Chemical analysis of sulfur (sulfide, sulfur, thiosulfate, and sulfite) and nitrogen (nitrite and ammonium) compounds and cell protein were performed as described previously (Sorokin et al. 2001; Banciu et al. 2004b). Sulfane sulfur atoms of polysulfide were analyzed in the same way as free sulfide, i.e., after precipitation as ZnS. Zero-valent sulfur in polysulfide was analyzed in the same way as free sulfur (i.e., by cyanalysis of acetone extract) after decomposition of polysulfide molecules by acid treatment. Total protein comparison of the isolates and the reactor biomass was performed using 5–15% gradient sodium dodecyl sulfate polyacrylamide gel electrophoresis (SDS-PAGE) according to Laemmli (1970). Repetitive-sequence-based polymerase chain reaction (REP-PCR) fingerprinting comparison of the SOB isolates was performed with the GTG5 primer set as described previously (Foti et al. 2006).

Genetic and phylogenetic analysis

Genomic deoxyribonucleic acid (DNA) was extracted from the cell pellet using the UltraClean Soil DNA Extraction Kit (MoBio Laboratories, USA), following the manufacturer’s instructions. For the pure cultures, the nearly complete 16S ribosomal ribonucleic acid (rRNA) gene was obtained using general bacterial primers GM3f (5′-AGAGTTTGATCCTGGCTCAG-3′) and GM4r (5′-TACTTGTACCTGGTACGACTT-3′). For the denaturing gradient gel electrophoresis (DGGE) analysis, partial amplification with a primer pair 341F=GC/907R was employed (Schäfer and Muyzer 2001). DGGE was performed as described by Muyzer et al. (1993), using a denaturing gradient of 20–35% to 60–70% denaturants in 8% polyacrylamide gel. Individual bands were excised, reamplified, and run again on a denaturing gradient gel to check their purity. PCR products for sequencing were purified using the Qiaquick PCR purification kit (QIAGEN, The Netherlands). The sequences were first compared with sequences stored in GenBank using the BLAST algorithm (http://www.ncbi.nlm.nih.gov/BLAST). Subsequently, the sequences were imported into the ARB software program (Ludwig et al. 2004), automatically aligned, and added to a phylogenetic tree using the Quick-add tool. Subtrees were then built using the neighbor-joining algorithm with automatic selected correction settings.

Results

Catalytic properties of the bioreactor biomass

Respiration profiles for different sulfur compounds were determined with washed cells directly from the bioreactors and used to characterize the activity and pH/salt response of the dominant SOB populations. A general trend could be seen that sulfide and, in case of the SL-BR reactors, polysulfide were much better respiratory substrates for the mixed SOB population in the reactors than thiosulfate (Fig. 1a). This is not usually the case with the SOB dominating fully aerobic conditions (Sorokin et al. 2006a). Sulfide/polysulfide specialization indicates that there should be a different pathway for oxidation of these highly reduced electron donors as compared to thiosulfate oxidation. One of the specialized components of such a pathway might be sulfide-quinone reductase – a flavin-containing enzyme oxidizing sulfide to elemental sulfur with quinones as electron acceptors (Griesbeck et al. 2000). We found a relatively high activity of this enzyme in the biomass of the analyzed bioreactors (Fig. 1b). Another parameter characteristic for a highly active respiratory chain in aerobic chemolithoautotrophs is the activity of cytochrome c oxidase together with the presence of a high-potential cytochrome c pool. This pair is responsible for the terminal delivery of the electrons obtained during oxidation of electron donor to oxygen. Comparison of the three reactor samples demonstrated that only in FBR2 (pH 8.8), it was at a level normal for aerobic haloalkaliphilic SOB (personal data on pure cultures), while in SL-BR2 (pH 10) and FBR1 (pH 9.5), the cytochrome c oxidase had a low specific activity. This might be connected to the condition of extremely low

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redox potential in the reactors, especially in SL-BR2, due to the presence of polysulfide at a high concentration.

One of the very important parameters of the SOB biomass activity in the reactors is its pH response. Comparison of the two FBR reactors, run at different pH (9.5 for FBR1 and 8.8 for FBR2), demonstrated a different pH response (Fig. 2). There was a clear difference in the neutral part of the pH profiles for sulfide between the two reactors. This indicates either the presence of a separate pH-neutral population in FBR2 (pH 8.8) or a dominance of facultatively alkaliphilic sulfide-oxidizing species in this reactor. The profile for polysulfide in FBR2 was similar to that of sulfide. In contrast, the profile for thiosulfate oxidation by FBR2 cells was typical for obligate alkaliphilic SOB. The latter profile might be due to the presence of different SOB populations specialized either in sulfide/polysulfide or thiosulfate or due to a different pH response of the same population with different substrates. Our pure culture data favor the first suggestion. But, in general, the respiratory data clearly indicated domination of haloalkaliphilic SOB in the reactors.

A direct comparison of the membrane proteins, which are dominated by the respiratory enzymes, showed major similarity between the two reactors FBR1 and FBR2 (Fig. 3), suggesting a presence of the same dominant SOB population.

Molecular analysis of the biomass from two SL-BR and two FBR bioreactors based on 16S rRNA gene DGGE showed low genetic diversity, typical for autotrophic mix cultures with domination of one to two SOB genotypes and some side heterotrophic populations (Fig. 4). Since analysis of the SL-BR and FBR biomasses was performed on different gels, the profiles could not be directly compared.
However, a general similarity of the FBR1 and FBR2 (pH difference 0.7 units) profiles were quite obvious, while the profiles of two SL-BR (difference in salinity is equivalent to 2 M K/Na) looked different. This might be explained by the fact that while pH 9.5 and 8.8 are still within alkalinophilic range, a salt content of 1.5 and 3 M total Na/K usually selects for different groups of haloalkaliphilic SOB (Sorokin et al. 2006a). The phylogenetic analysis of the DGGE band sequences demonstrated that in all samples, lithoautotrophic SOB belonging to the gamma-Proteobacteria were dominant (Fig. 5), although its affiliation differed at different reactor conditions. At moderate haloalkaline conditions (reactor SL-BR1), the dominant band belonged to a distant relative of the genus *Halothiobacillus*, while at higher salt (2–3 M K/Na), both in SL-BR2 and in FBR, the representatives of the genus *Thioalkalivibrio* were identi-
fied. Interestingly, in all three high-salt reactors, despite the difference in pH, the SOB sequence was most closely related to the facultatively alkaliphilic and extremely salt-tolerant *T. halophilus* (Banciu et al. 2004b). Other identified sequences either belonged to nonsulfur-oxidizing alkaliphilic heterotrophs, such as *Marinospirillum* (SL-BR2) or *Bacillus* (FBR2), or to haloalkaliphilic facultative sulfur oxidizers, for which sulfide oxidation might provide additional energy (Sorokin et al. 2000, 2006b), such as *Alkalispirillum* (FBR1) and *Rhobacteraceae* (FBR2).

**Isolation and identification of the dominant haloalkaliphilic SOB from the bioreactors**

The cultivation approach demonstrated the presence of culturable SOB in the reactor biomass, mostly at a very high density (Table 1). From the highest positive dilution, more than 20 pure cultures were obtained either with thiosulfate or with sulfide as the sulfur substrate. All but one of them (strain ALR15) were obligately chemolithoautotrophic SOB identified as the representatives of...
three subclusters within the genus Thioalkalivibrio by 16S rRNA gene sequencing (Fig. 5). Most of the isolates from the SL-BR reactors (pH 10) and from the FBR run at pH 10 were clustering around the core group of the genus which includes the type species Thioalkalivibrio versutus and its close relatives Thioalkalivibrio thiocyanoxidans, Thioalkalivibrio jannaschii, and Thioalkalivibrio nitratii, all obligate haloalkaliphiles. Only two isolates, ALR 3 and ALR 6, obtained from the high-pH FBR on sulfide, belonged to the cluster of facultative alkaliphilic halophile T. halophilus. On the other hand, all the isolates obtained with sulfide as substrate from the reactor with lowest pH (FBR2, pH 8.8) belonged to the T. halophilus subcluster, and only those enriched with thiosulfate clustered with the core group of obligate alkaliphiles. The latter results were consistent with the DGGE analysis (Figs. 4 and 5) of the biomass from FBR2 and with the pH profile of respiration (Fig. 2). On the other hand, the cultivation-based approach failed to produce the same results for SL-BR2, where molecular data also identified a dominance of a T. halophilus-like population, while only representatives of the core group of the genus Thioalkalivibrio were obtained in culture. This might be explained by the different culture conditions: In batch enrichment, cultivation at pH 10 from the SL-BR2 might have provided better conditions for the secondary population of obligate alkaliphiles.

A pH–salt response of one of the T. halophilus-like isolates, strain ALR 14, was studied in more details, since this type seemed to be an important player in both types of bioreactors. Growth experiments with thiosulfate demonstrated that, despite being phylogenetically closely related to facultatively alkaliphilic T. halophilus, strain ALR 14 can be regarded as an obligate alkalophile (Fig. 6a). On the other hand, its respiratory activity (Fig. 6b), especially with sulfide, was quite high already at subalkaline pH values (8.5–9.0), indicating good fitness to the reactor conditions (pH 8.8). Salt profiles corresponded to those of extremely salt-tolerant moderate halophiles (Fig. 6c) and also fit very well to the reactor conditions (2 M total Na/K). An interesting pH effect was observed in case of the oxidation of sulfide and polysulfide by ALR 14 (Fig. 6d): The oxidation of sulfane atoms (S⁻) proceeded mostly to elemental sulfur at near neutral pH, while its further oxidation to sulfate was increasing at an alkaline pH range. A similar effect of pH on product formation was found in the FBR bioreactors (van den Bosch et al. 2008), with one important difference: In case of washed cells of a pure culture, the final oxidation product was sulfate, while in the bioreactor, thiosulfate accumulated at high pH. This difference can be accounted to the nature of sulfane atom oxidation in the two systems. In the bioreactors, enzymatic oxidation of polysulfide sulfane atoms was apparently inhibited by very low redox potentials, resulting in spontaneous oxidation to thiosulfate. In contrast, the washed cells experiment was conducted at a high initial oxygen concentration, allowing enzymatic conversion of sulfane with sulfate as the final product.

A single heterotrophic isolate was obtained from FBR2 from the special colonies formed on alkaline plates incubated under the H₂S-containing gas phase. Since also DGGE analysis indicated a presence of heterotrophs in the reactor, there must be a source of organic carbon in the system. Such carbon could be provided by a dominant population of Thioalkalivibrio either by excretion or after lysis of dead cells. Usually, SOB are forming sulfur inside the colonies. In contrast, strain ALR 15 produced large sulfur halos around the colonies (Supplementary Fig. 2). Further investigation showed that the bacterium, which was identified as a member of the genus Halomonas, was an obligate heterotroph unable to actually use sulfide or thiosulfate as an energy source. However, during heterotrophic growth, it oxidized thiosulfate to tetrathionate, which is a well-known property of this group of gamma-Proteobacteria (Sorokin 2003). Our scenario to explain this extracolonial sulfur formation is the following (Supplementary Fig. 2): H₂S was being absorbed into the alkaline agar from the gas phase and partially converted to elemental sulfur. The latter reacted with sulfide to form polysulfide (indeed a yellowish coloration was observed after prolonged incubation of the plates). Spontaneous reaction of polysulfide with oxygen resulted in the formation of thiosulfate. In this reaction, the active role of the bacterium starts, in providing tetrathionate—a powerful oxidant for sulfide. The reaction of sulfide with tetrathionate produces sulfur and regenerates the substrate (thiosulfate) for the heterotroph. So, only traces of thiosulfate are necessary to catalyze the oxidation of sulfide to sulfur in the presence of tetrathionate-forming heterotrophs. Such a microbiochemical catalysis has been demonstrated for a marine heterotrophic bacterium Catenococcus (Sorokin et al. 1996). The difference with Halomonas ALR 15 is in the internal generation of thiosulfate from polysulfide, which is stable only at highly alkaline conditions. In the case of Catenococcus, thiosulfate had to be supplied externally. Although the colonies with external sulfur accumulation were quite common in our enrichments, this organism was not found in the reactor biomass by molecular analysis, which makes its role in sulfide oxidation in situ in comparison with the obligate autotrophic Thioalkalivibrio questionable.

Discussion

Our previous microbiology investigation of various soda lakes demonstrated a presence of highly diverse population of the obligately lithoautotrophic SOB of the genus Thioalkalivibrio which was dominating especially at ex-
extreme salinity (Sorokin, Kuenen 2005; Sorokin et al. 2006a; Foti et al. 2006). So, it is not surprising that in the bioreactors inoculated with the sediments from hypersaline soda lakes, these haloalkaliphilic SOB species were dominating. The reactor isolates were very closely related to the *Thioalkalivibrio* species obtained from the natural sediments isolated at fully oxic conditions with thiosulfate as substrate. This might mean that both low-potential oxidation of sulfide/polysulfide and high-potential thiosulfate oxidation pathway may coexist in the same SOB species. Indeed, that’s what usually can be seen in the respiratory profiles of the haloalkaliphilic SOB grown either with thiosulfate or sulfide at fully aerobic conditions, i.e., equal rates of sulfide- and thiosulfate-dependent respiration. On the other hand, the respiratory tests with the SOB biomass from the low redox potential bioreactors clearly indicated sulfide/polysulfide preference (see Fig. 1), suggesting a possibility of a different pathway for oxidation of these highly reduced electron donors as compared to thiosulfate oxidation. One of the specialized components of such a pathway might be sulfide-quinone reductase—a flavin-containing enzyme oxidizing sulfide to elemental sulfur with quinones as electron acceptors (Griesbeck et al. 2000), which activity was detected in the reactor biomass. Furthermore, the profound “sulfide/polysulfide specialization” of the biomass in SL-BR2 and FBR1 correlated with a relatively low cytochrome c oxidase activity. Taken together, this might indicate a substantial change in the electron flow pathway and needs further, more detailed investigation.

Another interesting result of this study is a diversity of a single culturable haloalkaliphilic SOB taxon found in the bioreactors at triple extreme conditions (high alkalinity, high total salt, high K). Although all of them belonged to a single genus, most of the isolates were genetically different from each other. The exact meaning of such difference is not completely clear, although some phenotypic difference, such as correlation with the pH in the reactor and with the substrate, used for isolation, can be seen in different subgroups. Apparently, the genus *Thioalkalivibrio*, despite being a relatively narrow specialized ecotype, possesses extraordinary potential for microadaptation. On the other
hand, the molecular analysis (DGGE) of the reactor populations indicated a presence of a single *Thioalkalivibrio* phylotype closely related to a facultatively alkaliphilic species *T. halophilus*. It is not easy to explain such a big difference between the results from two approaches. We can offer two. First, this could be a result of cultivation bias, since batch enrichment/isolation from the SL-BR reactors was performed at pH 10 and resulted in isolation of numerous strains of obligate alkaliphiles related to the core group of the genus *Thioalkalivibrio*. Perhaps, if lower pH values were used, isolates related to *T. halophilus* would be obtained at least with sulfide as the substrate, similar to the results with FBR reactors. A second explanation might be that the DNA from the obligately alkaliphilic types of *Thioalkalivibrio*, for one or another reason, was less accessible for PCR—a usual bias of the DGGE method. Judging from the previous results of the microbiological study of natural alkaline lakes, the major factor determining a domination of these two types of *Thioalkalivibrio* is pH in combination with high chloride content. For example, *T. halophilus*—like SOB—dominated among the isolates from the haloalkaline Wadi Natrun lakes in Egypt with NaCl as a dominant salt and pH around 9, while natrono (soda)philic *Thioalkalivibrio* species dominated in true soda lakes with pH around 10 where sodium carbonates were present at molar concentration (Sorokin et al. 2006a).

The genus *Thioalkalivibrio* has a great potential to thrive at extremely haloalkaline conditions and is a sure candidate for application in biological sulfide removal directly from spent sulfide caustics. In the natural soda lake sediments, often another genus of low salt-tolerant alkaliphilic SOB (*Thioalkalimicrobium*) can be found, which is characterized by extremely high rates of sulfide oxidation (Sorokin and Kuenen 2005; Sorokin et al. 2006a). The fact that it apparently was not present in the described bioreactors could probably be explained by high salt concentration which is above its capacity to grow.

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