First Gadolinium Loading to Super-Kamiokande

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Preprint submitted to Nucl. Instrum. Meth. A December 16, 2021
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Abstract

In order to improve Super-Kamiokande’s neutron detection efficiency and to thereby increase its sensitivity to the diffuse supernova neutrino background flux, 13 tons of Gd$_2$(SO$_4$)$_3$·8H$_2$O (gadolinium sulfate octahydrate) was dissolved into the detector’s otherwise ultrapure water from July 14 to August 17, 2020, marking the start of the SK-Gd phase of operations. During the loading, water was continuously recirculated at a rate of 60 m$^3$/h, extracting water from the top of the detector and mixing it with concentrated Gd$_2$(SO$_4$)$_3$·8H$_2$O solution to create a 0.02% solution of the Gd compound before injecting it into the bottom of the detector. A clear boundary between the Gd-loaded and pure water was maintained through the loading, enabling monitoring of the loading itself and the spatial uniformity of the Gd concentration over the 35 days it took to reach the top of the detector. During the subsequent commissioning the recirculation rate was increased to 120 m$^3$/h, resulting in a constant and uniform distribution of Gd throughout the detector and water transparency equivalent to that of previous pure-water operation periods. Using an Am-Be neutron calibration source the mean neutron capture time was measured to be 115 ± 1 µs, which corresponds to a Gd concentration of 111 ± 2 ppm, as expected for this level of Gd loading. This paper describes changes made to the water circulation system for this detector upgrade, the Gd loading procedure, detector commissioning, and the first neutron calibration measurements in SK-Gd.

Keywords: Water Cherenkov detector, Neutrino, Gadolinium, Neutron

1. Introduction

The 50 kiloton water Cherenkov detector Super-Kamiokande (SK) has been operating for more than 25 years and continues to provide measure-
ments and constraints covering a variety of topics in particle physics [1, 2] and astroparticle physics [3]. In order to extend the reach of SK to the as-yet unobserved diffuse supernova neutrino background (DSNB) flux, sometimes also called the supernova relic neutrino (SRN) flux, as well as improve SK’s performance during a supernova explosion in our own galaxy, the authors of Ref. [4] proposed adding gadolinium (Gd) to the detector’s water. As a result of its large neutron capture cross section and subsequent 8 MeV γ-ray cascade, the presence of Gd enhances the detector’s ability to identify and differentiate antineutrino-induced events from backgrounds via the coincidence detection of neutrons from inverse beta decay reactions: $\bar{\nu}_e(\mu) + p \rightarrow e^+(\mu^+) + n$.

Although the original proposal was primarily motivated by relic neutrino observations, this technique was also intended to extend to higher energy phenomena, allowing for neutrino-antineutrino discrimination in the atmospheric and beam neutrino fluxes as well as improved background rejection in proton decay searches.

After successful development of the technology using a 200 ton water Cherenkov demonstrator called EGADS [5], the Super-Kamiokande Collaboration initiated the SK-Gd project in 2015 with a final goal of adding 0.2% Gd$_2$(SO$_4$)$_3$·8H$_2$O (gadolinium sulfate octahydrate) by mass to the detector water. Following further research and development to scale the technology to the 50 kiloton SK, the first step of SK-Gd began with the loading of 13 tons of Gd$_2$(SO$_4$)$_3$·8H$_2$O, roughly 10% of the final target concentration, from July 14 to August 17, 2020.

In this paper we report the details of the Gd-loading and water circulation system, methods to control the flow of water in the detector, as well as calibration measurements to confirm the loaded Gd concentration. In Section 2 we describe the SK-Gd water system and its operation scheme (detailed specifications of the water system are described in Appendix A) before presenting details of the flow control method in Section 3. These can be compared with the flow configuration of previous detector phases described in Appendix B. The Gd loading for this first stage of SK-Gd is described in Section 4. Future prospects and concluding remarks are presented in Section 5.

2. SK-Gd Water System

With the exception of a few elements inherited from the SK ultrapure water system, the SK-Gd water system was newly designed and constructed to dissolve Gd$_2$(SO$_4$)$_3$·8H$_2$O into the detector water, pretreat it to remove
impurities, and then to circulate and continuously purify the resulting 50 kilotons of Gd-loaded water. The new system purifies the water in the same way as the previous system, removing contaminants such as bacteria, particulates, and most dissolved ions, while simultaneously preserving the dissolved gadolinium (Gd$^{3+}$) and sulfate (SO$_4^{2-}$) ions in solution. Water from the detector was continuously circulated and purified before, during, and after the Gd loading. A schematic diagram of the SK-Gd water system is shown in Fig. 1 and described below. Detailed specifications for each element in the system are listed in Appendix A.

2.1. Gd-dissolving System

The Gd-dissolving system is divided into two parts, responsible for the transportation of the Gd$_2$(SO$_4$)$_3$·8H$_2$O powder to a weighing hopper and then dissolving it into water in a buffer tank (the dissolving tank) via a circle feeder (Fig. 1). This setup allows for measured amounts of the Gd compound to be dissolved in order to achieve the desired concentration prior to returning the solution to SK. During dissolving, a fraction of the SK water being continuously recirculated is fed into a buffer tank (the solvent tank) before it is transferred to the dissolving tank to receive Gd$_2$(SO$_4$)$_3$·8H$_2$O from the shear blender. Water from the dissolving tank is used to mix and deliver the Gd$_2$(SO$_4$)$_3$·8H$_2$O powder in the shear blender before returning to the dissolving tank (Fig. 2). It is the circulation of water between the blender and dissolving tank that mixes and dissolves the powder into the SK water. The resulting solution is sent to the solution tank before being pumped to the pre-treatment system.

2.2. Pretreatment System

The pretreatment system and the main recirculation system were designed for SK-Gd in order to remove substances other than gadolinium and sulfate ions from the water. This design was tested with a 200-ton demonstrator experiment, the EGADS detector [5]. Following a passive one micron filter, in the first active stage of pretreatment gadolinium-loaded water from the solution tank is irradiated with ultraviolet (UV) light of sufficient energy to oxidize carbon and other compounds via a UV total organic carbon reduction lamp (TOC lamp). Any ionized impurities, including some radioactive impurities such as uranium and radium, are then removed by downstream ion-exchange resins.
To remove positively charged impurities, and radium ions in particular, a strongly acidic cation exchange resin, AMBERJET™ 1020 ("C-Ex Resin" in Fig. 1) is used. For the SK-Gd water system, this resin has been modified to contain gadolinium as the ion exchange group such that the resin’s cation exchange action never results in a loss of dissolved Gd content; \( \text{Gd}_2(\text{SO}_4)_3 \cdot 8\text{H}_2\text{O} \).
8H_2O powder of the same radiopurity as the primary solute was used to generate this custom resin.

In addition, negatively charged impurities are removed using a strongly basic anion exchange resin AMBERJET™ 4400 [7] (“A-Ex Resin” in the figure). This resin was introduced in order to remove uranium, which forms a negatively-charge uranyl complex in solution. As with the cation resin, this anion resin has been specially prepared, in this case with sulfate ions as the ion exchange group to prevent loss of sulfate from the Gd compound; electronic grade H_2SO_4 was used to produce the resin. In the pretreatment system the ratio of cation and anion exchange resin volumes is 1 : 1.

The Gd-loaded water is then sent to a UV sterilizer and a series of filters to remove bacteria introduced during the dissolution process. It should be noted that the pretreatment system is used only during dissolution and is otherwise bypassed during normal recirculation operation.

2.3. Water Recirculation System

During both gadolinium loading and subsequent data-taking, the Gd-loaded water in SK is continuously recirculated and purified to maintain high transparency. As shown in Fig. [1] there are two copies of most elements of the recirculation system installed in parallel such that water can be circulated at a flow rate of 60 m^3/h in either line or 120 m^3/h when both are operated simultaneously. It is therefore possible to maintain continuous recirculation with one line while performing maintenance on elements of the

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Figure 2: Schematic diagram of the shear blender.
other. The configuration of the recirculation system is similar to that of the pretreatment system, but with the 0.2 micron filters replaced by ultrafiltration (UF) modules as the final filtration stage. Additionally, the ratio of cation to anion exchange resin volumes is 1 : 2. In order to maintain precise control of the water temperature, heat-exchange units (HE) are installed immediately after the TOC lamps, just after the filtration stage, and just before the water is returned to the detector. Immediately before this final HE, a membrane degasifier (MD) is installed in order to remove Rn dissolved in the water.

Note that water rejected by the UF modules is returned to the first buffer tank in Fig. 1 for reprocessing so that no water is discarded by the system. Loss from the system is therefore limited to evaporation from the SK tank itself, which is less than a few liters per day, and from the membrane degasifier at a rate of between 30 and 60 ℓ/day depending on the flow rate. Water can be re-supplied from sources within the Kamioka mine as needed. The system achieves stable circulation at a fixed flow rate from the return pumps by automated control of the water levels in the two buffer tanks in the figure.

3. Water Flow in the Tank

The Gd$_2$(SO$_4$)$_3$ · 8H$_2$O powder was dissolved into SK while recirculating water from the SK tank through the water system described in the previous section. In order to efficiently achieve a uniform concentration of Gd in the tank, we injected Gd-loaded water at the bottom of the tank while removing pure water from its top as illustrated in Fig. 3. This was achieved by precise control of the supply water temperature and adjustment of the water flow at various water inlets and outlets on the tank. A brief description of the water flow control for the Gd loading is given in this section, whereas a more general description of the water flow in the Super-Kamiokande detector can be found in Appendix B.

3.1. Temperature Control

The temperature of the water being sent from the water system to the tank (known as “supply water”) is controlled at a precision better than 0.01 °C. This is accomplished by using a quartz thermometer which provides feedback to the heat-exchange unit installed in the final section of pipe before water is returned to the tank [8]. Prior to Gd loading, the water temperature in the tank was raised by setting the supply water temperature to
13.90 °C at Temperature Control Unit B in Fig. 1. Water was recirculated under these conditions for about 45 days. Afterwards the supply temperature was lowered to 13.55 °C to begin the Gd loading. This created an additional density difference between the Gd-loaded water and the pure water in the tank beyond that caused by the compound itself. In this way the spatial profile of the Gd-loaded water could be monitored by measuring the water temperature at different positions in the detector.

3.2. Water Injection and Extraction

Fig. 4 shows a schematic of the water piping and approximate flow rate at each location in the inner detector (ID) and outer detector (OD) regions of the tank. This piping was newly installed during a major in-tank refurbishment of the SK detector in 2018 and 2019 conducted in preparation for Gd loading. There are 12 inlets at both the top and bottom parts of the ID, eight in the annulus of the OD near the top and bottom, and four in the top and bottom OD endcaps. The end of each pipe is made of 50A polyvinyl chloride (PVC) tubing. In order to suppress convection due to the vertical flow of injected vertical water at the bottom, diffuser caps made of 14 cm diameter stainless-steel plates were installed in February 2020 on each of the bottom ID and bottom annular OD pipe outlets (see Appendix B). Diffuser cap installation was accomplished while the detector was filled with water through the use of a remotely-controlled submersible vehicle with a robotic arm [9].

In general, water was injected near the bottom and extracted near the top of the tank. In order to keep the height of Gd-loaded water uniform across the entire detector region, the ratio of water flow in the combined ID
and OD bottom region relative to that of the OD annular region was set to be roughly equal to the ratio of the ID and OD cross sections. During the initial stage of Gd loading, most of the water was injected through the OD bottom and OD annular outlets. After the rising front of Gd-loaded water reached the level of the bottom ID PMTs (on July 16, 2020), the water flow pattern was changed so that most of it was injected through the ID bottom and OD annular outlets. A similar adjustment was also made for outlets at the top of the OD and ID when the Gd-loaded water reached the top ID PMTs (August 13, 2020).

Figure 4: Water flow pattern in the SK tank during the Gd dissolving in 2020.

4. The Gd-loading

4.1. Gd Powder Specification

The Gd$_2$(SO$_4$)$_3$·8H$_2$O for SK-Gd had to fulfill stringent requirements regarding cleanliness to ensure it was free from problematic levels of contamination. As shown in Table I, criteria for radioactive impurities were set so that the additional event rate due to radioactive impurities in the powder – even after loading up to the final goal of 0.1% Gd concentration – would
be less than the unloaded background rates for SK’s solar neutrino measurements or supernova relic neutrino (SRN) searches \[10\]. In other words, less than a doubling of the pure water background rates for these analyses was deemed acceptable. In order to meet the requirements, chemical processing procedures were developed by an extensive R&D program \[5, 11\]. The calculations underlying the specifications of this ultraclean Gd$_2$(SO$_4$)$_3 \cdot$ 8H$_2$O powder are described elsewhere \[10, 11\].

Table 1: Criteria of radioactive impurities in Gd$_2$(SO$_4$)$_3 \cdot$ 8H$_2$O powder.

| Chain   | Isotope    | Criterion [mBq/kg] | Physics target |
|---------|------------|--------------------|----------------|
| $^{238}$U | $^{238}$U  | < 5                | SRN            |
|         | $^{226}$Ra | < 0.5              | Solar          |
| $^{232}$Th | $^{232}$Th | < 0.05             | Solar          |
|         | $^{228}$Ra | < 0.05             | Solar          |
| $^{235}$U | $^{235}$U  | < 30               | Solar          |
|         | $^{227}$Ac/$^{227}$Th | < 30          | Solar          |

The final production was conducted in batches of 500 kg. Every 500 kg lot of Gd$_2$(SO$_4$)$_3 \cdot$ 8H$_2$O powder was delivered in a special EVOH (ethylene-vinylalcohol copolymer) lined flexible container. Each batch was carefully screened at one (or more) of our collaborating underground scientific laboratories: Boulby in the UK, Canfranc in Spain, and the Kamioka Observatory in Japan \[12\].

Since the powder contained an average of 2.5% additional water left over from processing, the 13.2 tons of dissolved powder implies that the mass of Gd$_2$(SO$_4$)$_3 \cdot$ 8H$_2$O itself is 12.9 tons. This amount should yield a gadolinium (Gd) concentration in the SK tank of 0.011%, equivalent to an anhydrous gadolinium sulfate (Gd$_2$(SO$_4$)$_3$) concentration of 0.021%.

4.2. Loading Scheme

During Gd$_2$(SO$_4$)$_3 \cdot$ 8H$_2$O powder loading, the SK return water flow (after the “Return pumps” in Fig. 1) was set to 60 m$^3$/h. Of that, 48 m$^3$/h was directed to the main return line, while the rest was divided between the dissolving system (1.33 m$^3$/h) and its bypass line (10.67 m$^3$/h). In the dissolving system, the following powder dissolution processes were repeated:

1. Transfer 750 ℓ of the solvent – the return water from SK – from the solvent tank to the dissolving tank.
2. Using the circle feeder, put 8.2 kg of powder from the weighing hopper into the shear blender.

3. Circulate the solution between the blender and the dissolving tank for 15 minutes.

4. Stop the circulation, and transfer the solution from the dissolving tank to the solution tank. After that, return to process #1.

Each one of these cycles took about 30 minutes to complete, and the cycle ran continuously during the Gd loading period except when powder was being supplied to the weighing hopper. During this powder supplying process, the dissolution process itself was briefly interrupted, but the Gd loading of SK from the solution tank continued unabated. The dissolving cycle initially produced 0.9% Gd$_2$(SO$_4$)$_3$ water, which was then merged with the water from the bypass line to become 0.1% Gd$_2$(SO$_4$)$_3$. This in turn passed through the pre-treatment system (see Section 2.2) and was finally merged with the water from the main return line to produce the 0.02% Gd$_2$(SO$_4$)$_3$ water sent to SK.

4.3. Gd Loading History

Fig. 5 shows the cumulative mass of loaded Gd$_2$(SO$_4$)$_3$·$8H_2O$ powder for each cycle. It can be seen that the loading was very stable up to the target value of 13.2 tons, which corresponded to 5426 kg of Gd in the 49.47 kilotons of water in the SK tank and the water system. We assume 0.5% errors on both the amount of Gd and water; the estimated Gd concentration in the tank should therefore be 109.7±0.7 ppm (we refer to this Gd concentration as “0.011%” or “0.021%” Gd$_2$(SO$_4$)$_3$ concentration.).

The amount of Gd$_2$(SO$_4$)$_3$·$8H_2O$ powder added in one cycle was changed from 8.2 kg to 8.7 kg on August 4, 2020, and Gd loading was completed on August 17, 2020. Then the water recirculation at the rate of 120 m$^3$/h was started on August 18, 2020.

4.4. Water Transparency

As mentioned in Section 2, one of the main purposes of the water system is to keep the SK water transparency good enough for physics analyses. Although the transparency of the Gd-loaded water itself had been demonstrated with EGADS [3], the Gd-loading scheme, the water flow rate, and the water flow pattern in SK are different from those in EGADS. Here we report
Figure 5: The history Gd\(_2\)(SO\(_4\))\(_3\) \cdot 8\text{H}_2\text{O} powder loading in SK during 2020. On August 17, the amount of dissolved Gd\(_2\)(SO\(_4\))\(_3\) \cdot 8\text{H}_2\text{O} powder reached the target of 13.2 tons.

The effects of the Gd loading activity and the SK-Gd water recirculation on the water transparency.

The time variation of Cherenkov light attenuation length in the SK water tank measured with cosmic ray through-going muons is shown in Fig. 6. These results are used to correct observed PMT charges in the event reconstruction for all higher energy physics analyses such as atmospheric neutrino oscillations \[13\], nucleon decay searches, and long-baseline neutrino oscillations. The analysis details of the attenuation length measurement can be found elsewhere \[14\]. The attenuation length was about 90 meters just before loading Gd in the SK tank on July 14, 2020. After loading Gd\(_2\)(SO\(_4\))\(_3\) \cdot 8\text{H}_2\text{O} began, the attenuation length began to decrease. Around the end of August 2020, it reached a minimum value of around 75 m. Then, it started to recover, and had returned to almost 90 m at the beginning of December, 2020. The attenuation length became as long as it had been during the pure water phases of SK.
Figure 6: The light attenuation length measured with cosmic ray through-going muons from March 1, 2020, to March 1, 2021. From April 29, 2020, we lowered the temperature of the supply water to the bottom of the tank in order to simulate the Gd-loading water flow described in Section 3 and Appendix B.3. As a consequence, the water replacement efficiency and hence the transparency improved until the Gd-loading period began.

4.5. Determining the Gd$_2$(SO$_4$)$_3$·8H$_2$O Concentration from Direct Sampling in the SK Detector

During the Gd loading period, daily water samples were taken from calibration ports as depicted in Fig. 7. In the ID, two positions were used: the center-most port and the closest port to the OD in the $+X$ axis. In the OD, two positions were also employed: one in the $+X$ and another one in the $-X$ hemisphere.

The system to take the samples was rather straightforward (see Fig. 7). The sampling probe consisted of a flexible plastic tube 40 m long in which the last 25 cm were replaced by a stainless steel tube. This metal provided sufficient additional weight to compensate for the mild buoyancy of the flexible tube, and thereby kept the sampling probe straight even when it was completely submerged in the SK detector. The sampling probe was connected to a sampling system that consisted of three devices: a flow meter, a pump, and a conductivity meter which also functioned as a thermometer. At the end of this system there was a sampling port from which samples could be collected.
for later measurement of the Gd$_2$(SO$_4$)$_3$·8H$_2$O concentration with an Atomic Absorption Spectrometer (AAS). Excess water – in particular that used for flushing the sampling tube at each new position – was sent back into the SK water system, cleaned, and returned to the detector. Because a complete sampling operation (extracting water from different depths at a given calibration port) took about four hours, several measures were employed to avoid having to disturb the usual data taking of SK. Most of these measures focused on avoiding light leaks into the detector.

The general procedure to take samples was as follows:

1. The sampling probe was placed inside a darkened black tent above the chosen sampling port.
2. The probe was then immersed about 2 m into the SK detector and the pump was turned on to make sure that there was no air trapped in the system.
3. After waiting to allow the sampled water from this position to completely flush the system, the conductivity would become constant.

Figure 7: Water sampling system: a) (left) Schematic view of the position of the sampling ports and coordinate system in SK. b) (right) Schematic view of the sampling system. Φ-meter is a flow meter and Ω-meter is a resistivity meter.
4. Water flow, conductivity, and temperature were then recorded. A water sample was taken in a small (about 15 mL) bottle, upon which the position in the detector (sampling port and depth) and date were written.

5. The sampling tube was lowered 2 m further down into the detector.

6. Back to Step 3 until the lowest depth in the given port (Z=−16 m in the ID and Z=−18 m in the OD) was reached and sampled. The sampling tube was then pulled out of the detector and the system shut down.

Before loading Gd, the SK water conductivity was close to 55 nS/cm, the theoretical minimum, but after the addition of gadolinium and sulfate ions the conductivity rose to about 168 µS/cm. Because the pretreatment and water recirculation systems were specifically designed to remove all impurities except for these two ions, this should have made the conductivity a good indicator of the Gd$_2$(SO$_4$)$_3$ concentration.

Figure 8 shows the time evolution of conductivity in the ID center port position as a function of Z during the 2020 loading of Gd into the detector; the other ID port yielded very similar results and so is not shown. The gap between July 21 and July 29 was due to a problem in the sampling system. Gd loading started on July 14, but no significant change in the conductivity was observed until July 19. We can see a rather sharp boundary about 2 m thick existed between the Gd loaded layer (>100 µS/cm) and the pure water layer (<1 µS/cm). In agreement with the rate of water flow in the detector, this boundary advanced about 1.5 m/day.

Figure 9 shows the conductivity in the OD −X port; as was the case in the ID, the other OD port yielded similar results and so is not shown. The general behavior (boundary thickness and speed) was the same as in the ID, but we can observe that the boundary was about 1 m higher than in the ID due to the higher water flow in the OD. It can be seen that just after Gd loading was completed the conductivity, i.e. the concentration, was not homogeneous yet.

As observed above, conductivity should have been a good indicator of the Gd$_2$(SO$_4$)$_3$·8H$_2$O concentration. However, it was not a direct measurement; if anything unexpected had occurred and other ions were present in large amounts, then the conductivity would not have been a good indicator of the Gd$_2$(SO$_4$)$_3$·8H$_2$O concentration.

To make sure the Gd concentration was indeed as expected, most water
samples were analysed with an AAS. A Hitachi polarized Zeeman AAS of
the ZA3000 series was used with Pyro Tube HR cuvettes. The samples were
atomized at 2700 °C and illuminated with a Gd hollow-cathode lamp. For the
validation standard, samples containing 10 and 20 ppm Gd$_2$(SO$_4$)$_3$ · 8H$_2$O
were carefully prepared using the same Gd$_2$(SO$_4$)$_3$ · 8H$_2$O powder that was
used to load the SK detector. Calibration was performed before every series
of measurements and also in between them to monitor the measurement
stability. The uncertainty of a single measurement was about 3.5%

AAS measurements were conducted on samples taken during and after the
2020 period of Gd loading. This allowed us to confirm that the concentration
was becoming homogeneous using localized conductivity measurements as
well as the concentration final value. Figure 10 depicts the latest available
AAS measurements (from samples taken on March 25, 2021) in the ID and
OD regions, showing that the concentration had become completely homo-
genous with an average Gd$_2$(SO$_4$)$_3$ · 8H$_2$O concentration value of 271 ± 4
ppm. Taking into account the non-Gd components in the Gd$_2$(SO$_4$)$_3$ · 8H$_2$O
powder, this AAS result translates to an entirely uniform Gd concentration
in the SK water of 114 ± 2 ppm. This value is slightly larger than the esti-
mation from the weight described in Section 4.3, but the difference is within
the errors of the AAS measurement and the final concentration estimation.
4.6. Evaluation of Gadolinium Concentration by Am/Be Neutron Source

The thermal neutron capture cross section of gadolinium is about $10^5$ times larger than that of hydrogen as shown in Table 2. Thus, an increase of the Gd concentration in water results in a significantly shorter neutron capture time constant even at small concentrations in mass fraction.

By measuring the neutron capture time constant using an Am/Be neutron source ($^{241}\text{Am} \rightarrow ^{237}\text{Np} + \alpha, ^9\text{Be} + \alpha \rightarrow ^{12}\text{C}^* + n, ^{12}\text{C}^* \rightarrow ^{12}\text{C} + \gamma (4.4 \text{ MeV})$) deployed in the SK detector, the concentration of gadolinium was evaluated. The advantage of using an Am/Be source lies in the ability to identify its neutron emission due to the coincident emission of a 4.4 MeV gamma-ray. Placing the Am/Be source within a $5\times5\times5 \text{ cm BGO cube}$ (Fig. 11) allowed the initial gamma-ray to be detected by SK from the large number of scintillation photons generated by its passage through the BGO [17]. Following neutron capture and subsequent emission of a cascade of gamma-rays from the excited Gd nucleus, these delayed neutron-induced events were observed as a result of the de-excitation gammas Compton scattering off electrons in the SK water and thereby producing detectable Cherenkov light. The total gamma-ray energy produced from neutron capture on gadolinium is typically $\sim8 \text{ MeV}$, and as can be inferred from Table 2 primarily comes from two isotopes, $^{155}\text{Gd}$ and $^{157}\text{Gd}$: $n + ^{155}\text{Gd} \rightarrow$
$^{156}\text{Gd} + \gamma$'s [8.5 MeV in total], $n + ^{157}\text{Gd} \rightarrow ^{158}\text{Gd} + \gamma$'s [7.9 MeV in total].

The data were taken by deploying the Am/Be source into the SK inner detector through a calibration port near the center in the X-Y plane ($X = -3.9$ m, $Y = -0.7$ m). Three positions along the Z-coordinate were selected for periodic monitoring: $Z = 0$ m, $Z = +12$ m and $Z = -12$ m. When searching for neutron capture events in SK, specialized data acquisition triggers were applied: the so-called SHE (super-high-energy) and AFT (after) triggers [18]. An SHE trigger was generated whenever more than 60 ID photomultipliers tubes (PMTs) detected at least one photon within a 200 ns time window. These SHE triggers resulted in all photons detected by PMTs during the 35 $\mu$s following the SHE trigger being recorded, while those in a subsequent 500 $\mu$s window were also recorded by a sequentially issued AFT trigger. Gd(n,$\gamma$)Gd event candidates were then extracted from this recorded data by looking for greater than 30 active PMTs in a 200 ns time window and applying event vertex reconstruction [19].

The time distribution of neutron capture event candidates are shown in Fig. 12. Event selections were applied using the following event reconstruction parameters: the reconstruction timing goodness $g_t$ had to be greater than 0.4, the hit pattern goodness $g_p$ smaller than 0.4, and the event vertex located within 4 m from the Am/Be source position in the SK tank. Here,
Table 2: The abundance of isotopes in natural gadolinium and their thermal neutron (25 meV) capture cross sections for the Gd(n,γ)Gd reaction. Thermal capture cross sections and natural abundance of hydrogen (proton), oxygen, and sulfur – the only other elements present in significant quantities in SK’s Gd$_2$(SO$_4$)$_3$-loaded water – are also shown [15, 16].

| Isotope | Natural abundance ratio [%] | Thermal capture cross section [barn] |
|---------|-----------------------------|-------------------------------------|
| $^{152}$Gd | 0.20 | 740 |
| $^{154}$Gd | 2.18 | 85.8 |
| $^{155}$Gd | 14.80 | 61100 |
| $^{156}$Gd | 20.47 | 1.81 |
| $^{157}$Gd | 15.65 | 254000 |
| $^{158}$Gd | 24.84 | 2.22 |
| $^{160}$Gd | 21.86 | 1.42 |
| $^1$H | 99.99 | 0.33 |
| $^{16}$O | 99.76 | 0.0002 |
| $^{32}$S | 94.85 | 0.53 |

the timing goodness parameter is for testing the “narrowness” of the PMT hit timing residuals. The hit pattern goodness is for testing the azimuthal symmetry of the Cherenkov cone ($g_\rho = 0$ is perfectly symmetric, $g_\rho = 1$ is completely asymmetric). The definitions and typical distributions of these variables are in [20] [Sec. III B]. In addition, the initial SHE trigger events had to include 800 to 1300 active PMTs within 1.3 µs; doing so selected 4.4 MeV gamma-ray emission from the Am/Be source.

The neutron thermalization and capture time constants were considered when fitting the event candidate time distribution, as well as the presence of background events which were uniformly distributed in time. For the conversion from capture lifetime to Gd concentration, a Geant4 Monte Carlo simulation was applied (Fig. 13). More specifically, the Geant4.9.6p04 Monte Carlo simulation with its high precision and thermal scattering models was used to simulate the thermalization, capture, and other processes involving neutrons in the Gd-loaded water. G4NDL4.2 is applied as the neutron cross section library for this simulation. Interactions with the stainless steel Am/Be source container, the BGO scintillator, and the acrylic case which encloses the Am/Be+BGO components are also taken into account (Fig. 11). The neutron capture time constant was reasonably stable, within statisti-
cal errors, as shown by data taken between September and November 2020 (Fig. 14); it was also stable at several depths within SK. By applying Gaussian fitting to the 21 data points taken during this period, a mean neutron capture lifetime of $115 \pm 1 \text{ (sys.+stat.)} \mu s$ and a Gd concentration of $111 \pm 2 \text{ (sys.+stat.) ppm}$ were obtained. The Gd concentration obtained by the Am/Be measurement is consistent with the estimation in Section 4.3.

5. Conclusion

In the summer of 2020, 13.2 tons of $\text{Gd}_2(\text{SO}_4)_3 \cdot 8\text{H}_2\text{O}$ was dissolved into Super-Kamiokande and in so doing a large-scale (50 kiloton) gadolinium-enhanced water Cherenkov detector was realized for the first time in the
Figure 12: An example of the time distribution of neutron capture event candidates (black data points) and its fit function (red line), measured with the Am/Be source at the Z=0 m position on September 29, 2020. Each such measurement contained about 30 minutes of data with the Am/Be source deployed at various locations in the SK detector. Time zero is defined by the detection of the prompt 4.4 MeV gamma-ray BGO scintillation event. The neutron capture time constant is represented by $p_1$, while the thermalization time constant of $4.3 \mu s$ is derived from summed analysis of these measurements.

During this Gd loading, laminar flow of water in the tank was successfully achieved through careful control the Gd concentration and the water temperature. The Gd concentration throughout the tank became homogeneous shortly after the addition of Gd was completed. Next, the transparency of the Gd-loaded water improved after starting water recirculation with the new SK water system. Following a three month post-loading commissioning phase, the Gd-enhanced water’s transparency in SK became as good as that in the experiment’s previous pure water phases, demonstrating that the new SK-Gd water system works effectively for the purification of 0.021% Gd$_2$(SO$_4$)$_3$ water.

Based on this success, increasing the Gd concentration is planned for the next SK phase, which is currently expected to begin in 2022. The next target concentration is 0.06% Gd$_2$(SO$_4$)$_3$ or 0.03% Gd, which should result in 75% neutron tagging efficiency. Having gadolinium in the Super-Kamiokande water will enable the detector to positively identify low energy antineutrinos,
Figure 13: Neutron capture time constant as a function of the gadolinium concentration. The red points correspond to the Geant4 Monte Carlo simulation, while the black line corresponds to an approximate polynomial function. The horizontal blue band represents the mean neutron capture time constant measured with the Am/Be source, and the vertical blue band represents the derived concentration, which is consistent with the estimation from the weight (110 ppm) described in Section 4.3.

allowing it to make the world’s first observation of the diffuse supernova neutrino background flux via inverse beta decay.

**Acknowledgment**

We gratefully acknowledge the cooperation of the Kamioka Mining and Smelting Company. The Super-Kamiokande experiment has been built and operated from funding by the Japanese Ministry of Education, Culture, Sports, Science and Technology, the U.S. Department of Energy, and the U.S. National Science Foundation. Some of us have been supported by funds from the National Research Foundation of Korea NRF-2009-0083526 (KNRC) funded by the Ministry of Science, ICT, and Future Planning and the Ministry of Education (2018R1D1A3B07050696, 2018R1D1A1B07049158), the Japan Society for the Promotion of Science (JSPS KAKENHI Grant Numbers JP19H05807,JP26000003), the National Natural Science Foundation of China under Grants No.11620101004, the Spanish Ministry of Science, Uni-
Figure 14: The history of the neutron capture time constant in SK in the latter half of 2020, obtained from the analysis of Am/Be source data. Three positions along the Z-coordinate are shown here: Z=0 m (red circles), Z=+12 m (blue squares) and Z=−12 m (magenta triangles). The shaded area at the top of the plot indicates the neutron capture time constant in pure water [21]. Though the July 29 and August 5 data points at Z=+12 m are out of range (too high), they are nevertheless consistent with the pure water shaded region within about one sigma.

versities and Innovation (grant PGC2018-099388-B-I00), the Natural Sciences and Engineering Research Council (NSERC) of Canada, the Scinet and Westgrid consortia of Compute Canada, the National Science Centre, Poland (2015/18/E/ST2/00758), the Science and Technology Facilities Council (STFC) and GridPP, UK, the European Union's Horizon 2020 Research and Innovation Programme under the Marie Sklodowska-Curie grant agreement no.754496, H2020-MSCA-RISE-2018 JENNIFER2 grant agreement no.822070, and H2020-MSCA-RISE-2019 SK2HK grant agreement no. 872549.
Appendix A. Specifications of SK-Gd Water System

Appendix A.1. Gd Dissolving System

- **Measuring hopper** – Size: 700 mm ϕ, 900 mm H; material: SUS304; inside surface finish: buffing # 250; effective volume: 200 ℓ.

- **Circle feeder** – Maximum supply: 59.5 kg/min; minimum supply: 22.3 kg/min (at the factory test); rotation speed: 5.49-0.55 rpm; material: SUS304 (powder contact components w/ Teflon coating); motor: 1.5 kW 4 pole.

- **Shear blender** – The shear blender consists of three parts:
  - **Dissolving hopper** – Volume: 66 ℓ; material: SUS316L.
  - **Self-priming sanitary pump** – Model: SIPLA Adapta 28.1; flow rate: 23 m³/h; head: 20 m; power: 7.5 kW (4 pole, 200 V); rotation speed: 1750 rpm.
  - **Shear pump** – Model: EMP305; flow rate: 15 m³/h; head: 10 m; power: 7.5 kW (2 pole, 200 V); rotation speed: 3500 rpm.

- **Solvent tank** – Tank capacity: 6 m³ (1922 mm ϕ, 2350 mm H); material: PE; thickness: 9.5 mm.

- **Dissolving tank** – Tank capacity: 4 m³ (1740 mm ϕ, 1780 mm H (cylinder), 280 mm H (taper)); material: PE; thickness: 9 mm.

- **Solution tank** – Tank capacity: 6 m³ (1922 mm ϕ, 2350 mm H); material: PE; thickness: 9.5 mm.

- **Pumps** – Three pumps are in the dissolving system:
  - **Supply pump after solvent tank** – Flow rate: 48 m³/h; head: 20 m; power: 5.5 kW (2 pole, 200 V); speed: 3600 rpm.
  - **Transfer pump after dissolving tank** – Flow rate: 48 m³/h; head: 20 m; power: 5.5 kW (2 pole, 200 V); speed: 3600 rpm.
  - **Injection pump after solution tank** – Flow rate: 12 m³/h; head: 45 m; power: 3 kW (2 pole, 200 V); speed: 3600 rpm.
Appendix A.2. Pretreatment System

- **Prefilter** – Nominal pore size: 1 µm; size (one module): 62 mm φ outer, 30 mm φ inner, and 750 mm length; material: polypropylene; number of modules: 6.

- **TOC lamp (UV oxidation)** – Wavelengths 253.7 nm and 184.9 nm; power: 0.81 W; Chiyoda Kohan Steritron WOX (lamp: CX1501).

- **Cation exchange resin tank** – Size: 1600 mm φ 1460 H; material: SUS304; resin volume: 1200 ℓ; resin type: AMBERJET 1020(Gd).

- **Anion exchange resin tank** – Size: 1600mm φ 1460mm H; material: SUS304; resin volume: 2400 ℓ; resin type: AMBERJET 4400(SO₄).

- **Middle filter** – Nominal pore size: 1 µm; size (one module): 62 mm φ outer, 30 mm φ inner, and 750 mm length; material: polypropylene; number of modules: 6.

- **UV sterilizer** – Wavelength 253.7 nm; power: 0.3 W; Chiyoda Kohan Steritron UEX (lamp: CS1001N).

- **Postfilter** – Nominal pore size: 0.2 µm; size (one module): 62 mm φ outer, 30 mm φ inner, and 750 mm length; material: polypropylene; number of modules: 6.

Appendix A.3. Water Recirculation System

- **Return water filter** – Nominal pore size: 1 µm; size (one module): 62 mm φ outer, 30 mm φ inner, and 750 mm length; material: polypropylene; number of modules: 40.

- **First buffer tank** – Tank capacity: 10 m³ (2280 mm φ, 2780 mm H); material: PE; thickness: 12.5 mm.

- **Heat exchange unit (HE) after the relay pump** – Heat transfer area: 15.80 m²; plate material: SUS316 (electrolytic polishing finish); plate gasket: EPDM with PTFE coating.

- **TOC lamp (UV oxidation)** – Wavelengths: 253.7 nm and 184.9 nm; power: 4.02 W; Chiyoda Kohan Steritron WOX (lamp: CX1501).
• **Cation exchange resin tank** – Size: 2100 mm $\phi$ 1610 mm H; material: SUS304; resin volume: 2400 ℓ; resin type: AMBERJET1020(Gd).

• **Anion exchange resin tank** – Size: 2100 mm $\phi$ 1610 mm H; material: SUS304; resin volume: 4600 ℓ; resin type: AMBERJET4400(SO$_4$).

• **Middle filter** – Nominal pore size: 1 $\mu$m; size (one module): 62 mm $\phi$ outer, 30 mm $\phi$ inner, and 750 mm length; material: polypropylene; number of modules: 40.

• **UV sterilizer** – Wavelength: 253.7 nm; power: 0.97 W; Chiyoda Kohan Steritron UEX (lamp: CS1001N).

• **Ultrafiltration modules (UF)** – Nitto NTU-3306-K6R; inner/outer diameter of the capillary membrane: 0.7 mm / 1.3 mm; effective membrane area: 30 m$^2$/module; number of modules in one unit: 12; molecular weight cut-off: 6000; processed water TOC: $\leq$ 5 ppb; material: polysulfone (capillary membrane), polysulfone (housing).

• **Second buffer tank** – Tank capacity: 20 m$^3$ (2710 mm $\phi$, 3810 mm H); material: PE; thickness: 15 mm.

• **Heat exchange unit after the supply pump** – Heat transfer area: 24.74 m$^2$; plate material: SUS316 (electrolytic polishing finish); plate gasket: EPDM with PTFE coating.

• **Membrane degasifier (MD)** – DIC SEPAREL® EF-040P-JO; module size: 180 mm $\phi$ 673 mm H; number of modules: 60; operation pressure: $-92$ kPa; purge gas: radon-free air [14, 22]; purge gas flow rate: 1 ℓ/min (per module).

• **Final Heat exchange unit** – Heat transfer area: 21.15 m$^2$, plate material: SUS316; plate gasket: butyl (isobuthene-isoprene) rubber.

• **Pumps** – Pumps in the recirculation system:
  - **Return pump after Super-K tank** – Flow rate: 60 m$^3$/h; head: 70 m; power: 36 kW (200 V); speed: 3600 rpm.
  - **Relay pump after first buffer tank** – Flow rate: 60 m$^3$/h; head: 40 m; power: 18 kW (200 V); speed: 3600 rpm.
  - **Supply pump after second buffer tank** – Flow rate: 60 m$^3$/h; head: 62 m; power: 22 kW (200 V); speed 3600 rpm.
Appendix B. Water Flow in the SK Tank

Precise control of the water flow in the Super-Kamiokande tank is important not only for gadolinium loading, but also for maximizing the physics performance of the detector. Such precise control plays critical roles in reducing radioactive backgrounds in the detector’s fiducial volume as well as in improving water transparency. In this section, the operation and modeling of the water flow in the SK detector are described in more detail.

Appendix B.1. Water Piping

As illustrated in Fig. B.1, there are six groups of water inlets/outlets in the SK tank. The total flow and flow direction for each group can be individually adjusted by operating a set of valves located on top of the tank. These water pipes were upgraded during the refurbishment of the Super-Kamiokande detector in 2018–2019 to allow more precise control of water flow and also to permit a higher maximum total flow rate of 120 m$^3$/h (previously 60 m$^3$/h). In addition, diffuser caps, illustrated in Fig. B.15, were installed at all ID bottom and OD annular outlets in order to minimize the zones of turbulence near the water ejection points. It should be kept in mind that the separation between the ID and OD regions is not watertight and there potentially exists water flow between them.

Figure B.15: Illustration of water flow near the ID bottom outlets A) without, and B) with the diffuser caps installed in February 2020.
Appendix B.2. Water Flow Model

Typically, water is injected into the bottom region of the tank and extracted from the top. Once inside the tank, this injected water gradually becomes warmer due to heat produced by PMTs and the magnetic field compensation coils\(^1\); this heating results in a positive water temperature gradient from the bottom to the top of the detector.

Figure B.16 shows typical temperature profiles along the Z (vertical) coordinate of the detector during the SK-IV (2009-2018) and SK-V (2019-2020) phases. The region at a roughly constant temperature \((Z \sim -10 \text{ m for SK-IV})\) indicates a convection zone, while the regions with constant slope as a function of \(z\) indicate a steady vertical flow. During the SK-V period there is almost no convection region inside the ID, and the steady flow seems to be established at \(Z > -5 \text{ m}\).

![Figure B.16: Typical water temperature distributions in the SK tank during the SK-IV (left) and SK-V (right) periods. The left figure was taken from Ref. [19].](image)

The picture described above is supported by evaluating low energy background rates – events with a few MeV – in the detector. The dominant source of the low energy events at Super-Kamiokande is radon (Rn) emanated from the detector components. This Rn dissolves into the SK water and is then carried to various locations by water flow. If there is convection, Rn from the

\(^1\)There could also be heat transfer from the rock surrounding the detector tank, whose contribution is unknown. However, it was found that temperature change of water in the SK detector is consistent with the sum of the expected impacts from the PMTs and the coil.
PMTs and their associated hardware is quickly distributed into the center part of the detector and thus increases low energy backgrounds in the fiducial volume. In contrast, having slow, steady flow from bottom to top naturally minimizes such issues, in part because the Rn emanated from surfaces has more time to decay before reaching the fiducial volume. Figure B.17 shows vertex distributions for events in the range of $3.99 < E_{\text{kin}} < 4.49$ MeV for SK-IV and SK-V. Enhancement of the event rate in the convection region at $Z < -10$ m in SK-IV was clearly observed, and increased Rn concentration in the bottom convection region was directly observed by analyzing water sampled from the detector tank [23]. Such enhancement was largely eliminated in SK-V, in which convection was significantly suppressed by water flow tuning. This expanded the low background region in the center of the detector and improved the experiment’s low energy solar neutrino measurements.

Figure B.17: Vertex distributions in $z$ vs. $r^2$ for events in the range $3.99 < E_{\text{kin}} < 4.49$ MeV for SK-IV (left) and SK-V (right). Selection cuts based on those used for the solar neutrino analysis of SK data [19], except for the tight fiducial volume cut, are applied. The livetime for the SK-IV sample is 2047 days, while it is 107 days for the SK-V sample. Compared to the SK-IV configuration, the convection region (high event rate region) was significantly reduced in SK-V.

The size of the convection region is largely determined by the water injection scheme. On the other hand, the flow in the steady flow region is mostly governed by the heat produced in the tank and is almost independent of the water injection pattern. In the steady flow region, the water temperature at a
given Z position is equivalent in the ID and OD (right panel of Figure B.16), which indicates no major water flow between them. Under these conditions, the temperature gradient along the Z direction, \(dT/dZ\), can be described as

\[
\frac{dT}{dZ} \propto Q(\nu_Z),
\]

(B.1)

where \(Q\) is the heat injected to the system and \(\nu_Z\) is the vertical speed of the water flow in the tank. This relationship can be applied to the bulk behavior of the water, and also to the local behavior at a given location in the tank. In addition, \(dT/dZ\) is approximately a constant across the steady flow region. Therefore, we can deduce a simple relation that the vertical flow speed at a given position \(\nu_Z(X,Y,Z)\) is proportional to the amount of heat injected to the same position, \(Q(X,Y,Z)\).

This relationship indicates that the water flow speed is not constant across the detector volume, because the distribution of the heat sources (i.e. the PMTs and the magnetic field compensation coil) are not uniform. As illustrated in Figure B.18, the flow is expected to be faster near the PMTs and the detector walls where the coils are mounted, while it becomes much smaller near the detector center. The slowness of the vertical flow in the central region was confirmed by injecting Rn-rich water into the SK tank and tracing its spatial distribution over time.

This flow configuration works well for reducing Rn backgrounds in the
SK detector. Most of the Rn-rich water near the PMT structure flows vertically at a relatively fast speed, and then returns to the water purification system without going through the central region of the detector. The slowness of water replacement in the ID region also helps reduce Rn backgrounds, as most of the Rn atoms decay before reaching the fiducial volume. Additionally, it should be noted that long water attenuation lengths have been maintained with this configuration, typically ~90 m, based on measurements with cosmic-ray muons.

Appendix B.3. Water Flow for Gd Loading

Although this steady water flow is ideal for studying low energy neutrinos, it was not ideal for Gd loading as this flow does not efficiently replace water, especially near the central part of the detector. Therefore, we lowered the supply water temperature at the same time we started injecting Gd, in order to create a larger density difference between the new Gd-loaded water and the pure water remaining in the tank. This density difference ensured the efficient replacement of water throughout the detector volume as described in Section 3.

Movement of the Gd-loaded water in the tank was tracked by monitoring water temperature. Figure B.19 shows the time evolution of water temperature at different locations around the period of Gd loading. Arrival of Gd-loaded water at a given location in the detector was clearly observed with a sharp drop of water temperature there. This demonstrates that Gd-loaded water successfully replaced pure water from the bottom, and that the replacement uniformly occurred in both ID and OD regions. Smaller fluctuations of water temperature after the sharp drops were observed, which indicate that there was some turbulence within the Gd-water region. After recirculating water for another month after the conclusion of Gd loading, the temperature fluctuations naturally faded away and a stable detector condition was realized.
Figure B.19: Time evolution of water temperature around the 2020 Gd loading period at different vertical positions in the SK inner detector (top) and outer detector (bottom). Vertical dashed lines indicate the start and end dates of Gd loading. Relative biases of the temperature sensors were corrected using data taken between July 1, 2020, and July 10, 2020, during which time the water in the tank was in a state of full convection.

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