Maleic anhydride grafted onto high density polyethylene with an enhanced grafting degree via monomer microencapsulation

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1. Introduction

Plastic is economical, simple, adaptable, and waterproof. One of plastic types is polyolefin [1]. Polyolefin fibres are commonly derived from ethylene and propylene—polymers or copolymers of olefin hydrocarbons, which emanates from naphtha cracking of crude oil. The first extrusion of polyolefin fibres were applied from the low density polyethylene (LDPE) in 1930s after the synthesis of LDPE employed by Imperial Chemical Industries. Ziegler developed a process in addition polymerization for linear high density polyethylene (HDPE) in 1954, from which relatively small amounts of multi-filaments and monofilaments have been yielded for an amount of tiny-volume implementations requiring characteristic properties of the HDPE [2]. Whilst these fibres had resoundingly enhanced properties over the LDPEs, HDPE fibres of relatively low melting point could not portray a crucial role in textile general applications.

The presentation of multicomponent polymer frameworks depends to an enormous degree on the interface between periods of practically unique nature. Regularly, polymer blends show stage partition or a fairly little miscibility window due to the polymer-polymer interface being not thick enough to permit transfer of stress from one stage to the interface, and in this manner to the next stage. Chain adaptability changes from one polymer to the next due to contrast in science of macromolecules as far as disparate polarities, degree of polymerization, firmness, and conformational or configurational conditions of polymers in a polymer blend (Mostafapoor et al., 2020) [3]. In the compatibilized polymer blend, it is every now and again conceivable to tailor two chains of various characters by the utilization of a coupling specialist, known as "compatibilizer." We require to consider the mechanical properties as the primary mark of interface of compatibilized polymer mixes, while examinations on interface are as yet not many and spread. Prediction of interfacial tension of compatibilized polymer blends is a remarked-spiking problem, at which experiments and theories hardly corroborate each other. It was also strive to reveal the relationships between particle size and its distribution, as well as rheological properties of blends compatibilized with different amounts of HDPE-g-maleic anhydride precursor [4] (Hassanpour Asl et al., 2018).

Grafting reactive monomers such as glycidyl methacrylate (GMA) and MAH onto polyethylene was the subject of several works from different groups. High-density polyethylene (HDPE) is among the versatile polymers because of its suitable processability and acceptable mechanical properties [5]. The free-radical grafting of GMA onto HDPE in the
presence of styrene, as a comonomer proposed that increasing the DCP content led to an improvement in GMA grafting yield. Furthermore, the reaction time imparts minor effect on the final processing torque, and an interaction between DCP and GMA content was observable [6]. From our best knowledge, the modification of polyethylene via free-radical copolymerization grafted with maleic anhydride (MAH) as polar monomers is one of the crucial techniques in polyolefin functionalization for commercial applications owing to high activity and reliable processing capability [7, 8, 9]. The usage of MAH in the grafting process is highly preferred due to only a few oligomers emerged and no homopolymerization occurred during the grafting process [10, 11]. MAH is suitable for grafting onto polyethylene owing to its low reactivity towards itself and it directly grafts onto the polymer [12].

The grafting process of MAH to HDPE initially commenced in 1987 through blending process in a patent [13]. The blending process was then continuously applied to many studies of polymer such as grafting MAH into LLDPE [14], combining polystyrene (PS) and acrylonitrile-butadiene-Styrene (ABS) [15]. Reactive blending of GMA to PET-PP was known to yield grafting degree in between 1.58 to 3.68% [16] (Jazani et al., 2017). The other methods to attach MAH are ultrasonic initiation [17], extrusion process [18], one-step reactive melt mixing [19], ring-opening polymerisation [20], and solution-mixing and precipitation approach [21].

The key to an effective grafting of a functional group into a polymer molecule is reaction process. The occurred reaction must have an ability to direct the process mainly in a molecular approach. Hence, we adopt a process that mainly plays role in many organic applications, called microencapsulation to resemble the similar process in attaching a functional group to a main body molecule, here we directed a HDPE polymer. Microencapsulation is driven by controlled diffusion at the termination stage where the monomer molecules are trapped in the polymer pore so that segmental diffusion is closer which results in easier polymer-monomer interaction [22, 23, 24, 25, 26, 27, 28, 29, 30]. A Similar method has been recognized to propose the impact of HDPE-grafted maleic anhydride (HDPE-g-MAH) on the stabilization of phase morphology in the HDPE-based ternary polymer blends with inherent tendency to form core–shell microstructure at which the feasibility of yielding better composite droplets to form superior blends with enhanced rheological, morphological, thermal, and mechanical properties was obtained [31]. In this study we adopted the fundamental principle of microencapsulation by using a simple technique to enhance the grafting degree (GD) of MAH onto HDPE polymer before the reactive blending subsequently deployed.

| Parameters         | mHDPE   | HDPE-MAH |
|--------------------|---------|----------|
| Monomer conversion/% | 84.4    | 70.4     |
| Gel fraction content/% | 86.5    | 88.3     |
| Grafting degree/%   | 1.88    | 1.39     |

**Table 1.** Conversion values of monomers, gel fractions, and grafting degrees of mHDPE and HDPE-MAH (at 40% DCP and rotation rate of 80 rpm).

**Figure 1.** Torque graph against time for mHDPE and HDPE-MAH samples (DCP concentration of 40% mol and a rotation rate of 80 rpm).

**Figure 2.** An illustration to the different manifestation of MAH copolymerization in mHDPE-g-MAH and HDPE-g-MAH in this study.

**Figure 3.** FTIR spectra of samples (a) of HDPE origin, (b) mHDPE and (c) HDPE-MAH (at 40% DCP and rotation rate of 80 rpm) resulting from extraction with soluble xylene fraction.

2. **Experimental method**

2.1. **Materials**

The materials used in this study were HDPE with MFR = 0.01 g min⁻¹ and ρ = 0.950 g cm⁻³ obtained from PT Basell, Aldrich dicumyl peroxide,
acetone, chloroform, maleic anhydride, and xylene as well as all solvents used were products E-Merck with analytical grade.

2.2. Tools

The tools used in this study were, Tabai 6PHH-200 oven, Haake Rheomix 600p Roller Rotors R 600, analytical balance, Yamato brand DP 33 vacuum oven, soxhlet extraction equipment, hot press and cold press Gonno brand. The instrument used to test the characteristics of the MFR Dynisco Polymer Test brand, Perier Elmer brand Fourier transform infrared (FTIR) spectrophotometer, Nukleuar Magnetic Resonance (SS-NMR) Bruker Avance III spectrometer 300 MHz and Differential Scanning Calorimetry (DSC) brand Mettler Toledo 1 Star and Mettler Toledo 1 Star's Thermal Gravimetry Analysis (TGA).

2.3. The encapsulation process of HDPE

Into a 2.0 L aluminium container which was containing 2.0 kg of HDPE, 100 ml of 5% MAH solution was added in the acetone, stirring evenly and tightly closed. Every 10 min for an hour, the container is opened and the sample is stirred evenly so that the evaporation of acetone vapor occurs, then immediately closes again. The process continued for 6 h, adding 100 mL of 10% MAH solution in acetone while stirring evenly and closed again. Samples in containers are opened, stirred evenly, and tightly closed every hour for 6 h. The microencapsulation process has occurred marked by opaque HDPE colors. The microencapsulated polymer is noted as mHDPE.

2.4. The preparation of mHDPE-g-MAH, HDPE-g-MAH

A 50 g of mHDPE samples and DCP initiator with various concentration of 0; 10; 20, and 40% mole are mixed into the mixing container on the Haake Rheomix 600p with a blending temperature of 200 °C and a blending rate of 40; 60; 80; 100 rpm for 4 min. During the blending process the torque value is recorded at each time change. Torque is the rotational energy (Nm) used during the polymer blending process. Grafting products using microencapsulation are named mHDPE-g-MAH. While the mixing products are namely HDPE-g-MAH.

2.5. Analysis of HDPE-g-MAH grafting levels using acid-base titration

The sample was refluxed with xylene for 30 min, then cooled to a temperature close to 800C, then added with 0.2 N potassium hydroxide with ethanol solvent. Furthermore refluxed again for 15 min. The reflux sample is added with the phenolphthalein indicator, then titrated with 0.2 N hydrochloric acid/isopropyl alcohol until the color changes from pink to clear. The volume of hydrochloric acid/isopropyl alcohol used is recorded, then the grafting degree is calculated [26].

Table 2. Differences of melting (Tm) and crystallization temperature (Tc) of grafted and non-grafted HDPE and mHDPE.

| Sample  | Tm (°C) | Tc (°C) |
|---------|---------|---------|
| HDPE (g) | 125     | 116     |
| mHDPE(g) | 130     | 116     |
| HDPE(t) | 124     | 116     |
| mHDPE (t) | 124     | 116     |

Figure 4. FTIR spectra of samples (a) HDPE origin, (b) mHDPE and (c) HDPE-MAH (at 40% DCP and rotation rate of 80 rpm) extracted by organic xylene gel fraction.

Figure 5. DSC thermogram Tm values for samples (a) mHDPE gel fraction, (b) HDPE-g-MAH soluble fraction, (c) mHDPE soluble fraction and (d) HDPE-MAH gel fraction (40% DCP and 80 rpm torque rate).

Figure 6. DSC thermogram of sample Tc values (a) mHDPE soluble fraction, (b) HDPE-MAH gel fraction, (c) HDPE-MAH soluble fraction, and (d) mHDPE gel fraction (40% DCP and 80 rpm torque rate).

Figure 7. TGA thermogram of samples (a) mHDPE soluble fraction, (b) HDPE-MAH soluble fraction, (c) mHDPE gel fraction and (d) HDPE-MAH gel fraction (40% DCP and torque rate 80 rpm).
### 2. Chemical Shifts of Carbon in mHDPE Molecule

| Chemical Shift/ppm | C from functional groups assignment                  |
|-------------------|------------------------------------------------------|
| 177               | C (C=O at succinic anhydride)                        |
| 157               | C (C=O at maleic anhydride)                         |
| 30 and 32         | C (CH₂), polymer chain                              |
| 24                | C (CH₃), from the ring of succinic anhydride          |
| 13                | C (CH₃)                                              |

### 3. Result and Discussion

#### 3.1. Copolymerization of Maleic Anhydride Paste in HDPE

Figure 1 displayed the torque graph with respect to the mHDPE and HDPE-MAH sample times. After HDPE plasticization at the beginning of the reaction, the torque of the mHDPE sample rises to a maximum of 27 Nm and then gradually drops to 20 Nm at the end of the reaction. Whereas the maximum peak HDPE-MAH sample has a torque of 48 Nm, and drops to 40 Nm at the end of the reaction which is much higher than PET/PP-g-GMA with an addition of strontium in the similar range of time (1–4 min) [16]. This behaviour suggested that the stability and improved mechanical strength of HDPE-g-MAH could be obtained by employing our simple blending method.

A large torque value in the HDPE-MAH sample indicates that many cross-linking reactions occurred, whereas in the mHDPE sample there will be more MAH grafting reactions. By using the monomer microencapsulation method, MAH is trapped in the HDPE pore, so that diffusion-segmental is closer, the polymer-monomer is more evenly distributed and the interaction is facilitated to cause MAH attached more to the HDPE. The monomer conversion value and the grafting degree in the formation of the paste copolymer for the mHDPE and HDPE-MAH samples are shown in Table 1. The monomer conversion and the mHDPE paste level are greater than HDPE-MAH.

Figure 2 display an illustration to the different path of grafting process between HDPE and pre-microencapsulated HPDE. We can observe that the MAH was attached when the polymer melting underwent.

Figure 3 is the FTIR spectrum of the dissolved mHDPE and HDPE-MAH fractions. The process of maleation can be seen in FTIR uptake at wavenumbers of 1700 cm⁻¹ to 1800 cm⁻¹. At wavenumbers 1720 cm⁻¹ and 1780 cm⁻¹ (image insert), quantitatively the ratio of absorbance values calculated at wavenumbers 1720 cm⁻¹ and 1780.

Figure 4 showed the FTIR spectrum of mHDPE and HDPE-MAH gel fractions. The absorbance intensity at wavenumbers of 1780 cm⁻¹ and 1720 cm⁻¹ compared to the absorbance at wavenumber 1460 cm⁻¹ in HDPE-MAH samples is greater than that of mHDPE.

Thermal characterization using DSC was carried out to investigate the response of polymers to heating in which used to study the melting and crystallization of HDPE-g-MAH polymers. The DSC set-up is composed of a measurement chamber and a computer. The DSC thermogram showing the melting point, Tm of the mHDPE and HDPE-MAH samples is shown in Figure 5. The quantitative values of the thermogram are listed in Table 2. The Tm values appear unchanged between the mHDPE and HDPE-MAH soluble fraction samples, although for both sample gel fractions there are difference. This is because MAH is attached to HDPE in small amounts with a small grafting degree so it does not cause Tm changes.

We may see that the Tc of all HDPE samples remain constant which suggested that the microencapsulation process proposed stability of the samples and the main characteristic of HDPEs were not affected by the process and gel fraction. In situ polymerization using microencapsulation method is generally deployed in two stages. The initial process is the emulsion formation for liquid core or suspension for solid core. Subsequently, reactive monomers (or soluble prepolymers) would slowly precipitate on the core particles under the action of heat and catalysts [32]. These stages play significant role in the crystallization process that occurred in grafting process in which Tc remaining constant.

The melting temperature of the polymer, Tm in Figure 5 and the quantitative values in Table 2 showed that no change occurred in the value of Tm in the mHDPE and HDPE-MAH samples both the dissolved and gel fractions. This means that the presence of MAH stuck in small
amounts does not affect the crystallinity of HDPE. We may notice that the Ts of all HDPE-MAHs are ranged in between 120 to 130 °C as displayed in Figure 6 which is much lower than MHDPE/EVOH/PA-6 compatibilized with HDPE-g-MAH (150–180 °C). This suggested that the crystallization kinetic is more facilitated in at low temperature. The HDPE-g-MAH compatibilizer capable to ease the polymer chain mobility [31].

Figure 7 is a TGA thermogram of the mHDPE sample and HDPE-MAH soluble fraction and gel fraction. The quantitative percent decomposition values are listed in Table 3. In Table 3, the percentage of mHDPE decomposition of the dissolved fraction is greater than that of the HDPE-MAH sample at 325 °C and 425 °C. Meanwhile the gel fraction was relatively unchanged. We may observe that the percentage of decomposition in the temperature range of 325–425 °C which suggested the mass loss of MAH in HDPE mostly occurred in this temperature range. This shows that MAH is relatively more attached to the mHDPE sample. The change in percentage of decomposition can be clearly observed by implying the first derivative calculation, dy/dx, graphs of the calculation results which are listed in Figure 8. The gradient of the gel fraction sample does not change, while for dissolved fraction samples there is a difference between mHDPE and MAH.

The 13C-NMR analysis was employed to confirm the structure of attached MAH to HDPE in the form of succinate, maleic or acyclic succinic anhydride. The spectrum in Figure 9 displays the chemical shift that shows the type of carbon derived from certain functional groups summarized in Table 4. The intensity of the chemical shift 177 ppm is greater than 157 ppm, this indicates that MAH is attached more in the form of succinic anhydride than in the form maleic anhydride. Also, a chemical shift of 24 ppm indicates carbon (-CH2) from succinic anhydride [33]. The structure molecules fragmentation was displayed in Figure 10.

4. Conclusion
MAH paste copolymerization on HDPE using a monomer microencapsulation method with a DCP initiator can increase the degree of paste compared to the ordinary paste method. Samples using the monomer microencapsulation method, mHDPE-g-MAH have the grafting degree of 1.88%, whereas with the usual method, HDPE-g-MAH has the grafting degree of 1.39%. Our study implies that the simple blending technique could deliver similar or even improved properties of HDPE-g-MAH that is widely used as a compatibilizer to other polymers. The improved grafting degree using this simple method could bring an overview for the future work to improve more the grafting degree by employing our method.

Declarations

Author contribution statement

Iman Rahayu: Conceived and designed the experiments; performed the experiments; Acknowledgements

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Additional information

No additional information is available for this paper.

Author contribution statement

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Declared competing interests

The authors declare no conflict of interest.
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