The enhanced pyrocatalysis of the pyroelectric BiFeO$_3$/g-C$_3$N$_4$ heterostructure for dye decomposition driven by cold-hot temperature alternation

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Abstract: The BiFeO$_3$/g-C$_3$N$_4$ heterostructure, which is fabricated via a simple mixing-calcining method, benefits the significant enhancement of the pyrocatalytic performance. With the growth of g-C$_3$N$_4$ content in the heterostructure pyrocatalysts from 0 to 25 %, the decomposition ratio of Rhodamine B (RhB) dye after 18 cold-hot temperature fluctuation (25 °C - 65 °C) cycles increases at first and then decreases, reaching a maximum value of ~ 94.2 % at 10 % while that of the pure BiFeO$_3$ is ~ 67.7 %. The enhanced dye decomposition may be due to the generation of the internal electric field which strengthens the separation of the positive and negative carriers and further
accelerates their migrations. The intermediate products in the pyrocatalytic reaction also have been
detected and confirmed, which proves the key role of the pyroelectric effect in realizing the dye
decomposition using BiFeO3/g-C3N4 heterostructure catalyst. The pyroelectric BiFeO3/g-C3N4
heterostructure shows the potential application in pyrocatalytically degrading dye wastewater.

**Keywords:** Pyroelectric material; BiFeO3; g-C3N4; Heterostructure; Pyrocatalysis.

1 Introduction

The limited clean water has been seriously polluted by a large number of the chemical dyes
discharged from the textile and printing industries, which results in a heavy environmental crisis [1, 2]. Photocatalysis, as an advanced oxidation technology, in which the clean solar energy can drive
photocatalyst to generate free radicals in the end to degrade pollutants, has been widely reported for
wastewater treatment [3], which has been widely reported for wastewater treatment [4, 5]. However,
the disadvantages of no response in darkness and the high requirements on the light’s transmission
condition limit the practical application of photocatalysis in the dye decomposition [6]. Temperature
fluctuation, as a great source of the thermal energy, can change the internal polarization intensity of
the pyroelectric materials so that a charge imbalance forms between the internal polarization charges
and the external compensation charges, leading to the separation and migration of these
pyroelectrically-induced positive and negative charges to the surface of catalyst. Then, the
pyroelectrically-induced charges react with hydroxyl ions and the dissolved oxygens to form the
active free radicals with the strong oxidizing properties to decompose dye molecules [7, 8].

Recently, pyrocatalysis becomes increasingly popular in the dye decomposition [8-10]. Wu et al.
have reported that the BiFeO3 nanoparticles can decompose ~ 99 % Rhodamine B (RhB) dye after 85
cold-hot cycles [8]. Xu et al. have realized the decomposition ratio of ~ 99 % for RhB dye after 50 cold-hot cycles with Ba_{0.7}Sr_{0.3}TiO_3@1.5%Ag nanoparticles [9]. You et al. have reported a decomposition ratio of RhB dye up to ~ 86.5 % after 80 min with NaNbO_3 nanofibers in response to vibration together with cold-hot cycles [10]. How to further enhance the pyrocatalytic performance of the pyroelectric materials is crucial to their practical application in dye decomposition.

The method of fabricating heterostructure with the narrow-gap semiconductors to enhance catalytic performance has been widely applied in photocatalysis [11-13]. Benefitting from the generation of internal electric field on the interface, the heterostructure can strengthen the separation of the positive and negative carriers and further accelerate their migrations [14-16]. Therefore, this method may be available to enhance the pyrocatalytic performance of the pyroelectric materials in theory, which is rarely reported.

Graphitic carbon nitride (g-C_3N_4), as an organic semiconductor material, can be regarded as an ideal narrow-gap semiconductor option in the heterostructure due to its narrow band gap (E_g = 2.7 eV), metal-free property, great thermal and chemical stability [17-20]. Fabricating heterostructure with g-C_3N_4 has been widely used for improving the catalytic performance in the photocatalytic technology while its reports in pyrocatalysis field are rare up to now [21-23].

In our previous works, it has been reported that the pyroelectric materials of BaTiO_3 nanofibers [24], Pb(Zr_{0.52}Ti_{0.48})O_3 ceramics [7], ZnO nanorods [25] and NaNbO_3 nanorods [26] can respectively decompose ~ 99%, ~ 98%, ~ 98% and ~ 96% of RhB dye under the cold-hot cycles. Besides dye decomposition, other application of pyrocatalysis such as H_2 evolution [27, 28] has been realized. Some methods to enhance the pyrocatalytic performance have been developed such as the noble metal loading [29], fabricating heterostructures [30] and the optimizing poling field treatment [31].
In this work, a significantly-enhanced pyrocatalytic performance is found in the pyroelectric BiFeO$_3$/g-C$_3$N$_4$ heterostructure catalysts, which are fabricated via a simple mixing-calcining method. With the growth of g-C$_3$N$_4$ content in the heterostructure pyrocatalysts from 0 to 25 %, the decomposition ratio of Rhodamine B (RhB) dye after 18 cold-hot 25-65 ºC temperature fluctuation cycles increases at first and then decreases, reaching a maximum value of ~ 94.2 % at 10 % while that of the pure BiFeO$_3$ is ~ 67.7 %.

2 Materials and method

2.1 Synthesis of BiFeO$_3$

All the raw materials were analytical reagents in this experiment. BiFeO$_3$ was synthesized through a hydrothermal method [32, 33]. 2.425 g of Bi(NO$_3$)$_3$·5H$_2$O was dissolved in 50 mL of ethylene glycol. After the continuous magnetic stirring for 0.5 h, 1.352 g of FeCl$_3$·6H$_2$O and 200 mL of deionized water were added into the mixed solution. Then, NH$_3$·H$_2$O was added dropwise until the pH value of the solution up to ~ 11. The product in the solution was centrifugalized out and then washed with the deionized water until its pH value fell to ~ 7. Thereafter, the washed product was put into 40 mL of 5 M NaOH with the continuous magnetic stirring for 0.5 h. Finally, the mixture solution was put into a teflon-lined stainless steel autoclave and heated at 140 ºC for 72 h to obtain BiFeO$_3$.

2.2 Fabrication of BiFeO$_3$/g-C$_3$N$_4$ heterostructure

To obtain g-C$_3$N$_4$, 10 g of melamine was calcined in a muffle at 550 ºC for 4 h with a heating rate of 5 ºC/min [17]. To fabricate the BiFeO$_3$/g-C$_3$N$_4$ heterostructure, a certain amount of the prepared g-C$_3$N$_4$ and BiFeO$_3$ were dispersed in the absolute ethanol with the magnetic stirring for 0.5 h. Then, the mixture product was gained via centrifuge and dried at 70 ºC for 12 h. Finally, it was placed into
a muffle and calcining at 400 °C for 4 h. Based on this method, BiFeO$_3$/g-C$_3$N$_4$ heterostructures with different g-C$_3$N$_4$ weight fractions of 0 %, 5 %, 10 %, 15 %, 20 %, 25 % were obtained.

2.3 Characterization

An X-ray diffractometer (XRD, Rigaku MiniFlex/600 powder, Japan) was employed to characterize the crystal structures of samples. The infrared spectra of samples were recorded on a fourier transform infrared spectrometer (FTIR, Nicolet iS5, USA). The microstructure characterizations of samples were conducted through a scanning electron microscopy (SEM, Phenom ProX, the Netherlands) and a transmission electron microscope (TEM, Tecnai G2 F20 S-Twin, USA) with a high resolution transmission electron microscope (HRTEM). The pyrocatalytic decomposition performances of BiFeO$_3$/g-C$_3$N$_4$ heterostructure catalysts for RhB dye were measured via a UV-vis spectrophotometer (Ocean Optics QE65Pro, USA).

2.4 Pyrocatalytic dye decomposition

In this experiment, all the pyrocatalytic reactions were carried out in darkness to avoid the influence of photocatalysis on the RhB dye decomposition. 50 mg of BiFeO$_3$/g-C$_3$N$_4$ heterostructure catalyst and 50 mL of RhB aqueous solution (5 mg/L) were added into a brown bottle with the magnetic stirring for 1 h to achieve an absorption equilibrium. A single cold-hot temperature fluctuation cycle was carried out between 25 °C and 65 °C with a 10 min heating and 10 min cooling. The brown bottle with the RhB dye solution and the BiFeO$_3$/g-C$_3$N$_4$ heterostructure catalyst was placed in the middle of a water bath container (RCT-B-S25, IKA, Germany) to realize the cold-hot temperature fluctuation between 25 °C and 65 °C [6, 34]. The temperature was monitored via a thermometer placed in the middle of the mechanically-stirred dye solution [9]. After every 3 cycles, 3 mL of the mixture solution was taken out and centrifugalized for the UV-vis spectra measurements.
3 Results and discussion

Fig. 1 (a) shows the XRD patterns of BiFeO$_3$/g-C$_3$N$_4$ heterostructures as well as the pure BiFeO$_3$. The diffraction peaks of the pure BiFeO$_3$ accord well with the rhombohedral phase based on the JCPDS Card No. 86-1518 [32]. Because of the low g-C$_3$N$_4$ content, there is no obvious difference of the XRD patterns between BiFeO$_3$/g-C$_3$N$_4$ heterostructures and the pure BiFeO$_3$ can be seen in Fig. 1 (a) [21, 33, 35].

The FTIR spectra of the pure BiFeO$_3$, BiFeO$_3$/10%g-C$_3$N$_4$ heterostructure and g-C$_3$N$_4$ are employed to confirm the existence of g-C$_3$N$_4$ in BiFeO$_3$/g-C$_3$N$_4$ heterostructure, as shown in Fig. 1 (b). The pure BiFeO$_3$ displays two obvious infrared signal peaks at ~ 484 and ~ 592 cm$^{-1}$, attributing to the O-Fe-O bending vibrations and the Fe-O stretching of FeO$_6$ groups in BiFeO$_3$ [35, 36]. With regard to g-C$_3$N$_4$, the peak at ~ 802 cm$^{-1}$ is ascribed to the out-of-plane bending modes of C-N heterocycles [37, 38]. In the range of 1200 - 1600 cm$^{-1}$, several strong infrared signal peaks are seen clearly from the curve of g-C$_3$N$_4$, corresponding to the C=N and the aromatic C-N stretching vibration modes [39, 40]. The characteristic infrared signal peaks of g-C$_3$N$_4$ and the pure BiFeO$_3$ also exhibit in the infrared spectrum of BiFeO$_3$/10%g-C$_3$N$_4$ heterostructure, revealing the great combination between g-C$_3$N$_4$ and the pure BiFeO$_3$.

The pyrocatalytic mechanism with BiFeO$_3$/g-C$_3$N$_4$ heterostructure catalyst is proposed in Fig. 2. BiFeO$_3$ is a kind of crystal that possesses a spontaneous polarization property. While it keeps a thermal equilibrium with the external medium, its internal polarization charges are shielded by the external compensation charges so that BiFeO$_3$ shows the electroneutrality. Once the thermal equilibrium is broken, temperature fluctuation changes the electric dipole moment of BiFeO$_3$, 
which leads to the variation of the intensity of internal polarization. Therefore, a charge imbalance forms between the internal polarization charges and the external compensation charges [8]. It has been reported that the BiFeO$_3$ is a kind of $n$-type semiconductor ($E_g = \sim 2.2$ eV) while g-C$_3$N$_4$ behaves as an $p$-type semiconductor ($E_g = \sim 2.7$ eV) [41-43]. On the interface of the heterostructure, both the conduction band (CB) potential difference and the valence band (VB) potential difference between BiFeO$_3$ and g-C$_3$N$_4$ drive the electrons to diffuse from the CB of $n$-type BiFeO$_3$ to that of $p$-type g-C$_3$N$_4$, while on the contrary, holes diffuse from the VB of $p$-type g-C$_3$N$_4$ to that of $n$-type BiFeO$_3$ [44-46]. The diffusion of these carriers generates the negative charge center on the interface of g-C$_3$N$_4$ and the positive charge center on the interface of BiFeO$_3$, leading to the formation of the internal electric field, which further accelerates the separation of pyroelectrically-induced positive and negative charges, and the migration of pyroelectrically-induced positive charges from BiFeO$_3$ to g-C$_3$N$_4$.

Then, these pyroelectrically-induced charges react with hydroxyl ions and the dissolved oxygens on the surface of catalyst. The specific chemical equations in the pyrocatalytic reaction for dye decomposition with BiFeO$_3$/g-C$_3$N$_4$ heterostructure catalysts can be expressed as Eqs. (1) - (4) [47]:

\[
\text{BiFeO}_3 / g\cdot C_3N_4 \xrightarrow{\Delta T} \text{BiFeO}_3 / g\cdot C_3N_4 + q^+ + q^-
\]  
(1)

The dissolved oxygens ($O_2$) react with the pyroelectrically-induced negative charges ($q^-$) on the surface of BiFeO$_3$ to generate the superoxide radicals ($O_2^{-\cdot}$) according to the Eq. (2):

\[
O_2 + q^- \rightarrow O_2^{-\cdot}
\]  
(2)

Similarly, the pyroelectrically-induced positive charges ($q^+$) react with the hydroxyl ions (OH$^-$) on the surface of g-C$_3$N$_4$ to form the hydroxyl radicals (·OH) based on Eq. (3):

\[
\text{BiFeO}_3 / g\cdot C_3N_4 \xrightarrow{\Delta T} \text{BiFeO}_3 / g\cdot C_3N_4 + q^+ + q^-
\]
\[ \text{OH}^- + q^- \rightarrow \cdot \text{OH} \]  \hspace{1cm} (3)

Both the \( \cdot \text{OH} \) and \( \text{O}_2 \cdot^- \) have the strong oxidizing properties to decompose dye molecules on the basis of Eq. (4):

\[ \text{O}_2 \cdot^- (\text{or} \cdot \text{OH}) + \text{Dye Molecules} \rightarrow \text{Decomposition} \]  \hspace{1cm} (4)

The pure BiFeO\(_3\) of a square nanosheet structure with an average width of \( \sim 600 \text{ nm} \) and the g-C\(_3\)N\(_4\) of a layer structure are clearly seen in the SEM images of Fig. 3(a) and Fig. 3(b). The small size of BiFeO\(_3\) is beneficial for enlarging the surface area for reaction and shortening the migration distance for the pyroelectrically-induced charges to reach the surface of catalyst [7, 48]. BiFeO\(_3\) presents the similar morphology in Fig. 3(a) and Fig. 3(b), indicating that the formation of heterostructure do not significantly affect the square nanosheet structure of BiFeO\(_3\) [49]. Fig. 3(c) exhibits the TEM image of the BiFeO\(_3\)/g-C\(_3\)N\(_4\) heterostructure. The square nanosheet structure of BiFeO\(_3\) shown in Fig. 3(c) is in keeping with the observed morphology in the SEM images in Fig. 3(a) and Fig. 3(b). As displayed in Fig. 3(d), the HRTEM is employed to further confirm the microstructure of BiFeO\(_3\) and the combination between g-C\(_3\)N\(_4\) and BiFeO\(_3\). The lattice fringe in BiFeO\(_3\) is \( \sim 0.433 \text{ nm} \), which is in line with the (0 1 2) crystal plane of BiFeO\(_3\). The interface between g-C\(_3\)N\(_4\) and BiFeO\(_3\) is presented clearly in the HRTEM image while its enlarged image inset shows the extremely close attachment of two materials as well.

The pyrocatalytic performances of BiFeO\(_3\)/g-C\(_3\)N\(_4\) heterostructure catalysts are evaluated via the decomposition of RhB dye under cold-hot temperature fluctuation cycles. Fig. 4 shows the UV-vis absorption spectra of RhB dye solution with BiFeO\(_3\)/g-C\(_3\)N\(_4\) heterostructure catalysts at different temperature fluctuation (between 25 °C and 65 °C) cycles shown in the inset of Fig. 4 (a). The absorption peak locating at \( \sim 554 \text{ nm} \) decreases obviously with the increase of the cycle, indicating a
rapid decomposition of RhB dye. After undergoing 18 cycles, the BiFeO₃/10%g-C₃N₄ heterostructure catalyst displays an extremely weak signal of the absorption peak at ~ 554 nm, suggesting a nearly complete decomposition of RhB dye.

As the BiFeO₃/g-C₃N₄ heterostructure catalysts have demonstrated a obvious decomposition of RhB dye, it’s necessary to further estimate their pyrocatlytic decomposition performances. The corresponding degradation ratios \( D \) of RhB dye over BiFeO₃/g-C₃N₄ heterostructure catalysts are calculated via Eq. (5):

\[
D = (1 - C / C₀) \times 100 \%
\]  

Where the \( C₀ \) and \( C \) are the initial concentration and the current concentration of RhB dye solution, respectively [50]. Fig. 5 (a) exhibits the decomposition ratios of RhB dye at different cycles with BiFeO₃/g-C₃N₄ heterostructure catalysts. After 18 cycles, the BiFeO₃/g-C₃N₄ heterostructure catalysts with different g-C₃N₄ contents of 0 %, 5 %, 10 %, 15 %, 20 %, 25 % can respectively decompose ~ 67.7 %, ~ 76.7 %, ~ 94.2 %, ~ 91.7 %, ~ 87.4 % of RhB dye. The dependence of decomposition ratio on the g-C₃N₄ content of BiFeO₃/g-C₃N₄ heterostructure catalysts is shown in the inset of Fig.5 (a). The decomposition ratio of RhB dye increases significantly with the heterostructure and as high as ~ 94.2 %, which is the highest decomposition ratio of RhB dye among the BiFeO₃/g-C₃N₄ heterostructure catalysts, can be achieved via BiFeO₃/10%g-C₃N₄ heterostructure catalyst. As the g-C₃N₄ content of BiFeO₃/g-C₃N₄ heterostructure catalysts increases from 0 to 10 %, the increasing g-C₃N₄ content leads to a growing number of the BiFeO₃/g-C₃N₄ heterostructure unit so that the decomposition ratio of RhB dye increases at the beginning. When the content of g-C₃N₄ exceeds 10 %, the g-C₃N₄ of a layer structure stacks with itself, which becomes a new recombination center on the one hand and reduces the number of the BiFeO₃/g-C₃N₄ heterostructure unit on the
other hand [51, 52]. Both the increasing recombination ratio and the decreasing heterostructure unit number eventually result in the decrease of the RhB dye decomposition ratio.

A kinetic analysis of the pyrocatalytic reaction for RhB dye decomposition with BiFeO$_3$/$g$-C$_3$N$_4$ heterostructure catalysts is exhibited in Fig. 5 (b). The results accord well with the pseudo first order kinetic function based on the Eq. (6) [53-55]:

$$
\ln \left( \frac{C}{C_0} \right) = -K \cdot t
$$

Where $t$ and $K$ are the cycle and the kinetic rate constant in the pyrocatalytic reaction, respectively. The dependence of $K$ on the $g$-C$_3$N$_4$ content of BiFeO$_3$/$g$-C$_3$N$_4$ heterostructure catalysts can be found in the inset of Fig. 5 (b). As the $g$-C$_3$N$_4$ content of BiFeO$_3$/$g$-C$_3$N$_4$ heterostructure catalysts grows from 0 to 25 %, the value of $K$ increases at first and then decreases, giving a maximum value of ~0.1513 cycle$^{-1}$ at 10 %, which is about 3 times as high as the $K$ value of the pure BiFeO$_3$ (~0.0686 cycle$^{-1}$). The larger $K$ value means the better pyrocatalytic performance of the BiFeO$_3$/$g$-C$_3$N$_4$ heterostructure catalyst. All BiFeO$_3$/$g$-C$_3$N$_4$ heterostructure catalysts behave the better pyrocatalytic performance than the pure BiFeO$_3$, while the optimal performance appears at the $g$-C$_3$N$_4$ content of 10 % in heterostructure catalyst.

The decomposition ratios of RhB dye with different catalysts and under various experimental conditions are shown in Fig.6. In the absence of BiFeO$_3$/10%$g$-C$_3$N$_4$ heterostructure catalyst, RhB dye solution shows almost no decomposition, which presents the excellent stability of RhB dye and excludes the influence of temperature fluctuation on RhB dye decomposition. Without temperature fluctuation, no obvious decomposition of RhB dye can be observed with BiFeO$_3$/10%$g$-C$_3$N$_4$ heterostructure catalyst, revealing the essential role of the temperature fluctuation in pyrocatalytic reaction. When BiFeO$_3$/10%$g$-C$_3$N$_4$ heterostructure catalyst is replaced with the corresponding
masses of BiFeO₃ and g-C₃N₄, the decomposition ratio of RhB dye becomes almost the same as that of using the pure BiFeO₃, which further proves the formation of the heterostructure and its indispensable role played in the significantly-enhanced pyrocatalytic performance.

In order to detect the intermediate products that play an important role in the pyrocatalytic decomposition of RhB dye, the pyrocatalytic experiments are carried out through adding different kinds of scavengers respectively. As shown in Fig. 7 (a), the decomposition ratios of RhB using BiFeO₃/10%g-C₃N₄ heterostructure catalyst with different kinds of scavengers decrease in different degrees. The lower decomposition ratio of RhB dye means the stronger inhibition effect of scavenger to the catalyst’s pyrocatalytic performance. Ethylene diamine tetraacetic acid (EDTA), benzoquinone (BQ) and tert-butyl alcohol (TBA) are the scavenger of hole, O₂⁻ and ·OH, respectively [56]. Therefore, holes, ·OH and O₂⁻ are the main intermediate products in the pyrocatalytic reaction, while the lowest decomposition ratio of RhB dye using BiFeO₃/10%g-C₃N₄ heterostructure catalyst with BQ suggests that the O₂⁻ is the most crucial active substance among them.

The recycling utilization results of the BiFeO₃/g-C₃N₄ heterostructure catalyst for RhB dye decomposition can be seen from Fig. 7 (b). After 18 cold-hot cycles, the BiFeO₃/10%g-C₃N₄ heterostructure catalyst was centrifugalized out from the dye solution and washed with the deionized water. Then, it was dried at 70 °C for 12 h in an air oven and added into 50 mL of 5 mg/L RhB dye solution for the next 18 cycles. There is a slight decrease of the decomposition ratio after recycling the catalyst for 3 times, indicating the remarkable stability of its pyrocatalytic decomposition performance for RhB dye [57]. Furthermore, as a magnetic material, BiFeO₃ also has been reported with the excellent recyclable ability [58], which makes the recycling process of the catalyst convenient. Both the remarkable stability and the excellent recyclability of BiFeO₃/g-C₃N₄...
heterostructure catalyst are helpful to its practical application in dye decomposition.

4 Conclusions

The significantly-enhanced pyrocatalytic performance is realized via the BiFeO\textsubscript{3}/g-C\textsubscript{3}N\textsubscript{4} heterostructure, which is fabricated through a simple mixing-calcining method. The decomposition ratio of RhB dye using the BiFeO\textsubscript{3}/10\%g-C\textsubscript{3}N\textsubscript{4} heterostructure catalyst is about 30 \% higher than that using the pure BiFeO\textsubscript{3}. The main intermediate products in the pyrocatalytic reaction for RhB dye decomposition are detected and confirmed, among which the O$_2^-$ shows the most crucial influence. No obvious loss of the pyrocatalytic performance can be observed after recycling the catalyst for 3 times. The significantly-enhanced pyrocatalytic performance makes BiFeO\textsubscript{3}/g-C\textsubscript{3}N\textsubscript{4} heterostructure catalysts to have the potential in dealing with wastewater through utilizing the thermal energy of temperature fluctuation.

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**Figure Captions:**

Fig. 1 (a) The XRD patterns of the pure BiFeO3 and BiFeO3/g-C3N4 heterostructures. (b) The FTIR spectra of the pure BiFeO3, BiFeO3/10%g-C3N4 heterostructure and g-C3N4.

Fig. 2 The schematic diagram of the pyrocatalytic reaction with BiFeO3/g-C3N4 heterostructure catalyst.

Fig. 3 The SEM images of (a) the pure BiFeO3 and (b) BiFeO3/g-C3N4 heterostructure. (c) The TEM and (d) HRTEM images of BiFeO3/g-C3N4 heterostructure.

Fig. 4 The UV-vis spectra of RhB dye solution after different numbers of cycles using BiFeO3/g-C3N4 heterostructure catalysts. (a) The pure BiFeO3. The inset is the ideal temperature fluctuation curve in the pyrocatalytic experiment. (b) BiFeO3/5%g-C3N4. (c) BiFeO3/10%g-C3N4. (d) BiFeO3/15%g-C3N4. (e) BiFeO3/20%g-C3N4. (f) BiFeO3/25% g-C3N4.

Fig. 5 (a) The decomposition ratios of RhB dye after different numbers of cycles using BiFeO3/g-C3N4 heterostructure catalysts. The inset shows the dependence of decomposition ratio on
the g-C₃N₄ content after 18 cycles. (b) The plot of the negative logarithm of $C/C_0$ versus cycles. The inset shows the dependence of the kinetic rate constant on the g-C₃N₄ content.

Fig. 6 The comparison of the decomposition ratios of RhB dye with different catalysts and under different reaction conditions.

Fig. 7 (a) The detection of intermediate products in the pyro catalytic reaction using BiFeO₃/10%g-C₃N₄ heterostructure catalyst with different scavengers. (b) The recycling utilization of BiFeO₃/10%g-C₃N₄ heterostructure catalyst for RhB dye decomposition.