EVALUATION OF DIRECT RED 80 DYE ADSORPTION BY CHITOSAN MICROSPHERES

AVALIAÇÃO DA ADSORÇÃO DO VERMELHO DIRETO 80 POR MICROESFERAS DE QUITOSANA

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ABSTRACT
The damage caused to the environment by the textile industry creates a demand for simple and inexpensive methods to remove dyes from wastewaters. In this sense, the objective of this work was to evaluate and optimize the adsorption of the Direct Red 80 azo dye by chitosan microspheres. The SEM and FTIR techniques were used to characterize the materials. The results confirmed the occurrence of the adsorption phenomenon by the detection of characteristic bands and changes on the surface of the adsorbent, caused by the fixing of the dye. The response surface methodology in association with a Doehlert matrix was applied to optimize the adsorption process. The obtained response surface presented a saddle point, indicating that the optimal condition is outside of the experimental domain. Isotherms were constructed to describe the adsorption phenomenon. The experimental data presented a better regression adjustment (R^2 > 0.98) to the Freundlich nonlinear model. The results demonstrate that the chitosan microspheres presented high color removal efficiency (97% in 24h) and operational ease in its usage.

PALAVRAS-CHAVE
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RESUMO/RESUMEN
Os danos causados ao meio ambiente pela indústria têxtil criam uma demanda por métodos simples e baratos para remover corantes de águas residuárias. Nesse sentido, o objetivo deste trabalho foi avaliar e otimizar a adsorção do corante azo Vermelho Direto 80 por microesferas de quitosana. As técnicas de Microscopia Eletrônica de Varredura e Espectroscopia Vibracional no Infravermelho foram utilizadas para caracterizar os materiais. Os resultados confirmaram a ocorrência do fenômeno de adsorção pela detecção de bandas características e mudanças na superfície do adsorvente, causadas pela fixação do corante. A metodologia de superfície de resposta em associação a uma matriz Doehlert foi utilizada para otimização do processo de adsorção. A superfície de resposta obtida apresentou um ponto de sela, indicando que a condição ótima para os parâmetros se encontra fora do domínio experimental. Isotermas foram construídas para descrever o fenômeno de adsorção. Os dados experimentais apresentaram um melhor ajuste de regressão (R^2 > 0.98) ao modelo não lineal de Freundlich. Os resultados demonstram que as microesferas de quitosana apresentaram elevada remoção de cor (97% em 24h) e facilidade operacional na sua utilização.
1. INTRODUCTION

The textile sector is essential for the economy of a country. However, it is one of the industries that most generate wastewater during its production stages (Holkar et al., 2016; Volmajer et al., 2011). According to Neta et al. (2011), its wastewaters contain dyes applied in the manufacture, which were leached in the process.

The textile wastewaters present low biodegradability and intense color, which are characteristics related to the dyes carried to the affluent of the treatment plants (Kaur et al., 2017; Rodrigues et al., 2010). These dyes cause harmful effects on the environment and human health, such as alteration of the water bodies coloration, which inhibits the photosynthesis, and the generation of carcinogenic and mutagenic by-products (Paz et al., 2017).

The Azo class is the largest group of synthetic industrial dyes present on the market, consequently, it is the most discharged into water bodies (Kallel et al., 2016; Neta et al., 2011). Azo dyes are anionic compounds soluble in aqueous solutions, which exhibit coloration due to presence of certain functional groups in its molecular structure, such as chromophores (–N=N–) and the auxochromes (SO3–; =O) (Verma et al., 2012).

According to the literature, several studies have been focused on the treatment of effluents containing dyes due to their high potential of causing environmental impacts. Physical, chemical and biological processes currently used to treat these effluents exhibit certain inefficiency, as they usually present high cost and/or produce effluents with variable characteristics, that might contain secondary pollutants and toxic products (Ajmal et al., 2014; Natarajan et al., 2017). According to Kallel et al. (2016), among these processes, adsorption is the simplest and more economical for this purpose.

In this context, there is a demand for low-cost adsorbents generated from plants and animals to be applied on wastewater treatment (Verma et al., 2012). Chitosan (QTS), for example, is a low-cost biopolymer that has shown to be an adsorbent with great potential to remove dyes (Cao et al., 2014).

Chitosan is a product derived from the deacetylation of chitin, the largest component of crustacean exoskeletons (Cao et al., 2014; Rosa et al., 2010). It has been widely applied due to its properties, such as non-toxicity, structural flexibility, adsorptive capacity and the presence of functional groups (-NH2 and –OH), among others (Cao et al., 2014; Rosa et al., 2010; VAKILI et al., 2015).

In this paper, chitosan microspheres (mQTS) were prepared, characterized and applied on the removal of an azo dye. The Direct Red 80 (DR 80) textile dye was selected for the study because it is commonly used in this industrial sector. Therefore, the objective of this work was to evaluate the sorption capacity of DR 80 by mQTS and to optimize the process using the response surface methodology (RSM) in association with a Doehlert matrix.

2. MATERIALS AND METHODS

2.1 Reagents

All reagents used in the experiments were obtained from commercial sources, which were: glacial acetic acid (P.A; Manufacturer: ALPHATEC), sodium hydroxide micropearls (P.A; Manufacturer: Impex), ferrous sulphate (P.A; Manufacturer: Dinâmica), nickel nitrate (P.A; Manufacturer: Vetec), ethanol (P.A; Percentage: 99.7%; Manufacturer: ALPHATEC), sodium borohydride (P.A; Manufacturer: NEON), citric acid (P.A; Percentage: 99.8%; Manufacturer: NEON), anhydrous dibasic sodium phosphate ACS (P.A; Percentage: 99%; Manufacturer: VETEC), boric acid (P.A; Percentage: 99.5%; Manufacturer: VETEC), hydrochloric acid (P.A; Percentage: 37%; Density: 1.19 kg / L; Manufacturer: ALPHATEC), sodium nitrate ACS (P.A; Percentage: 99%; Manufacturer: VETEC). The Direct Red 80 (DR 80) dye and powdered chitosan (QTS) were supplied by the Itabira do Campo Industrial Company and the Environmental Chemistry Laboratory of the Federal University of Viçosa (UFV), respectively.

2.2 Production of chitosan microspheres

The chitosan microspheres (mQTS) were obtained by applying the methodology described by Cruz et al. (2015) with some adaptations. For the present study, a single batch of material was produced to be used in all the experiments.

QTS was added in a 5% (v/v) acetic acid solution to give a final 4% (m/v) QTS solution. Then, the solution was agitated with a vertical stirrer until its homogenization.

Finally, to obtain the mQTS, the produced QTS solution was dripped into an 8% (w v) sodium hydroxide solution using a syringe (v = 5 ml), keeping the distance (≈7 cm) between them constant during the procedure. The obtained material was kept at rest for 24 hours. Subsequently, the spheres were washed with distilled water until pH neutralization.

2.3 Characterization of materials

2.3.1 Diameter of the mQTS

The diameter of the mQTS was determined using a metal caliper (WESTERN). For this, 50 mQTS were aleatory selected and had its diameter measured. Then, the mean and standard deviation values of the samples were calculated.

2.3.2 Moisture content of the mQTS

Fifty mQTS were separated, identified, weighed using an analytical balance (ATX224, Manufacturer: SHIMADZU) and then left to dry under room temperature for 24 hours. After the drying process, the material was reweighed and had its moisture content quantified. Finally, the mean and standard deviation values were calculated.

2.3.3 Density of the mQTS

The density of the mQTS was determined by the pycnometry technique using an analytical balance (ATX224, Manufacturer: SHIMADZU). First, the mass of the picnometer was determined. Then, the mass of the picnometer filled with
distilled water was measured. Subsequently, the mass of a QTS sample (m₀) was measured and then the material was inserted into the picnometer, which had its volume completed with distilled water again. Finally, the mass of this set (picnometer + mQTS sample + water) was measured (mₙ). From this, the density of mQTS could be determined.

2.3.4 Degree of deacetylation (G₀)

The degree of deacetylation (G₀) of the QTS was determined by the Potentiometric Titration method, applying an adaptation of the methodology described by dos Santos et al. (2009). A QTS sample was dissolved in a 0.1 mol L⁻¹ HCl solution in the ratio 1:100 (g QTS / mL HCl). Then, the resultant solution was titrated with a standard 0.1 mol/L NaOH solution under continuous stirring. From the obtained data, the G₀ was determined using the Equation (1).

\[ G₀ = 100xMₐX \frac{ΔVxNaOH}{ΔVxNaOHxMₐ+MₐQTS}, \text{onde } ΔM = Mₐ - MₐO \]  

Where: Mₐ is the deacetylated unit (C₅H₉O₃N) molar mass (161.1558 g mol⁻¹), MₐO is the acetylated unit (C₅H₉O₃N) molar mass (203.1925 g mol⁻¹) and CₐNaOH is the sodium hydroxide concentration (0.1 mol L⁻¹).

2.3.5 Infrared vibrational spectroscopy (FTIR)

The materials, mQTS and DR 80, were analysed by Infrared Vibrational Spectroscopy. The infrared spectrum was obtained in the region of 400 – 4000 cm⁻¹ using an Infrared Spectrophotometer Varian 660-IR with a PikeGladiATR accessory.

2.3.6 Scanning electron microscopy (SEM)

The materials, mQTSs before (wet) and after being utilized in the DR 80 dye adsorption process, were characterized by Scanning Electron Microscopy.

2.3.7 Evaluation of the behavior of DR80 as a function of pH

The behavior of the DR 80 dye in solution was evaluated at different pH values (2, 4, 6, 8 e 10). For this, solutions containing: 15 mL of dye solution (15 mg L⁻¹), 5 mL of universal buffer (0.05 mol L⁻¹ C₄H₆O₇; 0.05 mol L⁻¹ NaH₂PO₄ and 0.1 mol L⁻¹ H₃BO₃) with the pH adjusted to the desired value and 5 mL of NaN₂O₃ (0.5 mol L⁻¹) were prepared. The spectra were obtained in the range of 200-600 nm.

2.4 Adsorption tests

2.4.1 Adsorption kinetics

The experiment executed to describe the adsorption kinetics were conducted in a cylindrical reactor containing 250 mL of a DR 80 solution (15 mg L⁻¹). These experiments were performed without pH adjustment (natural pH of the dye solution ~ 6.10), using an mQTS dose of 10 g L⁻¹, under orbital agitation (agitator table SL ~ 180/A, intensity 3) and at room temperature (25 ± 1°C). In order to keep track of the adsorption process, aliquots were collected at different time intervals in a 24 h period, and analysed by UV-Vis Molecular Absorption Spectrophotometry (quartz cuvette, optical path 1 cm) monitoring the absorbance at λ = 527 nm. The experiments were performed in duplicate.

The remaining concentrations of DR80 in solution were estimated based on an analytical curve in the concentration range of 0-20 mg L⁻¹. The experimental data were adjusted to a linear model according to the Lambert-Beer Law and the quality of fit was evaluated by the coefficient of determination.

2.4.2 Optimization of the adsorption process

The response surface methodology (RSM) in association with a Doehlert matrix was used to evaluate the effects of two variables, the DR 80 initial concentration and the initial pH of the system, on the color removal. The values adopted in the experiments for these parameters are shown in Table 1. The color removal was determined by UV-Vis Molecular Absorption Spectrophotometry. For this, analytical curves were constructed for each pH value adopted in the experiments (the absorbance was monitored at the wavelength of maximum absorption – peak of the spectrum) by varying the dye concentration from 0 to 20 mg L⁻¹. The aliquots were withdrawn after the same time interval taken for the system to reach equilibrium in the adsorption kinetic experiment performed previously (item 2.4.1).

All the experiments were carried out in a 125 mL cylindrical reactor, containing 5 mL of universal buffer (0.05 mol L⁻¹ C₄H₆O₇; 0.05 mol L⁻¹ NaH₂PO₄ and 0.1 mol L⁻¹ H₃BO₃) with the pH adjusted to the desired value, 5 mL of NaN₂O₃ (0.5 mol L⁻¹), 15 mL of DR 80 solution and 0.25 g of mQTS.

The obtained spectra were analyzed using the Origin 8.5.9 SR1 software in order to verify the need for baseline correction.

Table 1. The Doehlert matrix design performed to determine the optimal condition for the adsorption of DR 80 by mQTS. The first number is the experimental value and the one inside the parenthesis is the coded factor.

| Experiment | Initial pH | Concentration / mg L⁻¹ |
|------------|------------|------------------------|
| 1          | 2.00 (-1)  | 12.5 (0)               |
| 2          | 4.00 (-0.5)| 20 (-0.866)            |
| 3          | 4.00 (-0.5)| 5 (0.866)              |
| 4          | 6.00 (0)   | 12.5 (0)               |
| 5          | 8.00 (1)   | 20 (-0.866)            |
| 6          | 8.00 (1)   | 5 (0.866)              |
| 7          | 10.00 (0.5)| 12.5 (0)              |
| 8          | 6.00 (0)   | 12.5 (0)               |
| 9          | 6.00 (0)   | 12.5 (0)               |
| 10         | 6.00 (0)   | 12.5 (0)               |

2.4.3 Adsorption isotherms

The equilibrium experiments were performed in a batch cylindrical reactor containing 50 mL of DR 80 solution, 0.5 g of mQTS, at T = 25.2°C, at pH = 6.0 and under constant orbital agitation. The adopted concentrations were 15, 20, 30, 50, 90, 170 and 330 g L⁻¹. As described by CHENG et al. (2015), the amount of material adsorbed at equilibrium (Qₑ) is obtained by the Equation (2):

\[ Qₑ = \frac{(C₀ - Cₑ)V}{m} \]  

Where C₀ e Cₑ are the initial and equilibrium concentrations of the dye in solution respectively; V is the reaction volume and
m is the mass of the adsorbent. The Freundlich’s (Equation 3) and the Langmuir’s (Equation 4) theoretical models were used to describe the adsorption of DR80 by mQTS.

Freundlich’s model: \[ q = k_F C_e^{1/n} \] (3)

Langmuir’s model: \[ q = \frac{q_{\text{max}}k_L C_e}{1 + k_L C_e} \] (4)

3. RESULTS AND DISCUSSION

3.1 Characterization of Direct Red 80 dye

UV-Visible absorption spectra as a function of the DR 80 concentration (50 to 5 mg L\(^{-1}\)) are expressed in the complementary material (Figure 1S). All the solutions under study presented a characteristic absorption band in the visible region (\(\lambda_{\text{max}}=527\) nm) and another two in the UV region (\(\lambda=227\) nm and \(\lambda=285\) nm). According to Mahmoodi et al. (2005), the elevated absorption in the visible region corresponds to the chromophore group (-N=N-), whereas the ones in the UV refer to benzene and naphthalene rings. This property is also described by Li et al. (2015), which mention that the absorption in the UV region is a consequence of the presence of benzene-like structures and the one in the visible region is due to an azo bond between two aromatic rings.

The behavior of the DR 80 in solution as a function of the pH was also evaluated and expressed in the complementary material (Figure 2S). By analysing the curves, it is possible to observe that there was a significant displacement of the absorption peaks correspondent to 285 and 527 nm, whereas there was an increase of the absorbance intensity on the peak located at 227 nm, however, accompanied by a considerable background noise. Therefore, it can be concluded that the wavelength correspondent to the maximum absorbance value is pH dependent, which justifies the construction of an analytical curve (Figure 1) for each pH value adopted in the experiments.

In order to understand this phenomenon occurred in the spectrum, scans were performed in the same regions contemplated in the graphs presented in Figures 1S and 2S (supplementary material), with DR80 in the used pH values and the buffer (graphs not expressed in the present work). The results show that the buffer absorbs energy at \(\lambda = 300\) nm and the absence of other peaks. The dye, however, presents a displacement to the red region only for pH 2 and 4, not showing significant changes for the other pH values. It can be concluded that the addition of the buffer solution (0.05 mol L\(^{-1}\) \(\text{CH}_3\text{CO}_2\text{H}, 0.05\) mol L\(^{-1}\) \(\text{NaH}_2\text{PO}_4\) and 0.1 mol L\(^{-1}\) \(\text{H}_3\text{BO}_3\)) and the pH adjustment cause interactions with the chromophore groups and/or the constituents of the buffer. This results in a bathochromic shift (\(\lambda = 527\) to \(\lambda = 541 - 544\) nm) and a hyperchromic effect (\(\lambda = 212\) nm), moreover, the 300 nm band of the buffer overlaps the DR 80 band.

From these results, analytical curves for the DR 80 were constructed in the studied pH values, obtained at the maximum absorbance wavelengths (\(\lambda_{\text{max}}\)). It is possible to visualize that for each analytical curve, a linear relation between the variables is established in agreement with the Lambert-beer Law. The quality of the adjustments was evaluated by the determination and Pearson correlation coefficients, which indicated a positive and linear relationship. It is possible to discern that the linear model determined for pH 6 presents less sensitivity when compared to the others. Higher sensitivities are observed in more basic conditions. These changes in the sensitivity might be associated with substitutions in the chromogenic reactant molecule caused by its interaction with the pH and the buffer.

3.2 Characterization of Chitosan microspheres

The adsorbent used in the experiments was characterized in order to understand its chemical and physical structures and discuss the adsorptive processes involved. A pre-characterization of the mQTS properties is presented in Table 2.

Table 2. Properties of chitosan.

| Parameter                  | Value            |
|----------------------------|------------------|
| Moisture (%)               | 93.400 ± 0.971   |
| Mass (g)                   | 0.0196 ± 0.0013  |
| Diameter (cm)              | 0.285 ± 0.063    |
| Density                    | 0.971 ± 0.031    |
| Depolymerization degree (%)| 79.11 ± 1.44     |

The produced mQTS (Figure 4) presents a dispersion of diameter (Figure 2, a) inherent of its production process, since the QTS solution is dripped onto the coagulant solution.
This characteristic is affected by the amount of material dripped, density of the material and the properties of the solutions. Because of the non-uniformity of the mQTS, its mass values also present a significant dispersion (Figure 2, b). Despite the characteristics of these parameters, the experiments proved to be reproducible and easy to characterize.

The G_D was determined by Potentiometric Titration (Figure 3, a). It is possible to observe the presence of three distinct regions, in the first one, the elevation of pH is caused by the neutralization of free HCl in solution; the second one, which includes an inflection point, corresponds to the neutralization of the HCl and the protonated amino groups in the QTS; the third one, is characterized by an increased base excess (NaOH). Thus, it was possible to determine the equivalence point (Figure 3, b), that is, the volume of base needed to neutralize the acid group (NH_3) and to apply it in Equation 1 to determine the GD, which was equal to 79.11 ± 1.44%.

![Figure 3. Potentiometric titration: (a) curve of chitosan and (b) 1st derivative of pH.](image)

The morphological studies of the samples were performed by Scanning Electron Microscopy (SEM). The SEM images of mQTSs wet and after the adsorption of the studied dye are presented in Figure 4. The diameter of the mQTS, determined using the ImageJ software, was approximately 1.84 mm, which is inside the dispersion interval presented in Figure 2 (a).

It can be observed that the mQTS have a non-porous surface. An evidence of the adsorption of DR 80 on the surface of the adsorbent was given by SEM (Figure 4, b). This image shows a more regular and grooved surface, which indicates the binding of the dye throughout the entire surface of the mQTS, also shown by the photograph of Figure 3S (supplementary material).

Similar results were obtained by Vakili et al. (2015) and Perez et al. (2016). It can also be observed that the mQTS are not totally spherical, presenting a slight tail extension. In agreement with the experiments, this characteristic is directly related to the technique of dripping.

The FTIR technique was used to confirm the occurrence of the adsorption phenomenon, identify the compounds and emphasize the chemical structures before and after the process. In Figure 5 (a) the adsorption band near 3303 cm^{-1} refers to the vibrations of stretching the bounds of the –OH and –NH groups (Vakili et al., 2015). The low-intensity peak at 2885 cm^{-1} is attributed to the presence of –CH. Regarding the peak appearance at 1637 cm^{-1}, Cao et al. (2014) attributed it to the torsional vibration of the –NH_2 and its intensity and area may be consequences of the stretching vibrations of the C=O group, bound to the primary and secondary amides, in the region of 1580 cm^{-1}. The peaks of 1421, 1382 and 892 cm^{-1} are resulting from the flexing of the CH_2, CH_3 and C-H bonds, respectively. In addition, those of 1149 and 1031 cm^{-1} refer to the stretching vibrations of C-OH (Igberase et al., 2014).

![Figure 4. Images obtained by scanning electron microscopy (SEM) with increase of x100 (a) wet mQTS and (b) mQTS after the process of adsorption of DR 80.](image)
Figure 5. The FTIR spectra of (a) wet mQTS, (b) DR 80, (c) wet mQTS after the adsorption process of DR 80.

From the comparative analysis of Figure 5 (c) with (a) and (b), it is possible to understand the spectrum after the adsorptive process. It shows a spectrum modification at the junction of regions 1 and 2 of the spectrum (red circle). This prominent part refers to the functional groups present in both molecules (region 1) and the fingerprint (region 2). These modifications prove the occurrence of the adsorption mechanism of the system under study. Thus, this phenomenon causes changes in the stretches of the main bonds and/or it simply causes changes of position due to spatial and electronic factors. In addition, it confirms the identity of the new compound, since coupled vibrational bands and vibrations concerning the carbon skeleton of the molecules change (region 2, comparing Figure 5 (a) (b) with respect to (c)).

3.3 Adsorption kinetics

The mQTS have been widely applied in studies of color removal (Kimura et al., 1999; Patel et al., 2012; Zhu et al., 2009). This fact is associated to the characteristics of this compound, such as application flexibility (Shukla et al., 2013), ease of characterization and the adsorptive capacity of the OH and NH₂ groups (Igerase et al., 2015).

An approximately 97% color removal in 24 h was obtained on the kinetics assay (Figure 6). After reaching this removal value, the system goes into equilibrium.

The adsorption occurs in a casing mode, in other words, around the mQTS. It can be seen in Figures 4 (b) and 3S (complementary material), which present the material before and after the process. By analyzing Figure 4, it is clear that the dye adheres to the surface of the mQTS covering it to form a film, which is evidenced by the surface color change shown in Figure 3S (complementary material).

Figure 6. Adsorption kinetics of DR 80 by mQTS. Experimental conditions: [mQTS] = 10 g L⁻¹, [DR 80] = 15 ppm, pH without adjustment, T = 25°C.

The operational variables of the adsorption process were optimized based on the Doehlert matrix, reducing the number of experiments. The data were treated using the program STATSOFT STATISTICA 7.0.61.0. According to the Pareto chart (Figure 7), the initial pH and DR 80 concentration, its linear and quadratic relations, and its interactions are statistically significant considering a 95% confidence limit. The increase in the values of the variables (1) initial pH and (2) DR 80 initial concentration favors the color removal, as can be visualized in Figure 8.

Figure 7. Pareto chart of the pH and initial concentration variables in the DR 80 adsorption.

The results (Figure 8) show that, when working with these factors, the concentration at 3 levels and the pH at 5 levels, did not contribute to the obtention of an optimal point. However, the constructed experimental design estimated coefficients that presented good adjustments ($r^2 = 0.9761$) to the empirical mathematical model employed in the Doehlert matrix within the delimited experimental domain. This methodology uses a quadratic polynomial function (Equation 5) to explore the optimization (Ferreira, 2004).

Figure 8. Response surface obtained from the Doehlert Matrix to evaluate the effects of the pH and DR 80 concentration on the color removal.

From this surface, it was possible to obtain an equation that correlates the color removal with the variables that statistically influence the system. In order to explore information about the critical points, the Lagrange criterion was applied based on the value of the Hessian determinant, in Equation (5), reaching $	ext{det}[H] = -0.46$, characterizing a saddle point (Ferreira, 2004), that is, the meeting of the maximum
value of one variable with the minimum of the other. For the experimental conditions applied in this methodology, the response surface did not allow to predict data for the optimization of the adsorption of DR 80 by mQTS. However, values of pH > 6 provide removals between 80-100%, being excellent results.

\[ Z = 69.40 + 10.83X - 0.57X^2 - 6.05Y + 0.19Y^2 + 0.15XY \]  
(5)

Where, \( Z \) = color removal, \( X \) = initial pH e \( Y \) = DR 80 initial concentration.

Another important factor in obtaining the response surface was the baseline correction of the spectra, which presented a displacement towards the ordinate axis. Analyzing the color removal phenomenon, Verma et al. (2012) report that mQTS has a long and full chain of free sites for adsorption. According to Li et al. (2005), these alterations on the adsorption process are resultant of the acid-base properties of mQTS (Equations (9) and (10)).

\[ \text{NH}_2 + H^+ \rightarrow \text{NH}_3^+ \]  
(6)

\[ \text{NH}_2 + \text{OH}^- \rightarrow \text{NH}_2\text{OH}^- \]  
(7)

Through the equations and the knowledge of the DR 80 and mQTS chemical structures, it is possible to infer that the amino group of chitosan will interact by neutralization of charges with the sulphonic group at acidic pH and by intermolecular interactions at basic pH. Moreover, Verma et al. (2012) mention that the interparticle interaction occurs through \( \pi \) electrons of the dye molecule and -OH group of mQTS.

### 3.4 Isotherms

Adsorption isotherms are fundamental for the understanding of the adsorptive phenomenon between two phases, liquid and solid, in equilibrium. To determine a model that best described the system under study, the Langmuir and Freundlich models were tested. The results were compared using the coefficient of determination (R²). The results indicate that the mQTS adsorb DR 80 following a Freundlich’s model (Figure 9), since it presented R² > 0.98.

**Figure 9. Freundlich’s isotherm model adjustment to the experimental data of the DR 80 adsorption by mQTS**

**experiment, Stirring time=24 h. Experimental conditions:** 
[mQTS] = 10 g L\(^{-1}\), [DR 80] = 15 - 500 mg L\(^{-1}\), pH without adjustment, \( T = 25^\circ\text{C} \).

According to Cheng et al. (2015), this mechanism occurs by the adsorption of the studied dye at sites, with distinct energies, present on the heterogeneous surface of the adsorbent. In accordance to the results, the DR80 is retained only on the external specific area of the mQTS.

### 4. CONCLUSIONS

In the present work, chitosan microspheres were tested for the remediation of the Direct Red 80 textile dye. Excellent results were obtained, with a 97% removal in 24 h. FTIR and SEM analyses showed that the dye adsorbs on the surface of the chitosan microspheres. Assays employing a Resonse Surface Methodology, Doehlert matrix, demonstrated that the pH of the system strongly influences the adsorption process, altering the adsorption mechanism of the dye molecules by the mQTS (in acid pH - neutralization of charges, while in basic pH - intermolecular interaction). The experimental data fitted to the Freundlich nonlinear model \( (R^2 = 0.98444) \). The application of this material for remediation showed to be advantageous due to its high removal capacity, ease of handling, low cost and low environmental impact. Thus, the mQTS presented a potential to be applied in the future to remove color of effluents.

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