Improving dynamic response of PEMFC using SMES and bidirectional DC/DC converter

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ABSTRACT
Nowadays, the use of renewable energy systems, especially fuel cells, has become very widespread in various applications. Some of their most important applications include using electric vehicles and local off-grid power systems. One of the challenges with the fuel cells is the slow dynamic response to load power changes. In fact, when the load power changes suddenly, the fuel cell supplies it with a time delay, and this can cause disturbances in the performance of the loads. In this research, a new control method for a bidirectional DC/DC converter equipped with a superconducting magnetic energy storage system (SMES) is presented to exchange the stored energy with the proton-exchange membrane fuel cell (PEMFC) in a high response dynamic to overcome the slow dynamic of the fuel cell feeding load. The appropriate validation of the proposed system is verified by simulation in the MATLAB SIMULINK environment. The results illustrate that the slow-response of PEMFC is improved appropriately.

1. Introduction
Fuel cells (FC) as one of the renewable energies have recently been highly regarded by various researchers and investors. In particular, the companies producing electric vehicles and local distribution loads pay special attention to it as one of the methods of producing pollution-free electricity. Fuel cell systems can generate electrical power with high efficiency across a wide range of sizes and situations. As FCs can be implemented in small sizes, they can be located near the electrical loads, enabling the thermal energy provided as a result of the chemical reaction to be used for cogeneration applications, making the combined efficiency even more attractive. Moreover, the FC systems usually emit a low level of common air pollutants and reduce carbon dioxide emissions. These systems operate silently. In contrast to the wind and solar systems, they have a dispatchable and predictable distributed generating technology [1]. Research work has [2] discussed the optimal estimation of proton exchange membrane fuel cell (PEMFC) parameters based on coyote optimization algorithms. A novel control strategy for enhancing microgrid operations connected to photovoltaic generation and energy storage systems is being investigated [3]. Abubakr et al. [4] analysed a comprehensive review of renewable energy sources in Egypt’s current status, grid codes and future vision. Some of the most important challenges of the FCs are reviewed in the following.

One of the most common uses of the FCs is in electric vehicles. In any case, there is an unavoidable issue that the required power in electric vehicles varies due to time. This issue makes the FC operate under dynamic loads. Subsequently, water flooding or layer drying out, which antagonistically decreases the lifetime of the FC, may happen. To increase the lifetime of the FCs during the sharp dynamic load demands, experts have tried to optimize the materials, structures and control systems to enhance the operating condition inside the FCs [5]. Due to the electro-osmotic drag, the water in the anodic ionomer moves rapidly with the protons to the cathode, while the current increases. This causes the rapid dehydration of ionomers in anodes and also leads to a high Ohmic overvoltage. Also, cathode flooding occurs because of the increased water generated by the reaction and movement by protons. This event causes an increase in mass transfer loss because of the difficulty in O2 mass transfer [5]. With the back-diffusion process and absorption of the membrane, the water in the anode is being reallocated and the Ohmic over-voltage decreases again [5]. This can be a major obstacle to the instantaneous acceleration of electric vehicles using FCs. It is also an important issue in supplying electricity to the consumers who are locally fed from the FCs.
and are not connected to the grid. In this case, if the load demand increases suddenly, the FC is not able to supply the load demand quickly. In addition to depreciation, the voltage and current of the load will not be stable, which can be harmful to some loads. In the following, it is assumed to investigate and review other research articles to overcome this phenomenon.

Many studies such as [6–13] used energy storage system (EES), especially supercapacitors to improve the low dynamic response of the PEMFC. In [6], researchers used a supercapacitor equipped with a bidirectional DC/DC converter to release or absorb high power density to the load in rapid load changes. The simulation results showed that the EES performed well against load fluctuations. Authors [7] proposed a new system based on energy management and control strategy for a doubly fed induction generator (DFIG) based wind turbine/FC system equipped with a supercapacitor to control and manage the hybrid system in rapid load changes appropriately. A combination of photovoltaic (PV) and FC systems forms a good pair with acceptable performance for distributed generation applications [8]. Many researchers have focused their work similarly. Authors [9] proposed a completely decentralized energy management system with high reliability for the FC and supercapacitor based on an energy storage system. Improving the lifetime of solid oxide FC with the new backup battery converter was proposed and investigated in [10]. In [11], researchers proposed a real-time predictive energy management strategy for the FC/battery/ultra-capacitor hybrid energy storage system in electric vehicles which mainly focused on the management of EES to improve the performance of FCs in electric vehicles.

Other research such as [14–18] are based on battery systems to overcome the low dynamic response of PEMFC, but the main drawback of this system is the low power density of batteries and limitation of batteries’ lifetime. Usually, a supercapacitor storage device is preferable due to its high power density, high dynamics, and long lifetime rather than a battery [8]. For instance, authors [14] proposed a novel energy management policy based on FC/battery power sources for electrical scooter supply. In other research, authors proposed a control strategy of a fuel cell-battery hybrid system for optimizing the lift truckload cycle [15]. In [16], the authors proposed a simulation analysis of the fuel economy of an FC/battery passive hybrid power system for commercial vehicles. A rule-based energy management strategy for an FC/battery hybrid locomotive is being investigated [17] as new research based on hybrid usage of FC and batteries to improve the FC performance during variable loadings. Another similar research investigated [18] is based on multi-objective optimal predictive energy management for FC/battery hybrid construction vehicles.

Some research such as [19] used SMES to improve the operation of PEMFC. Authors [20] suggested using the SMES/battery besides PEMFC in space applications. The aim of using EES is to improve the PEMFC capability to feed different electrical load variations. The other important matter investigated [21] is the design and implementation of SMES and other EESs feeding different loads such as electric vehicles. Although using EES such as SMES can improve the dynamic response of PEMFC and other renewable energies, their control systems have some difficulties. In [22] the authors proposed a new control method based on pulse width modulation in current source converters (PWM-CSC) to manage the active and reactive power absorbed by the SMES independently. Moreover, another difficulty that the SMES systems face with is their cooling systems having to remain superconducting in different conditions. New research on M-SMES temperature equilibrium control strategies considering state assessment is being investigated [23].

Also, researchers [24, 25] have proposed and implemented different SMES cooling systems, such as developing a cryogen-free cooled SMES demonstrator based on MgB2. Some other researchers [26] worked on improving the efficiency of hybrid fuel cell-based vehicles through energy management strategies through online systemic management of fuel cells. Also, researchers [27] proposed an optimal fuzzy logic control for an FC hybrid electric vehicle based on particle swarm and advisor to improve the performance of the fuel cells. Another research represented a comparative study of a PEMFC, battery and supercapacitor based energy source owing to the hybrid vehicle to improve the FC dynamic response [28]. Interestingly research based on the performance of the SMES system with a non-linear dynamic evolution control approach for pulsed power load compensation is investigated and analysed in [29] while the authors formulated the SMES system connected to a DC/DC converter so brilliantly with a new control method for the converter to absorb or release the desired power by the SMES. Another related research for SMES technology systems is represented in [30]. The authors proposed an SMES/battery hybrid energy storage system based on a bidirectional Z-source inverter for electric vehicles. In [31], a coordinated-control strategy of scalable superconducting magnetic energy storage under an unbalanced voltage condition is being investigated.

As reviewed, a few articles have addressed the use of SMES in the FCs as energy storage, and most of them generally use supercapacitors or batteries. As a result, the pristine use of this system led us to consider using the SMES alongside PEMFC. In this paper, the proposed method is based on a DC/DC converter to use the energy stored in SMES in such a way that during a sudden increase in load with the help of an FC in the supply of load power and while the load power decreases, the
surplus energy is saved. The proposed control system for controlling the relevant converter was proposed and studied and simulated in the MATLAB environment, and the results illustrate the appropriate operation of the proposed system to improve the dynamic response of the FC to load demand supply.

2. PEMFC modelling

The PEMFC develops as one of the best candidates for electric vehicles because of its straightforwardness, practicality, speedy beginning up, lower working temperature, higher control thickness and general electrical effectiveness compared to some sized internal combustion engines. The output voltage in an FC under the standard state condition (25°C and 1 atm.) is near 1.229 V [5]. Although the practical voltage of FC is usually less than the perfect one because of the non-reversible voltage drops happening in FC systems, this is mentioned in Figure 1. The voltage drops in an FC system can be divided into three terms, which are non-reversible voltage drops. They are specific voltage drop, resistive voltage drop and concentration voltage drop. At low current conditions, the activation voltage drop is capable of the voltage drop of the FC. Concentration over voltage is more important at high current densities. The impacts of these three voltage drops and comparing the variation of FC voltage are illustrated from its polarization diagram in Figure 1. The foremost proficient working locale for the FC is the straight locale compared to the cell voltage between 0.55 and 0.8 V, as shown in Figure 1. The FC operation in this linear region is very imperative for system efficiency. The equations representing the voltage of the PEMFC are mentioned below [6]

\[
V_{FC} = E_{Nerst} - V_{act} - V_{conc} - V_{ohmic}
\]

\[
E_{Nerst} = 1.229 - (8.5 \times 10^{-4} \times (T - 298.15)) + 4.308 \times 10^{-4} \times T \times \ln \left( P_{H_2} + \frac{1}{2} P_{O_2} \right)
\]

In the above equations, the \( V_{FC} \), \( E_{Nerst} \), \( V_{act} \), \( V_{conc} \), \( V_{ohmic} \), \( T \) are FC output voltage, the Nerst chemical voltage produced by the FC, activation voltage drop, concentration voltage drop, Ohmic voltage drop and the FC temperature, respectively. The relative pressures of hydrogen and oxygen (\( P_{H_2} \) and \( P_{O_2} \)) are assumed to change between predefined lower and upper limitations for anode and cathode pressures. These pressures are inversely relative to the molar \( H_2 \) and \( O_2 \) flows and appropriately to the FC current. The molar \( H_2 \) pressure that responds to an arrangement to meet the load variations can be inferred as Equation (3), while the temperature variations of the FC can be represented as

\[
q_{H_2} = \frac{I_{FC} \times N_s \times N_p}{2FU}
\]

\[
T = 273 + T_0 + (T_0 - T_{rt} + T_{ic} \times I_{FC})(1 - e^{-\frac{I_{FC}}{T_{ic}}})
\]

Also, the activation voltage can be calculated as follows, while the \( C_{O_2} \) is the dissolved oxygen concentration in the interface of the cathode catalyst.

\[
V_{act} = \xi_1 + \xi_2 T + \xi_3 T \ln(I_{FC}) + \xi_4 \ln(C_{O_2})
\]

As Henry’s law describes, the dissolved \( O_2 \) concentration value at the gas or liquid interface can be represented as Equation (6), while the \( U \) is the utilization factor of FC can be defined as Equation (7). The utilization factor is one of the important variables of the FC that describes the ratio of the flow of the hydrogen reacted (\( q_{H_2}^{act} \)) to the input hydrogen flow (\( q_{H_2}^{in} \)). This parameter is proportional to the FC current and must be less than unity. This means the rapid load current increase can overload the FC and the protective devices will trip the FC due to protective scenarios [5,6]

\[
C_{O_2} = \frac{P_{O_2}}{5.08 \times 10^6 e^{-\frac{198}{T}}}
\]
Figure 3. Simplified model of the FC system [6].

\[
U = \frac{qH_2^{\text{react}}}{qH_2^{\text{in}}} = \frac{N_0IFc}{2FqH_2^{\text{in}}} \tag{7}
\]

where the \( N_0, IFc \) are the FC stack numbers and current, respectively. The next voltage drop, named Ohmic voltage drop, can be expressed by multiplying the FC current into the resistance of the FC electrolyte and other connecting equipment and wires as mentioned in Equation (8)

\[
V_{\text{ohmic}} = IFc \times R_{\text{Ohmic}} = IFc \times (R_m + R_C) \tag{8}
\]

where the \( R_c \) represents the concentration Ohmic resistance of FC and also by Ohm’s law the resistance of \( R_m \) can be defined as follows:

\[
R_m = \frac{r_m \times l}{A} \tag{9}
\]

where the \( l \) and \( A \) are the FC stack length and area. The Nafion series proton exchange membrane resistivity mentioned in Equation (9) can be determined as follows

\[
r_m = \frac{181.6 \left[ 1 + 0.03 \times J + 0.062 \left( \frac{r_m}{1000} \right)^2 \times J^{2.5} \right]}{[\lambda - 0.634 - 3J]e^{4.18 \times \left( T - \frac{303}{T} \right)}} \tag{10}
\]

\[
J = \frac{IFC}{A} \tag{11}
\]

where \( \lambda \) is the water content of the membrane. Equation (12) represents the concentration voltage of the FC and is defined as the voltage drop that is caused by the transportation of mass within the cell. This transportation influences the \( H_2 \) and \( O_2 \) concentrations effectively, particularly at high current densities.

\[
V_{\text{con}} = B \times \ln(1 - \frac{J}{J_{\text{max}}}) \tag{12}
\]

One of the important issues in FC systems is the double-layer charge effect of the capacitor. The FC equivalent circuit considering the capacitor effect is shown in Figure 2. The capacitor shows the layer of electrical charge on or close to the electrode–electrolyte interface, which is the capacity for electrical charge and vitality. Considering the impact of this effect, the elements of the FC yield voltage can be obtained more precisely [6]. As shown in Figure 2, it could be a variable resistance that represents the actuation, and concentration voltage drops are mentioned below.

\[
R_a = \frac{V_{\text{act}} + V_{\text{con}}}{IFc} \tag{13}
\]

According to the equivalent FC circuit, as shown in Figure 2, the KCL law can be written as Equation (14). Therefore, the output voltage of the FC can be calculated as Equation (15)

\[
d\frac{V_C}{dt} = \frac{IFC}{C} - \frac{V_C}{RaC} \tag{14}
\]

\[
V_{FC} = E_{\text{Nerst}} - V_C - V_{\text{Ohmic}} \tag{15}
\]
Table 1. Parameters of the fuel cell used in the simulation [6].

| Parameter | Value                          | Definition                                                                 |
|-----------|--------------------------------|---------------------------------------------------------------------------|
| A         | 6.25 [Cm² Cell⁻¹]              | Cell area                                                                 |
| B         | 0.016 (V)                      | Coefficient of concentration voltage                                       |
| C         | 2.5 (F)                        | FC double layer capacitance                                               |
| F         | 96486.7 [CKmol⁻¹]              | Coefficient of Faraday                                                   |
| Iₘₜₜ     | 1.5 [A]                        | Maximum Current Density                                                  |
| Nₛ        | 60                             | Series Cells Number                                                       |
| Nₚ        | 1                             | Parallel Cells Number                                                     |
| Rₖ        | 2 × 10⁻⁴                      | Concentration Ohmic Resistance                                            |
| T₀, T₁ₜ₁, T₂, Tₐ   | 28, 20, 0.7, 4000           | Empirical parameters used for modeling of the temperature fluctuation of FC|
| ξ₁, ξ₂, ξ₃, ξ₄ | -0.9514, 0.00312, 7.4 × 10⁻⁵, -1.87 × 10⁻⁴ | Activation voltage coefficient                                               |

Therefore, the output voltage of a series stack of a number of FCs is represented below.

\[ V_{\text{Stack}} = N_{S} \times V_{\text{FC}} \] (16)

Figure 3 illustrates the demonstration of the PEMFC based on the mentioned formulas, which were inserted into the MATLAB environment. Experiments show that the protection system of the FC limits the utilization factor \( U \) to more than 0.7 and also less than 0.9, \((0.7 < U < 0.9)\), elsewhere the protection system trips the FC. As conferred from Equation (7), the utilization factor is proportional to the FC current. Therefore, the immediate increase in load current increases the utilization factor. It is clear that the sharp variation of FC current will cause a trip command to FC in each stack.

Table 1 shows the fundamental parameters of the FC used in the simulation process [6].

3. SMES and converter system modelling

In the following the SMES and DC/DC bidirectional converter modelling are investigated.

3.1. SMES modelling

The most viewpoint of the SMES system is superconducting materials which are free of dissipation since there is no resistance to these materials. The coil is made of these materials to mitigate conductive energy loss. High-density energy is stored in the magnetic field. The biggest challenge of the SMES unit systems is keeping the coil within the superconducting state, in which the cryogenic system is capable of acting appropriately in the presence of a protective system to secure the SMES under irregular conditions. The impedances between the grid and the SMES coil can be accomplished by the control of electronic converter circuits. The DC/DC bidirectional converter used to accomplish SMES in FC application is illustrated in Figure 4. Equation (17) and Equation (18) represent the SMES power \( P_{\text{SMES}} \) and the energy \( E_{\text{SMES}} \) in terms of the magnet coil inductance \( L_{\text{SMES}} \), where are the SMES voltage \( V_{\text{SMES}} \) and current \( I_{\text{SMES}} \) respectively.

\[
E_{\text{SMES}} = \frac{1}{2} L_{\text{SMES}} I_{\text{SMES}}^2 \quad (17)
\]

\[
P_{\text{SMES}} = \frac{dE_{\text{SMES}}}{dt} = L_{\text{SMES}} I_{\text{SMES}} \frac{dI_{\text{SMES}}}{dt} = V_{\text{SMES}} I_{\text{SMES}} \quad (18)
\]

3.2. Bidirectional converter modelling

In Figure 4, the topology of a bidirectional DC/DC converter is illustrated to interconnect the SMES system to the FC for charge and discharge appropriately. As shown in Figure 4, by adjusting the duty cycle \( D \) of the switches \( S_1 \) and \( S_2 \), the average power exchanged by the SMES system can be controlled in a flexible condition in each switching period. The equation demonstrates the relation between the power of SMES and its current as modelled as the following [32]:

\[
P_{\text{SMES}} = V_{c} (2D - 1) I_{\text{SMES}} \quad (19)
\]

It can be inferred that while \( D > 0.5 \), the SMES will absorb energy by conducting the source current from \( S_1 \) and \( S_2 \), thus the SMES will charge. Elsewhere, while \( D < 0.5 \), the SMES will release the stored energy into the load by conducting the \( D_1 \) and \( D_2 \).

3.3. Proposed bidirectional DC/DC converter control system

The proposed system to control the bidirectional DC/DC converter is presented in Figure 5, which is
based on a PWM system and PI controller. In the proposed control system, the difference between $V_{dc\text{ref}}$ and $V_{dc\text{measured}}$ is delivered to a PI controller to produce the appropriate control signal to eliminate the steady-state error. The output of the controller is passed through a saturation block, which limits the signal between $-1$ and $+1$ to prevent high values and saturation. In the following, the produced signal is added by a constant value of 0.5 and compared to a sawtooth pulse (PWM) to produce the gate pulses which drive the bidirectional converter. Consider when the FC is in a stable condition and the load power is constant and the FC is producing the whole load power. In this condition, it is expected that the SMES power is equal to zero. So the values of $V_{dc\text{ref}}$ and $V_{dc\text{measured}}$ are the same. Thus, the error signal is equal to zero.

Figure 5. Proposed control block diagram of the bidirectional DC/DC converter.

Figure 6. Schematic of the FC connected with bidirectional DC/DC converter with SMES.

Figure 7. Load power increasing with and without SMES.
Also, by adding a constant value of 0.5 and comparing it with a saw tooth pulse that varies between 0 and 1, the produced duty cycle of 50% is generated. Due to Equation (19), the active power released/absorbed by the SMES is equal to zero, which means appropriate operation. In another condition, while the load increases rapidly, so the error voltage signal increases and by passing through the saturation block and other items, the duty cycle will decrease, which means releasing the SMES stored energy to the load and vice versa. The main advantages of the proposed method to other similar research are the simplified implementation, fast dynamic and accurate response with zero steady-state error.
4. Simulation results

It is assumed to analyse, review and discuss the simulation results of the proposed system in this section. Figure 6 illustrates the schematic of a 10 kW, 45 V PEMFC connected to a bidirectional DC/DC converter equipped with SMES into a variable DC load. As shown, the FC system is connected to the load through a boost DC/DC converter to compensate for the variations in the output voltage of the FC due to variations in load power demand and to deliver a stabilized voltage into the load. Moreover, the proposed system includes a bidirectional DC/DC converter to connect the SMES, which is connected to the DC link through a current smoothing inductance. The bidirectional converter is controlled by the proposed PWM controller to release or absorb enough energy due to load demand variations.
Figure 7 illustrates the variations of the load power demand in the presence and absence of the SMES system. As illustrated, the load power is increased +50% suddenly at $t = 20$ second. According to the diagram, it can be inferred that in the absence of the SMES, it takes longer to fully supply the load power, and this causes more pressure on the FC system. Similarly, Figure 8 investigates the same diagram in a condition where the load power is accompanied by a sudden decrease of $-50\%$ at $t = 25$ second.

Figures 9 and 10 show the load voltage (DC link voltage) diagram in two modes of presence and absence of the SMES system, while the load increases and decreases. As can be seen, the SMES and the bidirectional converter were able to relatively smoothen the load voltage fluctuations more, while the load power changes. It is inferred from Figure 9 that while the load demand power increases, the DC link voltage drops to overcome the instantaneous load power increase. The important matter is in case of the FC equipped with the bidirectional DC/DC converter and SMES, the depth of voltage drop is less than in the case of without SMES.

Also it is noticeable from Figure 10 that while the load demand power decreases, the DC link voltage increases to absorb the instantaneous load power reduction. The important matter is in case of the FC is equipped with a bidirectional DC/DC converter and SMES, the overshoot of the voltage increase is less than in the case without SMES.

Figure 11 illustrates the FC output voltage in each of the two mentioned conditions. It is inferred that the SMES is able to reduce the FC voltage fluctuations during the load changes.

The DC/DC bidirectional converter's current is illustrated in Figure 12, which shows the SMES charging or discharging energy states. Before the load demand increases, the bidirectional converter is in absorbing energy mode, so its current is negative, while after the load demand increases at $t = 20$ seconds, the SMES releases the stored energy into the load periodically, so the current increases to a positive value. Finally, after the load demand reduction, the SMES condition is changed again to the charging mode.

In the same condition, Figure 13 illustrates the SMES’s current while the charging and discharging conditions are shown. Also, the SMES’s voltage is illustrated in Figure 14. In charging conditions, its voltage is positive and in discharging conditions, the voltage varies from negative to positive periodically with a negative average value.

Finally, Figure 15 shows the diagram of the $H_2$ utilization factor of the FC. As expected, in the presence
of the SMES, the rapid fluctuations of this parameter are adjusted. As mentioned [5,6], preventing sudden variations of the utilization factor can increase the performance and lifetime of the FC. Moreover, the $H_2$ utilization factor of FC exceeds 0.9 in the absence of SMES, which means the protective device will trip the FC, while the same factor is less than 0.8 in the presence of SMES.

Table 2 represents the load response settling time comparison between the presence and absence of the SMES and bidirectional DC/DC converter, controlled by the proposed system. As inferred from Table 2, the SMES and bidirectional converter equipped with the proposed control system made an impressive performance to improve the FC response in load variations. This achievement can be used in various applications such as electric vehicles and microgrids.

### 5. Conclusion

In this research, the effect of using SMES with a new control system for a bidirectional converter to improve the FC performance was investigated. For this purpose, a DC/DC bidirectional converter controlled by a PWM-based control system was proposed, designed and investigated. The summary of the results shows that the FC system is not able to provide sudden load demand variations. In other words, the FC is able to provide the load demand within a time delay. To overcome the problem, the EES with the proposed control system was operated. It was not only able to compensate for the delay time well, but also by limiting the sudden variations in the utilization factor of the FC, it can increase its lifetime and provide better performance. The comparison between the presence and absence of the SMES with the proposed system illustrates a 35–52% improvement in settling time and a significant improvement in load demand feeding appropriately. For future studies, it is recommended to investigate the robustness test of the bidirectional converter due to load changes. All the simulation process is evaluated and simulated in a MATLAB/Simulink environment.

### Disclosure statement

No potential conflict of interest was reported by the author(s).

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