Potential of *Chrozophora tinctoria* Seed Oil as a Biodiesel Resource

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**Featured Application:** Produced biodiesel through this research work can be used as a suitable fuel source instead of petroleum-derived fuels.

**Abstract:** Biodiesel is a renewable fuel that has been widely used in recent years. There are various resources used as biodiesel feedstocks, including animal fats, waste oils, and vegetable oils. In the present study, *Chrozophora tinctoria* seed oil is introduced as a new biodiesel feedstock. *C. tinctoria* is a weed and non-edible plant. So, the primary cost of this resource is very low, and hence it can be considered as a biodiesel source. This plant can also grow in most weather conditions. In the present study, the research team tried to produce biodiesel from *C. tinctoria* seeds through a transesterification reaction. To intensify the transesterification reaction, an ultrasonic device was used. In order to perform the transesterification reaction, potassium hydroxide was used as a catalyst. Important parameters, such as the reaction temperature, reaction time, molar ratio of methanol, and concentration of the catalyst, were adjusted. Based on the adjusted conditions, a biodiesel yield of 84% was attained. The properties of the *C. tinctoria* biodiesel was compared with the American Society for Testing and Materials (ASTM) standard. The results show the properties of a biodiesel: the density, kinematic viscosity, pour point, flash point, cloud point, and acid number are 0.868 g/cm$^3$, 3.74 mPa, −7 °C, 169 °C, 4 °C, and 0.43 mg, respectively. The specification properties of *C. tinctoria* biodiesel can thus pass the requirement of the ASTM standard. So, *C. tinctoria* seed oil can be used as a suitable fuel source instead of petroleum-derived fuels.

**Keywords:** biomass; biodiesel; *Chrozophora tinctoria*; seed oil

1. Introduction

Due to an increasing global population, the use of liquid fuels, especially in the transportation sector, has grown. Reduction of fossil fuel resources, increasing greenhouse gas emissions, and increasing oil prices created the need to find sustainable, renewable, efficient, cost-effective, and low-emission alternatives [1,2]. One of the alternative fuel types is biodiesel, which was introduced as a suitable fuel instead of conventional diesel fuel for using in heating systems and specifically for diesel engines [3,4]. Chemically, biodiesel is a combination of fatty methyl ester acids that are produced by the reaction of diglycerol with alcohols in the presence of a catalyst along a process called transesterification [5,6].
Biodiesel is made from bio-oils. The number of carbons in the carbon chain of diesel fuel is similar to vegetable oils (containing 14–18 carbons). Because of the structural properties of biodiesel, this resource can play an important role as a viable alternative to conventional (diesel) energy [7]. Generally, the production price of biodiesel is high, being almost twice that of diesel’s price. The price of biodiesel production consists of two main components that are the price of the raw material and price of the biodiesel production process [8,9]. Although, large amounts of oils, such as restaurant waste oil and animal fat, can be used to produce the biodiesel, the main problem with using these resources is that the transesterification reaction of some of these resources is very difficult. As a result, the cost of biodiesel production from these materials increase [10]. One of the main issues that play an important role in the final price of the biodiesel is the price of the oil that is used as the feedstock. The appropriate way to reduce the price of the produced biodiesel is the use of non-edible oils as feedstocks in the biodiesel production process, which reduces the price of finished product. So far, several researches have been done on the application of non-edible oils as the feedstock of biodiesel [11–23], such as rapeseed [24], sea mango [25], rubber seed [26], mahua [27], Hodgsonia macrocarpa [28], karanja [29], moringa [30], palm [31], jatropha [32], and tree of heaven [33]. So, intensive research on bioenergy resources, including crops with less food importance, or non-edible, can help to decrease the greenhouse gas emission and control climate change. The ideal non-edible resources should be water and nutrient efficient, fast growing, have a high tolerance to environmental stresses, and low invasive potential [34,35]. One of the non-edible resources that could be a novel resource for biodiesel is Chrozophora tinctoria seeds.

1.1. Why Chrozophora tinctoria?

*C. tinctoria* is an annual summer and warm season weed plant [36]. It can be observed under different light, soil, and moisture conditions [37,38]. Recently, some researchers suggested that *C. tinctoria* fruit could provide a new resource of oil [39,40]. The fruit of *C. tinctoria* is like a capsule in the shape of three spheres attached to a rounded-triangular structure. Fruit of *C. tinctoria* has three angular seeds [41]. *C. tinctoria* seeds are a valuable source of oil, which can be suitable for bioenergy purposes. Moreover, *C. tinctoria* is a non-edible, weed plant, so the primary cost of *C. tinctoria* seed is very low and, hence, can be introduced as a biodiesel source. This research focuses on *C. tinctoria* as a potential bioenergy crop. The biofuel production possibilities from this crop is investigated in this research paper.

1.2. *C. tinctoria* in the World and Iran

*C. tinctoria* is mainly found in the central/south Asia and Mediterranean region. This plant is described as native to the different countries (Figure 1), including Afghanistan, Albania, Algeria, Bulgaria, Cyprus, Egypt, France, Greece, India, Iran, Italy, Kazakhstan, Libya, Morocco, Pakistan, Palestine, Portugal, Romania, Saudi Arabia, Spain, Tunisia, Turkey, Turkmenistan, and Yemen [42,43]. By considering the weather conditions of Iran, *C. tinctoria* can be cultivated in all the regions of Iran (Figure 1). For example, different species of the Chrozophora genus have been found in the different provinces in Iran, such as East-Azerbaijan [37], Chaharmahal and Bakhtiari, Markazi, Qom, Qazvin, and Isfahan [36].

Based on the above literature review on the potential of *C. tinctoria* seeds as a novel non-edible resource for biodiesel production, in the present study the application of *C. tinctoria* seed oil as a novel feedstock was experimentally investigated. In the Section 2, the experimental procedure for biodiesel production from the *C. tinctoria* seed oil is presented. It is noteworthy that ultrasonic waves were also used in this research to reduce the transesterification reaction time. Finally, in the Section 3, the properties of the biodiesel are evaluated and then the properties of the produced biodiesel are compared with the ASTM standards.
2. Materials and Methods

2.1. Raw Materials

*C. tinctoria* were collected from the Fars province (Southwest of Iran), in August of 2019. A Global Positioning System (GPS) was used to mark the locations (the longitude of 40°51′–50°51′ E and latitude of 20°30′–30°30′ N, and altitude of 2890 m). The sampling was done by a randomized collection in an area of about 2000 m². Matured fruits were isolated manually from the aerial parts and the seeds were separated from the fruit, then the fruits were washed with sterile water, and then dried at ambient temperature for seven days. In Figure 2, the different stages of plant sampling are shown.

![Figure 1. Potential countries for *C. tinctoria* cultivation [43].](image1)

![Figure 2. The plant sampling and seed separation process of *C. tinctoria*.](image2)
The seeds of *C. tinctoria* were prepared to determine their properties, and thus that of the seed oil and biodiesel. The *C. tinctoria* seeds were removed from the fruits. Seeds were powdered using a coffee grinder. Then the crushed seeds were transferred to a Soxhlet extractor to extract the oil. Oil extraction was performed using n-hexane for 8 h. The solvent was evaporated under reduced pressure at 60 °C using a rotary evaporator for 3 h.

2.2. Methodology

Fatty acids of the *C. tinctoria* seed oil were determined using Metcalfe procedure [44], and fatty acid composition were identified using a gas chromatography (Clarus580 GC) equipped with a FID detector. That equipment has been sourced from FARASOUT SANAT Eng CO, Tehran, Iran. One microliter of prepared sample was injected to the gas chromatography unit, which was equipped with a BP-30 column and FTIR detector that was kept isothermally standardized to encounter BS-EN 14103 standard. The total run time for each sample was 30 min. Fatty acid profile was determined by classifying and calculating relative peak areas.

In order to perform the transesterification reaction, an ultrasonic reactor was used. In the first step, a catalyst (e.g., potassium hydroxide (KOH)) and methanol was mixed together by a magnetic stirrer. It is noteworthy that methoxide was prepared by mixing methanol that had a molar ratio of 1:7, with 1 wt% of KOH. The prepared methoxide was added to the *C. tinctoria* seed oil. Then, the solution was transferred into the ultrasonic reactor. An ultrasonic device (Hielscher Model UP400S, USA) was applied to perform the transesterification reaction. That equipment has been sourced from FARASOUT SANAT Eng CO, Tehran, Iran. The ultrasonic device was controlled using a computer with the help of UPC software. An ultrasonic probe with a diameter of 10 mm and a height of 60 mm was used to transmit the ultrasound to the solution. The effective length of the probe that was placed inside the solution was 55 mm. The reaction time was adjusted every 5 min. The reaction temperature was adjusted to 45 ± 0.45 °C with the help of water circulating between the two reactor walls, and all experiments were performed at atmospheric pressure. After completing the reaction time, the biodiesel mixture was removed from the ultrasonic reactor. In order to stop the reaction, the biodiesel mixture was put into a cold ice bath. The mixture was stored in a separation plate and the mixture was completely separated into two phases. The lower phase was glycerin and the upper one was biodiesel. In Figure 3, the biodiesel production process is shown. After separation of the glycerin, the biodiesel should be purified. The separated part from the glycerin was washed by warm water to purify the biodiesel. In the next section, in order to remove the water from the biodiesel, the washed biodiesel was heated up for one hour in an oven (temperature was adjusted to 60 °C). Finally, a gas chromatography unit was used to identify the yield of the biodiesel. Equation (1) was used [34,45] to determine the yield of the biodiesel.

\[
\text{Biodiesel yield} = \frac{\sum A - AIS}{AIS} \times \frac{MIS}{M}
\]

where \(\sum A\) is the total area under the peak of total fatty acids, \(MIS\) is the weight of the internal standard, \(AIS\) is the area under the peak for the internal standard (C19:0), and \(M\) is the weight of the sample.

After purification of the biodiesel, the most important physicochemical properties of the biodiesel, including the kinematic viscosity at 40 °C (ASTM D445), density at 15 °C (ASTM D4052), pour point (ASTM D6751), cloud point (ASTM D6751), flash point (ASTM D93), oxidation stability at 110 °C (EN 14112), acid value (ASTM D664), and cetane number (ASTM D613), were determined, based on ASTM standard [46].
3. Results and Discussion

3.1. Seed Oil Properties

The seed and oil physico-chemical characteristics of *C. tinctoria* are shown in Table 1. The oil content was 26%. So, the oil content of *C. tinctoria* seed is appropriate, and this feedstock can thus be introduced as a feasible primary material to produce biodiesel. The kinematic viscosity of the *C. tinctoria* oil is 4.32 mPa s. The viscosity of the *C. tinctoria* oil is less than that of some other feedstocks. This property is an important characteristic of the oil as a new feedstock to produce biodiesel.

| Physico-Chemical Parameters | Unit   | Content |
|-----------------------------|--------|---------|
| Oil content                 | %      | 26      |
| Weight of 1000 seeds        | g      | 15      |
| Density                     | g/cm³  | 0.872   |
| Kinematic viscosity         | mPa s  | 4.32    |
| Acid value                  | Mg KOH/g oil | 2.5 |
| Iodine value                | g I₂/100 g oil | 170 |
| Water content               | mg/g   | 50      |

3.2. Fatty Acid Profile

In Table 2, the fatty acid structure of the *C. tinctoria* seed oil is shown. *C. tinctoria* seed oil consists of both unsaturated and saturated fatty acids. According to Table 2, the main fatty acids of *C. tinctoria* seed oil are unsaturated fatty acids; in other words, the unsaturated fatty acid content of this oil is 91.45% of the total oil. *C. tinctoria* seed oil contains a high content of polyunsaturated fatty acids, as the main fatty acid. The main fatty acids were identified as palmitic acid (5.32%), linoleic acid (76.68%), stearic acid (3.15%), and oleic acid (13.99%).

3.3. *C. tinctoria* Biodiesel Properties

After purification of the *C. tinctoria* biodiesel, the biodiesel yield was calculated by Equation (1). The results show that the biodiesel yield from the oil is 84%. In order to investigate the properties of *C. tinctoria* biodiesel as a new resource, the physicochemical characteristics of the produced biodiesel was measured. In Table 3, the physicochemical characteristics of the *C. tinctoria* biodiesel is presented.
According to the results, it is obvious that all the physicochemical characteristics of the produced biodiesel are in agreement with the ASTM standards.

**Table 2.** Fatty acid composition of oil extracted from *C. tinctoria* seeds.

| Fatty Acid                  | Content (%) |
|-----------------------------|-------------|
| Palmitic acid (C16:0)       | 5.32 ± 0.047|
| Palmitoleic acid (C16:1)    | 0.11 ± 0.50 |
| Stearic acid (C18:0)        | 3.15 ± 0.19 |
| Oleic acid (C18:1)          | 13.99 ± 0.29|
| Linoleic acid (C18:2)       | 76.68 ± 0.16|
| Linolenic acid (C18:3)      | 0.67 ± 0.13 |

\[\sum \text{UFA} = 91.45\]
\[\sum \text{SFA} = 8.43\]
\[\sum \text{MUFA} = 14.10\]
\[\sum \text{PUFA} = 77.35\]
\[\sum \text{UFA: SFA} = 10.85\]
\[\sum \text{MUFA: PUFA} = 0.18\]

Note: UFA, unsaturated fatty acids; MUFA, monounsaturated fatty acids; PUFA, polyunsaturated fatty acids; SFA, saturated fatty acids.

**Table 3.** Properties of the biodiesel produced from *C. tinctoria*.

| Parameters                     | Method          | Limitation       | Units     | Content |
|--------------------------------|-----------------|------------------|-----------|---------|
| Density at 15 °C               | ASTM D 4052     | 0.86–0.90 g/cm³ |           | 0.862   |
| Kinematic Viscosity @ 40 °C   | ASTMD445        | 1.9–6.0 mm²/s   |           | 3.74    |
| Flash Point, Closed Cup        | D93             | >130 °C         |           | 169     |
| Cloud point                    | ASTM D6751      | −3 to 12 °C     |           | 4       |
| Pour point                     | ASTM D6751      | −15 to 10 °C    |           | −7      |
| Acid Number                    | ASTMD664        | 0.50 mg         |           | 0.43    |

Viscosity is one of the important properties of biodiesel. By considering the biodiesel standard (ASTM), the viscosity of a biodiesel should be in the range of 1.9–6.0 mm²/s. The results show that the viscosity of *C. tinctoria* biodiesel is 3.74 mm²/s, which is lower than different biodiesel resources; for example, moringa (5 mm²/s) [47], karanja (6.13 mm²/s) [48], and neem (5.21 mm²/s) [47]. Another important characteristic of a biodiesel resource is its density. Density plays an important role in the fuel atomization in the combustion process of a diesel engine [49]. Based on the biodiesel standards (ASTM and EN), the range of a new biodiesel resource should be 0.86–0.9 (g/cm³). The result of the present study shows that the density of *C. tinctoria* biodiesel is 0.862 (g/cm³). By reviewing the recent studies, it is clear that the density of the *C. tinctoria* biodiesel is lower than many of the other resources, such as karanja (0.931 g/cm³) [48], moringa (0.883 g/cm³) [47], rapeseed (0.882 g/cm³) [47], and tobacco (0.888 g/cm³) [48]. Another biodiesel property that plays an important role in the corrosion of the internal parts of diesel engines, is the acid number. The ASTM standard consider a strict law for acid number. Based on the ASTM standard, the acid number of a new biodiesel should not exceed 0.5 mg KOH/g. According to the result of the present study, the acid number value of the *C. tinctoria* biodiesel is 0.41 mg KOH/g. So, this acid number is suitable for a new biodiesel resource. In this present study, other properties of the *C. tinctoria* biodiesel have been measured, including the cloud point, pour point, and flash point. The results show these properties of the *C. tinctoria* biodiesel pass the ASTM standard. It is noteworthy that the specification properties of the *C. tinctoria* biodiesel are within the ASTM standard range and that the biodiesel produced from *C. tinctoria* seed oil can be used as a suitable fuel source instead of petroleum-derived fuels.
4. Conclusions

In this research, the *C. tinctoria* seed oil, which is a weed plant, was introduced as a new resource for biodiesel production. In order to intensify the transesterification reaction, an ultrasonic device was used. Potassium hydroxide was also used as the catalyst for the transesterification reaction. Important parameters, such as the reaction temperature, reaction time, molar ratio of methanol, and concentration of the catalyst, were adjusted. Based on the adjusted condition, a biodiesel yield of 84% was obtained. The important properties of the *C. tinctoria* biodiesel were investigated. The results show that the properties of the biodiesel, namely, the density, kinematic viscosity, pour point, cloud point, and acid number, are 0.868 g/cm$^3$, 3.74 mPa$^{-1}$, $−7$ °C, 169 °C, and 0.43 mg, respectively. The physicochemical properties of the *C. tinctoria* biodiesel are thus in agreement with the biodiesel standard (ASTM standard). In other words, it is clear that the specifications of the physical and chemical characteristics of *C. tinctoria* biodiesel are in agreement with the ASTM standard range. So, biodiesel produced from *C. tinctoria* seed oil can be used as a suitable fuel source instead of petroleum-derived fuels.

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**References**

1. Brennan, L.; Owende, P. Biofuels from microalgae—A review of technologies for production, processing, and extractions of biofuels and co-products. *Renew. Sustain. Energy Rev.* 2010, 14, 557–577. [CrossRef]
2. Hoseini, S.S.; Najafi, G.; Ghobadian, B.; Mamat, R.; Sidik, N.A.C.; Azmi, W.H. The effect of combustion management on diesel engine emissions fueled with biodiesel-diesel blends. *Renew. Sustain. Energy Rev.* 2017, 73, 307–331. [CrossRef]
3. Xue, J.; Griff, T.E.; Hansen, A.C. Effect of biodiesel on engine performances and emissions. *Renew. Sustain. Energy Rev.* 2011, 15, 1098–1116. [CrossRef]
4. Xue, J. Combustion characteristics, engine performances and emissions of waste edible oil biodiesel in diesel engine. *Renew. Sustain. Energy Rev.* 2013, 23, 350–365. [CrossRef]
5. Shahid, E.M.; Jamal, Y. Production of biodiesel: A technical review. *Renew. Sustain. Energy Rev.* 2011, 15, 4732–4745. [CrossRef]
6. Makareviciene, V.; Skorupskaite, V.; Levisauskas, D.; Andruleviciute, V.; Kazancev, K. The optimization of biodiesel fuel production from microalgae oil using response surface methodology. *Int. J. Green Energy* 2014, 11, 527–541. [CrossRef]
7. Demirbas, A. Biodiesel production from vegetable oils via catalytic and non-catalytic supercritical methanol transesterification methods. *Prog. Energy Combust. Sci.* 2005, 31, 466–487. [CrossRef]
8. Demirbas, A.; Karslioglu, S. Biodiesel production facilities from vegetable oils and animal fats. *Energy Sources Part A* 2007, 29, 133–141. [CrossRef]
9. Yusuf, N.; Kamarudin, S.K.; Yaakub, Z. Overview on the current trends in biodiesel production. *Energy Convers. Manag.* 2011, 52, 2741–2751. [CrossRef]
10. Canakei, M. The potential of restaurant waste lipids as biodiesel feedstocks. *Bioresour. Technol.* 2007, 98, 183–190. [CrossRef]
11. Balat, M. Potential alternatives to edible oils for biodiesel production—A review of current work. *Energy Convers. Manag.* 2011, 52, 1479–1492. [CrossRef]
12. Abtahi, A.; Badruddin, I.A.; Badarudin, A.; Khayoon, M.; Triwahyono, S. Recent scenario and technologies to utilize non-edible oils for biodiesel production. *Renew. Sustain. Energy Rev.* 2014, 37, 840–851.
13. Banković-Ilić, I.B.; Stamenković, O.S.; Veljković, V.B. Biodiesel production from non-edible plant oils. *Renew. Sustain. Energy Rev.* 2012, 16, 3621–3647. [CrossRef]
14. Ayoob, A.K.; Fadhil, A.B. Valorization of waste tires in the synthesis of an effective carbon based catalyst for biodiesel production from a mixture of non-edible oils. *Fuel* **2020**, *264*, 116754. [CrossRef]
15. Mardhiah, H.H.; Ong, H.C.; Masjuki, H.; Lim, S.; Lee, H. A review on latest developments and future prospects of heterogeneous catalyst in biodiesel production from non-edible oils. *Renew. Sustain. Energy Rev.* **2017**, *67*, 1225–1236. [CrossRef]
16. Malani, R.S.; Shinde, V.; Ayachit, S.; Goyal, A.; Moholkar, V.S. Ultrasound-assisted biodiesel production using heterogeneous base catalyst and mixed non–edible oils. *Ultrason. Sonochem.* **2019**, *52*, 232–243. [CrossRef]
17. Gupta, J.; Agarwal, M.; Dalai, A. Optimization of biodiesel production from mixture of edible and nonedible vegetable oils. *Biocatal. Agric. Biotechnol.* **2016**, *6*, 112–120. [CrossRef]
18. Yadav, A.K.; Khan, M.E.; Dubey, A.M.; Pal, A. Performance and emission characteristics of a transportation diesel engine operated with non-edible vegetable oils biodiesel. *Case Stud. Therm. Eng.* **2016**, *8*, 236–244. [CrossRef]
19. Devi, A.; Das, V.K.; Deka, D. Ginger extract as a nature based robust additive and its influence on the oxidation stability of biodiesel synthesized from non-edible oil. *Fuel* **2017**, *187*, 306–314. [CrossRef]
20. Singh, Y.; Farooq, A.; Raza, A.; Mahmood, M.A.; Jain, S. Sustainability of a non-edible vegetable oil based bio-lubricant for automotive applications: A review. *Process Saf. Environ. Prot.* **2017**, *111*, 701–713. [CrossRef]
21. Ong, H.C.; Mofijur, M.; Silitonga, A.; Gumilang, D.; Kusumo, F.; Mahlia, T. Physicochemical Properties of Biodiesel Synthesised from Grape Seed, Philippine Tung, Kesambi, and Palm Oils. *Energies* **2020**, *13*, 1319. [CrossRef]
22. Corral Bobadilla, M.; Fernández Martínez, R.; Lostado Lorza, R.; Somovilla Gómez, F.; Vergara González, E.P. Optimizing Biodiesel Production from Waste Cooking Oil Using Genetic Algorithm-Based Support Vector Machines. *Energies* **2018**, *11*, 2995. [CrossRef]
23. Corral Bobadilla, M.; Lostado Lorza, R.; Escribano García, R.; Somovilla Gómez, F.; Vergara González, E.P. An improvement in biodiesel production from waste cooking oil by applying thought multi-response surface methodology using desirability functions. *Energies* **2017**, *10*, 130. [CrossRef]
24. Westbrook, C.K.; Naik, C.V.; Herbinet, O.; Pitz, W.J.; Mehli, M.; Sarathy, S.M.; Curran, H.J. Detailed chemical kinetic reaction mechanisms for soy and rapeseed biodiesel fuels. *Combust. Flame* **2011**, *158*, 742–755. [CrossRef]
25. Kansedo, J.; Lee, K.T.; Bhatia, S. Cerbera odollam (sea mango) oil as a promising non-edible feedstock for biodiesel production. *Fuel* **2009**, *88*, 1148–1150. [CrossRef]
26. Ahmad, J.; Yusup, S.; Bokhari, A.; Kamil, R.N.M. Study of fuel properties of rubber seed oil based biodiesel. *Energy Convers. Manag.* **2014**, *78*, 266–275. [CrossRef]
27. Aalam, C.S.; Saravanan, C. Effects of nano metal oxide blended Mahua biodiesel on CRDI diesel engine. * Ain Shams Eng. J.* **2017**, *8*, 689–696. [CrossRef]
28. Cao, L.; Zhang, S. Production and characterization of biodiesel derived from Hodgsonia macrocarpa seed oil. *Appl. Energy* **2015**, *146*, 135–140. [CrossRef]
29. Pradhan, R.; Naik, S.; Bhatnagar, N.; Swain, S. Moisture-dependent physical properties of Karanja (*Pongamia pinnata*) kernel. *Ind. Crops Prod.* **2008**, *28*, 155–161. [CrossRef]
30. Matinise, N.; Fuku, X.; Kaviyarasu, K.; Mayedwa, N.; Maaza, M. ZnO nanoparticles via Moringa oleifera green synthesis: Physical properties & mechanism of formation. *Appl. Surf. Sci.* **2017**, *406*, 339–347.
31. Benjumea, P.; Agudelo, J.; Agudelo, A. Basic properties of palm oil biodiesel–diesel blends. *Fuel* **2008**, *87*, 2069–2075. [CrossRef]
32. Garnayak, D.; Pradhan, R.; Naik, S.; Bhatnagar, N. Moisture-dependent physical properties of jatropha seed (*Jatropha curcas L.*). *Ind. Crops Prod.* **2008**, *27*, 123–129. [CrossRef]
33. Hoseini, S.S.; Najafi, G.; Ghobadian, B.; Mamat, R.; Ebadi, M.T.; Yusaf, T. Ailanthus altissima (tree of heaven) seed oil: Characterisation and optimisation of ultrasonication-assisted biodiesel production. *Fuel* **2018**, *220*, 621–630. [CrossRef]
34. Moosavi, S.A.; Aghaaliakhani, M.; Ghobadian, B.; Fayyazi, E. Okra: A potential future bioenergy crop in Iran. *Renew. Sustain. Energy Rev.* **2018**, *93*, 517–524. [CrossRef]
35. Kole, C.; Joshi, C.P.; Shonnard, D.R. *Handbook of Bioenergy Crop Plants*; CRC Press: Boca Raton, FL, USA, 2012.
36. Golkar, P.; Taghizadeh, M.; Jalali, S.A.H. Determination of phenolic compounds, antioxidant and anticancer activity of Chrozophora tinctoria accessions collected from different regions of Iran. *J. Food Biochem.* **2019**, *43*, e13036. [CrossRef]
37. Asghar Aliloo, A.; Mustafavi, S.-H.; Ezzati, F. Allelopathic potential of Chrozophora tinctoria on early growth of Barley and Wheat. *Azarian J. Agric.* **2015**, *2*, 12–18.
38. Usman, H.; Musa, Y.; Ahmadu, A.; Tijani, M. Phytochemical and antimicrobial effects of Chrozophora senegalensis. *Afr. J. Tradit. Complement. Altern. Med.* **2007**, *4*, 488–494. [CrossRef]
39. Hazrati, S.; Nicola, S.; Khurizadeh, S.; Alirezalu, A.; Mohammadi, H. Physico-chemical properties and fatty acid composition of Chrozophora tinctoria seeds as a new oil source. *Grasas y Aceites* **2019**, *70*, 328. [CrossRef]
40. Al-Snaifi, A.E. A review on lawsonia inermis: A potential medicinal plant. *Int. J. Curr. Pharm. Res.* **2019**, *11*, 1–13. [CrossRef]
41. Van Welzen, P.C. Revision and phylogeny of subtribes Chrozophorinae and Doryxylinae (*Euphorbiaceae*) in Malesia and Thailand. *Blumea-Biodivers. Evol. Biogeogr. Plants* **1999**, *44*, 411–436.
42. Delazar, A.; Talischi, B.; Nazemiyeh, H.; Rezazadeh, H.; Nahar, L.; Sarker, S. Chrozophorin: A new acylated flavone glucoside from Chrozophora tinctoria (*Euphorbiaceae*). *Rev. Bras. Farmacogn.* **2006**, *16*, 286–290. [CrossRef]
43. Chrozophora Tinctoria. Available online: [http://www.plantsoftheworldonline.org/taxon/urn:lsid:ipni.org:names:340969-1#source-KBD](http://www.plantsoftheworldonline.org/taxon/urn:lsid:ipni.org:names:340969-1#source-KBD) (accessed on 17 April 2020).
44. Metcalfe, L.; Schmitz, A.; Pelka, J. Rapid preparation of fatty acid esters from lipids for gas chromatographic analysis. *Anal. Chem.* **1966**, *38*, 514–515. [CrossRef]
45. Borugadda, V.B.; Goud, V.V. Biodiesel production from renewable feedstocks: Status and opportunities. *Renew. Sustain. Energy Rev.* **2012**, *16*, 4763–4784. [CrossRef]
46. Knothe, G. Analyzing biodiesel: Standards and other methods. *J. Am. Oil Chem. Soc.* **2006**, *83*, 823–833. [CrossRef]
47. Atabani, A.E.; Silitonga, A.S.; Badruddin, I.A.; Mahlia, T.; Masjuki, H.; Mekhilef, S. A comprehensive review on biodiesel as an alternative energy resource and its characteristics. *Renew. Sustain. Energy Rev.* **2012**, *16*, 2070–2093. [CrossRef]
48. Hasni, K.; Ilham, Z.; Dharma, S.; Varman, M. Optimization of biodiesel production from Brucea javanica seeds oil as novel non-edible feedstock using response surface methodology. *Energy Convers. Manag.* **2017**, *149*, 392–400. [CrossRef]
49. Anwar, M.; Rasul, M.G.; Ashwath, N. Production optimization and quality assessment of papaya (*Carica papaya*) biodiesel with response surface methodology. *Energy Convers. Manag.* **2018**, *156*, 103–112. [CrossRef]

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