Immobilization of an Iridium Pincer Complex in a Microporous Polymer for Application in Room-Temperature Gas Phase Catalysis

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Abstract: An iridium dihydride pincer complex \([\text{IrH}_2\text{-}(\text{POCOP})]\) is immobilized in a hydroxy-functionalized microporous polymer network using the concepts of surface organometallic chemistry. The introduction of this novel, truly innocent support with remote OH-groups enables the formation of isolated active metal sites embedded in a chemically robust and highly inert environment. The catalyst maintained high porosity and without prior activation exhibited high efficacy in the gas phase hydrogenation of ethene and propene at room temperature and low pressure. The catalyst can be recycled for at least four times.

Organometallic pincer complexes have received tremendous interest due to their great number of applications in homogeneous catalysis, such as dehydrogenation, coupling, hydrogen transfer, as well as aldol and Michael reactions\cite{1-9}.

Immobilization of pincer complexes by covalent bond formation with the supporting material, such as silica and metal oxides\cite{10-18} as well as metal-organic frameworks\cite{19-23} have been reported. Immobilization of molecular catalysts onto porous materials combines advantages of homogeneous as well as heterogeneous catalysis, such as high conversion rates and good reusability\cite{24,25}. Most importantly, molecular catalysts can be made accessible for gas phase catalytic reactions using this approach. Porous silica is probably the most common support used for immobilization of molecular catalysts and surface organometallic chemistry; however, this inorganic support provides many, densely packed hydroxy functionalities, so that pre-treatments are essential to control the binding of a metal organic complex either on one, two or even more hydroxy groups. Indeed various analytical tools are needed to elucidate the binding state of organometallic complexes on silica supports\cite{24,25}.

Microporous polymer networks (MPNs) exhibit some intriguing properties such as the accessible high surface area, chemical robustness, and tunable functionality, which make these materials interesting for various applications and also for immobilization of molecular catalysts\cite{26}. Even though MPNs with various functional moieties in their backbone have been presented, some examples are also solely composed of carbon and hydrogen and show no extended \(\pi\)-conjugation, such as the highly porous PAF-1\cite{27} or PPN-6\cite{28}. If organometallic species could be grafted on such a MPN, this would ensure homogeneous distribution of a single-site catalyst over the entire surface area of a non-functional and inert organic polymer, thus a truly “innocent” support. Such kind of materials have been reported to be active in catalysis application in condensed phase\cite{29-49} but rarely in gas phase\cite{50}.

Herein, we present the immobilization of an organometallic molecular iridium pincer complex on a high-surface area microporous polymer network (Scheme 1) and its application in catalytic gas phase hydrogenation of ethene and propene. The novel MPN features an inert environment with isolated anchor points for the immobilization of the highly active metal-organic complex, ensuring the formation of a single-site catalyst.

In order to provide a reactive hydroxy functionality as anchor point while also following the tetraphenylethane structural motif of the highly porous PAF-1\cite{27}/PPN-6\cite{28} tris(4-bromophenyl)-methanol\cite{51} was synthesized and converted into 4-hydroxyphenyl-tris(4-bromophenyl)methane 1. To avoid possible interactions with the utilized metal species during polymerization, the hydroxy group was protected by methylation to yield 4-methoxyphenyl-tris(4-bromophenyl)methane 2 (Scheme 1; further details can be found in the supporting information). The structures of 1 and 2 were confirmed by single crystal X-ray diffraction analyses (SI Figure S1–S3). Since its first application in 2009\cite{52} the nickel-mediated Yamamoto polymerization has been a convenient method for the synthesis of microporous polymer networks. Following this methodology, 2 was successfully converted into MPN-OMe with a \(S_A\text{BET}\) of 1096 m\(^2\) g\(^{-1}\). The assumed chemical structure was confirmed by \(^{13}\)C CP/MAS-NMR spectroscopy (Figure 1 a). The signals of the quaternary methane carbon atom and of the methoxy group could be identified in the aliphatic region at 60 ppm and 50 ppm, respectively. For the aromatic carbon atoms several signals between 155 and 109 ppm were found, whereby the signal at 155 ppm can be most probably assigned to the \(C_{\text{aryl}}\text{-O}\). To

\[ \text{IrH}_2\text{-}(\text{POCOP}) \]
and immobilization of iridium pincer complex [IrH$_2$(POCOP)] onto MPN-OH and drying in vacuum yielded the immobilized iridium pincer complex. Its color turned from beige to orange (Figure 3b). Filtration confirmed by 13C CP/MAS-NMR spectroscopy (Figure 1).

Porosity was evaluated for MPN-O-[Ir] by low-pressure argon sorption studies and compared to MPN-Ome and MPN-OH. All samples showed high gas uptake at low pressures, which is characteristic for microporous materials (Figure 3a). Using the Brunauer–Emmett–Teller (BET) model, surface areas (S$_{BET}$) were determined to be 1096, 1087 and 451 m$^2$/g for MPN-Ome, MPN-OH and MPN-O-[Ir], respectively. The successful demethylation was confirmed by solid state NMR spectroscopy (Figure 1). In the 13C CP/MAS-NMR spectrum additional peaks in the aromatic region at 167, 164 and 101 ppm are observed due to the phosphinoxyphenyl ligand of the pincer complex. The signal at 24 ppm can be assigned to the tert-butyl methyl groups, and both signals at 39 and 35 ppm can be assigned to the quaternary tert-butyl carbon atoms. Due to non-identical chemical environments inside a solid, two signals instead of one are observed for the quaternary tert-butyl carbon atoms. The 31P MAS-NMR spectrum confirms the intact pincer ligand as its chemical shift of 169 ppm closely resembles the values reported in literature. Minute signals at 200 and 180 ppm can be ascribed to traces of uncomplexed [IrH$_2$(POCOP)] and [IrHCl(POCOP)] species. The signal at 64 ppm occurs most likely due to decomposed iodide catalyst and can be assumed to be di-tert-butyl-phosphine oxide.

The elemental composition of MPN-O-[Ir] was explored by X-ray photoelectron spectroscopy (XPS), revealing a 1:2 ratio of iridium to phosphorus which confirms again the immobilization of the intact iridium pincer complex. The high-resolution C 1s core-level spectrum of MPN-O-[Ir] gives two peaks at 284.8 and 286.1 eV, which are attributed to C–C and C–O species, respectively. Two peaks in the O 1s spectrum at 530.1 and 533.2 eV can be assigned to a metal oxide. The P 2p spectrum shows a doublet signal at 61.9 and 65.0 eV in the P 2p spectrum at 64 ppm occurs most likely due to decomposed iodide catalyst and can be assumed to be di-tert-butyl-phosphine oxide.

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Successful immobilization of the iridium pincer complex was confirmed by solid state NMR spectroscopy (Figure 1). In the 13C CP/MAS-NMR spectrum additional peaks in the aromatic region at 167, 164 and 101 ppm are observed due to the phosphinoxyphenyl ligand of the pincer complex. The signal at 24 ppm can be assigned to the tert-butyl methyl groups, and both signals at 39 and 35 ppm can be assigned to the quaternary tert-butyl carbon atoms. Due to non-identical chemical environments inside a solid, two signals instead of one are observed for the quaternary tert-butyl carbon atoms. The 31P MAS-NMR spectrum confirms the intact pincer ligand as its chemical shift of 169 ppm closely resembles the values reported in literature. Minute signals at 200 and 180 ppm can be ascribed to traces of uncomplexed [IrH$_2$(POCOP)] and [IrHCl(POCOP)] species. The signal at 64 ppm occurs most likely due to decomposed iodide catalyst and can be assumed to be di-tert-butyl-phosphine oxide.

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The tridentate iridium pincer complex [IrH$_2$(POCOP)] was synthesized according to literature. Then, a pentane solution of [IrH$_2$(POCOP)] was added to a suspension of MPN-OH in pentane at room temperature under inert conditions. While stirring overnight the polymer swelled and was synthesized according to literature. Then, a pentane solution of [IrH$_2$(POCOP)] was added to a suspension of MPN-OH and drying in vacuum yielded the immobilized iridium pincer complex MPN-O-[Ir] (Scheme 1).

To explore the binding geometry of the immobilized pincer complex a model compound was synthesized and analyzed by single crystal x-ray diffraction analysis (Figure S4).
respectively. After immobilization of the iridium catalyst, the SA \textsubscript{BET} decreased from 1087 to 451 m\textsuperscript{2} g\textsuperscript{-1}, which is almost the expected SA \textsubscript{BET} due to the large increase in molecular weight by a factor of 2.8, assuming full conversion of hydroxy groups. The pore size distributions were calculated from quenched solid density functional theory (QSDFT) and resulted in 0.69 nm for MPN-OMe and MPN-OH and 0.56 nm for MPN-O-[Ir] (Figure S8).

The immobilized iridium pincer complex was investigated in the catalytic hydrogenation of ethene and propene. There have been reports wherein different complexes immobilized on various supports were studied for gas phase hydrogenation of alkenes (Table S1).

The permanent porosity of MPNs is a feature, which is not necessarily needed in solution-based reactions as any non-porous but swellable crosslinked polymer could be equally efficient. Indeed, stable permanent surface areas and porosities of MPNs could be much better exploited and will yield a significant benefit when applied in gas phase catalytic reactions.

In this case, the catalytic hydrogenation of alkene and formation of alkane was monitored by \textsuperscript{1}H NMR gas phase spectroscopy. MPN-O-[Ir] was transferred to an intermediate pressure NMR tube (2.5 mL) which was subsequently evacuated, followed by addition of a 1:1 mixture of alkene and hydrogen (2 bar). After the addition the NMR tube was immediately inserted into the NMR spectrometer and \textsuperscript{1}H gas phase NMR spectra were collected. The obtained signals for alkene and alkane were normalized, integrated, converted into mole fraction and plotted as a function of time (Figure 4a and b). The hydrogenation reactions of ethene and propene were accomplished after 2 h almost quantitatively. Comparing the conversions of the hydrogenation of ethene and propene (Figure 4c and Table S2) it is noticeable that the formation of ethane is slightly faster. This can be explained by the higher reactivity of ethene in comparison to propene but may additionally result from the smaller kinetic diameter of ethene and therefore easier access and diffusion through the micropores of the catalytic system.

Owing to the rapidity of the reaction in the NMR tube, which causes difficulties in following the reaction, the hydrogenation of ethene was further conducted on a larger scale to evaluate kinetic data in a more reliable fashion as this allows reducing the ratio of catalyst per substrates (Table 1). The reaction follows a seemingly linear pathway for the first two...
hours and is complete after 4 hours at room temperature (Figure 4d).

After 30 min the conversion to ethane was 16% which equals to a TON of 56 and a TOF of 1.9 min⁻¹. In comparison to a pincer complex supported on mesoporous silica (SBA-15)[13] the MPN supported catalyst shows a much higher activity per catalyst mass but a lower one when compared to the number of active, that is, Ir sites (see Table S1). One reason could be the diffusion limitation due to the smaller pores. Apart from that it is conceivable that some active sites inside the material are not accessible. It should be noted that a possible heating effect of the catalyst due to the exothermic hydrogenation reaction could not be detected on the polymeric powder catalyst, but has to be also considered when discussing the reaction kinetics.

The catalyst MPN-O-[Ir] could be reused for at least four times after evacuation and removal of the product under vacuum for 15 min (Inset Figure 4d). All recycle runs where performed with a reaction time of 30 min as to reach not full conversion. Surprisingly, the conversion increased from the first to the third cycle from 16% to 31%. It cannot be excluded that some inactive iridium sites are formed during catalyst preparation, for example, by contact with some traces of air or moisture. During the hydrogenation, that is, under H₂ atmosphere, such inactive sites are probably regenerated to the iridium-hydrido-complex, which is described as the actual catalyst for the hydrogenation of ethene.[13] This will lead to an increase in activity when the catalyst is recycled. After the complex is formed it remains as such in the subsequent runs and is immediately active. The decrease of the conversion in the fourth cycle is within margin of error of the measurement.

FT IR measurements before and after catalysis furthermore confirmed the presence of the expected carbon, oxygen, phosphorus and iridium species. A homogeneous distribution of iridium and phosphorus was confirmed by scanning electron microscopy. After immobilization of the molecular catalyst the SA BET of the microporous network decreased from 1087 to 451 m² g⁻¹ due to the increased specific weight but without loss of the microporous characteristics. The catalytic performance was demonstrated in the room temperature hydrogenation of ethene and propene, which was monitored by ¹H NMR gas phase spectroscopy. Near-quantitative conversions were observed after 2 h at room temperature (94% for ethene and 92% for propene after 0.5 h) and the recyclability of the catalyst was demonstrated. We believe that this new class of support material ensures the formation of single-site catalytically active species inside a chemically robust and inert polymer, offering ample opportunity for the field of surface organometallic chemistry.

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Conflict of interest

The authors declare no conflict of interest.

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Table 1: Catalytic hydrogenation of ethene at room temperature,[a]

| Entry | t [h] | Cycle | Conversion [%] | TON | TOF [min⁻¹] |
|-------|------|-------|----------------|-----|-------------|
| 1     | 0.1  | 3     | 11             | 1.9 |             |
| 2     | 0.5  | I     | 56             | 1.9 |             |
| 3     | 0.5  | II    | 84             | 2.8 |             |
| 4     | 0.5  | III   | 111            | 3.7 |             |
| 5     | 0.5  | IV    | 105            | 3.5 |             |
| 6     | 1    | –     | 135            | 2.3 |             |
| 7     | 2    | –     | 290            | 2.4 |             |
| 8     | 4    | –     | 360            | –   |             |

[a] Reaction conditions: 8 mg catalyst MPN-O-[Ir], no solvent, room temperature, 1:1 ratio of ethene to hydrogen, initial total pressure of 2 bar, reactor volume 55 mL. The conversion was determined by integration of the ¹H NMR gas phase spectra.
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