Photo-tailored heterocrystalline covalent organic framework membranes for organics separation

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Organics separation for purifying and recycling environment-detrimental solvents is essential to sustainable chemical industries. Covalent organic framework (COF) membranes hold great promise in affording precise and fast organics separation. Nonetheless, how to well coordinate facile processing—highly crystalline structure—high separation performance remains a critical issue and a grand challenge. Herein, we propose a concept of heterocrystalline membrane which comprises high-crystalline regions and low-crystalline regions. The heterocrystalline COF membranes are fabricated by a two-step procedure, i.e., dark reaction for the construction of high-crystalline regions followed by photo reaction for the construction of low-crystalline regions, thus linking the high-crystalline regions tightly and flexibly, blocking the defect in high-crystalline regions. Accordingly, the COF membrane exhibits sharp molecular sieving properties with unprecedented organic solvent permeance up to 44-times higher than the state-of-the-art membranes.
Global demand for organic solvents is expected to surpass 20 million tons by 2023 for use in chemical, fragrance, and pharmaceutical processes due to the solubility and product selectivity requirements. These solvents must be separated from intermediate chemicals or products for recycling and minimizing emission\(^1\)\(^-\)\(^4\). Pressure-driven membrane separation operating at mild conditions without phase change holds great promise due to its much lower energy consumption and organic vapor emission compared with the commonly used thermal-based distillation technology\(^5\)\(^-\)\(^8\). However, conventional membranes which are fabricated from network polymers are often difficult to simultaneously achieve high solvent resistance and fast molecular sieving performance\(^9\)\(^,\)\(^10\), necessitating new-generation membrane materials with highly robust, ordered, and porous structures.

Two-dimensional covalent organic framework (COF) is an emerging crystalline framework material comprising rigid molecular building blocks connected by robust in-plane covalent bonds and out-of-plane \(\pi-\pi\) interactions, exhibiting excellent solvent-resistant properties\(^11\)\(^-\)\(^14\). Moreover, the COF material features an ordered porous structure that has up to 100 times higher surface area than most network polymers\(^15\). Theoretically, high-crystalline COF membranes (COMs) formed totally by rigid crystallites can harvest high solute selectivity and possible high solvent permeability, however, the defect-free membranes are quite difficult to fabricate\(^16\)\(^-\)\(^18\). Low crystalline COMs are much easier to fabricate, but often accompany with much less ordered structure and a dramatic sacrifice in solute selectivity as well as possible solvent permeability\(^19\)\(^,\)\(^20\). It proves a grand challenge to acquire good membrane processibility and sufficiently high crystallinity through adjusting the crystallinity of the whole COM. In this case, the COM can be regarded as the homocrystalline COM.

Herein, we propose a concept of heterocrystalline membrane comprised of both high-crystalline regions and low-crystalline regions. The heterocrystalline COM is prepared through a two-step procedure based on sequential Schiff-base reactions where the bond linkage can tautomerize under photo irradiation. The first step is dark reaction to generate the high-crystalline COM. The second step is photo reaction to generate low-crystalline regions in the intercrystalline defect of the COM, thus linking the high-crystalline regions tightly and flexibly, blocking the defect in high-crystalline regions. Photochemistry, which can interfere in proton transfer, is a widely-used and green way to modulate chemical reactions\(^21\). It has been demonstrated that photo-induced excited-state intramolecular proton transfer (ESIPT) can enable enol-imine to keto-enamine tautomerization\(^22\)\(^,\)\(^23\), while the enol-imine linkage is the key for the commonly used Schiff-base COF to form high-crystalline structure\(^24\). This photo-induced tautomerization provides the chemical basis to control the reactive-crystallization procedure of COF by photo irradiation. In this study, we present a photo-tailoring strategy to prepare the heterocrystalline COM. Under dark settings, the reversible enol-imine linkage can break up and reform, thus correcting the initial mismatched amorphous structure, allowing the formation of a high-crystalline COM. Subsequently, photo irradiation is introduced and the phototautomerization of
enol-imine linkage inhibits the "error-correcting" process, allowing the formation of low-crystalline regions in the intercrystalline defects of the COM (Fig. 1). By tuning the photo reaction time, the low-crystalline regions can tightly and flexibly link the high-crystalline regions to obtain the defect-free COM. Meanwhile, the well-preserved high-crystalline regions with ordered porous structures would enable precise and fast organics separation. The resulting COM displayed sharp molecular sieving properties, as manifested by the unprecedented organic solvents permeance up to 44-times higher than the state-of-the-art membranes.

Fig. 1 | Schematic preparation of heterocrystalline COM. Preparation of heterocrystalline COM by subsequent dark reaction and photo reaction using interfacial polymerization, where the top light-blue layer is the aqueous phase and the bottom navy-blue layer is the organic phase. 1,3,5-triformylphloroglucinol (Tp) and 2,2'-bipyridine-5,5'-diamine (Bpy) are used as aldehyde monomer and amino monomer, respectively, to prepare Schiff-base Tp-Bpy COM. The inset digital photograph is the photo-tailored heterocrystalline COM deposited on non-woven fabrics with the size of approximately 15 cm×8 cm (Supplementary Fig. 1).

Photo-tailored reactive-crystallization of Schiff-base COM

The synthetic routes of COMs by either dark reaction or photo reaction were illustrated in Fig. 2a. Initially, the reactive monomers would polymerize into an amorphous network via enol-imine linkage. During dark reaction, the reversible enol-imine linkage breaks and reforms slowly, thus converting the initial amorphous network into the thermodynamically stable crystalline framework as a result of the "error-correcting" process. Then, the enol-imine linkage tautomerizes irreversibly to stable keto-enamine form. The Fourier transform infrared (FTIR) spectrum confirms the formation of the keto-enamine-linked COM by dark reaction (DCOM), which is verified by the C=C stretching band at ca. 1566 cm⁻¹ (Supplementary Fig. 2). X-ray diffraction (XRD) pattern suggests the high crystallinity of the DCOM, which shows an intense and sharp peak at ~3.5° corresponding to the reflection from the 100 crystal plane (Fig. 2b).
Fig. 2 | Photo-tailored reactive-crystallization of Schiff-base COM. a, Synthetic route of COMs by either dark reaction or photo reaction. b, XRD patterns of the DCOM and PCOMs formed under varied irradiation intensity. c, Schematic illustration of the ESIPT process of enol-imine linkage. d, Steady-state photoluminescence emission spectra of the initial amorphous material dispersed in either aqueous phase (solid lines) or organic phase (dashed lines). These samples were excited at 300 nm.

The light source of photo reaction is supplied by a xenon lamp (λ = 200–400 nm) with an irradiation intensity from 1.5 mW cm$^{-2}$ to 9.0 mW cm$^{-2}$. During photo reaction, the initially formed reversible enol-imine linkage tautomerizes rapidly into keto-enamine form due to the photo-induced ESIPT (Fig.2a, c, $k_{\text{ESIPT}} > 10^{12}$ s$^{-1}$)$^{22,23}$, resulting in a decrease of reversible enol-imine linkage and thus inhibiting the "error-correcting" process. This photo-induced tautomerization from enol-imine to keto-enamine is confirmed by the steady-state photoluminescence emission spectrum. Fig. 2c shows the fluorescence properties of the initial amorphous material dispersed in either the aqueous phase or the organic phase of interfacial polymerization. A dual fluorescence emission phenomenon is observed, with the wavelength emission at 400-450 nm representing the enol-imine form (normal emission) and the wavelength emission at 580-630 nm reflecting the keto-enamine tautomeric form (ESIPT emission)$^{29,30}$, confirming
photo-induced enol-imine to keto-enamine tautomerization. The COMs formed by photo reaction (PCOMs) display a substantially weaker and wider (100) diffraction peak than DCOM (Fig. 2b), even under low irradiation intensity (1.5 mW cm$^{-2}$), indicating the pronounced influence of photo irradiation on the COM crystallization. The crystallinity of the PCOMs decreases with the increase of the irradiation intensity (Fig. 2b), offering a facile approach to control the crystalline structure. Besides, the FTIR spectra demonstrate that the C=C stretching band of PCOMs was more intense than that of DCOM (Supplementary Fig. 2), indicating that the enol-imine linkage within PCOMs is more sensitive to tautomerization due to the low energy barrier of phototautomerization$^{31}$. These findings demonstrate a simple and effective strategy for tailoring the crystalline structure of Schiff-base COM, offering the rich possibility to tailor heterocrystalline COM by controlling the dark and photo reactions during membrane formation.

**Preparation and characterizations of DPCOMs**

The morphologies of DCOM formed under dark condition and PCOMs formed under varied irradiation intensity are systematically investigated. For DCOM, fibre-crystallite assembled morphology with tens-of-nanometre-sized intercrystalline defects can be observed (Fig. 3a, Supplementary Fig. 3), revealing poor processibility of high-crystalline COM. In contrast, the morphology of PCOMs changes into a flexible polymer-like structure with inappreciable intercrystalline defects by increasing the irradiation intensity from 1.5 to 9.0 mW cm$^{-2}$ (Fig. 3a, Supplementary Fig. 4), manifesting the superior processability of low-crystalline COM formed under 9.0-mW cm$^{-2}$ irradiation intensity.

The heterocrystalline COM, denoted as DPCOM, was fabricated by dark reaction first in the same way as DCOM, followed by 9.0-mW cm$^{-2}$ photo irradiation (Fig. 1). After photo reaction, the successful incorporation of low-crystalline regions into DPCOM is revealed by FTIR analysis, where the C=C (1566 cm$^{-1}$) of keto-enamine linkage gradually increases with the increase of photo reaction time (Supplementary Fig. 5). Transmission electron microscope (TEM) analysis indicates that the low-crystalline regions grow in the edge of the high-crystalline regions bearing lattice diffraction pattern and the growth area is proportional to photo reaction time (Fig. 3b). After forming low-crystalline regions, the size and quantity of the intercrystalline defects within DPCOM observably decrease (Fig. 3a, Supplementary Fig. 3). Moreover, the thickness of the DPCOM does not increase (~55 nm, inset in Fig. 3a), suggesting that the low-crystalline regions grow in the intercrystalline defects instead of along the thickness of the membrane. This is ascribed to the inherent self-inhibition effect in the interfacial polymerization process, where the monomers dissolved separately in organic and aqueous phase prefer to infuse and polymerize in the defects of interfacial membrane$^{32}$. We also use atomic force microscope (AFM) tip to determine the local Young's modulus of
the individual regions of COMs (Fig. 3c). The DP\textsubscript{20}COM (3.2 GPa) exhibits much higher average modulus than that of PCOM (0.6 GPa) and DCOM (2.0 GPa) due to the rigid high-crystalline regions with large modulus and the decreased defect regions bearing tiny modulus. These results demonstrate that the intercrystalline defects of DP\textsubscript{20}COM are effectively sealed by the low-crystalline regions. Furthermore, our strategy can even seal the several-hundred-nanometre defects of COM (Supplementary Fig. 6).

**Fig. 3** | **Structure and morphology characterizations.** a, Top-view SEM images of COMs deposited on track-etched substrate membranes. The intercrystalline defects are marked by the white circle. The cross-sectional SEM images inset showing the thickness of COMs. Scale bar = 500 nm. b, TEM images of the COMs. Insets are high-magnification images where the high-crystalline regions show lattice diffraction patterns. Scale bar = 10 nm. c, Young's moduli of COMs tested using the peak force quantitative nano-mechanical property mapping method. d, e, XRD patterns (d) and N\textsubscript{2} adsorption isotherms (e) of COMs. The PCOM here is fabricated under 9.0-mW cm\textsuperscript{-2} irradiation intensity.
The photo irradiation would not affect the crystalline structure of high-crystalline regions, which can be proved by the almost unchanged full width at half maximum (FWHM) of the (100) diffraction peak of DPCOM (Fig. 3d). This high crystallinity endows DP_{2h}COM with a very porous structure, which shows a Brunauer–Emmett–Teller surface area ($S_{BET}$) of up to 1443 m² g⁻¹ (Fig. 3e). This value is slightly lower than that of DCOM due to the incorporation of low-crystalline regions but an order of magnitude higher than previously reported organics separation membranes (Supplementary Table 1). The above results prove that the as-prepared heterocrystalline COMs can simultaneously satisfy the requirements for both membrane processibility and sufficient high crystallinity.

**Organics separation performance of DPCOMs**

The organics separation performance of COMs was evaluated in terms of dye rejection and organic solvent permeance. The DCOM bearing an intrinsic pore of 1.6 nm displays poor rejection (45%) to Evans blue (EB) with a dimension of 1.2×3.1 nm due to the tens-of-nanometer intercrystalline defects (Fig. 4a). The rejection of DP_{2h}COM rises to 99%, as high as that of defect-free and dense PCOM prepared under 9.0-mW cm⁻² irradiation intensity (Fig. 4a, Supplementary Fig. 7), confirming that the generated low-crystalline regions seal the non-selective intercrystalline defects effectively. We further investigated the rejections of DP_{2h}COM to a series of dye solutes with various molecular weights (Supplementary Table 2). For all dyes, the adsorption on membranes is as low as 0.41 ug m⁻², which suggests that the rejection value is based on size exclusion rather than adsorption (Supplementary Fig. 8). As shown in Fig. 4b, the molecules with molecular weights >800 Da (RR 24 and EB) can be effectively rejected by DP_{2h}COM with rejections more than 90%, while molecules with molecular weights <600 Da (MO and P) can easily permeate through the membrane with rejections less than 10%. The D-value of molecular weight cutoff (MWCO, 800 Da) and molecular weight retention onset (MWRO, 600 Da) is only 200 Da. The rejection curve of DP_{2h}COM is much steeper than that of high-crystalline DCOM, low-crystalline PCOM, and other previously reported membranes attributing to its defect-free and crystalline ordered pore structure (Fig. 4c, Supplementary Table 3). Furthermore, a mixed dye separation experiment of MO (327 Da) and EB (961 Da) was conducted (Supplementary Fig. 9). The EB can be completely rejected by DP_{2h}COM, while the MO could pass through freely. This precise molecular sieving ability endows DP_{2h}COM with prospective potential for separating organic mixtures.
**Fig. 4 | Organics separation performance.** a, Pure ethanol permeance and EB rejection of COMs. b, Rejection versus molecular weight of dyes: MO (327 Da); P (453 Da); AB (616 Da); RR24 (788 Da) and EB (961 Da). The fitted sigmoidal model of the rejection curve is Doseresp. c, Comparison of the rejection curve of DP$_{2h}$COM with the reported state-of-the-art membranes. d, Permeance of pure organic solvents through the DP$_{2h}$COM as a function of their inverse viscosity. e, Variation of the ethanol flux of DP$_{2h}$COM under varying pressure. f, Ethanol permeance of DP$_{2h}$COM after solvent immersion. g, Comparison of the dye (700–900 Da) rejection and solvent permeance (ethanol or methanol) of DP$_{2h}$COM with the reported state-of-the-art membranes. The specific separation data of the reported membrane are listed in Supplementary Table 1, 3. The Error bars represent standard deviations from duplicate measurements of at least three independent samples. Dye concentration: 20 ppm for EB, 50 ppm for other dyes.

The ethanol permeance of DP$_{2h}$COM is as high as 81 L m$^{-2}$ h$^{-1}$ bar$^{-1}$, 26-times higher than that of PCOM with 3.6-times lower porosity, demonstrating the importance of porous structure in the organic molecules transport (Fig. 4a). The DP$_{2h}$COM exhibits superior organophilic behaviour (Supplementary Fig. 10), and then we further evaluated its permeation properties for different types of organic solvents including apolar (toluene), polar protic (methanol, isopropanol, butanol), and polar aprotic (acetonitrile, acetone, ethyl acetate, dimethylformamide, tetrahydrofuran) solvents (Fig. 4d). The solvent permeance of DP$_{2h}$COM is found to be linearly proportional to the inverse of solvent viscosity ($\eta^{-1}$). Acetonitrile, with a viscosity of $3.4 \times 10^{-4}$ Pa·s, gives the highest permeance of 316 L m$^{-2}$ h$^{-1}$ bar$^{-1}$
Methanol, the most used model solvent, with a smaller viscosity of $5.4 \times 10^{-4}$ Pa·s, gives the second-highest permeances of 264 L m$^{-2}$ h$^{-1}$ bar$^{-1}$. The viscous flow behavior of the solvent through DP$_{2h}$COM is ascribed from the solvent resistance and rigid pore structure$^{34,35}$. Moreover, due to this structure, the solvent flux of DP$_{2h}$COM increases linearly with an increase in the transmembrane pressure, revealing superior compaction resistance of DP$_{2h}$COM (Fig. 4e). And the permeance keeps constant even after 7 days solvent immersion (Fig. 4f, Supplementary Fig. 11).

The solute rejection and solvent permeance are compared with reported state-of-the-art organics separation membranes. As demonstrated in Fig. 4g, the membranes prepared by emerging COFs (marked as blue pentagon) present preponderant separation performance but face a trade-off between permeance and rejection. Our phototailoring strategy can create heterocrystalline COMs with both high-crystalline regions and low-crystalline regions, allowing for fast and precise organics separation by eliminating non-selective intercrystalline defects. The as-prepared heterocrystalline COM exhibits stable and up to 44-times higher solvent permeance than previously reported COMs with similar rejection. We further evaluate the separation performance of DP$_{2h}$COM in cross-flow mode to simulate realistic application circumstances. Our DP$_{2h}$COM can withstand continuous cross-flow shear forces and exhibit stable separation performance over 48-hour operation (Supplementary Fig. 12), indicating great potential for large-scale organic molecular separation process.

**Discussion**

In summary, we propose a concept of heterocrystalline membrane which comprises high-crystalline regions and low-crystalline regions, which delicately solves the dilemma between high crystallinity and easy fabrication of defect-free membrane. The preparation of heterocrystalline COM is *via a two-step procedure, where a high-crystalline COF membrane forms in the first dark reaction step and the low-crystalline regions form in the second photo reaction step. By tuning the photo reaction time, the low-crystalline regions can tightly and flexibly link the high-crystalline regions to acquire the defect-free COMs with ultrahigh porosity. Accordingly, the resulting COM displays sharp molecular sieving properties with remarkable organic solvents permeance up to 44-times higher than the state-of-the-art membranes. We envisage that our strategy of using photo reaction to tailor the crystallinity of COF membranes may enlighten the manufacture of other crystalline polymer materials, and particularly the concept of heterocrystalline membrane will greatly enrich the design of heterostructure membranes for organics separations and other precise separations.
Data availability

Source data are provided with this paper.

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Author contributions

H.W., Z.J., and J.Y. conceived the idea and designed the research. J.Y. and X.Y. carried out the experiment. J.S. and Z.X. performed the permeation measurement. R.L. and Y.L. provided constructive suggestions for results and discussion. R.Z., N.K., and M.L. helped to revise the paper. All authors participated in the discussion. H.W., Z.J., J.Y., and X.Y. co-wrote the paper.

Competing interests

The authors declare no competing interests.
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