Manipulation of pH Shift to Enhance the Growth and Antibiotic Activity of Xenorhabdus nematophila

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Received 2 September 2010; Accepted 19 March 2011

Academic Editor: Ali Khraibi

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To evaluate the effects of pH control strategy on cell growth and the production of antibiotic (cyclo(2-Me-BABA-Gly)) by Xenorhabdus nematophila and enhance the antibiotic activity. The effects of uncontrolled- (different initial pH) and controlled-pH (different constant pH and pH-shift) operations on cell growth and antibiotic activity of X. nematophila YL001 were examined. Experiments showed that the optimal initial pH for cell growth and antibiotic production of X. nematophila YL001 occurred at 7.0. Under different constant pH, a pH level of 7.5 was found to be optimal for biomass and antibiotic activity at 23.71 g/L and 100.0 U/mL, respectively. Based on the kinetic information relating to the different constant pH effects on the fermentation of X. nematophila YL001, a two-stage pH control strategy in which pH 6.5 was maintained for the first 24 h, and then switched to 7.5 after 24 h, was established to improve biomass production and antibiotic activity. By applying this pH-shift strategy, the maximal antibiotic activity and productivity were significantly improved and reaching 185.0 U/mL and 4.41 U/mL/h, respectively, compared to values obtained from constant pH operation (100.0 U/mL and 1.39 U/mL/h).

1. Introduction

X. nematophila is a Gram-negative bacterium, belonging to the family Enterobacteriaceae which is symbiotically associated with the entomopathogenic nematode in the genus Steinernema (Steinernematidae) [1]. The production of metabolites with antibiotic properties is a characteristic common to the bacteria. X. nematophila has been known to produce xenocoumacins (benzopyranone derivatives) [2], nematophin (indoles derivatives) [3], benzylacetone (monoterpenoid) [4], and xenematide (peptides) [5]. These metabolites not only have diverse chemical structures, but also have a wide range of bioactivities of medicinal and agricultural interest, such as antibiotic, antymycotic, insecticidal, nematicidal, antiulcer, antineoplastic, and antiviral properties [6]. Xenocoumacins are highly active against Gram-positive bacteria and also exhibit antymycotic activity against species of Cryptococcus, Aspergillus, Trichophyton, and Candida [2]. Nematophin is also active against Gram-positive bacteria and a plant-pathogenic fungus, Botrytis cinerea.

In comparison, benzylacetone and xenematide are active against Gram-negative bacteria. These naturally occurring antibiotics provide useful leads in the research and development of drugs and agrochemicals.

We isolated a new strain of X. nematophila YL001 from the symbiotic nematode, Steinernema sp. YL001, collected in China, and the strain has unique genetic (e.g., 16S ribosomal DNA sequence) and biochemical characteristics compared to other isolates of this taxon [7, 8]. In vitro and In vivo, the bacterium showed high antibiotic activity against some bacteria and fungi such as Phytophthora capsici, Blumeria graminis and Pseudoperonospora cubensis, which have not been thoroughly evaluated as antifungal targets of X. nematophila [9]. The study showed for the first time the potential of these products to control diseases of living plants although such crude mixtures were unlikely to be registered for use in commercial agriculture. Moreover, a new antibiotic, cyclo(2-Me-BABA-Gly), was isolated from the strain [10]. The results suggest that X. nematophila YL001 is
a unique, potential resource of new agrochemicals and antimicrobial compounds.

Antibiotic types and concentration produced by X. nematophila depend on the strains of bacteria and their culture conditions [6]. In general, for metabolite biosynthesis, the optimal conditions used for cell growth and metabolites biosynthesis may be quite different. The cell growth and product accumulation vary with medium composition and process parameters, including pH. In order to obtain high biomass and metabolites, it is important to optimize the conditions for cell growth and metabolite biosynthesis during X. nematophila fermentation. Well-directed process parameters shift representing a valuable control strategy will be beneficial to the cell growth and metabolite biosynthesis. pH-shift operation has been proven to be an effectual strategy for the production of bioactive metabolites in other microorganism [11–16].

In previous studies, it was found that initial pH played an important role in the antibiotic production by X. nematophila [17–19]. However, until now, there is no report about the effect of pH control strategy on cell growth and antibiotic activity of this bacterium. Therefore, it would be interesting to investigate whether the pH control strategy will lead to a quantum improvement in its biomass and antibiotic activity. The objective of this work was to evaluate the effects of pH control strategy on cell growth and antibiotic activity in batch fermentation by X. nematophila YL001. An optimum pH control strategy was proposed to optimize its cell growth and metabolites biosynthesis, and the fermentation efficiency was greatly improved. This work is expected to help develop the large-scale fermentation of X. nematophila for the simultaneous production of biomass and antibiotics. The outcome of this work is expected to help in the development of other strains for useful metabolite production.

2. Materials and Methods

2.1. Microorganism. X. nematophila YL001 was isolated from its nematode symbiont, Steinernema sp. YL001 was obtained from the soil of Yangling, China. Phase I variant of the bacteria was used throughout the study.

X. nematophila YL001 was maintained on nutrient agar (NA) slants and subcultured monthly. NBTA medium, NA supplemented with triphenyltetrazolium chloride 0.040 g/L and bromothymol blue 0.025 g/L, was used to test the phase variant of the bacteria. Phase I is distinguished from phase II by its adsorption of bromothymol blue to produce a red core colony overlaid by dark blue and surrounded by a clear zone after 2–3 days of incubation in darkness at 28°C.

2.2. Inoculum Preparation. A loopful of the phase I of X. nematophila YL001 growing on an NBTA plate was inoculated into a 250 mL flask containing 100 mL fresh NB (NA without agar) medium, which was adjusted to a final pH of 7.20 and then cultured in darkness at 28°C on an Eberbach rotary shaker at 150 rpm for 16–24 h, during which time the optical density (600 nm) was approximately between 1.50 and 2.00.

2.3. Fermentation Process in Shake Flask. The effect of initial pH on cell growth and antibiotic activity of the strain was studied using shake flask cultures at different initial pH values. 250 mL Erlenmeyer flask contained 50 mL medium consisting of the following components (g/L): glucose 6.13, peptone 21.29, MgSO4·7H2O 1.50, (NH4)2SO4 2.46, KH2PO4 0.86, K2HPO4 1.11, and Na2SO4 1.72. The medium pH was adjusted to 4.5, 6.5, 7.5, and 9.5 by adding 1 mol/L NaOH or 1 mol/L HCl. Ten percent (v/v) of the seed culture was used to inoculate the flasks. The culture was incubated on a rotary shaker at 28°C and 150 rpm for 72 h. Three batches were repeated for each experiment.

2.4. Batch Fermentation Process in 5-L Laboratory-Scale Fermenter. The effect of pH on the strain culture was also studied by batch fermentation in a 5-L bioreactor (Eastbio, China) with a working volume of 3.5 L. The fermenter was equipped with one six-blade disk turbine impeller, the probes of pH (Mettler-Toledo GmbH, Switzerland), DO (Mettler-Toledo GmbH, Switzerland), temperature, and foam. Temperature, pH, dissolved oxygen, and agitation speed were measured online. The medium, inoculum ratio and temperature used in this study were the same as that of the shake flask culture. The other main operation conditions were aeration ratio of 2.5 L/min and agitation speed of 300 rpm. A pH profile was adjusted to a set pH with 2.0 mol/L NaOH and 2.0 mol/L HCl. Temperature levels were maintained automatically. The fermenters were incubated according to the culture condition for 72 h. Four cultures were carried out simultaneously in the fermenter with homogeneous cell source under well-controlled process conditions but at different test culture conditions.

2.4.1. Different Constant pH Culture. The significance of different constant pH on X. nematophila YL001 growth and metabolites accumulation was studied by setting culture pH at 4.5, 6.5, 7.5, and 9.5 during the entire fermentation process in the fermenter. For comparison, the control experiment was initially run at a pH of 7.0, with no further to adjustment to pH (i.e., at an initial pH of 7.0).

2.4.2. pH-Shift Culture. Based on the impact of culture pH, a pH-shift culture was proposed by combining the first stage at a pH of 6.5 with the following culture at pH 7.5 (i.e., the second stage). The control experiment was conducted without the pH control in the second-stage culture for comparison. The impact of shift time between the cell growth phase and antibiotic accumulation phase was investigated by setting the shift time on 12, 24, 36, and 48 h. The other culture conditions were the same as in the experiments above.

2.5. Analytical Methods

2.5.1. Assay of Antibiotic Activity. The antibiotics were extracted as Li [10]. X. nematophila YL001 were cultured
as described above. Samples of ca. 30 mL were withdrawn each 6 h approximately. An amount of 20 mL aliquots of the fermentation broth were centrifuged (RCF 22400 g, 20 min, 4°C, Himac CR 22G) to separate the bacterial cells from the supernatant. The supernatants (pH 8-9), containing the proteinaceous component, were subjected to ammonium sulphate precipitation to remove the protein by filtration. The filtrate was then placed on the top of a column which had been filled with activated D101 macroporous adsorption resin (Shanghai Hualing Resin Co., Ltd, China). After washing the column with distilled water, the column was eluted with methanol. The extract was lyophilized and then redissolved in H2O (20 mL) and bioassayed by agar diffusion plate assay with Bacillus subtilis [20]. Briefly, 1 mL of the subculture containing 10^7–10^8 cells of B. subtilis was applied to NA plate. After 2 h incubation at 28°C, 6-mm disc filters (Whatman 3-mm paper; Whatman, Clifton, NJ) treated with the extracts (50 μL) were put on the NA plate and incubated at 28°C for 48 h to determine the relationship between the size of the zones of inhibited bacterial growth and the concentration of the antibiotic. Zones of inhibition were measured from the edge of antibiotic disk to the margin of the zone of inhibition. Antibiotic activity was expressed as units of activity per milliliter (supernatants) of the cultures, where 1 U was defined as a 1.0 mm annular clearing around the antibiotic disk.

To confirm the assumption that changes in the size of the zones of inhibition (expressed as units of activity per milliliter the supernatants of culture) represented changes in antibiotic concentrations, the extracted antibiotics were diluted with water or concentrated by lyophilization and resuspension in fixed volumes of distilled water. The antibiotic levels, based upon dilution or concentration of the antibiotic extract, ranged from 1/10 to twice the concentration found in the culture. The relationship of the log_{10} transformed concentration of the antibiotic relative to the level in the unmodified extract (20 mL) (which was assigned a value of 1.00) (antibiotic levels of 0.1, 0.5, 1.0, 1.5, and 2.0 [log transformations of -1, -0.3, 0.00, 0.18 and 0.30, resp.]) to the diameter of the zone of inhibition (9.5, 13.5, 16.7, 19.3, and 21.5 mm) revealed a linear correlation (r = 0.972; P > .05). Similarly, log_{10} transformed concentrations of the antibiotic (cyco(2-Me-BABA-Gly)) (antibiotic concentrations of 5.0, 10.0, 15.0, 20.0, and 25.0 μg/mL [log transformed concentrations of 0.699, 1.00, 1.177, 1.301 and 1.398, resp.]) produced inhibition zones (23.0, 25.0, 27.0, 29.0, and 29.5 mm) that were linearly correlated (r = 0.987; P > .05). Thus, both procedures validated the use of the size of the zone of inhibition as an indicator of antibiotic concentration. Maxwell et al. [20] confirmed the assumption that the changes in the size of the zones of inhibition (expressed as units of activity per gram of insect tissue) represented changes in antibiotic concentration. The antibiotics were extracted from insect larvae killed by X. nematophila by homogenizing the insects in distilled water. The assumption has been used successfully to measure the antibiotic activity of X. nematophila YL001 [19, 21]. Therefore, the size of the zones of inhibition served as a measure of antibiotic titer of X. nematophila YL001.

2.5.2. Measurement of Cell Growth. Cell growth was measured by optical density of the culture at 600 nm, and biomass concentrations (dry cell weight: g/L) were determined using a calibration curve. The calibration curve was calculated using dilutions of a biomass suspension with known optical density. A fixed volume of the dilutions was centrifuged at 10,000 rpm for 20 min (Himac CR 22G, Japan). The supernatant was discarded, and the cell pellets were dried at 110°C to constant weight. All the cell pellets were weighed after drying. Thus, a relationship between biomass concentration (g/L) and optical density were determined.

2.5.3. Measurement of Glucose Concentration. The glucose concentration was measured by the 3, 5-dinitrosalicylic acid spectrometric method [22].

3. Results

3.1. Effects of Initial pH on X. nematophila YL001 Fermentation in Shaking Flasks. Results of the flasks experiments after 72 h of fermentation with various initial pH ranging from 4.0 to 10.0 are shown in Figure 1. It is clear that pH plays an important role in the process of X. nematophila YL001 fermentation. Cell concentration and antibiotic activity profiles had a similar trend in response to initial pH. With the increase in initial pH, cell concentration and antibiotic activity increased, and both had a maximum when the initial pH was 7.0; thereafter, the cell density and antibiotic activity decreased modestly. The maximum DCW and antibiotic activity were 15.68 g/L and 80 U/mL, respectively. The influence of pH on cell growth was not significant as compared to that of antibiotic production within the range of 5.5–8.5. In spite of the uncontrolled-pH nature of flask cultures, these results indicate that neither the higher pH nor lower pH were beneficial to cell growth and antibiotic production. Similar results appeared in the previous work [16, 17], in which it was reported that the antibiotic production by X. nematophila BJ and Xenorhabdus sp. D43 were affected by the initial pH within the range of 4.5–8.5 and optimal initial pH for cell growth and antibiotic production occurred at 6.0–8.0. However, Wang et al. [19, 21] reported that the optimal initial pH for cell growth and antibiotic production of X. nematophila YL001 occurred at 7.64. Nevertheless, with the uncontrolled system, the flask experiment of different initial pH values might provide the preliminary information of the pH effects on growth and antibiotic production of X. nematophila. The above results showed that it was necessary to investigate the effects of pH on antibiotic production and cell growth in batch fermentation.

3.2. Kinetics of Batch Fermentation of X. nematophila YL001 at Initial pH 7.0. Based on the results of the flask experiments, the kinetics of batch fermentation of X. nematophila YL001 in 5-L laboratory-scale fermenter at initial pH 7.0, agitation speed of 300 rpm, aeration ratio of 2.5 L/min, and fermentation temperature of 28°C were studied. Time-course data on DCW, antibiotic activity, glucose concentration, and
pH are shown in Figure 2. It was found that cell growth showed a distinct exponential phase and a stationary phase; antibiotics biosynthesis occurred throughout the culture and continued even when all the residual sugars were consumed. While culture pH was uncontrolled, it fell gradually from 7.0 to 5.9 in the early stage of fermentation and then increased gradually to around 9.75 at the end of culture. As with X. nematophila YL001 culture, the culture broth pH of Xenorhabdus sp. RIO decreased during the first few hours of growth and then increased as the bacteria approached and reached stationary phase [23]. This pH variation may be due to the relatively high glucose consumption at early stage, which might result in production of certain organic acid(s) and would keep the medium pH at a low value. The pH increase may be related with ammonia production, a common antibacterial metabolite that is known to be produced by Xenorhabdus sp. in TSB [24]. It seems that to growth and antibiotic activity of X. nematophila YL001, it is important to determine the role of pH at different phase of cell growth and antibiotic production.

3.3. Effect of pH on the Cell Growth of pH Controlled Fermentation. Among the controlled-pH operations, cell formation changed considerably with the pH operation applied (Figure 3(c)). The absence of a noticeable lag phase at pH 6.5 was characterized by a rapid decrease in dissolved oxygen (Figure 4). At pH 4.5, 7.5, and 9.5, a lag phase of 18 h was observed during fermentation. The result may be related to the initial pH; the optimal initial pH for cell growth was 7.0 (Figure 1). During 0–30 h of the bioprocesses, the DCW was noticeably higher at pH 6.5 than that at all other pH values assayed, after 42 h, the DCW were higher at pH 7.5 than that at all other pH values. The maximum DCW of each controlled pH showed an optimal value of 23.71 g/L at pH 7.5, and decreased by 45%, 12%, and 81% at pH 4.5, 6.5, and 9.5, respectively. The optimal cell yield on glucose (Y_{X/S}) was 2.50 g/g at pH 6.5, which was higher than that at all other pH values. However, the maximum cell productivity (P_{X}) occurred at pH 7.5 were 0.33 g/L/h. It is obvious that higher or lower culture pH would inhibit cell formation. Consistent with the decreasing cell growth, the consumption of glucose declined. Especially at pH 9.5, glucose uptake was much slower (Figures 3(a) and 3(b)). These results indicate that shifting of pH levels greatly affected the cell growth. The optimal pH control strategy for maximal cell growth seemed to be pH 6.5 in the early stage of fermentation and pH 7.5 in the later stage of fermentation.

The specific cell growth rate (μ) was determined from the slope of the semilogarithmic plot of DCW versus fermentation time. In other words, it was obtained from the following equation:

$$\mu = \frac{1}{x} \frac{dx}{dt} = \frac{1}{x_{\text{lim}} - x} \frac{\Delta x}{\Delta t}.$$  

We interpose normally on the line of cell growth (Figure 3(c)) and compute the DCW at definite time (Δt = 0.1 h) with GrafTool Version 07.09.97 (LHarc-Archiv), then μ at definite time was obtained through computing DCW with Microsoft Excel. Time courses of the specific cell growth rate (μ) at different pH are shown in Figure 3(d). As shown in Figure 3(d), the μ_{max} at different pH showed that the optimum pH for cell growth was 6.5 and μ_{max} reached 0.092 h^{-1}, but the fastest decreasing rate was observed at this pH operation. Although μ_{max} was correspondingly low at pH 7.5 compared to that at pH 6.5, the decreasing rate of μ was small, and μ reached highest after 16 h. So, it is clear that at the early phase of fermentation, pH should be controlled at 6.5 in order to shorten the lag phase of cell growth, and thus the total fermentation time, and to maximize the specific cell growth rate.

3.4. Effect of pH on Antibiotic Activity in pH Controlled Fermentation Bioprocess. The effect of controlled pH on the antibiotic activity of X. nematophila YL001 is shown in Figure 3(e). At pH 6.5 and 7.5, the antibiotic activity was higher than that at pH 4.5 and 9.5. During 0–30 h of the bioprocesses, the antibiotic activity was higher at pH 6.5 than at pH 7.5; after 30 h, the antibiotic activity was not significantly different at pH 6.5 and 7.5. The highest antibiotic activity (100 U/mL) was obtained at pH 7.5, where the highest cell concentration was obtained. On the other hand, at the end of the bioprocesses, the lowest antibiotic
activity (27.5 U/mL) was obtained at pH 9.5, where the least amount of cell was generated. This result in turn indicates that, antibiotic production could be enhanced by increasing the concentration of antibiotic producing cells, probably either by making use of a complex production medium, or developing a substrate feeding strategy, or a combination of both. The maximum antibiotic activity ($P_{\text{max}}$) of each pH controlled showed an optimal value of 100.0 U/mL at pH

Figure 3: Time profiles of glucose (a), $q_s$ specific glucose consumption rates (b), cell growth (c), $\mu$-specific cell growth rate (d), antibiotic activity (e), $q_p$-specific antibiotic production rate (f) in the cultivation of *X. nematophila* YL001 at different pH pH 4.5 (○); pH 6.5 (■); pH 7.5 (▲); and pH 9.5 (×).
7.5, and decreased by 60% at pH 4.5, decreased by 7.5% at pH at 6.5 and decreased by 72.5% at pH at 9.5. Likewise, the optimal antibiotic yield on glucose ($Y_{PS}$) and the antibiotic productivity ($P_P$) occurring at pH 7.5 were 18.36 U/g and 1.39 U/mL/h, respectively. However, the optimal antibiotic yield on cell ($Y_{PSX}$) was 11.94 U/g obtained at pH 9.5. It can be concluded that among the controlled-pH operations pH 7.5 was favorable for antibiotic production due to the higher cell concentration and antibiotic activity obtained.

The specific antibiotic production rate ($q_p$) was determined from reciprocal of cell density and the slope of antibiotic activity versus fermentation time. In other words, it was obtained from the following equation:

$$q_p = \frac{1}{x} \frac{dp}{dt} = \frac{1}{\Delta t}\lim_{\Delta t \to 0} \frac{\Delta p}{\Delta t}$$

$q_p$ was obtained with the method similar to $\mu$. Profiles of $q_p$ at different pH had similar tendencies, the duration of reaching the maximum $q_p$ was similar at different pH, and the decreasing rate was also different after $q_p$ reached the maximum (Figure 3(f)). The value of the maximum $q_p$ were different at different pH, the highest $q_p$ could be achieved at pH 7.5. During the bioprocesses, at pH 6.5 and 7.5, the average specific antibiotic formation rate was 0.20 and 0.36 U/g/h, respectively. So, it was concluded that during the whole bioprocess, it is appropriate to control pH at high value (e.g., pH 7.5) to maximize $q_p$.

### 3.5. Two-Stage pH-Shift Strategy

During the whole process, the suitable pH for cell growth and antibiotic formation is different; it is favorable to use a two-stage pH-control process instead of constant pH process. From the results earlier, relative low pH value (e.g., pH 6.5) at earlier fermentation stage not only made the lag phase of cell growth shorter but also was advantageous to cell growth and antibiotic production. At mid- and later-stage, properly increasing pH value (e.g., pH 7.5) can strengthen cell growth and antibiotic production (Figures 3(c), 3(d), and 3(e)).

However, Figure 3(f) shown that relative high pH value (e.g., pH 7.5) during the whole bio-process can increase the antibiotic activity. The approaches to pH control was not only beneficial to cell growth but also was advantageous to antibiotic production. Based on the above results, a pH-shift culture by combining the first-stage culture at pH 6.5 with the following second-stage culture at pH 7.5 was proposed in order to increase biomass and antibiotic activity. Here, effect of shift time (i.e., hour 12, 24, 36, and 48) between the first stage and the second stage was tested.

The results of fermentation parameters are listed in Table 1. In all cases, a gradual increase of antibiotic activity was observed within the culture time. At the shift time of 12 and 24 h, the antibiotic activity remained unchanged, and was improved significantly compared with that at the shift time of 36 and 48 h. Not only the maximal DCW ($X_{\text{max}}$), specific cell growth rate ($\mu$), cell yield on glucose ($Y_{X/S}$) and cell productivity ($P_X$), but also the maximal antibiotic activity ($P_{\text{max}}$), specific antibiotic production rate ($q_p$), antibiotic yield on glucose ($Y_{PS}$), and antibiotic productivity ($P_P$) were attained at the shift time of 24 h. Nevertheless, in spite of an increased average specific antibiotic production rate during the whole process, the average specific growth rate remained unchanged at the shift time of 12 and 24 h (data not shown), suggesting that the additional energy flux obtained from direct fermentation of glucose was used for functions other than growth. The slight increase in $Y_{X/S}$ at the shift time of 24 h suggests that controlling the pH would improve the coupling between energy production and biomass synthesis. This indicated that optimal pH-shift controlled strategy was developed as follow: in the first stage, the culture pH was controlled at a pH 6.5 around 24 h; it was then shifted to pH 7.5 in the secondary stage. The fermentation process in the fermenter with the pH-shift controlled operation was performed to improve the biomass and antibiotic activity as demonstrated in Figure 5.

The antibiotic activity of the two-stage batch fermentation process further enhanced by 46% and 59% as compared to that of the fermentation at pH 7.5 and initial pH 7.0, respectively, reaching 185.0 U/mL. The cell yield on glucose
of the two-stage process was 3.87 g/g, which was slightly higher than the Y_{XS}, 3.82 g/g, of the fermentation at pH 6.5. However, the highest antibiotic yield on cell (Y_{P/X}) and antibiotic productivity (P_{P}) of the two-stage fermentation process were achieved at 11.77 U/g and 4.41 U/mL/h, respectively. To conclude, a pH-shift culture of *X. nematophila* YL001 was successfully developed.

### 4. Discussion

Since the phases of a bioprocess are dynamic and are the consequences of directed functioning of the bioreaction network interacting strongly with the microenvironment of the cell, the influence of the operational variable pH on the overall bioreaction is indeed important and needs clarification in order to develop an operational strategy. In this work, we systematically studied the effect of pH on growth and activity of *X. nematophila* YL001. To improve biomass and antibiotic activity, this research used unique strategies. The effects of uncontrolled- (different initial pH) and controlled-pH (different constant pH) operations on dissolved oxygen, glucose, cell, and antibiotic activity profiles were determined throughout the bioprocess. Based on the kinetic information about pH effects on the fermentation of *X. nematophila* YL001, the two-stage pH control strategy was established to improve the biomass and antibiotic activity.

Under the condition of pH changing naturally, the maximum biomass and antibiotic activity occurred at initial pH of 7.0. At initial pH 7.0 with the use of glucose as sole carbon source, the pH of the fermentation broth varied between 5.9 and 9.75. However, the broth pH varies with different strains, operational conditions, and medium composition, with the use of complex carbon sources which will result in considerable changes in the medium pH. Isaacson and Webster [23] reported that *Xenorhabdus* sp. RIO showed growth *in vitro* similar to that of other *Xenorhabdus* species grown in TSB, the culture broth pH of RIO decline from 7.07 to pH 6.89 during the first few hours of growth, and then increased throughout the course of the experiment reaching 8.79 at 168 h [23]. The culture broth pH of *X. nematophila* BJ varied from 6.5 to 8.5 [16]. Although microbial cells have the ability to respond to environment alterations and a remarkable ability to maintain the intracellular pH at a constant level even with large variations in the pH of the extracellular medium, the pH of the environment has a natural tendency to change along with the bioprocess. Provided that these alterations proceed within the acceptable ranges in which growth and metabolism is not affected. In this study, whether the pH variations go beyond the acceptable ranges and have disadvantageous effect on the growth and antibiotic activity of *X. nematophila* YL001. In order to clarify the problem, the effect of controlled-pH operations on fermentation were determined; the pH variation values were near the extreme values at initial pH 7.0, because low and high pH value (e.g., pH 4.5 and 9.5) was disadvantageous to cell growth and antibiotic production. When pH was kept stable in the fermentation process, the most optimal reaction condition was at constant pH of 7.5. However, at earlier fermentation stage, a constant pH of 6.5 was advantageous to cell growth and antibiotic production, at mid- and later stage, pH of 7.5 can strengthen cell growth and antibiotic production. Also, in all cases, the antibiotic production could be enhanced by increasing the concentration of antibiotic producing cells. Similar results were obtained in the reports of Sundar and Chang [25], Isaacson and Webster [23] and Ji et al. [4], as the bacterial population increased, the antibacterial activities increased and reached the maximal level at the stationary growth phase of the bacteria [4, 23, 25]. The result also could be validated by the profiles of DO concentration at different constant pH. During 0–18 h, due to higher DCW at pH 6.5 the antibiotic activity was noticeably higher than that at pH 7.5, this also result in lower DO concentration. After 42 h, the DO concentration was lower at pH 7.5, as the DCW was higher compared to that at pH 6.5. However, the antibiotic

### Table 1: The parameters of the batch fermentation of *X. nematophila* YL001 under various pH controlled processes.

| Different pH Controlled processes | X_{max} (g/L) | μ (h\(^{-1}\)) | P_{X} (g/L/h) | Y_{XS} (g/g) | P_{max} (U/mL) | P_{P} (U/mL/h) | q_{P} (U/g/h) | Y_{P/S} (U/g) | Y_{P/X} (U/g) |
|----------------------------------|--------------|---------------|--------------|-------------|---------------|--------------|-------------|--------------|--------------|
| Initial pH 7.0 (uncontrolled)    | 19.45        | 0.10          | 0.27         | 3.49        | 76.0          | 1.58         | 1.086       | 13.80        | 4.42         |
| Controlled at pH 4.5             | 13.07        | 0.055         | 0.18         | 2.37        | 40.0          | 0.56         | 1.316       | 7.23         | 3.06         |
| Controlled at pH 6.5             | 20.77        | 0.092         | 0.29         | 3.82        | 92.5          | 1.29         | 0.844       | 17.00        | 4.45         |
| Controlled at pH 7.5             | 23.71        | 0.075         | 0.33         | 4.37        | 100.0         | 1.39         | 1.855       | 18.36        | 4.30         |
| Controlled at pH 9.5             | 4.46         | 0.021         | 0.06         | 0.93        | 27.5          | 0.42         | 1.093       | 5.90         | 11.94        |
| pH-shift controlled\(^1\)        | 20.57        | 0.074         | 0.29         | 3.51        | 185.0         | 4.41         | 3.137       | 36.13        | 13.10        |
| pH-shift controlled\(^2\)        | 21.31        | 0.079         | 0.30         | 3.87        | 185.0         | 4.41         | 2.986       | 37.65        | 11.77        |
| pH-shift controlled\(^3\)        | 19.53        | 0.060         | 0.27         | 3.55        | 155.0         | 4.31         | 2.402       | 32.43        | 16.40        |
| pH-shift controlled\(^4\)        | 18.46        | 0.072         | 0.26         | 3.37        | 148.3         | 4.12         | 2.385       | 30.58        | 14.13        |

- **X_{max}**: maximal dry cell weight; **μ**: specific cell growth rate; **P_{X}**: cell productivity; **Y_{XS}**: cell yield on glucose; **P_{max}**: maximal antibiotic activity; **P_{P}**: antibiotic productivity; **q_{P}**: specific antibiotic production rate; **Y_{P/S}**: antibiotic yield on glucose; **Y_{P/X}**: antibiotic yield on cell.

\(^1\) Culture pH was controlled at pH 6.5 within the first 12 h, then shifted to pH 7.5 until the end of the fermentation.

\(^2\) Culture pH was controlled at pH 6.5 within the first 24 h, then shifted to pH 7.5 until the end of the fermentation.

\(^3\) Culture pH was controlled at pH 6.5 within the first 36 h, then shifted to pH 7.5 until the end of the fermentation.

\(^4\) Culture pH was controlled at pH 6.5 within the first 48 h, then shifted to pH 7.5 until the end of the fermentation.
activity was not significantly different at pH 6.5 and 7.5 (Figures 3 and 4). In aerobic fermentations, the supply of oxygen is often the rate limiting step and oxygen limitation concomitant with an increase in the cell concentration in culture is well known to have a detrimental effect on cell activity and to decrease the productivity of antibiotics [26]. In this study, DO concentration stabilized at zero level at all constant pH except for pH 9.5 during the growth phase, and oxygen limitation took place, at mid- and later stage, the DO level increased and a high DO level was maintained throughout the fermentation as the growth of cell was lower. However, at pH 9.5 the DO concentration was above 80% until the end of fermentation, and the lowest DCW and antibiotic activity was obtained. So, in order to improve the antibiotic activity, the pH control must be beneficial to the growth of X. nematophila YL001. Based on the results, the two-stage pH control strategy was developed. The highest antibiotic activity of 185.0 U/mL was obtained when pH was shifted from 6.5 to 7.5 on 24 h, which was increased by 50% and 45.6% compared with the cultures at pH 6.5 and 7.5, respectively. By this mechanism, the pH of the fermentation medium is kept between the desired values without increasing the stress on the microorganism.

Global regulators, which affect the transcription of gene ensembles via regulatory cascades, typically govern the production of small molecules in bacteria [27]. Identification and manipulation of these global regulators could provide a powerful approach to complete sets of biologically important and previously uncharacterized small molecules. Kontnik et al. [28] coupled a global transcriptional regulator, HexA, to secondary metabolite production in Photorhabdus luminescens. P. luminescens ΔhexA mutant led to dramatic upregulation of biosynthesized small molecules [28]. The CpxRA signal transduction systems involved in the pathogenic and mutualistic interactions of the entomopathogenic acterium X. nematophila [29–31]. The Cpx system of E. coli consists of three proteins, CpxA, CpxR, and CpxP. CpxA, an sensor histidine kinase with autokinase, phosphotransfer, and phospho-CpxR phosphate activities, is located in the cytoplasmic membrane, where it senses diverse signals, including alkaline pH. In response, CpxA autophosphorylates and donates its phosphoryl group to CpxR, the cognate response regulator. When phosphorylated, this transcription factor controls part of the envelope stress response system, pilus assembly, type III secretion, motility and chemotaxis, adherence, and biofilm development [32]. CpxR negatively influences the antibiotic activities in X. nematophila [29]. So, CpxR-phosphate negatively regulates the antibiotic activities of X. nematophila. CpxP was identified as an alkaline-induced member of the Cpx regulon. This periplasmic chaperone binds to the periplasmic domain of CpxA and inhibits its autokinase activity [32]. In this study, when pH was shifted from 6.5 to 7.5 on 24 h, the alkaline pH may induced the production of CpxP and inhibits CpxA autophosphorylates and CpxR phosphorylates. So, the antibiotic activities of X. nematophila YL001 were enhanced.

5. Conclusions

It was demonstrated in this study that different modes of pH manipulation had remarkably distinct effects on cell growth and antibiotic activity of X. nematophila in shaking flasks and 5-L fermenter. The optimal initial pH values for cell growth and antibiotic activity was identified (pH 7.0). In the cultivations at constant pH, the highest values of biomass and antibiotic activity were obtained at pH 7.5. pH value at a further higher level would inhibit biomass formation and antibiotic activity. Although the lower pH value (e.g., pH 6.5) limited cell growth, the biomass and antibiotic activity were relatively higher in the earlier stage of cultivation compared to what gained in the case with a higher pH value (e.g. pH 7.5). A two-stage pH control strategy intending to obtain higher biomass and antibiotic activity throughout the cultivation were proposed. The two-stage pH control strategy was proved to be the better policy for the enhancement of antibiotic activity and productivity. By fine tuning of pH-shift strategy, there may be a scope for further enhancement of the antibiotic activity. In addition to pH, other parameters such as dissolved oxygen (including agitation speed and aeration rate) and temperature may also be changed in the two-stage process to optimize cell growth and antibiotic production, respectively. However, this hypothesis remains to be verified further.

Acknowledgment

The financial support by National Department Public Benefit Research Foundation of China (200903052), Young People Science Program (no. 52211241), and Scientific Research Special Project of Northwest A & F University is gratefully acknowledged.

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