Enhancement in Selectivity of Coking Coal Flotation by Ultrasound Simultaneous Treatment

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Abstract. The influence of ultrasound simultaneous treatment on coking coal flotation were investigated by adding ultrasound to the pulp zone. The flotation results showed ultrasound simultaneous flotation (USF) produced the clean coal of lower ash content compared with conventional flotation (CF). Moreover, the combustible recovery rate of USF was higher than that of CF. Scanning electron microscope found that the ultrasound could reduce the high-ash fine slime coated on coal surface. Particle size distribution results showed the ultrasound simultaneous treatment increased the recovery of coarse coal. Th e coal surface oxidation was found by the X-ray photoelectron spectroscopy of coal surface with/without ultrasound treatment. The negative impact of ultrasound on the surface oxidation was much less than the positive effect of ultrasound on reducing the slime coating on coal surface and increasing the aggregates of the bubbles. It is concluded that USF of coking coal has a higher selectivity than CF.

Keywords: coal flotation; ultrasound; selectivity; scanning electron microscope; X-ray photoelectron spectroscopy.

1 Introduction

Coking coal is the mainly used to produce coke as raw material in the metallurgical industry [1, 2]. Before the utilization, it is necessary to remove the minerals from the coal by flotation and gravity separation [3]. At present, flotation is the main ways to effectively remove fine gangue particles from fine coal particles [4, 5]. The flotation mechanism relies on the physical and chemical differences between the coal and gangue surface, while the hydrophobic coal particles are carried to the froth layer and the gangue particles are left in the pulp. Coking coal have great floatability due to its high degree of metamorphism. Flotation can get a high clean coal yield when the dosage of collector is low. However, a lot of high-ash slime can coat on clean coal surface during flotation, which pollutes the clean coal and decreases the grade of clean coal products [6, 7]. Thus, it is particularly important to use technical means to effectively reduce the ash content of coal. Xia et al.[8] discovered that the mixture collector of nano-carbon particles and n-dodecane can increase the yield of coking coal by about 1% and also decrease the ash content of clean coal. Li et al.[9] used soybean oil as a sustainable flotation collector to not only increase the clean coal yield but also reduce the clean coal ash content. In addition, the application of flotation column in coal separation can effectively reduce the clean coal ash content [10, 11]. Ultrasound simultaneous flotation (USF) is also used in low-rank coal flotation as an emerging high-efficiency flotation method in recent years [12-14]. Mao et al. [13] found that ultrasound evidently improved the flotation of fine lignite particles and the water recovery. Ozkan et al.[15] found that USF can not only increase the recovery rate of hard coal, but also reduce the ash content of clean coal. In addition, the effect of ultrasonic treatment on the particle size, shape and ash content of lignite was studied through Mao et al [16]. Chen et al.[17] found that ultrasound pretreatment can not only clean the slime on the coking coal surface, but also enhance the dispersion of collector in pulp. There are few studies on the influence of ultrasound on the coking coal flotation and its deashing performance. Therefore, this study innovatively studied the enhanced selectivity mechanism of coking coal flotation through adding ultrasound to the pulp zone.

This paper took coking coal as sample and investigated the influence of USF on the coking coal. Scanning electron microscope (SEM) was used to observe the influence of ultrasound on the slime coated on coal surface. X-ray photoelectron spectroscopy (XPS) was used to determine the influence of ultrasound on the
coking coal surface properties. The laser particle size was used to analysis the influence of ultrasound on the clean coal particle size distribution.

2 Experiment

2.1 Coal Samples

The samples used for the work were taken from a coking coal preparation plant in Shanxi province, China. Table 1 shows the proximate analysis result of coal sample. Table 2 shows the result of coal size composition. The density fraction analysis of raw coal was shown in Table 3.

The screening test result of raw coal sample showed that the main size fraction was 0.5~0.25 mm, followed by <0.045 mm. There were many coarse particles in the coal sample as well as high-ash slime. The high-ash slime were easy to cause entrainment in the froth layer, leading to the high clean coal ash content. Table 3 revealed the theoretical clean coal yield was about 68% with the ash content of 10% at about 1.57 kg/L.

| Moisture (%) | Ash (%) | Volatile (%) | Fixed Carbon (%) |
|--------------|---------|--------------|-----------------|
| 0.45         | 24.16   | 24.49        | 50.90           |

Table 2. Coal sample screening test results

| Size Fraction (mm) | Yield (%) | Ash (%) | Cumulative Undersize Yield (%) | Ash (%) |
|--------------------|-----------|---------|-------------------------------|---------|
| ≥0.500             | 7.95      | 23.94   | 7.95                          | 23.94   |
| 0.500-0.250        | 37.47     | 23.87   | 45.42                         | 23.88   |
| 0.250-0.125        | 15.76     | 23.36   | 61.19                         | 23.75   |
| 0.125-0.074        | 10.82     | 23.33   | 72.01                         | 23.69   |
| 0.074-0.045        | 6.33      | 21.52   | 78.34                         | 23.51   |
| <0.045             | 21.66     | 25.95   | 100.00                        | 24.04   |
| Total              | 100.00    | 24.04   |                               |         |

Table 3. Coal sample float and sink test results

| Gravity Range (kg/L) | Yield (%) | Ash (%) | Cumulative Floats Yield (%) | Ash (%) |
|----------------------|-----------|---------|----------------------------|---------|
| -1.3                 | 21.32     | 2.05    | 21.32                       | 2.05    |
| 1.3-1.4              | 22.87     | 8.11    | 44.19                       | 5.19    |
| 1.4-1.5              | 17.04     | 16.98   | 61.23                       | 8.47    |
| 1.5-1.6              | 11.72     | 28.32   | 72.95                       | 11.66   |
| 1.6-1.7              | 7.63      | 36.99   | 80.58                       | 14.06   |
| 1.7-1.8              | 4.47      | 46.52   | 85.06                       | 15.77   |
| ≥1.8                 | 14.94     | 72.14   | 100.00                      | 24.19   |
| Total                | 100.00    | 24.19   |                               |         |

2.2 SEM and Laser Particle Size Tests

The clean coal surface after coating with a layer of gold was analyzed by Quanta 250 SEM (FEI, USA) at a magnification of 1,000.

Microtrac Inc S3500 laser particle size analyser (America) was applied to analyze the size distribution of clean coal particles. In order to disperse the coal particles effectively, coal particles were added to a 5 wt.% aqueous solution of sodium hexametaphosphate and stirred by ultrasound treatment for 5 min.
2.3 XPS Tests

The XPS analysis of the clean coal surface was carried out in an ultra-high vacuum (UHV) system with the surface analysis system (ESCALAB 250 Xi, America) at room temperature. The peak fitting was analyzed by XPS Peak fitting software.

2.4 Flotation Experiments

Flotation were operated in a 1.5 L flotation cell and the mass fraction of coal sample in pulp was 6%. In addition, the impeller speed at 1800 rpm. The kerosene was used as collector at 200 g/t coal. The sec-octyl alcohol was used as frother at 80 g/t coal.

Firstly, the coal and water were added into flotation cell and conditioned for 180 s. Secondly, adding kerosene and stirring for 120 s. Thirdly, adding sec-octyl alcohol and stirring for 30 s. Finally, the air flow rate was 250 ml/min and the flotation froth was collected at 10s, 30s, 60s, 120s and 180s. The USF was consistent with CF. The difference was that the ultrasound probe was inserted into the pulp zone of flotation cell when the air was given during USF. Ultrasound power setting of 100 W was selected for USF tests. The clean coal and tailings were collected, dried, weighed and analyzed. The yield and ash content of clean coal were used to evaluate the effect of flotation behavior of coal with ultrasound treatment. The combustible recovery rate, yield and ash content were calculated from the following equation [18, 19]:

\[
\text{Combustible recovery rate} = \frac{Y_C (100 - A_C)}{Y_F (100 - A_F)} \times 100
\]

where \(Y_C\) is the yield of the clean coal (%); \(Y_F\) is the yield of the feed (%), 100%; \(A_C\) is the ash content of the clean coal (%); \(A_F\) is the ash content of the feed (%).

\[
Y_C = \frac{W_C}{W_C + W_T}
\]

\[
A_C = \frac{W_A}{W_F}
\]

where \(W_C\) is the weight of the clean coal (g); \(W_T\) is the weight of the tailings (g); \(W_A\) is the residual ash weight after coal combustion completely (g); \(W_F\) is the sample weight before combustion (g).

3 Results and Discussion

3.1 SEM and Laser Particle Size Results

![Figure 1. SEM results of the clean coal by conventional (a) and ultrasound simultaneous (b) flotation](image)
Figure 1 indicated the clean coal surface of CF has more coated slime particles than that of USF. It indicated that the ultrasound had a cleaning action on the coal surface. This behavior was beneficial to reduce the ash content of clean coal. Reducing the hydrophilic slime coated on the coal surface can indirectly increase the hydrophobicity of the coal in the flotation pulp, thereby increasing the adhesion probability between the coal and bubbles. Mao et al [20] also found that ultrasound have a strong cleaning effect on the lignite surface, resulting in the high yield and the low ash content of clean coal by USF. In addition, they found that the ultrasound can also reduce the high-ash slime coated on the lignite surface, which benefits the improving the adsorption of collector on lignite surface and improving the flotation recovery [13]. Therefore, USF can enhance the selectivity of coking coal flotation.

![Figure 2](image1.png)

**Figure 2.** Laser particle size analysis results of clean coal produced by CF and USF

![Figure 3](image2.png)

**Figure 3.** Pictures of the influence of ultrasound on bubble aggregates (a, 0 W; b, 20 W; c, 110 W; d, 200 W)[21].

Figure 2 illustrated size distribution analysis results of clean coal produced by CF and USF. The d50 of CF clean coal was 241 μm and the d50 of the clean coal by USF was increased to 342 μm. It indicated that in the coking coal flotation, the addition of ultrasound was good for coarse coal particles to float. This is different from the results of Mao et al [13], the sample of their study were lignite with low hardness,
while the samples used in this study were hard coking coal. Compared with lignite, ultrasound is not easy to break coking coal. As shown in Figure 3, Mao et al [21] found the addition of ultrasound during the flotation process was not only advantageous for the generation of large bubbles, but also for the aggregates or attraction of the bubbles. According to their finds, 100W ultrasound can lead to the bubbles aggregate in the pulp in this study. These bubble aggregates had a greater carrying capacity than the single bubble and they can carry coarse coal particles into the froth layer, which enhances coarse coking coal flotation. The interaction between bubble aggregates contributed to drainage between the bubbles [22], and the high-ash slimes return to the pulp zone with the drainage, thereby enhancing the secondary enrichment of fine coal in the flotation froth. Therefore, the content of high-ash slimes was reduced effectively in the flotation clean coal.

3.2 XPS Results

![Figure 4. C1s peak of coal surface produced by a) conventional flotation and b) ultrasound simultaneous flotation](image)

![Figure 5. Functional group content of clean coal surface produced by conventional and ultrasound simultaneous flotation](image)

Figure 4 and Figure 5 showed the C1s narrow energy spectrum results of clean coal surfaces by CF and USF. For the C1s, the peaks position at about 284.7 eV, 285.4 eV and 286.6 eV correspond to the groups:
C-C/C=C, C-O and C=O [23-26]. Figure 5 showed when the ultrasound was added in the flotation process, the content of C-C/C=C on the clean coal surface was reduced a little compared to that without the ultrasound treatment, while the content of C-O and C=O increases a little. Which indicated that ultrasound had a slight oxidation effect on coking coal surface. Xu et al. [12] found that 20 minutes of ultrasound pretreatment increased the content of oxygen-containing functional groups on the surface of oxidized coal. They thought this is caused by the reoxidation of coal surface through ultrasound treatment. Although the ultrasound treatment time is short in this study, it is found that the reoxidation of coking coal surface was strong with ultrasound through XPS results. The oxide on low rank coal/oxidized coal surface is firstly removed by ultrasound in the process of ultrasound treatment, the new surface is secondly reoxidized through ultrasound until the oxide is removed. However, the oxide can be removed in a short time of ultrasound treatment due to the coking coal surface with less oxide compared with low rank coal/oxidized coal, and then the new surface produced by ultrasound can be reoxidized through ultrasound. Ultrasound were prone to the cavitation in water, which in turn produces cavitation bubbles, some of which may adhere to the coal surface, and some cavitation bubbles may aggregate or merge or even rupture. On the one hand, shock waves can clean the pollutants on the coal surface, on the other hand, they can clean the oxides on the coal surface. However, the rupture of cavitation bubble can also lead to the generation of •OH and •H through thermal decomposition [27]. It can be inferred from XPS results that •OH and •H free radicals can secondary reactions to produce H2O2 [12].

\[
\begin{align*}
H_2O &\rightarrow \cdot H + \cdot OH \\
\cdot H + O_2 &\rightarrow \cdot HO_2 \\
\cdot HO_2 + \cdot HO_2 &\rightarrow H_2O_2 + O_2 \uparrow \\
\cdot OH + \cdot OH &\rightarrow H_2O_2 
\end{align*}
\]

• OH and H2O2 had strong oxidation ability and reactivity. Which can oxidize the coal surface under ultrasound treatment [14]. Ultrasound oxidation inevitably leaded to an increase in the oxygen-containing functional groups on the coal surface, which ultimately leads to a slight decrease in the coal surface hydrophobicity. Combined with the flotation results in Figure 6, the yield of USF clean coal decreased slightly, which indicated that the oxidation of coal surface by ultrasound cavitation could eventually lead to the decrease of clean coal yield, but this decrease can be ignored. However, USF had a higher combustible recovery rate than CF as shown in Figure 7. The advantage was that it has a good influence on the float of coarse low-ash coal and the reduction of clean coking coal ash content. It showed that the negative impact of ultrasound on reducing the coal surface hydrophobicity was much less than the positive effect of ultrasound on the flotation selectivity.

3.3 Flotation Results

Figure 6 showed the cumulative yield of clean coal by USF was slightly higher than the CF at first stage of 30s. In the 30s-180s period, the CF cumulative clean coal yield was slightly higher than the USF. Since during the 10s aeration, the USF caused the coarse coal to float into the froth layer, resulting in a higher clean coal yield than CF. The clean coal yield was slightly decreased in the USF compared with that in the CF because the recovery of fine slime was reduced in USF. After adding ultrasound, the flotation of clean coal ash content was reduced by about 2% compared with the CF. Because of the physical cleaning action of ultrasound, which reduced the high-ash slime coated on the coal, and enhanced the selectivity of coking coal flotation.

To clearly show the difference in the efficiency of two flotation methods, the combustible recovery rate was computed and the results were showed in Figure 7. The combustible recovery rate of USF was greater than that of CF. It showed that the selectivity of USF was better than that of CF. USF is beneficial to reducing the high-ash fine slime coated on the clean coal surface, so it enhances the selectivity of coking coal flotation.
4 Conclusion

In this paper, the recovery of coking coal by CF and USF was compared. It was found that the ultrasound cleaning the coal surface and reducing the high-ash fine slime coated on coal surface. The ultrasound promoted the recovery of coarse coal particles. Therefore, USF helps to enhance the coking coal flotation and reduce the clean coal ash content. In addition, the ultrasound can oxidize coking coal surface slightly, increase the content of oxygen-bearing functional groups on the coking coal surface, thereby reducing the hydrophobicity of coal surface. The negative impact of ultrasound on reducing the coal surface hydrophobicity was much less than the positive impact on the flotation selectivity. Therefore, the USF benefited the flotation of coking coal if a lower clean coal ash was required in coal flotation industry.
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