Transition metal (TM) dissolution is a long-known degradation phenomenon of lithium manganese spinel-type cathode active materials for Li-ion batteries. It is amplified by temperature, high cathode potentials, and large BET surface area of the particles. As layered lithium nickel cobalt manganese oxide (NCM) cathode materials are cycled to higher cutoff potentials to maximize the energy density of Li-ion cells, transition metal dissolution also becomes significant for NCMs. Experimental and ab initio modeling studies suggest that the electrochemical oxidation of LiPF$_6$-based electrolytes at high voltages and/or follow-up reactions of the electrolyte with oxygen released from the NCM host lattice can generate HF, which then corrodes the layered transition metal oxide cathode materials. Upon lattice oxygen release (occurring upon delithiation to $\sim$80% in NCMs), not only manganese, but also nickel and cobalt are dissolved as TM$^{2+}$ ions into the electrolyte at concentration ratios that reflect the stoichiometry of the bulk material.

The most apparent consequences of transition metal dissolution are capacity and power fade. However, the amount of dissolved cathode active material is typically less than 1%, which is too low to explain the observed capacity losses. Instead, the transition metal ions deposit on the graphite anode, where they lead to a significant decrease of the coulombic efficiency and to a large increase in anode impedance. It is not fully understood how transition metal ions cause these detrimental effects, yet the negative impact of manganese on graphite anode capacity retention is considerably worse compared to nickel and cobalt.

Recent studies have shown that Mn$^{2+}$ ions exchange rapidly with Li$^+$ ions contained in the solid electrolyte interface (SEI), as evidenced by soaking either preformed graphite electrodes or single SEI compounds such as LiF or Li$_2$CO$_3$ in Mn$^{2+}$-containing electrolytes. Furthermore, Mn$^{2+}$ ions were found to accumulate at the interface between organic (outer) and inorganic (inner) SEI in EC-based electrolytes without additives. While some groups identified exclusively Mn(+II) species like MnCO$_3$ and MnF$_2$, others found also reduced manganese in its 0 or +1 oxidation state on lithiated graphite. Considering that nano-sized transition metal carbonates and -fluorides have been tested as conversion-type anode materials, a reduction of these species in the SEI to metallic manganese seems likely. However, since the irreversible capacity on graphite anodes is typically 30–50 times higher than the capacity required for a 2-electron reduction of the accumulated manganese, additional side reactions must be taking place, consuming active lithium. One proposed hypothesis is that reduced manganese in contact with electrolyte re-oxidizes to Mn$^{2+}$ by simultaneously reducing solvent molecules, as supported by DFT calculations from Han et al. If then the Mn$^{2+}$ ions can be reduced again, a catalytic cycle would be established by which active lithium would be lost continuously into the SEI. While this appears plausible, the question remains why manganese would not eventually be covered by SEI species that would prevent new solvent molecules from reaching the active TM center, and thus would stop the electrolyte reaction with the TM center. To resolve this question, Leung and Joshi et al. suggested that transition metals also decompose organic SEI species, thus compromising the passivating properties of the SEI.

Despite the many mechanistic insights gained by the above described studies, the nature of the electrolyte or SEI decomposition reactions associated with manganese deposited on graphite anodes remains unclear. Moreover, the number of analogous studies on the effect of nickel ions is limited, although nickel is the most commonly dissolved transition metal from Ni-rich NCMs and NCA. The scientific debate is further complicated, as the typical sample washing and/or drying steps required for conducting detailed ex-situ diagnostics like X-ray photoelectron spectroscopy (XPS), X-ray absorption spectroscopy (XAS) or scanning electron microscopy (SEM) can easily affect the transition metal oxidation state. Therefore, the use of operando techniques for investigating the transition metal redox mechanism in the SEI has become imperative.

In this work, we use on-line electrochemical mass spectrometry (OEMS) to investigate the fundamental reactions of carbonate based electrolytes with nickel and manganese ions on a graphite anode. In order to mimic the effect of a typical dissolution of $\sim$0.3 wt% of the cathode active material observed in the above discussed studies, we use an ethylene carbonate (EC)/LiPF$_6$ model electrolyte containing Mn$^{2+}$ or Ni$^{2+}$ ions at the corresponding amounts. To avoid deposition of the transition metal ions on the lithium counter electrode, we use a sealed 2-compartment cell setup, separating the working and counter electrode compartments by a lithium ion conducting solid electrolyte. As ethylene is the major gaseous product of the reductive decomposition of EC, we will especially focus on its evolution during formation and cycling of graphite electrodes in Mn- or Ni-containing electrolytes. Considering that in real lithium-ion cells, transition metal dissolution occurs predominantly after the battery formation process.
Experimental

Preparation of electrodes and electrolytes.—Graphite electrodes were prepared by mixing graphite (SLP30, 7 m²\text{BET}/g, Timcal, Switzerland) and polyvinyl difluoride (PVDF, Kynar HSV 900, Arkema, France) in a ratio of 95:5 with N-methyl-pyrrolidone (NMP, anhydrous, Sigma-Aldrich, Germany; ink solid content 40%) in a planetary mixer (Thinky Corp., USA) at 2000 rpm for 15 min. The ink was then coated onto a polyester separator (FS 24316, Freudenberg, Germany) and dried at 50 °C for 10 h. Electrodes with 15 mm diameter were punched out, dried in a glass oven (Büchi, Switzerland) under dynamic vacuum at 120 °C for 12 h and transferred into the glove box without exposure to air. The final electrodes had a loading of 6.1 ± 0.2 mg\text{graphite}/cm² (≈ 2.3 mA h/cm²). Glassfiber and polyester separators were also dried at 120 °C under dynamic vacuum prior to use.

Electrolytes were prepared by mixing LiPF₆ (BASF SE, Germany) with ethylene carbonate (EC, BASF SE, Germany) or dimethylcarbonate (DMC, BASF SE, Germany) to yield a 1.5 M LiPF₆ concentration. For preformation of graphite anodes with an SEI-forming additive, vinylene carbonate (VC, BASF SE, Germany) was added at a concentration of 2 wt% to the as-prepared DMC/LiPF₆ electrolyte. Manganese bis-(trifluorosulfonylimide) (Mn(TFSI)₂, 99.5%, Alfa Aesar, United States) were dried under dynamic vacuum at 120 °C for 3 days and added to the electrolytes to yield a metal concentration of 10 mM, corresponding to a total amount of 1.5 μmol in the cell or 0.85 μmol/cm² per geometric graphite electrode area (based on 150 μL electrolyte and 0.15 mm electrodes). For a full-cell with our graphite anodes and a balanced cathode with a loading of 13.5 mg\text{CAT}/cm² (≈ 2.2 mA h/g for a specific capacity of 165 mA h/g), the total amount of dissolved transition metal would translate to ≈ 3.4 μg/m² for carbonyl groups.

Isotopologue measurements.—For on-line electrochemical mass spectrometry (OEMS) analysis, we used an Agilent 5975C inert gas introduction system coupled to an 7000B LTQ-FTMS to determine the reaction of pristine graphite electrodes, i.e., when no SEI is present. This represents the situation in commercial Li-ion cells prior to battery formation, where dissolved transition metals are observed upon electrolyte storage of the pristine materials, likely formed by the reaction of cathode active materials with HF, which is present in commercial LiPF₆-based electrolytes at the level of several tens of ppm, or at even higher concentration if cell components are dried improperly. As ethylene carbonate (EC) is reduced to mostly lithium ethylene dicarbonate (LiEC) and C₂H₄, so that the latter is the main gaseous product during graphite SEI formation in EC-based electrolytes, we first focus on C₂H₄ as a marker of the reaction of pristine graphite electrodes in EC/LiPF₆ without added transition metal salts, or with either 1.5 μmol Mn²⁺ or 1.5 μmol Ni²⁺ added as TFSI salts (equating to ≈ 140 μmol/m²\text{graphite}. Which would correspond to ≈ 0.3 wt% dissolution of a NCM cathode active material in a balanced full-cell; for details see Experimental section). The blue lines in Figure 1 show the baseline for the transition metal-free electrolyte. During the first cycle, a reduction peak current around 0.5 V vs. Li⁺/Li appears (Figure 1a), alongside with the evolution of ≈ 80 μmol/g C₂H₄ (Figure 1b), in good quantitative agreement with the ≈ 10 μmol/m²\text{BET} C₂H₄ found in earlier studies on the same graphite (BET: 7 m²/g). In the following cycles, the C₂H₄ evolution stops (as indicated by the constant concentration), also consistent with our previous reports. When 1.5 μmol Ni(TFSI)₂ are added to the electrolyte, an additional reduction feature in the first cycle, starting at 2.5 V vs. Li⁺/Li, can be seen in the current response (green line in Figure 1a). For the Ni-containing electrolyte, C₂H₄ is evolved at much less negative potentials in the first reduction cycle (at ≈ 1.6 V vs. Li⁺/Li) and at higher amounts (112 μmol/g, see green lines in Figure 1b; for details please also refer to our previous publication).
to Figure 5), which increases slightly up to 117 µmol/g by the end of 4 charge/discharge cycles. As previous studies showed an identical gassing behavior of graphite electrodes cycled in either transition metal-free LiTFSI\(^{44}\) or LiPF\(_6\)^{52,53} based electrolytes, the effect of the TFSI\(^-\) anions on gassing should be negligible, so that the changes upon the addition of Ni(TFSI)\(_2\) must be due to the presence of Ni\(^{2+}\). The addition of 1.5 µmol Mn(TFSI)\(_2\) (see yellow lines in Figure 1) leads to the highest C\(_2\)H\(_4\) evolution in the 1st cycle, namely 128 µmol/g. Quite strikingly, with Mn\(^{2+}\), a distinct C\(_2\)H\(_4\) evolution is seen in each cycle, accumulating to 164 µmol/g C\(_2\)H\(_4\) after 4 charge/discharge cycles. A more detailed discussion on the potentials at which the 1st cycle reduction current peaks and the onset of C\(_2\)H\(_4\) evolution occur can be found in the Discussion section (see Figure 5).

While C\(_2\)H\(_4\) is the main gaseous product from EC reduction, H\(_2\), CO, and CO\(_2\) are also commonly observed during the formation of graphite in carbonate-based electrolytes. The total quantities of C\(_2\)H\(_4\), H\(_2\), and CO after 4 cycles are shown in Figure 2a. After 4 cycles in the TM-free electrolyte (blue bars in Figure 2a), 48 µmol/g H\(_2\) and 20 µmol/g CO have been evolved in addition to the initial capacity for graphite electrodes.\(^9\) The cumulative irreversible capacity is 22 mAh/g, after the 4 CV cycles depicted in Figure 1a. For the TM-free electrolyte (blue bars), the cumulative irreversible capacity is 22 mAh/g, which fits well to the expected formation losses of 7–10% of the initial capacity for graphite electrodes.\(^7\) The cumulative irreversible capacity over 4 cycles in an electrolyte with Ni\(^{2+}\) ions (green bars) is significantly higher (37 mAh/g), but still smaller than that of the Mn\(^{2+}\)-containing electrolyte (48 mAh/g), which fits to the observation that the latter also exhibits the highest amount of evolved gas (Figure 2a). Note that the additional cumulative irreversible capacity losses in the Ni-containing and the Mn-containing electrolytes (+15 mAh/g and +26 mAh/g, respectively) substantially exceed the capacity of ∼7.5 mAh/g required for a simple 2-electron reduction of the TM\(^{2+}\) ions (see horizontal gray dashed line in Figure 2b; based on the added salt concentration of 0.85 µmol/cm\(^2\) and the graphite loding of 6.1 mg/cm\(^2\), namely by a factor of ∼2 for Ni\(^{2+}\) and of ∼3.5 for Mn\(^{2+}\). This clearly indicates that at least the difference between the measured cumulative irreversible capacity and the theoretical charge for the TM ion reduction to the metal (i.e., the ∼7.5 mAh/g) must have gone into the irreversible reduction of the electrolyte.

The results from Figure 1 and Figure 2 show that in the presence of TM ions, especially Mn\(^{2+}\), strong additional electrolyte reduction takes place, consuming lithium and generating gas. As the composition of the evolved gas is comparable for all electrolytes, the fundamental reactions during SEI formation in TM-free and TM-containing electrolytes are apparently very similar. Moreover, the results demonstrate that manganese species continuously decompose electrolyte, whereas the activity of nickel species toward electrolyte reduction subsides much quicker.

**Preformed graphite electrodes.**—In commercial cells, the majority of transition metal dissolution occurs typically during cycling at high temperatures or voltages over extended periods of time. In this case, the SEI is already formed when the transition metal ions reach the anode. Therefore, we also investigate the effect of Ni\(^{2+}\) and...
Figure 3. a) Currents and b) ethylene evolution, normalized to graphite mass, during the first 4 voltammetric cycles of preformed graphite electrodes in EC/1.5 M LiPF₆ electrolyte with/without added metal salts. Preformation was done with TM-free electrolyte in a separate cell vs. an LFP cathode (2 cycles at C/8), using two different preformation electrolytes: i) EC/1.5 M LiPF₆ for the OEMS experiments in TM-free electrolyte (blue) or electrolyte with either 1.5 μmol Mn(TFSI)₂ (green lines) or 1.5 μmol Mn(TFSI)₂ (yellow); ii) DMC/1.5 M LiPF₆ + 2% VC for the OEMS experiment in electrolyte with 1.5 μmol Mn(TFSI)₂ (orange). The voltammetric cycles at 0.2 mV/s were done between 0.1–3.0 V vs. Li⁺/Li⁺, starting from OCV (∼2.9 V vs. Li⁺/Li⁺).

Mn²⁺ ions on preformed graphite electrodes. The SEI formation was achieved by pre-cycling (2 cycles at C/8) the graphite electrodes in a 1-compartment OEMS cell with capacitively oversized LFP counter electrodes in a TM-free EC + 1.5 M LiPF₆ electrolyte; the resulting SEI is known to consist mostly of LEDC and LiF, with only traces of Li₂CO₃ present. Afterwards, the cells were deep-discharged to a cell voltage of 0.3 Vcell (corresponding to a graphite electrode potential of ∼2.9 V vs. Li⁺/Li⁺), and the graphite electrodes were then transferred without further washing into the 2-compartment OEMS cell in an Ar-filled glove box. The discharge capacity over these first two formation cycles was 350–355 mAh/g, while the irreversible capacity accumulated to 25–27 mAh/g.

Figure 3 shows the current density (a) and the integral C₂H₄ evolution (b) during 4 CV cycles of the thus preformed graphite electrodes in electrolytes containing 1.5 μmol Mn²⁺ (yellow lines), 1.5 μmol Ni²⁺ (green lines) or no transition metal ions (blue lines). As one would expect, the TM-free electrolyte baseline for the preformed graphite electrode does no longer show the EC reduction current peak at ∼0.5 V vs. Li⁺/Li⁺, consistent with the observation that only traces of C₂H₄ (∼0.5 μmol/g) are evolved compared to the ∼80 μmol/g C₂H₄ evolved on a pristine graphite electrode (blue line in Figure 1b). Hence, the passivating properties of the SEI preformed in EC/LiPF₆ remained largely intact after transferring the preformed graphite electrode into the 2-compartment OEMS cell. On the other hand, with 1.5 μmol Ni²⁺ in the electrolyte, ∼2 μmol/g C₂H₄ are evolved during the first cycle (see green lines in Figure 3b), without any further C₂H₄ evolution in the subsequent cycles. If we compare the additional C₂H₄ evolution over 4 charge/discharge cycles induced by the presence of Ni²⁺ in the electrolyte on pristine graphite electrodes (∼36 μmol/g; green line in Figure 1b) vs. on preformed graphite electrodes (∼2 μmol/g; green line in Figure 3b), it becomes apparent that the effect of Ni²⁺ in the electrolyte is greatly suppressed by the presence of an SEI. Besides, also the additional reduction peaks between 2.5–1.5 V vs Li⁺/Li⁺ seen in Figure 1a (green line) are no longer observed on the preformed graphite electrode (green line in Figure 3a). This suggests that nickel ions released into the electrolyte from cathode active materials over the course of extended charge/discharge cycling should hardly compromise the stability of the SEI, and thus should only have a very minor negative impact on the active lithium inventory of the cell.

On the contrary, the addition of 1.5 μmol Mn²⁺ to a graphite electrode preformed in EC/LiPF₆ (yellow lines in Figure 3) leads to a ∼20-fold higher C₂H₄ evolution in the first cycle (39 μmol/g) compared to Ni²⁺, which continues in subsequent cycles, accumulating to a total amount of evolved C₂H₄ of ∼69 μmol/g after 4 cycles. This amounts to ∼80% of the additional C₂H₄ evolved on a pristine graphite electrode upon the addition of Mn²⁺ ions to the electrolyte (see difference between blue and yellow lines in Figure 1), which therefore implies that even if the SEI is formed in an Mn²⁺-free electrolyte, it is not able to suppress the detrimental electrolyte reduction reactions triggered by Mn²⁺ ions. In summary, while an SEI preformed in EC/LiPF₆ almost completely suppresses the negative effect of Ni²⁺ ions on electrolyte decomposition, it is not very effective in the presence of Mn²⁺ ions.

To better understand the effect of the SEI on the reactions caused by Mn²⁺ ions, we used the same graphite preformation procedure, but replaced the electrolyte for formation with DMC/LiPF₆ + 2 wt% vinylic carbonate (VC). In this case, the SEI formed with VC consists mainly of poly(VC) and Li₂CO₃, and has been reported to partially mitigate the poor coulombic efficiency and impedance growth caused by transition metal ions; furthermore, due to the absence of EC, no LEDC is being formed. After formation (2 cycles at C/8, yielding a cumulative irreversible capacity of ∼31 mAh/g), the electrode was rinsed with pure DMC to remove any remaining VC, and was transferred into the 2-compartment OEMS cell. The orange lines in Figure 3 show the current profile and the C₂H₄ evolution of the VC-preformed graphite electrode cycled in EC/LiPF₆ + 1.5 μmol Mn²⁺ electrolyte. Although C₂H₄ is still evolved throughout all 4 cycles, its overall amount after 4 cycles is only ∼20% of that obtained with the graphite electrode preformed in EC/LiPF₆ electrolyte (viz., 14 μmol/g vs. 69 μmol/g, comparing the orange vs. the yellow lines in Figure 3).

Figure 4a shows the evolution of C₂H₄, H₂, and CO after 4 cycles from all the experiments shown in Figure 3. The gas evolution in the TM-free electrolyte (blue bar) is limited to low amounts of H₂ (∼1 μmol/g), probably from the reduction of newly introduced HF or trace water of the fresh electrolyte, its reduction largely prohibited by the preformed SEI. All of the TM-containing electrolytes evolve more H₂ (∼23 μmol/g (Ni²⁺) and ∼32 μmol/g (Mn²⁺)) for electrodes preformed in EC/LiPF₆; ∼28 μmol/g (Mn²⁺) for electrodes preformed in DMC/2%VC/LiPF₆, suggesting that TM ions can catalyze the reduction of protic species, which is normally hindered by the SEI. While for the electrode cycled in Ni²⁺-containing electrolyte (green bars), only traces of CO (∼1 μmol/g) are observed, the Mn²⁺-containing electrolyte evolves ∼32 μmol/g CO after 4 cycles if preformed in EC/LiPF₆ (yellow bars), lowered to ∼12 μmol/g CO if preformed in DMC/2%VC/LiPF₆ (orange bars).

The corresponding cumulative irreversible capacity for the preformed electrodes after 4 cycles is displayed in Figure 4b. As expected from the gas evolution, the electrode cycled in the TM-free electrolyte (blue bars) shows the lowest irreversible capacity (∼6 mAh/g). For the Ni²⁺-containing electrolyte (green bars), the cumulative irreversible capacity is ∼13 mAh/g, so that the excess irreversible loss (∼7 mAh/g) is rather close to the theoretical capacity required for the 2-electron reduction of all Ni²⁺ ions (∼7.5 mAh/g, see above). The highest irreversible capacity (∼29 mAh/g) comes from the electrode preformed in EC and cycled in Mn²⁺-containing electrolyte (yellow bars); the excess irreversible capacity measured for the EC/LiPF₆ preformed electrode caused by Mn²⁺ (∼23 mAh/g more than in the TM-free electrolyte) is comparable to the additional irreversible capacity in
the experiment with pristine electrodes (~26 mAh/g, see yellow bars in Figure 2b), in agreement with the similar additional total gas evolution (C₂H₄ + H₂ + CO with respect to the TM-free electrolyte) of ~120 µmol/g on preformed electrodes (see yellow bars in Figure 4a) and ~121 µmol/g on pristine electrodes (see yellow bars in Figure 2a). On the contrary, the electrode preformed in DMC/LiPF₆ + 2% VC and cycled in an electrolyte with Mn²⁺ ions (orange bars in Figure 4b) shows a largely reduced irreversible capacity that is only ~7 mAh/g higher compared to the ~6 mAh/g obtained in the TM-free electrolyte, and thus this difference is very close again to the theoretical capacity required for the 2-electron reduction of all Mn²⁺ ions (~7.5 mAh/g, see above). While this additional capacity found for DMC/LiPF₆ + 2% VC preformed graphite in Mn²⁺-containing electrolyte is identical to that for Ni²⁺ -containing electrolyte for EC/LiPF₆ preformed graphite (compare orange vs. green bars in Figure 4b), the additional amount of gas produced in the presence of Mn²⁺ ions is substantially larger (~44 µmol/g vs. ~16 µmol/g; compare orange vs. green bars in Figure 4a) compared to Ni²⁺, suggesting that Mn²⁺ ions more effectively catalyze SEI and/or solvent reduction. The results of Figure 3 and Figure 4 show that the activity of Ni²⁺ ions toward electrolyte reduction is suppressed by an EC-derived SEI, as no significant irreversible capacity or gas evolution is observed. This indicates the passivating effect of the EC-derived SEI on graphite electrodes, as previously observed by Gilbert et al.3 and Jung et al.3 However, additives like VC can help to mitigate the detrimental effect of manganese, as apparently the SEI composition plays a crucial role on the reactivity of manganese toward electrolyte reduction.

Discussion

In order to obtain further insights into the effect of dissolved transition metals on the formation, the passivating properties, and the stability of the SEI on graphite electrodes, we will initially examine the very first voltammometric reduction and oxidation cycle on a pristine graphite electrode. Figure 5 magnifies the current density and plots the C₂H₄ evolution rate (obtained by taking the derivative of the integral OEMS signals) vs. the graphite potential for the first voltammometric cycle shown in Figure 1b. For the TM-free electrolyte (see blue lines in Figures 5a and 5b), the first main reduction peak is observed at ~0.5 V vs. Li⁺/Li, which coincides with a maximum in ethylene evolution rate (see gray-shaded area in Figure 5). This peak appears for all three electrolytes and is ascribed to the reduction of EC to lithium ethylene dicarbonate (LEDIC) and C₂H₄ on graphite.51,52,55,59–63 The electrolyte containing 1.5 µmol Ni²⁺ ions (green lines in Figure 5) shows an additional reduction current already at ~2.5 V vs. Li⁺/Li, merging into a second small reduction current peak at ~1.5 V vs. Li⁺/Li that is accompanied by a first peak in the C₂H₄ evolution rate. Jung et al.3 observed the reduction of Ni²⁺ in a carbonate-based electrolyte at ~2.22 V vs. Li⁺/Li, so that we ascribe the first reduction peak in the Ni-containing electrolyte at ~2.5 V vs. Li⁺/Li (green line in Figure 5a) to the onset of Ni²⁺ reduction. By up-integrating the current density difference between the Ni-containing and the TM-free electrolyte during this initial part of the first reduction scan, it becomes apparent that the ~7.5 mAh/g needed for the reduction of Ni²⁺ to Ni⁰ are only reached at ~1.4 V vs. Li⁺/Li, which suggests that also the second peak around 1.5 V vs. Li⁺/Li belongs to the reduction of Ni²⁺. The concurrent C₂H₄ evolution initiating at below ~1.8 V vs. Li⁺/Li is likely related to a reduction of EC on the nascent Ni⁰ surface, which occurs apparently at higher potentials than the EC reduction on the graphite surface in TM-free EC/LiPF₆ electrolyte (blue line in Figure 5b), initiating at ~0.9 V vs. Li⁺/Li (the same onset potential for C₂H₄ formation was observed for EC/EMC (3/7) with 1 M LiPF₆52 or 1 M LiTFSI).64 Interestingly, after the first two

![Figure 4](image_url)  
**Figure 4.** Total evolved gas and cumulative irreversible capacity (both normalized to graphite mass) over the first 4 cycles of the preformed graphite electrodes in EC/1.5 M LiPF₆ with/without added metal salts, as shown in Figure 3. a) Total evolved C₂H₄ (solid bars), H₂ (dashed bars), and CO (squared bars). b) Cumulative irreversible capacity, with the gray arrow indicating the theoretical charge for 2-electron reduction of the added Ni²⁺ or Mn²⁺ ions. Preformation was done in two different electrolytes: i) EC/1.5 M LiPF₆ for the OEMS experiments in TM-free electrolyte (blue) or electrolyte with either 1.5 µmol Ni(TFSI)₂ (green lines) or 1.5 µmol Mn(TFSI)₂ (yellow); ii) DMC/1.5 M LiPF₆ + 2% VC for the OEMS experiment in electrolyte with 1.5 µmol Mn(TFSI)₂ (orange).

![Figure 5](image_url)  
**Figure 5.** Currents and ethylene evolution rate during the first voltammetric cycle of pristine graphite electrodes in EC/1.5 M LiPF₆ electrolyte without added metal salts (blue lines), with 1.5 µmol Ni(TFSI)₂ (green lines), or with 1.5 µmol Mn(TFSI)₂ (yellow lines). a) Currents normalized to graphite mass (solid lines) and potential (red dashed line); b) integral ethylene evolution normalized to graphite mass. The data are extracted from Figure 1.
reduction peaks (i.e., at 1.25 V vs. Li+/Li), the integrated current accounts to ~7.9 mAh/g, whereas the charge required for the two-electron reduction of the formed C₂H₄ (11.8 μmol/g ≡ 0.63 mAh/g) and CO (9.3 μmol/g ≡ 0.50 mAh/g) together with the reduction of Ni⁴⁺ to Ni²⁺ (7.5 mAh/g) would require a total charge of ~8.6 mAh/g. This suggests that some of the electrolyte must have been reduced chemically rather than electrochemically, possibly via the re-oxidation of Ni⁰ back to Ni²⁺ in a similar mechanism as suggested for manganese.33,39

When Mn²⁺ ions are added (see yellow lines in Figure 5), no additional current peak can be seen, even though the onset for C₂H₄ evolution (~1.1 V) is shifted ~0.2 V more positively compared the TM-free electrolyte. Since the onset for Mn²⁺ reduction was reported to occur at ~1.29 V vs. Li⁺/Li⁺, the more positive onset for C₂H₄ evolution in Mn²⁺-containing electrolyte compared to TM-free electrolyte suggests that EC reduction is catalyzed by Mn⁰ formed at the graphite electrode. Overall, these results with Ni²⁺- and Mn²⁺-containing electrolyte indicate that the earlier onset of C₂H₄ evolution occurs only below the respective reduction potential of the transition metal ions, suggesting that only the reduced transition metals are active toward electrolyte reduction. Rather noteworthy in the case of Mn²⁺-containing electrolyte is that the C₂H₄ evolution rate increases again during the first positive-going potential scan, with a maximum at ~0.1 V vs. Li⁺/Li⁺ (see gray dashed line at 0.1 V vs. Li⁺/Li⁺ in Figure 5), in stark contrast to the vanishing C₂H₄ evolution rate in TM-free or Ni²⁺-containing electrolyte. This is a clear evidence for the SEI decomposing properties of Mn²⁺ in contrast to Ni²⁺.

That transition metals can affect the composition and stability of the SEI on graphite was proposed, e.g., by Joshi et al., who added 10 mM concentrations of each Ni²⁺, Mn²⁺, and CO₂ to a EC/DEC/LiPF₆ electrolyte and found evidence that transition metal ions catalyze the decomposition of LEDC in the SEI to Li₂CO₃, presumably by the release of C₂H₄, CO₂, and O₂. Later on, Leung proposed that Mn²⁺ trapped in the SEI could decompose LEDC to alkoxides by releasing CO₂, which could convert to CO₂ by transferring the excess electron to a solvent molecule. This is consistent with the catalytic effect of Mn²⁺ on SEI decomposition deduced from Figure 3 and Figure 4, where continuous electrolyte decomposition even on a preformed graphite electrode is observed in the presence of Mn²⁺ ions. To better understand how transition metal ions in the electrolyte affect the SEI composition on a preformed electrode (in a TM-free EC/LiPF₆ electrolyte according to the above described procedure), they were transferred without washing into a new cell which we assembled with a fresh separators, a capacitively oversized electrode, and an EC/LiPF₆ electrolyte with 1.5 M LiPF₆. The electrode was cycled in the TM-free EC/LiPF₆ with 5 mL DMC, and then cycled them in the 2-compartment OEMS cell with DMC/LiPF₆ electrolyte containing either 1.5 μmol Mn²⁺ ions or no TM ions. As the reduction of DMC generates CO, but no C₂H₄, we should now be able to differentiate between electrolyte reduction and SEI decomposition. To first test if any EC remains in the pores of the electrode after washing, we additionally soaked a graphite electrode with the EC/LiPF₆ electrolyte, rinsed it, and then cycled it in the TM-free DMC/LiPF₆ electrolyte. Figure 7 shows the current density (a) and the C₂H₄ evolution (b) over the course of 4 voltammetric cycles. The electrode that was stored in EC/LiPF₆ and cycled in DMC/LiPF₆ shows a strong CO evolution (dashed navy colored line), amounting to ~148 μmol/g CO over 4 cycles, as no passivating SEI layer is present; these results are similar to a previous gas evolution study on EMC/LiPF₆ electrolytes by our group, where CO is the only gas evolved upon the reduction of EMC. However, for the EC/LiPF₆ soaked graphite electrode, ~11 μmol/g C₂H₄ (solid navy colored line) is evolved over the 4 cycles, which originate from the remaining EC that could not be removed by the washing step (however, still a minor amount compared to the evolved CO). In contrast, the preformed electrode that was cycled in the TM-free DMC/LiPF₆ electrolyte (superimposing blue solid and dashed lines in Figure 7) shows neither CO nor C₂H₄ (<0.1 μmol/g), meaning that the SEI has not been damaged due to the washing process.

Lastly, the yellow lines in Figure 7 show the behavior of the preformed graphite electrode cycled in the Mn²⁺-containing DMC/LiPF₆ electrolyte. In this case, both CO and C₂H₄ are evolved throughout
all 4 cycles. As the C$_2$H$_4$ evolution from the Mn$^{2+}$-containing electrolyte is $\sim$30 μmol/g after 4 cycles (see solid yellow line in Figure 7b) while the EC residuals from the EC-soaked electrode account to only $\sim$11 μmol/g C$_2$H$_4$ (see solid navy line in Figure 7b), we hypothesize that this additional $\sim$19 μmol/g C$_2$H$_4$ originate from the decomposition of LEDC. This LEDC-derived amount of C$_2$H$_4$ may be compared to the higher amount of $\sim$69 μmol/g C$_2$H$_4$ evolved for an identically preformed graphite electrode but cycled in EC/LiPF$_6$ electrolyte in a separate cell vs. an LFP cathode (2 cycles at C/8); harvested electrodes were washed with DMC prior to building the 2-compartment OEMS cells. To determine the efficacy of the washing procedure, a pristine graphite electrode soaked in EC/1.5 M LiPF$_6$ electrolyte and then washed was also examined (dark purple lines). The voltammetric cycles at 0.2 mV/s were done between 0.1–3.0 V vs. Li$^+$/Li, starting from OCV ($\sim$2.9 V vs. Li$^+$/Li),

The Mn$^{2+}$ ion can now accept further electrons and pass them on to surrounding LEDC or EC molecules (5), thereby leading to a catalytic cycle of electrolyte decomposition and active lithium loss from the lithiated graphite. This cycle can continue until the Mn$^{2+}$ ion is eventually fully encapsulated by non-reducible decomposition products, so that an electron transfer from the lithiated graphite is no longer feasible. As Wandt et al.4 found manganese almost exclusively in its 2+ oxidation state by operando XAS, the re-oxidation of Mn$^{2+}$ to Mn$^{2+}$ must be faster than the reduction of Mn$^{2+}$, i.e., the diffusion within the SEI and the electron transfer (steps 2 and 5 in Scheme 1) are the rate-limiting steps.

While both nickel and manganese have shown activity toward electrolyte decomposition in their reduced state (i.e., on pristine electrodes, see Figure 1), the presence of a preformed SEI greatly suppressed the effect of Ni$^{2+}$-containing electrolyte on both gas evolution (see Figure 3b, green line) and the enrichment of Li$_2$CO$_3$ in the SEI (see Figure 6, green line). Hence, we can assume that the diffusion and/or the electron transfer of Ni$^{2+}$ within the SEI is slowed down compared to Mn$^{2+}$. As suggested by Shkrob et al.,38 it is possible that nickel and manganese are not fully reduced, but only one electron is transferred through the SEI to the transition metal ion. DFT-calculations by Leung,50 indicate that a Ni(I) species is far less likely to transfer an electron to neighboring SEI molecules compared to its Mn(I) counterpart. In this case, the catalytic cycle for Ni would be effectively interrupted. Additionally, Wandt et al.4 found that Mn$^{2+}$ in the SEI is reduced within minutes once the electrolyte is completely removed, whereas nickel stays in its 2+ state. As the reduction potential of Ni$^{2+}$/Ni is $\sim$1 V higher than the reduction potential of Mn$^{2+}$/Mn,54 the electron transfer from lithiated graphite to Ni$^{2+}$ should have a higher thermodynamic driving force. Hence, another possible reason for the apparent difference between Ni and Mn is that the Li$^+$/Ni$^{2+}$ exchange and the diffusion of Ni$^{2+}$ within the SEI is much slower compared to Mn$^{2+}$.

For Li-ion batteries, this has two implications: i) The same amount of TM dissolution leads to less severe capacity fading if the cathode active material is Ni-rich and Mn-poor, which is advantageous for Ni-rich NMCs and especially Mn-free NCA (as seen by Gilbert et al.7); ii) future additive design should focus on the formation of an SEI which enables Li$^+$ ion transport while slowing down the diffusion of all transition metal ions, or which form SEI products which consist of chemically stable species that cannot be further reduced. In this context, a thermally aged SEI that contains more LiF and other
stable inorganic species\textsuperscript{75} might be more robust toward the detrimental side reactions induced by manganese ions. However, as Mn\textsuperscript{2+} rapidly exchanges with Li\textsuperscript{+} from LiPF\textsubscript{6} in the SEI\textsuperscript{25,37} a high Li\textsuperscript{+} content will likely not act as a barrier for Mn\textsuperscript{2+} diffusion.

Conclusions

In this work, we applied on-line electrochemical mass spectrometry (OEMS) to follow the reactions triggered by manganese and nickel that ultimately lead to the loss of active lithium and poor capacity retention in full-cells. For the first time, we have investigated the effect of Mn\textsuperscript{2+} and Ni\textsuperscript{2+} on the gassing behavior of graphite, using EC/LiPF\textsubscript{6} model electrolytes with Mn(TFSI)\textsubscript{2} or Ni(TFSI)\textsubscript{2} in a 2-compartment cell. Both manganese and nickel significantly increase the C\textsubscript{2}H\textsubscript{4} evolution and ethylene carbonate (EC) reduction on pristine graphite electrodes. Furthermore, the Mn\textsuperscript{2+}-containing electrolyte showed an ongoing EC reduction and C\textsubscript{2}H\textsubscript{4} evolution throughout several cycles after formation.

As a second step, we investigated the effect of Mn\textsuperscript{2+} and Ni\textsuperscript{2+} on graphite electrodes which already featured an SEI by preforming them in a TM-free electrolyte. We found that the effect of nickel is greatly suppressed by the SEI, whereas manganese showed almost the same activity toward electrolyte reduction as on pristine electrodes. However, a preformation in a VC-containing electrolyte could significantly lower the side reactions caused by Mn\textsuperscript{2+} ions. As this showed that the SEI chemistry plays a crucial role, we found by post-mortem ATR-FTIR spectroscopy that the graphite electrodes cycled in an Mn\textsuperscript{2+}-containing electrolyte consisted of more Li\textsubscript{2}CO\textsubscript{3} compared to electrodes cycled in an electrolyte with Ni\textsuperscript{2+} ions or no transition metals. Further OEMS experiments with preformed graphite electrodes and a DMC electrolyte (which allowed us to distinguish between electrolyte reduction and SEI decomposition) indicated that Mn\textsuperscript{2+} leads to the decomposition of LDEC to C\textsubscript{2}H\textsubscript{4} and Li\textsubscript{2}CO\textsubscript{3}; however, the major part of the gas evolution still originated directly from the electrolyte reduction. Our results suggest that cathode active materials containing inorganic species\textsuperscript{75} might be more robust toward the detrimental effects of transition metal dissolution, and that SEI-stabilizing additives can be an efficient way to decrease the side reactions caused by transition metal ions in Li-ion batteries.

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ORCID

Sophie Solchenbach  https://orcid.org/0000-0001-6517-8094
Roland Jung  https://orcid.org/0000-0003-1135-7438

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