Thermodynamic Evaluation of Equilibrium Oxygen Composition of UO$_2$-Mo Nuclear Fuel Pellet Under High Temperature Steam

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Micro-plate or microcell UO$_2$–Mo is considered a promising accident tolerant fuel candidate for water-cooled power reactors. In this work, we evaluated the anticipated oxidation behavior of a UO$_2$–Mo system under high-temperature steam to understand the impact of Mo oxidation on the fuel degradation mechanism in the event of steam ingress through cracks in the cladding. The equilibrium oxygen compositions of UO$_2$ and Mo in various steam atmospheres relevant to reactor operating conditions were predicted using thermodynamic calculations and then compared with previous results. The oxidation behavior of UO$_2$–Mo pellets was discussed through thermodynamic calculations and in terms of kinetic parameters such as oxygen diffusion, fuel temperature profile, and pellet microstructure. Mo oxidation was found to have an insignificant effect on pellet integrity in a cladding leakage scenario under normal reactor operating conditions.

Keywords: accident tolerant fuel, UO$_2$–Mo pellet, steam oxidation, equilibrium composition, oxygen potential

INTRODUCTION

UO$_2$–Mo micro-plate or microcell pellets, in which small amounts of molybdenum metal particles are arranged in the form of directionally aligned plates or continuous networks, are actively studied worldwide as a promising accident tolerant fuel candidate for light water reactors, because they have improved thermal conductivity (Kim et al., 2017; Kim et al., 2018; Buckley et al., 2019; Cheng et al., 2019; Finkeldei et al., 2019; Cheng et al., 2020; Lee et al., 2020). This fuel design might be easily implemented in nuclear power plants in the near term, as it inherits the superior safety performance of UO$_2$ nuclear fuel and can leverage existing knowledge and infrastructure.

To successfully implement the micro-plate or microcell concepts in a UO$_2$ pellet, research is underway on addressing various technical issues. A conventional pressure-less sintering process has been established to produce composite pellets with a specific microstructure (Kim et al., 2017; Kim et al., 2018). From an economic perspective, the fuel cycle length in a UO$_2$–Mo system is reduced because the addition of Mo reduces U loading, and Mo has a larger neutron absorption cross-section. The neutron penalty is partly mitigated by limiting the Mo addition to less than 3 vol%. The lower fuel operating temperature owing to the improved thermal conductivity is conducive to neutron utilization owing to the MTC feedback effect (Jo et al., 2020). Preliminary calculation showed that UO$_2$–3vol% Mo fuel with a U235 enrichment of 4.95% can achieve the same fuel cycle length as that in a 4.65% enriched UO$_2$ fuel.

Phase equilibria serve as a basis for the manufacturing and performance characterization of nuclear fuels. In particular, a comprehensive understanding of phase equilibrium and
thermochemical properties is essential to support licensing by providing data on changes in the thermophysical properties, irradiation damage, and behavior of fission products. Chemical reactions between fuel materials and the atmosphere can result in fuel degradation and is one of the main factors governing nuclear fuel performance. During irradiation in a nuclear reactor, fuel pellets can in two states where the partial pressure of oxygen in the environmental gas increases. The first state is during normal operation. The oxygen separated from UO$_2$ by the fission of U increases the oxygen potential of the atmosphere in the fuel rod (Spino and Peerani, 2008). Another state is the ingress of steam through a damaged fuel cladding. The coolant flows into the hot fuel rod and vaporizes, and the steam is decomposed to generate oxygen, which increases the oxygen partial pressure inside the fuel rod. Thermodynamically, Mo has a high oxygen affinity and can undergo oxidization and evaporation when exposed to a high-temperature atmosphere containing oxygen. If UO$_2$–Mo pellets are oxidized in a leakage scenario (e.g., cladding breach), the oxidation and evaporation of Mo and the resulting volume expansion of the fuel pellets may cause fuel rod failure and exacerbate the accident.

The aim of this study was to evaluate thermodynamically the change in the equilibrium oxygen composition of UO$_2$–Mo pellets when exposed to high-temperature steam. The impact of Mo oxidation on the degradation behavior of UO$_2$ pellets in the event of a cladding breach is also discussed. Our preliminary assessments are expected to contribute to the evaluation of this material for use as an accident-tolerant fuel.

**CALCULATION OF OXYGEN PARTIAL PRESSURE IN STEAM GAS UNDER VARIOUS CONDITIONS**

In fuel rod failure scenarios, UO$_2$ pellets are exposed to steam at high temperatures and high pressures. In this environment, UO$_2$ pellets oxidize to a composition that is in equilibrium with the gas phase. To calculate the equilibrium deviation from the stoichiometry of UO$_2$, it is necessary to know the partial pressure of oxygen in the environment. The oxygen partial pressure of the gas is determined by the temperature, gas composition, and pressure. Under normal operating conditions, the fuel temperature is typically in the range of 400–1,300°C. The internal pressure of the damaged fuel rod is equivalent to a typical reactor operating pressure of 150 atm. Regarding the composition of the gas introduced into the rod, the steam is mixed with hydrogen produced during the oxidation reaction of steam with Zr (Garzarolli and Stehle, 1979; Review of Fu, 2010). Previous studies reported that the highest deviation from the stoichiometry (x in UO$_{2+x}$) for the pellets in the damaged fuel rods is approximately 0.1 (Une et al., 1995; Kim, 2003; Verrall et al., 2005; Higgs et al., 2007). This deviation implies that some amount of hydrogen is mixed in the introduced steam and that the hydrogen composition varies depending on the location in the fuel rod. Considering the typical operating conditions and anticipated steam compositions, the equilibrium oxygen partial pressure with respect to the temperature was calculated under different hydrogen contents of the mixed steam gas (0, 10, and 1,000 ppm).

Two calculation procedures were applied to obtain the equilibrium oxygen partial pressures in this study: 1) The Gem module from HSC Chemistry 9 (HSC Chemistry 9, 2018), which utilizes the built-in Gibbs energy minimization method, and 2) Olander’s transcendental equation (Olander, 1986). According to the Olander’s transcendental equation, the oxygen partial pressure ($p_{O_2}$) in the steam and hydrogen mixture can be estimated using the following expression:

$$K_i(p_{O_2})^{1/2} \left[ \left( \frac{Q}{2} - 1 \right) + \left( \frac{Q}{2} + 1 \right) \frac{p_{O_2}}{p_i} \right] = 1 - (Q + 1) \left( \frac{p_{O_2}}{p_i} \right)$$

where,

$$K_i = \exp \left( - \frac{\Delta G}{RT} \right), \quad \Delta G = -250800 + 57.8T \text{ (J/mol)}$$

$R$ is the universal gas constant (8.3145 J/mol-K), and $p_i$ is the total system pressure. The hydrogen-to-oxygen atom ratio ($Q$) of the environment is given by

$$Q = 2 \left( 1 + \frac{n_{H_2}}{n_{H_2O}} \right)$$

**Figure 1** shows the calculated variation in the oxygen partial pressures as a function of temperature for steam and steam–hydrogen mixtures at 1 and 150 atm. For pure steam, the oxygen partial pressure calculated by Olander’s formula agrees well with that obtained using the HSC9 program. However, for the steam–hydrogen mixture, the oxygen partial pressures obtained from Olander’s solution were slightly lower. Many previous studies have used Olander’s equation to evaluate the equilibrium oxygen partial pressure of steam–hydrogen mixed gases. In this study, Olander’s solution was used to estimate the equilibrium oxygen composition to ensure consistency with previous results.

**Figure 2** shows the equilibrium oxygen partial pressures of the mixed steam as a function of temperature at pressures of 1 and 150 atm obtained by Olander’s solution. The mixing of a small amount of hydrogen significantly reduces the equilibrium oxygen partial pressure of the steam. However, as the temperature increases, the oxygen partial pressure difference between the pure steam and the mixture gradually narrows because of the decomposition reaction of the steam. Evidently, in pure steam, the oxygen partial pressure increases with increasing pressure in the calculated temperature range. In the case of the mixed gas, the pressure has little effect in the low-temperature region. Above a certain temperature, however, the oxygen concentration increases because of the
decomposition reaction of the steam, thereby increasing the oxygen partial pressure at high pressures.

EVALUATION OF EQUILIBRIUM OXYGEN COMPOSITIONS OF UO₂ AND Mo AT HIGH TEMPERATURE STEAM AND STEAM-HYDROGEN MIXTURES

The equilibrium oxygen composition of U–O and Mo–O systems can be estimated using the oxygen partial pressures of the environment and $p$-$C$-$T$ ($pO_2$-composition-temperature) diagram. Figure 3 shows the phase diagram of the U–O system with oxygen pressure isoatms, presented by Kim (Kim, 2000). Figure 2 indicates that the equilibrium oxygen partial pressure of pure steam at 1000 K and 1 atm is approximately $1 \times 10^{-7}$. At this oxygen partial pressure, $\text{U}_3\text{O}_{8-x}$ is in a stable oxide phase, as denoted by point B (red dot) in Figure 3. On the other hand, at 1500 K, the equilibrium oxygen partial pressure increases to approximately $1.2 \times 10^{-4}$, and the corresponding equilibrium phase should be $\text{UO}_2^{3+}$ as marked by point A (blue dot) in Figure 3.

Figures 4A,B show the phase stability diagrams of the U–O system constructed using thermodynamic equations established

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**FIGURE 1** | Comparison of equilibrium oxygen partial pressures of steam and steam–hydrogen mixed gases as a function of temperature for total pressures of (A) 1 atm and (B) 150 atm, calculated through the HSC9 program (HSC Chemistry 9, 2018) and Olander’s equation (Olander, 1986).

**FIGURE 2** | Effects of H₂ mixing and pressure on the equilibrium oxygen partial pressures of steam calculated by Olander’s equation (Olander, 1986).

**FIGURE 3** | The phase diagram of the U–O system with oxygen pressure isoatms, presented by Kim (Kim, 2000).

**FIGURE 4** | The phase stability diagrams of the U–O system constructed using thermodynamic equations established.
FIGURE 3 | Variation in the equilibrium oxygen stoichiometry with temperature of the U–O system in pure steam atmosphere. The points A (blue dot) and B (red dot) indicate the equilibrium oxygen partial pressures of pure steam at 1500 and 1000 K, respectively. The U–O phase diagram is from Ref. (Kim, 2000).

FIGURE 4 | U–O stability diagram and equilibrium oxygen potentials of steam and steam–hydrogen mixed gas. U–O stability boundary is constructed using (A) thermodynamic equations in Ref. (Kim, 2000), and (A) Tpp module in HSC9 Chemistry (HSC Chemistry 9, 2018).
Figure 4 reveals that reducing the pressure or mixing a small amount of hydrogen in the steam can help prevent UO2 pellets from being oxidized to U3O8. The two stability diagrams shown in Figures 4A and 4B are similar but not entirely consistent. As shown in the stability diagram of Figure 4A obtained using HSC9, the UO2 pellets pulverize to U3O8 when exposed to steam at a pressure of 150 atm and a temperature below 1373 K. This temperature limit is ~200 K lower than that shown in Figure 4A.

Figure 5 shows detailed variations in the calculated equilibrium O/U ratio of the U–O system with the steam composition, pressure, and temperature. The equilibrium O/U ratio was calculated using the equations presenting the best p–C–T relationship proposed by Kim (Kim, 2000). As expected, in Figure 4A, the O/U ratio of pure steam abruptly changes at the stability boundary temperature between the cubic phases (UO2+x, U4O9−y), and U3O8. When the steam-to-hydrogen ratio (H2O/H2) is 100,000, the cubic phase is stable over the calculated temperature range, and no U3O8 phase is expected. Since the oxygen potential curve of this gas is closest to the stability boundary at approximately 1273 K, the equilibrium O/U ratio shows a parabolic shape with a peak value located in the temperature range of approximately 1,273–1,373 K. When the hydrogen content is increased further (H2O/H2 = 1,000), the oxygen potential of the atmosphere is largely reduced, and consequently, the equilibrium O/U ratio decreases. Published experimental data (Abrefah et al., 1994; Hashizume et al., 1999; Lewis et al., 1990; Cox et al., 1986) on O/U ratio variations following UO2 oxidation in steam and steam–hydrogen mixture are compared in Figure 5A. The experimental data measured above 1273 K are in good agreement with the calculated values. While several experimental datasets on the equilibrium O/U ratio exist for steam oxidation of UO2 pellets above 1273 K, few data are available for steam oxidation below 1273 K owing to the slow oxidation of UO2 at low temperatures and the challenges related to controlling the steam–hydrogen composition. Kuhlman (Kuhlman, 1948) found no significant weight change in UO2 after exposure to oxygen-free steam at 873 K for 6 h. Bittel et al. (Bittel et al., 1969) reported that the final average O/U ratio of pellets annealed at 1158 K for 290 min in steam was 2.039, which is far below the calculated value. On the contrary, Dumitrescu et al. (Dumitrescu et al., 2015) reported that UO2 pellets pulverize to U3O8 after annealing in 873 K steam for 10 h. Recently, Jung et al. (Jung et al., 2020) have also shown the formation of U3O8 particles on the UO2 pellet annealed for 1,000 min in steam maintained at a temperature range of 673–733 K. This discrepancy between the experimental results appears to be due to the very slow oxidation reaction in low-temperature steam and the strong influence of the oxygen and hydrogen contents on the equilibrium oxygen potential of the steam.

The melting point of pure molybdenum is 2896 K. However, the formation of low-melting-temperature oxides is the drawback of this refractory metal. The Mo–O temperature–concentration diagram shows various molybdenum oxides, where the principal stable oxide phases in the Mo–O system are MoO3 (Tm = 1073 ± 5 K) and MoO2 (Tm = 2600 ± 100 K) (Brewer and Lamoreaux, 1980).

The phase stability diagrams for the Mo–O system with the variations in the temperature and oxygen partial pressure have been presented by several researchers (Chen et al., 2018; Lee et al., 2019a; Zhang et al., 2014). Figure 6 shows the stability diagrams applied in this study, plotted using the Tpp module in HSC9 program (HSC Chemistry 9, 2018). The stability diagram is similar to that prepared by Chen (Chen et al., 2018) using...
FactSage 6.2 (GTT Technologies, Germany) and that calculated by Lee (Lee et al., 2019a) using meta-generalized-gradient approximation and hybrid density functional theory calculations. Zhang et al. constructed a Mo–O stability diagram using the CALPHAD method (Zhang et al., 2014). However, the stability diagram differs considerably from that shown in Figure 6, characterized by a narrower area of stability for solid oxides.

The oxygen partial pressure or equilibrium oxygen potential curves were superimposed on these figures to assess the anticipated equilibrium oxygen composition of the Mo–O system when exposed to atmospheres as those shown in Figure 2. Figure 6 indicates that MoO$_3$ is a stable oxide in pure steam. Therefore, when Mo is exposed to steam, it will oxidize to MoO$_3$, becoming a liquid above 1073 K and vaporizing above 1428 K. Indeed, the oxidation test of Mo in 100% steam showed a rapid weight loss above 1073 K (Nelson et al., 2014). The oxidation behavior of Mo changes significantly even when very small amounts of hydrogen is added to the steam. As shown in Figure 6, in 150 atm steam mixed with 1,000 ppm of hydrogen, the equilibrium oxide composition is MoO$_2$, and a liquid phase is formed at approximately 1673 K, which is approximately 600 K higher than that in the case of pure steam. The effect of hydrogen content in steam on the oxidation of Mo has been determined at 1273 K. The test result shows that the material loss rate can be meaningfully reduced by adding hydrogen to the steam, consistent with the effect of hydrogen predicted and shown in Figure 6 (Nelson et al., 2014).

**PREDICTION OF THE OXIDATION BEHAVIOR OF UO$_2$-Mo PELLETS IN THE EVENT OF CLADDING BREAKAGE DURING THE NORMAL OPERATION**

The oxidation behavior of UO$_2$ and Mo in various steam atmospheres relevant to reactor operating condition was studied independently. In this section, the oxidation behavior of UO$_2$–Mo pellets is predicted when steam is introduced into the fuel rod through cladding leaks under reactor operating conditions.

Figure 7 shows a comparison of the calculated temperature profile along the radial direction between conventional UO$_2$ and micro-plate UO$_2$–3vol% Mo pellets operating at a linear heat generation rate of 30 kW/m. The temperature gradient of the UO$_2$ pellets was calculated using the thermal conductivity model from the MATPRO handbook (Hagrmann and Reymann, 1979). The temperature profile of UO$_2$–3vol% Mo pellets was calculated using the measured thermal conductivity of the pellet in which Mo plates with an average diameter of $\sim$45 μm and an average thickness of $\sim$1.5 μm were dispersed in UO$_2$ (Kim et al., 2020). The thermal conductivity of both pellets was corrected to 95% of the theoretical density for temperature calculation.

Since the thermal conductivity is more than 80% higher than that of UO$_2$ pellets, the operating temperature is significantly reduced in the case of the UO$_2$–3vol% Mo pellet. The centerline
temperature of UO₂−3vol% Mo is calculated to be 1093 K, approximately 300 K lower than that of UO₂.

As shown in Figure 5, the high-pressure steam ingress into the fuel rod pulverizes the UO₂ pellets, and consequently, the fuel rods are severely damaged because of the volume expansion and fission gas release. However, the fuel failure mechanism due to the oxidation of UO₂ pellets has not been reported thus far. In fact, the secondary failure mechanisms observed in defective fuel rods were mostly due to the formation of ZrO₂ or ZrH₂ ([2010]. Review of Fu, 2010). As mentioned in Calculation of Oxygen Partial Pressure in Steam Gas Under Various Conditions, this fact reveals that the steam introduced to the fuel rod is mixed with hydrogen and consequently has a much lower oxygen partial pressure than pure steam.

Assuming a constant thermal conductivity of the fuel pellets during the oxidation reaction, the oxidation behavior of UO₂−3vol% Mo pellets operating at a 30 kW/m when exposed to 150 atm steam mixed with hydrogen can be predicted as follows. Figures 4, 5 indicate that the equilibrium oxygen composition deviation from stoichiometric UO₂ (x in UO₂+x) is ~0.22 and decreases toward the pellet periphery, when the hydrogen content in the steam is 10 ppm. The equilibrium phase of Mo under this condition is MoO₂, which has a melting temperature of ~1193 K, as shown in Figure 6. When the hydrogen content in the steam increases to 1,000 ppm, the maximum deviation of x in UO₂+x decreases to less than 0.02, and the melting temperature of MoO₂ increases to ~1673 K. The theoretical densities of Mo, MoO₂ and MoO₃ are 10.28, 6.47, and 4.69 g/cm³, respectively. The lattice parameters of UO₂+x are known to contract linearly with an increase in x, and the contraction factor (line slope) is in the range of ~0.132 and ~0.07 Å, depending on temperature and x (Perio, 1955; Rachev et al., 1965; Belbeoch et al., 1967; Touzelin and Dode, 1969; Teske et al., 1983; Yakub et al., 2009). Considering the specific situation where only Mo is oxidized to MoO₂ in UO₂−3vol% Mo pellet, the pellet will show a volume increase of up to 3.6%. However, in that situation, UO₂ is also oxidized to UO₂+x, so the volume expansion due to MoO₂ formation is offset by the volume reduction due to oxidation of UO₂. If we assume the oxidation reaction terminated with the formation of solid MoO₂ and UO₂+x, and the contraction factor is ~0.07 Å, the volume of the pellet will be increased by about 3%. When the oxidation reaction with the steam-hydrogen mixture is completed and the pellet reaches an equilibrium state, the pellet volume is expected to increase to less than 3%, considering the volume expansion due to MoO₂ formation and volume reduction due to UO₂ oxidation. Moreover, no liquid phase is expected in the equilibrium state because the maximum pellet temperature is much lower than the melting temperature of MoO₂.

The diffusion mobility of oxygen as well as the kinetic parameters should also be considered in the prediction of the oxidation behavior. Higgs et al. have developed a theoretical model to evaluate the UO₂ pellet oxidation behavior in operating defective fuel elements, taking into account multi-phase transport including oxygen diffusion by both chemical and thermal gradients and steam-hydrogen transport along gap and in fuel cracks (Higgs et al., 2007).

Thermomechanical fracture owing to the temperature gradient dominates the formation of primary radial cracks in UO₂ pellets under irradiation (Oguma, 1983; Lee et al., 2019b; Li and Shirvan, 2021). The number of cracks measured under various out-of-pile conditions in the UO₂ pellet is roughly proportional to linear power of the fuel rod (Oguma, 1983). Multiphysics phase-field modeling of quasi-static cracking in UO₂ pellet showed typically eight primary radial cracks are developed and interconnected during the reactor startup and cooling (Li and Shirvan, 2021). In the case of UO₂-Mo composite pellet, lower temperature gradient would reduce the thermal hoop stress, thereby decreasing pellet region where the thermal hoop stress is higher than fracture stress of UO₂ (Lee et al., 2019b), suggesting the UO₂-Mo could be more resistant to cracking than the UO₂ pellet even for the same linear power, as was observed in U₃Si₂ fuel (Cappia and Harp, 2019). However, the composite structure would probably have insignificant effect on cracking behavior because the volume fraction of Mo plates or Mo wall is just 3% and its thickness is only several micrometers. Therefore, the linear power will be a dominant factor in the cracking behavior and, if the temperature gradients between the UO₂ and UO₂-Mo pellets are the same, the crack patterns observed in both pellets are expected to be similar to each other.

Two assumptions have been made. First, the UO₂-3 vol% Mo pellet are fragmented into eight parts by eight primary radial cracks that penetrate the center. Second, considering the average diameter of Mo plates (~45 μm), the Mo particles located within 50 μm of the fragments surface will be exposed to environment directly. Under the circumstance, it is calculated that about 0.45 vol% of Mo among the 3 vol% of Mo will directly contact with steam transported along the gap and fuel cracks, and the remaining 2.55 vol% of Mo will be embedded in the UO₂ matrix.

The oxidation reaction of the Mo plates embedded in the UO₂ matrix will be governed by oxygen diffused through UO₂ lattice or grain boundaries. Therefore, oxygen diffusion inside the UO₂ matrix is an important parameter that needs to be considered to better understand the influence of Mo on oxidation behavior. Considering the diffusion distance for oxygen to reach the Mo surface via the dense UO₂ and the low lattice diffusion rate owing to the low pellet temperature of less than 1093 K (Bittel et al., 1969), relatively long incubation time seems to be required for the Mo inside the pellet fragment to meet with oxygen and start the oxidation reaction. The MoO₂ layer is known to adhere to the Mo surface and act as an anti-corrosion layer, so the formation of a MoO₂ surface layer is expected to further delay the oxidation rate. Therefore, the oxidation reaction rate of Mo by oxygen diffusion is expected to be low, particularly in the outer region of the pellet with low temperature. In contrast to the Mo plate inside the pellet fragment, the Mo plate located near the pellet periphery or fragment surface would be rather quickly oxidized even at low temperature by direct contact with the steam introduced through the cladding defects, gas gaps and fuel cracks. In particular, the volume expansion due to preferential oxidation of Mo possibly develops secondary cracks on the surface, and steam can penetrate through the cracks to accelerate oxidation. However, the rapid oxidation of exposed Mo is expected to be confined to a small number of pellets located around the defect. The experimental and computational results showed that O/U ratio of a fuel rod located at opposite side of or far from the defect is much lower than that of pellet near the defect (Ume et al., 1995; Kim, 2003; Verrall et al., 2005; Higgs et al., 2007). The steam-hydrogen transport rate,
another important parameter controlling the rate of reaction, is probably limited in the opposite area of the pellet to defect or at a location away from the defect. In particular, the hydrogen concentration increases where the gas transports is stagnant, and then, the local oxidation rate is further delayed.

There was a concern about the accelerated degradation of UO₂–Mo fuel rods due to the oxidation of Mo in a cladding leakage scenario. However, a thermodynamic evaluation showed that the equilibrium composition of Mo is the solid phase of MoO₂, and the maximum volume expansion of a pellet due to the complete oxidation of Mo to MoO₂ is estimated to be less than 3%. Given the low fuel temperature and the microstructure of the pellets, where most of Mo is imbedded in UO₂ matrix, and considering UO₂ pellet oxidation behavior in operating defective fuel element (Garzarolli and Stehle, 1979; Review of Fu, 2010; Une et al., 1995; Kim, 2003; Verrall et al., 2005; Higgs et al., 2007), it will take a long time for Mo to reach the equilibrium composition of MoO₂ and the volume expansion of the pellet will also proceed gradually. Therefore, the effect of Mo oxidation on the pellet integrity in a cladding leakage scenario is expected to be insignificant.

The thermodynamic prediction of the oxidation behavior was evaluated under the assumption that the thermal conductivity of the pellet remains constant and that there are no reactions at the UO₂/ MoO₂ interface. However, the thermal conductivity may decrease depending on the degree of oxidation of UO₂ and Mo, and the formation of new compounds has an additional effect on the volume change. Subsequently, the pellet temperature will increase, and the oxidation behavior of the fuel rod may vary. U-Mo-O ternary compounds, which are possibly formed at the UO₂/Mo interface, would influence the oxygen transport and thus the oxidation behavior of the pellets. When the thermal conductivity decreased and fuel temperature increased, Mo oxides in the central region of pellet might form liquid or vapor phases. Those phases can negatively affect the integrity of the fuel rods by increasing the fuel internal pressure and reacting with pellet and cladding. Therefore, to accurately assess the fuel behavior, further experimental studies are required to obtain data on the diffusion mobility of oxygen near the phase boundary between UO₂ and Mo, reactions at the UO₂/Mo and UO₂+x/MoO₂ interfaces (Bharadwaj et al., 1984; Sarrasin et al., 2019), phase equilibria in U-Mo-O ternary system and the change in the thermal conductivity with the degree of oxidation. Multiple and complex chemical reactions, including cladding and fission products, as well as interactions between UO₂-Mo and steam are expected to occur under accidents such as loss of coolant or station black out. Although the volume fraction of Mo in UO₂ is small (3%), which is expected to have a limited impact on accident progress, integral test of fuel rods is required to understand the behavior of UO₂-Mo pellets and their interactions with cladding in the event of accidents.

CONCLUSION

The oxidation behavior of a UO₂–Mo system in a steam atmosphere relevant to reactor operating conditions was evaluated through thermodynamic calculations for a preliminary assessment of the impact of Mo oxidation on the fuel behavior of UO₂–Mo pellets in the event of steam ingress through cracks in the cladding. In the thermodynamic equilibrium state, the oxidation reaction is terminated with the formation of solid MoO₂ and hyper-stoichiometric UO₂+x, and the volume expansion after the termination of the reaction is estimated to be less than 3%. In terms of the kinetic parameters, such as the steam-hydrogen flow, fuel temperature, and cracked-pellet microstructure, the impact of Mo oxidation on the fuel integrity in a cladding leakage scenario is expected to be insignificant. Limitations of the current preliminary thermodynamic assessment include the thermal conductivity degradation due to the formation of U-Mo-O compounds, steam/hydrogen transports along the fuel cracks and gap, and simplified thermo-mechanical cracking behavior. Future experimental study would include the oxidation behavior of Mo located near fuel crack and inside UO₂ under the anticipated oxygen potential, the microstructure change after the mechanical cracks or during the oxidation, and the variation of effective thermal conductivity owing to the formation of Mo-oxides and U-Mo-O compounds. Integral test using fuel and cladding assembly would also be necessary to estimate the effect of steam/hydrogen mixed gas transport in the defective fuel rod and its local composition on the overall oxidation behavior of UO₂-Mo-Zr fuel system. Combining the thermodynamic evaluation in this study with experimental data in the future, it will be possible to simulate the behavior of fuel rods in the event of a cladding breach.

DATA AVAILABILITY STATEMENT

The original contributions presented in the study are included in the article/Supplementary Material, further inquiries can be directed to the corresponding author.

AUTHOR CONTRIBUTIONS

JHY: Conceptualization, Methodology, Calculation, Visualization, Writing-Original draft, Review and; Editing. KWS: Methodology, Data collection, Review and; Editing. DSK: Methodology, Data collection, Review and; Editing. D-JK: Methodology, Data collection, Review and; Editing. HSL: Methodology, Data collection, Review and; Editing. J-HY: Methodology, Data collection, Review and; Editing. Y-HK: Methodology, Review and; Editing.

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**Conflict of Interest:** The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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