Mechanism of CaF$_2$ under Vacuum Carbothermal Conditions for Recovering Nickel, Iron, and Magnesium from Garnierite

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Abstract: Nickel laterite ore is divided into three layers and the garnierite examined in this study belongs to the third layer. Garnierite is characterized by high magnesium and silicon contents. The main contents of garnierite are silicates, and nickel, iron, and magnesium exist in silicates in the form of lattice exchange. Silicate minerals are difficult to destroy so are suitable for smelting using high-temperature pyrometallurgy. To solve the problem of the large amounts of slag produced and the inability to recycle the magnesium in the traditional pyrometallurgical process, we propose a vacuum carbothermal reduction and magnetic separation process to recover nickel, iron, and magnesium from garnierite, and the behavior of the additive CaF$_2$ in the reduction process was investigated. Experiments were conducted under pressures ranging from 10 to 50 Pa with different proportions of CaF$_2$ at different temperatures. The experimental data were obtained by various methods, such as thermogravimetry, differential scanning calorimetry, scanning electron microscopy, energy dispersive spectrometry, X-ray diffraction, and inductively coupled plasma atomic emission spectroscopy. The analysis results indicate that CaF$_2$ directly reacted with Mg$_2$SiO$_4$, MgSiO$_3$, Ni$_2$SiO$_4$, and Fe$_2$SiO$_4$, which were isolated from the bearing minerals, to produce low-melting-point compounds (FeF$_2$, MgF$_2$, NiF$_2$, etc.) at 1315 and 1400 K. This promoted the conversion of the raw materials from a solid–solid reaction to a liquid–liquid reaction, accelerating the mass transfer and the heat transfer of Fe–Ni particles, and formed Si–Ni–Fe alloy particles with diameters of approximately 20 mm. The smelting materials appeared stratified, hindering the reduction of magnesium. The results of the experiments indicate that at 1723 K, the molar ratio of ore/C was 1:1.2, the addition of CaF$_2$ was 3%, the recovery of Fe and Ni reached 82.97% and 98.21% in the vacuum carbothermal reduction–magnetic separation process, respectively, and the enrichment ratios of Fe and Ni were maximized, reaching 3.18 and 9.35, respectively.

Keywords: garnierite; vacuum carbothermal reduction; mechanism; CaF$_2$; recovery
1. Introduction

Nickel is an important metal in the modern world, used in stainless steel, electroplating, rechargeable batteries, and super alloys [1,2] to improve peoples’ quality of life, and widely used in improving human health in nickel-containing medical devices, medical artificial bones, stents, and new anticancer drugs [3–6]. With the increase of demand for nickel and the rapid depletion of nickel sulfide ore, more attention is being paid to low-grade nickel laterite ore [7–9]. Generally, nickel laterite ore can be divided into three categories: limonitic ore, transition ore, and garnierite [10–12]. According to the different compositions of every layer, nickel laterite ores are treated using different methods, including pyrometallurgical and hydrometallurgical methods [13]. Hydrometallurgical techniques are more applicable to limonitic ore, which includes ammonia–ammonium carbonate leaching, pressure acid leaching (PAL), and high-pressure acid leaching (HPAL) [14–20]. Garnierite is more suitable for pyrometallurgical methods due to the high content of magnesium. At present, the mature industrial pyrometallurgical methods include rotary kilns-electric furnaces (RKEF) and Krupp–Ren [21–23].

Previous studies reported that CaF$_2$ is used as additive in pyrometallurgy of nickel laterite ore. Ma et al. [24] studied the influence of CaF$_2$ in the nickel laterite ore reduction process. The results indicated that the aggregation of nickel and iron particles increased significantly from 1 to 200 µm after adding CaF$_2$, which indicates that CaF$_2$ can effectively reduce the surface tension of the newly formed alloy. This is beneficial for magnetic separation process and increases the nickel grade. Cao et al. [25] determined the production and enrichment rates of nickel and iron under different smelting conditions by changing the amount of added reducing agent and comparing the different production rates of ferronickel with CaF$_2$, CaF$_2$, and hydrated lime. However, the authors did not report the optimal conditions, nor did they specifically explore the mechanism of CaF$_2$ and hydrated lime in the reduction process.

Previous studies only focused on the extraction of Ni and Fe, and ignored the extraction of higher values magnesium. The behavior of CaF$_2$ in the reduction process has not been reported in the literature. Therefore, we propose a vacuum carbothermal reduction–magnetic separation process to recover nickel, iron, and magnesium from garnierite, and investigated the behavior of the added CaF$_2$ in the reduction process. In this process, magnesium was reduced to magnesium vapor and condensed to obtain magnesium metal [26,27]. The experimental flow chart is shown in Figure 1.

![Figure 1. Work flow of the experimental procedure.](image-url)
2. Materials and Methods

2.1. Raw Materials

The garnierite sample used in this study was obtained from Yuanjiang, Yunnan province, China. The X-ray diffraction (XRD) analysis and the chemical analysis of the sample are shown in Figure 2 and Table 1. According to the XRD analysis, we found that the major phases of garnierite are lizardite, nepouite, kaolinite, and quartz. CaF$_2$ was used as an additive in this study. The compositions of CaF$_2$ and the coking coal are listed in Tables 2 and 3, respectively.

![Figure 2. X-ray diffraction (XRD) patterns of garnierite.](image)

**Table 1.** The composition of the garnierite (wt. %).

| Component | SiO$_2$ | MgO | Fe  | Ni  | Co  | Al$_2$O$_3$ | Others |
|-----------|--------|-----|-----|-----|-----|-------------|--------|
| Content   | 38.82  | 22.83 | 12.66 | 0.72 | 0.03 | 4.57        | 20.37  |

**Table 2.** The composition of the CaF$_2$ (wt. %).

| Component | CaF$_2$ | Si  | Fe  | Heavy Metal | Chloride | Sulfate | Nitride |
|-----------|---------|-----|-----|-------------|----------|---------|---------|
| Content   | ≥98.5   | ≤0.01 | ≤0.003 | ≤0.003 | ≤0.01 | ≤0.05 | ≤0.005 |

**Table 3.** The composition of the coking coal (wt %).

| Component | C | Ash | Moisture | Volatile | K (g) |
|-----------|---|-----|----------|----------|------|
| Content   | 85.83 | 12.02 | 0.14 | 2.01 | 7187.2 |

2.2. Experimental Method and Equipment

All garnierite and coking coal were crushed and screened to less than 74 μm, and the ore and C were mixed in a molar ratio of 1:1.2. The masses of CaF$_2$, which were 0%, 3%, 6%, 9%, and 12%, were studied with regard to their behavior and effect on the experimental results. In the first, the mixed materials were formed into pellets of Φ20 mm × 20 mm at 5 MPa and then placed in a corundum crucible. Heating was applied under pressures ranging from 10 to 50 Pa by placing the corundum crucible into a graphite crucible in a vacuum furnace. The system temperature was raised from room temperature to the desired temperature and was held this temperature for 120 min. After, the reaction product was cooled to room temperature and removed. The schematic model of the vacuum distillation furnace for experiment is shown in Figure 3. For the nickel-rich residue, we used a vibrating grinding machine to crush the material to approximately 74 μm, and we placed the crushed materials into a planetary ball mill for 4 h of ball milling, allowing the materials to be mixed thoroughly and uniformly. After the ball milling was completed, the materials were removed, sampled, and sent for analyses, and magnetic separation was conducted for the remaining residue.
were determined using scanning electron microscopy (SEM, TM-3030 Plus, HITACHI, Tokyo, Japan) where Ma and M0 refer to the masses of metals in the nickel-rich residue and in the ore, respectively. The recovery α of the reduction process is expressed as:

\[ \alpha_1 = \frac{M_{a}}{M_{0}}, \]  

where Ma and M0 refer to the masses of metals in the nickel-rich residue and in the ore, respectively. The recovery α2 of the reduction magnetic separation process is expressed as:

\[ \alpha_2 = \frac{M_{b}}{M_{a}}, \]  

where Ma and Mb refer to the masses of metals in the magnetic substances and in the nickel-rich residue, respectively. The recovery α of the whole process is expressed as:

\[ \alpha = \alpha_1 \times \alpha_2. \]  

2.3. Analysis Methods

The nickel-rich residue was identified with X-ray diffraction (XRD) Dmax-R diffractometer (Rigaku, Tokyo, Japan, Cu Kα radiation, 40 mA, 50 kV). The diffraction angle (2θ) was scanned from 10° to 90° in 4° increments. The morphology and the elemental composition of the particular regions were determined using scanning electron microscopy (SEM, TM-3030 Plus, HITACHI, Tokyo, Japan) equipped with energy-dispersive X-ray spectroscopy (EDS, INCA, Oxford, UK). Chemical analysis of the nickel-rich residue was performed using inductively coupled plasma atomic emission spectroscopy (ICP-OES) with an Optima 8000 (Perkin Elmer, Waltham MA, USA).

3. Results and Discussion

3.1. Experimental Phenomena and XRD/EDS Analysis

During the removal of the Fe–Ni-rich residue, we found different phenomena at the end of the experiment; no melting occurred at the experimental temperature when the addition of CaF2 was 0%. When the addition of CaF2 was 3%, the raw materials appeared to experience micro-melting at 1623 and 1723 K, however, the raw materials melted completely at 1823 K, as shown in Figure 4.

Figure 3. Schematic model of the vacuum distillation furnace: 1, high vacuum valve; 2, release valve; 3, bypass valve; 4, main valve; 5, rotary vane pump; 6, diffusion pump; 7, inflation valve; 8, vacuum pipe; 9, raw materials; 10, graphite crucible; 11, graphite heater; 12, heat shield; 13, water cooled walls; 14, graphite condensing pipe; and 15, condensation.
The left part of Figure 5 is the picture of the material removed after the vacuum carbothermal reduction. The black fluffy material in the picture is located on the top of the corundum crucible. After pouring the black fluffy material, we found that the material in the corundum crucible completely melted, with a layer of gray white material solidified with no hole on the surface on the top of the melted material. After the corundum crucible was broken, we found many large cavities in the melted material, and the color of solidified material below was gray black. Finally, large metal particles were found at the bottom of the corundum crucible. According to the above phenomena, we drew a layering diagram of the materials in the corundum crucible, as shown in the right part of Figure 5.

XRD and SEM/EDS analysis were conducted to determine the phase of black fluffy material and the composition of silver-white metal particles of the first layer, as shown in Figure 6. According to XRD analysis, the black fluffy material was mainly carbon, and the ferrosilicon should be the silver-white metal particles, which mixed with the black matter. SEM/EDS analysis showed that the carbon content reached 75.28%, the remaining materials were mainly Fe and F, and the contents of Fe and F were 12.71% and 5.30%, respectively.

![Figure 4. The reduced slag at (a) 1623 K, (b) 1723 K, and (c) 1823 K with 3% CaF2.](image)

![Figure 5. Phenomena of stratification for the residue after reduction at the experimental temperature with more than 3% CaF2.](image)

![Figure 6. XRD pattern and energy-dispersive X-ray spectroscopy (EDS) analysis of Layer 1.](image)
The thermodynamic analysis of Equation (4) performed at 50 Pa showed that the initial reaction temperature of the production of FeF$_2$ was 1398 K, and FeF$_2$ will directly sublimate at 1373 K. We considered that the source of F was the volatilization of FeF$_2$, with part of the Fe sourced from the ferrosilicon mixed in black matter, and the other part from the volatilization of FeF$_2$. The equation can be expressed as:

$$Fe_2SiO_4(s) + 6C(s) + CaF_2(s) = FeSi(s) + CaC_2(s) + FeF_2(g) + 4CO(g)$$

$$\Delta G_T = 1731.126 - 1.238T \text{kJ/mol.} \quad (4)$$

XRD and SEM/EDS analysis were performed to determine the phase and composition of the second layer, as shown in Figure 7. The XRD results showed that the white matter phase of the second layer was MgAl$_2$O$_4$, and the SEM/EDS results indicated that the white matter mainly contained Mg, Al, and O, at 14.28%, 26.58%, and 50.38%, respectively.

![Figure 7. XRD pattern and EDS analysis of Layer 2.](image)

| Elements | Mg  | Al | O | Si | Ca | Ni | Fe | F |
|----------|-----|----|---|----|----|----|----|---|
| Content (%) | 14.28 | 26.58 | 50.38 | 1.83 | 2.57 | 0.12 | 0.47 | 3.77 |

Combined with the thermodynamic calculation, Equations (5) and (6) showed that the reaction initial temperature for the formation of MgAl$_2$O$_4$ was 875 K, so the reaction to form MgAl$_2$O$_4$ could occur at the experimental conditions. The reason of Al$_2$O$_3$ did not reduce by carbon was the initial temperature of the reduction reaching 1691 K under the pressure of 50 Pa, which is much larger than the reaction initial temperature of MgAl$_2$O$_4$. The MgAl$_2$O$_4$ is denser than carbon, so the carbon floats above the MgAl$_2$O$_4$. The equations can be expressed as:

$$Mg_2SiO_4(s) + 2Al_2O_3(s) = 2MgAl_2O_4(s) + SiO_2(s)$$

$$\Delta G_T = 19.255 - 0.022T \text{kJ/mol,} \quad (5)$$

$$Al_2O_3(s) + 3C(s) = 2Al(s) + 3CO(g)$$

$$\Delta G_T = 1344.640 - 0.795T \text{kJ/mol.} \quad (6)$$

XRD and SEM/EDS analysis were performed to determine the phase and composition of the material in the third layer as well, as shown in Figure 8. XRD analysis revealed that the main phases in the third layer were Mg$_2$SiO$_4$ and MgAl$_2$O$_4$; SEM/EDS analysis showed that the main elements of this layer were Mg and Si, with contents of 45.97% and 29.10%, respectively, mixed with a small amount of F, Fe, Ca, and Al. According to the thermodynamic calculation in Equation (7), the reaction initial temperature of Mg$_2$SiO$_4$ under the pressure of 50 Pa was 1472 K, which is higher than the melt initial temperature. According to the analysis of the first and second layers, we found that after the melting,
the carbon and the materials stratified, so most of the magnesium was not reduced. The equation can be expressed as:

\[
3\text{Mg}_2\text{SiO}_4(s) + 6\text{C}(s) + 2\text{CaF}_2(s) = 6\text{Mg}(g) + 6\text{CO}(g) + 2\text{CaSiO}_3(s) + \text{SiF}_4(g)
\]

\[\Delta G_T = 4297.884 - 2.920T\text{ kJ/mol.} \tag{7}\]

According to the experimental findings, due to the block created by the second layer, many bubbles were trapped underneath, so the Mg vapor could not overflow. This further hindered the reduction, so a large amount of Mg\(_2\)SiO\(_4\) remained in the materials, and a large amount of Mg\(_2\)SiO\(_4\) formed after the end of the experiment. The density of Mg\(_2\)SiO\(_4\) is greater than that of MgAl\(_2\)O\(_4\), resulting in MgAl\(_2\)O\(_4\) floating above the Mg\(_2\)SiO\(_4\).

XRD and SEM/EDS analysis were performed to determine the phase and composition of the fourth layer, as shown in Figure 9. XRD analysis revealed that the fourth layer was mainly Fe\(_x\)Si\(_y\) in various compositions. SEM/EDS analysis revealed that the layer mainly elements were Fe, Ni, and Si, with contents of 66.90%, 4.15%, and 25.72%, respectively.
From the thermodynamic calculations of Equations (4) and (8)–(10), we found that the formation of Fe, Fe$_2$Si$_y$, Ni, and FeNi formed before the materials melted. Under the pressure of 50 Pa, the initial temperature of reactions were 1344, 808, 618, and 1389 K, respectively. After the materials melted, the mass transfer and heat transfer of Ni and Fe accelerated, forming a large particle of Fe–Ni–Si ternary alloy. Due to being denser than Mg$_2$SiO$_4$, it sunk into the bottom of the crucible to form the fourth layer. The equations can be expressed as:

$$3\text{Fe}_2\text{SiO}_4(s) + 6\text{C}(s) + 2\text{CaF}_2(s) = 6\text{Fe}(s) + 6\text{CO}_4(g) + 2\text{CaSiO}_3(s) + \text{SiF}_4(g)$$  
$$\Delta G_T = 1336.421 - 1.653T \text{kJ/mol,}$$  

$$3\text{Ni}_2\text{SiO}_4(s) + 6\text{C}(s) + 2\text{CaF}_2(s) = 6\text{Ni}(s) + 6\text{CO}_4(g) + 2\text{CaSiO}_3(s) + \text{SiF}_4(g)$$  
$$\Delta G_T = 1110.829 - 1.797T \text{kJ/mol,}$$  

$$\text{Ni}_2\text{SiO}_4(s) + 6\text{C}(s) + \text{CaF}_2(s) = \text{NiSi}(s) + \text{CaC}_2(s) + \text{NiF}_2(s) + 4\text{CO}_4(g)$$  
$$\Delta G_T = 1384.267 - 1.055T \text{kJ/mol.}$$

At the end of the experiment, a dense condensate with a silvery white metallic luster was found on the lid, as shown in Figure 10. XRD and SEM/EDS analysis were performed to determine the phase and composition of the condensate. XRD analysis revealed that condensate was mainly calcium–silicon compounds. SEM/EDS analysis showed that the elemental contents of Si, Ca, and Fe were 54.85%, 16.58%, and 8.47%, respectively. From the thermodynamic calculations of Equations (7)–(9) and (11)–(13), we found that the initial temperatures of the formation of SiF$_4$ and SiO were 1472, 808, 618, and 1389 K, respectively. Therefore, the Si in the condensate was mainly produced from the condensation of SiF$_4$ and SiO, the Fe from the sublimation of FeF$_2$, and Ca from the condensation of calcium compounds. The equations can be expressed as:

$$\text{Fe}_2\text{SiO}_4(s) + 3\text{C}(s) = \text{SiO}_2(g) + 2\text{Fe}(s) + 3\text{CO}_4(g)$$  
$$\Delta G_T = 1044.890 - 0.962T \text{kJ/mol,}$$  

$$\text{Ni}_2\text{SiO}_4(s) + 3\text{C}(s) = \text{SiO}_2(g) + 2\text{Ni}(s) + 3\text{CO}_4(g)$$  
$$\Delta G_T = 968.751 - 1.008T \text{kJ/mol,}$$  

$$\text{SiO}_2(s) + \text{C}(s) = \text{SiO}_4(g) + \text{CO}_4(g)$$  
$$\Delta G_T = 697.671 - 0.487T \text{kJ/mol.}$$

| Elements | Si | Ca | O | Al | Fe | F |
|----------|----|----|---|----|----|---|
| Content (%) | 54.85 | 16.58 | 10.38 | 4.85 | 8.47 | 5.13 |

Figure 10. XRD pattern and EDS analysis of the condensate on the graphite crucible lid.
According to the above analysis of the phase and composition of each layer of materials, we found that the first layer was mainly coking coal, the small silver-white metal particles were Fe–Ni–Si, and the main component of the second transition layer was MgAl₂O₄. The third layer was mainly Mg₂SiO₄ with a small amount of MgAl₂O₄ and calcium–silicon compounds, and the large metal particles in the fourth layer were Fe–Ni–Si ternary alloy. The condensate on the lid was mainly Si.

3.2. Behavior of CaF₂

The thermogravimetry-differential scanning calorimetry (TG and DSC) curves of the garnierite are shown in Figure 11. We observed three peaks at different temperatures. According to a previous report [28], the first endothermic peak at 352 K represents the loss of the adsorption water, the second endothermic peak at 885.4 K represents the dehydroxylation of the lizardite, and the third strong exothermic peak at 1097.8 K represents the decomposition of Mg₃Si₂O₇. The process is expressed in Equations (14) and (15).

\[
\text{Mg₃Si₂O₅(OH)₄(s)} = \text{Mg₃Si₂O₇(s)} + 2\text{H₂O(g)} \\
\text{Mg₃Si₂O₇(s)} = \text{Mg₂SiO₄(s)} + \text{MgSiO₃(s)}
\]

The TG and DSC curves of the garnierite with CaF₂ are shown in Figure 12. By comparing Figures 11 and 12, we found two more endothermic peaks at 1315 and 1400 K. The two endothermic peaks represented the conversion of the raw materials from solid to liquid, which produced low-melting-point compounds such as FeF₂, NiF₂, and MgF₂. The thermodynamic calculations in Equations (4), (10) and (16) were performed at 50 Pa. The equations can be expressed as:

\[
\text{Mg₂SiO₄(s)} + \text{SiF₄(g)} = 2\text{MgF₂(s)} + 2\text{SiO₂(s)} \\
\Delta G_T = -271.244 + 0.221T \text{kJ/mol.}
\]

Based on Equations (4) and (10), the initial temperatures of the two reactions were 1398 and 1312 K, which corresponded to the two endothermic peaks in Figure 12.

![Figure 11](image-url)
Figure 12. TG and DSC curves of the raw materials in presence of CaF$_2$.

3.3. Analysis of the Reduction Process

After the vacuum carbothermal reduction, chemical analysis was performed on the Fe–Ni-rich residue. According to the calculation, we obtained the direct recovery of Fe and Ni, which is plotted in Figures 13 and 14, respectively. The figures indicate that with the increase in CaF$_2$, the grades and direct recovery of Fe and Ni first rose and then fell, with maximal grades and direct recovery achieved at 3% CaF$_2$. With increasing temperature, the curves in the figures divided into two parts. The addition of CaF$_2$ at less than or equal to 3% was the first part, in which the grades and direct recovery of Fe and Ni first rose and then fell, with the best grades and direct recovery achieved at 1723 K. The addition of CaF$_2$ at more than 3% was the second part, in which the grades and direct recovery of Fe and Ni showed a downward trend.

Figure 13. The effect of additives and temperature on Fe enrichment (%), the upper three lines in the figure represents the recovery of Fe, and the lower three lines in the figure represents the grade of Fe.
which resulted in low grades and direct recovery of Si. The equations are expressed in Equations (7)–(9)

(3) When the addition of CaF$_2$ was 3%, the CaF$_2$ could react with the raw materials to form
low-melting-point compounds, such as FeF$_2$, NiF$_2$, and MgF$_2$. The reduction process transformed
from a solid–solid reaction to a solid–liquid reaction, which accelerated the heat transfer and the
mass transfer of the materials. The Fe and Ni aggregated and grew easily in the molten materials
and formed small visible Fe–Ni particles on the surface of the Fe–Ni-rich residue. The raw
materials were not completely melted in the reduction process due to the low addition of CaF$_2$. 
Therefore, Fe and Ni were sufficiently reduced in the raw materials, which results in high grades
and direct recovery of Fe and Ni.

(4) Due to excessively high temperatures during the reduction process, the raw materials melted
completely at temperature of 1823 K with 3% CaF$_2$, hindering the reduction process, which reduced
the grades and direct recovery of Fe and Ni. Therefore, the grades and direct recovery of Fe
and Ni were lower than 1723 K with 3% CaF$_2$.

Our analyses demonstrate that the addition of 3% CaF$_2$ at 1723 K is the optimal condition.

According to Figure 15, with increasing temperature and CaF$_2$, the grades and recovery of Si showed a downward trend because Si would volatilize in the form of SiO and SiF$_4$ at high temperature, which resulted in low grades and direct recovery of Si. The equations are expressed in Equations (7)–(9) and (11)–(13).
According to Equations (7)–(9) and (11)–(13), the initial temperatures of these reactions were 1472, 808, 618, 1086, 961, and 1432 K, respectively. All the reactions could occur under experimental conditions. These analysis results were consistent with the above four explanations.

Figure 16 shows that the removal rate of Mg increased with increasing temperature and CaF₂ content. However, the removal rate was low because the raw materials changed from a solid–solid reaction to a liquid–liquid reaction with increasing CaF₂ content, which caused the reduction of Mg to only occur in the early period. However, after the materials melted completely, the coking coal and the raw materials were stratified, which preventing the coking coal from contacting the raw materials. The steam of the Mg could not pass through the transition layer, resulting in the removal rate of Mg increasing slowly. The best example of this was at a temperature of 1823 K with 3% CaF₂, where the removal rate of Mg was significantly lower than 1723 K with 3% CaF₂. These analysis results were consistent with the findings in Section 3.2.

As seen in Figures 13–16, we can conclude that adding 3% CaF₂ is beneficial to the recovery of Ni and Fe, however, the recovery of Si and Mg are not good enough. At 1723 K, the recovery...
of Si is less than 45% and the recovery of Mg is less than 55%. The effect of temperature and the adding amount of CaF$_2$ on the recovery of Si and Mg showed the opposite trend, that is, with the increase of temperature and the amount of CaF$_2$, the recovery of Si showed a downward trend, while the recovery of Mg showed an upward trend. This become a contradiction point for recovering of garnierite comprehensively; therefore, the recovery of Si and Mg will not be ideal if only adding CaF$_2$. Our previous research [29] has proved that CaO can greatly enhance the recovery of Si and Mg. We could consider the mixture of CaF$_2$–CaO as an additive to achieve the purpose of comprehensive recovery of valuable metals from garnierite.

3.4. Phase Analysis of Fe–Ni-Rich Residue

Figures 17 and 18 show that the main phases of the Fe–Ni-rich residue were forsterite, spinel, and FeSi, as well as a small amount of CaSiO$_3$ and low-melting-point compounds (FeF$_2$, NiF$_2$, and MgF$_2$). According to the literature, forsterite, Fe$_2$SiO$_4$, and Ni$_2$SiO$_4$ are mainly produced after the dehydroxylation of lizardite. Forsterite can react with coking coal to form Mg steam at high temperatures. However, the Fe–Ni-rich residue was mainly forsterite in this experiment, which indicated that most of the forsterite did not participate in the reduction reaction.

![XRD patterns of the Fe–Ni-rich residue at different temperatures with 3% CaF$_2$.](image1)

![XRD patterns of the Fe–Ni-rich residue at 1723 K with 0–12% CaF$_2$.](image2)

After the lizardite decomposed, the CaF$_2$ reacted with Fe$_2$SiO$_4$ and Ni$_2$SiO$_4$ to form low-melting-point compounds (FeF$_2$, NiF$_2$, and MgF$_2$), as shown in Figure 17. With increases in CaF$_2$ and temperature, the raw materials changed from the solid to the liquid state. This caused some of the forsterite to react...
with the coking coal during the melting process, although a large part of forsterite could not react with coking coal due to the stratification after the raw materials melted completely, which caused a large amount of the forsterite to remain in the Fe–Ni-rich residue. The proportion of Ca in the raw materials was less than that of Si, the reduction of Fe and Ni could have combined with Si to form Si–Fe–Ni ternary alloy particles, and the proportion of Ni was low. Therefore, the Si–Fe–Ni ternary alloy showed up as an Fe–Si peak in the XRD pattern. The forsterite and the Al₂O₃ could have reacted to form spinel, which caused a spinel peak to be found in the Fe–Ni-rich residue. The equations were expressed as Equations (5) and (6) in Section 3.1.

According to Equations (5) and (6), the initial temperatures of the two reactions were 875 K and 1691 K. These results indicate that the reaction in Equation (5) more easily occurred than that in Equation (6), which meant the spinel could be produced under experimental conditions.

As shown in Figure 18, at 1723 K with 3% CaF₂, the forsterite peak was weakest and the Fe–Si peak was strongest, which indicates that the reduction of the raw materials was effective under these conditions.

3.5. Mechanism of CaF₂ in the Reduction Process

TG-DSC and thermodynamic analysis indicated that the solid materials began to melt at 1315 K and 1400 K and produced low melting point eutectic materials (NiF₂ and FeF₂) as heating progressed. In the reduction progress, the raw materials reacted with CaF₂ to produce SiF₄, and forsterite reacted with SiF₄ to form another low melting point eutectic material, MgF₂, which further accelerated the melting of the materials, causing the materials to transition from solid to liquid. The melting point of NiF₂ is 1653 K at 1 atm, the boiling point is 1772 K, the melting point of FeF₂ is 1243 K, the boiling point is 1373 K, and FeF₂ undergoes sublimation at 1373 K. At 50 Pa, the melting points of NiF₂ and FeF₂ decrease, therefore, once FeF₂ is formed, it undergoes sublimation and NiF₂ volatilizes simultaneously. According to the thermodynamics calculations, the initial temperature where MgF₂ forms is 1227 K, the melting point of MgF₂ is 1534 K, and the boiling point is 2533 K, therefore, MgF₂ would not have volatilized under the experimental conditions.

The 20-mm-diameter Fe–Ni–Si ternary alloy collected in the experiment showed that the melted materials accelerated the heat transfer and the mass transfer of Fe and Ni, promoting the FeNi particles to aggregate and grow. With increasing temperature and the increase in addition of CaF₂, the volatility of Si in the form of SiO and SiF₄ were promoted, causing a sharp drop in the recovery of Si. Due to the density of coking coal being less than that of MgAl₂O₄, MgAl₂O₄ being less dense than Mg₂SiO₄, and Mg₂SiO₄ being less dense than Fe–Ni–Si ternary alloy, the materials stratified. The stratification of the raw materials and coking coal hindered the reduction of Mg, causing a slow increase in the removal rate of Mg, as shown in Figure 19.

![Figure 19](image-url). The influence and behavior of CaF₂ on the reduction process.
3.6. Magnetic Separation Process

Table 4 shows that after the magnetic separation, the grades of Fe were low, probably because Fe was present in the forsterite and spinel during the reduction process, which resulted in a low chemical analysis result. At the optimal conditions, the direct recoveries of Fe and Ni were 82.97% and 98.21%, respectively, in the vacuum carbothermal reduction–magnetic separation process, and the enrichment ratios were 3.18 and 9.35, respectively, as shown in Table 5. The data in the tables indicate that adding a proper amount of CaF$_2$ could effectively improve the grades and recovery of Fe and Ni.

Table 4. The content and recovery of Fe and Ni using the magnetic separation process and using the vacuum carbothermal reduction–magnetic separation process.

| Temperature (K) | CaF$_2$ (wt. %) | Quality of Magnetic Material (g) | Chemical Analysis of Fe, Ni in Magnetic Materials (%) | Quality of Non-Magnetic Material (g) | Chemical Analysis of Fe, Ni in Non-Magnetic Materials (%) |
|----------------|-----------------|---------------------------------|-----------------------------------------------------|-------------------------------------|-------------------------------------------------------|
| 1623           | 3               | 24.49                           | Fe         | 32.46                              | Ni         | 5.18                       | 35.66                       | Fe         | 0.42                                  | Ni         | 0.04                                  |
| 1823           | 3               | 30.29                           | Fe         | 38.17                              | Ni         | 6.98                       | 21.71                       | Fe         | 0.33                                  | Ni         | 0.05                                  |
| 1723           | 0               | 50.54                           | Fe         | 14.95                              | Ni         | 1.04                       | 50.54                       | Fe         | 0.00                                  | Ni         | 0.00                                  |
| 1723           | 3               | 11.16                           | Fe         | 40.20                              | Ni         | 6.37                       | 21.75                       | Fe         | 0.18                                  | Ni         | 0.03                                  |
| 1723           | 6               | 23.61                           | Fe         | 38.30                              | Ni         | 6.69                       | 50.57                       | Fe         | 0.23                                  | Ni         | 0.07                                  |
| 1723           | 9               | 23.06                           | Fe         | 37.30                              | Ni         | 6.22                       | 49.73                       | Fe         | 0.26                                  | Ni         | 0.06                                  |
| 1723           | 12              | 19.03                           | Fe         | 34.75                              | Ni         | 5.11                       | 49.13                       | Fe         | 0.38                                  | Ni         | 0.02                                  |

Table 5. Enrichment ratio of Fe and Ni with different dosages of CaF$_2$ at different temperature and Recovery of Fe and Ni during the vacuum carbothermal reduction–magnetic separation process.

| Temperature (K) | CaF$_2$ (wt. %) | Enrichment ratio of Fe (%) | Enrichment ratio of Ni (%) | Recovery of Fe (%) | Recovery of Ni (%) |
|-----------------|-----------------|---------------------------|---------------------------|--------------------|--------------------|
| 1623            | 3               | 2.56                      | 1.18                      | 73.19              | 73.87              |
| 1823            | 3               | 3.02                      | 1.18                      | 73.18              | 73.87              |
| 1723            | 6               | 3.03                      | 1.18                      | 73.18              | 73.87              |
| 1723            | 9               | 2.95                      | 2.75                      | 73.18              | 73.87              |

4. Conclusions

A vacuum carbothermal reduction–magnetic separation method to recover Ni, Fe, and Mg from garnierite was proposed, and the experiments indicated that the optimal conditions for this method for the recovery of Fe and Ni are 1723 K, a molar ratio of ore/C of 1:1.2, and the addition of CaF$_2$ at 3%. The recovery of Fe and Ni reached 82.97% and 98.21%, respectively, in the vacuum carbothermal reduction–magnetic separation process, and the enrichment ratios of Fe and Ni reached a maximum of 3.18 and 9.35, respectively.

The CaF$_2$ in the vacuum carbothermal process formed low-melting-point compounds (FeF$_2$ and NiF$_2$) at 1315 K and 1400 K, respectively, to transform the raw materials from solid to liquid, which accelerated the mass transfer and the heat transfer of Fe–Ni particles, and formed Si–Ni–Fe alloy particles with diameters of approximately of 20 mm. Simultaneously, the melting materials appeared stratified, hindering the reduction of magnesium.

The removal rate of Mg increased and the maximal recovery only reached 74.12%. The reason for this low Mg removal rate is the stratification of the coking coal and the molten materials, which limited the increase in the recovery of Mg. However, the recovery of Si and the removal rate of Mg showed the opposite trend, this becomes a contradiction point for recovering garnierite comprehensively. Previously, we used this method to recover Ni, Fe, Si, and Mg with CaO as an additive, achieved some good experiment results, especially for the removal rate of Mg [29]. Subsequently, we could consider the mixture of CaF$_2$–CaO as an additive to solve the contradiction of Si and Mg, and achieve the purpose of comprehensive recovery of valuable metals from garnierite.
The method used in this article can solve the problem of the large amounts of slag produced and the inability to recycle the magnesium in the traditional pyrometallurgical process. For the future industrial application, it is necessary to solve the problem of magnesium condensation technology. If magnesium can be recycled in a reduction process, not only can it increase the economic benefits of enterprises, but it can also solve the problem of environment pollution, therefore, it has a certain industrialization significance. In addition, this article clarifies the behavior mechanism of CaF$_2$ in the reduction process of garnierite, it can be used for reference in guiding industrial production.

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