Data Article

**Data on the removal of metals** \((\text{Cr}^{3+}, \text{Cr}^{6+}, \text{Cd}^{2+}, \text{Cu}^{2+}, \text{Ni}^{2+}, \text{Zn}^{2+})\)** from aqueous solution by adsorption using magnetite particles from electrochemical synthesis

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**A R T I C L E  I N F O**

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**A B S T R A C T**

Magnetic materials are promising adsorbents for removing heavy metals from polluted wastewaters. Magnetite particles were prepared by electrolytic synthesis (average crystallite size 37.9±1.2 nm, surface area = 17.2 m²/g, isoelectric point = 6.3, magnetic saturation = 62 emu g⁻¹) and used as adsorbent of heavy metals in aqueous solutions. The adsorption capacity of the magnetite was highly dependent on pH value, for Cd²⁺, Zn²⁺, Ni²⁺ and Cu²⁺ the removal performance was higher than 80% at pH = 8. For Cr³⁺, the acid pH showed removal percentage higher than 90%.

The adsorbent was separated from the system, reactivated and reused in subsequent tests using batch adsorption. It was found that removal efficiencies were higher than 70% even during a third cycle of adsorption. Finally, the kinetic behavior of the adsorption of each adsorbate was described by a first-order. The range of values of \(q_e\) (mg/g) and \(k\) (min⁻¹) were 1.3166–1.6367 and 0.0377 to 0.0826 respectively.

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1. Data

This brief data set describes the electrochemical synthesis of magnetite particles (Fig. 1), the Figs. 2–4 shows the N₂ isotherms, zeta potential and magnetization hysteresis curves.

Fig. 5 shows adsorption capacity of magnetite on metal ions (Cd²⁺, Zn²⁺, Ni²⁺, Cu²⁺) solutions, the Table 1 shows the molar distribution of the ions versus pH.

For Cr⁶⁺, the removal percentage and species type in function of pH are shown in Fig. 6 and Fig. 7 respectively.

The regenerated adsorbent was separated (Fig. 8) and re-used in three adsorption cycles, the Fig. 9 shows the removal percentage for Cd²⁺, Ni²⁺ and Cr⁶⁺.

Finally, the Table 2, Fig. 10 and Fig. 11 shows the adsorption kinetics parameters and kinetics curves of metal ions adsorption on magnetite particles.

1.1. Magnetite synthesis and characterization

Under the conditions described in the experimental section, following a previously reported methodology, a black precipitate was obtained and identified as pure magnetite (Fe₃O₄) by mean of X-Ray diffraction-XRD [1]. Fig. 1 shows the diffractogram of a sample obtained and every peak was identified by comparing with the standard pattern for magnetite (Registry JCPDS number: 01-088-0315) [2].

From Rietveld refinement results (Pseudo-Voigt Model: $\chi^2 < 1.5$; $R(F^2) < 0.1$), crystalline structure can be classified as Face Centered Cubic (FCC) with space group Fd3m. The crystallite size was calculated in the parallel, equation (1), and perpendicular, equation (2), directions to the growth anisotropy using the Scherrer equations [3]:

| Specifications table |
|----------------------|
| **Subject area**     | Chemical engineering |
| **More specific subject area** | Adsorption process |
| **Type of data**     | Figures and tables   |
| **How data was acquired** | The magnetite particles was obtained by electrochemical synthesis. XRD, N₂ Adsorption, ZPC and magnetic properties was used in the characterization of materials. Data were obtained by adsorption test from cation solutions at room conditions. |
| **Data format**      | Analyzed             |
| **Experimental factors** | All experimental tests were performance to laboratory scale. |
| **Experimental features** | Metal ions adsorption using magnetite obtained by electrochemical synthesis were investigated. |
| **Data source location** | Universidad del Valle, Cali, Colombia and Universidad Autonoma de Nuevo León, Monterrey, México. |
| **Data accessibility** | The data is found only in this article. |
| **Related research article** | J. Manrique-Julio, F. MacHuca-Martinez, N. Marriaga-Cabrales, M. Pinzon-Cardenas, Production of magnetite by electrolytic reduction of ferric oxyhydroxide, J. Magn. Magn. Mater. (2016). https://doi.org/10.1016/j.jmmm.2015.10.018 |

**Value of data**
- A new method to produce magnetite with high specific area was used as heavy metals adsorbent in aqueous solutions.
- The removal of Cr⁶⁺, Cd²⁺, Cu²⁺, Ni²⁺, and Zn²⁺ from synthetic wastewater onto magnetite was performed using batch adsorption.
- Adsorption tests performed without an adsorbent alkaline pretreatment suggested that the process is primarily driven by electrostatic attraction.
- The adsorption kinetics was found to follow a Pseudo-first order model for every metal ion.
\[
\phi_{\parallel} = \frac{18000 \, k \, \lambda}{\pi (L_x + ptec)}
\]  

(1)

\[
\phi_{\perp} = \frac{18000 \, k \, \lambda}{\pi L_x}
\]  

(2)

Where \( k = 0.9 \) is the Scherrer constant, \( \lambda = 0.154056 \) is the wavelength of the Cu K\(_{\alpha}\) radiation, and \( L_x \) and \( ptec \) are the isotropic and anisotropic Lorentzian broadenings, respectively, of the crystallite size [3]. The \( ptec \) value was calculated to be zero for each sample, which indicates that the crystallites were spherical. The average crystallite size of all samples, calculated by Scherrer equation, was found to be 37.9±1.2 nm.

Based on the N\(_2\) adsorption/desorption isotherm, shown in Fig. 2, the Brunauer, Emmett and Teller-BET surface area of the Fe\(_3\)O\(_4\) particles was estimated to be 17.2 m\(^2\)g\(^{-1}\), a value higher than the average specific areas of a commercially available magnetite (6.9 m\(^2\)g\(^{-1}\)) and the natural occurring magnetite, < 4 m\(^2\)g\(^{-1}\) [2,4].

Fig. 1. XRD diffractogram of magnetite particles obtained at 18 mA cm\(^{-2}\) and a distance between electrodes of 0.3 cm.

Fig. 2. N\(_2\) adsorption/desorption isotherms of commercial (Sigma-Aldrich) and electrolytically prepared magnetite at 18 mA cm\(^{-2}\).
The adsorption/desorption isotherm of the prepared samples can be classified as a Type-IV isotherm with a hysteresis loop in the range of pressure of 0.3–0.95, suggesting that the samples are mesoporous. Pore size, determined by BJH method, was estimated to be around 5 nm, which can be classified as mesoporous (2–50 nm) [2,6].

The determination of the zeta potential was performed to indicate the sign of the surface charge depending on the pH media and the isoelectric point (IEP). As shown in Fig. 3 the IEP was calculated to be around 6.3.

Below the IEP, the particles developed a positive surface charge owing to a protonation of surface sites and over this value it turned into negative surface charges. Changes in surface charge are due to the protonation and deprotonation of surface hydroxyl groups formed during the pretreatment of the particles with a NaOH solution, equation (3), described by equations (4) and (5) for acidic and alkaline media, respectively [5,7].

![Fig. 3. Zeta potential values of the magnetite particles in a NaCl solution, 100mg l⁻¹.](image)

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![Fig. 4. Magnetization curve of magnetite obtained by Vibrating Sample Magnetometry at 300K.](image)
\[
\frac{1}{2} \text{Fe}_3 \text{O}_4/\text{surf} + \text{OH}^- \rightleftharpoons [\text{Fe}_3 \text{O}_4]_{\text{surf}} - \text{OH}^- \quad (3)
\]

\[
[\text{Fe}_3 \text{O}_4]_{\text{surf}} - \text{OH} + \text{H}^+ \rightleftharpoons [\text{Fe}_3 \text{O}_4]_{\text{surf}} - \text{OH}_2^+ \quad (4)
\]

\[
[\text{Fe}_3 \text{O}_4]_{\text{surf}} - \text{OH} + \text{OH}^- \rightleftharpoons [\text{Fe}_3 \text{O}_4]_{\text{surf}} - \text{O}^- + \text{H}_2\text{O} \quad (5)
\]

**Fig. 4** shows the magnetization hysteresis loop of the magnetite particles synthesized. The values of magnetic saturation (M_s), remanence and coercivity obtained were 62 emu g\(^{-1}\), 0.09 kOe and 7.5 emu g\(^{-1}\) respectively.

The magnetic saturation obtained from the hysteresis curve was lower than the values reported in the literature, 92–100 emu g\(^{-1}\) [2]. This behavior can be attributed to a possible surface oxidation of the magnetite particle into another oxide with a lower M_s, like maghemite, M_s = 72 emu g\(^{-1}\) [2]. Some authors also attribute this variation of M_s to the synthesis method used to prepare the particles [6,7].

### 1.2. Heavy metals adsorption tests

The Batch adsorption test for every metal cation at different pH values were performed. **Fig. 5** shows the removal percentage obtained for Cd\(^{2+}\), Zn\(^{2+}\), Ni\(^{2+}\) and Cu\(^{2+}\) metal cations at pH 8.0. The adsorption tests performed at pH values lower than 8.0 evidenced negligible removal efficiencies (less than 10%). This behavior can be attributed to the fact, that at these conditions, magnetite and the aqueous species formed by the metal cations are positively charged, hindering the attraction between them. According to simulations performed in Visual Minteq, the only species formed by the cations is the hexa-aquo complex, [M(OH\(_2\))]\(_6\)\(^{2+}\) (M = Cd\(^{2+}\), Zn\(^{2+}\), Ni\(^{2+}\) or Cu\(^{2+}\)).

In the adsorption test performed with the Cr(III) solution, removal efficiencies were negligible at pH values less than 7.0. This can be explained by the repelling effect between magnetite (positive surface charge at this pH value) and the species formed at those acidity levels: [Cr(OH\(_2\))]\(_6\)\(^{3+}\) and...
The addition of NaOH to the Cr(III) solution caused the immediate precipitation of the cation in the form of \( \text{Cr(OH)}(\text{OH}_2)_3^{2+} \) at any alkaline pH level; therefore it was not necessary to perform adsorption test at these conditions [9].

In contrast to trivalent chromium, hexavalent chromium does not precipitate at any pH value [10], i.e. does not produce any quantifiable uncharged aqueous species, Fig. 6. This can be explained by the fact that \( \text{Cr}^{6+} \) ion can strongly polarize water molecules due to its high formal charge.

| Cation | Species | Molar distribution (%) |
|--------|---------|------------------------|
| \( \text{Cd}^{2+} \) | \( \text{Cd(OH)}(\text{OH}_2)_3^{2+} \) | 99 |
| \( \text{Cd(OH)}(\text{OH}_2)_3^{+} \) | 1 |
| \( \text{Zn}^{2+} \) | \( \text{Zn(OH)}_2(\text{OH}_2)_4^{+} \) | 84 |
| \( \text{Zn(OH)}(\text{OH}_2)_3 \) | 7 |
| \( \text{Ni}^{2+} \) | \( \text{Ni(OH)}_2(\text{OH}_2)_4^{+} \) | 9 |
| \( \text{Ni(OH)}(\text{OH}_2)_3^{2+} \) | 99 |
| \( \text{Ni}^{2+} \) | \( \text{Cu(OH)}_2(\text{OH}_2)_3^{+} \) | 11 |
| \( \text{Cu(OH)}(\text{OH}_2)_3 \) | 2 |
| \( \text{Cu}^{2+} \) | \( \text{Cu(OH)}_2(\text{OH}_2)_3^{+} \) | 13 |
| \( \text{Cu(OH)}(\text{OH}_2)_3 \) | 70 |

**Fig. 6.** Speciation diagram of hexavalent chromium at concentration of 50 mg l\(^{-1}\) and room temperature.

\[ \text{[Cr(OH)(OH}_2)_3]^{2+} \]. The addition of NaOH to the Cr(III) solution caused the immediate precipitation of the cation in the form of \( \text{[Cr(OH)}_2(\text{OH}_2)_3 \) at any alkaline pH level; therefore it was not necessary to perform adsorption test at these conditions [9].

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**Fig. 7.** Effect of pH on adsorption efficiency of \( \text{Cr}^{6+} \) onto magnetite surface, from a 50 mg l\(^{-1}\) aqueous solutions.
Hexavalent chromium adsorption efficiencies in function of pH are shown in Fig. 7. Acidic pH values showed the highest removal values; this can be attributed to the difference in electrostatic charge between magnetite (positive zeta potential) and the species formed in aqueous media by hexavalent chromium (HCrO$_4^-$) shown in the speciation diagram, Fig. 6.

This species, also described as [CrO$_3$(OH)]$^-_2$, undergoes a dimerization reaction, equation (6), turning into dichromate Cr$_2$O$_7^{2-}$ that can also be attracted by the positive surface charge of magnetite [11].

$$2\text{HCrO}_4^- \rightarrow \text{Cr}_2\text{O}_7^{2-} + \text{H}_2\text{O}$$  

(6)

Low removal values at high pH values can be explained by a similar argument; magnetite and hexavalent chromium repeal each other because of their charges, negative zeta potential and CrO$_2^{2-}$ respectively.

The alkaline pretreatment (NaOH solution 1.0 M during 15 minutes prior to each adsorption test) to the adsorbent particles, to increase the number of hydroxyl groups, plays an important role in the adsorption efficiency [11]. Adsorption tests performed without this pretreatment showed low removal
Table 2
Adsorption kinetic models parameters.

|          | Pseudo-first order |          | Pseudo-second order |          |
|----------|--------------------|----------|--------------------|----------|
|          | $q_e$ (mg/g) | $k$ (min$^{-1}$) | $R^2$ | $q_e$ (mg/g) | $k$ (min$^{-1}$) | $R^2$ |
| Cr$^{6+}$ | 1.6367     | 0.0826      | 0.9901  | 1.7516     | 0.0659      | 0.9714  |
| Cd$^{2+}$ | 1.5581     | 0.0363      | 0.9883  | 1.7316     | 0.0264      | 0.9786  |
| Cu$^{2+}$ | 1.5302     | 0.0401      | 0.9789  | 1.6912     | 0.0301      | 0.9695  |
| Ni$^{2+}$ | 1.4429     | 0.0444      | 0.9904  | 1.5959     | 0.0345      | 0.9768  |
| Zn$^{2+}$ | 1.3166     | 0.0377      | 0.9879  | 1.4746     | 0.0306      | 0.9769  |

Fig. 10. Fitted pseudo-first order adsorption kinetic curves of Cr$^{6+}$, Zn$^{2+}$ and Cd$^{2+}$ in $\text{Fe}_3\text{O}_4$.

**Fig. 11.** Fitted pseudo-second order adsorption kinetic curves of Cr$^{6+}$, Zn$^{2+}$ and Cd$^{2+}$ in $\text{Fe}_3\text{O}_4$.  

$\text{Cd}^{2+}$ in $\text{Fe}_3\text{O}_4$
percentages (less than 10%) for all the cations; this result suggests that the adsorption could be primarily due to electrostatic attraction between the aqueous cationic species and the charged hydroxyl groups formed onto the surface of magnetite.

1.3. Desorption and reuse of the adsorbent

Once the batch adsorption tests finished, magnetite was separated from the solution by using a magnetic retriever, as shown in Fig. 8. The used adsorbent was washed with a 0.05 M NaOH solution of pH 12 and rinsed with distilled water for several times, in order to use it subsequent adsorption tests.

The recovery of the adsorbent was calculated using equation (7).

\[
\text{Recovery} = 100\frac{N_{\text{Rec}}}{N_{\text{Ads}}} \tag{7}
\]

Where \( N_{\text{Ads}} \) and \( N_{\text{Rec}} \) are the adsorbed and recovered moles of the metal cation, respectively. The recovery of the adsorbent was between 60 and 80%; this suggests that some of the metal cations could be chemically adsorbed on the surface of magnetite \([12,13]\).

The regenerated adsorbent was used in subsequent metal cations adsorption tests, and removal efficiencies were as high as 70% even in the third cycle of adsorption, Fig. 9. The decreasing removal capacity of the adsorbent, after each regeneration cycle, suggests that some of the species could be chemically adsorbed onto magnetite surface, as previously reported \([14]\).

1.3.1. Adsorption kinetics

In order to understand the kinetic behavior of the adsorption process, two kinetic models were fitted to the experimental data: pseudo-first and pseudo-second order kinetic models, equations (8) and (9), respectively:

\[
q_t = q_e \left(1 - e^{-kt}\right) \tag{8}
\]

\[
q_t = \frac{kq_e^2 t}{1 + kq_e t} \tag{9}
\]

Where \( q_t \) and \( q_e \) are the amount of absorbed cations at time \( t \) (min) and equilibrium, respectively; and \( k \) is the rate constant (min\(^{-1}\)). Best fit estimates of these parameters obtained by a non-linear regression analysis are summarized in Table 2 and the fitting plots using both models are illustrated in Figs. 10 and 11, jointly with the experimental data.

Hexavalent chromium presented the higher values of kinetic constants, evidenced in a fast adsorption rate at the initial stage. This behavior could be attributed to the higher electrostatic attraction between this cation and the adsorption sites of magnetite, unlike the other cations with low formal charge, and to the initial concentration gradient \([13-15]\).

Pseudo-first order model showed the higher correlations (represented as \( R^2 \)), suggesting that this kinetic model is more suitable for describing the adsorption behavior of these metallic cations on magnetite than the pseudo-second order model. This result does not agree with that reported by Martinez et al. \([14]\) and Hosseinzadeh et al. \([13]\); in these studies, it was concluded that the pseudo-second order equation fits better, this result could be attributed to the fact that nanosized magnetite was used. The discrepancy in the results obtained could be explained by the fact that in both studies nanosized magnetite was used as adsorbent, able to strongly chemically interact with the cationic species due to size effects.

2. Experimental section, materials and methods

2.1. Magnetite particles synthesis and characterization

Magnetite particles (Fe\(_3\)O\(_4\)) were synthesized by using the electrochemical method using a monopolar arrangement of carbon steel electrodes, immersed in a 0.04 M NaCl solution at neutral pH, and a current density of 18 mA cm\(^{-2}\) using an EXTECH 382280 DC power source, up to an electric
charge of 3000 CL⁻¹ (Fig. 12). The distance between the electrodes was fixed to 0.3 cm and room conditions were used in all experiments, as previously reported [1].

Phase composition and crystallite size of the particles were studied by X-ray diffraction using an X’Pert Pro PANalytical diffractometer (PANalytical, Netherlands). Copper radiation ($\lambda_{K\alpha1} = 1.54056 \text{ Å}$, $\lambda_{K\alpha2} = 1.54439 \text{ Å}$) was used in a 2θ range of 15°–90° at a step size of 1° at room temperature. The crystallographic analysis was performed by Rietveld method using the X’Pert High Score Plus software (PANalytical, Netherlands).

Surface area and pore size distribution were determined by measuring the N₂ adsorption isotherms in an ASAP 2020 system (Micromeritics, USA). Previous to each measurement, the samples were degassed at 353 K during 12 h, in order to eliminate physically adsorbed moisture. BET (Brunauer-Emmet-Teller) and BJH (Barret-Joyner-Halenda) methods were used for determining the specific surface area and pore size, respectively [16,17].

Point of zero charge of the magnetite was determined in a Zeta-Meter Z402 (Zeta-Meter Inc, USA) by measuring the electrophoretic mobility ($\mu$) of the particles in a 100 ppm NaCl solution in a pH range of 2–12, adjusted by adding drops of HCl and NaOH. From the obtained electrophoretic mobility, zeta potential ($\zeta$) was calculated using the Smoluchowski equation (10):

$$\zeta = \frac{4\pi\eta\mu}{\varepsilon}$$

Where $\eta$ is the viscosity of the suspension medium and $\varepsilon$ the viscosity of the fluid phase.

Magnetic properties measurement of the samples was carried out using a PPMS (Physical Properties Measurement System, Quantum Design, San Diego - USA) in VSM mode (Vibrating Sample Magnetometry) with a sweeping from $-10$ to $+10$ kOe at 300 K.

2.2. Preparation of heavy metal solutions

All heavy metal solutions, with a concentration of 50 mg·l⁻¹, were prepared by dilution, with ultrapure water of type 1, of standard solutions (Atomic absorption standard solutions with a concentration of 1000 mg·l⁻¹). Table 3 summarizes the information concerning the standard solutions used.

2.3. Adsorption tests

Adsorption tests of metal cations (Cd²⁺, Zn²⁺, Ni²⁺, Cu²⁺, Cr³⁺ and Cr⁶⁺) were performed in batch mode, using 250 ml of each solution, over a wide range of pH (2–10) at room conditions. pH values
were adjusted by adding drops of HCl (0.5 M) or NaOH (0.5 M) for acidic or alkaline conditions, respectively.

Adsorbent concentration was fixed to a previously determined value, 30 g/L, and the particles were treated with a NaOH solution (1.0 M) for 15 minutes, prior to each adsorption test, to increase the number of hydroxyl groups onto the surface of the particles [12]. A reciprocating shaker bath (Thermo Scientific 2870, Massachusetts) was used to agitate the solution/adsorbent mixture at 120 rpm for 120 minutes.

After contact time, adsorbent particles were removed from solution by using a magnetic retriever and treated again with a NaOH solution with a concentration of 1.0 M to desorb the metal cations and reuse the adsorbent.

The concentration of the metal cations, remaining in solution, was measured by atomic absorption spectroscopy, using a Varian SpectrAA 220 FS spectrometer (Varian Inc, Palo Alto). Metal cation adsorption efficiency was reported as removal percentage (% Rem) and calculated by using equation (11):

\[
\% \text{Rem} = \frac{100 \times (C_i - C_f)}{C_i}
\]  

(11)

Where \( C_i \) and \( C_f \) are the initial and final metal cations concentrations respectively.

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**Transparency document**

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**References**

[1] J. Manrique-Julio, F. MacHuca-Martinez, N. Marriaga-Cabrales, M. Pinzon-Cardenas, Production of magnetite by electrolytic reduction of ferric oxyhydroxide, J. Magn. Magn. Mater. (2016), https://doi.org/10.1016/j.jmmm.2015.10.018.

[2] R. Cornell, U. Schwertmann, The Iron Oxides, second ed., WILEY-VCH Verlag GmbH & Co, Weinheim, 2003.

[3] A.C. Larson, R.B. Von Dreele, General Structure Analysis System, GSAS), 2004, https://doi.org/10.1103/PhysRevLett.101.107006.

[4] H. He, Y. Zhong, X. Liang, W. Tan, J. Zhu, C.Y. Wang, Natural magnetite: an efficient catalyst for the degradation of organic contaminant, Sci. Rep. (2015), https://doi.org/10.1038/srep10139.

[5] J.-P. Jolivet, De la solution à l’oxyde. Condensation des cations en solution aqueuse, Chimie de surface des oxydes., 1994.

[6] A.H. Lu, E.L. Salabas, F. Schüth, Magnetic nanoparticles: synthesis, protection, functionalization, and application, Angew. Chem. Int. Ed. (2007), https://doi.org/10.1002/anie.200602866.

[7] H. Shokrollahi, A review of the magnetic properties, synthesis methods and applications of maghemite, J. Magn. Magn. Mater. (2017), https://doi.org/10.1016/j.jmmm.2016.11.033.

[8] J.P. Gustafsson, Visual MINTEQ 3.0 User Guide, Stockholm, 2014.
[9] V.C.G. Dos Santos, A.D.P.A. Salvado, D.C. Dragunski, D.N.C. Peraro, C.R.T. Tarley, J. Caetano, Highly improved chromium (III) uptake capacity in modified sugarcane bagasse using different chemical treatments, Quim. Nova. (2012), https://doi.org/10.1590/S0100-40422012000800021.

[10] S. Singha, U. Sarkar, S. Mondal, S. Saha, Transient behavior of a packed column of Eichhornia crassipes stem for the removal of hexavalent chromium, Desalination (2012), https://doi.org/10.1016/j.desal.2012.04.016.

[11] M. Szabó, J. Kalmár, T. Ditrói, G. Bellér, G. Lente, N. Simic, I. Fábián, Equilibria and kinetics of chromium(VI) speciation in aqueous solution – a comprehensive study from pH 2 to 11, Inorg. Chim. Acta 472 (2018) 295–301, https://doi.org/10.1016/j.ica.2017.05.038.

[12] B.A. Bolto, Magnetic Particle Technology: Desalination and Water Reuse Applications, Desalination, 1996, https://doi.org/10.1016/S0011-9164(96)00102-6.

[13] M. Hosseinza deh, S. Ali, E. Eb rahimi, S. Raygan, S. Morteza, A. Magnetic, Removal of cadmium and lead ions from aqueous solution by nanocrystalline magnetite through mechanochemical activation, J. Ultrafine Grained Nanostruct. Mater. 49 (2016) 72–79, https://doi.org/10.7508/jufgnsm.2016.02.03.

[14] L.J. Martínez, A. Muñoz-Bonilla, E. Mazario, F.J. Recio, F.J. Palomares, P. Herrasti, Adsorption of chromium(VI) onto electrochemically obtained magnetite nanoparticles, Int. J. Environ. Sci. Technol. (2015), https://doi.org/10.1007/s13762-015-0832-2.

[15] N.N. Nassar, Rapid removal and recovery of Pb(II) from wastewater by magnetic nanoadsorbents, J. Hazard Mater. (2010), https://doi.org/10.1016/j.jhazmat.2010.08.069.

[16] ISO (International Organisation for Standardisation), Determination of the Specific Surface Area of Solids by Gas Adsorption - BET Method, 2010, https://doi.org/10.1007/s11367-011-0297-3 (ISO 9277).

[17] E.P. Barrett, L.G. Joyner, P.P. Halenda, The determination of pore volume and area distributions in porous substances. I. Computations from nitrogen isotherms, J. Am. Chem. Soc. (1951), https://doi.org/10.1021/ja01145a126.