Remediation of soil and groundwater contaminated with organic chemicals using stabilized nanoparticles: Lessons from the past two decades

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1 Introduction

Groundwater is a vital drinking water source in many parts of the world. For example, groundwater accounts for 18% of China’s annual total water consumption (610 billion m³)

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(O’Carroll et al., 2013; MWR, 2015), and makes up one third of potable water supplies in England (WHO, 2006).

Yet, with the rapid urbanization and industrialization over the past decades, large volumes of soil and groundwater have been contaminated by various legacy and emerging organic chemicals. For instance, in China, the widespread environmental pollution has caused extensive groundwater contamination, and ca. 80% of the extractable shallow groundwater was found polluted (MEE, 2016).

Of the various priority contaminants, chlorinated solvents such as trichloroethene (TCE), tetrachloroethene (PCE), and carbon tetrachloride (TeCA) have been the most widely studied legacy pollutants in soil and groundwater. For instance, TCE was detected in over 1000 of the 1699 Superfund Sites in the US, and according to a US Geological Survey report, PCE, TCE and TeCA were detected in 8.9%, 5.1% and 4.7%, respectively, of the >5000 wells studied throughout the conterminous United States (Moran et al., 2007). Due to continued uses in many industrial sectors, thousands of sites have been found contaminated with chlorinated solvents throughout Asia, Europe and other industrialized areas in the world over the past decades, and the concentration of the chlorinated solvents in groundwater was found to reach the mg/L level (Azzellino et al., 2019; Squillace and Moran, 2007).

In addition, numerous other legacy and emerging organic contaminants have been detected in contaminated soil and groundwater, such as pesticides, dioxins, polychlorinated biphenyls (PCBs), polycyclic aromatic hydrocarbons (PAHs), pharmaceuticals and personal care products (PPCPs), flame retardants, and plasticizers. For examples, PAHs were found in >600 of the 1408 National Priorities List sites designated by the US Environmental Protection Agency (EPA) (Duan et al., 2015). A recent study in Ireland revealed that mecoprop, phenoxyacetic acid, and 2,4-dichlorophenol were detected in 36%, 39%, and 26% of the 730 groundwater samples collected in 6 agricultural sites (McManus et al., 2017). According to a national reconnaissance of pharmaceuticals and other organic contaminants in the US groundwater, which analyzed groundwater samples from a network of 47 sites across 18 states, organic contaminants were detected in 81% of the samples, with the most frequently detected compounds including N,N-diethyliouluamide (35%), bisphenol A (30%), tri(2-chloroethyl) phosphate (30%), sulfamethoxazole (23%), and 4-octylphenol monoethoxylate (19%) (Barnes et al., 2008). More recently, per- and polyfluoroalkyl substances (PFAS) have been found at more than 400 military sites in the US.

These organic chemicals are often recalcitrant to natural degradation and can be retained in soil and groundwater for decades or even hundreds of years, causing long-term threat to the environmental and human health.

To mitigate the associated environmental risks, various remediation methods have been studied or applied to remove or degrade organic contaminants in soil and groundwater, including pump and treat (P&T), permeable reactive barriers (PRBs), soil replacement, soil washing, electrokinetic removal/degradation, phytoextraction, and thermal treatment (Gong et al., 2018). For instance, since the 1980s, P&T has been widely applied to contaminated sites; but this ex-situ technique suffers from poor efficiency, contaminant redound, tailing and back diffusion, long remediation time, and high energy consumption (O’Connor et al., 2018). Likewise, since its invention in the 1990s, PRBs have been widely employed in the subsurface to intercept and transform contaminants in groundwater (Obiri-Nyarko et al., 2014). In 1991, O’Hannesin and Gillham (1992) applied granular zero valent iron (ZVI) in a PRB for in situ removing TCE and PCE in groundwater. Other than ZVI, many other materials have been tested for in situ remediation of groundwater contaminated with halogenated organics, phenolic compounds, pharmaceuticals, and nitroaromatics (Guan et al., 2015). For instance, zeolite (Vignola et al., 2011), calcite (Turner et al., 2008), pyrite (Wang et al., 2020), combined calcium peroxide and straw/biochar (Liu et al. 2019) have been used or tested as PRB filling materials. In addition, biochar (Tang et al., 2013), mackinawite (FeS) (Jeong and Hayes, 2007; Duan et al., 2019b), FeS-modified ZVI (Duan et al., 2019a; Kim et al., 2011; 2013), and MnO2-activated persulfate (Mazloomi et al., 2016) have been tested to remediate soil and groundwater contaminated with organic pollutants. However, PRBs are held back not only by the high installation cost, but also the reactive lifetime of the active materials, and may not be suitable for many soil geological and hydraulic conditions; and the bulk materials are limited to only amending surface soil for the poor deliverability in soil.

Over the last two decades or so, the development of innovative nanomaterials, in particular, stabilized nanoparticles, has brought about some major changes in groundwater and soil remediation. Stabilized nanoparticles offer some unprecedented advantages over traditional bulk materials, including much larger specific surface area, higher activity, and soil deliverability. Especially, because of the improved soil transportability, stabilized nanoparticles can be directly delivered into the source zone in contaminated soil or deep aquifers to destroy the contaminants in situ (Gong et al., 2018). Figure 1 shows a conceptualized schematic of in situ dechlorination of TCE and polychlorinated biphenyls (PCBs) as well as reduction of nitrobenzene by injection of stabilized ZVI nanoparticles into the contaminated source area. Compared to conventional remediation technologies, the in situ remediation by stabilized nanoparticles offers some key advantages, including: 1) it is less destructive and more cost effective, 2) it can proactively attack pollutants in source zones, and thus cuts down the remediation timeframe (Karn et al., 2009; Zhao et al., 2016), and 3) it...
can reach contaminant plumes in deep aquifers or in areas where conventional technologies cannot be applied.

The concept of direct injection of nanoscale ZVI (nZVI) for in situ dechlorination in the subsurface was first proposed in 1997 by Wang and Zhang (1997). After 4 years, Elliott and Zhang (2001) conducted the first field test for in situ dechlorination by delivering non-stabilized bimetallic (Fe/Pd) particles into a contaminated subsurface. However, this study and many follow-on studies revealed that the nanoparticles are prone to rapid aggregation, hindering the transport and deliverability of the nanoparticles (Elliott and Zhang, 2001).

To facilitate particle delivery, various particle stabilization methods have been investigated in the past 20 years. Typically, some macromolecules are coated on the surface of nanoparticles either during the nanoparticle formation (pre-aggregation stabilization) or after the particles (post-aggregation stabilization) are formed, and the resulting electrostatic or/and steric repulsion forces keep the nanoparticles from aggregation (Zhao et al., 2016). The earliest work on the particle stabilization for environmental applications was for stabilizing ZVI nanoparticles, where Zhao and coworkers at Auburn University first invented a method for preparing highly stable ZVI nanoparticles by adding a low cost stabilizer (starch or carboxymethyl cellulose (CMC)) during the particle synthesis (He and Zhao, 2005, 2007). The resulting nanoparticles have been considered the most deliverable ZVI nanoparticles so far, and have been tested or applied in several field scale tests or practices for in situ degradation of chlorinated solvents in soil and groundwater (see Section 3.1). Following the similar particle stabilization mechanisms, our group and others have also developed several other stabilized nanoparticles, such as Fe₃O₄, FeS, Fe-Mn binary oxides, and Fe₃(PO₄)₂.

Stabilized nanoparticles offer some unique features over conventional granular or powder materials, including: 1) stabilized nanoparticles remain dispersible in water and soil, maximizing soil deliverability and the specific surface area and reactivity of the nanoparticles, 2) the particle size, transportability and reactivity may be manipulated by using stabilizers of different physical-chemical properties (e.g., molecular weight, degree of substitution, functional groups, and hydrophobicity), especially when the pre-aggregation stabilization technique is applied (Zhao et al., 2016), and 3) stabilized nanoparticles may be directly delivered into the source zones to remediate contaminated soil/groundwater in situ.

Numerous bench-scale studies have been reported over the last decade or so to demonstrate the effectiveness of stabilized nanoparticles for potential in situ degradation of organic contaminants in soil and groundwater (He et al., 2007; Wei et al., 2010; Swindle et al., 2014). In addition, increasingly more field-scale studies have been also carried out, which have unveiled the pros and cons of the nanoparticle-based in situ remediation technologies (O’Carroll et al., 2013; Wu and Zeng, 2018). While these studies have demonstrated tremendous potential of the stabilized nanoparticles, they also revealed some challenges in the engineering applications, including: 1) highly stable and well dispersed nanoparticles are required to facilitate delivery of the nanoparticles in the subsurface and to avoid plugging the porous media; 2) the mobility of the injected nanoparticles need to be further improved to achieve homogeneous distribution of the nanoparticles in the target zones with a significant radius of active zone; 3) the long-term impacts on the local biogeochemical conditions remain poorly understood; and 4) the long-term fate and transport of the delivered nanoparticles need to be investigated.

Overall, this work aims to critically overview the evolution and some recent development of stabilized nanoparticles for degradation of organic contaminants in soil and groundwater. The specific objectives are to: 1) overview fundamental mechanisms in nanoparticle stabilization; 2) summarize key applications of stabilized nanoparticles for in situ remediation of soil and groundwater contaminated by legacy and emerging organic chemicals; 3) update the latest knowledge on the environmental impacts, fate and transport of stabilized nanoparticles; 4) address the merits and constraints of stabilized nanoparticles in environmental remediation applications; and 5) examine the knowledge gaps and future research direction of stabilized nanoparticles for remediation of contaminated soil and groundwater.

Per instructions of this invited special issue, this review is focused on contributions from our group, which, however, is supplemented by important relevant works by others. The knowledge gained is expected to further advance the science and technology in the environmental applications of stabilized nanoparticles.

## 2 Stabilized nanoparticles

### 2.1 Basic chemistry for synthesis of engineered nanoparticles

Generally, there are two strategies to fabricate nano-sized particles (Wiesner and Bottero, 2007; Zhao et al., 2016), including 1) top-down, namely to break down the large pieces of materials into nano-sized particles through physical methods such as ball-milling and grinding; and 2) bottom-up, namely to build up the nano-sized materials from atomic or molecular entities. The bottom-up approach has been more commonly used to prepare nanoparticles with better controlled properties, and thus will be the focus in this review.

Typically, iron-based nanoparticles, such as ZVI, magnetite and FeS, are synthesized through redox reactions and/or precipitation processes in aqueous solution starting with Fe²⁺ and/or Fe³⁺. The formation of
nanoscale clusters typically undergoes 4 steps (Wiesner and Bottero, 2007): 1) formation of zero-charged precursors, usually with redox reactions, hydroxylation and complexation involved; 2) nucleation, namely the zero-charged precursors assemble and condense through olation or oxolation; 3) growth of the nuclei to saturation or solubility limit for the precursors; and 4) aging stage, at which the minimum activation energy is reached and thermodynamically stable clusters/nanoparticles are formed. To produce nanoparticles with desired size, crystalline structure, and morphology, all of these 4 steps should be well-controlled.

For environmental applications (e.g., water treatment and soil remediation), several key criteria must be taken into account in the material synthesis, including: 1) the nanoparticles must be non-toxic, 2) the synthesis should avoid uses of toxic and expensive organic solvents, i.e., aqueous solution based synthesis is preferred, and 3) the overall process should be simple, low-cost and environmentally benign.

In line with these criteria, iron-based nanomaterials have been the most preferred nanomaterials for environmental uses, such as ZVI, iron sulfide (FeS), magnetite (Fe$_3$O$_4$), iron phosphate (Fe$_3$(PO$_4$)$_2$), binary metal oxides (Fe-Mn oxides), and sulfidated ZVI (S-nZVI).

ZVI has been the most studied iron-based nanoparticles (Liu et al., 2015). Nano-sized ZVI materials (typically aggregates of nanoscale primary particles) can be synthesized through high energy ball-milling (a top-down method), or reductive precipitation (bottom-up), or gas-phase reduction of nanoscale iron oxide (Zhao et al., 2016). Wang and Zhang (1997) pioneered the use of ZVI for treating chlorinated solvents in water, where clustered ZVI particles were prepared by reducing Fe(III) using NaBH$_4$. Since then, the borohydride reduction method has been widely used, though different precursors and reducing agents have also been employed (Zhao et al., 2016). Equation (1) illustrates the reductive formation of elemental Fe$^0$ from Fe(II) or Fe(III).

$$\text{Fe}^{2+} (\text{or Fe}^{3+}) + \text{reducing agent} \rightarrow \text{Fe}^0 \quad (1)$$

The nucleation of the resulting Fe$^0$ gives the clustered ZVI particles or aggregates. Typically, inert or anoxic conditions are desired during the synthesis to assure efficient reduction and avoid oxidation of the ZVI particles. Sodium/potassium borohydride is a strong reducing agent but comes with a relatively high cost. Consequently, some cheaper and “greener” reducing agents were also tested such as tea-based polyphenolic compounds (Hoag et al., 2009) or sorghum bran extracts (Njagi et al., 2011), but the resulting ZVI nanoparticles exhibited different morphologies and size distributions and weakened reactivity due to the slower nucleation and particle growth rates.

FeS nanoparticles have drawn extensive interests in environmental remediation recently for the moderate reducing power, longer-lasting reactive life than ZVI, and strong sorption capacity toward many heavy metals (Gong et al., 2016a). Conventionally, FeS nanoparticles can be synthesized through mixing stoichiometric amounts of Fe(II) and S$^2$ under inert or anoxic conditions as shown in Eq. (2) (Gong et al., 2016a),

$$\text{Fe}^{2+} + \text{S}^{2-} \rightarrow \text{FeS} \quad (2)$$

Magnetite (Fe$_3$O$_4$) nanoparticles have been shown to offer high adsorption capacities toward many important contaminants such as arsenic and chromium due to the larger specific surface area (Liang et al., 2012; Liang and Zhao, 2014). Generally, magnetite particles are prepared...
per the classical precipitation approach (Anderson, 1956). Typically, a base solution (NaOH or NH₃) is introduced dropwise into the solution containing Fe(III) and Fe(II) at a molar ratio of 2:1, thereby transforming Fe(III) and Fe(II) into FeOOH and Fe(OH)₂, respectively, as shown in Eqs. (3) and (4). During the follow-on aging stage, FeOOH reacts with Fe(OH)₂ to form the magnetite particles Eq. (5).

\[
\text{Fe}^{3+} + 3\text{OH}^- \rightarrow \text{Fe(OH)}_3 \rightarrow \text{FeOOH} + \text{H}_2\text{O} \tag{3}
\]

\[
\text{Fe}^{2+} + 2\text{OH}^- \rightarrow \text{Fe(OH)}_2 \tag{4}
\]

\[
2\text{FeOOH} + \text{Fe(OH)}_2 \rightarrow \text{Fe}_3\text{O}_4 + 2\text{H}_2\text{O} \tag{5}
\]

Iron or calcium phosphate compounds have been found effective for sequestering heavy metals such as Pb²⁺ and Cu²⁺ through the formation of metal phosphate precipitates and surface complexation (Liu and Zhao, 2007, 2013). Liu and Zhao (2007) synthesized iron phosphate nanoparticles through a straightforward stoichiometric precipitation approach per Eq. (6) (Liu and Zhao, 2007),

\[
3\text{Fe}^{2+} + 2\text{PO}_4^{3-} + 8\text{H}_2\text{O} \rightarrow \text{Fe}_3(\text{PO}_4)_2 \cdot 8\text{H}_2\text{O} \tag{6}
\]

Binary metal oxides are commonly found in lithosphere and pedosphere, and show high affinity to metalloid anions (As or Se oxyanions). Fe-Mn binary oxides have been the most studied binary particles for treating arsenic and other metal/metalloids in water. Typically, Fe-Mn binary oxide particles are prepared by reacting Fe(II) with KMnO₄ to form a mixed phase of Fe₂O₃ and MnO₂, following the stoichiometry of Eqs. (7) and (8) (An and Zhao, 2012),

\[
3\text{Fe}^{2+} + \text{MnO}_4^- + 4\text{OH}^- + 3\text{H}_2\text{O} \rightarrow 3\text{Fe(OH)}_3 + \text{MnO}_2 + \text{H}^+ \tag{7}
\]

\[
2\text{Fe(OH)}_3 \rightarrow \text{Fe}_2\text{O}_3 + 3\text{H}_2\text{O} \tag{8}
\]

S-nZVI has been recently synthesized through one-step or two-step synthesis method to enhance the reactivity and selectivity of pristine ZVI (Kim et al., 2011; Gong et al., 2017; Duan et al., 2019a). In the one-step method, a mixture of borohydride and dithionite solution is dropwise added to the Fe³⁺ solution. The dithionite decomposes through Eqs. (9)–(11) to produce sulfide (Kim et al., 2011), and Fe⁰ and FeS were simultaneously formed via Eqs. (1) and (2) in one pot,

\[
2\text{S}_2\text{O}_4^{2-} + \text{H}_2\text{O} \rightarrow 2\text{HSO}_3^- + \text{S}_2\text{O}_3^{2-} \tag{9}
\]

\[
\text{S}_2\text{O}_4^{2-} + \text{S}_2\text{O}_3^{2-} + 2\text{H}_2\text{O} + \text{H}^+ \rightarrow 3\text{HSO}_3^- + \text{H}_2\text{S} \tag{10}
\]

In the two-step method, Fe⁰ is first formed according to Eq. (1), then a sulfur source is introduced to react with remaining Fe²⁺ to form FeS via Eq. (2) but in the presence of Fe⁰, resulting in a core-shell structure FeS-on-Fe⁰ particles (Duan et al., 2019a).

### 2.2 Principles of nanoparticle stabilization

In the nanoscale, surface forces far exceed gravity. As such, surface interactions dominate the physical stability of the nanoparticles. Moreover, nanoparticles possess very high surface energy and thus are thermodynamically unstable, i.e., they tend to agglomerate into larger particles and/or react with the media. Agglomeration of nanoparticles usually occurs in three manners (Zhao et al., 2016), including 1) Ostwald ripening, i.e., smaller or ‘immature’ particles may dissolve and become feeding materials for larger particles, leading to an increase of the mean particle size; 2) arrested precipitation (precipitation facilitated by formation of nucleation centers); and 3) attractive interactions between particles (e.g., van der Walls and magnetic forces).

Depending on the extent, aggregation can alter the physico-chemical properties of the particles and affect the environmental uses of nanoparticles. For instance, aggregated nanoparticles may partially or completely lose the characteristics of nanoscale particles such as high specific surface area, high reactivity, high-surface-to-volume ratio, and size-dependent physico-chemical properties. In addition, aggregated nanoparticles are much less transportable in soil or sediment (He et al., 2007). Consequently, particle stabilization is often required to resist aggregation and to obtain a stable dispersion for intended uses.

According to the classic Derjaguin-Landau-Verwey-Overbeek (DLVO) theory, the net interaction energy between particles is the sum of repulsive energy and attraction energy (Phenrat et al., 2008). Typical attractive forces include van der Waals and magnetic attraction, whereas repulsive forces include electrostatic double layer repulsion, osmotic repulsion and elastic-steric repulsion. Coating nanoparticles with a proper stabilizers and at an appropriate concentration can increase the energy barrier between two approaching nanoparticles by enhancing the repulsive forces.

A stabilizer can function in two ways to increase the dispersion stability: 1) surface modification, i.e., charged stabilizer molecules are attached to particle surfaces, inducing electrostatic repulsion between like-charged surfaces; and 2) network or steric stabilization, i.e., stabilizer molecules (usually long-chained macromolecules) are attached on the surface to form a network to induce steric or osmotic separation of the nanoparticles. Accordingly, three particle stabilization mechanisms are often cited, namely, 1) electrostatic stabilization (charged
Stabilizers are sorbed on the surface to create/enhance the electrostatic double layer repulsion due to Coulombic forces; 2) steric stabilization (osmotic repulsion occurs when the layers of macromolecules on approaching particles overlap); and 3) electrosteric stabilization (the combination of electrostatic and steric repulsions. In some cases, network stabilization may also refer to particle separation due to the formation of a dense viscous gel matrix between two particles due to hydrogen bonding and polymer entanglements, which may occur at high doses of large viscous macromolecules (Comba and Sethi, 2009). However, it is probably more accurate to refer to this type of particles as networked or bridged nanoparticles because they often appear as large flocs that settle by gravity and cannot form a stable suspension.

Stabilizers may be introduced into a dispersion before or after the aggregates are formed, which are termed as pre-agglomeration and post-agglomeration stabilization, respectively (Fig. 2). For pre-agglomeration stabilization, stabilizers are added before or during the nucleation and growth and aging of nanoparticles, and thus, pre-agglomeration stabilization often results in smaller and more uniform nanoparticles. For example, highly stable stabilized ZVI nanoparticles were prepared in the presence of CMC as a stabilizer (Fig. 2). In contrast, in post-agglomeration stabilization, the stabilizers are applied after the aggregates of nanoparticles are formed, where the formed aggregates are broken into finer particles via external energy (e.g., sonication) in the presence of a stabilizer. In this case, the size of the resulting particles will be dependent on efficiency of the aggregate breakage, and thus, post-agglomeration stabilization is often less efficient than pre-agglomeration approach in terms of both particle size and reactivity. For instance, Cho and Choi (2010) found that pre-agglomeration stabilized ZVI nanoparticles were more reactive than bare ZVI particles when tested for dechlorination of chlorinated solvents, whereas Phenrat et al. (2009) reported that the post-agglomeration stabilization did not enhance the reactivity of bare nZVI. In addition, for reactive nanoparticles like ZVI, the sonication process could also induce elevated corrosion of the particles, resulting in significant reactivity loss (Tratnyek et al., 2011).

2.3 Effect of stabilizer on particle reactivity for target contaminants

In a typical aqueous suspension, stabilizer molecules will distribute between the aqueous phase and the nanoparticle surface. As shown in Fig. 3, stabilizers can influence the interactions between nanoparticles and a target contaminant in a number of ways. First, adsorption of stabilizers on the particle surface can alter the surface properties, such as the surface charge/potential and accessibility. As a result, the modified surface becomes more selective toward different contaminants. For example, coating negatively charged CMC on Fe₃O₄ or Fe-Mn binary nanoparticles turned the surface much more negative than that for starch-modified counterparts. Consequently, starch-modified nanoparticles showed more favorable adsorption for arsenate (An and Zhao, 2012; Liang et al., 2012; Liang and Zhao, 2014); conversely, CMC-stabilized FeS nanoparticles were more favorable for taking up cationic heavy metals such as Hg²⁺ (Gong et al., 2014). Second, stabilizer
molecules may compete with the target contaminants for
the adsorption/reaction sites on the nanoparticle surface, or
adsorption of stabilizers may block some of the reactive
sites or render the sites less accessible. This is particularly
the case when small-molecule stabilizers are used. For
instance, previous studies on stabilized Pd, Fe-Pd and FeS
nanoparticles indicated that glucose-modified Pd nanopar-
ticles were less reactive as a catalyst than CMC-stabilized
Pd because the adsorbed glucose layer was much denser
than the CMC layer (He and Zhao, 2008; Gong et al.,
2014). Moreover, the presence of too much stabilizer on
the particle surface can inhibit the contaminant mass
transfer and reactivity (Gong et al., 2014). Third, some
organic stabilizers (especially those with quinone and
phenol moieties) may serve as a catalyst or electron shuttle
to facilitate redox reactions between the nanoparticles
(e.g., ZVI and FeS) and the contaminants (Tratnyek et al.,
2011). Lastly, while most stabilizer molecules are expected
to be adsorbed on the surface, some remain dissolved in the
solution. These free molecules can complex with the target
contaminants (e.g., CMC-Hg²⁺), resulting in increased
solubility/mobility of the target chemicals.

The overall effects of stabilizers are the sum of all the
interactions. Therefore, the selection of the most suitable
stabilizer should consider a number of factors, including
type of the nanoparticles, properties of the target
contaminants, stabilizer molecular size, charge, and
functional groups, environmental friendliness, and cost.
When used for soil or groundwater remediation, environ-
mental factors including soil properties, particle deliver-
ability, and fate and transport of the stabilizers and
nanoparticles, should be taken into account as well.

2.4 Common types of stabilizers

For environmental remediation uses, stabilizers can be
divided into five groups (Zhao et al., 2016): 1) surfactants;
2) synthetic or natural macromolecules or polyelectrolytes;
3) viscosity modifiers; 4) oil emulsifiers; and 5) micro-

Surfactants are widely used surface modifiers to improve
the dispersion stability and the mobility of nanoparticles.
Both anionic and cationic surfactants can improve the
electrostatic repulsion between nanoparticles resulting in
enhanced particle stability. Surfactant molecules can exist
in the aqueous phase as monomers, aggregates and
micelles. Typically, micelles function better to disperse
colloids/nanoparticles. However, the formation of micelles
requires a dosage higher than the critical micelle
concentration, which may impede its practicality for field
applications. In addition, the toxicity of surfactants and the
possible solubilization effect on problem contaminants
should also be considered.

Natural bio-polymers including starch, guar gum,
xanthan gum have been used as neutral stabilizers for
engineered nanoparticles (Zhao et al., 2016), where
particle stabilization is achieved through the steric or
network repulsion mechanism. In contrast, engineered
functional polymers or macromolecules, such as CMC,
poly acrylic acid (PAA), polyaspartate, and poly styrene
sulfonate, are all negatively charged, which offer better
particle stabilization through concurrent electrostatic and
steric repulsion mechanisms. Overall, these bio-polymers
or synthetic polymers (especially, polysugars) are not only
effective stabilizers for many environmentally relevant
nanoparticles (e.g., ZVI, iron oxides, and Pd), but low-cost
and environmental friendly. There have been many of these
macromolecules available on the market, with different
molecular weights (few hundreds to million Daltons),
degrees of substitution (DS), and viscosity. The abundant
options provide a convenient means to manipulate the
nanoparticle growth and size by use of a suitable stabilizer
or a combination of two or more different stabilizers.

Some high molecular-weight macromolecules may
stabilize nanoparticles by increasing the suspension viscosity and network effect. For instance, xanthan gum (Comba and Sethi, 2009) and guar gum (Sakulchaicharoen et al., 2010) have been used as viscosity modifiers to inhibit aggregation of ZVI nanoparticles.

Oil emulsifiers can modify the hydrophobicity of nanoparticles, which are often desirable for remediation of dense non-aqueous phase liquids (DNAPLs). For instance, vegetable oil (along with some surfactants) was introduced in ZVI suspension to facilitate particle delivery and inhibit the particle corrosion in groundwater (Quinn et al., 2005).

Solid supports or protective solid coatings may also keep nanoparticles from aggregating. For instance, SiO2 or C-based materials (biochar, carbon nanoparticles, and carbon microspheres) have been used to support ZVI nanoparticles (Zheng et al., 2008; Sunkara et al., 2010; Wei et al., 2019), where nanoparticles are embedded on the surface or in the porous structure of the supports. However, such supported nanoparticles are not directly deliverable in soil, and as such, they are more suitable for water treatment or uses in PRBs in groundwater remediation.

Overall, our knowledge on particle stabilization has come a long way. The use of stabilizers, especially in the pre-agglomeration stabilization process, can facilitate formation of well stabilized aqueous suspensions of desired size and reactivity. Depending on the type of nanoparticles and their uses, different stabilizers may be used. To this end, there is a need for engineered stabilizers of controlled molecular weight (MW) and structure, functionality, and viscosity to optimize the performances of the resulting nanoparticles.

3 Stabilized nanoparticles for degradation of organic pollutants in soil and water

For environmental cleanup, the most promising uses of stabilized nanoparticles are for in situ remediation of contaminated soil due to the improved soil deliverability of the nanoparticles. In situ degradation of chlorinated solvents using stabilized ZVI nanoparticles has been one of the most studied subjects over the last two decades or so. Early studies showed that bare ZVI particles appear as micron to millimeter scale aggregates, which are hardly mobile or deliverable in soil (Schrick et al., 2004). Since the invention of the starch- and CMC-stabilized ZVI nanoparticles (He and Zhao, 2005; He et al., 2007), a great deal of effort has been devoted to developing various stabilized or surface modified nanoparticles that can be directly delivered into the contaminated soil. As shown in Fig. 3, CMC-stabilized Fe-Pd nanoparticles were transportable through a loamy sand column within 30 s under gravity, while bare Fe-Pd nanoparticles were completely blocked on top of the sand column (He et al., 2007). In addition, the CMC coating also mitigates adverse effects of the nanoparticles on biota. For instance, Lee et al. (2008) found that bare nZVI may invade and deactivate E.coli cells (Fig. 3), while Dong et al. (2016) reported that the presence of CMC coating reduced the cytotoxicity of ZVI nanoparticles due to surface electrostatic repulsive forces between the CMC-coated particles and the negatively charges cells. In fact, the presence of the polysaccharide stabilizers may induce some fortuitous positive effects. For example, in a pilot-scale study, He et al. (2010) reported that polysaccharide stabilizers (like CMC) could serve as a carbon source to stimulate the local bacteria activity and induce biodegradation of chlorinated solvents after delivery into the subsurface.

3.1 Reductive degradation of organic pollutants

Chlorinated solvents are the most widespread organic contaminants and have been listed as the priority contaminants in soil and groundwater (Stroo et al., 2003; Zimmermann et al., 2020). Typical chlorinated solvents include PCE, TCE, 1,1,2-trichloroethane (TCA), chloroform (CF) and other chlorinated aliphatic hydrocarbons (CAHs). ZVI nanoparticles (usually with Pd or another novel or transition metal as the catalyst) have been extensively studied for dechlorination of these chlorinated hydrocarbons. Equations (12)–(13) illustrate the redox
reactions in a typical dechlorination process, and Fig. 4 depicts the reaction mechanisms.

\[
\text{Fe}^0 \rightarrow \text{Fe}^{2+} + 2e^- \\
E_0 = -0.44 \text{ V at pH 7 (12)}
\]

\[
\text{RCl} + 2e^- + H^+ \rightarrow \text{RH} + \text{Cl}^- \\
E_0 = 0.5 - 1.5 \text{ V at pH 7 (13)}
\]

Typically, the dechlorination occurs through an initial adsorption followed by reductive breakage of the carbon-halogen bonds. Usually, a small fraction (~1%) of a secondary metal such as Pd, Ni or Cu is incorporated on ZVI to catalyze the dechlorination rate. As depicted in Fig. 4(a), the introduction of a metal catalyst can facilitate electron transfer and lead to production of more reactive atomic hydrogen (\(\text{H}^\cdot\)). In particular, \(\text{H}^\cdot\) adsorbed on the metal surface was found the predominant contributor to TCE dechlorination (He et al., 2018). In addition, particle stabilization can also speed up the reaction rate. Earlier, He and Zhao (2005) found that starch stabilized Fe-Pd bimetallic nanoparticles showed 37 times faster dechlorination rate for TCE than bare Fe-Pd nanoparticles, and later, the authors found that CMC-stabilized Fe-Pd nanoparticles offered two times faster dechlorination rate than starch-stabilized Fe-Pd nanoparticles due to increased specific surface area and the catalytic activity (He and Zhao, 2008). Zhang et al. (2011) reported the first systematic study of degradation of soil-sorbed TCE by CMC-stabilized Fe-Pd nanoparticles and found that the TCE sorbed by soil with higher soil organic matter (SOM) was more recalcitrant to the reductive dechlorination. The possible reasons include: 1) SOM may lessen the stabilizer effect, 2) adsorption of SOM may block the reaction sites for ZVI nanoparticles, 3) SOM may compete with TCE for electron donors, and 4) SOM may suppress the catalytic effect of Pd (Zhang et al., 2011). Moreover, this study demonstrated that the addition of some surfactants can enhance TCE desorption and degradation effectiveness by CMC-Fe/Pd, and the overall effect depends on the physiochemical properties of surfactants and soil characteristics (Zhang et al., 2011).

He et al. (2010) conducted a pilot-scale field study on in situ degradation of PCE, TCE and PCBs by delivering CMC-Fe/Pd into the contaminated subsurface. Two injections were administered, and the concentrations of the contaminants were followed for ~600 days. In the first injection, ~150 gallons of CMC-Fe/Pd (0.2 g/L) were gravity-fed into the 50-ft (15.2 m) deep unconfined aquifer. After one month, another batch of ~150 gallons were delivered but at a higher concentration (1.0 g/L). Analyses of PCE and TCE in the monitoring wells (located 1.5 and 3.0 m from the injection well) indicated that PCE and TCE were rapidly degraded with the highest degradation rate occurred in the first week of the injections. The concentrations of the chlorinated solvents rebounded to the pre-injection levels after ~2 weeks, indicating exhaustion of the ZVI's reactivity. However, the injection of CMC-Fe/Pd initiated a biological dechlorination that started after four weeks of the first injection and lasted throughout the monitoring period. After ~600 days, the combined concentration of TCE, PCE and their biodegradation byproducts in the two monitoring wells remained 40% and 61% lower than the pre-injection level. This was the first field evidence suggesting that CMC-Fe/Pd facilitated a rapid abiotic dechlorination in the early stage and then initiated a long-lasting biotic dechlorination process with CMC and \(\text{H}_2\) as additional sources of carbon and electrons.

One of the critical drawbacks of stabilized ZVI nanoparticles has been the relatively short reactive lifetime (hours to days) due to competitive side reactions such as corrosion by water or dissolved oxygen (DO). As such, stabilized ZVI nanoparticles should be prepared on site and used right before an attempt injection. To extend the reactive life and improve the reaction selectivity, S-nZVI have been prepared in recent years (He et al., 2018; Duan et al., 2019a). As shown in Fig. 4(b), the sulfidation may facilitate the electron transfer while suppressing the side corrosion reactions (He et al., 2018). Compared to pristine Fe-Pd, S-nZVI showed a 190 folds faster TCE degradation rate and 36 folds greater electron efficiency (He et al., 2018). He et al. (2018) also claimed that TCE dechlorination is more favorable at the FeS\(_x\) sites in S-nZVI, while other side reactions (e.g., corrosion) occur predominantly on the FeO\(_x\) sites; specifically, the FeS\(_x\) sites contributed ~72% to the TCE degradation based on the electron utilization efficiency while FeO\(_x\) contributed only ~28%. Moreover, S-nZVI degrades TCE mainly through electron transferring on the FeS\(_x\) sites, whereas the reactive atomic hydrogen mechanism played only a minor role (He et al. 2018). Fan et al. (2017) pointed out that sulfidation of nZVI may offer the following advantages: 1) it can generate more FeS\(_x\) phases thereby enhancing the dechlorination process, 2) sulfidation can suppress the formation of iron oxides on the particle surface resulting in less undesired reactions, and 3) it may immobilize metals by forming sparingly soluble metal sulfides.

Cai et al. (2018b) studied CMC-stabilized ZVI nanoparticles for reductive removal of nitrobenzene (NB) in water and a field soil (Cai et al., 2018b). The materials displayed 3.7 times higher reactivity toward NB degradation than bare ZVI based on the pseudo-first order reaction rate constants (0.643 vs. 0.175 min\(^{-1}\)). The study also revealed that the degradation reaction proceeded as NB \(\rightarrow\) nitrosobenzene \(\rightarrow\) phenylhydroxylamine \(\rightarrow\) aniline, where aniline is easily biodegradable (Zhao et al., 2019). Moreover, the stabilized nanoparticles at 0.6 g/L were able to nearly completely degrade soil-sorbed NB (0.01 mmol/
g). By comparing the NB desorption and degradation rates, the availability of electrons was found to be the rate-limiting step in the degradation of soil-sorbed NB.

While stabilized nanoparticles have shown to be a promising remediation technology, there are still several technical issues that need to be addressed. First, although stabilized nanoparticles were initially contemplated to be used for in situ remediation of contaminated soil, most studies so far have been focused on testing the particles’ reactivity in the aqueous phase. As such, there exists a data gap on the reactivity and transport behaviors of stabilized nanoparticles when used for treating soil-sorbed organic pollutants. Second, while CMC-stabilized nanoparticles appeared to be most transportable in soil, controlled deliverability of stabilized nanoparticles in the desired source zone remains a challenge, in most cases, the technology is limited by the limited transport distance. Third, more information is needed on the performances of stabilized nanoparticles under actual field conditions, and more pilot- and/or field scale data are yet to be collected to identify the most suitable stabilizers as well as the physical, geological, biogeochemical and hydrodynamic conditions. Fourth, the long-term reactivity, fate and transport of the delivered nanoparticles and the stabilizers need to be investigated. Fifth, the impacts of delivered nanoparticles on the soil physico-chemical properties, the local biogeochemical conditions, and the stability of other co-existing contaminants need to be investigated.

3.2 Stabilized nanoparticles as a catalyst

Stabilizers have been widely used in fabricating more reactive catalytic nanoparticles for water or soil treatment. Elemental Pd is a powerful catalyst and nanosized Pd particles (with an average size of 2.4 nm) were synthesized through a facile NaBH₄ reduction method with CMC as the stabilizer (Liu et al., 2008). The catalytic activities of CMC-stabilized Pd nanoparticles were examined through TCE hydrodechlorination reactions, and the observed pseudo first-order reaction rate constant was increased from 224 to 828 L/min/g and the mean particle size of Pd decreased from 4.7 to 2.5 nm when CMC content increased from 0.001 to 0.050 wt.% (Liu et al., 2008). The work also demonstrated the size-effect and the more active roles of corner and edge atoms of the Pd nanoparticles (Liu et al., 2008). To facilitate water treatment uses of the stabilized Pd nanoparticles, Bacik et al. (2012) loaded CMC-Pd onto a commercial porous Al₂O₃ support through an incipient wetness impregnation technique. The CMC-Pd nanoparticles were well-dispersed on the support and composite materials offered >7 times greater activity when used for TCE hydrodechlorination compared to commercial alumina supported Pd particles (Zhang et al., 2013). Low concentrations of SOM (< 10 mg/L) exhibited negligible effect on TCE hydrodechlorination, while high concentrations of SOM (>30 mg/L) decreased the rate constant for nearly 88% (Zhang et al., 2013). These studies confirmed that CMC or other similar polysaccharides may serve as effective stabilizers for preparing stable noble metal catalysts. To take advantages of the high catalytic activity of the stabilized nanoparticles, and to facilitate treating contaminants in water in standard reactors (e.g., batch or fixed-bed column), the nanoparticles can be deposited on low-cost supporting materials such as activated alumina and/or activated carbons. High temperature calcination may not be needed although moderate thermal treatment (~300 °C) can consolidate the particle loading and burn off the stabilizer after the loading (Zhang et al., 2013).

3.3 Oxidative degradation of organic chemicals using stabilized nanoparticles

PPCPs have been widely detected in groundwater, surface water, and soil owing to their widespread consumption and poor removal efficiency by conventional water treatment processes (Cai et al., 2018a; Hu et al., 2019; Wang et al., 2019). While reductive degradation is often more effective for halogenated organics, oxidation is the common degradation path for many PPCPs. As such, stabilized oxidizing nanoparticles have been prepared and tested to degrade PPCPs in groundwater and soil (Chen et al., 2012; Han et al., 2015; Han et al., 2017b).

MnO₂ has been a known oxidant and can oxidize pharmaceuticals (Du et al., 2018). For example, estradiol can be oxidized by MnO₂ to form estrone Eq. (14) and 2-hydroxyestradiol Eq. (15) (Jiang et al., 2009):

\[
\begin{align*}
C_{18}H_{24}O_2 + MnO_2 + 2H^+ &\rightarrow C_{18}H_{22}O_2 + Mn^{2+} + 2H_2O \\
C_{18}H_{24}O_2 + MnO_2 + 2H^+ &\rightarrow C_{18}H_{24}O_3 + Mn^{2+} + H_2O
\end{align*}
\]

However, the reaction rate with non-stabilized MnO₂ particles is rather slow due to the low specific surface area and limited reactive sites. To enhance the reactivity and facilitate soil deliverability, CMC-stabilized MnO₂ nanoparticles were prepared and tested for degradation of aqueous and soil-sorbed 17β-estradiol (Han et al., 2015; Han et al., 2017b). The CMC stabilization technique resulted in discrete and rather uniform-sized MnO₂ nanoparticles, with a mean particle size of 36.84±10.17 nm at a CMC-to-MnO₂ molar ratio of 1.39×10⁻³. Moreover, CMC-stabilized MnO₂ nanoparticles displayed much greater specific surface area, improved reactivity and improved soil deliverability. For example, when tested for oxidative degradation of estradiol in water, the apparent pseudo first-order rate constant \(k_a\) at pH 7 was increased.
from 0.067 h⁻¹ for non-stabilized MnO₂ to 0.071 h⁻¹ for CMC-stabilized MnO₂, and the 24 h removal was increased by 9% (Han et al., 2015). The advantages of stabilized MnO₂ nanoparticles became more evident when the nanoparticles were used to degrade soil-sorbed estradiol. After 96 h of reactions, 83% of estradiol in a soil slurry system was degraded using 2 × 10⁻² mol/L of CMC-stabilized MnO₂ nanoparticles, while only 70% of estradiol was degraded by the same dosage of non-stabilized MnO₂ particles. The improved reactivity was attributed to the protection of the CMC coating that complexes with inhibitive soil components (such as DOM, Ca²⁺, Mn²⁺, and their complexes). Moreover, CMC-stabilized MnO₂ displayed much improved soil transportability or deliverability. At a low injection pressure of 2.14 psi, the breakthrough of CMC-stabilized MnO₂ through a sandy loam soil bed occurred at ~3 pore volumes (PVs), and full breakthrough was reached at ~7 PVs with the C/C₀ plateau maintained at ~0.90 (i.e. 90% of the influent level). Stabilized MnO₂ nanoparticles were found evenly distributed along the column bed (Han et al., 2015). The soil deliverability enabled the nanoparticles to be used for in situ oxidative degradation of the estradiol or likely other PPCPs sorbed in soil. Up to 88% of water-leachable 17β-estradiol was degraded when an estradiol-laden soil was treated with 22–130 PVs of a CMC-stabilized MnO₂ suspension (MnO₂ = 0.174 g/L) (Han et al., 2017b).

The degradation involves a first-step adsorption of the solutes on the particle surface and then the oxidation reaction. As such, the degradation effectiveness can be influenced by factors that affect adsorption and reactivity of MnO₂, such as particle size, surface area, surface charge, and accessibility of the reactive sites. Lower pH was found to favor the reaction, which is attributed to the proton-catalyzed reduction of MnO₂ via Eq. (16). In addition, lower pH is associated with higher reduction potential, lower surface charge, and less adsorption of Mn²⁺ on the particle surface. Some leachable soil components such as Ca²⁺ and organic matter were found to inhibit the reaction in the early stage, but promoted the reaction in the longer term. The inhibition was due to the rapid uptake of DOM and cations onto the nanoparticles surface, blocking some of the reactive sites; however, over the longer run, DOM may serve as a scavenger for Mn²⁺ generated in the redox reaction process, alleviating the inhibitive effect (Han et al., 2015).

\[
\frac{1}{2}\text{MnO}_2(s) + 2\text{H}^+ + e^- \rightarrow \frac{1}{2}\text{Mn}^{2+}(aq) + \text{H}_2\text{O} \quad (16)
\]

The desorption rate of estradiol from soil was found to critically affect the degradation effectiveness. If the desorption is too fast, it may be flushed away to the downstream of the groundwater by the injected nanoparticle slurry, resulting in limited contact with the nanoparticles; conversely, slow desorption may limit the overall degradation rate. Therefore, the use of the in situ technology must consider the soil properties especially the SOM content and adsorption/desorption behaviors of the contaminants.

It should be noted that MnO₂ is a relatively weak oxidant, so it may not completely mineralize PPCPs, rather, it may transform the chemicals into less toxic byproducts. Thus, the MnO₂ oxidation may be combined with other processes such as advanced oxidation processes (AOP), if complete mineralization is desired (Du et al., 2018).

Stabilized ZVI nanoparticles may be used to induce Fenton-like reactions under oxic conditions to oxidize organic contaminants in water via reactive oxygen species (ROS) (Joo and Zhao, 2008). Compared to the classical Fenton reactions, the nanoparticle-induced Fenton process can proceed at relatively higher pH (>6). For instance, Joo and Zhao (2008) prepared and tested CMC-stabilized Fe/Pd bimetallic nanoparticles for degradation of lindane and atrazine (Joo and Zhao, 2008). Batch kinetic tests showed that under oxic conditions, the nanoparticles facilitated Fenton-like reactions, which led to oxidation of 65% of lindane within 10 min (initial concentration = 1 mg/L, ZVI dose = 0.5 g/L, Pd = 0.8% of Fe, initial pH = 7.9–8.4, final pH = 6.2–6.9). While the particle stabilization greatly enhanced the anaerobic degradation of lindane, the CMC coating was found to consume nearly 50% of the hydroxyl radicals generated from the nanoparticles-mediated Fenton process, leading to lowered degradation efficiency despite faster reaction rate. Therefore, more oxidation-resistant stabilizers should be explored for this purpose.

Compared to reductive nanoparticles, much less information is available on stabilized oxidative nanoparticles. The degradation pathway of oxidative process is not well understood, and the environmental impacts of the reaction by-products as well as the oxidative nanoparticles need to be investigated. Recent works have indicated that high concentrations of stabilized Fe₃O₄ and FeS nanoparticles under oxic conditions can cause oxidative stress and tissue damage toward zebrafish (Zheng et al., 2018a,b).

More reactive materials are needed, which can either directly extract electrons from the target contaminants or facilitate generation of highly reactive oxidizing species to completely mineralize the target contaminants. While solutions of strong oxidants such as permanganate or persulfate have been used to oxidize soil-sorbed organic contaminants, the solution form of these chemicals bears with some critical limitations, including: 1) the solution may move along with the groundwater and may spread and cause undesired side effects, and 2) due to the limited contact time with the target contaminants, the reactivity may not be well utilized and the effectiveness is severely limited by the desorption rate of the contaminants from the soil. Instead, once delivered, reactive nanoparticles may stay attached to the soil matrix and offer prolonged reactive life without affect the down-gradient flow. The particle
stabilization technique may also be extended to prepare photoactive materials for oxidative treatment of persistent organic chemicals by preparing photoactive semiconductors in the presence of a stabilizer. For instance, Xu et al. (2020a) prepared a type of iron oxide/carbon sphere composite material in the presence glucose that serve as both a carbon source and a stabilizer, and the new material showed much enhanced photoactivity toward perfluorooctanoic acid (PFOA).

3.4 Adsorptive removal of persistent organic chemicals using stabilized nanoparticles

Stabilized nanoparticles may also be used for adsorptive removal of persistent organic pollutants (POPs) in water or immobilization of POPs in soil or sediment. Gong et al. (2016b) prepared stabilized magnetite nanoparticles (Fe₃O₄) for removing PFOA from water. Batch kinetic experiments revealed that the starch-stabilized nanoparticles facilitated fast PFOA uptake with a sorption equilibrium time of 30 min, and provided 2.4 times higher adsorption capacity (maximum Langmuir capacity = 62.5 mg/g) than non-stabilized magnetite aggregates due to the smaller particle size and larger specific surface area. Fourier transform infrared (FTIR) spectra suggested that the main PFOA removal mechanism was inner-sphere complexation. Moreover, when tested in wheat germination, the starch-stabilized magnetite nanoparticles were able to mitigate the toxic effect of PFOA on the seeding growth. The results demonstrated promise of stabilized Fe₃O₄ nanoparticles as a “green” adsorbent for effective removal/immobilization of PFOA in soil and groundwater (Gong et al., 2016b).

Much more work has been done with stabilized nanoparticles for in situ immobilization of metals and metalloids (Liu et al., 2015; Zhao et al., 2016). However, much less information is available for organic chemicals. As adsorption of organic contaminants often involve carbonaceous materials, stabilized carbonaceous materials may be developed. For instance, Liu et al. (2016) prepared stabilized multi-walled carbon nanotubes (MWNTs) using CMC, starch and leonardite humic acid (LHA), and found the stabilization effectiveness ranked as CMC>starch>LHA. For chemicals of both hydrophobic and lipophobic properties, such as PFOA or perfluorooctanesulfonic acid (PFOS), stabilized composite materials consisting of carbonaceous materials and metal oxides may be developed to induce corporative adsorption mechanisms. For instance, Xu et al. (2020a,b) reported a new class of iron oxide/carbon sphere and carbon-bismuth phosphate composite materials. The composite materials were able to adsorb PFOA through interactions with both the head carboxylic groups and the structural –CF groups instead of the head only or tail only adsorption modes when individual metal oxides or activated carbon are used.

4 Transport of stabilized nanoparticles

As stated above, for in situ remediation of soil and groundwater, it is desirable to deliver the nanoparticles into the contaminated source zone, or to create a reactive zone by evenly distributing the nanoparticles in the target space. In general, non-stabilized particles are hardly deliverable in typical soil or sediment due to the strong soil filtration and/or straining effects. As such, proper particle stabilization is required to facilitate direct injection of the reactive nanoparticles into the source zone. This in situ remediation method is particularly advantageous when the contaminants are located deep in the aquifer or when surface remediation actions are not possible (e.g., when a contaminant plume is located under an existing structure). Alternatively, a permeable reactive zone may be built around a contaminant plume to contain its spreading by directly delivering stabilized nanoparticles without digging out the soil. To this end, understanding the transport properties of stabilized nanoparticles that are delivered in the soil is critical to set up the injection points and injection pressure, to assess the effective area, and to evaluate the maximum travel distance of the nanoparticles. It is also noteworthy that the transport behavior, and thus the suitability of the direct injection method, may be affected by the physical and biogeochemical properties of the porous media, such as hydraulic conductivity, mineral compositions, zeta potential, pH, and NOM (Lefèvre et al., 2016; Han et al., 2017a; Cai et al., 2018b; Ji et al., 2019).

4.1 Nanoparticle aggregation and transport theory

The classical DLVO theory has been widely adopted to interpret the aggregation behavior of nanoparticles (Liu et al., 2016). According to the theory, interactions between nanoparticles are governed by a superposition of van der Waals attractive forces and electrostatic double layer forces. Typically, the van der Waals attractive forces between nanoparticles are approximated by assuming spherical nanoparticles, but the unique shapes and compositions of nanoparticles induce the inaccuracy. Moreover, coating nanoparticles with an organic stabilizer causes additional steric repulsion forces, rendering the particle interactions occur only in the secondary minimum zone. As such, the forces, such as bridging, osmotic, steric, hydrophobic, Lewis acid-base, and magnetic forces, can be of equivalent magnitude as van der Waals attractive forces and electrostatic double layer forces. To deal with the restrictions of the classical model and to take into account the surface heterogeneities, several extended DLVO (XDLVO) models have been developed to evaluate the particle-particle and particle-collector interactions under more realistic conditions and/or in the presence of an organic coating (Phenrat et al., 2007; Hotze et al., 2010).

The transport of nanoparticles in saturated porous media
is typically interpreted by the filtration theory (Zhang et al., 2017). According to the classical filtration theory, nanoparticles are deposited on porous media following two consecutive steps: 1) transport of nanoparticles to the matrix surface by Brownian diffusion, interception, and gravitational sedimentation, and 2) deposition of the nanoparticles to the matrix surface (Kretzschmar et al., 1999). He et al. (2009) reported the first systematic study on the transport of CMC-stabilized ZVI nanoparticles through various porous media, and reported that Brownian diffusion was the predominant mechanism for the filtration of the nanoparticles, whereas gravitational sedimentation also played an important role, which account for 30% of the overall single-collector contact efficiency for coarse glass beads and 6.7% for a sandy soil.

It should be noted that the classical filtration model does not distinguish adsorption from other filtration removal mechanisms, although adsorption can play important roles in the overall removal of the nanoparticles (Han et al., 2017b; Zhang et al., 2017). To overcome this drawback, Zhang et al. (2017) developed a modified transport model by incorporating a Langmuir-type adsorption rate law into the classic convection-dispersion equation. Using experimentally derived adsorption parameters, the model was able to assess the role of adsorption in the transport of CMC-stabilized ZVI nanoparticles. Based on the experimental and modeling data, the filtration removal was found to be primary mechanism for particle retention at low flow velocities, whereas adsorption becomes more significant at elevated flow rates (Zhang et al., 2017).

4.2 Transport of stabilized nanoparticles in porous media

Stabilizers can affect the particle size, surface charge and interactions between the nanoparticles and the collectors, and thus affect the particle transportability in porous media (He et al., 2007). Liu et al. (2016) studied effects of CMC, starch and LHA on the aggregation and stabilization of MWCNs in aqueous suspensions. The researchers found that while all three stabilizers inhibited aggregation of the nanoparticles, the stabilization mechanisms differed, namely, the coating of negatively charged CMC enhanced electrophoretic mobility, the neutral starch slightly curbed electrophoretic mobility, and LHA hardly affected electrophoretic mobility of the particles. Moreover, CMC stabilizes the nanoparticles through enhanced electrostatic repulsion, primary energy barrier and steric hindrance, whereas starch and LHA work primarily through steric hindrance (Liu et al., 2016). Consequently, CMC demonstrated to be the most effective stabilizer. Among various reported commercial stabilizers, CMC exhibited 1–2 orders of magnitude lower attachment efficiency other commercial polymers (He et al., 2009).

Coating of CMC or other polyelectrolytes of higher MW on nanoparticles induces a higher charge density and steric barriers, resulting in enhanced electrosteric repulsion between the nanoparticles. He and Zhao (2007) found that CMCSs of higher MW resulted in much smaller ZVI nanoparticles and improved transportability. Saleh et al. (2008) and Liang et al. (2012) tested transport behaviors of ZVI particles modified through the post-agglomeration stabilization approach using a high MW (125 kg/mol) poly (methacrylic acid)-b-(methyl methacrylate)-b-(styrene sulfonate) triblock copolymer, a low MW polyaspartate biopolymer, and the surfactant sodium dodecyl benzene sulfonate (MW = 348.5 g/mol). While all the stabilizers rendered the zeta-potential of nZVI more negative, and the stabilizers with larger MW resulted in more negative zeta-potential and more transportable ZVI nanoparticles through a sand column. However, caution needs to be exercised that the higher the MW, the more viscous the stabilizer solution, which may impede the transport of nanoparticles in field soil. So far, CMC with MW of 90,000 has been most widely used as a stabilizer for a host of nanoparticles and has been shown most effective.

He et al. (2009) investigated the breakthrough behaviors of CMC-stabilized ZVI nanoparticles (size = 18.1±2.5 nm) through four saturated model porous media: sandy soil, clean sand, coarse and fine glass beads, and simulated the transport performance using both classical filtration theory and a modified convection–dispersion equation with a first-order removal rate law. A constant concentration plateau (C/C₀) was observed at full breakthrough, ranging from 0.69 for the soil to 0.99 for glass beads. The particle removal and maximum travel distance (Lmax) were found strongly dependent on the interstitial flow velocity, but only modestly affected by up to 40 mmol/L of calcium. He et al. (2009) also proposed a correlation method to estimate the Lmax based on flow velocity (or injection pressure). The simulation results indicate that once delivered, 99% of the nanoparticles are expected to stay in the soil matrix within 16 cm at a groundwater flow velocity of 0.1 m/day, but may travel over 146 m at a flow velocity of 61 m/d. Later, An et al. (2015) studied transport of CMC- or starch-stabilized Fe-Mn binary oxides nanoparticles and found that their transport distance can be harnessed by manipulating the injection pressure or the injection flow rate.

Johnson et al. (2013) investigated transport of CMC-stabilized nZVI in a field-scale large 3D model aquifer (10 m×10 m×2.4 m deep), and suggested that the very-aggressive flow conditions were necessary to achieve 2.5 m of nZVI transport using a hydraulically constrained flow path between injection and extraction wells. The authors also indicated that the particle injection altered the groundwater flow, likely due to hydrogen bubble formation, which diverted the nZVI away from the targeted flow path. Using a spectrophotometric method, the authors asserted that deployment of unoxidized nZVI for groundwater remediation would likely be difficult.

The field study by He et al. (2010) showed that when benchmarked against the bromide tracer, approximately
37.4% and 70.0% of the injected Fe were detected in the first monitoring well (1.5 m from the injection well) following the two injections, confirming the mobility or deliverability of CMC-Fe/Pd under the field soil setting. Moreover, the soil deliverability was further boosted when the injection pressure was elevated.

Bennett et al. (2010) carried out a series of three single well push-pull field tests to investigate the transportability of CMC-nZVI (0.2 or 1.0 g/L) or CMC-Fe/Pd (0.33 g/L) in a saturated aquifer. Monitoring the Fe concentration in the extracted groundwater indicated that the stabilized nanoparticles were transportable in the soil, but the mobility dropped with time, possibly due to the soil filtration effect. The results also suggested that the advective nanoparticle transport may be enhanced by circulating the groundwater/nanoparticle suspension between two wells and by maintaining high post-injection groundwater velocities.

The deviation between the bench-scale laboratory data and some of the larger-scale results can be attributed to many factors, including: 1) heterogeneity of field conditions (e.g., hydraulic conducted, adsorption and filtration characteristics of the soil), 2) particle stabilization conditions (type and concentration of CMC and the nanoparticles), and 3) injection pressure. While sufficiently high injection pressure should be supplied to facilitate particle transport, too high hydraulic pressure may lead to the “caking” effect at the wall of the injection well, leading to clogging the entrance pores. Instead of “pushing” from the injection well, a “pulling” technique may be exercised by extracting groundwater from a monitoring well. In all cases, the bottleneck for the direct injection approach remains to be the insufficient transportability or deliverability. Therefore, more effective particle stabilization strategies are needed. In addition, it is worth noting that the advective delivery (injection) of nanoparticle suspensions pushes away the existing aqueous contaminants without sufficient contact or reaction, and thus, direct injection of nanoparticles is best directed toward the stationary/sorbed contaminants or residual non-aqueous phase liquids within source zones (Bennett et al., 2010).

### 4.3 Factors affecting transport of stabilized nanoparticles

According to the filtration theory, soil retention of nanoparticles involves transport of nanoparticles to the collector’s surface and then deposition of particles to the soil matrix. Physical parameters such as surface coating agents, flow velocity, surface properties of soil and nanoparticles, and the accessible surface area can affect the mass transfer of the nanoparticles, whereas the solution and surface chemistry will govern the kinetics of the particle deposition (Kretzschmar et al., 1999; He et al., 2009; Zhang et al., 2013). For instance, Zhang et al. (2017) investigated the effects of aluminum oxide and iron oxide on the transport of CMC-ZVI nanoparticles by column breakthrough experiments, and observed that aluminum oxide and iron oxide coatings on quartz sand enhanced particle retention, reducing the full breakthrough plateau \((C/C_0)\) from 0.90 for plain sand to 0.76 when either of the metal oxides was coated on the sand. Both experimental and modeling resulting confirmed that the presence of both metal oxides increased the adsorption capacity of the nanoparticles, with the \(k_{ads}\) (adsorption coefficient) increased by a factor of 1.6–1.8, and the \(k_{fil}\) (filtration coefficient) increased by ~2.2 compared to the plain sand. At lower pore velocities, filtration was the primary mechanism for particle retention; however, at elevated velocities, adsorption became more significant. The presence of NOM (40–80 mg/L) and ionic strength (up to 200 mmol/L CaCl₂) had negligible effect on the breakthrough profiles of the nanoparticles. While a water-soluble neutral starch was also able to stabilize the nanoparticles, much larger (mean hydrodynamic diameter = 303 nm) were obtained, leading to a higher particle retention than CMC-nZVI. Moreover, the narrower pore size and larger specific surface area will result in more collisions, which are favorable for nanoparticle retention through the filtration mechanism. He et al. (2009) reported that media with >1.5 times greater specific surface area provided >10% greater removal efficiency for CMC-stabilized nZVI.

In addition to the material heterogeneity, variation of groundwater flow should be taken into account. Under elevated external pressure, the injected nanoparticle suspension may take a different path from the normal groundwater flow pattern, and sometimes it may be forced to be seeped out from the ground surface (e.g., in the case of shallow and unconfined aquifer).

In some real-world 3D systems, gravity may affect the particle flow pattern especially for metallic nanoparticles. Kanel et al. (2008) tested the 2-D transport of PAA-stabilized ZVI nanoparticles through a two-dimensional sand box under saturated, steady-state flow conditions, and found that the nanoparticle plume migrated downward as it moved horizontally through the porous media, indicating that the density gradients influenced on two-dimensional transport. A variable-density groundwater flow model SEAWAT was able to simulate the observed density-driven transport patterns.

Field water matrix and chemistry may alter the physical-chemical properties of the nanoparticles that are observed in the bench scale. For instance, Swindle et al. (2014) compared the size-dependent reactivity of magnetite nanoparticles (~6 nm, ~44 nm, and ~90 nm) in a field setting to a laboratory analog. Field results indicated that an organic coating developed on the particle surfaces, which inhibited the reactivity and dissolution of the nanoparticles, with the amount of dissolution decreasing
as particle size decreased, which reversed the size-dependent reactivity trends observed in laboratory investigations.

NOM may act as a stabilizer or bridging agent affecting particle aggregation and transport (Su, 2017). For instances, the coating of humic acid (HA) was found to lower the pH_{PZC} of magnetite nanoparticles, promoting the mobility of nanoparticles in negatively charged soil matrix (Hu et al., 2010). Cuny et al. (2015) reported that adsorption of HA on iron-based nanoparticles induced a more negative zeta potential, which did not alter the particle size but positively affected the particle mobility. However, the details about the impacts of different types and concentrations of HA on the aggregation and transport of nanoparticles are lacking.

Solution pH and ionic strength play a critical role in the aggregation of nanoparticles by regulating their surface potentials, which may be used to manipulate retention or transport of nanoparticles. For example, the pH_{PZC} of nZVI is generally lower than that of soil matrix, thus more nanoparticles may be retained in a soil matrix by adjusting the pH to a level (e.g., 6.4) where the surfaces of the nanoparticles and soil matrix are positively charged (Kim et al., 2012). It should be noted, however, that too low pH can cause dissolution of metal-based nanoparticles, and promote undesired corrosion of nZVI (Cai et al., 2018b), while too high pH may induce metal hydroxides precipitations inhibiting the particle reactivity.

Ionic strength, especially polyvalent cations, is expected to cause double-layer compression and facilitate particle aggregation and collector-particle interactions (Saleh et al., 2008). However, CMC appears to be able to resist such effects common groundwater conditions. For instance, He et al. (2009) and Zhang et al. (2017) observed that the presence of Ca\textsuperscript{2+} at up to 40 mmol/L only moderately affected the transport of CMC-stabilized nZVI. However, much greater effect of ionic strength should be expected for non-stabilized nanoparticles. For instance, Tosco et al. (2012) reported that under natural flow conditions, synthetic ferrihydrite nanoparticles were able to transport over 5–30 m at the normal ionic strength (2–5 mmol/L) in the tested European aquifers, but only traveled a few meters when the ionic strength was elevated to 10 mmol/L.

5 Concluding remarks and prospects

Building upon the classical colloid physics and chemistry, our understanding of stabilized nanoparticles has come a long way in the last two decades or so, and the momentum in their environmental remediation remains strong and diverse, especially in the field of in situ remediation of soil and groundwater. To maintain high reactivity and to facilitate soil deliverability of nanomaterials, various stabilizers and particle stabilization techniques have been investigated through numerous bench- and field-scale studies.

This review overviews the evolution of stabilized nanoparticles with respect to environmental cleanup uses, encompassing the fundamental principles and bench- to field-scale experimentations toward an innovative in situ remediation technology using stabilized nanoparticles. The merits and limitations of the remediation are discussed.

This review also revealed some critical research needs. In addition to the technology gaps mentioned in various sections, the following future research needs are identified:

1) While the particle stabilization technique can greatly improve the soil deliverability of nanoparticles, the transport distance remains a bottle neck for effective application of the technology, especially for soil of low permeability. There is a need to further modify the stabilization technique to facilitate the deliverability and distribution of stabilized nanoparticles into the target contaminated source zones.

2) Other surface modifiers than organic macromolecules should be sought to achieve particle stabilization, extended reactive lifetime and reaction selectivity toward the target contaminants. In this regard, recent works showed that sulfidation of ZVI in combination with CMC stabilization showed both enhanced stability and dechlorination reactivity; and loading sulfur on ZVI enhances particle hydrophobicity and thus selectivity toward hydrophobic compounds. Yet, caution need to be exercised that the addition of the surface modifiers may increase the particle size and impede the transportability when used for in situ remediation of soil.

3) Information on the long-term effectiveness and reactivity of the injected nanoparticles is lacking. Such long-term monitoring data, especially in the field-scale, are critical for assessing the technology effectiveness and optimizing the process design.

4) Although there has been no evidence showing that stabilized nanoparticles pose significant toxic effects on biota under environmentally relevant conditions and dosages, long-term monitoring data are needed to address the environmental fate and impacts of the nanoparticles delivered in the subsurface. Further studies are needed to investigate how delivered nanoparticles affect the biogeochemical conditions and mobility of other chemicals (especially heavy metals) in the subsurface, in particular under field conditions; likewise, the effects of local environmental conditions on the fate, transport and transformation of the nanoparticles should be investigated.

5) The effect of the delivered nanoparticles on the hydraulic conductivity should be further confirmed at the field scale and over extended period of time.

6) Mechanistically sounder transport model that couples adsorption/desorption and chemical transformation rates is needed for better predicting remediation time and the transport and fate of stabilized nanoparticles in soil.
7) While many studies have revealed the promise that stabilized nanoparticles may enhance microbial degradation of organic contaminants, further cross-disciplinary studies are needed to understand the synergistic or antagonistic interactions of stabilized nanoparticles and microbial activities to facilitate more efficient application of the technology.

8) More field work is needed to determine the most suitable field conditions (soil properties and geology, groundwater flow characteristics and water chemistry) and to assess the effects of environmental parameters on the effectiveness of the nanomaterials. The information is essential for scaling up treatment designs derived from bench-scale experiments.

9) While the in situ remediation technology holds the potential to be more cost-effective and can treat contaminated aquifers that cannot be by other existing technologies, a comprehensive cost-benefit analysis approach is needed to justify the economic and technical feasibility, as well as the environmental benefits.

10) The applicability of stabilized nanoparticles in unsaturated media needs to be investigated.

11) While stabilized nanoparticles may not be suitable for treating contaminants in water due to separation issues, they may be loaded on high-surface area porous supports such as activated alumina or carbons. Alternatively, bridged or networked nanoparticles may be developed by using large polymeric bridging agents or CMC/starch at low concentrations.

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