1. Introduction

Heat pipes can be used to enhance the amount of heat transfer. Since heat transmitted through a heat pipe is based on phase change, it can be pointed out that using a heat pipe with similar dimensions of a solid metal pipe, larger amounts of heat transfer will be obtained [1]. Due to the two-phase characteristics, the heat pipe is ideal for transferring heat over long distances with a very small temperature drop and for creating a nearly isothermal surface for temperature stabilization. As the working fluid operates in a thermodynamic saturated state, heat is transported using the latent heat of vaporization instead of sensible heat or conduction where the heat pipe then operates in a nearly isothermal condition [2 and 3].

Their application is wide and can be used, for example, in energy conservation, such as heat recovery in hot exhaust gas system, and for use in domestic and industrial applications. Solar heating is also another example for the application of heat pipes [4 and 5]. For example, a heat pipe solar collector is widely used nowadays [6 and 7].

Optimization of condenser plays important role in efficient operation of the system. In order to improve the performance of condenser it is required to elaborate thermal analysis for different mass flows and temperatures. In this article different power of condenser in regard to various mass flows and the temperatures on the heat pipe of condenser are investigated.

2. Condenser design

In this section, the heat power and pressure drop of condenser are calculated. The investigated system consists of the condenser (see Fig. 1). Condenser is placed on the heating zone of heat pipe and is used for efficient heat transfer from one medium to another. The water is used as a working fluid in the heat pipe and in the condenser is used thermal oil as cooling medium which is pumped through the connection (see Fig. 1).

![Fig. 1 Heat pipe condenser](image)

The main objective of this work was to identify the pressure build-up in the condenser (dP), the outlet temperature of the thermal oil (Tout) and the output effect (quantity kW added to the thermal oil).

This task was done for the different temperatures on the heat pipe 100°C -150°C -200°C -250°C -300°C (the temperature was constant over the whole surface), with flow 10-20-30-40 g/s of thermal oil, with the fixed inlet temperature of 80°C. The aim of
the task is to design stationary simulation of the heat exchanger to cool the condenser of the heat pipe.

3. CFD Modelling

Computer modelling reduces the total effort required in the experiment design and data acquisition. Numerical simulation of this case was used in order to predict fluid flow, heat transfer and pressure over the condenser.

Physical model

The 3D model of a heat exchanger was created based on the drawings and subsequently was modified to be able to use simulations in finite volume. Calculated model consists of a heated finned tube, jacket and oil (see Fig. 2).

Thermal oil is pumped in through the connection and then it spins around the heat pipe via the three parallel tracks before it comes out again through the second connection.

The most important part of the work was the determination of the detailed boundary conditions. In Table 1 are boundary conditions that were set at the inlet of condenser.

4. Analysis of results

In this section are presented results of numerical solution for the heat pipe condenser. In Fig. 3 is shown a position of the line where the output temperatures were calculated. This line is situated in the middle of distance between the jacket and heat pipe. In this point average values of temperature and pressure were calculated.

Results of case No. 1:
- Numerical simulations for mass flow of thermal oil 0.01 kg.s⁻¹;
- Temperature on the heat pipe was set as follows: 100°C - 150°C - 200°C - 250°C - 300°C.

In Table 2 are presented results of five different simulations for following parameters:
- Output temperature of the thermal oil (Tout)
- Heat power of the condenser (Q)
- Differential pressure over the condenser (dP)

The purpose of this section is to evaluate effect of different temperatures on the heat pipe to the output temperature of the thermal oil. Figure 4 shows the dependence of temperatures on the length of the condenser.

### Table 1

| Name                  | Type              | Mass flow (kg.s⁻¹) | Temperature (°C) | Turbulence (%) |
|-----------------------|-------------------|--------------------|------------------|----------------|
| IN                    | Mass-flow-inlet   | 0.01 - 0.04        | 80               | 10             |
| OUT                   | Pressure-outlet   |                    | -                | 10             |
| Surface of the heat pipe | Wall             |                    | 100 - 300        |                |

### Table 2

| Parameter | T - Heat Pipe | Tout | Q | dP |
|-----------|---------------|------|---|----|
| Units     | °C | °C | W | Pa |
| 1         | 100 | 97 | 386 | 6718 |
| 2         | 150 | 140 | 1371 | 4972 |
| 3         | 200 | 182 | 2455 | 4043 |
| 4         | 250 | 224 | 3633 | 3282 |
| 5         | 300 | 266 | 4920 | 2658 |

Discussion

The purpose of this section is to evaluate effect of different temperatures on the heat pipe to the output temperature of the thermal oil. Figure 4 shows the dependence of temperatures on the length of the condenser.
Figure 5 compares the predicted effect of temperature on the heat pipe to the output temperature at the condenser.

Results of case No. 3:
- Numerical simulations for mass flow of thermal oil 0.03 kg.s⁻¹.
- Temperature on the heat pipe was set as follows: 100°C - 150°C - 200°C - 250°C - 300°C.

Table 4 presents results of numerical simulations for the condenser.

This section presents distribution of temperature on the length of the condenser with flow 0.03 kg.s⁻¹ of thermal oil.

Figure 5

Results of case No. 2:
- Numerical simulations for mass flow of thermal oil 0.02 kg.s⁻¹.
- Temperature on the heat pipe was set as follows: 100°C - 150°C - 200°C - 250°C - 300°C.

Table 3 presents results of numerical simulations for the condenser.

This section presents distribution of temperature on the length of the condenser with flow 0.02 kg.s⁻¹ of thermal oil.

Figure 4

Table 4

| Mass flow | Tin |
|-----------|-----|
| 0.03 kg.s⁻¹ | 80 °C |

| Parameter | T - Heat Pipe | Tout | Q | dP |
|-----------|---------------|------|---|----|
| Units     | °C | °C | W | Pa |
| 1 | 100 | 93 | 591 | 17189 |
| 2 | 150 | 127 | 2134 | 14061 |
| 3 | 200 | 161 | 3797 | 11820 |
| 4 | 250 | 194 | 5609 | 9893 |
| 5 | 300 | 229 | 7526 | 8492 |

Results of case No. 4:
- Numerical simulations for mass flow of thermal oil 0.04 kg.s⁻¹.
- Temperature on the heat pipe was set as follows: 100°C - 150°C - 200°C - 250°C - 300°C.

Table 5 presents results of numerical simulations for the condenser.

This section presents distribution of temperature on the length of the condenser with flow 0.04 kg.s⁻¹ of thermal oil.

Figure 6

The purple curve (temperature on the heat pipe - 300°C) presents the maximum difference between temperature at the inlet and outlet (Fig. 6).

Results of case No. 4:
- Numerical simulations for mass flow of thermal oil 0.04 kg.s⁻¹.
- Temperature on the heat pipe was set as follows: 100°C - 150°C - 200°C - 250°C - 300°C.

Table 5 presents results of numerical simulations for the condenser.
Calculated data were compared and following conclusions were reached. The highest thermal power of condenser was observed in case No. 4 (mass flow 0.04 kg.s\(^{-1}\) and temperature on the heat pipe 300°C). The lowest differential pressure over the condenser was noticed in case No. 1 (mass flow 0.01 kg.s\(^{-1}\) and temperature on the heat pipe 300°C).

In the case of differential pressure the pressure drop is observed with the increase of temperature. When the flow of thermal oil increases, the condenser reaches higher heat performance. This effect can be very well observed when the temperature on the heat pipe is 300\(^\circ\)C. At a flow rate 0.01 kg.s\(^{-1}\) only half of heat power is achieved in comparison with the flow 0.04 kg.s\(^{-1}\).

Acknowledgements

This work is supported by the financial assistance of the company Goodtech Recovery Technology AS.

This article is supported by the financial assistance of the project VEGA No. 1/1353/12.

The research is supported by European regional development fund and Slovak state budget by the project Research centre of University of Zilina, ITMS 26220220183.
References

[1] JEBRAIL, F. F., ANDREWS, M. J.: Energy Research, 21, 101-112, (1998).
[2] HOLUBCIK, M., HUZVAR, J., JANDACKA J.: Combined Production of Heat and Electricity with Use of Micro Cogeneration, IN-TECH 2011 - proc. of intern. conference on innovative technologies, Bratislava, Slovakia. - [S.l.]: Jan Kudlacek, 2011. ISBN 978-80-904502-6-4. - S. 200-202.
[3] HUZVAR, J., KAPJOR, A.: Micro-cogeneration Incl. the Conversion of Chemical Energy of Biomass to Electric Energy and the Low Potential Heat, vol. 1337, 2011, 40-42, 4th Global Conference on Power Control and Optimization, Sarawak.
[4] LENHARD, R., MALCHO, M.: Numerical Simulation Device for the Transport of Geothermal Heat with Forced Circulation of Media. Mathematical and Computer Modelling, vol. 57, No. 1-2, 111-125, 2013, ISSN 0895-7177.
[5] NEMEC P., CAJA A., MALCHO M.: Mathematical Model for Heat Transfer Limitations of Heat Pipe. Mathematical and Computer Modelling, vol. 57, 1-2, 2013, 126-136.
[6] PILAT, P., PATSCH, M., MALCHO, M: Solar Heat Utilization for Adsorption Cooling Device, vol. 25, Article No. 01074, Conference on Experimental Fluid Mechanics, EFM 2011, Jicin, 2012.
[7] SCHMALHOFER, J., FAGHRI, A.: Heat Mass Transfer, 36, 201-212, 1993.