Unique extension of the maximum entropy principle to phase coexistence in heat conduction

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The maximum entropy principle determines the values of thermodynamic variables in thermally isolated equilibrium systems. This paper extends the principle to a variational principle that applies to liquid–gas coexistence in heat conduction. We show the uniqueness of the extension under the assumption that the variational principle and the fundamental thermodynamic relation are simultaneously extended in the linear response regime with the total energy fixed. Using the extended variational principle, we calculate the thermodynamic quantities in this steady state and find that the temperature of the liquid–gas interface deviates from the equilibrium transition temperature, which should be verified in experiments.

I. INTRODUCTION

The values of extensive unconstrained variables in thermally isolated equilibrium systems maximize the total entropy. This variational principle is called the maximum entropy principle and plays a fundamental role in equilibrium thermodynamics [1]. The principle leads to the definition of temperature and provides the equation of state. Additionally, the fluctuation law of thermodynamic variables is naturally conjectured from the variational principle and turns out to be consistent with the principle of equal weight in statistical mechanics [2]. The main question addressed in this paper is whether the maximum entropy principle extends to out-of-equilibrium systems.

The first approach to answering the above question relies on nonequilibrium statistical mechanics. In the last two decades, several universal properties of systems out of equilibrium have been understood with the aid of the fluctuation theorem and its several variants [3–12]. In particular, the difference in the stationary distribution from nonequilibrium to equilibrium has been studied when the Shannon entropy has been assumed to be the unique extension of the maximum entropy principle to phase coexistence in heat conduction. We show the uniqueness of the extension under the assumption that the variational principle and the fundamental thermodynamic relation are simultaneously extended in the linear response regime with the total energy fixed. Using the extended variational principle, we calculate the thermodynamic quantities in this steady state and find that the temperature of the liquid–gas interface deviates from the equilibrium transition temperature, which should be verified in experiments.

The important thing here is that the extended maximi-
num entropy principle should provide a novel prediction of quantitative phenomena that can be observed in experiments. From this viewpoint, the liquid–gas phase coexistence in heat conduction has turned out to be a good target even in the linear response regime. Our previous papers predicted that the interface temperature deviates from the equilibrium transition temperature [30, 31]. Numerical simulations have quantitatively confirmed this prediction [32]. Such phase coexistence may become studied by extending the maximum entropy principle to the linear response regime in energy-conserving heat-conduction systems.

Here, we briefly review the maximum entropy principle for the liquid–gas coexistence at equilibrium. At constant pressure, the thermodynamic entropy $S$ is a function of the energy and the number of particles of the whole system, whereas the variational function $\mathcal{S}$ is a function of those of the liquid with the total energy and the total number of particles of the system fixed. The two entropies are functionally different and connected by the maximum entropy principle; i.e., the value of $S$ is equal to the maximum value of $\mathcal{S}$. The maximization determines the unique equilibrium state. The equilibrium entropy possesses a remarkable property that the two entropies, $S$ and $\mathcal{S}$, are similarly expressed as the sum of the entropy of the liquid and the entropy of the gas.

We proceed to the heat conduction state in the linear response regime. The respective entropies of the liquid and the gas are given by the integration of the local entropy density in the respective regions. One may then guess that the variational function $\mathcal{S}$ is obtained by summing these entropies similarly to the equilibrium cases. However, there is no reason to assume the additivity of entropy for out-of-equilibrium systems. Instead of assuming the additivity, we impose that the value of the variational function in the steady state satisfies the thermodynamic relation with the global temperature introduced in Refs. [30].

From this fundamental assumption and other assumptions of the extensive/intensive nature of variables, we can uniquely determine the form of the variational function. The remarkable result obtained in this paper is that the variational function has a non-additive contribution even in the linear response regime. This term is specific to phase coexistence because it is proportional to the latent heat. Furthermore, we show that the steady state determined within this framework is identical to that determined by the free energy minimum principle with the global temperature fixed [30]. As a consequence, the interface temperature deviates from the equilibrium transition temperature.

The remainder of the paper is organized as follows. Section II reviews the maximum entropy principle for determining the thermodynamic state of coexisting liquid and gas phases with the total enthalpy, pressure and total particle number fixed. Section III describes the setup for the heat conduction states that we study. Section IV addresses the problem that we want to solve; i.e., we seek a form of the variational function as an extension of the maximum entropy principle. Section V presents the form of the variational function, which gives the unique answer to the problem. Section VI argues the thermodynamic equivalence of steady states in heat conduction. Section VII provides a quantitative result for the steady state. The final section is devoted to concluding remarks. Derivations of the results and formulas are separately presented in the appendices. In this paper, we define the temperature using the energy unit $k_B = 1$ for simplicity.

II. BRIEF REVIEW ON THE ROLE OF ENTROPY IN EQUILIBRIUM

Let us start with a familiar liquid–gas transition observed in a fluid at constant pressure $p$ in contact with a heat bath of temperature $T$. The density of the fluid exhibits a discontinuous jumps at $T = T_c(p)$. The fluid behaves as a liquid at $T < T_c(p)$ and as gas at $T > T_c(p)$. Letting the equation of state for the liquid and gas be $\rho = \rho^L(T, p)$ and $\rho = \rho^G(T, p)$, respectively, we obtain the particle number density at the liquid–gas transition as $\rho^L(p) = \lim_{T \to T_c(p)} \rho^L(T, p)$ and $\rho^G(p) = \lim_{T \to T_c(p)} \rho^G(T, p)$. See Fig. 2(a). The latent heat generated in a transition to gas from liquid is equivalent to the jump in enthalpy $H$, where $H = U + pV$ with the internal energy $U$ and the volume $V$ of the system. As shown in Fig. 2(b), letting $\hat{h}^L(T, p)$ and $\hat{h}^G(T, p)$ be the enthalpy per particle for liquid and gas, the latent heat per particle is

$$q(p) = \hat{h}^G(p) - \hat{h}^L(p),$$

(II.1)
where \( \hat{h}_L^{c}(p) = \lim_{T \to T_c(p)} \hat{h}_L(T,p) \) and \( \hat{h}_G^{c}(p) = \lim_{T \to T_c(p)} \hat{h}_G(T,p) \).

For a thermally isolated fluid from the environment of constant pressure, enthalpy \( H \) is the conserved energy, which corresponds to the sum of the energy of the system and the interaction potential between the system and the environment. Figure 3 shows the equilibrium temperature of the system as a function of \( \hat{h} = H/N \) with \( p \) fixed. This figure is equivalent to Fig. 2(b) except for the swapping of the vertical and horizontal axes. The system exhibits stable liquid–gas coexistence for a certain range of enthalpy, say \( \hat{h}_L^{c}(p) < \hat{h} < \hat{h}_G^{c}(p) \), while it is occupied by liquid for \( \hat{h} < \hat{h}_L^{c}(p) \) or by gas for \( \hat{h} > \hat{h}_G^{c}(p) \). Choosing \( \hat{h} \) as a certain value in the range of coexistence, the distribution of \( H \) and \( N \) to the liquid and the gas are uniquely determined as \( H^L \) with \( H^G = H - H^L \) and \( N^L \) with \( N^G = N - N^L \).

A remarkable point in equilibrium thermodynamics is the correspondence of the thermodynamic entropy \( S \) with the entropy as the variational function \( \mathcal{J} \) in their functional forms. Suppose that \( H^L \) and \( N^L \) are the variational variables corresponding to the distribution of the enthalpy and the number of particles to liquid, which should be uniquely determined in equilibrium as \( H^L \) and \( N^L \). The entropy function as the variational function is given by

\[
\mathcal{J}(H^L, N^L; H, p, N) = S(H^L, p, N^L) + S(H^G, p, N^G)
\]

with \( H^G = H - H^L \) and \( N^G = N - N^L \). Meanwhile, the thermodynamic entropy \( S \) of the total system satisfies

\[
S(H, p, N) = S(H^L, p, N^L) + S(H^G, p, N^G),
\]

where \( H^G = H - H^L \) and \( N^G = N - N^L \). The functional form of the right-hand side of (II.3) is the same as that of (II.2). However, we note the difference in variables between \( \mathcal{J} \) and \( S \); i.e., \( \mathcal{J} \) is a five-variable function whereas \( S \) is a three-variable function. The two functions appear in different contexts.

In equilibrium thermodynamics, thermodynamic entropy \( S \) is related to the variational function \( \mathcal{J} \) as follows. Equilibrium states maximize the entropy (variational function) \( \mathcal{J} \) according to the second law of thermodynamics, and the equilibrium states are expressed as

\[
(H^L, N^L) = \arg \max_{H^L, N^L} \mathcal{J}(H^L, N^L; H, p, N).
\]

Thus, \( H^L \) and \( N^L \) are the solutions to the simultaneous equations for \( H^L \) and \( N^L \),

\[
\left( \frac{\partial \mathcal{J}}{\partial H^L} \right)_{N^L, H, p, N} = 0, \quad (\text{II.5})
\]

\[
\left( \frac{\partial \mathcal{J}}{\partial N^L} \right)_{H^L, H, p, N} = 0, \quad (\text{II.6})
\]

from which we identify the equilibrium state as

\[
H^L = H^L(H, p, N), \quad N^L = N^L(H, p, N).
\]

Substituting this solution into (II.2), we obtain

\[
\mathcal{J}(H^L(H, p, N), N^L(H, p, N); H, p, N) = S(H, p, N),
\]

which means that the maximum value of the variational function \( \mathcal{J} \) is equal to the thermodynamic entropy \( S \).
We also have
\[ S(H, p, N) = S(H^L(H, p, N), p, N^L(H, p, N)) \]
\[ + S(H^G(H, p, N), p, N^G(H, p, N)) \] (II.9)
as the exact expression of (II.3). The relation of \( S \) with \( S \) is presented in Fig. 4.

The temperatures of the liquid and gas are defined as
\[ \frac{1}{T^L} = \left( \frac{\partial S}{\partial H^L} \right)_{p, N^L}, \quad \frac{1}{T^G} = \left( \frac{\partial S}{\partial H^G} \right)_{p, N^G}. \] (II.10)
Substituting (II.2) with \( \mathcal{H}^G = H - H^L \) into the variational equation (II.5), we have
\[ T^L = T^G, \] (II.11)
which is the balance of temperature between the liquid and gas in equilibrium. Similarly, because the chemical potentials are given by
\[ \frac{\mu^L}{T^L} = -\left( \frac{\partial S}{\partial N^L} \right)_{p, H^L}, \quad \frac{\mu^G}{T^G} = -\left( \frac{\partial S}{\partial N^G} \right)_{p, H^G}, \] (II.12)
the variational equation (II.6) together with \( T^L = T^G \) and \( N^G = N - N^L \) yields
\[ \mu^L = \mu^G, \] (II.13)
which corresponds to the balance of the chemical potential between the liquid and gas. With these two balances, we obtain the fundamental relation of thermodynamics for the total system as
\[ dS = \frac{1}{T} dH - \frac{V}{T} dp - \frac{\mu}{T} dN, \] (II.14)
in which we write \( T = T^L = T^G \) and \( \mu = \mu^L = \mu^G, \)
\[ V = V^L + V^G \] is the total volume of the system.

As we have reviewed so far, the correspondence of the two entropy functions, \( S \) and \( S \), is concluded from the second law of thermodynamics, and the correspondence is a strong property of the equilibrium entropy describing macroscopic phenomena.

### III. SETUP

We focus on enthalpy-conserving systems at constant pressure in heat conduction. See Fig. 1. \( N \) particles are enclosed in a container made of thermally insulating material except for the left and right boundaries. The top plate of the container at the position \( L_z \) is set freely movable to keep the pressure constant, whereas the other five walls are fixed with constant lengths \( L_x \) and \( L_y \). The volume of the system \( V = L_x L_y L_z \) is not fixed whereas the total enthalpy \( H \) of the system is kept constant. We assume that the transition temperature \( T_c(p) \) is far below the critical temperature. For simplicity, gravity effects are ignored such that the pressure is uniform over the system.

To conserve enthalpy, we control the in- and out-flow heat currents from the left and right boundaries to be strictly \( JL_y L_z \) per unit time. For \( J < 0 \), the liquid localizes on the left side of the system, and there is an interface that separates the liquid from the gas. Such violation of left–right symmetry continues to \( J \to 0^- \). The steady state for \( J > 0 \) is obtained by the space-inversion of the system with \( -J \) as shown in Fig. 5. When \( J \) is continuously changed from negative to positive values, local thermodynamic quantities may jump from those of liquid to gas or vice versa at \( J = 0 \). This indicates the singularity at \( J = 0 \).

For fixed values of \( H, p, N, \) and \( J \), the enthalpy and particle distributions are determined uniquely. We assume that \( |J| \) is so small that each local thermodynamic quantity is uniform in the section perpendicular to \( x \), and we therefore write the local quantity as a function of \( x \). This means that the heat conduction system remains extensive in \( y \) and \( z \) directions even for \( J \neq 0 \) because the value of \( L_y \) or \( L_z \) does not affect any local state. Using local temperature \( T(x) \), we write the temperatures at the two ends as
\[ T_1 = \lim_{x \to 0^+} T(x), \quad T_2 = \lim_{x \to L_x} T(x). \] (III.1)

We observe liquid–gas coexistence when \( T_1 < T_c(p) < T_2 \) for \( J < 0 \), or \( T_1 > T_c(p) > T_2 \) for \( J > 0 \). As a dimensionless parameter representing the degree of nonequilibrium, we set
\[ \varepsilon = \frac{T_2 - T_1}{T_c(p)}. \] (III.2)

Suppose that the liquid–gas interface is situated at \( x = X \), where the thickness of the interface is not macroscopic and is ignored in the present description. We express the enthalpy and the particle number of the phase in the left
(right) region of $x < X$ ($x > X$) as

$$H^t = L_y L_z \int_0^X dx \ h(x), \quad H^r = L_y L_z \int_X^L_x dx \ h(x),$$

(III.3)

$$N^t = L_y L_z \int_0^X dx \ \rho(x), \quad N^r = L_y L_z \int_X^L_x dx \ \rho(x),$$

(III.4)

where $h(x)$ and $\rho(x)$ denote local enthalpy density and number density. The total enthalpy and total number of particles in the system are

$$H = H^t + H^r, \quad N = N^t + N^r.$$  

(III.5)

Conventionally, one may interpret $\ell = L$ and $r = G$ for $J < 0$ and vice versa for $J > 0$. The variational variables $\hat{H}^{L/G}$ and $N^{L/G}$ in Sec. II are replaced with $\hat{H}^{L/G}$ and $N^{L/G}$.

When we know the values of $T(x)$ and $p$ and the local phase as liquid or gas, we can identify any local thermodynamic quantity from equilibrium thermodynamics regardless of whether the local state is stable or metastable. For instance, when the local phase is liquid, local entropy density is written as $s(x) = \rho^L(T(x), p) \hat{s}^L(T(x), p)$ with equilibrium entropy $\hat{s}(T, p)$ per particle. The entropies for the left (right) region are expressed as the spatial integration of the local density; i.e.,

$$S^t = L_y L_z \int_0^X dx \ s(x), \quad S^r = L_y L_z \int_X^L_x dx \ s(x).$$

(III.6)

These entropies are defined in heat conduction; however they are written by the equilibrium entropy functions,

$$S^t = S(H^t, p, N^t), \quad S^r = S(H^r, p, N^r)$$

(III.7)

with an error of $O(\varepsilon^2)$, as shown in Sec.3 of [31]. See Appendix A 1.

In the last of this section, we mention the treatment of the singularity at $J = 0$ associated with the left–right symmetry demonstrated in Fig. 5. When $J$ is varied continuously from negative to positive values, thermodynamic quantities for the left region become discontinuous at $J = 0$. We assume that this discontinuity can be expressed as the limit of smooth functions of $\varepsilon$ by introducing some regularization parameters. We set the regularization parameters to be zero in the last step of the calculation of the thermodynamic quantities. Here, we choose the regularization parameters in such a way that the global thermodynamics is formulated consistently.

IV. PROBLEM

Our aim in this paper is to extend the maximum entropy principle to heat conduction states. We introduce a nonequilibrium intensive variable $\phi$ and its conjugate extensive variable $\Psi$ with the condition

$$\phi = O(\varepsilon), \quad \Psi = O(\varepsilon^0).$$

(IV.1)

We then seek extended forms of the entropy $S$ and variational function $\mathcal{S}$ that satisfy three conditions.

The first condition is that $S$ and $\mathcal{S}$ take the same form

$$S(H, p, N, \phi) = S(H^t, p, N^t) + \phi \Psi(H, p, N, \phi),$$

(IV.2)

$$\mathcal{S}(H^t, N^t; H, p, N, \phi) = S(H^t, p, N^t) + \phi \psi(H^t, N^t; H, p, N),$$

(IV.3)

where the function $\psi$ does not depend on $\phi$ explicitly.

The second condition for $S$ and $\mathcal{S}$ is that the thermodynamic entropy $S$ corresponds to the maximum value of the variational function $\mathcal{S}$; i.e.,

$$S(H, p, N, \phi) = \mathcal{S}(H^t, N^t; H, p, N, \phi),$$

(IV.4)

with the steady state values

$$H^t = H^t(H, p, N, \phi), \quad N^t = N^t(H, p, N, \phi).$$

(IV.5)

We assume that the steady state maximizes $\mathcal{S}$. Then, $H^t$ and $N^t$ are determined as

$$(H^t, N^t) = \arg \max_{H^t, N^t} \mathcal{S}(H^t, N^t; H, p, N, \phi).$$

(IV.6)

The third condition for $S$ and $\mathcal{S}$ is that $S(H, p, N, \phi)$ satisfies the fundamental relation of thermodynamics

$$dS = \frac{1}{T} dH - \frac{V}{T} dp - \frac{\hat{\mu}}{T} dN + \Psi d\phi,$$

(IV.7)

where $\hat{T}$ is the global temperature defined by

$$\hat{T} = \frac{\int_0^{L_x} dx \ \rho(x) T(x)}{\int_0^{L_x} dx \ \rho(x)},$$

(IV.8)

which was introduced in [30]. We also define the global chemical potential as

$$\hat{\mu} = \frac{\int_0^{L_x} dx \ \rho(x) \mu(x)}{\int_0^{L_x} dx \ \rho(x)},$$

(IV.9)

where $\mu(x)$ is the local chemical potential. We emphasize that, once we decide to adopt $\hat{T}$ as a temperature to characterize the heat conduction states, $\hat{\mu}$ is concluded to be a unique extension of the equilibrium chemical potential. See Sec. 7 of [31].
Summarizing the above, we attempt to determine an entropy extended to liquid–gas coexistence in heat conduction using simultaneous equations, specifically two equations from the variational principle (IV.7),

\[
\left( \frac{\partial \mathcal{F}}{\partial H^\ell} \right)_{N^\ell, H^\ell, p, N, \phi, H^\ell = H^\ell} = 0, \quad (IV.11)
\]

\[
\left( \frac{\partial \mathcal{F}}{\partial N^\ell} \right)_{H^\ell, H^\ell, p, N, \phi, N^\ell = N^\ell} = 0, \quad (IV.12)
\]

and four equations from the fundamental relation (IV.8),

\[
\left( \frac{\partial S}{\partial H} \right)_{p, N, \phi} = \frac{1}{T}, \quad (IV.13)
\]

\[
\left( \frac{\partial S}{\partial p} \right)_{H, N, \phi} = -\frac{V}{T}, \quad (IV.14)
\]

\[
\left( \frac{\partial S}{\partial N} \right)_{H, p, \phi} = -\frac{\tilde{\mu}}{T}, \quad (IV.15)
\]

\[
\left( \frac{\partial S}{\partial \phi} \right)_{H, p, N} = \Psi, \quad (IV.16)
\]

V. RESULTS

Solving the equations (IV.11), (IV.12), (IV.13), (IV.14), (IV.15), and (IV.16) under the conditions described in Sec. III, we determine the functional form of \( \phi \) and \( \psi \) as

\[
\phi = \varepsilon \quad (V.1)
\]

and

\[
\psi(H^\ell, N^\ell; H, p, N) = \frac{H^\ell N^\ell - H^\ell N^r}{2NT_c(p)} \quad (V.2)
\]

up to a multiplicative constant. This multiplicative constant does not affect any quantitative prediction and we thus set it as a specific value as discussed in Appendix B4.

The steady-state value of \( \psi \) is expressed as

\[
\Psi(H, p, N, \phi) = \frac{\phi}{\varepsilon} \frac{\tilde{\mu}(p)}{2T_c(p)} \frac{N^L N^G}{N} \quad (V.3)
\]

using (V.5) and (V.2), where \( N^L/G \) is the steady number of particles in the liquid and gas and we have used the relation for the steady state value of enthalpy as \( H^L/G = h^L/G(p)N^L/G + O(\varepsilon) \). The expression (V.3) clarifies that the new quantity \( \Psi \) is associated with the phase coexistence because it is connected to the latent heat \( \tilde{\mu}(p) \). Meanwhile, \( \phi \) is a nonequilibrium variable that is never associated with equilibrium properties. Moreover, we emphasize that \( \phi \) is uniquely determined by (V.1) as the difference in temperature at the two boundaries and not as the steady heat current \( J \) although \( J \) is an operational parameter that controls the enthalpy conservation in heat conduction.

Using the variational function (IV.3) with (V.1) and (V.2), the variational equations (IV.11) and (IV.12) are expressed as

\[
\frac{1}{T^\ell} - \frac{1}{T^r} = \frac{\phi}{2T_c(p)}, \quad (V.4)
\]

\[
\frac{\tilde{\mu}^\ell - \tilde{\mu}^r}{T^\ell - T^r} = \frac{\phi H}{2T_c(p) N}. \quad (V.5)
\]

Here, \((\ell, r) = (L, G)\) for \( \varepsilon > 0 \) and \((\ell, r) = (G, L)\) for \( \varepsilon < 0 \), where \( T^L \) and \( T^G \) are global temperatures for the liquid and gas, respectively, and \( \tilde{\mu}^L \) and \( \tilde{\mu}^G \) are the respective global chemical potentials. (V.4) and (V.5) at \( \varepsilon = 0 \) correspond to the equilibrium balances of temperature and chemical potential between the liquid and gas. Thus, these relations at \( \varepsilon \neq 0 \) provide the first-order correction of the balances. Indeed, (V.4) is transformed as

\[
\tilde{T}^r - \tilde{T}^\ell = \frac{\phi}{2} T_c(p) + O(\varepsilon^2), \quad (V.6)
\]

which leads to (III.2) with \( \phi = \varepsilon \) as derived from (A.18).

We emphasize that (V.4) and (V.5) are sufficient to identify steady states. As we will demonstrate in Sec. VII, (V.4) and (V.5) lead to all thermodynamic quantities for the liquid–gas coexistence in heat conduction. For instance, (VII.2) and (VII.14) provide experimentally accessible relations for the steady states, which may act as the check of the validity of the present theory. We will also see that \( \theta \) is not necessarily equal to \( T_c(p) \) because metastable states, such as super-cooled gas or super-heated liquid, may be stably observed in heat conduction. Moreover, the steady states are consistent with those determined by the variational principle for heat conduction systems attached to two heat baths of \( T_1 \) and \( T_2 \) [31]. See Sec. VI for the correspondence between the enthalpy-conserving and nonconserving systems.

VI. THERMODYNAMIC EQUIVALENCE OF STEADY STATES IN HEAT CONDUCTION

The thermodynamic relations of equilibrium systems are independent of whether the system is adiabatic or isothermal and whether the system is at constant pressure or constant volume. Remarkably, the equivalence between the fundamental thermodynamic relations can be formulated using the Legendre transformation. We then ask whether there exist similar relations among different formulations for heat conduction systems. See Table I. Specifically, we study the three cases presented in Fig. 6. So far, we have studied enthalpy conserving systems at constant pressure in heat conduction, which is shown in the top panel. In the second panel, we attach a heat bath of \( T_1 \) at the left wall and a heat bath of \( T_2 \) at
the right wall, where \( T_1 \leq T_2 \) is assumed without loss of generality. Below, we assume that there are no temperature gaps between the system and the heat baths (i.e., \( T(0^+) = T_1 \) and \( T(L^x_z) = T_2 \)) in steady states. In the bottom panel of Fig. 6, the system is kept at constant volume instead of at constant pressure. While the fundamental thermodynamic relations and the variational principles for the systems of constant pressure or constant volume were investigated in [31], we reformulate them from the results in the previous section.

**A. Thermodynamic relations**

We define the Gibbs free energy in heat conduction as

\[
G = L_y L_z \int_0^{L_x} dx \mu(x) \rho(x). \tag{VI.1}
\]

The entropy \( S \) given in (IV.2) with \( \phi = \varepsilon \) and \( \Psi \) as (V.3) satisfies

\[
S = \frac{H - G}{T} + O(\varepsilon^2) \tag{VI.2}
\]

with the global temperature \( \tilde{T} \) in (IV.9). See Appendix C for the derivation of (VI.2). Substituting (VI.2) into (IV.8), we obtain

\[
dG = -S d\tilde{T} + V d\mu + \tilde{\mu} dN - \tilde{T} \Psi d\phi. \tag{VI.3}
\]

From this relation, we find that the functional form

\[
G = G(\tilde{T}, p, N, \phi) \tag{VI.4}
\]

is useful. Because the global Helmholtz free energy

\[
F = L_y L_z \int_0^{L_x} dx f(x) \tag{VI.5}
\]

satisfies

\[
F = G - pV, \tag{VI.6}
\]

(VI.3) is transformed into the fundamental relation

\[
dF = -S d\tilde{T} - pdV + \tilde{\mu} dN - \tilde{T} \Psi d\phi, \tag{VI.7}
\]

which leads to the expression

\[
F = F(\tilde{T}, V, N, \phi). \tag{VI.8}
\]

Thus, the fundamental relations of global thermodynamics are formed consistently among \((H, p, N, \phi), (\tilde{T}, p, N, \phi), \) and \((\tilde{T}, V, N, \phi)\). The transformation into \((U, V, N, \phi)\) is also straightforward. These transformations are nothing but the Legendre transitions. See Appendix E for further arguments on the additivity of \( G \) and \( F \).

We here present a remark. The fundamental relations of global thermodynamics derived in [31] were expressed in slightly different forms from (VI.3) and (VI.7); i.e.,

\[
dG = -(S^L + S^G) d\tilde{T} + V d\mu + \tilde{\mu} dN - \Psi d\Xi, \tag{VI.9}
\]

\[
dF = -(S^L + S^G) d\tilde{T} - pdV + \tilde{\mu} dN - \Psi d\Xi, \tag{VI.10}
\]

where \( \Xi = T_2 - T_1 \). (VI.9) and (VI.10) are obtained by substituting \( \phi = \Xi/\tilde{T} \) into (VI.3) and (VI.7). While the expression (VI.9) is equivalent to (VI.3), the former implies the extension of the Gibbs free energy in the form \( G = G(\tilde{T}, p, N, \Xi) \), in which the nonequilibrium variable is not \( \phi \) but \( \Xi \). As long as we discuss thermodynamic properties for the systems attached to heat baths, both the relations work consistently. However, the connection to the thermodynamic relation in enthalpy-conserving systems is more clearly seen in (VI.3).

**B. Variational principles**

We first explain the variational principle corresponding to the minimization of the Gibbs free energy \( G \). In equilibrium, this minimization is performed by fixing \((T, p, N)\). The extension of this variational principle to heat conduction is not straightforward because the temperature profile cannot be given as an external parameter of the setup. Nevertheless, referring to the thermodynamic relation (VI.3), we formally adopt the fixed condition as \((\tilde{T}, p, N, \phi)\). To fix \( \tilde{T} \) and \( \phi \) in the variation at constant \( p \), we shift the two temperatures by the
Thermodynamic relation

\[ d\mathcal{F} = L_y L_z \int_0^{L_z} s(x) \, dx + \phi \psi \]  

same amount while fixing \( T_2 - T_1 = \Xi \) and find heuristically the shift required to keep the right-hand side of (IV.9) as \( T \). Thus, fixing \( (\tilde{T}, p, N, \phi) \) is the same as fixing \( (T, p, N, \Xi) \), whose variational principle and the steady states given by it have already been investigated in [31].

In brief, taking a variational function as a natural extension from equilibrium,

\[ \mathcal{G} = L_y L_z \int_0^{L_z} \mu(x)\rho(x) \, dx, \quad (VI.11) \]

we obtain

\[ \mathcal{G}(\mathcal{N}_L; \tilde{T}, p, N, \phi) = G^L(\mathcal{T}^L(\mathcal{N}_L; \tilde{T}, N, \phi), p, N^L), \]

\[ + G^G(\mathcal{T}^G(\mathcal{N}_L; \tilde{T}, N, \phi), p, N - N^G), \quad (VI.12) \]

where \( G^L(\mathcal{T}^L, p, N^L) = \mu^L(\mathcal{T}^L, p)N^L \) and \( G^G(\mathcal{T}^G, p, N^G) = \mu^G(\mathcal{T}^G, p)(N - N^G) \). \( \mathcal{T}^L \) and \( \mathcal{T}^G \) are the global temperatures for the liquid and gas, which are considered as variational quantities because they depend on \( N^L \) according to

\[ \mathcal{T}^L = \tilde{T} \left( 1 - \frac{\phi N - N^L}{2N} \right), \quad \mathcal{T}^G = \tilde{T} \left( 1 + \frac{\phi^L N^L}{2N} \right). \]

\[ (VI.13) \]

(VI.13) results from the definition of \( \tilde{T} \) and \( \phi \) with \( \tilde{T} = T_1(p) + O(\varepsilon) \) assuming that local temperature is continuous everywhere, even at the liquid–gas interface. See the discussion around (A.19).

The steady state is specified by determining the distribution of particles to liquid as

\[ N^L = \arg\min_{\mathcal{N}_L} \mathcal{G}(\mathcal{N}_L; \tilde{T}, p, N, \phi), \quad (VI.14) \]

which is rewritten as

\[ \left( \frac{\partial \mathcal{G}}{\partial \mathcal{N}_L} \right)_{\tilde{T}, p, N, \phi} = 0. \quad (VI.15) \]

Using (VI.12) together with (VI.13), the variational equation (VI.15) leads to

\[ \mu^L - \mu^G = \phi \tilde{T} \left( \frac{S^L + S^G}{2N} \right). \quad (VI.16) \]

where we applied the fundamental relation of global thermodynamics, which is briefly reviewed in Appendix A1. We show the equivalence between (V.5) and (VI.16) in Appendix D.

We next deal with constant-volume systems in heat conduction. We assume that the steady state for a given \( (\tilde{T}, V, N, \phi) \) is obtained as the state minimizing the total Helmholtz free energy of the system,

\[ \mathcal{F} = L_y L_z \int_0^{L_z} f(x) \, dx. \quad (VI.17) \]

More precisely, we formulate the variational function as

\[ \mathcal{F}(V^L, N^L; \tilde{T}, V, N, \phi) = F(\mathcal{T}^L(V^L; \tilde{T}, N, \phi), V^L, N^L), \]

where \( \mathcal{T}^L \) and \( \mathcal{T}^G \) are functions given by (VI.13). The steady state is obtained as

\[ (V^L, N^L) = \arg\min_{V^L, N^L} \mathcal{F}(V^L, N^L; \tilde{T}, V, N, \phi). \quad (VI.19) \]

That is to say,

\[ \left( \frac{\partial \mathcal{F}}{\partial V^L} \right)_{\tilde{T}, V, N, \phi, N^L} = 0, \quad (VI.20) \]

\[ \left( \frac{\partial \mathcal{F}}{\partial N^L} \right)_{\tilde{T}, V, N, \phi, V^L} = 0. \quad (VI.21) \]

The first equation (VI.20) leads to

\[ p^L = p^G \quad (VI.22) \]

corresponding to the balance of pressure in the liquid and gas. The second equation (VI.21) yields (VI.16).

In summary, the minimization of free energy \( \mathcal{G} \) with \( (\tilde{T}, p, N, \phi) \) fixed and the minimization of \( \mathcal{F} \) with \( (\tilde{T}, V, N, \phi) \) fixed provide the same results as the maximization of entropy \( \mathcal{S} \) with \( (H, p, N, \phi) \) fixed; i.e., the steady states are equivalent among the three.

\[ \text{VII. STEADY STATES} \]

This section summarizes the thermodynamic quantities in the steady heat conduction state, which result
from the variational principle. The derivations of the formulas are presented in Appendix F.

In Sec. VII A, we refer to the expression of the temperature at the liquid–gas interface, which was derived in [31]. We demonstrate various quantities in the steady state of the enthalpy-conserving systems with \( J \neq 0 \) as slight changes from corresponding equilibrium quantities in Sec. VII B. Such perturbative treatment is difficult to apply to systems in contact with two heat baths at constant pressure because the equilibrium position of the liquid–gas interface is not unique at \( T_c(p) \), whereas the liquid and gas do not coexist at \( T \neq T_c(p) \). This indicates that we cannot formulate a naive perturbative expansion in heat conduction near equilibrium. The thermodynamic equivalence holds in steady states as discussed in Sec. VI, and we may therefore transform the formulas for the steady state in \( (H, p, N, \phi) \) into \( (\bar{T}, p, N, \phi) \). See Sec. VII C. Below, we omit the dependence of \( \rho \) for the equilibrium quantities at the transition temperature.

When we set \( J \) as a parameter, the nonequilibrium variable \( \phi = (T_2 - T_1)/T_c \) is determined as

\[
\phi = -\frac{J L_x}{T_c} \frac{1}{\kappa_c^L \kappa_c^G} \left( \rho_c^L \kappa_c^G (\hat{h} - \hat{h}_c^G) + \rho_c^G \kappa_c^L (\hat{h}_c^G - \hat{h}) \right) + O(\varepsilon^2),
\]

(VII.1)

where \( \kappa_c^L/G \) is heat conductivity. Note that (VII.1) holds regardless of the sign of \( J \) and \( \phi J \leq 0 \). In the estimates below, we use \( \phi \) as it means (VII.1).

A simple sketch of the steady state is presented in Fig. 7 for \( J < 0 \) in comparison with equilibrium liquid–gas coexistence at \( J \to 0^- \). There is a region occupied by super-cooled gas on the adjacent to the liquid–gas interface. When we take \( J > 0 \), the steady state is obtained as the mirror image of \( J < 0 \) as shown in Fig. 5, where the physical properties are equivalent to those for \( J < 0 \). Thus, all steady-state properties should be expressed by functions of \( |J| \) or \( |\phi| \).

A. Temperature at the liquid–gas interface

From the variational principle (V.4) and (V.5), the temperature \( \theta \) at the interface is formulated as

\[
\theta = T_c - \frac{X(L_x - X)}{2L_x} \left[ |J| \left( \frac{1}{\kappa_c^G} - \frac{1}{\kappa_c^L} \right) + |\phi| \frac{T_c \rho_c^L - \rho_c^G}{\bar{\rho}} \right],
\]

(VII.2)

in which \( \bar{\rho} = N/V \) and \( X \) is the width of the liquid region as reported in [31]. Another form of (VII.2) is

\[
\theta = T_c - \frac{X(L_x - X)}{2L_x} |J| \left( \frac{\rho_c^G}{\rho} \frac{1}{\kappa_c^G} - \frac{\rho_c^L}{\bar{\rho}} \frac{1}{\kappa_c^L} \right)
\]

(VII.3)

as shown in Appendix F 7. (VII.2) indicates that \( \theta \) becomes lower than \( T_c \) in the linear response regime. Moreover, the absolute values \( |J| \) and \( |\phi| \) in (VII.2) imply that the true equilibrium state with a vanishing current \( J = 0 \) is singular. It is noted that \( \theta \) may deviate from \( T_c \) in experiments, as has been quantitatively discussed for a specific material such as water [31].

B. Steady-state expressions as functions of \((H, p, N, \phi)\)

From the variational equations (V.4) and (V.5), we identify the width of the liquid \( X = X(H, p, N, \phi) \), the volume \( V = V(H, p, N, \phi) \), the number of particles \( N_L = N_L(H, p, N, \phi) \), and the enthalpy \( H_L = H_L(H, p, N, \phi) \). The following estimates have precision of \( O(\varepsilon) \) and error of \( O(\varepsilon^2) \). The detailed derivation for each estimate is presented in Appendix F.

In the equilibrium limit \( |J| \to 0 \), the interface corresponds to the Gibbs dividing surface. For a given \((H, p, N)\), we obtain the numbers of particles as

\[
\frac{N_L^L}{N} = \frac{\hat{h}_c^G - \hat{h}}{\hat{q}}, \quad \frac{N_G^G}{N} = \frac{\hat{h} - \hat{h}_c^L}{\hat{q}},
\]

(VII.4)

the respective volumes as

\[
V_L^L = \frac{N}{\rho_c^L} \frac{\hat{h}_c^G - \hat{h}}{\hat{q}}, \quad V_G^G = \frac{N}{\rho_c^G} \frac{\hat{h} - \hat{h}_c^L}{\hat{q}},
\]

(VII.5)

and the width of the liquid as

\[
\frac{X_{eq}}{L_x} = \frac{\rho_c^G (\hat{h}_c^G - \hat{h})}{\rho_c^L (\hat{h} - \hat{h}_c^L) + \rho_c^G (\hat{h}_c^G - \hat{h})}.
\]

(VII.6)
Imposing the heat current $J$, the distributions of conserved quantities to each bulk deviate as follows. Letting $c_p^{L/G}$ be the specific heat at constant pressure, the numbers of particles are

$$\frac{N^L - N_{eq}^L}{N} = -\phi \frac{T_c}{2\tilde{q}} \left[ \left( \frac{\tilde{h}_c^G - \tilde{h}}{\tilde{q}} \right)^2 \frac{\tilde{c}_p^L}{\tilde{q}} - \left( \frac{\tilde{h} - \tilde{h}_c^L}{\tilde{q}} \right)^2 \frac{\tilde{c}_p^G}{\tilde{q}} \right],$$

(VII.7)

$$\frac{N^G - N_{eq}^G}{N} = \phi \frac{T_c}{2\tilde{q}} \left[ \left( \frac{\tilde{h}_c^G - \tilde{h}}{\tilde{q}} \right)^2 \frac{\tilde{c}_p^L}{\tilde{q}} - \left( \frac{\tilde{h} - \tilde{h}_c^L}{\tilde{q}} \right)^2 \frac{\tilde{c}_p^G}{\tilde{q}} \right],$$

(VII.8)

the enthalpies per particle are

$$\tilde{h}_c^L - \hat{h}_c^L = -\phi \frac{T_c}{2\tilde{q}} \tilde{h}_c^G - \tilde{h} \tilde{c}_p^L,$$

(VII.9)

$$\tilde{h}_c^G - \hat{h}_c^G = \phi \frac{T_c}{2\tilde{q}} \tilde{h} - \tilde{h}_c^L \tilde{c}_p^G,$$

(VII.10)

and the volumes are

$$V^L - V_{eq}^L = -\phi \frac{T_c}{2\rho_c^L} \frac{N}{\tilde{q}} \left[ \left( \frac{\tilde{h}_c^G - \tilde{h}}{\tilde{q}} \right)^2 \alpha_c^L \frac{\tilde{c}_p^L}{\tilde{q}} - \left( \frac{\tilde{h} - \tilde{h}_c^L}{\tilde{q}} \right)^2 \alpha_c^G \frac{\tilde{c}_p^G}{\tilde{q}} \right],$$

(VII.11)

$$V^G - V_{eq}^G = \phi \frac{T_c}{2\rho_c^L} \frac{N}{\tilde{q}} \left[ \left( \frac{\tilde{h}_c^G - \tilde{h}}{\tilde{q}} \right)^2 \alpha_c^L \frac{\tilde{c}_p^L}{\tilde{q}} - \left( \frac{\tilde{h} - \tilde{h}_c^L}{\tilde{q}} \right)^2 \alpha_c^G \frac{\tilde{c}_p^G}{\tilde{q}} \right],$$

(VII.12)

where $\alpha_c^L$ and $\alpha_c^G$ are thermal expansion coefficients at constant pressure for saturated liquid and gas. The scaled width of the liquid region, $x \equiv X/L_x$, changes as

$$x - x_{eq} = -\phi \frac{T_c}{2\tilde{q}} x_{eq} (1 - x_{eq}) \left[ \frac{\tilde{h} - \tilde{h}_c^L}{\tilde{q}} \alpha_c^L + \frac{\tilde{h}_c^G - \tilde{h}}{\tilde{q}} \alpha_c^G \right] + \left( \frac{\tilde{h}_c^G - \tilde{h}_c^L}{\tilde{q}} \frac{\tilde{c}_p^L}{\tilde{q}} - \frac{\tilde{h} - \tilde{h}_c^L}{\tilde{q}} \frac{\tilde{c}_p^G}{\tilde{q}} \right).$$

(VII.13)

Using (VII.6), (VII.13) is reformulated as

$$x - x_{eq} = -\phi \frac{T_c}{2\tilde{q}} x_{eq} (1 - x_{eq}) \frac{\alpha_c^G \rho_c^G (1 - x_{eq}) + \alpha_c^L \rho_c^L x_{eq}}{\rho_c^L (1 - x_{eq})} + \frac{\tilde{c}_p^L}{\tilde{q}} \frac{\rho_c^L}{\rho_c^G} x_{eq} - \rho_c^L \frac{\tilde{c}_p^L}{\tilde{q}} \frac{\rho_c^L}{\rho_c^G} (1 - x_{eq})^2.$$  

(VII.14)

When the liquid and gas satisfy $\rho_c^L \gg \rho_c^G$ and $\alpha_c^L \ll 1$, which are usually satisfied when $T_c$ is much lower than the critical temperature, formula (VII.14) can be simplified as

$$x - x_{eq} \simeq -\phi \frac{T_c}{2\tilde{q}} \frac{\rho_c^L \tilde{c}_p^L}{\rho_c^G} \left( 1 - x_{eq} \right)^2,$$

(VII.15)

Because $\rho_c^L \gg \rho_c^G$, the interface may shift drastically with a violent increase in volume when imposing a slight heat current while maintaining the amount of enthalpy.

C. Steady-state expressions as functions of $(\tilde{T}, p, N, \phi)$

Owing to the thermodynamic equivalence, the above estimates can be translated to functions of $(\tilde{T}, p, N, \phi)$ once specifying the global temperature as $\tilde{T}(H, p, N, \phi)$ and its inverse function as $H(\tilde{T}, p, N, \phi)$. As derived in Appendix F, the global temperature for a given $(H, p, N, \phi)$ is written as

$$\tilde{T} = T_c + \phi \frac{T_c}{\tilde{q}} \left( \hat{h}_c^L + \hat{h}_c^G \right),$$

(VII.16)

which has two limiting cases of $\tilde{T} \to T_c (1 - |\phi|/2)$ for $\tilde{h} \to \hat{h}_c^L$ and $\tilde{T} \to T_c (1 + |\phi|/2)$ for $\tilde{h} \to \hat{h}_c^G$. The former limit indicates that $T_c (1 - |\phi|) < T(x) < T_c$, where the system is almost completely occupied by liquid with $x \to 1$. The latter limit indicates that $T_c < T(x) < T_c (1 + |\phi|)$ (i.e., $x \to 0$), where the system is occupied by gas.

Solving (VII.16), we obtain $\hat{h}$ as

$$\hat{h} = \frac{\hat{h}_c^L + \hat{h}_c^G}{2} + \phi \frac{\tilde{q}}{T_c} \hat{h}_c^L - \hat{h}_c^G + O(\varepsilon),$$

(VII.17)

which is a function of $(\tilde{T}, p, \phi)$. Note that the relation (VII.17) does not provide the value of $\hat{h}$ out of equilibrium owing to the error term of $O(\varepsilon)$. However, compared with the equilibrium liquid–gas coexistence at $T_c$ at which $\hat{h}$ can take an arbitrary value in $\hat{h}_c^L < \hat{h} < \hat{h}_c^G$, (VII.17) specifies a value of $\hat{h}$ uniquely in the equilibrium limit $|\phi| \to 0$ once we set $\tilde{T}$ as $\tilde{T} = T_c (1 + |\phi|/2)$ for $\tilde{h} \to \hat{h}_c^L$, $T_c (1 - |\phi|/2)$ as $\tilde{h} \to \hat{h}_c^G$. There, the system is almost occupied by liquid as $x_{eq} \to 1$, and the liquid–gas interface may jump with a sudden increase in the volume once a temperature difference between the two heat baths is imposed.
heat conduction state with a liquid–gas interface is not additive once super-cooled gas is stabilized by the heat current.

We are able to transform the non-additive expression (IV.2) into an additive form by considering an isentropic surface, $S(H, p, N, \phi) = S(H_{\phi}, p, N)$, which connects a nonequilibrium state $\langle H, p, N, \phi \rangle$ with an equilibrium state $\langle H_{\phi}, p, N \rangle$. Here, $H_{\phi} = H + T_{c}(p) \phi \Psi$ for $J \neq 0$. The equilibrium entropy is the sum of that for liquid and that for gas. We thus write

$$S(H, p, N, \phi) = S(H_{\phi}^{L}, p, N_{\phi}^{L}) + S(H_{\phi}^{G}, p, N_{\phi}^{G})$$  \hspace{1cm} (VIII.1)

with $H_{\phi}^{L} + H_{\phi}^{G} = H_{\phi}$ and $N_{\phi}^{L} + N_{\phi}^{G} = N$. $H_{\phi}$, $H_{\phi}^{L/G}$, and $N_{\phi}^{L/G}$ are determined in Appendix G. Although (VIII.1) may look additive, we note that $H_{\phi}^{L} + H_{\phi}^{G} \neq H$ for $J \neq 0$, and therefore, $S$ and $H$ cannot be simultaneously additive quantities no matter what transformation is performed. Non-additivity is essential for the coexistence of liquid and gas under heat conduction.

When the transition temperature $T_{c}(p)$ is close to the critical temperature, the metastable region may disappear. Equation (VII.2) suggests that the interface temperature $\theta$ does not deviate from $T_{c}(p)$ because both thermal conductivity and density become equal in liquid and gas. The extensive variable $\Psi$ vanishes because it is proportional to the latent heat $q$. Moreover, our initial assumption of the negligible thickness of the interface may not be valid at the critical point because fluctuations grow up and the width of the liquid–gas interface may become macroscopic.

We proposed in this paper a scheme with which we construct the variational function $\mathcal{S}$ using the correspondence with thermodynamic entropy $S$. For equilibrium systems, the variational function of thermodynamics is closely related to the probability density of unconstrained thermodynamic variables in fluctuation theory [1]. This idea may apply to systems out of equilibrium. We thus naturally conjecture that, in the setup we study, the probability density of the unconstrained thermodynamic variables is also expressed by the variational function $\mathcal{S}$. To confirm the validity of the conjecture, we will study the potential for the fluctuation of thermodynamic variables by analyzing mesoscopic stochastic systems.

Apart from the maximum entropy principle, there are several variational principles aimed at explaining nonequilibrium phenomena. In the linear response regime from equilibrium, the principle of minimum entropy production has been formulated [33]. The principle states that the stationary distribution minimizes the entropy production rate [34], which is well founded from the dynamical fluctuation theory based on statistical mechanics [35]. Moreover, as an attempt to apply the variational principle to various nonequilibrium phenomena, the principle of the maximum entropy production rate has also been studied [36]. However, these variational principles are not yet connected to the maximum entropy principle in thermodynamics. The extended maximum

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**FIG. 8.** Schematic explanation for the violation of additivity in heat conduction. If there is a region occupied by super-cooled gas, the local states are not kept in the separation of the system.

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**VIII. CONCLUDING REMARKS**

We derived a unique extension of the entropy function to heat conduction. The extension works as a variational function whose maximum gives the steady state and it maintains the fundamental thermodynamic relation by adopting the global temperature as the temperature of the whole system. The different fundamental thermodynamic relations are connected by the Legendre transformation. See Table I for the overall view of the thermodynamic structure of the global thermodynamics. The steady state is equivalent between the energy-conserving heat conduction system imposing a constant heat current and the standard heat conduction system in contact with three parts as shown in Fig. 8, where the same heat current is occupied by super-cooled gas, whose local temperature is $\theta < T(x) < T_{c}(p)$. Once the middle part is separated from the other parts, this super-cooled gas is no longer in a steady state, and some portion of the middle part may transition into liquid. In this way, we expect that the
entropy principle proposed in this paper describes phenomena in the linear response regime, and the connection with the principle of minimum entropy production should thus be studied in the future. Furthermore, the concept of using global quantities may be applied to a wide class of phenomena far from equilibrium. It may then be interesting to find an interface between our theory and variational principles far from equilibrium.

Last but not least, we remark that several important concepts of nonequilibrium thermodynamics have not yet been studied. For example, excess heat is the key concept for an extension of the Clausius formula [10, 23, 37–42]. The basic idea is that the heat in the time evolution is decomposed into a house-keeping part and an excess part, where the former is identified as the part necessary for maintaining the nonequilibrium steady state. However, there are several versions of the decomposition, and it has not been established which decomposition is most useful. We constructed an extended entropy for the phase coexistence in heat conduction, and we may therefore ask what is a measurable heat $Q$ defined by an extended Clausius equality $Q = T \Delta S$ with the entropy and the global temperature formulated in this paper. If such a quantity $Q$ is explored in the present framework, the isentropic surface defined by $S(H, p, N, \phi) = S(H_0, p, N)$ provides quasi-static adiabatic processes. Generalizing the argument, we may further consider general adiabatic processes in which the entropy never decreases. There, $-T_\epsilon(p)\Theta$, which corresponds to $H - H_\epsilon$, may be regarded as the minimum work that induces steady heat current. It is a challenging problem to operationally identify adiabatic conditions for heat conduction systems.

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Appendix A: Preliminaries

1. Global thermodynamics for liquid and gas in heat conduction

In this section, we briefly review global thermodynamics that holds in each region of liquid and gas. As derived in [31], liquid or gas in the linear response regime of heat conduction is thermodynamically equivalent to a corresponding equilibrium system. This is because the profile of any thermodynamic density is approximately linear and therefore all global thermodynamic quantities defined averaged over the whole system are identified by the trapezoidal rule applied to the integration.

Below, we assume $J < 0$ without loss of generality. Similarly to (IV.9), global temperatures of liquid and gas are defined by

$$\bar{T}^L = \frac{\int_0^X dx \, \rho(x)T(x)}{\int_0^X dx \, \rho(x)}, \quad \bar{T}^G = \frac{\int_X^L dx \, \rho(x)T(x)}{\int_X^L dx \, \rho(x)},$$

(A.1)

and corresponding inverse temperatures by

$$\bar{\beta}^L = \frac{\int_0^X dx \, \rho(x)\beta(x)}{\int_0^X dx \, \rho(x)}, \quad \bar{\beta}^G = \frac{\int_X^L dx \, \rho(x)\beta(x)}{\int_X^L dx \, \rho(x)},$$

(A.2)

where $\beta(x) = 1/T(x)$. We derive

$$\bar{\beta}^L = \frac{1}{T^L} + O(\varepsilon^2), \quad \bar{\beta}^G = \frac{1}{T^G} + O(\varepsilon^2),$$

(A.3)

which are the same as the relations at equilibrium. Then, defining

$$\alpha^L = -\bar{\beta}^L\mu^L(\bar{T}^L, p) + O(\varepsilon^2),$$

$$\alpha^G = -\bar{\beta}^G\mu^G(\bar{T}^G, p) + O(\varepsilon^2)$$

(A.4)

with equilibrium chemical potential $\mu^L(T, p)$ and $\mu^G(T, p)$ of liquid and gas, we have the fundamental relation of thermodynamics in each region as

$$dS^L = \bar{\beta}^L dH^L - \bar{\beta}^L V^L dp + \alpha^L dN^L,$$

$$dS^G = \bar{\beta}^G dH^G - \bar{\beta}^G V^G dp + \alpha^G dN^G,$$

(A.6)

where $S^L$ and $S^G$ are the spatial integration of entropy density in (III.6). These relations indicate

$$S^L = S(H^L, p, N^L), \quad S^G = S(H^G, p, N^G).$$

(A.8)

That is, $S^L$ and $S^G$ are expressed by the equilibrium entropy function $S(H, p, N)$. We emphasize that both liquid and gas are out of equilibrium with conducting heat.

2. Functions in liquid–gas coexistence

Let $H^L$ and $N^L$ be the variational variables describing the enthalpy and the particle number in the left region of $0 < x < X$. In the argument below, six variable function $A(H^L, N^L; H, p, N, \phi)$ and four variable function $A_\epsilon(H, p, N, \phi)$ appear. More precisely, for any six variable function $A(H^L, N^L; H, p, N, \phi)$, $A_\epsilon$ denotes the four variable function defined by

$$A_\epsilon(H, p, N, \phi) =$$

$$A(H^L(H, p, N, \phi), N^L(H, p, N, \phi); H, p, N, \phi),$$

(A.9)

where $H^L(H, p, N, \phi)$ and $N^L(H, p, N, \phi)$ are the steady-state values when $(H, p, N, \phi)$ are given. Here, we assume that $\phi$ is also determined uniquely for a given $J$. The relation (IV.4) is simply expressed by $S = \mathcal{S}_\epsilon$. Obviously, $H^L = H^L_\epsilon$ and $N^L = N^L_\epsilon$.

Although we do not specify the function type once they are defined, the function types are fixed throughout this section, which is not the standard convention in thermodynamics. Thus, for example, a partial derivative is simply expressed as

$$\frac{\partial A}{\partial H}.$$
Accordingly, the partial derivative at the steady state is defined. For instance, the partial derivative with respect to \( \mathcal{H}_t \) is written as

\[
\frac{\partial A}{\partial \mathcal{H}_t} = \left. \frac{\partial A}{\partial \mathcal{H}_t} \right|_{(\mathcal{H}_t, \mathcal{N}_t) = (\mathcal{H}_t^*, \mathcal{N}_t^*)} \quad (A.11)
\]

### 3. Basic quantities for the liquid–gas coexistence

Thermodynamic relations in each liquid or gas hold for given \( \mathcal{H}_t \) and \( \mathcal{N}_t \). Therefore, for the thermodynamic states, \( (\mathcal{H}_t^*, \mathcal{N}_t^*) \) and \( (\mathcal{H}_r^*, \mathcal{N}_r^*) \) with \( \mathcal{H}_t = \mathcal{H}_r^* \) and \( \mathcal{N}_t = \mathcal{N}_r^* \), \( \beta_t^* \) and \( \beta_r^* \) can be defined from the fundamental thermodynamic relations (A.6) and (A.7) as

\[
\beta_t^* = \left( \frac{\partial S_t^*}{\partial \mathcal{N}_t^*} \right)_{\mathcal{N}_t^*, p}, \quad \beta_r^* = \left( \frac{\partial S_r^*}{\partial \mathcal{N}_r^*} \right)_{\mathcal{N}_r^*, p} \quad (A.12)
\]

We then introduce the global inverse temperature \( \tilde{\beta} = \beta(\mathcal{H}_t^*, \mathcal{N}_t^*; H, p, N) \) in the liquid–gas coexistence as

\[
\tilde{\beta} = \frac{N_t^*}{N} \beta_t^* + \frac{N_r^*}{N} \beta_r^* \quad (A.13)
\]

which is consistent with

\[
\tilde{\beta} = \int_0^L dx \rho(x) \beta(x) / \int_0^L dx \rho(x) \quad (A.14)
\]

Developing a similar argument for \( \alpha = -\mu/T \), we have

\[
\alpha_t^* = \left( \frac{\partial S_t^*}{\partial \mathcal{N}_t^*} \right)_{\mathcal{H}_t^*, p}, \quad \alpha_r^* = \left( \frac{\partial S_r^*}{\partial \mathcal{N}_r^*} \right)_{\mathcal{N}_r^*, p} \quad (A.15)
\]

from which we define the global quantity in the liquid–gas coexistence \( \tilde{\alpha} = \tilde{\alpha}(\mathcal{H}_t^*, \mathcal{N}_t^*; H, p, N, \phi) \) as

\[
\tilde{\alpha} = \frac{N_t^*}{N} \alpha_t^* + \frac{N_r^*}{N} \alpha_r^* \quad (A.16)
\]

consistently with

\[
\tilde{\alpha} = \int_0^L dx \rho(x) \alpha(x) / \int_0^L dx \rho(x) \quad (A.17)
\]

In the steady state, we expect that the temperature profile \( T(x) \) is continuous in \( 0 < x < L_x \) including the liquid–gas interface. This is because there is no particle current to produce latent heat at the interface. Since the temperature profile satisfies \( T(x) = T_\epsilon(p) + O(\epsilon) \), we have \( \tilde{\beta}_* = \beta_*(p) + O(\epsilon) \). Let \( \theta \) be the temperature at the interface. The global temperatures of left and right regions are estimated as

\[
\tilde{T}_t^* = \frac{T_1 + \theta}{2} + O(\epsilon^2), \quad \tilde{T}_r^* = \frac{T_2 + \theta}{2} + O(\epsilon^2) \quad (A.18)
\]

by applying the trapezoidal rule to the integration (A.1). These expressions result in

\[
\frac{\tilde{T}_t^* - \tilde{T}_r^*}{T_\epsilon(p)} = \frac{\epsilon}{2} + O(\epsilon^2), \quad (A.19)
\]

which is equivalent to

\[
\frac{\tilde{\beta}_t^* - \tilde{\beta}_r^*}{\beta_*(p)} = \frac{\epsilon}{2} + O(\epsilon^2). \quad (A.20)
\]

Together with (A.13), this relation leads to

\[
\tilde{\beta}_t^* = \tilde{\beta}_* \left( 1 + \frac{\epsilon N_t^*}{2 N} \right), \quad \tilde{\beta}_r^* = \tilde{\beta}_* \left( 1 - \frac{\epsilon N_r^*}{2 N} \right). \quad (A.21)
\]

Multiplying the formula (A.13) and \( \tilde{T} = (N_t^* \tilde{T}_t^* + N_r^* \tilde{T}_r^*)/N \), and applying (A.3), we have

\[
\tilde{\beta}_* \tilde{T}_* = \left( \frac{N_t^*}{N} \right)^2 + \left( \frac{N_r^*}{N} \right)^2 + \frac{N_t^* N_r^*}{N^2} \left( \frac{\tilde{\beta}_t^*}{\tilde{\beta}_*} + \frac{\tilde{\beta}_r^*}{\tilde{\beta}_*} \right). \quad (A.22)
\]

Since (A.21) leads to \( \tilde{\beta}_t^*/\tilde{\beta}_r^* = 1 + \epsilon/2 + O(\epsilon^2) \), we transform (A.22) into

\[
\tilde{\beta}_* = \frac{1}{T_*} + O(\epsilon^2), \quad (A.23)
\]

using \( N_t^* + N_r^* = N \). By a similar argument, we can show

\[
\tilde{\alpha}_* = -\frac{\tilde{\mu}_*}{T_*} + O(\epsilon^2). \quad (A.24)
\]

Thus, we can write the fundamental relation of thermodynamics (IV.8) as

\[
dS = \tilde{\beta}_* dH - \tilde{\beta}_* V_* dp + \tilde{\alpha}_* dN + \Psi d\phi. \quad (A.25)
\]

### Appendix B: Derivation of (V.1) and (V.2)

We first argue the concept of intensive and extensive variables in Appendix B1. Next, in Appendix B2, we determine \( \Psi \) from the variational equations and fundamental thermodynamic relations. In Appendix B3, we formulate the singularity at \( \epsilon = 0 \). Finally, in Appendix B4, we determine \( \psi \) and \( \lambda \). Appendix B5 is devoted to discussion on the singularity.

#### 1. Intensive and extensive variables

Since heat conduction states are inhomogeneous along the horizontal direction parallel to the heat current, the extensive property is not trivial for global thermodynamic variables. On the other hand, thermodynamic states are homogeneous along the section perpendicular to the heat current, and therefore we can consider the
extensive property for the size scaling procedure in this direction. As schematically shown in Fig. 9, we fix $L_x$ and $J$ in the argument below, where $J$ is defined as the current per unit area. The total amount of heat current is proportional to $L_y L_z$.  

We define an intensive variable $\phi$ indicating the degree of nonequilibrium, which is proportional to $\varepsilon$ and invariant for the scaling transformation of $L_y L_z \rightarrow aL_y L_z$ with $H \rightarrow aH$ and $N \rightarrow aN$ in Fig. 9, where $a$ is an arbitrary constant. This invariance allows $\phi$ to depend on $\hat{h} = H/N$ and $p$. Thus, we express $\phi$ as

$$\phi = \frac{\varepsilon}{\lambda(\hat{h}, p)} \quad \text{(B.1)}$$

without loss of generality, where $\lambda$ is an intensive function to be determined in the steady state.

As the conjugate variable to $\phi$, we set $\Psi$ as it is an extensive variable. More precisely, $\Psi(H, p, N, \phi)$ is equal to the steady state value $\psi_s$ determined as (IV.5) from $\psi(H^\ell, N^\ell; H, p, N)$. For the scaling transformation in Fig. 9, the extensivity is expressed as

$$a \psi(H^\ell, N^\ell; H, p, N) = \psi(a H^\ell, a N^\ell; aH, p, aN). \quad \text{(B.2)}$$

Differentiating both sides in $a$ and setting $a = 1$, we have the Euler relation,

$$\psi = \frac{\partial \psi}{\partial H^\ell} H^\ell + \frac{\partial \psi}{\partial N^\ell} N^\ell + \frac{\partial \psi}{\partial H} H + \frac{\partial \psi}{\partial N} N. \quad \text{(B.3)}$$

2. Determination of $\psi$ and $\Psi$

Differentiating the variational function $\mathcal{J}$ in (IV.3), we have

$$\frac{\partial \mathcal{J}}{\partial H^\ell} = (\hat{\beta}^\ell - \hat{\beta}^\ell), \quad \text{(B.4)}$$

$$\frac{\partial \mathcal{J}}{\partial N^\ell} = (\alpha^\ell - \alpha^\ell), \quad \text{(B.5)}$$

$$\frac{\partial \mathcal{J}}{\partial H} = \hat{\beta}^\ell + \phi \frac{\partial \psi}{\partial H}, \quad \text{(B.6)}$$

$$\frac{\partial \mathcal{J}}{\partial p} = -\hat{\beta}^\ell V^\ell - \hat{\beta}^\ell V^\ell + \phi \frac{\partial \psi}{\partial p}, \quad \text{(B.7)}$$

$$\frac{\partial \mathcal{J}}{\partial N} = \alpha^\ell + \phi \frac{\partial \psi}{\partial N}, \quad \text{(B.8)}$$

$$\frac{\partial \mathcal{J}}{\partial \phi} = \psi. \quad \text{(B.9)}$$

Comparing these with (IV.11), (IV.12), (IV.13), (IV.14), (IV.15), and (IV.16), we obtain five differential equations for $\psi$ at the steady state as

$$\phi \left( \frac{\partial \psi}{\partial H^\ell} \right)_s = \hat{\beta}^\ell - \hat{\beta}^\ell, \quad \text{(B.10)}$$

$$\phi \left( \frac{\partial \psi}{\partial N^\ell} \right)_s = \alpha^\ell - \alpha^\ell, \quad \text{(B.11)}$$

$$\phi \left( \frac{\partial \psi}{\partial H} \right)_s = \hat{\beta}^\ell - \hat{\beta}^\ell, \quad \text{(B.12)}$$

$$\phi \left( \frac{\partial \psi}{\partial p} \right)_s = -\hat{\beta}^\ell V^\ell + \hat{\beta}^\ell V^\ell + \hat{\beta}^\ell V^\ell, \quad \text{(B.13)}$$

$$\phi \left( \frac{\partial \psi}{\partial N} \right)_s = \alpha^\ell - \alpha^\ell. \quad \text{(B.14)}$$

Substituting these five relations into (B.3) at the steady state, we have

$$\phi \psi = -\left( \hat{\beta}^\ell - \hat{\beta}^\ell \right) \left( H^\ell - \frac{N^\ell}{N} H \right). \quad \text{(B.15)}$$

Using (A.20) and (B.1), we further rewrite it as

$$\psi = -\frac{\lambda(\hat{h}, p)}{2} \beta_s(p) \left( H^\ell - \frac{N^\ell}{N} H \right). \quad \text{(B.16)}$$

The functional form of $\lambda(\hat{h}, p)$ still remains to be determined.

3. Relation emerged from singularity

Noting that the trivial relation $H = H^\ell + H^\ell$ with the number fraction $c^\ell \equiv N^\ell/N$ and the enthalpy per particle $\hat{\ell}^\ell = H^\ell/N^\ell$ gives

$$H^\ell - \frac{N^\ell}{N} H = -N(\hat{h}^\ell - \hat{h}^\ell)(1 - c^\ell)c^\ell, \quad \text{(B.17)}$$
We rewrite (B.16) as

$$\Psi = N \frac{\lambda}{2} \beta_c (\hat{h}^r - \hat{h}^l)(1 - c^l)c^l. \quad (B.18)$$

From the left–right symmetry, $\Psi$ should change its sign for $\varepsilon \to -\varepsilon$. Indeed, the expression in (B.18) explicitly shows this property because $c^l \leftrightarrow c^r = 1 - c^l$ for $\varepsilon \leftrightarrow -\varepsilon$ and $\hat{h}^r - \hat{h}^l$ changes its sign at $\varepsilon = 0$ as shown in Fig. 10.(c), where $\hat{q} = \hat{h}^l - \hat{h}^r$ with

$$\begin{align*}
\lim_{\varepsilon \to 0^+} \hat{h}^r(\phi) &= \hat{h}^l, \\
\lim_{\varepsilon \to 0^-} \hat{h}^r(\phi) &= \hat{h}^l, \\
\lim_{\varepsilon \to 0^+} \hat{h}^l(\phi) &= \hat{h}^l, \\
\lim_{\varepsilon \to 0^-} \hat{h}^l(\phi) &= \hat{h}^l. \quad (B.19)
\end{align*}$$

The left side region of the interface is occupied by liquid for $\varepsilon > 0$ whereas by gas for $\varepsilon < 0$. The position of the interface may jump at $\varepsilon = 0$ and the number fraction $c^l$ suddenly changes its value; i.e.,

$$\lim_{\varepsilon \to 0^+} c^l(\phi) = c^l, \quad \lim_{\varepsilon \to 0^-} c^l(\phi) = 1 - c^l. \quad (B.21)$$

with the equilibrium fraction of liquid $c^l_e$. See Fig. 10(b).

The singularity at $\varepsilon = 0$ is critical for the extension of entropy. To see it, we differentiate (IV.2) in $\phi$ with $H$, $p$, and $N$ fixed and obtain

$$\frac{\partial S}{\partial \phi} = (\hat{\beta}^r_e - \hat{\beta}^l_e) \frac{\partial H^l}{\partial \phi} + (\alpha^e - \alpha^l) \frac{\partial N^l}{\partial \phi} + \Psi + O(\varepsilon) \quad (B.22)$$

by noting $H^l = H^l(H, p, N, \phi)$ and $N^l = N^l(H, p, N, \phi)$. Comparing (B.22) with (IV.16) and applying (A.20), we obtain

$$\frac{\varepsilon}{2} \beta_c \frac{\partial H^l}{\partial \phi} + (\alpha^l - \alpha^l) \frac{\partial N^l}{\partial \phi} = O(\varepsilon). \quad (B.23)$$

At first glance, (B.23) is trivial because its left-hand side appears to be $O(\varepsilon)$. However, we should be careful to differentiate $H^l$ and $N^l$ in $\phi$ due to the singular behavior in Fig. 10. Using $\hat{h}^l$ and $c^l$, (B.23) is transformed into

$$\left(\alpha^l - \alpha^l + \frac{\varepsilon}{2} \beta_c \hat{h} \right) \frac{\partial c^l}{\partial \phi} = \frac{\varepsilon}{2} \beta_c \frac{\partial (\hat{h}^l - \hat{h}^l)c^l(1 - c^l)}{\partial \phi}. \quad (B.24)$$

We thus need to define the singular functions $c^l$ and $\hat{h}^l$. We introduce a regularization parameter $\varepsilon_1$ to make $c^l(\phi)$ a smooth function in $\varepsilon$:

$$c^l(\phi) = \frac{1}{2} + \left( \frac{c^l - 1}{2} \right) \tanh \left( \frac{\varepsilon}{\varepsilon_1} \right). \quad (B.25)$$

Since $\hat{h}^l(\phi) - \hat{h}^l(\phi)$ is antisymmetric in $\varepsilon$, we write

$$\hat{h}^l(\phi) - \hat{h}^l(\phi) = \hat{q} \tanh \left( \frac{\varepsilon}{\varepsilon_2} \right) \quad (B.26)$$

with another regularization parameter $\varepsilon_2$. Note that $\varepsilon_1$ and $\varepsilon_2$ should be set to zero after the calculation.

Accepting these regularizations, we can calculate the derivatives with $\phi$ at $\varepsilon = 0$ as

$$\frac{\partial c^l}{\partial \phi}_{|_{\varepsilon=0}} = \lambda \frac{c^l - 1}{\varepsilon_1}, \quad \frac{\partial (\hat{h}^l - \hat{h}^l)}{\partial \phi}_{|_{\varepsilon=0}} = \lambda \frac{\hat{q}}{\varepsilon_2} \quad (B.27)$$

See Sec. B.5 for the interpretation of the regularization parameters.

Substituting the derivatives (B.27) into (B.24), we obtain

$$\alpha^l - \alpha^l + \frac{\varepsilon}{2} \beta_c \hat{h} = \frac{\varepsilon_1}{\varepsilon_2} \beta_c \hat{q} c^l(1 - c^l), \quad (B.28)$$

where we ignored the contribution of $O(\varepsilon^2)$. Now, we consider the limit $\varepsilon_1 \to 0$ and $\varepsilon_2 \to 0$ with $\varepsilon_1/\varepsilon_2$ fixed. The right-hand side of (B.28) diverges at $c^l = 1/2$ if $\varepsilon_1/\varepsilon_2 \neq 0$, while the left-hand side remains regular. To avoid such inconsistency, the only possible case is that $\varepsilon_1/\varepsilon_2 = 0$, which leads to

$$\alpha^l - \alpha^l + \frac{\varepsilon}{2} \beta_c \hat{h} = 0. \quad (B.29)$$

We mention that (B.29) provides the balance of chemical potential in heat conduction.

4. Determination of $\psi$ and $\lambda$

Since the functional form of $\Psi$ is expressed as (B.16), we set $\psi$ as

$$\psi(\hat{h}^l, N^l; H, p, N) = -\frac{B}{2} \beta_c(p) \left( \hat{h}^l - \frac{N^l}{N} H \right), \quad (B.30)$$

where $B$ is an intensive function

$$B = B \left( \frac{\hat{h}^l}{N}, \frac{N^l}{N}, \frac{H}{N}, p \right). \quad (B.31)$$
Note that $B$ is independent of $\phi$ because $\psi$ does not depend on $\phi$. To be consistent with (B.16), we have

$$B_\ast = \lambda(\hat{h},p).$$  \hspace{1cm} (B.32)

Differentiating (B.30), we have

$$\frac{\partial \psi}{\partial \mathcal{H}^t} = -\frac{B}{2} \beta_c(p) - \frac{\beta_c(p)}{2N} \left( \mathcal{H}^t - \frac{N^t}{N} H \right) \frac{\partial B}{\partial (\mathcal{H}^t/N)},$$  \hspace{1cm} (B.33)

$$\frac{\partial \psi}{\partial N^t} = \frac{B}{2} \beta_c(p) H - \frac{\beta_c(p)}{2N} \left( \mathcal{H}^t - \frac{N^t}{N} H \right) \frac{\partial B}{\partial (N^t/N)},$$  \hspace{1cm} (B.34)

$$\frac{\partial \psi}{\partial H} = \frac{B}{2} \beta_c(p) \frac{N^t}{N} - \frac{\beta_c(p)}{2N} \left( \mathcal{H}^t - \frac{N^t}{N} H \right) \frac{\partial B}{\partial (N^t/N)},$$  \hspace{1cm} (B.35)

$$\frac{\partial \psi}{\partial p} = -\frac{B}{2} \frac{d\beta_c}{dp} \left( \mathcal{H}^t - \frac{N^t}{N} H \right) - \frac{\beta_c(p)}{2} \left( \mathcal{H}^t - \frac{N^t}{N} H \right) \frac{\partial B}{\partial p}.$$  \hspace{1cm} (B.36)

Comparing (B.10), (B.11), and (B.12) with (B.33), (B.34), and (B.35), respectively, we obtain

$$\left( \frac{\partial B}{\partial (\mathcal{H}^t/N)} \right)_\ast = 0,$$  \hspace{1cm} (B.37)

$$\left( \frac{\partial B}{\partial (H/N)} \right)_\ast = 0,$$  \hspace{1cm} (B.38)

$$\left( \frac{\partial B}{\partial (N^t/N)} \right)_\ast = 0,$$  \hspace{1cm} (B.39)

where we have used (A.13), (A.16), (A.20), (A.21), (B.29), and (B.32). Meanwhile, (B.13) and (B.36) bring a relation

$$\left( \frac{\partial B}{\partial p} \right)_\ast = -B \left( \frac{1}{\beta_c} \frac{d\beta_c}{dp} + \frac{N^tV^t - N^tV^t}{N^t H^t - N^t H^t} \right).$$  \hspace{1cm} (B.40)

The Clausius–Clapeyron relation

$$\frac{dT}{dp} = T_c \frac{\dot{\bar{v}} - \bar{\bar{v}}}{\bar{\bar{h}} - \bar{\bar{h}}}$$  \hspace{1cm} (B.41)

leads to the simplification of (B.40). Indeed, noting $N^tV^t - N^tV^t = (\hat{\bar{\bar{v}}} - \bar{\bar{v}})N^tV^t$ with specific volumes $\hat{\bar{\bar{v}}}^t$ and $N^tH^t - N^tH^t = (\hat{\bar{\bar{h}}} - \bar{\bar{h}})N^tV^t$, we obtain

$$\left( \frac{\partial B}{\partial p} \right)_\ast = 0.$$  \hspace{1cm} (B.42)

Summarizing (B.37), (B.38), (B.39), and (B.42), we find that $B$ takes the form

$$\lambda_0 + \sum_{k+l \geq 2} a_{k,l}(\mathcal{H}^t - H^t(H,p,N,\phi))^{k}(N^t - N^t(H,p,N,\phi))^l$$  \hspace{1cm} (B.43)

with a numerical constant $\lambda_0$, where $a_{k,l}$ are functions of $(\mathcal{H}^t,N^t,H,p,N)$. However, since $B$ does not explicitly depend on $\phi$, $H^t(H,p,N,\phi)$ should not appear in $B$. This means that $a_{kl} = 0$, and we conclude

$$B = \lambda_0.$$  \hspace{1cm} (B.44)

Thus, (B.30) is written as

$$\psi = \frac{\lambda_0}{2} \beta_c(p) \left( \mathcal{H}^t - \frac{N^t}{N} H \right).$$  \hspace{1cm} (B.45)

Recalling (IV.2), (IV.3), and the fundamental relation of thermodynamics (IV.8), the value of the numerical constant $\lambda_0$ does not affect experimental observations at all. Thus, we set $\lambda_0 = 1$ without loss of generality. We then reach (V.1) and (V.2).

5. Interpretation of the regularization parameters

Mathematically, the regularization parameters $\epsilon_1$ and $\epsilon_2$ are introduced to set the discontinuous functions in Figs. 10(b) and (c) to be a limit of continuous functions (B.25) and (B.26). We here provide their interpretation. As demonstrated in Fig. 5, two configurations, $(\ell,r) = (L,G)$ and $(\ell,r) = (G,L)$, are equivalent at $\epsilon = 0$ due to the left–right symmetry of the system. The symmetry is violated by imposing heat current: In $\epsilon > 0$, the probability of observing the configuration with $(\ell,r) = (L,G)$ becomes higher than that with $(\ell,r) = (G,L)$ because the temperature of the left region is lower than the right region. The probability approaches unity beyond some magnitude of $\epsilon$, which corresponds to the regularization parameters. For $\epsilon$ beyond the regularization parameters, we observe the steady states as shown in Fig. 10(a).

Recalling that the enthalpy and particle number are both conserved quantities, their spatial distributions are not necessarily functionally dependent. This indicates that $\epsilon_1$ can be intrinsically independent of $\epsilon_2$. The two regularization parameters should satisfy $\epsilon_1/\epsilon_2 \rightarrow 0$ in the limit $\epsilon_1 \rightarrow 0$ and $\epsilon_2 \rightarrow 0$ for the present framework to be consistent as discussed in Appendix B.3. Although we do not have a physical interpretation of this result, we expect that such regularization parameters may naturally appear in the analysis of statistical mechanics of the phase separation in heat conduction. Performing molecular dynamics simulations of finite-size systems, we observe the obvious separation of the liquid from gas when $|J|$ is not too much small. The separation becomes subtle for sufficiently small but non-vanishing values of $|J|$. For instance, liquid and gas regions fluctuate and sometimes exchange, which leads to the smearing of the discontinuous change at $J = 0$. The crossover value of $|J|$ depends on the system size. Characterizing such finite-size smearing effects may shed light on the properties of the regularization.
Appendix C: Derivation of (VI.2)

From local thermodynamic relation $h(x) - \mu(x)\rho(x) = T(x)s(x)$, we have

$$H - G = L_y L_z \int_0^{L_x} dx \, T(x)s(x). \quad (C.1)$$

Decompose the integral of the right-hand side as

$$\int_0^{L_x} dx \, T(x)s(x) = \hat{T} \int_0^{L_x} dx \, s(x) + \int_0^{L_x} dx \, (T(x) - \hat{T})\rho(x)s(x), \quad (C.2)$$

where $\hat{s}(x) = s(x)/\rho(x)$. $\hat{s}(x)$ is discontinuous at the interface; i.e., $\hat{s}(x) = \hat{s}^f(T(x), p)$ for $0 < x < X$ and $\hat{s}(x) = \hat{s}^r(T(x), p) + O(\epsilon)$ for $X < x < L_x$. We then estimate $\hat{s}^r(T(x), p) = \hat{s}^f(T_c(p), p)$, where $\hat{s}^f(T_c(p), p) = \hat{s}^r(T_c(p), p)$. Ignoring the contribution of $O(\epsilon^2)$, we transform the last term of (C.2) as

$$\hat{s}^f \int_X^1 dx \, (T(x) - \hat{T})\rho(x) + \hat{s}^r \int_0^{L_x} dx \, (T(x) - \hat{T})\rho(x)$$

$$= \hat{s}^f(\hat{T} - \hat{T}) \frac{N^\ell}{L_y L_z} + \hat{s}^r(\hat{T} - \hat{T}) \frac{N^r}{L_y L_z}, \quad (C.3)$$

where the second line is obtained from the definition of the global temperature for each region. From $NT = N^\ell \hat{T} + N^r \hat{T}$, we also have

$$\hat{T}^\ell - \hat{T} = - \frac{N^r}{N}(\hat{T}^r - \hat{T}^\ell), \quad \hat{T}^r - \hat{T} = \frac{N^\ell}{N}(\hat{T}^\ell - \hat{T}^r). \quad (C.4)$$

Substituting these two relations into (C.3), we express the right-hand side as

$$\phi T_c(p)(\hat{s}^f - \hat{s}^r) \frac{N^\ell N^r}{2N} \frac{1}{L_y L_z}, \quad (C.5)$$

where we have used (D.9) and (D.10). Note that $\hat{s}^f - \hat{s}^r = \hat{q}T_c$ when $(\ell, r) = (L, G)$ and $-\hat{q}T_c$ when $(\ell, r) = (G, L)$. As $(\ell, r) = (L, G)$ for $\phi > 0$ and $(G, L)$ for $\phi < 0$, we further rewrite (C.5) as

$$|\phi|\hat{q}(p) \frac{N^\ell N^G}{2N} \frac{1}{L_y L_z}. \quad (C.6)$$

Comparing (C.6) with $\Psi$ in (V.3), we conclude

$$\int_0^{L_x} dx \, (T(x) - \hat{T})\rho(x)s(x) = \frac{T_c(p)\phi\Psi}{L_y L_z}. \quad (C.7)$$

Then, noting $\tilde{T} = T_c(p) + O(\epsilon)$, we write (C.1) as

$$H - G = \tilde{T} \left( L_y L_x \int_0^{L_x} dx \, s(x) + \phi\Psi \right), \quad (C.8)$$

which is (VI.2).

Appendix D: Equivalence of (V.5) to (VI.16)

According to (A.4) and (A.5), we write

$$\alpha^\ell = \alpha^f(\tilde{\beta}^\ell, p), \quad \alpha^r = \alpha^r(\tilde{\beta}^r, p). \quad (D.1)$$

We expand these functions around $\beta_c(p)$ as

$$\alpha^\ell = \alpha^f(\beta_c(p), p) - (\tilde{\beta}^\ell - \beta_c(p))\hat{h}^\ell + O(\epsilon^2), \quad (D.2)$$

$$\alpha^r = \alpha^r(\beta_c(p), p) - (\tilde{\beta}^r - \beta_c(p))\hat{h}^r + O(\epsilon^2), \quad (D.3)$$

where we have used $(\partial\alpha/\partial\beta)_p = \hat{h}$ resulted from the Gibbs-Duhem relation. Let us substitute these equations into a re-expressed form of (V.5); i.e., into

$$\alpha^\ell - \alpha^r + \phi\beta_c(p)H \frac{2N}{\hat{h}} = 0. \quad (D.4)$$

Then, using $\alpha^f(\beta_c(p), p) = \alpha^r(\beta_c(p), p)$ and $H = \hat{h}^\ell N^\ell + \hat{h}^r N^r$, we obtain

$$-(\tilde{\beta}^\ell - \beta_c(p))\hat{h}^\ell + (\tilde{\beta}^r - \beta_c(p))\hat{h}^r$$

$$+ \frac{\phi\hat{h}}{2} \left( \frac{N^\ell}{N}\hat{h}^\ell + \frac{N^r}{N}\hat{h}^r \right) = 0, \quad (D.5)$$

where $\phi\beta_c(p)$ is replaced by $\phi\hat{h}$ by ignoring the difference of $O(\epsilon^2)$. Substituting (A.21) into $\beta^\ell$ and $\beta^r$, we further transform (D.5) into

$$\hat{h}^r - \hat{h}^\ell \left[ \tilde{\beta} + \frac{\phi N^r}{2N} \right] \beta_c(p) = 0. \quad (D.6)$$

Since $|\hat{h}^r - \hat{h}^\ell|$ at $\epsilon = 0$ corresponds to the latent heat $\hat{q}$, $\hat{h}^r - \hat{h}^\ell$ is non-zero. Thus, we conclude that the variational principle (V.5) is written as

$$\tilde{\beta} = \beta_c(p) \left( 1 - \frac{\phi N^r}{2N} \right), \quad (D.7)$$

which is equal to

$$\tilde{T} = T_c(p) \left( 1 + \frac{\phi N^r}{2N} \right). \quad (D.8)$$

Substituting (D.7) into (A.21), we have

$$\hat{T}^\ell = T_c(p) \left( 1 + \frac{\phi N^r}{2N} \right), \quad (D.9)$$

$$\hat{T}^r = T_c(p) \left( 1 + \frac{\phi N^r}{2N} \right). \quad (D.10)$$

We can repeat a similar procedure starting with (VI.16). We expand the two chemical potentials $\mu^\ell = \mu^f(\hat{T}^\ell, p)$ and $\mu^r = \mu^r(\hat{T}^r, p)$ as

$$\mu^\ell = \mu^f(T_c(p), p) - (\hat{T}^\ell - T_c(p))\hat{s}^\ell + O(\epsilon^2), \quad (D.11)$$

$$\mu^r = \mu^r(T_c(p), p) - (\hat{T}^r - T_c(p))\hat{s}^r + O(\epsilon^2), \quad (D.12)$$
where we have used \((\partial \mu / \partial T)_p = -\dot{s}\). Here, \(\tilde{T}^e\) and \(\tilde{T}^r\) are estimated by (A.21) with \(\tilde{T}^e = 1/\beta^e\) and \(\tilde{T}^r = 1/\beta^r\). Substituting these into (VI.16) and noting that 

\[
\mu^L(T^e(p), p) = \mu^r(T^r(p), p),
\]

we have

\[
(\tilde{s}^e - \dot{s}^e) \left( \tilde{T} - T^e(p) - \frac{\phi \tilde{T} N^r - N^e}{2} \right) = 0. \tag{D.13}
\]

Since \(\tilde{s}^e \neq \dot{s}^e\), we obtain the same relation as (D.8). That is, the steady state is equivalent.

We add a comment. Summing up the last two formulas and using (A.18) and (D.8), we have the temperature relation

\[
\tilde{T} - \frac{T_1 + T_2}{2} = \theta - T_c(p), \tag{D.14}
\]

which was derived in [31].

**Appendix E: Additivity of \(G\) and \(F\)**

According to (VI.1) and (VI.5), the free energies are expressed by additive forms,

\[
G = G^L + G^G, \tag{E.1}
\]

\[
F = F^L + F^G, \tag{E.2}
\]

where \(G^L = L_y L_z \int_0^x dx \mu^L(x) \rho(x), \ G^G = L_y L_z \int_0^x dx \mu^G(x) \rho(x), \ F^L = L_y L_z \int_0^x dx f(x)\), and \(F^G = L_y L_z \int_0^x dx f(x)\). As has been derived in [31] and shortly reviewed in Appendix A1, respective global thermodynamics hold in liquid and gas, and therefore

\[
G^L = \mu^L(\tilde{T}^L, p) N^L, \quad G^G = \mu^G(\tilde{T}^G, p) N^G, \tag{E.3}
\]

\[
F^L = F(\tilde{T}^L, V^L, N^L), \quad F^G = F(\tilde{T}^G, V^G, N^G) \tag{E.4}
\]

with respective global temperatures

\[
\tilde{T}^L = \tilde{T} \left( 1 - \phi \frac{N^G}{2N} \right), \quad \tilde{T}^G = \tilde{T} \left( 1 + \phi \frac{N^L}{2N} \right). \tag{E.5}
\]

which are consistent with (VI.13).

We notice \(\tilde{T}^L \neq \tilde{T}^G \neq \tilde{T}\) for \(\varepsilon \neq 0\). Respecting the global temperature \(\tilde{T}\), we rewrite (E.1) and (E.2) as parallel expressions to the non-additive entropy (IV.2);

\[
G = G^L(\tilde{T}, p, N^L) + G^G(\tilde{T}, p, N^G) - \phi \tilde{T} \Psi, \tag{E.6}
\]

\[
F = F(\tilde{T}, V^L, N^L) + F(\tilde{T}, V^G, N^G) - \phi \tilde{T} \Psi \tag{E.7}
\]

by expanding \(G^{L/G}\) and \(F^{L/G}\) around \(\tilde{T}\) and ignoring the contribution of \(O(\varepsilon^2)\). Here, \(G^L(\tilde{T}, p, N^L) = \mu^L(\tilde{T}, p) N^L\) and \(G^G(\tilde{T}, p, N^G) = \mu^G(\tilde{T}, p) N^G\). Despite the apparent consistency of (E.6) and (E.7) with (IV.2) for the non-additive entropy, we do not adopt \(\tilde{T}\) as the temperature to characterize liquid and gas because the fundamental thermodynamic relations of liquid and gas are (A.6) and (A.7) with \(T^{L/G}\) as each global temperature. Indeed, these fundamental relations provide

\[
dS^{L/G} \neq \frac{dH^{L/G}}{T} - V^{L/G} dP - \frac{\mu^{L/G}(\tilde{T}, p)}{T} dN^{L/G}, \tag{E.8}
\]

which implies that \(\tilde{T}\) does not work as global temperature for liquid or gas. Nevertheless, we can show

\[
S^L = \frac{H^L - G^L(\tilde{T}^L, p, N^L)}{T^L}, \tag{E.9}
\]

\[
S^G = \frac{H^G - G^G(\tilde{T}^G, p, N^G)}{T^G} = \frac{H^G - G^G(\tilde{T}, p, N^L)}{T}. \tag{E.10}
\]

This suggests that \(\tilde{T}\) plays some role of the temperature in each region.

**Appendix F: Derivations of relations in Sec. VII**

We derive various relations for the steady state in heat conduction reported in Sec. VII with assuming \(J \leq 0\). We can change \(\phi\) and \(J\) into \(|\phi|\) and \(|J|\) for the obtained relations with taking care of \(\phi\) \(\leq 0\), because these formulas are common in \(J \geq 0\). We then arrive at the formulas in Sec. VII.

1. Preliminaries

We introduce a ratio representing the particle distribution as

\[
\frac{N^L}{N} = r \equiv -r + 1, \quad \frac{N^G}{N} = r + \frac{1}{2}. \tag{F.1}
\]

by which we have

\[
\frac{N^L}{N} = -r + \frac{1}{2}, \quad \frac{N^G}{N} = r + \frac{1}{2}. \tag{F.2}
\]

We first consider equilibrium liquid–gas coexistence with \((H, p, N)\) fixed. Let \(H^{L/G}_{eq}\) and \(N^{L/G}_{eq}\) be the enthalpy and the particle number of liquid and gas at equilibrium. In the coexistence state at given \(p\), there are constraints among \(H^{L/G}_{eq}\) and \(N^{L/G}_{eq}\) such that

\[
H^{L}_{eq} = \hat{h}^{L}(p), \quad H^{G}_{eq} = \hat{h}^{G}(p), \quad N^{L}_{eq} = N^{G}_{eq}. \tag{F.3}
\]

Combining with \(H = H^{L}_{eq} + H^{G}_{eq}\) and \(N = N^{L}_{eq} + N^{G}_{eq}\), we have

\[
r_{eq} = \frac{\hat{h}^{G}(p)}{\hat{q}(p)}, \tag{F.4}
\]

where

\[
\hat{h}_{m}(p) = \frac{\hat{h}^{L}(p) + \hat{h}^{G}(p)}{2}. \tag{F.5}
\]
2. Derivation of (VII.16)

The formulas (D.8), (D.9), and (D.10) for the global temperatures $\tilde{T}$, $\tilde{T}^L$, and $\tilde{T}^G$ are rewritten with $r$ as

$$\tilde{T} = T_c (1 + \phi r) + O(\varepsilon^2), \quad (F.6)$$

$$\tilde{T}^L = T_c \left( 1 + \frac{\phi}{2} \left( r - \frac{1}{2} \right) \right), \quad (F.7)$$

$$\tilde{T}^G = T_c \left( 1 + \frac{\phi}{2} \left( r + \frac{1}{2} \right) \right). \quad (F.8)$$

By substituting (F.4) with (F.5) into these equations, we obtain

$$\tilde{T} = T_c \left( 1 + \frac{\hat{h} - \hat{h}_m}{q} \right), \quad (F.9)$$

$$\tilde{T}^L = T_c \left( 1 - \frac{\phi \hat{h}^G - \hat{h}}{q} \right), \quad (F.10)$$

$$\tilde{T}^G = T_c \left( 1 + \frac{\phi \hat{h} - \hat{h}_c}{q} \right). \quad (F.11)$$

Here, (F.9) corresponds to (VII.16).

3. Derivation of (VII.9), (VII.10) and (VII.7), (VII.8)

As demonstrated in Appendix A1, heat conduction states for liquid and gas in the linear response regime are mapped to equilibrium states. We then express

$$H^L = \hat{h}^L (\tilde{T}^L, p) N^L. \quad (F.12)$$

Substituting (F.10) into it and then expanding $\hat{h}^L$ in $\varepsilon$, we obtain

$$H^L = \left( \hat{h}_c^L - \frac{T_c}{2} \frac{\alpha_c}{\rho_c} \frac{\hat{h}^G - \hat{h}}{q} \right) N^L. \quad (F.13)$$

which is (VII.9). Similarly, we have

$$H^G = \left( \hat{h}_c^G + \frac{T_c}{2} \frac{\alpha_c}{\rho_c} \frac{\hat{h} - \hat{h}_c}{q} \right) N^G. \quad (F.14)$$

which is (VII.10). Recalling that $H = H^L + H^G$ and applying (F.2) and (F.4), we have

$$\hat{h} = \left( \frac{1}{2} - r \right) \hat{h}_c^L + \left( \frac{1}{2} + r \right) \hat{h}_c^G$$

$$- \frac{T_c}{2} \left[ \left( \frac{\hat{h}_c^G - \hat{h}}{q} \right)^2 \frac{\alpha_c}{\rho_c} - \left( \frac{\hat{h} - \hat{h}_c}{q} \right)^2 \frac{\alpha_c}{\rho_c} \right]. \quad (F.15)$$

Solving (F.15) in $r$, we obtain

$$r = \frac{\hat{h} - \hat{h}_m}{q} + \frac{T_c}{2q} \left[ \left( \frac{\hat{h}_c^G - \hat{h}}{q} \right)^2 \frac{\alpha_c}{\rho_c} - \left( \frac{\hat{h} - \hat{h}_c}{q} \right)^2 \frac{\alpha_c}{\rho_c} \right]. \quad (F.16)$$

Thus, the value of $r$ is uniquely determined for given $\hat{h}$ and $p$. Explicitly, the number of particles is written as

$$\frac{N^L}{N} = \frac{\hat{h}_c^G - \hat{h}}{\hat{h}} - \frac{T_c}{2q} \left[ \left( \frac{\hat{h}_c^G - \hat{h}}{q} \right)^2 \frac{\alpha_c}{\rho_c} - \left( \frac{\hat{h} - \hat{h}_c}{q} \right)^2 \frac{\alpha_c}{\rho_c} \right],\quad (F.17)$$

$$\frac{N^G}{N} = \frac{\hat{h} - \hat{h}_c}{q} + \frac{T_c}{2q} \left[ \left( \frac{\hat{h}_c^G - \hat{h}}{q} \right)^2 \frac{\alpha_c}{\rho_c} - \left( \frac{\hat{h} - \hat{h}_c}{q} \right)^2 \frac{\alpha_c}{\rho_c} \right], \quad (F.18)$$

which correspond to (VII.7) and (VII.8).

4. Derivation of (VII.11) and (VII.12)

The volumes of liquid and gas are connected to the densities as

$$V^{L/G} = \frac{N^{L/G}}{\rho^{L/G}} = \frac{N^{L/G}}{N} \frac{N}{\rho^{L/G}}. \quad (F.19)$$

By substituting (F.7) and (F.8) into $\rho^L = \rho^L(\tilde{T}^L, p)$ and $\rho^G = \rho^G(\tilde{T}^G, p)$ and expanding them in $\varepsilon$, we have

$$\rho^L = \rho_c^L \left[ 1 - \frac{\phi T_c}{2} \left( \frac{r - \frac{1}{2}}{\rho_c^L} \right) \alpha_c^L \right], \quad (F.20)$$

$$\rho^G = \rho_c^G \left[ 1 - \frac{\phi T_c}{2} \left( \frac{r + \frac{1}{2}}{\rho_c^G} \right) \alpha_c^G \right], \quad (F.21)$$

where $\alpha_c^L$ and $\alpha_c^G$ are thermal expansion coefficients of liquid and gas at constant pressure, defined by

$$\alpha_c^L = -\frac{1}{\rho_c^L} \left( \frac{\partial \rho^L}{\partial T} \right)_p, \quad \alpha_c^G = -\frac{1}{\rho_c^G} \left( \frac{\partial \rho^G}{\partial T} \right)_p. \quad (F.22)$$

$\alpha_c^L$ and $\alpha_c^G$ are the values at the saturation. Thus, (F.19) leads to

$$V^L = \frac{N^{L/G}}{\rho_c^L} \left[ 1 + \phi \frac{T_c}{2} \left( r - \frac{1}{2} \right) \alpha_c^L \right], \quad (F.23)$$

$$V^G = \frac{N^{L/G}}{\rho_c^G} \left[ 1 + \phi \frac{T_c}{2} \left( r + \frac{1}{2} \right) \alpha_c^G \right]. \quad (F.24)$$
Substituting (F.16), (F.17), and (F.18) into these, \(V^L\) and \(V^G\) for given \((\hat{h}, p, \phi)\) are written as

\[
V^L = \frac{N}{\rho_c^L} \left[ \frac{\hat{h}^G - \hat{h}}{q} - \phi \frac{T_c}{2} \left( \frac{\hat{h}^G - \hat{h}}{q} \right)^2 \alpha^L_c \right]
- \phi \frac{T_c}{2q} \left( \left( \frac{\hat{h}^G - \hat{h}}{q} \right)^2 \varepsilon_p^L - \left( \frac{\hat{h}^L - \hat{h}}{q} \right)^2 \varepsilon_p^G \right),
\]

(F.25)

\[
V^G = \frac{N}{\rho_c^L} \left[ \frac{\hat{h} - \hat{h}^L}{q} + \phi \frac{T_c}{2} \left( \frac{\hat{h} - \hat{h}^L}{q} \right)^2 \alpha^L_c \right]
+ \phi \frac{T_c}{2q} \left( \left( \frac{\hat{h}^G - \hat{h}}{q} \right)^2 \varepsilon_p^L - \left( \frac{\hat{h}^L - \hat{h}}{q} \right)^2 \varepsilon_p^G \right),
\]

(F.26)

which are (VII.11) and (VII.12).

5. Derivation of (VII.13)

We define the normalized position of the liquid–gas interface as

\[
x \equiv \frac{X}{L_x} = \frac{V^L}{V^L + V^G}.
\]

(F.27)

From (F.25) and (F.26), the volumes in equilibrium are written as

\[
V^L_{eq} = \frac{N}{\rho_c^L} \frac{\hat{h}^G - \hat{h}}{q}, \quad V^G_{eq} = \frac{N}{\rho_c^L} \frac{\hat{h} - \hat{h}^L}{q},
\]

(F.28)

and the ratio of the volume in heat conduction deviates from the equilibrium ratio as

\[
\frac{V^G}{V^L} = \frac{V^G_{eq}}{V^L_{eq}} \left( 1 + \phi \frac{T_c}{2} A \right),
\]

(F.29)

where

\[
A = \alpha^L_c \frac{\hat{h} - \hat{h}^L}{q} + \alpha^G_c \frac{\hat{h}^G - \hat{h}}{q} + \frac{\varepsilon_p^L}{q} \frac{\hat{h}^G - \hat{h}}{q} \frac{\hat{h}^L - \hat{h}}{q} \frac{\hat{h}^G - \hat{h}}{q}.
\]

(F.30)

From (F.27) and (F.29), it is found that

\[
x - x_{eq} = -\phi \frac{T_c}{2} \left( 1 + \frac{V^G}{V^L} \right)^{-2} \frac{V^G_{eq}}{V^L_{eq}} A.
\]

(F.31)

Here, the equilibrium position \(x_{eq}\) is calculated from (F.27) and (F.28) as

\[
x_{eq} = \frac{\rho_c^G (\hat{h}^G - \hat{h})}{\rho_c^L (\hat{h} - \hat{h}^L)} + \frac{\rho_c^G (\hat{h}^G - \hat{h})}{\rho_c (\hat{h}^G - \hat{h})}.
\]

(F.32)

Since \(V^G_{eq}/V^L_{eq}\) is connected to \(x_{eq}\), we have

\[
x - x_{eq} = -\phi \frac{T_c}{2} x (1 - x_{eq}) A
= -\phi \frac{T_c}{2} x_{eq} (1 - x_{eq}) \times
\]

\[
\left[ \frac{\hat{h} - \hat{h}^L}{q} + \frac{\varepsilon_p^L}{q} \frac{\hat{h}^G - \hat{h}}{q} + \frac{\varepsilon_p^G}{q} \frac{\hat{h} - \hat{h}^L}{q} \frac{\hat{h}^L - \hat{h}}{q} \right],
\]

(F.33)

which corresponds to (VII.13).

6. Derivation of (VII.1)

Since the steady heat current \(J\) is homogeneous in the container, we have

\[
J = -\kappa^L_c \frac{\theta - T_1}{X} = -\kappa^G_c \frac{T_2 - \theta}{L_x - X},
\]

(F.34)

which leads to

\[
\theta = \frac{\kappa^L_c}{\kappa^G_c} (L_x - X) T_1 + \frac{\kappa^G_c X}{\kappa^L_c} T_2.
\]

(F.35)

Using this expression, (F.34) is written as

\[
J = -\kappa^L_c (1 - x_{eq}) + \kappa^G_c x_{eq} \frac{T_2 - T_1}{L_x}.
\]

(F.36)

Substituting (F.32) into (F.36), we arrive at (VII.1).

7. Derivation of (VII.2)

The uniformity of the heat current in \(x\),

\[
J = -\kappa^L_c \frac{\theta - T_1}{X} = -\kappa^G_c \frac{T_2 - \theta}{L_x - X},
\]

(F.37)

leads to

\[
\hat{T}^L = \theta + J \frac{X}{2\kappa^L_c} \phi,
\]

(F.38)

\[
\phi = -\frac{J}{T_c(p)} \left( \frac{X}{\kappa^L_c} + \frac{L_x - X}{\kappa^G_c} \right),
\]

(F.39)

where \(\hat{T}^L = (T_1 + \theta)/2\) and \(\phi = (T_2 - T_1)/T_c(p)\). Substituting (F.38) and (F.39) into (D.9), we obtain

\[
\theta = T_c(p) - \frac{J L_x}{2} \left( \frac{X}{N^G_c} \frac{N^L_c}{N_c^L} - \frac{L_x - X}{N^L_c} \frac{N^G_c}{N_c^G} \right).
\]

(F.40)

Since (F.19) yields

\[
\frac{N^L_c}{N} = \frac{X}{L_x} \frac{\rho^L_c}{\rho}, \quad \frac{N^G_c}{N} = \frac{L_x - X}{L_x} \frac{\rho^G_c}{\rho},
\]

(F.41)
where \( \tilde{\rho} = N/V \), we write (F.40) as

\[
\theta = T_c(p) - \frac{J}{\rho} \left( \frac{1}{\kappa_c^{G}} \left[ \kappa_c^{G} \kappa_c^{L} - \frac{1}{\kappa_c^{L}} \right] - \frac{1}{\rho} \kappa_c^{L} \right) \frac{X(L_x - X)}{2L_x}. \tag{F.42}
\]

Using

\[
\tilde{\rho} = \frac{X}{L_x} \rho^L + \frac{L_x - X}{L_x} \rho^G, \tag{F.43}
\]

we have

\[
\frac{\rho^G C}{\tilde{\rho}^0} \frac{1}{\kappa_c^{G}} \frac{1}{\kappa_c^{L}} = \frac{1}{\kappa_c^{L}} - \frac{1}{\kappa_c^{G}} \frac{X}{\kappa_c^{G} L_x} + \frac{L_x - X}{\kappa_c^{L} L_x} \frac{\rho^L - \rho^G}{\tilde{\rho}} \tag{F.44}
\]

\[
= \frac{1}{\kappa_c^{L}} - \frac{1}{\kappa_c^{G}} \frac{\phi T_c}{JL_x} \frac{\rho^L - \rho^G}{\tilde{\rho}}, \tag{F.45}
\]

where we have applied (F.36) to transform into the second line. Substituting this into (F.42), we obtain

\[
\theta = T_c(p) - \left[ J \left( \frac{1}{\kappa_c^{L}} - \frac{1}{\kappa_c^{G}} \right) + \frac{\phi T_c}{JL_x} \frac{\rho^L - \rho^G}{\tilde{\rho}} \right] \frac{X(L_x - X)}{2L_x}, \tag{F.46}
\]

which corresponds to (VII.2) for \( J < 0 \). We can repeat the same argument for \( J > 0 \) and conclude (VII.2).

**Appendix G: Derivation of (VIII.1)**

We start with an expansion in \( \phi \) as

\[
S(H, p, N, \phi) = S(H, p, N) + \phi \left( \frac{\partial S}{\partial \phi} \right)_{H, p, N} + O(\varepsilon^2)
= S(H, p, N) + \phi \Psi + O(\varepsilon^2), \tag{G.1}
\]

where we used (IV.16) to obtain the second line. Let \( H_\phi \) be a slightly shifted enthalpy from \( H \), whose form will be determined. Assuming \( H - H_\phi = O(\varepsilon) \), we have

\[
S(H, p, N) = S(H_\phi, p, N) + \left( \frac{\partial S}{\partial H} \right)_{p, N} (H - H_\phi) + O(\varepsilon^2). \tag{G.2}
\]

Comparing this form with (G.1), we find that the term \( \phi \Psi \) in (G.1) cancels out by setting \( H_\phi \) to

\[
H_\phi = H + T_c(p) \phi \Psi. \tag{G.3}
\]

Thus, we can write

\[
S(H, p, N, \phi) = S(H_\phi, p, N) \tag{G.4}
\]

in the linear response regime. We interpret that (G.4) defines an isentropic surface to connect a heat conduction state \( (H, p, N, \phi) \) with an equilibrium state \( (H_\phi, p, N) \).

Since the right-hand side of (G.4) is the equilibrium entropy, the nonequilibrium entropy can be expressed by the sum of the entropy of liquid and gas in (VIII.1); i.e.,

\[
S(H, p, N, \phi) = S(H_\phi^L, p, N_\phi^L) + S(H_\phi^G, p, N_\phi^G), \tag{G.5}
\]

with \( N = N_\phi^L + N_\phi^G \) and \( H_\phi = H_\phi^L + H_\phi^G \). We emphasize that \( H_\phi \neq H \) indicates \( H \neq H_\phi^L + H_\phi^G \). This may be another aspect of the violation of the additivity of the liquid–gas coexistence in heat conduction.

We can identify \( H_\phi^L/G \) and \( N_\phi^L/G \) as functions of \( (H, p, N, \phi) \). Substituting \( H_\phi^L = \hat{h}_\phi^L(p) N_\phi^L \), \( H_\phi^G = \hat{h}_\phi^G(p) N_\phi^G \), and (G.3) into \( N = N_\phi^L + N_\phi^G \) and \( H_\phi = H_\phi^L + H_\phi^G \), we obtain

\[
N_\phi^L = \frac{\hat{h}_\phi^L(p)}{\hat{q}(p)} N - H - T_c(p) \phi \Psi, \tag{G.6}
\]

\[
N_\phi^G = -\frac{\hat{h}_\phi^G(p)}{\hat{q}(p)} N - H - T_c(p) \phi \Psi. \tag{G.7}
\]

Comparing (G.6) with (F.17), we confirm \( N_\phi^L \neq N^L \) for \( \phi \neq 0 \).

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