Soft granular materials consist of close-packed deformable grains separated by thin fluid films. They are ubiquitous in industries, forming food and cosmetic products and in nature, examples including dense emulsions, foams, as well as certain types of biological tissues, among others [1–7]. The presence of the internal lengthscale in such materials, associated with the grain size, leads to a complex many-body dynamics governed by the sequences of grain deformations and rearrangements [8, 9], which in turn result in complex flows and rheological behavior, including plasticity and viscoelasticity, memory effects and avalanches [10–15].

The flow of such types of materials confined to narrow geometries is of primary interest to the physics of amorphous solids and glasses [8, 9, 16], as well as of technological relevance for the generation of compartmentalized capsules [17] and porous materials [18] or in bioprinting [19]. The dynamics of soft granular media in constrictions under external flow is also of significant interest in tissue mechanics [20], as it could shed light on the behavior of cell clusters passing through physiological constrictions, a process that remains one of the critical stages of tumor metastasis.

Previous microfluidic approaches to soft granular materials addressed the behavior of foams or dense emulsions inside channels, however without considering the interaction with an external flow [8, 9, 13, 21, 22]. Here, we systematically study the behavior of a model ‘wet’ soft-granular medium (a tightly packed monodisperse emulsion) under external viscous forces. We use a flow-focusing geometry in which the emulsion is fed through the middle channel and the external immiscible phase through the side channels. Accordingly, the emulsion is focused by the external flow and narrows until passing through an orifice, a situation which closely resembles the flow of cell clusters in capillaries.

Typically, in microfluidics, flow-focusing junctions are used to generate highly monodisperse emulsions [23]. Thus, in Newtonian liquids, one typically observes two primary dynamical modes: dripping, in which monodisperse droplets are created inside the orifice, and jetting, in which the focused phase flows in parallel with the focusing phase beyond the orifice, only to break-up much later [23–25] due to the Rayleigh-Plateau instability [24], although other regimes have also been reported [25, 26, 27].

Here, in the case of a granular medium, we find new dynamical patterns, distinct from simple viscous jetting...
and dripping, such as (i) formation of fluctuating jets in which the fluctuations of jet width are influenced by avalanche-like ‘discharge’ of the dispersed granular phase at the junction rather than by the Rayleigh-Plateau instability of the jet, (ii) formation of very thin jets—single-file chains of grains—via ‘unfolding’ of thicker jets under extensional viscous stresses, and (iii) irregular break-up of the jets resulting in highly polydisperse grain clusters with a non-Gaussian size distribution. We highlight the stochasticity of the transport of the close-packed emulsion through the orifice in the various regimes and the impact of the behavior of individual grains on the dynamics of the entire emulsion (e.g., its break-up). Furthermore, we perform ad-hoc numerical simulations based on a recently developed Lattice Boltzmann method for multi-component fluids with near-contact interactions [28, 29] which reproduce the experimental findings. The simulations employ a perfectly monodisperse emulsion which demonstrates that the observed stochasticity of the system is intimately associated with the granular structure and not, in particular, with polydispersity of the droplets.

The droplets (‘grains’) of the innermost phase are reproducibly formed at a T-junction of channels of rectangular cross-sections. Subsequently, the monodisperse emulsion is pushed into a wider channel (see Fig. 1) and focused by the continuous phase into an orifice. We use three Newtonian liquids to formulate the double emulsion: fluorinated fluid [30] as the continuous phase, oil with surfactant as the middle (lubricating) phase, and dyed water as the innermost ‘grain’ phase (see SM for details). The T-junction generates droplets at a volume fraction of 86% (the highest possible for which the emulsion is monodisperse and stable). Based on measured frequency of generation of the aqueous droplets, we estimate droplet volume to be around 0.11 pL which yields the diameter of an undeformed spherical droplet $D_0 = 0.28$ mm. Since the value of $D_0$ is larger than the channel height $H = 0.11$ mm, the droplets are flattened by the lower and upper walls. Based on the measured apparent areas of the generated clusters we estimate the diameter of the flattened droplets $D_{||} = 0.37$ mm with a coefficient of variation $CV_{D_{||}} = 9.2\%$.

The ensuing emulsion is stable enough to produce flows for several minutes, with only occasional coalescence of the aqueous droplets.

Our LB simulations, performed using a fully three-dimensional Color-Gradient approach augmented with near-contact interactions [28, 29], use slightly different, but similar, parameters for the system and droplets. See SM and [31] for details on the simulation methods and implementation.

In the experiment, we change the flow rate of the continuous phase $Q_c$, while keeping the flow rate of the dispersed phase (the emulsion) $Q_d$ constant and equal $Q_d = 0.5$ mL/h [32]. As a result, we observe several types of dynamic flow patterns as illustrated in Fig. 2 and movies SM1–SM4. We find superficial similarity to jetting and dripping regimes present in simple fluids, however the observed dynamics is much richer. We can distinguish four different modes: (i) jetting with a large and moderately oscillating jet width, further referred to simply as jetting (ii) jetting with thin, strongly oscillating jets and occasional break-up, further referred to as oscillating jetting (iii) dripping resulting in a strongly polydisperse double-emulsion, further referred to as irregular dripping (iv) dripping resulting in a relatively monodisperse double-emulsion, further referred to simply as dripping. The numerical simulations recreate the same dynamical modes at values $Q_c/Q_d$ similar to yet slightly different than the experimental ones, see Fig. 2 and movies SM5–SM8. We attribute the differences to slightly different geometrical parameters and volume fractions as imposed by the numerical constrains (see SM).

In order to understand the impact of granularity of the focused fluid on the onset of oscillating jetting/irregular dripping regimes, we repeat the flow focusing experiment with a simple fluid (water or oil) as the dispersed phase. We find simple jetting (see SM9 and SM10 for oil at $Q_c/Q_d = 1$ and 2 respectively), highly monodisperse dripping ($CV_{A_{||}} = 2.2\%$ for oil, where $A_{||}$ is the area of a flattened oil drop, at $Q_c/Q_d = 3$; see SM11) or bi-disperse dripping [33] (the latter, with 2 narrow peaks, in the case with oil at high $Q_c/Q_d$, see SM12 and SM13 for examples with $Q_c/Q_d = 4$ and 8 respectively; see SM for relevant histograms), but never observe irregular oscillations and rich dynamics similar to the case of a focused emulsion (see Fig. 2). In particular, we find only dripping for the case with water and the jetting-dripping transition for oil, which both agree with previous predic-
FIG. 3. (a) Fluctuations of the minimum jet width $w_{\text{min}}(t)$ (b) Fluctuations of jet width $w_0(t)$ at the entrance to the constriction. The avalanche-like events are marked with arrows. (c) Number of grains $N$ in clusters generated in the dripping and irregular dripping regimes ($Q_c/Q_d = 16$ and 8) vs the index of cluster $i$ in order of generation, and (d)-(e) the corresponding histograms $n(N)$. The histogram in (f) shows analogous data for a system with a much thinner and longer orifice, yet with $Q_c/Q_{c,\text{match}}$ very close to the case in (e) (see main text and SM for further discussion).

We further examine the four distinct dynamical modes observed for the focused emulsion in more detail. We define the minimum instantaneous jet width, $w_{\text{min}}(t) = \min_{x \in [0, L]} w(x, t)$ where $w(x, t)$ is the full spatio-temporal profile of the jet within the narrowing, as a measure of jet oscillations in time (Fig. 3a). We find that the corresponding time average, $\langle w_{\text{min}} \rangle = T^{-1} \int_0^T dt w_{\text{min}}(t)$, where $T$ is the time of duration of the experiment, decreases upon increasing $Q_d/Q_c$ while the stochastic fluctuations of $w_{\text{min}}(t)$ remain of similar absolute magnitude. Accordingly, this leads to occasional break-up ($w_{\text{min}} = 0$) of the jet in the oscillating jetting mode.

Additionally, in the jetting mode, we frequently observe abrupt granular "discharge" of the junction, associated with rapid entrance of several droplets in-parallel into the constriction. In order to quantify such avalanche-like behavior we measure the width of the jet $w_0(t)$ precisely at the entrance to the constriction. We find that $w_0(t)$ develops a saw-tooth like profile (Fig. 3b) characteristic of avalanches and previously also observed in sheared foams and dense suspensions [12, 34].

Next, we measure the sizes of the subsequently generated clusters in the dripping and irregular dripping modes (Fig. 3c). Whereas in the former case the clusters are relatively monodisperse (yet much more polydisperse than in dripping of simple viscous fluids), in the latter case we observe recurring peaks in the cluster size corresponding to extremely large clusters. More quantitatively, in the dripping mode the number of grains $N$ in a cluster does not apparently deviate from the Gaussian distribution. The coefficient of variation $CV_N = 19.5\%$ (see Fig. 3d) is significantly larger then in the case with the granular emulsion replaced by the pure oil phase ($CV_{A_{\text{oil}}} = 2.2\%$), yet still moderate. In contrast, in the irregular dripping mode the distribution of cluster sizes $N$ features a long right tail for large $N$ (see Fig. 3e), with $CV_N = 74.3\%$ and a very large skewness, as documented by a Pearson’s moment coefficient of skewness (see SM for a formal definition) $S_N = 3.1$.

We associate the formation of the extremely large clusters in the irregular dripping regime with the emergence of single-file chains of grains within the narrowing, which, once formed, exhibit remarkable stability. In principle, such chains remain stable once the local velocity of the continuous phase around the chain $U_c$ matches the velocity of the grains inside the chain $U_{d,\text{chain}}$, which in turn is set by the rate of feeding of the grains into the orifice (note that this condition also determines the boundary between the dripping and jetting modes). Considering that $U_c = Q_c/[H \times (W - W_{\text{chain}})]$ and $U_{d,\text{chain}} = Q_d/[H \times W_{\text{chain}}]$, where $W_{\text{chain}}$ is the width of the chain, the requirement $U_c = U_{d,\text{chain}}$ leads to the following condition on the matching flow rate of the continuous fluid $Q_{c,\text{match}}$: 

$$Q_{c,\text{match}}/Q_d = W/W_{\text{chain}} - 1$$

We note that this requirement resembles the condition for continuity of soft polymer fibers stretched by an accelerating co-flow, studied by Mercader et al. [35]. In fact, our granular chains resemble semi-solid fibers rather than viscous jets as demonstrated by (i) the lack of the Rayleigh-Plateau instability (typical of viscous jets) [25] and (ii) longitudinal stretching and/or compression of the chain as visualized by droplet deformations within the constriction, see Fig. 4a. We associate such elastic solid-like behavior with a combination of the capillary arrest and deformability of the droplets within the chain.

From the experimentally measured average width of chain $W_{\text{chain}} = 0.68 D_f = 0.253 W$ we obtain $Q_{c,\text{match}}/Q_d = 2.95$. This is close to the value $Q_c/Q_d = 2$ corresponding to the oscillating jetting regime; however, we actually observe single-file chains more often when $Q_c/Q_d = 8$, in the irregular dripping mode. We suspect that the relative scarcity of single-file chains for $Q_c/Q_d = 2$ results from spontaneous "folding" of single-file chains into wider jets in the immediate vicinity of the theoretical matching velocity $U_{d,\text{chain}}$ (see SM2, frames 51-72, 145-164, 670-691). At the same time, due to the finite length of the orifice $L$, chains are able to survive
extensional stresses at $Q_c \gtrsim Q_{c, \text{match}}$ which may explain their abundance at $Q_c/Q_d = 8$.

We note that even at matched velocities the chains can break due to irregularity of the grain feeding into the orifice associated with stochasticity of grain rearrangements upon approaching the constriction. When a pair of grains enter the narrowing simultaneously they may rearrange, or 'unfold', into a chain or not- in the latter case entering as a 2-grain cluster or a 'fold' (see Fig. 4). When the fold enters the orifice the continuous phase needs to locally accelerate and pass around it to conserve flux. The increased viscous forces acting at the fold result in chain stretching via longitudinal grain deformation which may eventually cause chain breakup.

Our LB simulations allow us to extract precise information about the velocity gradients within the system and verify this scenario. Indeed, we find progressively increasing velocity gradients around the doublet (see the purple marker in the last snapshot of Fig. 4b). We propose that a similar mechanism (i.e., the acceleration of the continuous phase around wider parts of the jet) might also lead to the enhancement of fluctuations of jet width in the jetting and the oscillating jetting modes.

Next, we also perform a series of experiments with a smaller width of the orifice ($W \lesssim D_0$), for which a simultaneous entry of two grains into the narrowing is hindered (see SM for details). In this case, the complex dynamical picture is lost and we only observe a transition between single-file jetting and dripping. To provide an example, we quantify the cluster size distribution in this geometry in Fig. 3f when $Q_c/Q_{c, \text{match}}$ (which serves as a measure of proximity to the jetting-dripping transition) is almost identical as in the long-tailed irregular dripping mode (Fig. 3e). We still observe strong polydispersity ($CV_N = 44\%$), however, no long tails ($S_N = 0.73$). This further confirms the impact of individual grain rearrangements and, more specifically, the manner in which the grains enter the constriction, on the fate of the entire system, including the large-scale stochastic behavior.

Finally, we provide an example of how granular rearrangements observed in our flow-focusing setup could serve as a 'benchmark' for more complex soft granular flows including confined biological flows. In fact, sequences of cell rearrangements have been previously studied in circulating tumor cell clusters transiting a narrowing channel [20]. Upon approaching a constriction the clusters were often able to unfold into a single-file chain without break-up. In some cases, the order in which the cells approached the narrowing seemed to determine their order of entry, but in some other cases the order was strongly disturbed by cell rearrangements (see Fig. 4c). This is interpreted in [20] as the effect of heterogeneity of cell-cell interactions and polydispersity of cells. However, our experiments demonstrate that even in a homogeneous, monodisperse passive granular system the order of entry is not strictly determined by the order of approach but rather depends on stochastic rearrangements upon entry (see Fig. 4d). Accordingly, we argue that the phenomena reported by Au et al. [20] may result from the immanent irregularity of flow patterns associated with many-body interactions and general stochastic dynamics of soft granular media, and not only from heterogeneity of the grains.

In summary, we develop a model platform to study the behaviour of soft granular media subjected to external flows and demonstrate rich phenomenology including stochastic granular jetting- and dripping-like modes with no counterpart in simple fluids.

We note that series of two (or more) microfluidic junctions have been previously used to produce double-emulsion core-shell droplets with multiple cores [36–42]. A couple of recent works considered cores-in-shell volume fractions high enough (> 80\%) for the double-emulsion drops to be considered soft granular clusters [17, 37, 43, 44]. However, those previous works exploited generation of the clusters via one-by-one feeding of the cores into the shell without actually considering the flow of a soft-granular medium per se. In this Letter, we ar-
gue that the latter poses a completely different problem and involves phenomena not present in simple fluids.

Our findings open up several avenues for future work. First, the full dynamical phase diagram in the 3-dimensional \((Q_c, Q_d, \phi)\)-space including possible hysteretic behavior at transitions between the modes—also depending on the viscosities and interfacial tensions—remains to be established. Second, the statistics of rearrangements between individual grains could be further investigated to shed light on the effective phases of matter (solid- vs fluid-like) occurring in such a system. Finally, our platform could also be further developed to allow tracking of the internal relaxation dynamics of the generated granular clusters. This poses possible significance e.g., to the recovery of tissues after mechanical injury or the dynamics of CTC’s in capillaries during cancer metastasis.

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Supplemental Material for the article Stochastic jetting and dripping in confined soft granular flows

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MATERIALS AND METHODS

All microfluidic channels are fabricated via milling in polycarbonate. Precise parameters of the Newtonian liquids used to formulate the double emulsion: fluorinated fluid FC40 with 1% w/w fluorosurfactant (PFPE-PEG-PFPE [30]) as the continuous phase, a mixture of silicone oil (PMX 200, 5cSt), hexadecane, and the surfactant SPAN80 in w/w proportions 70:30:1 as the middle (lubricating) phase (referred in the main text and further here as ‘oil’), and water dyed with 0.1% w/w Erioglaucine as the innermost ‘grain’ phase. Based on literature values, we estimate the corresponding viscosities to be 4.1, 4.0, and 3.4 mPa s, respectively. The interfacial tensions of the water-oil and oil-external interfaces are 3.4 and 4.9 mN/m, respectively, as measured by pendant drop method.

In LB simulations, the geometrical parameters, expressed in simulation units, are as follows: \(W_0 = L = 280\), \(W = 140\), \(H = 30\), while the total length of the computational domain is 846. The droplets are generated by imposing an internal boundary condition, as proposed in [31]; the volume fraction is estimated as \(\sim 0.75\), with a completely uniform droplet diameter of \(D = 45\) simulation units.

FORMAL DEFINITION OF PEARSON’S COEFFICIENT OF SKEWNESS

The formal definition of the Pearson’s moment coefficient of skewness \(S_X\) for a random variable \(X\) (which we use to quantitatively assess the asymmetry of the measured probability distributions of sizes of granular clusters) is:

\[
S_X = E \left[ \left( \frac{X - \mu_X}{\sigma_X} \right)^3 \right] \tag{1}
\]

Where \(E\) is the expectation value of the expression in the squared parenthesis, while \(\mu_X\) and \(\sigma_X\) are respectively the mean and standard deviation of the variable \(X\).

EXPERIMENTS WITH ALTERNATIVE SYSTEM DIMENSIONS

In order to further verify the role of the formation of 2-grain ‘folds’ upon entry into the orifice in the behavior of the system, we repeat the experiments in an alternative set-up, in which the orifice is narrow enough to prevent the formation of such folds. The microfluidic system is again as in Fig. 1 of the main text, but with the following dimensions modified to the values specified: \(W = 0.2\) mm, \(L = 4\) mm, \(H = 0.18\) mm. Note this means the orifice is now narrower than the diameter of a single grain. As expected, the simultaneous entry of two droplets into the narrowing is now impossible (see Fig. 1 and supporting movies, respectively SM17 for \(Q_c/Q_d=0.4\), SM18 for \(Q_c/Q_d=0.5\), SM19 for \(Q_c/Q_d=0.6\), SM20 for \(Q_c/Q_d=0.8\)). The complex dynamical picture as described in the main text is now lost, with long right tails characteristic of the irregular dripping regime absent; we now observe a simple transition between jetting and dripping upon increasing \(Q_c/Q_d\), with a reduction of cluster size within the dripping regime upon a further increase of \(Q_c/Q_d\).

FLOW FOCUSING OF PURE ‘OIL’

In Fig. 2 we illustrate the effect of granularity on the variation of the areas of formed clusters/drops by com-
paring histograms of $N$ for the emulsion’s granular *dripping* mode (panel c) with histograms of $A_||$ for monodisperse (panel a) and bi-disperse (panel b) dripping modes of the oil itself. The $x$ axes are re-normalised to the mean of the distribution in each case to help visualise relative variations.

**FIG. 2.** Histograms of numbers of grains $N$ in clusters of the emulsion $n(N)$ and of areas $A_||$ of flattened drops of the oil $n(A_||)$, formed during dripping of the emulsion and the pure oil respectively.

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